

OPTIMUM ANAEROBIC DIGESTER LOADING RATE FOR
MAXIMUM METHANE GAS PRODUCTION
FROM SWINE MANURE

By

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PREFACE

This study was concerned with the anaerobic digestion of swine manure. The primary objectives were to determine the optimum digester loading rate of swine manure for maximum methane gas production and to characterize the farm used to supply the manure.

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To my parents, Edward and O'Delle, and my family I dedicate this thesis.

TABLE OF CONTENTS

Chapter	Page
I. INTRODUCTION	1
The Problem	1
Objectives	3
Scope of Study	3
Digestion Study	3
Commercial Operation Characterization	4
Thesis Organization	5
II. LITERATURE REVIEW	6
Fundamentals of Anaerobic Digestion	6
Anaerobic Digestion Applied to the Treatment of Swine Manure	13
III. FACILITIES	27
Swine Production Facilities	27
Building Descriptions	27
Manure Treatment System	32
Anaerobic Digestion Facilities	34
Digestion Chambers	34
Gas Collection and Measurement System	38
Mixing Scheme	42
Temperature Control	42
IV. EXPERIMENTAL PROCEDURE AND MATERIAL	47
Commercial Operation Characterization	47
Digestion Study	49
Study Format	49
Digester Operation	49
Seed Material	49
Feed Material	51
Daily Operating Procedures	53
Gas Sampling Procedure	60
Parameters Monitored	63
V. RESULTS AND DISCUSSION	66
Commercial Operation Characterization	66
Livestock Inventories	66

Chapter	Page
Lagoon System	66
Manure Characterization	69
Discussion of the Commercial Operation	
Characterization	89
Anaerobic Digestion	91
Digester Responses to Five Dilutions of	
Swine Manure	91
Gas Composition	118
Discussion of the Anaerobic Digestion Study	122
VI. SUMMARY AND CONCLUSIONS	126
Summary	126
Conclusions	126
Recommendations for Future Research	128
A SELECTED BIBLIOGRAPHY	130
APPENDIXES	133
APPENDIX A - PARTIAL LISTING OF EQUIPMENT USED IN	
THE ANALYSIS OF MANURE AND DIGESTER	
CHARACTERISTICS	134
APPENDIX B - SUPERNATANT AMMONIA NITROGEN DETERMINATION	
PROCEDURE	139
APPENDIX C - EXPECTED DAILY MANURE PRODUCTION	
CALCULATIONS FOR EACH OF THE FARM'S	
CONFINEMENT BUILDINGS	143
APPENDIX D - MANURE CHARACTERIZATION DATA	146
APPENDIX E - DIGESTER FEED CHARACTERIZATION DATA	150
APPENDIX F - DIGESTER RESPONSE DATA	184
APPENDIX G - PROCEDURE FOR DETERMINING GAS COMPOSITION	
AND GAS COMPOSITION DATA	218
APPENDIX H - STATISTICAL ANALYSES RELATED TO GAS	
COMPOSITION AND LOADING RATE	223
APPENDIX I - SAMPLE CALCULATIONS FOR ADJUSTING DAILY	
GAS PRODUCTION	227
APPENDIX J - STATISTICAL ANALYSES RELATED TO GAS	
PRODUCTION AND LOADING RATE	229

LIST OF TABLES

Table	Page
I. Stimulatory and Inhibitory Concentrations of Alkali and Alkaline-Earth Cations	10
II. Effect on Ammonia Nitrogen on Anaerobic Treatment	11
III. Results Summary of the Swine Manure (Feces) Digestion Study Conducted by Gramms et al. (1971)	16
IV. Results Summary of the Swine Manure (Feces and Urine) Digestion Study Performed by Taiganides (1963)	19
V. Results Summary of the Swine Manure (Feces and Urine) Digestion Study Performed by Schmid and Lipper (1969)	20
VI. Results Summary of the Swine Manure (Feces and Urine) Digestion Study Conducted by Hobson and Shaw (1973)	22
VII. Characteristics of Swine Manure Fed to an On-Farm Anaerobic Digester Reported by Booram et al. (1975)	23
VIII. Approximate Daily Manure Production (Median Value for Undiluted Manure Without Bedding)	26
IX. Analysis Scheme for Manure Characterization	48
X. Format for Investigating Digester Loading Rates	50
XI. Expected Daily Manure Production (Liquid and Solids) for Commercial Farm Characterized	52
XII. Composition of a 1.0 λ Straight Feed Preparation	53
XIII. Analysis Schedule for Parameters Monitored for Each Digestion System	63
XIV. Farm's Monthly Livestock Inventories (January 1976 to November 1976)	67
XV. Farm's Monthly Livestock Sales and Birth Records (January 1976 to November 1976)	68

Table	Page
XVI. Sow and Boar Barn Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	70
XVII. Farrower Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	73
XVIII. Nursery I Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	77
XIX. Nursery II Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	78
XX. Grower Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	84
XXI. Finisher Manure Characterization Results Summary (June 1, 1976 to November 1, 1976)	87
XXII. Data Summary for Digesters Fed the One-Seventh Dilution of Swine Manure	96
XXIII. Data Summary for Digesters Fed the One-Fifth Dilution of Swine Manure	100
XXIV. Data Summary for Digesters Fed the One-Third Dilution of Swine Manure	105
XXV. Data Summary for Digesters Fed the One-Half Dilution of Swine Manure	110
XXVI. Data Summary for Digesters Fed the Straight Swine Manure Suspension	115
XXVII. Summary of the Gas Composition Results	120
XXVIII. Summary of Duncan's New Multiple Range Test of Treatment Means for Percent Methane in the Digester Gas ($\alpha = 0.01$)	120
XXIX. Comparative Summary of Selected Research Data on the Performance of Anaerobic Digesters Fed Swine Manure . . .	124
XXX. Expected Daily Manure Production (Solids and Liquid) Calculations for Each of the Farm's Confinement Buildings	145
XXXI. Retention Times of Common Digester Gases in Gas Chromatograph Column	219
XXXII. Gas Composition Data	222

Table	Page
XXXIII. Analysis of Variance of Effect of Dilution or Loading Rate on Gas Methane Content	224
XXXIV. Analysis of Variance of Regression Equation for Methane Content Versus Daily Loading Rate	226
XXXV. Analysis of Variance of Effect of Dilution or Loading Rate on Total Gas Production	230

LIST OF FIGURES

Figure	Page
1. Methane Gas Production (0°C and 1 atm Pressure) for Various C/N Ratios	17
2. Farm Layout	28
3. Standpipe to Control Measure Level Shown in Position. (Typical)	29
4. Lagoon System Layout	33
5. Schematic Drawing of Anaerobic Digestion System	35
6. Anaerobic Digestion System (Digestion Chamber is Concealed by Temperature Control Bath)	36
7. Digestion Chamber with Rubber Stopper in Place	37
8. Modified 3201 Pony [®] Clamp Used to Seal Access Ports (Pictured in Insets) to Digestion System	39
9. Graduated Glass Collection Cylinders	40
10. Gas Volume Measurement Scheme	41
11. Cole Parmer (115 V, 60 Hz, 17 W, 0.25 A) Oscillating Pump	43
12. Tenny Environmental Stand (Model 6PLB-6050C)	44
13. Sheet Metal Plate Positioned Over Temperature Control Bath	46
14. Liquid in the Aspirator Bottle and Gas Collection Cylinder at Equal Levels for Reading Gas Production	55
15. Positive Pressure Applied to System by Raised Aspirator Bottle	56
16. A Modified 3201 Pony [®] Clamp Applied to the Pump Line Below Tee and 200 ml of Digesting Material Being Removed	57
17. Negative Pressure Applied to System by Lowered Aspirator Bottle and 200 ml of Feed Material Being Added to Digesters	58

Figure	Page
18. Gas Collection System Zeroed After Feeding	59
19. Gas Sampling Cylinder (Typical)	61
20. Positive Pressure Applied to System by Raised Aspirator Bottle and Gas Sample Being Taken	62
21. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Sow and Boar Barn (June 1, 1976 to November 1, 1976)	72
22. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Farrower (June 1, 1976 to November 1, 1976)	74
23. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from Nursery I (June 1, 1976 to November 1, 1976)	79
24. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from Nursery II (June 1, 1976 to November 1, 1976)	81
25. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Grower (June 1, 1976 to November 1, 1976)	85
26. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Finisher (June 1, 1976 to November 1, 1976)	88
27. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Seventh Dilution (March 9, 1976 to May 31, 1976)	93
28. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on One-Seventh Dilution (March 9, 1976 to May 31, 1976)	94
29. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the One-Seventh Dilution (June 10, 1976 to November 15, 1976) . .	95
30. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Fifth Dilution (June 10, 1976 to August 11, 1976)	98
31. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Fifth Dilution (August 20, 1976 to November 15, 1976) . .	99

Figure	Page
32. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Third Dilution (March 9, 1976 to May 31, 1976)	102
33. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Third Dilution (March 9, 1976 to May 31, 1976)	103
34. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the One-Third Dilution (June 10, 1976 to November 15, 1976)	104
35. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Half Dilution (June 10, 1976 to August 11, 1976)	108
36. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Half Dilution (August 20, 1976 to November 15, 1976)	109
37. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the Straight Dilution (March 24, 1976 to May 31, 1976)	112
38. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the Straight Dilution (March 9, 1976 to May 31, 1976)	113
39. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the Straight Dilution (June 10, 1976 to October 7, 1976)	114
40. Methane Content Versus Daily Loading Rate	121
41. Average Daily Gas Production (24°C) Versus Average Daily Loading Rate	123
42. Block Diagram of LKB-9000(P) Gas Chromatograph-Mass Spectrometer	136
43. Standard Curve--Absorbance (615 nm) Versus NH_4^+ - N Concentration	141
44. Typical Chromatogram for a Sample of Digester Gas	220
45. Characteristic Mass Spectrometer Readout for a Sample of Digester Gas	221

LIST OF SYMBOLS

- ADGP = Average daily gas production (24°C), ℓ /1000 mg TS of digester
- ADLR = Average daily loading rate, mg TS of digester
- AGP = Adjusted gas production
- ALK = Alkalinity, mg/ ℓ as CaCO_3
- AMMON = Ammonia nitrogen, mg/ ℓ as NH_4^+
- ANIT = Ammonia nitrogen, mg/ ℓ as N
- BOD = Biochemical oxygen demand
- C = Carbon
- CaCO_3 = Calcium carbonate
- CH_4 = Methane
- CH_3COOH = Acetic acid
- CO_2 = Carbon dioxide
- COD = Chemical oxygen demand
- COD MLSS = Chemical oxygen demand of mixed liquor suspended solids suspension, mg/ ℓ
- COD SP = Chemical oxygen demand of supernatant, mg/ ℓ
- DLR = Daily loading rate, mg TS/ ℓ of digester
- DS = Dissolved solids, mg/ ℓ
- DT = Detention time
- GAS = Total daily gas production (24°C), ml/4 ℓ of digester
- H = Hydrogen
- HAc = Acetic acid

HCO_3^- = Carbonate
 H_2CO_3 = Bicarbonate
 H_2O = Water
 H_2S = Hydrogen sulfide
MC = Methane content, %
N = Nitrogen
 NH_3 = Ammonia nitrogen
 NH_4^+ = Ammonium nitrogen
 NH_4^+ - N = Ammonia nitrogen concentration, mg/l as N
 NO_3^- = Nitrate
O = Oxygen
OH = Hydroxide
S = Sulfur
SS = Suspended solids, mg/l
 SO_4^{2-} = Sulfate
TEMP = Temperature, °C
 θ_C^M = Minimum mean cell residence time, days
TOC = Total organic carbon
TS = Total solids, mg/l
TVS = Total volatile solids, mg/l
UVA = Un-ionized volatile acids
VA = Volatile acids, mg/l as HAC
VDS = Volatile dissolved solids, mg/l
VS = Volatile solids, mg/l
VSS = Volatile suspended solids, mg/l

CHAPTER I

INTRODUCTION

The Problem

The present trend in the United States swine industry is towards more concentrated production using partial or total confinement housing. Confinement housing provides producers the means to closely regulate growing conditions.

Intensive animal production currently has two major problems: (1) manure treatment and/or disposal and (2) odor abatement. Separating animal and feed production operations has reduced access, in some cases, to ample acreage for the land disposal of manure. Land disposal is further hampered because the pollution potential to ground and surface waters exists. The odor problem is mainly due to increased urban expansion in close proximity to farm production units.

Increasing energy needs coupled with the need to treat manure has renewed interest in the anaerobic digestion process. Low cost petroleum energy for fuel and agri-chemicals is no longer available. Swine utilize 4,056 kcal of the available 5,553 kcal in a 1.0 kg corn ration (dry basis) (National Academy of Sciences, 1969). Therefore, the manure excreted has chemically stored energy. The anaerobic process affords a means to partially harvest biologically the chemical energy remaining in the manure. At the same time, manure's environmentally offensive nature

is reduced.

Advantages of the anaerobic process are:

1. The partial reduction and stabilization of the manure's organic content.
2. The production of a combustible gas having commercial value.
3. The reduction of odors.
4. The conservation of the raw manure's fertilizer constituents.

Disadvantages of the anaerobic process are:

1. The high initial investment for equipment.
2. The requirement of daily feeding, maintenance, and supervision.
3. The requirement for the additional treatment of digested material prior to final disposal.

The anaerobic process is applied in the United States as a domestic waste sludge treatment. Domestic waste sludge and animal manure are characteristically different. Domestic waste sludge is an aerobic biological treatment product. The aerobic process converts soluble nutrients in relatively dilute domestic wastes to biomass. The biomass is separated from the water flow and concentrated for further treatment. Anaerobic digestion is one process applied to treat the concentrated biomass.

Animal manure, in comparison, is a concentrated material having a high solids content. Manure contains compounds not readily biologically degraded such as cellulose, grain particles, and hair.

Numerous digestion studies conducted with various swine feces loading rates indicated treatability. However, similar studies feeding feces and urine combined experienced digester failure (limited methane production) due to ammonia toxicity. The ammonia toxicity was indicated by

the researchers to be due to the inclusion of urine.

Gas production and system stability information is a necessity when determining the economic feasibility of treating manure anaerobically. The existing swine manure anaerobic digestion data are for studies conducted with manure from only grower and finisher buildings. Many swine farms involve all production levels, farrow to finish. The manure (feces and urine) from such a farm better represents the material to be treated in many production situations.

One treatment alternative to overcome ammonia toxicity caused by feces and urine combined is to dilute the manure prior to anaerobic digestion. However, more information is needed on the nature of the combined manure flow from a farrow to finish swine operation and on the recommended practical amount of dilution. The report discusses research to determine the needed information.

Objectives

The research objectives were:

1. To determine the swine manure dilution required to maximize methane production and minimize ammonia toxicity. The swine manure (feces and urine) was obtained from a commercial swine operation, farrowing through finishing.
2. To characterize the commercial swine farm used for the source of digester feed material.

Scope of Study

Digestion Study

The study monitored the response of completely mixed bench scale

batch fed anaerobic digesters to different swine manure dilutions. Digester detention time and temperature were held constant. The feed material was obtained from a total confinement farm, including all levels of swine production farrowing through finishing.

Preliminary studies were conducted to evaluate the physical setup of the digesters and to obtain experience operating the digester and performing the required analyses. Details of the preliminary studies are not presented in this report.

The study investigated five dilutions of a manure preparation representing the farm's daily manure production. Manure collected from the farm's finishing barn was also fed to one series of digesters. Two to three replications of each loading rate were performed. The digesters were maintained for extended periods of time to obtain indications of each system's stability. The parameters monitored included pH, alkalinity, temperature, solids, COD (chemical oxygen demand), soluble $\text{NH}_4^+\text{-N}$ (ammonia nitrogen), VA (volatile acids), and gas volume and composition.

Gas production, gas composition and system stability were evaluated to determine if an optimum loading rate existed.

Commercial Operation Characterization

The commercial operation characterization study focused on factors affecting the volume, characteristics, and treatability of the manure produced. The information compiled included farm layout, yearly production, building description, herd size, feed rations, medications, management practices, and manure collection and treatment systems. Swine manure produced at each production level, farrow to finish, was

characterized. Parameters monitored included pH, COD, soluble $\text{NH}_4^+\text{-N}$, and solids.

Thesis Organization

The review of literature in Chapter II covers information on the fundamentals of anaerobic digestion and on the applications of anaerobic digestion to treating swine manure. A detailed description of the digestion system used in the study is presented in Chapter III. Chapter IV outlines the experimental materials and procedures used to characterize the farm and to evaluate the digestion study. Results and discussion of the farm characterization and the digestion study are included in Chapter V. Summary and conclusions of the research information compiled are presented in Chapter VI.

CHAPTER II

LITERATURE REVIEW

Fundamentals of Anaerobic Digestion

Anaerobic digestion is a complex process occurring in two stages: liquefaction or "acid" stage and gasification or "methane" stage. Both stages proceed simultaneously in a balanced system. Extracellular enzymes excreted by "acid formers" hydrolyze complex organic solids: proteins, carbohydrates, and fats, to simpler soluble compounds; peptides and amino acids; sugars and alcohols, and glycerol and fatty acids, respectively. The solubilized compounds, except fatty acids, are fermented by the "acid formers" to volatile acids: (1) acetic, (2) butyric and (3) propionic acids, primarily. The "acid formers", except for a few strict anaerobes, are facultative bacteria. The bacteria grow readily with relatively little sensitivity to environmental changes (McKinney, 1962; McCarty, 1964a).

The "methane formers" metabolize the volatile and fatty acids to methane (CH_4) and carbon dioxide (CO_2). Unlike the "acid formers", the methanogenic bacteria are strict anaerobes. Strict anaerobes have slow growth rates and are highly sensitive to environmental changes. Methane is generated primarily by the direct cleavage of acetic acid to methane and carbon dioxide ($\overset{*}{\text{CH}_3}\text{COOH} \rightarrow \overset{*}{\text{CH}_4} + \text{CO}_2$) and the reduction of carbon dioxide ($8[\text{H}] + \text{CO}_2 \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$). Bacteria metabolizing the principle

volatile acids, acetic and propionic acids, have the slowest growth rates (minimum mean cell residence time (θ_C^M) is two to four days) and are considered the rate limiting step in the digestion process (McCarty, 1964a; Jeris and McCarty, 1965).

The energy present in organic substrates is released by successive biological dehydrogenations of carbon chains. The hydrogen atoms thus removed are transferred to a final acceptor. The chemical transfer of the hydrogen atoms to the final acceptor releases energy for other biological activities. The anaerobic process is a hydrogen acceptor (energy) limited system and as a result the bacterial populations have slow growth rates and low yields (Sawyer and McCarty, 1967; Salle, 1973; Doelle, 1975).

Anaerobic bacterial fermentations primarily utilize portions of the organic substrate as the final hydrogen acceptor. A few facultative bacteria, however, are able to use nitrates as their final electron acceptor ($5H_2 + 2NO_3^- \rightarrow N_2 + 4H_2 + 2OH^-$). Also, the strict anaerobes, Desulforibrio and Methanobacterium, are able to use sulfates ($4H_2 + SO_4^{2-} \rightarrow S^{2-} + 4H_2O$) and carbon dioxide ($8[H] + CO_2 \rightarrow CH_4 + 2H_2O$), respectively as their final hydrogen acceptor (Sawyer and McCarty, 1967; Salle, 1973; Doelle, 1975).

The anaerobic process achieves optimum substrate conversion to methane if a constant temperature, detention time, and loading rate are maintained. A few degrees rise in temperature does not affect digestion. However, a 3°C temperature decrease will inhibit methane production without substantially affecting the acid producing bacteria, thus leading to excessive acid accumulation and possibly digestion failure. Methane bacteria are active at two temperature ranges: (1) mesophilic

(18° to 45°C, 36°C optimum) and (2) thermophilic (45° to 85°C, 54°C optimum). Digesters, to date, are usually operated in the mesophilic range, 33° to 37°C, even though thermophilic bacteria convert substrate to methane faster. Operation of digesters in the thermophilic range has not been extensive due to: (1) increased bacterial sensitivity to environmental changes, (2) the additional heat requirements, (3) a strong odorous supernatant, and (4) a problem with solids caking on some types of heat exchangers (Buswell, 1947; McKinney, 1962; McCarty, 1964b).

Detention times range between 30 and 90 days for standard rate digesters and between 10 and 30 days for high rate digesters. Complete mixing of digester contents with either mechanical or gas mixer has been in part responsible for shorter detention times. The average detention time for a high rate complete mix digester operated at 35°C is 15 days (McKinney, 1962; Metcalf and Eddy, 1972).

Digester loading rates depend on the type unit, standard or high rate, and on the composition and degradability of the feed material. Standard rate digesters are normally loaded between 480 and 1600 mg VS/ℓ/day. High rate digesters are loaded at rates between 1600 and 6400 mg VS/ℓ/day (Metcalf and Eddy, 1972).

Additional environmental requirements of the anaerobic process are anaerobic conditions, sufficient biological nutrients, suitable pH, and absence of toxic materials. Free oxygen, when present, is toxic to the methane formers and prevents the production of methane. However, once the oxygen is consumed or excluded, the bacteria are able to resume methane production (McCarty, 1964b; Salle, 1973).

The anaerobic bacteria require inorganic nutrients to maintain growth. The primary nutrients needed by the bacteria are nitrogen (11%

of cell volatile weight) and phosphorous (2% of cell volatile weight) plus essential trace elements (McCarty, 1964b).

The anaerobic process functions between pH 6.6 and 7.6 but is optimum between pH 7.0 and 7.2. Within the neutral pH range, the bicarbonate/carbonic acid system ($\text{HCO}_3^-/\text{H}_2\text{CO}_3$) is the major chemical system buffering pH. The equilibrium equation ($\text{H}_2\text{CO}_3 \rightleftharpoons \text{H}^+ + \text{HCO}_3^-$) indicates the system's relation to pH. The carbonic acid concentration is related to the percentage of carbon dioxide in the digester gas. Alkalinity is a measure of the digester's buffering capacity. Alkalinity levels between 2500 and 5000 mg/l as calcium carbonate (CaCO_3) are recommended to buffer digester pH against possible rapid volatile acid production. The methanogenic bacteria are inhibited at pH 6.6 while the acid forming bacteria are not inhibited until pH 5.0. Lack of sufficient alkalinity to buffer rapid increases in volatile acids will result in a drastic pH drop, thus inhibiting the methane formers. However, alkalinities of 10000 mg/l as CaCO_3 or greater are indicative of malfunctioning digesters (McCarty, 1964b; Sawyer and McCarty, 1967; American Public Health Association, 1971).

Alkali and alkaline earths, ammonia, sulfides, and heavy metals are toxic to the anaerobic process. The inhibitory effect of alkali and alkaline salts is normally associated with the cation rather than the anion portion of the salt. Table I lists the cations and the effect various concentrations have on the system. When compared on an equal molar concentration basis, monovalent salts are less toxic than divalent salts. The nature of salt inhibition is quite complex. The effect of combinations of the salts is even more complex due to antagonistic (reduced toxicity) and synergistic (increased toxicity) reactions among

the cations. Salt toxicity treatments are the addition of chloride salts of sodium and potassium as antagonists, and dilution (McCarty and McKinney, 1961; McCarty, 1964c).

TABLE I
STIMULATORY AND INHIBITORY CONCENTRATIONS OF
ALKALI AND ALKALINE-EARTH CATIONS

Cation	Stimulatory mg/l	Moderately Inhibitory mg/l	Strongly Inhibitory mg/l
Sodium	100-200	3500-5500	8000
Potassium	200-400	2500-4500	12000
Calcium	100-200	2500-4500	8000
Magnesium	75-150	1000-1500	3000

Source: McCarty, 1964c.

Ammonia, usually formed from the degradation of proteins and urea, inhibits the anaerobic process at high concentrations. Ammonia can be present either as ammonium ion (NH_4^+) or as dissolved ammonia gas (NH_3). The equilibrium equation, $\text{NH}_4^+ \rightleftharpoons \text{NH}_3 + \text{H}^+$, indicates the relative concentrations of each form is pH dependent. At pH 7.2 or less the process inhibition is related to NH_4^+ concentration. Above pH 7.2, the NH_3 concentration is the cause of inhibition. Ammonia gas inhibits at lower concentrations than does the ammonium ion. Table II presents ranges of ammonia concentration, ion and gas combined, and the effect each range

has on the anaerobic system. Recommended treatments to overcome ammonia toxicity are dilution and the removal of the source from the digester feed (Albertson, 1961; McCarty, 1964c).

TABLE II
EFFECT OF AMMONIA NITROGEN ON
ANAEROBIC TREATMENT

Ammonia Nitrogen Concentration mg/l	Effect on Anaerobic Treatment
50-200	Beneficial
200-1000	No adverse effect
1500-3000	Inhibitory at higher pH values
Above 3000	Toxic

Source: McCarty, 1964c.

Sulfides resulting either from direct introduction into the system as part of the waste stream or as a product of biological sulfate reduction can be toxic to the anaerobic process. Sulfides are either soluble or insoluble depending on the associated cation. Soluble sulfides are toxic to the anaerobic system. The system can tolerate soluble sulfide concentration varying from 50 to 100 mg/l without acclimation and concentrations up to 200 mg/l in a continuously fed digester with some acclimation. Soluble sulfide concentrations above 200 mg/l are toxic. Gas scrubbing, dilution, precipitation with iron salts, or removal of the

sulfate stream from the stream to be treated are recommended treatments to reduce sulfide toxicity (McCarty, 1964c).

Soluble heavy metal salts of copper, zinc, and nickel are toxic to the anaerobic system even at low concentrations. Sodium sulfide or reducible sulfate salt additions to precipitate the heavy metal is the recommended treatment to remove heavy metal toxicity (McCarty, 1964c).

Waste stabilization, COD reduction, in the anaerobic process is related directly to methane production. The CH_4/COD relationship is expressed by the formula: $\text{CH}_4 + 2\text{O}_2 \rightarrow \text{CO}_2 + 2\text{H}_2\text{O}$. The formula shows one mole of methane is equivalent to two moles of oxygen or 1.0 mg of stabilized COD equals 0.37 ml of methane at 20°C and 760 mm Hg pressure. Digester gas (60% CH_4 /40% CO_2) has a 22.4 Joule (J)/ml calorific value at 20°C and 760 mm Hg pressure (McCarty, 1964a; Smith and Miner, 1975).

Waste stabilization efficiency in a completely mixed digester is equal to effluent COD divided by influent COD. Efficiencies are normally between 0.60 and 0.90 under satisfactory operating conditions. A digester operating at less than normal efficiency is considered unbalanced. Unbalanced conditions can be either temporary or prolonged in character. Temporary digester unbalances are generally due to a sudden change in temperature, loading, or feed composition. Prolonged digester unbalances are caused by the presence of toxic materials, an extreme drop in pH, or slow bacterial growth during startup. The digester will become "stuck" unless factors causing the unbalance are corrected. A stuck digester is defined as a digester whose waste stabilization efficiency is almost zero. A digester, once stuck, is difficult to restart (McCarty, 1964a).

The onset of digester unbalance is indicated by increases in volatile acids concentration and carbon dioxide percentage in gas, and decreases in pH, total gas production, and waste stabilization. Although no single parameter exclusively denotes the onset of unbalance, volatile acids concentration is the best individual parameter. The accumulation of volatile acids means the methane formers are inhibited in their conversion of volatile acids to methane and carbon dioxide. A high volatile acid concentration is the result and not the cause of unbalanced treatment. Digesters have been operated with good gas production at 20000 mg/l volatile acids concentration provided pH was maintained above 6.5 (McKinney, 1962; McCarty, 1964b).

A balanced anaerobic digester produces a gas containing 25 to 35% carbon dioxide, 65 to 75% methane, and possibly small amounts of ammonia, hydrogen, sulfide, nitrogen and oxygen. An increased carbon dioxide percentage results when methanogenic bacteria fail to convert the volatile acids to methane (Eckenfelder and O'Connor, 1961).

Anaerobic Digestion Applied to the Treatment of Swine Manure

Prior to 1940, American agriculture produced livestock on the open range where manure disposal was not a problem. But during the 1940's, the American farmer began to shift from the open range system to partial or total confinement animal production systems. The confinement systems produce large volumes of manure requiring treatment and/or disposal. Anaerobic digestion is one possible treatment (Shindala and Scarbrough, 1971). However, the application of anaerobic digestion to treat concentrated animal manure is relatively new and has received only limited

acceptance in the United States (Metcalf and Eddy, 1972; Merrill and Merrill, 1973).

Laboratory scale anaerobic digesters have been operated at different loading rates, temperatures, and detention times to determine process response and limitations to the swine manure substrate. Jeffery et al. (1965), using feces and loading digesters at three rates--2500, 2800, and 3100 mg volatile solids (VS) per ℓ per day (mg/ ℓ /day)--researched the effects of loading on the digestion process. Their digesters were operated at a 20-day detention time and 35°C, and depended on rising gas bubbles for mixing. The volatile acids concentration and pH for the digesters loaded at the two lower rates were 126 to 154 mg/ ℓ as acetic acid (HAc) and 7.4, respectively. Their results indicated loadings in excess of 2800 mg VS/ ℓ /day resulted in digester failure.

Cross and Duran (1970), feeding feces, investigated (using a factorial design) digester response to three temperatures (10°, 21°, and 32°C) and three loading rates (800, 1600, and 3200 mg VS/ ℓ /day). Their digesters were operated at a 15-day detention time and depended on rising gas bubbles for mixing. The hogs were fed a corn and milo ration at the time feces were collected. Cross and Duran (1970) could not explicitly evaluate each digester's performance due to the short duration of run. Therefore, evaluation of the results by the researchers was restricted to the tendency of each digester towards success or failure based on solids removal performance. The digesters tending towards success were those operating with a 800 mg VS/ ℓ /day loading rate at all three temperatures and a 1600 mg VS/ ℓ /day loading rate at the 32°C temperature. All other temperature-loading combinations tended towards digester failure. The authors reported no gas production data.

Gramms et al. (1971), also using feces, studied factorially the effects of loading (1900 and 3800 mg VS/ℓ/day) and detention time (10 and 15 days) on the digestion process. Their digesters were maintained at 32.5°C and mixed once or twice daily. Table III shows a summary of their results. Gramms et al. (1971) concluded digesters operated at a 3800 mg VS/ℓ/day loading, 32.5°C temperature, and 10 and 15 days detention time achieved satisfactory reductions in VS and COD.

Sievers and Brune (1976) studied factorially the effects of loading rate (1120, 2240, and 4000 mg VS/ℓ/day) and feed carbon-nitrogen ratio (C/N) (2/1, 6/1, 16/1, 20/1, and 25/1 mg/mg) on the digestion process. The authors adjusted the C/N ratio of the feces fed by adding either glucose or urea. Their digesters were operated at a 15-day detention time and 35°C, and were mixed prior to and after each feeding. A rise in organic acids and a decline in buffer capacity inhibited the methane producing organisms at the high C/N ratios, 20/1 and 25/1, even though sufficient nitrogen was available for metabolism. Digesters operated at 2/1 C/N ratio failed due to ammonia toxicity. The high ammonium levels developed at the 6/1 C/N ratio tended to stabilize conditions as the digesters became highly buffered. However, gas production was inhibited at the 6/1 C/N ratio. Maximum methane production was obtained between 9/1 and 16/1 C/N ratio for all three loadings (Figure 1) and corresponded to a 55 to 60% reduction in total organic carbon (TOC). Sievers and Brune (1976) indicated the range of optimum C/N ratios narrowed as the loading rate increased. The authors also concluded un-ionized volatile acid (UVA) and ammonia (NH₃) appeared to inhibit gas production in an additive manner.

TABLE III

RESULTS SUMMARY OF THE SWINE MANURE (FECES) DIGESTION STUDY
CONDUCTED BY GRAMMS ET AL. (1971)

Parameter				
<u>Loadings:</u>				
VS (mg/ℓ/day)	1900	1900	3800	3800
Detention time (days)	10	15	10	15
Temperature (°C)	32.5	32.5	32.5	32.5
<u>Digester Influent:</u>				
VS (mg/ℓ)	19200	28800	38400	57600
COD (mg/ℓ--average)	23300	35000	46600	70000
NH ₃ + NH ₄ ⁺ - N (mg/ℓ as N)	190	285	380	570
Organic - N (mg/ℓ)	700	1050	1400	2100
Alkalinity (mg/ℓ as CaCO ₃)	1670	2500	3340	5000
pH	7.0	6.9	7.0	6.9
% VS	83.4	83.4	83.4	83.4
<u>Operating Conditions:</u>				
Gas (ml/ℓ of digester/day)	500	780	1560	1630
CO ₂ /CH ₄	0.64	0.67	0.72	0.69
VA (mg/ℓ as HAc)	1090	200	1080	290
Alkalinity (mg/ℓ as CaCO ₃)	2960	4440	6330	7130
pH	6.76	7.14	7.17	7.27
<u>Digester Effluent:</u>				
VS reduction, %	51.6 ± 3.7	60.9 ± 2.9	49.2 ± 2.6	59.2 ± 2.3
COD reduction, %	33.7 ± 9.9	54.6 ± 6.3	35.5 ± 4.1	41.8 ± 10.5
Gas (ml/mg VS removed/day)	490	690	830	760
(NH ₃ + NH ₄ ⁺) - N (mg/ℓ as N)	450	594	730	1010
Organic - N (mg/ℓ as N)	440	674	1000	1244

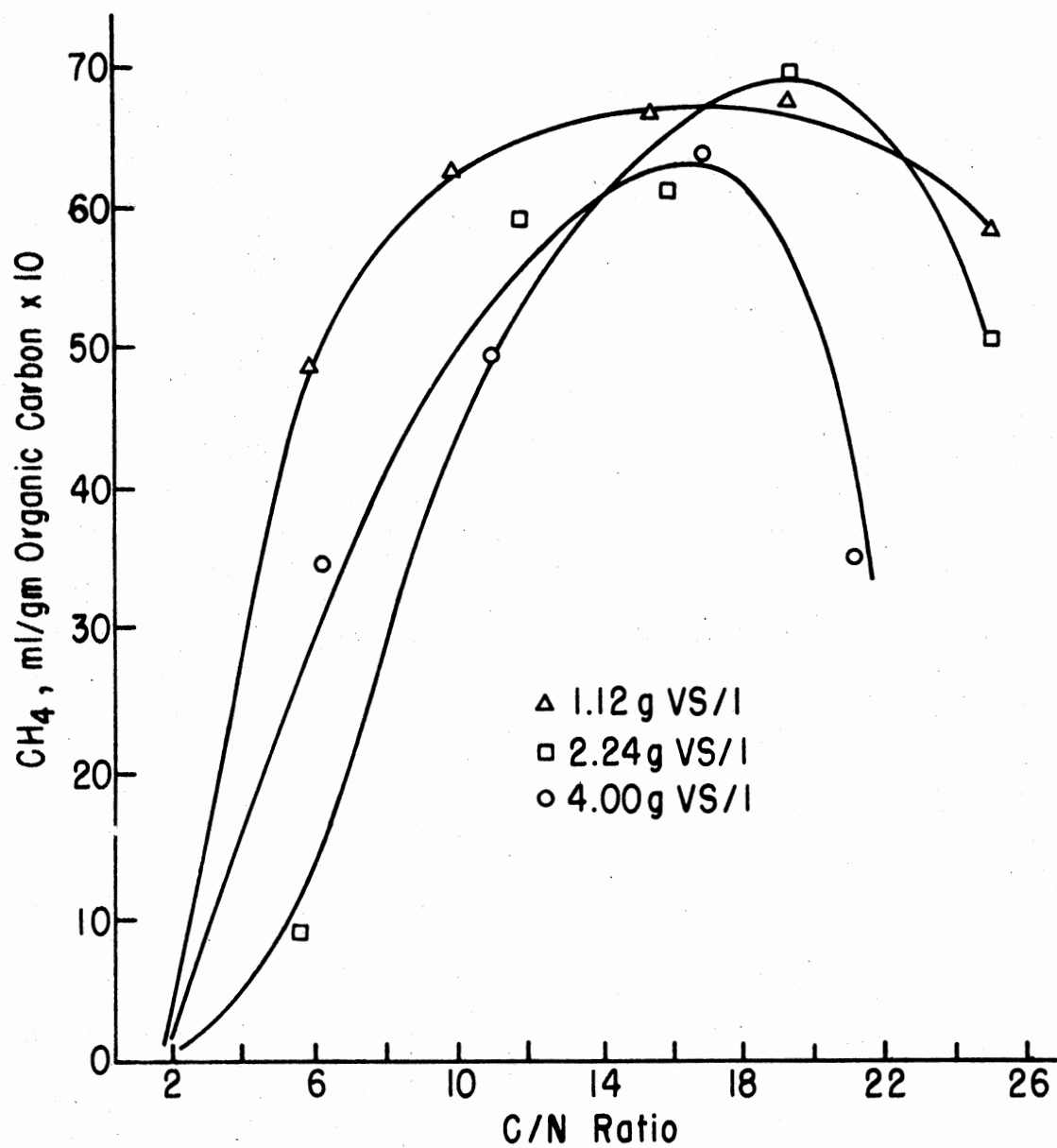


Figure 1. Methane Gas Production (0°C and 1 atm Pressure) for Various C/N Ratios

Taiganides (1963), feeding feces and urine, investigated the effects of loading rate and detention time on the anaerobic digestion process. He operated the digesters at 34°C and mixed contents continuously. Results of the study are summarized in Table IV. Taiganides (1963) indicated digesters operated at loading rates of 400, 960, and 1200 mg VS/l/day and detention times of 48, 25 and 22 days, respectively, exhibited satisfactory performance. However, the other three loading rate-detention time combinations resulted ultimately in digester failure.

Schmid and Lipper (1969) studied the effects of temperature (20 and 35°C), detention time (10 and 20 days), and mixing (continuous and 15 minutes mixing each four-hour period) on the digestion process. They fed digesters with feces and urine collected from hogs fed a 17% protein ration (sorghum and soybean). Results of the study are summarized in Table V. Because the digester with periodic mixing showed no significant difference from the unit with continuous mixing at the same organic loading, the authors included only the data for the continuously mixed digester. Schmid and Lipper (1969) reported digester failure (limited methane production) at all levels due to ammonia toxicity, possibly resulting from inclusion of urine. They concluded manure liquification would occur satisfactorily at ambient temperatures and short detention time.

Hobson and Shaw (1973), also feeding feces and urine, studied the effects of starting procedures (seeded versus unseeded) and loading rate on digester response. Their digesters were operated at a 35°C and a 14-day detention time except for the lowest loading rate when they used a 19-day detention time. The starting procedures tested by the researchers included initiation of digestion with seed from a domestic sludge

TABLE IV
RESULTS SUMMARY OF THE SWINE MANURE (FECES AND URINE) DIGESTION STUDY
PERFORMED BY TAIGANIDES (1963)

Parameter							
<u>Loadings:</u>							
VS (mg/ℓ/day)	400	960	1200	1800	1900	1900	
Detention time (days)	48	25	22	37	25	40	
Duration (days)	40	30	110	35	40	20	
Temperature (°C)	34	34	34	34	34	34	
<u>Operating Conditions:</u>							
CO ₂ /CH ₄	1.0	--	0.69	0.69	0.69	0.69	
VA (mg/ℓ as HAc)	1200	800	1500	800	800	800	
				rising	rising	rising	
				to	to	to	
				3400	3200	2800	
Alkalinity (mg/ℓ as CaCO ₃)	6800	6800	6800	6800	6800	6800	
pH	7.4	7.2	7.4	7.4	7.4	7.4	
<u>Digester Effluent:</u>							
VS reduction, %	43	41	47	52	54	54	
Gas (ml/mg VS removed)	1.47	1.41	1.23	1.09	1.01	1.05	
(NH ₃ + NH ₄ ⁺) - N (mg/ℓ as N)	1200	900	1300	1200	1000	1400	
				rising	rising	rising	
				to	to	to	
				2000	1800	1800	

TABLE V

RESULTS SUMMARY OF THE SWINE MANURE (FECES AND URINE) DIGESTION STUDY
PERFORMED BY SCHMID AND LIPPER (1969)

Parameter				
<u>Loadings:</u>				
VS (mg/l/day)	3200	6400	3200	6400
Detention time (days)	20	10	20	10
Temperature (°C)	35	35	20	20
<u>Operating Conditions:</u>				
Gas (ml/l digester/day)	—	—	—	—
CO ₂ /CH ₄	2.33	2.33		
	rising to	rising to		
	5.67	5.67	5.67	5.67
VA (mg/l as HAc)	16500	19000	16800	17500
Alkalinity (mg/l as CaCO ₃)	10700	11800	15000	15000
pH	6.65	6.65	6.80	6.90
<u>Digester Effluent:</u>				
VS reduction, %	—	—	—	20
(NH ₃ + NH ₄ ⁺) - N	1800	1800	2200	2500

digester and initiation of digestion with swine manure alone. Table VI presents a summary of their results. Hobson and Shaw (1973) concluded digestion could be initiated successfully using either procedure tested, but they indicated the loading rate used initially when starting a digester was a critical factor. The authors reported no digester failures due to ammonia toxicity. However, they did report a decline in digester performance above a loading rate of 2600 mg total solids (TS)/ ℓ /day.

Booram et al. (1975) monitored the response of an on-farm digester to a swine manure substrate. The digester had a 2.4×10^5 ℓ capacity and was operated at a 32-day hydraulic detention time. The digester was fed the combined manure flow from three production units: a 230 boar test unit, a 48 sow farrowing unit, and a 250 animal confinement unit. Table VII presents characteristics of the combined manure flow. The authors reported the actual gas production, 0.08 ℓ/ℓ of digester (maximum), was only 25% of the calculated gas production. The gas produced contained 55% methane. Booram et al. (1975) cited: (1) fluctuating temperatures between 15 and 27°C, (2) slug loading, and (3) large variations in animal population as reasons for the lower than expected gas production.

The research by Jeffery et al. (1965), Cross and Duran (1970), Gramms et al. (1971), and Sievers and Brune (1976) determined swine feces can be anaerobically digested for methane production. Gramms et al. (1971), operating digesters at a 3800 mg VS/ ℓ /day loading rate, 10 and 15 days detention times, and 35°C, reported gas production between 1.5 and 1.6 ℓ/ℓ of digester. The gas produced contained 59 to 61% methane. Schmid and Lipper (1969), however, reported digesters operated under

TABLE VI

RESULTS SUMMARY OF THE SWINE MANURE (FECES AND URINE) DIGESTION STUDY
CONDUCTED BY HOBSON AND SHAW (1973)

Parameter	Seeded					Unseeded				
Loading:										
TS (mg/l/day)	1100	1900	2600	3300	3700	1100	1900	2600	3300	3700
Detention time (days)	19	14	14	14	14	19	14	14	14	14
Temperature (°C)	35	35	35	35	35	35	35	35	35	35
Duration (days)	140	32	35	28	35	70	28	28	28	28
Digester Influent:										
TS (mg/l)	20800	26000	36400	46000	51800	20800	26000	36400	46000	51800
COD (mg/l)	24300	30400	42500	54400	60500	24300	30400	42500	54400	60500
BOD (mg/l)	5400	6700	9500	12100	13400	5400	6700	9500	12100	13400
Operating Conditions:										
Gas (m ³ /l of digester/day)	233	453	660	680	787	287	447	733	880	933
CO ₂ /CH ₄	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67	0.67
VA (mg/l as HAc)	163	216	1530	222	685	581	313	417	220	644
Alkalinity (mg/l as CaCO ₃)	5880	3320	4300	5480	6800	5490	6590	2430	5300	5950
Digester Effluent:										
TS reduction, %	13.0	--	21.0	24.9	14.1	34.0	33.0	26.0	31.3	8.3
COD reduction, %	30.0	23.0	54.0	9.1	18.0	22.0	30.0	31.0	46.0	56.7
BOD reduction, %	74.0	71.0	79.0	24.6	53.4	80.0	82.0	56.0	67.0	59.9
(NH ₃ + NH ₄ ⁺) - N	581	731	1148	1008	1288	580	700	840	1176	1400

TABLE VII
CHARACTERISTICS OF SWINE MANURE FED TO AN ON-FARM ANAEROBIC
DIGESTER REPORTED BY BOORAM ET AL. (1975)

Parameter	Range of Values
Daily flow (l/day)	7560 (approximate)
pH	5.8 to 6.6
(Organic + NH ₃) - N (mg/l)	284 to 1374
TS (mg/l)	3252 to 19184
VS (mg/l)	1740 to 5608
COD (mg/l)	2368 to 8581

similar conditions failed due to ammonia toxicity when fed feces and urine combined. Therefore, if swine manure (feces and urine) is to be digested for methane production, the ammonia toxicity problem must be eliminated. McCarty (1964c) recommended either the removal of the ammonia nitrogen source from the digester feed or dilution as treatment alternatives for ammonia toxicity.

Schmid et al. (1975) investigated desorption as a method to remove toxic ammonia from the anaerobic environment, thereby enhancing the treatability of swine manure (feces and urine) at the higher solids loading rates. The researchers calculated their desorption system could collect 6510 kg of nitrogen from a 2000 head growing and finishing operation when operated at pH 8.0 and 35°C. Their calculations assumed 50% ammonia removal and were based on equations presented by Srinath and Loehr (1974) describing desorption of ammonia from an aqueous solution. Schmid et al. (1975) reported the ammonia gas stripped would be adsorbed into a phosphoric acid solution forming ammonium phosphate, a valuable fertilizer. Due to mechanical problems and short duration of test runs, however, the researchers were unable to evaluate economic feasibility of the system.

The research by Taiganides (1963) and Hobson and Shaw (1973) demonstrated dilution was an effective treatment alternative for eliminating the ammonia toxicity problems reported by Schmid and Lipper (1969). Taiganides (1963) and Hobson and Shaw (1973) indicated manure (feces and urine) can be digested for methane production if digesters are fed at loading rates lower than recommended for feces alone. Hobson and Shaw (1973), operating digesters at 3700 mg TS/ℓ/day (approximately 3100 mg VS/ℓ/day) loading rate, a 14-day detention time, and 35°C,

reported gas production between 0.8 and 0.9 ℓ/ℓ of digester. The gas produced contained 60% methane. The researchers, however, stated digester performance was maximum when digesters were operated at a 2600 mg TS/ ℓ /day (approximately 2200 mg VS/ ℓ /day) loading rate.

Laboratory swine manure digestion research has been conducted with manure collected solely from growing and finishing operations. Many swine operations, however, encompass the entire production spectrum from farrowing to finishing. In addition, the laboratory digesters were fed at constant loading rates. A constant loading rate is inconsistent with what is to be expected under actual on-farm operating conditions. Manure characteristics vary with manure collection methods, production facilities, and farm management practices. Knowledge of the variations occurring in the daily manure production is essential to the engineer when designing a waste treatment system, particularly a biological treatment system such as anaerobic digestion. Average daily manure production values for the various stages of swine growth are readily available in the literature, Table VIII (Muehling, 1969). Taiganides and Hazen (1966) stated the daily quantity of manure varied with the seasons of the year and the status of the animal. They reported the average weight of manure from a 45.4 kg hog will vary from 1.3 to 4.3 kg/day. Booram et al. (1975) demonstrated the adverse effects fluctuations in loading had on methane gas production. Therefore, a waste treatment system when designed must include enough flexibility to withstand variations in manure characteristics without the system failing. However, no data was found for laboratory studies where anaerobic digesters were fed manure (feces and urine) representing the daily flow from a farrow to finish swine production operation.

TABLE VIII
 APPROXIMATE DAILY MANURE PRODUCTION (MEDIAN VALUE FOR
 UNDILUTED MANURE WITHOUT BEDDING)

	Size of Hog		Waste Production	
	Age (wk)	Weight (kg)	Liquid and Solid (ℓ)	Wet Solid Only (kg)
Pigs	6-9	18.2	1.9	1.1
	9-13	45.4	3.8	2.7
	13-18	68.2	6.4	4.0
	18-23	95.4	8.3	5.4
Sows, boars	20-52	136.4	11.3	5.4
	52+	227.3	18.9	13.6
Sow and litter			15.1	13.6

Source: Muehling, 1969.

CHAPTER III

FACILITIES

Swine Production Facilities

The commercial operation characterized includes eight buildings: office and shop, storage, sow and boar barn, farrower, nursery I, nursery II, grower, and finisher on 4.05 ha (see Figure 2 for layout). Information presented on the commercial operation is based on personal communication with herdsman Edwards (1975-1976) and personal observations.

The farm's yearly production ranges between 5500 and 6400 head, 60% for slaughter and 40% for breeding. The farm maintains an average population of 3860 head (198000 kg, live weight). All feed preparations are purchased in bulk form from local mills.

The animals are grown on aluminum slotted floors with manure collection pits located below. Animal activity and urine force manure through slotted floor to the pit. The pits were designed by the owner to be drained on a six to eight week staggered schedule to lagoons for treatment. Manure levels in the pits are controlled by standpipes (Figure 3).

Building Descriptions

Office and Shop. The office building includes an office for business transactions and production records, restroom facilities, a shop area for farm maintenance, and a small nursery. The nursery has a 54

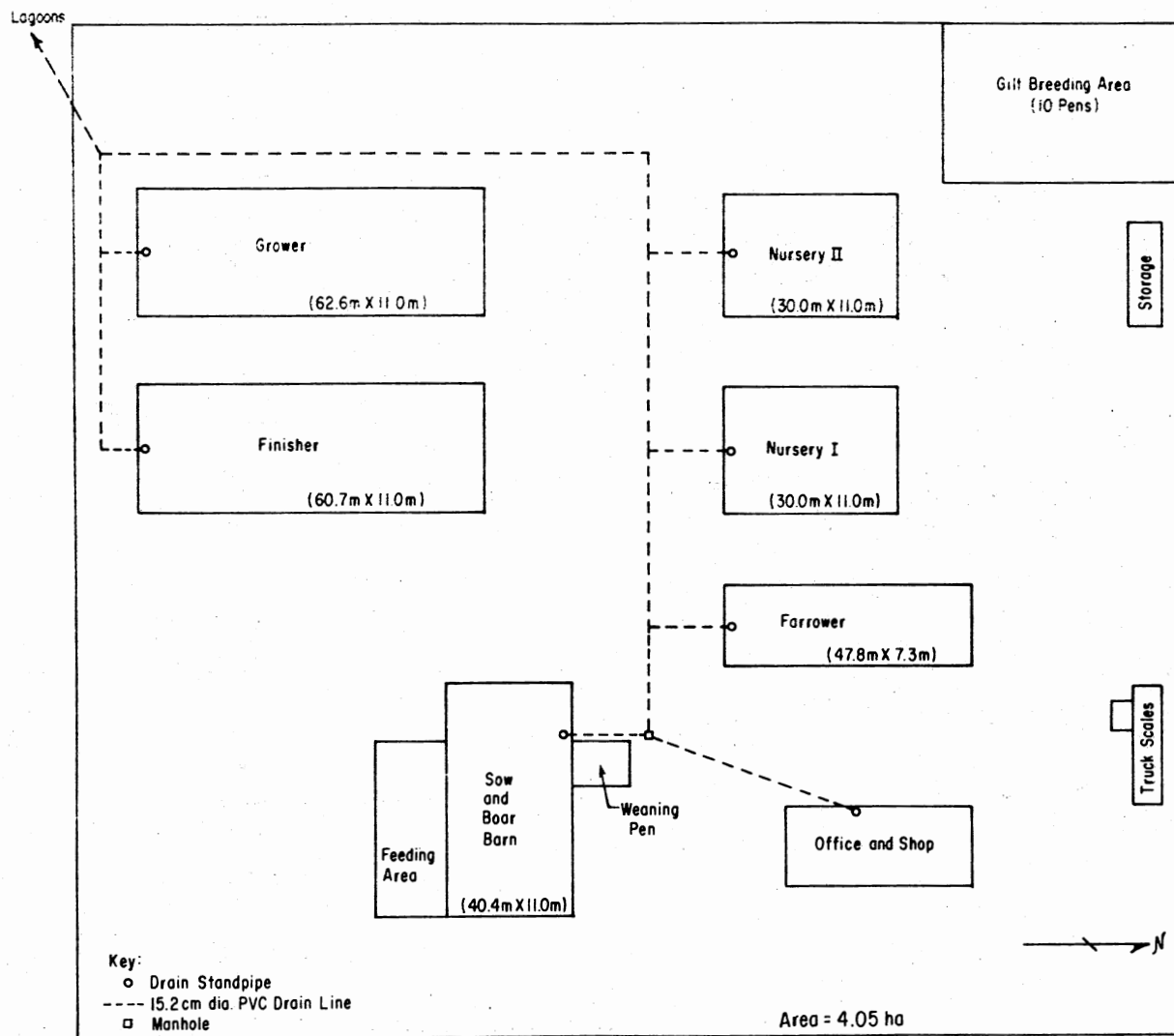


Figure 2. Farm Layout

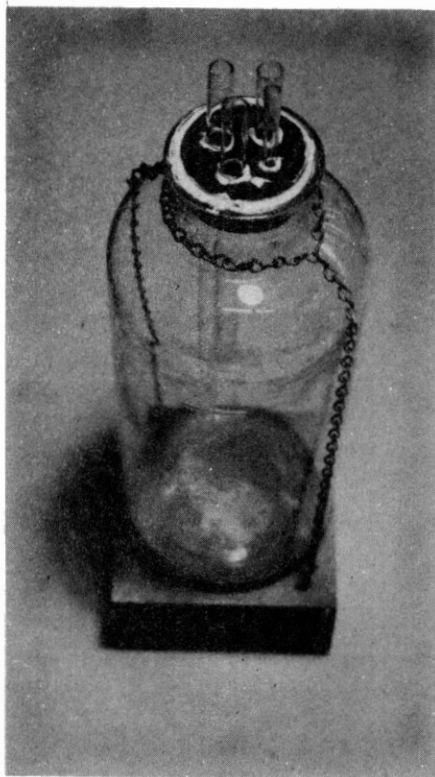


Figure 3. Standpipe to Control Measure
Level Shown in Position
(Typical)

head capacity and is for pigs weighing between 0.9 and 8.2 kg requiring special care.

Storage. The storage structure, an old box car, provides storage area for feed and bedding used for gestating gilts maintained on nearby dirt lots.

Sow and Boar Barn. The sow and boar barn is divided into 11 holding pens and six breeding stalls. The stalls are at the building's west end. The floor under the stalls is half slotted floor and half dirt.

The building houses 18 to 24 boars and 250 to 300 sows and gilts. The animals weigh between 159.1 and 204.5 kg. The water supply, typical of all buildings, is a gravity flow system to MonValv[®] watering nozzles. The animals consume, on the average, 5.4 kg per head per feeding period of a 14% protein ration (corn and soybean) containing alfalfa meal for bulk. A feeding period is two hours every other day.

The feeding area is a concrete slab adjacent to the barn on the south side. The fenced area is divided into four sections. Only animals from one holding pen occupy a feed section at a time. The slab is sloped so manure washed away by rain is collected in the pit.

A weaning pen on dirt is adjacent to the northwest corner of the barn. The pen holds an average of 16 sows for five days before the sows re-enter the barn.

Ten dirt lot pens on the farm's northwest corner confine gilts during gestation. The herdsman moves the gilts back to the sow barn one month prior to farrowing.

Farrower. The farrowing building is divided into three rooms

containing 16 pens each. The building houses 48 sows and 360 nursing pigs. The average weight of the sows and pigs is 159.0 kg and 1.8 kg, respectively. The herdsman moves the sows to the farrower two to three days prior to farrowing. The sows consume 1.4 to 1.8 kg per head of a 14% protein ration (corn and soybean) twice daily. The ration includes alfalfa for bulk and the medication Furox for uterine infection control.

The herdsman, two days after farrowing, castrates, removes tails, clips needle teeth, and gives iron and combiotic (penicillin and streptomycin) shots to the pigs. The pigs remain in the farrower for two to three weeks.

The herdsman washes the farrowing rooms in rotation, one per week, in preparation for the next group of sows. The room is initially wet down using an ordinary lawn sprinkler (0.52 l/s) for 8 to 12 hours. The wet down is followed by hand scrubbing of pens with an iodine solution and a high pressure spray rinse (0.11 l/s). The scrub and rinse take approximately three hours to complete.

Nursery I and II. The two nurseries are identical to each other in layout and construction. Each is divided into three rooms containing 16 pens per room. The nurseries house 48 sows, 360 nursing pigs, and 500 to 600 weaned pigs. The average weight of the sows, nursing pigs, and weaned pigs is 159.0 kg, 5.0 kg, and 15.9 kg, respectively. The herdsman moves the sow and nursing pigs to the nursery during the second or third week after farrowing. The sows get the same ration that is fed in the farrower.

The pigs are weaned during the fourth to fifth week after farrowing. The weaned pigs consume 0.9 to 1.4 kg per head per day of a 22% high protein creep ration (corn and soybean). The ration includes the

medication Mecadox for worm control. The pigs remain in the nursery until the tenth week.

The herdsman washes the six nursery rooms in rotation, one room per week, following the same procedures outlined for the farrower.

Grower. The grower is divided into four rooms containing 12 pens each. The building houses 1400 to 1500 animals having an average weight of 36.4 kg. The herdsman moves the pigs to the grower the tenth week after farrowing. The pigs remain in the grower until 16 weeks old. The animals consume 1.4 to 2.7 kg per head per day of 16% protein ration (corn and soybean).

Finisher. The finisher is divided into two rooms containing 12 pens each. The building houses 650 to 750 head having an average weight of 91.0 kg. The animals consume 2.7 to 3.6 kg per head per day of a 15% protein ration (corn and soybean). The herdsman moves the animals to the finisher during the sixteenth week after farrowing. The duration of the animal's confinement in the finisher varies from 26 to 36 weeks. The period of confinement is affected by market demand and market price.

Manure Treatment System

A two lagoon system retains the manure from the production facilities. The lagoons are on 2.02 ha adjacent to the southwest corner of the farm. Each lagoon has a surface area of 0.405 ha, a liquid depth of about 2.2 m, and side slopes of three horizontal to one vertical. The influent enters the system on the north side of the lagoon closest to the farm (Figure 4) through a single 15.9 cm diameter PVC pipe.

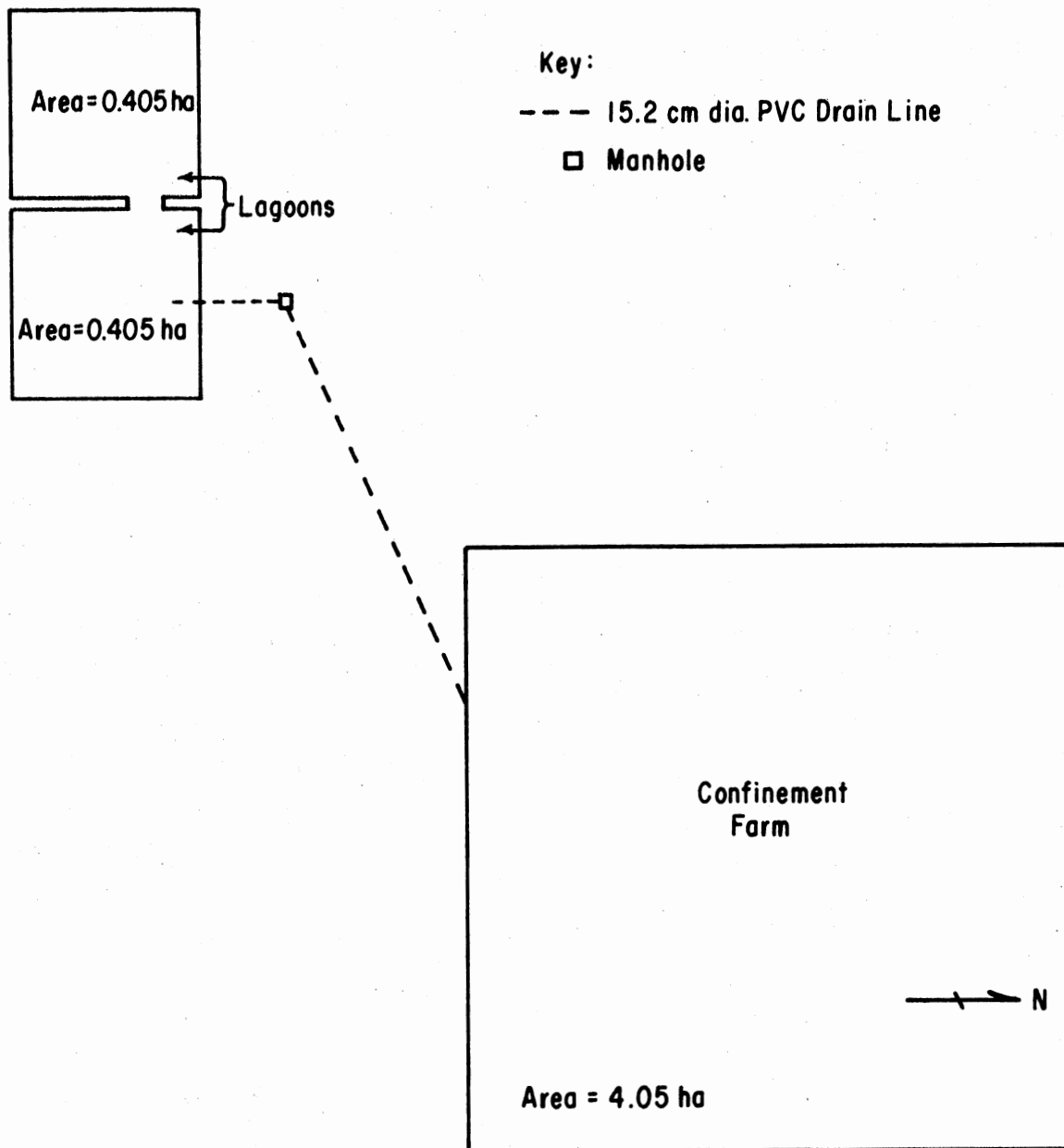


Figure 4. Lagoon System Layout

Initially, one lagoon was used for primary treatment and the second lagoon for secondary treatment. The system did not perform as intended and there was an odor problem. Therefore, the owners made a cut in the dike between the lagoons to in effect make them a single lagoon. The cut was made by a backhoe with the cut size limited to the backhoe's reach. The resulting cut was about 1.2 m deep by about 1.8 m wide. The dike separating the lagoons had a top width of approximately three meters.

Anaerobic Digestion Facilities

Six identical completely mixed bench scale, batch fed anaerobic digesters were operated simultaneously. Figure 5 presents a schematic diagram of the anaerobic digestion system used in the study. Figure 6 shows the actual anaerobic digestion system used in the study.

Digestion Chambers

The chambers were wide mouth solution bottles, 34.6 x 16.4 cm having approximately 4.3 l capacity (Figure 7). The solution bottles were sealed with number 12 rubber stoppers. Four holes were made in each stopper. The holes were ports for feed inlet, gas outlet, mixing pump intake, and mixing pump return. A silicon rubber compound applied to all glass-rubber interfaces insured an air tight seal.

The feed inlet was a 14.0 cm length of 1.0 cm (ID) glass rod. The inlet dispensed the feed material above the digester's liquid level. A 10.0 cm length of 1.0 cm (ID) latex tubing was attached to the exterior end of the feed inlet. The latex tubing was a flexible coupling between the glass inlet and the funnel used when feeding. A modified 3201 Pony[®]

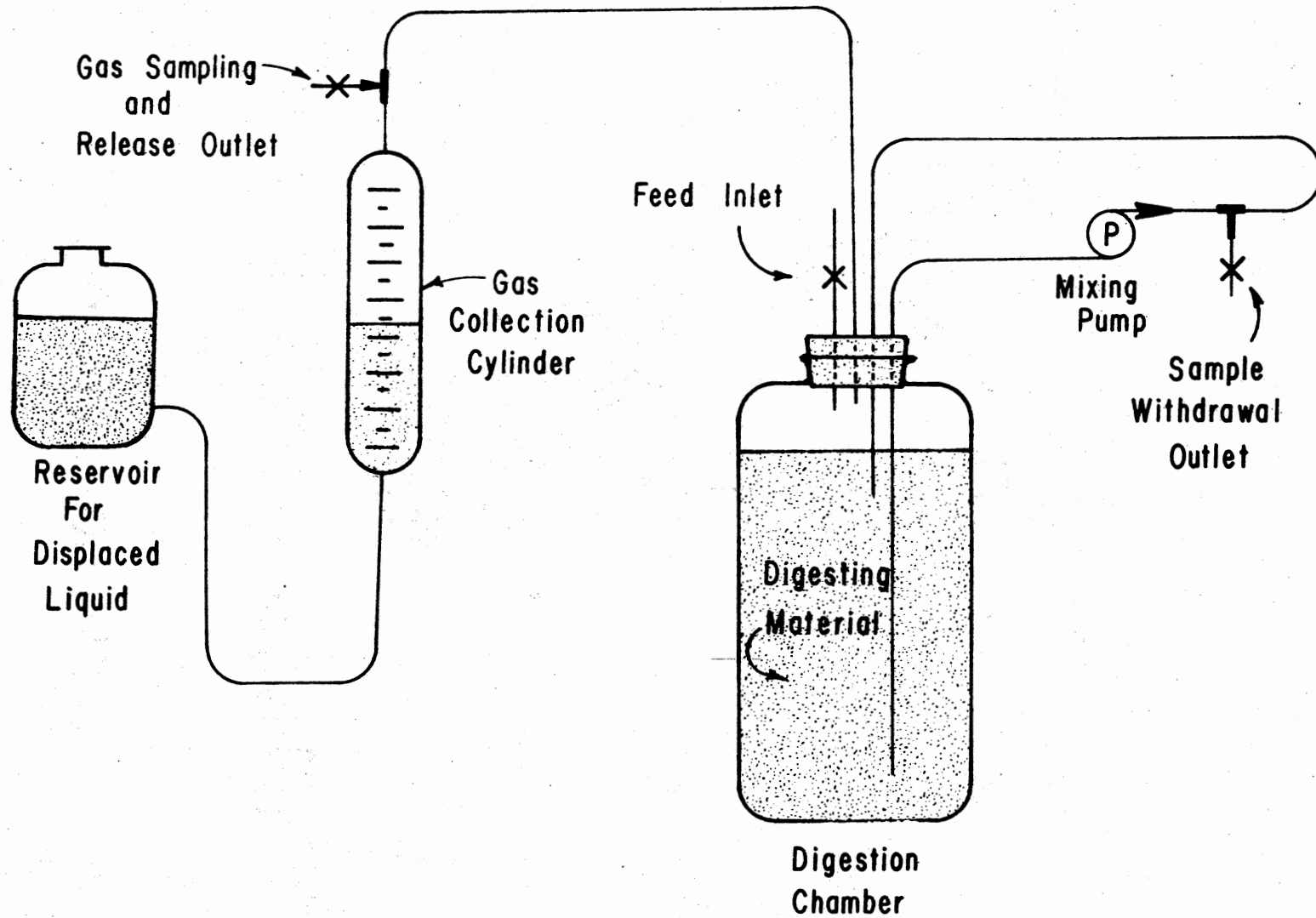
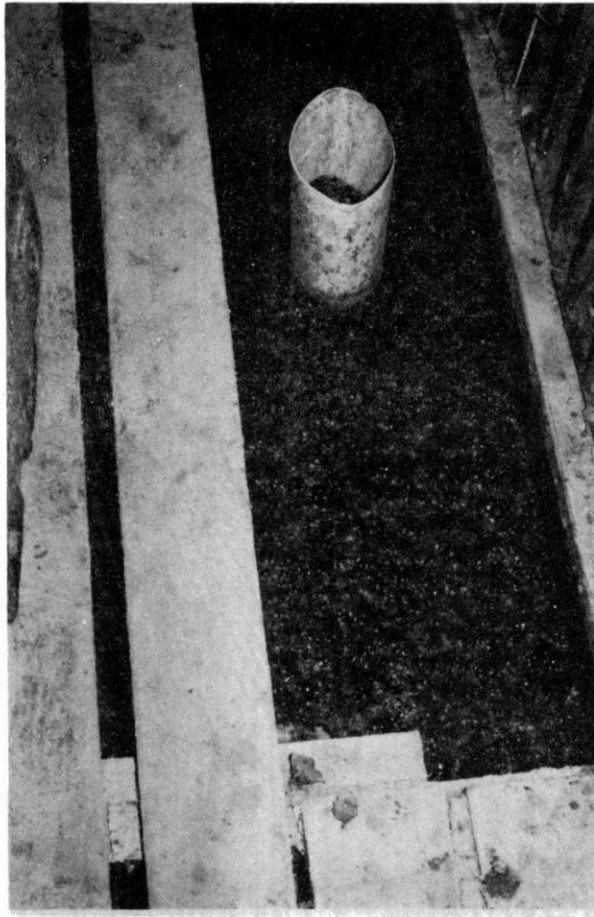


Figure 5. Schematic Drawing of Anaerobic Digestion System



**Figure 6. Anaerobic Digestion System
(Digestion Chamber is
Concealed by Temperature
Control Bath)**



Figure 7. Digestion Chamber
with Rubber
Stopper in
Place

clamp (Figure 8) was applied to the tubing to seal the feed inlet between feedings (Figure 8, Inset A).

The gas outlet was a 10.0 cm length of 0.55 cm (ID) glass rod. The outlet projected 1.0 cm into the digester.

The mixing pump intake was a 32.0 cm length of 1.0 cm (ID) glass rod. The pump intake extended to within 8.0 ± 1.0 cm of the digester's bottom. The pump return was a 19.0 cm length of 1.0 cm (ID) glass rod. The return extended 5.0 ± 0.5 cm below the digester's liquid level.

Gas Collection and Measurement System

Two sizes of graduated glass gas collection cylinders were used in the study. The graduated cylinders had both ends tapered and fitted with tubing outlets (Figure 9). The smaller cylinder had 0.25 l capacity graduated in 10 ml increments. The larger cylinder had 1.6 l capacity graduated in 50 ml increments.

The cylinders were calibrated with tap water at $24 \pm 2^\circ\text{C}$. Each cylinder was filled with water. The water was released at 10 or 50 ml increments, depending on cylinder size, through the linear range of the cylinder. The increments were marked at the meniscus.

The volume of gas generated was measured by liquid displacement (Figure 10). Latex tubing, 0.6 cm (ID), connected the top of the gas collection cylinder to the digester's gas outlet. The expected gas volume determined collection cylinder size, 0.25 or 1.6 l. The displacement liquid was a saturated sodium chloride solution containing 5% sulfuric acid and methyl orange for color.

Latex tubing, 0.6 cm (ID), connected the bottom of the collection cylinder to an aspirator bottle. The aspirator bottle was the reservoir

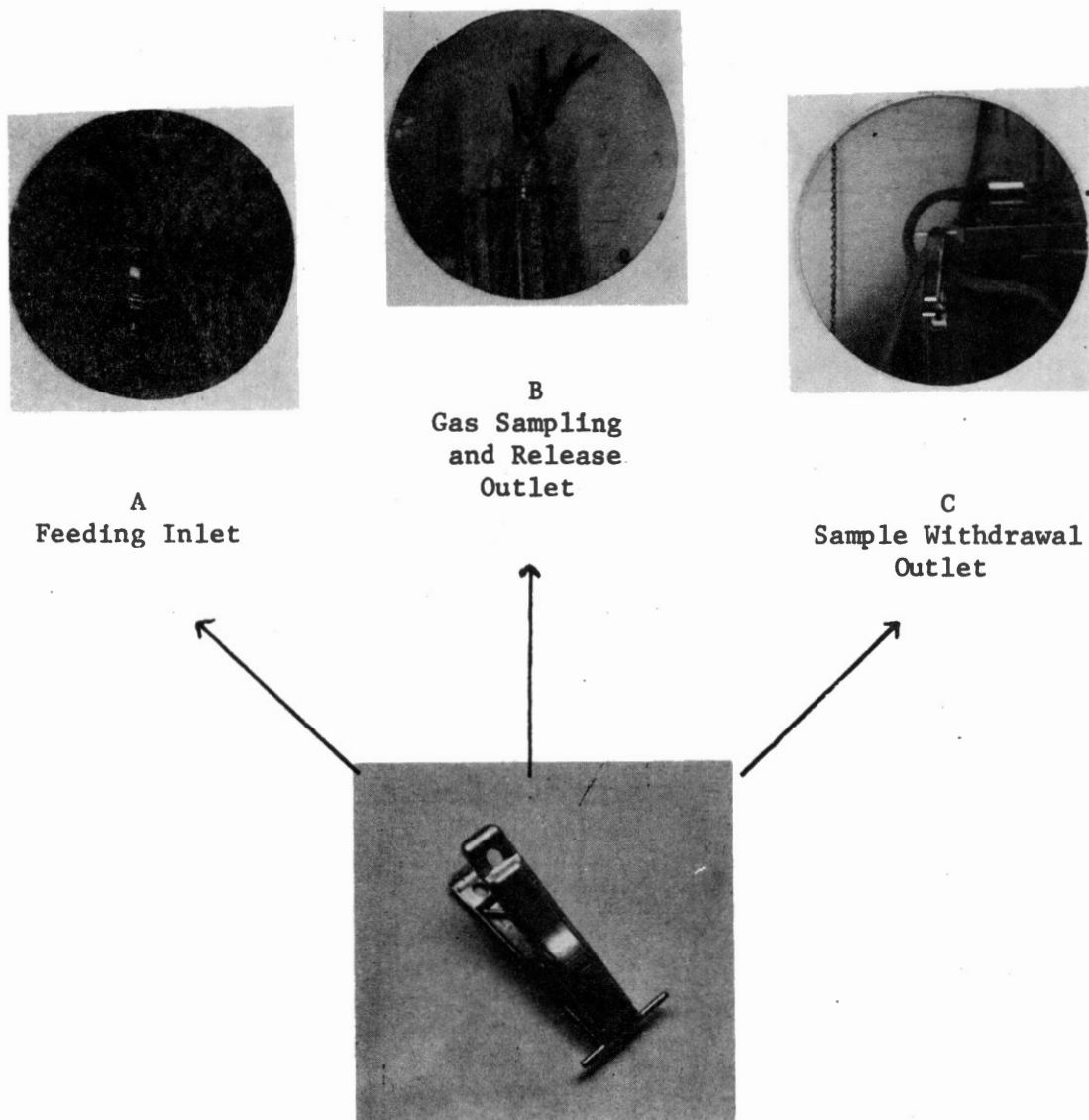


Figure 8. Modified 3201 Pony[®] Clamp Used to Seal Access Ports (Pictured in Insets) to Digestion System

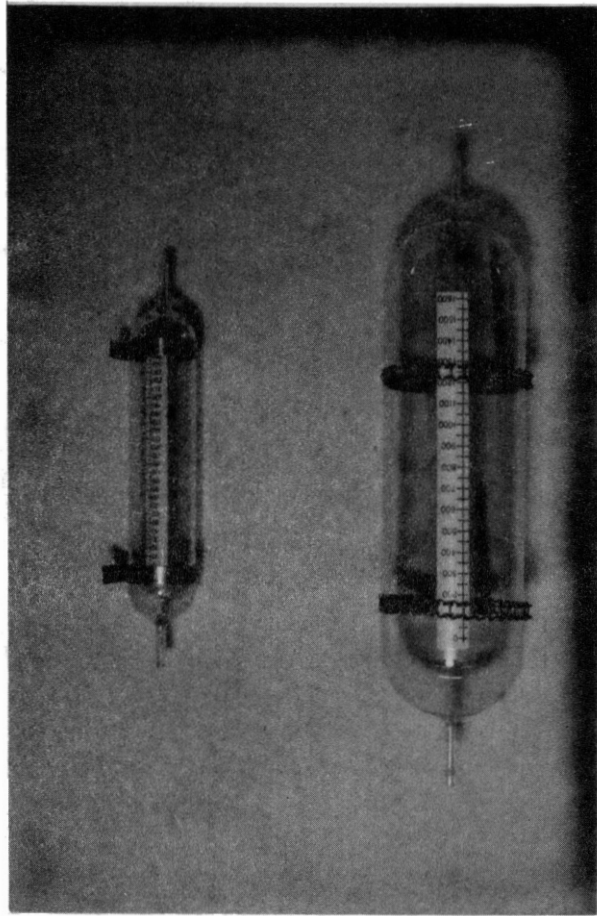


Figure 9. Graduated Glass
Collection
Cylinders

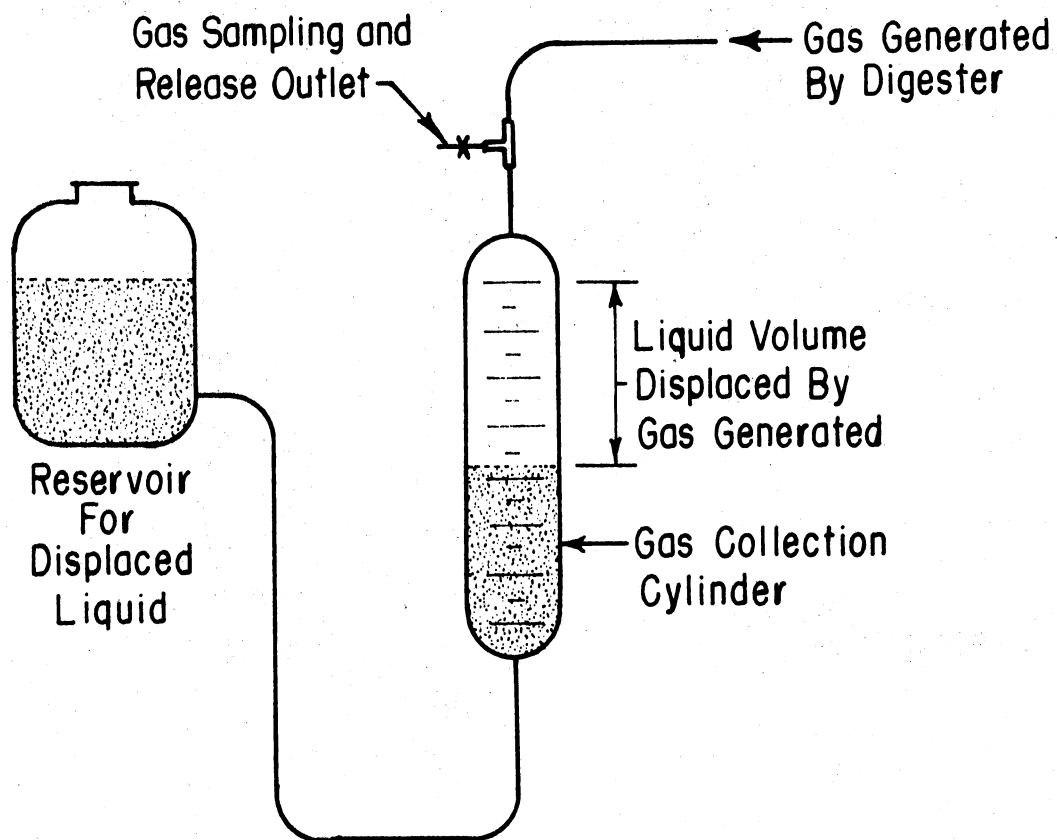


Figure 10. Gas Volume Measurement Scheme

for the liquid displaced by the gas generated. The collection cylinder's size determined the aspirator bottle capacity, 0.5 or 2.0 l.

A plastic tee, 0.4 cm (ID), was inserted in the gas line near the top of the gas collection cylinder. The tee arrangement had two functions: (1) to provide an orifice for the release of gas generated daily, and (2) to provide an orifice for the collection of gas samples used for chromatographic analysis. A modified 3201 Pony[®] clamp was applied to latex tubing on the tee to seal the orifice (Figure 8, Inset B).

Mixing Scheme

A Cole-Parmer (115 V, 60 Hz, 17 W, 0.25 A) oscillating pump (Figure 11) mixed the contents of each digester. Latex tubing, 1.0 cm (ID), connected the pump to the digester's pump intake and return. The pump continually circulated the digester contents at the rate of 17 to 23 ml/s. The pump circulated bottom material to the top of the digester. The return outlet was positioned below the liquid surface to prevent foaming in the digesters. The digesting material was assumed completely mixed.

A plastic tee, 1.0 cm (ID), was inserted in the pump return line. The tee provided an orifice for the digesting material wasted daily. Positioning the tee upright prevented the solids settling in the extraction line. A modified 3201 Pony[®] clamp was applied to the latex tubing on the tee to seal the orifice (Figure 8, Inset C).

Temperature Control

A Tenny environmental stand, model 6PLB-6050C, (Figure 12) was used to maintain digesters within desired temperature range. The unit has six liquid baths with independent temperature controls. The liquid

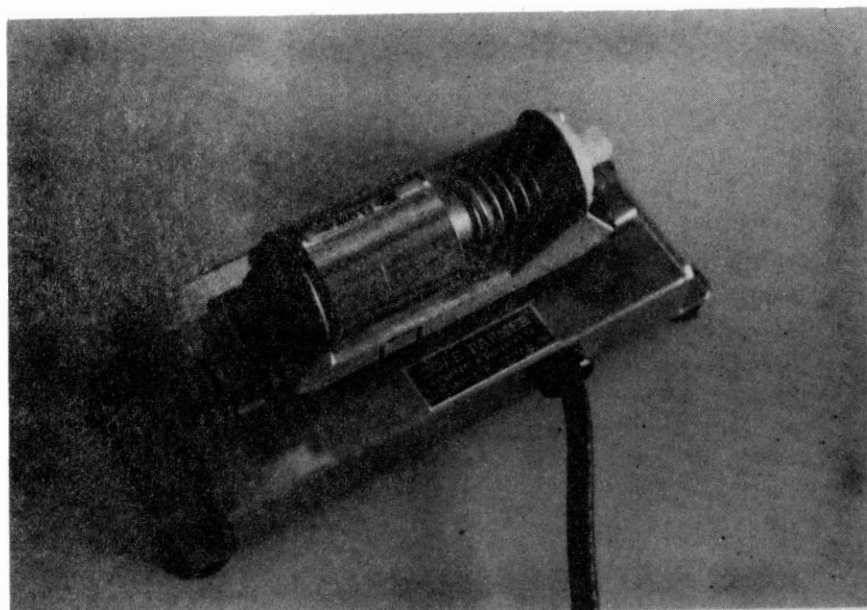


Figure 11. Cole Parmer (115 V, 60 Hz,
17 W, 0.25 A) Oscillating
Pump

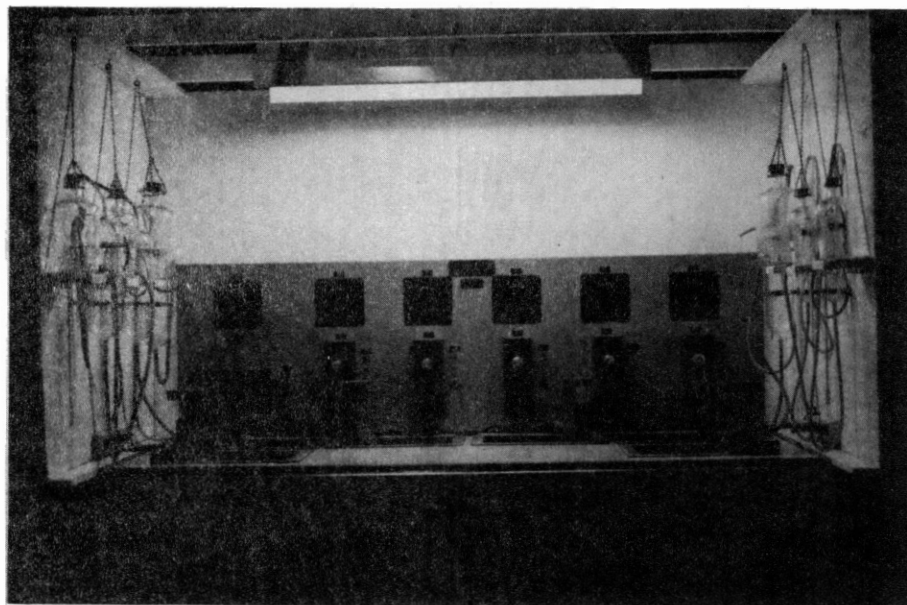


Figure 12. Tenny Environmental Stand
(Model 6PLB-6050C)

used in the baths was a 50-50 mixture of ethylene glycol and distilled water. Sheet metal plates (Figure 13) were placed over the baths to reduce evaporation losses.

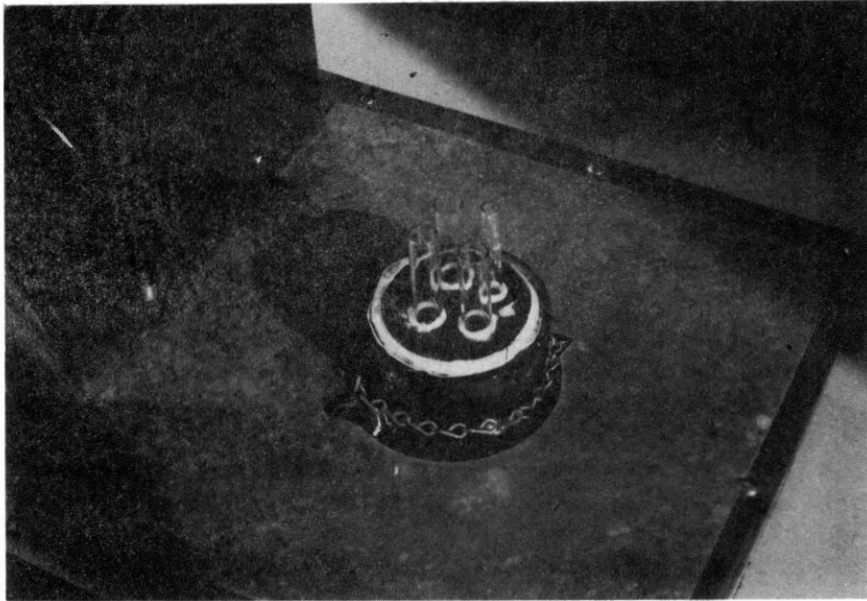


Figure 13. Sheet Metal Plate Positioned
Over Temperature Control
Bath

CHAPTER IV

EXPERIMENTAL PROCEDURE AND MATERIAL

Commercial Operation Characterization

A characterization study was performed on the commercial total confinement swine operation described in Chapter III. The facility was selected because: (1) the operation includes all levels of swine production from farrowing to finishing, (2) the animals are grown on slotted floors and the manure is in a concentrated form, and (3) the owner permitted access to the facility.

Manure generated in each of the farm's confinement buildings was characterized. The manure pits were sampled over a nine-month period, March 1976 to November 1976. Samples were taken every 7 to 14 days. The sampling area for each pit was limited to the area below the opening providing access to the pit's drain standpipe (Figure 3). The manure sampled was assumed representative of the manure throughout the pit.

The herdsman provided information on the pits drained since the last samples were collected. The information included the date a pit was drained and the manure level in the pit after being drained. The manure level and visual characteristics (thick, thin) were observed prior to each sampling. The manure was vigorously mixed before sampled. The minimum sample taken was 1.0 l.

Screening manure through 0.635 cm hardware cloth prior to analysis

removed large particles and most hair. Table IX lists the analyses performed on manure samples.

TABLE IX
ANALYSIS SCHEME FOR MANURE CHARACTERIZATION

Analysis	Raw Waste	Liquid Fraction	Solid Fraction
pH	X		
Solids	X	X	X
COD	X	X	
NH_4^+ - N		X	

All analyses, except ammonia nitrogen, were conducted in accordance to procedures outlined in Standard Methods for the Examination of Water and Wastewater (American Public Health Association, 1971). Appendix A presents a partial listing of the equipment used in the analyses. Total solids, suspended solids, and dissolved solids were determined by drying samples overnight at 103°C. Liquid and solid phase separation of samples for COD, NH_4^+ - N, and solids analysis was obtained by centrifuging. Manure samples were spun at 83 rps for 40 minutes to achieve separation. The decanted liquid fraction for COD and NH_4^+ - N analyses was filtered through a reeve angel glass fiber filter prior to analysis.

Ammonia nitrogen was determined by a procedure outlined by Ecker and Lockhart (1961). Details of the procedure are presented in Appendix B.

Digestion Study

Study Format

The digestion study investigated six swine manure loading rates. The manure fed to digesters was obtained from the total confinement farm described previously. Five loading rates were dilutions (straight, 1/2, 1/3, 1/5, 1/7) of the farm's calculated daily manure production. The sixth loading rate was material collected directly from the finishing barn. Two to three replications of each loading rate were performed.

The study was performed in three segments. Each segment included six simultaneously operated digesters. Three loading rates were fed in duplicate during the first segment. Each of the six loading rates were fed during both the second and third segment. However, three digesters in the third segment were holdovers from the second segment. The three digesters were maintained until the gas generated was analyzed for composition. Table X presents the format followed when investigating the six loading rates.

Digester Operation

The digesters were 4.0 l completely mixed bench scale batch fed systems. Digester detention time and temperature were held constant throughout the study at 20 days and $35 \pm 2^\circ\text{C}$, respectively. Each digester was operated a minimum of 60 days (three detention periods) to obtain indications of the system's stability.

Seed Material

Seed material in preliminary studies was anaerobic sludge from the

Stillwater Municipal Waste Treatment Plant, Stillwater, Oklahoma. Screening sludge through 0.635 cm hardware cloth prior to seeding digesters removed large particles and hair. The digesters were started with 4.0 l of straight sludge.

TABLE X
FORMAT FOR INVESTIGATING DIGESTER LOADING RATES*

Segment	Digester Loading Rates					
	Finisher	Straight	1/2	1/3	1/5	1/7
1		2		2		2
2	1	1	1	1	1	1
3	1	**	1	**	1	**
Total Number of Trials	2	3	2	3	2	3

*Numbers indicate the number of digesters fed at the indicated loading rate during each segment.

**Indicates the digesters held over from previous segment and maintained until the gas generated was analyzed for composition.

Problems were encountered maintaining an active biomass beyond 14 days on swine manure feed. A new seed source was sought after repeated attempts to acclimate seed to swine manure failed.

The new seed source was a lagoon at the commercial farm characterized as part of the study. The lagoon material had the advantage of being acclimated to swine manure. Samples of the lagoon's anaerobic

bottom material were taken with a Kemmerer water sampler. Prior to seeding digesters the lagoon material was screened. Each digester was started with 4.0 l of straight lagoon material.

Three digesters, seeded with lagoon material, were fed a synthetic glucose feed. These preliminary trials were conducted to determine if the previous problem with the biomass was because of the seed material or the physical setup of the digester. No problems maintaining an active biomass (gas production) were experienced during a month of operation. Therefore, all digesters, except two, in the study were seeded with 4.0 l of anaerobic lagoon material. The two exceptions were digesters in the first segment switched from glucose to swine manure feeds.

Feed Material

Expected Daily Manure Production. The expected daily manure production of each of the farm's confinement buildings was calculated. The mean manure production values (liquid and solids) based on livestock weight and age reported by Muehling (1969) were used for the calculations. The herdsman provided the information on each building's livestock population. The calculations did not include the additional water resulting from wastage and washing operations. Table XI presents the calculated values. Detailed calculations are shown in Appendix C.

Preparation and Storage. Manure samples used to prepare digester feeds were collected simultaneously with the samples used to characterize manure. Therefore, the same sampling limitations and assumptions discussed previously applied to samples collected. All manure was screened prior to preparing feed solutions to remove large particles and most hair.

TABLE XI
 EXPECTED DAILY MANURE PRODUCTION (LIQUID AND SOLIDS)
 FOR COMMERCIAL FARM CHARACTERIZED

Building	Expected Manure Production (ℓ/day)	Percent of Total (%)
Sow and Boar Barn	3780	21.5
Farrower	726	4.1
Nursery I and II	1584	10.1
Grower	5481	31.3
Finisher	5821	33.0
Total	17392	100.0

The straight feed solution was prepared by mixing manure from each building in the proportions calculated for the daily manure production. Table XII presents the composition of a 1.0 ℓ straight feed preparation. The straight feed solution was prepared in 3.0 ℓ batches.

The straight feed solution was the stock solution used in preparing the 1/2, 1/3, 1/5, and 1/7 dilutions of the calculated daily manure production. The diluted feed solutions were prepared in 1.0 ℓ batches. The required volume of straight feed solution for each dilution was transferred to a 1.0 ℓ volumetric flask (i.e., 500 ml of straight feed for the 1/2 dilution) and the manure was diluted to 1.0 ℓ with distilled water.

The finisher feed solution was the undiluted manure collected directly from the farm's finishing barn.

TABLE XII
COMPOSITION OF A 1.0 % STRAIGHT FEED PREPARATION

Source	ml of Manure
Sow and Boar Barn	215
Farrower	41
Nursery I	50
Nursery II	51
Grower	313
Finisher	330
Total	1000

The feed solutions were kept refrigerated at about 5°C between feedings. The solutions were brought to room temperature prior to each feeding. The straight feed and finisher stock feed solutions were stored in a freezer maintained at -6.6°C until needed.

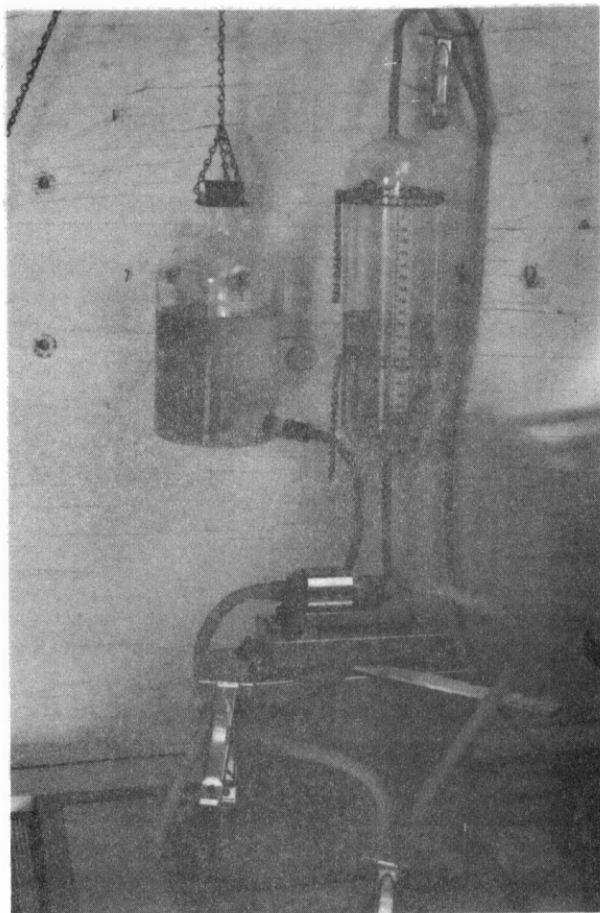
Characterization. Feed solutions were analyzed following the same scheme outlined for characterizing manure samples (Table IX). All analyses, except phase separation for solids, were conducted according to procedures and specifications presented for the manure samples. Liquid and solid phase separation for solids analysis was obtained by filtering samples through 0.45 µm filters.

Daily Operating Procedures

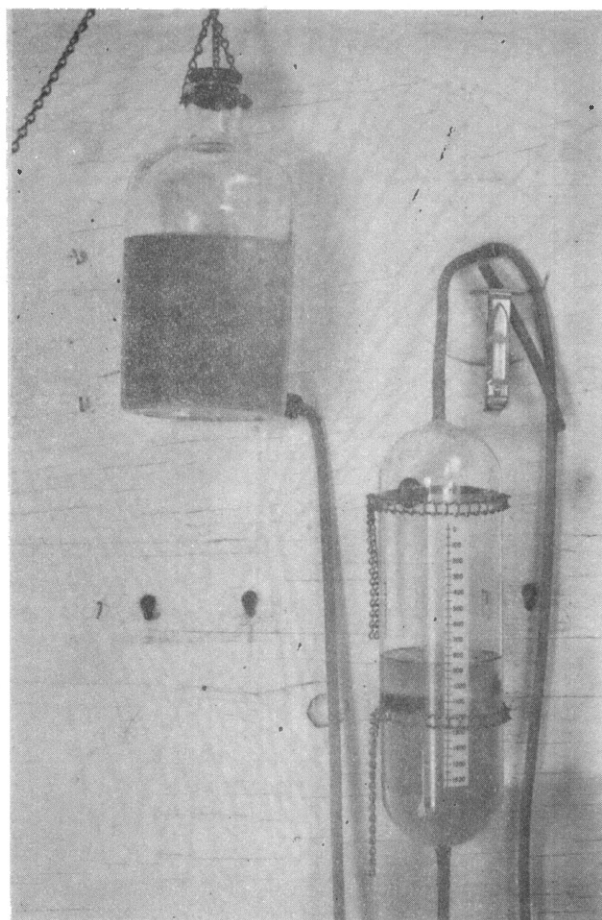
The digesters were fed once daily, normally between 8:30 a.m. and

10:30 a.m. The procedures followed for the daily operating and feed of each digester were:

1. Gas production with the liquid in the aspirator bottle and gas collection cylinder at equal levels (Figure 14) was recorded. Room temperature was recorded at the time of gas reading.
2. Positive pressure was applied to the system by raising aspirator bottle (Figure 15).
 - a. A gas sample to be used for determining gas composition was taken when required.
 - b. A modified 3201 Pony[®] clamp was applied to the pump line below tee. The clamp sealing extraction line was released and 200 ml of digesting material was removed (Figure 16). The extraction line was resealed and the clamp was removed from the pump line. Temperature of the digesting material wasted was taken immediately with a chemical thermometer (-20 to 110°C, 1°C divisions) and recorded.
3. Negative pressure was applied to system by lowering aspirator bottle. The clamp sealing the feed port was opened and 200 ml of feed material was added to the digester (Figure 17). Re-sealing the feed port as the last of the feed entered the digester kept oxygen from entering the system.
4. Gas was expelled from the system by removing the clamp on gas release outlet. Gas was expelled until the liquid surface in the collection cylinder read zero and was level with the liquid surface in the aspirator bottle (Figure 18). The gas release outlet was resealed.



**Figure 14. Liquid in the Aspirator
Bottle and Gas Collec-
tion Cylinder at Equal
Levels for Reading Gas
Production**



**Figure 15. Positive Pressure Applied
to System by Raised
Aspirator Bottle**

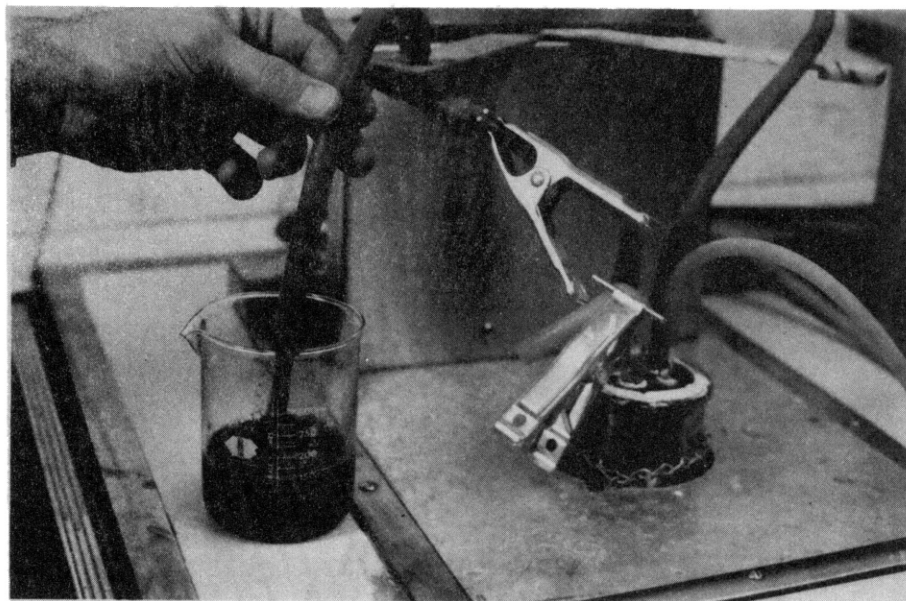


Figure 16. A Modified 3201 Pony[®] Clamp Applied to the Pump Line Below Tee and 200 ml of Digesting Material Being Removed

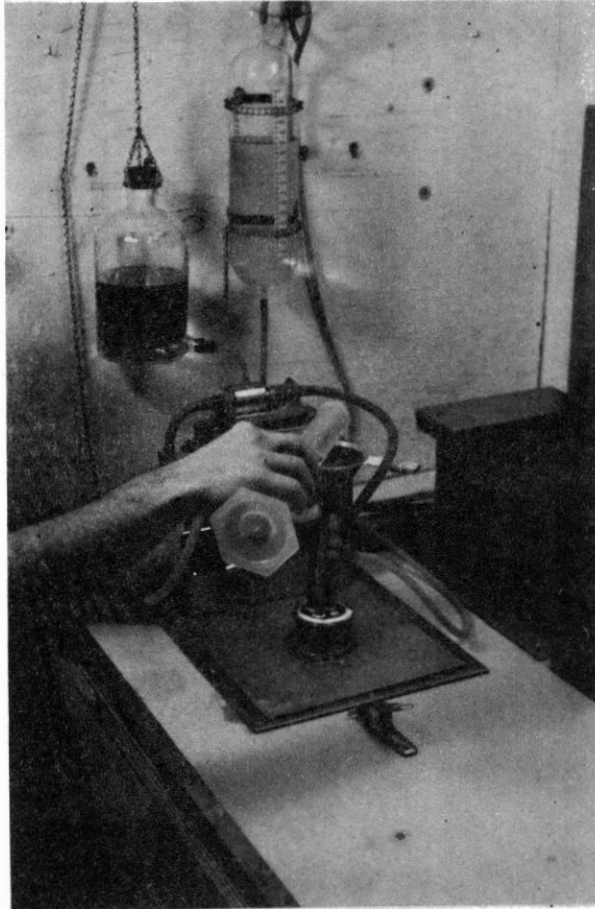


Figure 17. Negative Pressure Applied to System by Lowered Aspirator Bottle and 200 ml of Feed Material Being Added to Digesters

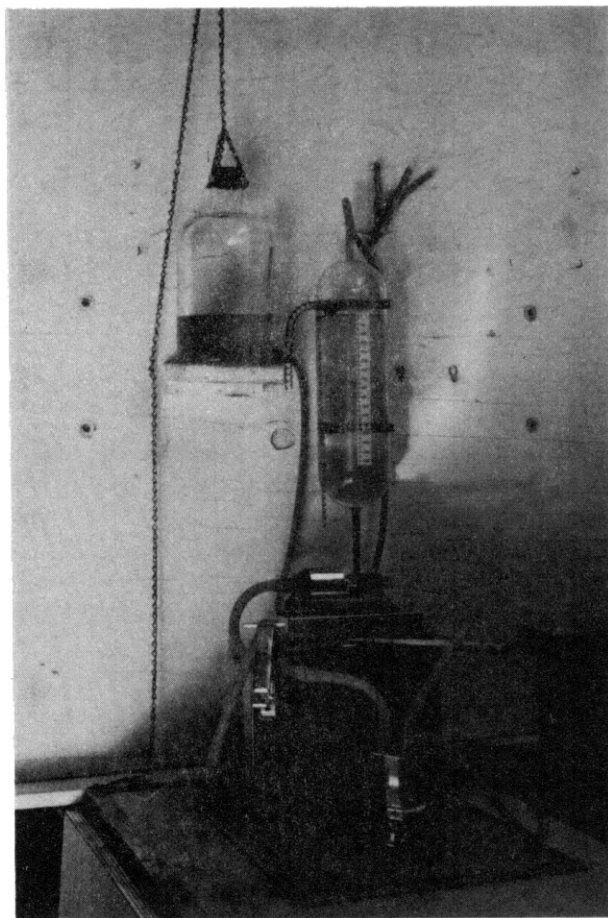


Figure 18. Gas Collection System
Zeroed After Feeding

5. Gas production with the liquid in the aspirator bottle and gas collection cylinder at equal levels was measured and recorded periodically during the day. The data were used to determine and compare rates of gas production. Room temperature was recorded at time of gas reading. Gas was expelled from the system to a reference level if the production appeared to be going to exceed the collection cylinder's capacity before the next feeding.

Gas Sampling Procedure

Samples of gas generated were taken to determine gas composition. A reusable sampling cylinder was used to collect a sample from each digestion system. The reusable sampling cylinder was a glass chamber, 20 to 30 ml capacity, fitted with a vacuum stopcock at either end (Figure 19). The sampling cylinder had a port sealed with a rubber septum to permit needle withdrawal of samples for analysis. The septum was replaced prior to each sampling.

A positive pressure was applied to the system and a sampling cylinder was attached to the latex tubing on the gas collection cylinder's sampling outlet (Figure 20). Both stopcocks on the collection cylinder were opened and the clamp on the gas sampling outlet released. A minimum of 100 ml of gas from a 0.25 l collection cylinder was flushed through the sampling cylinder prior to sampling. A minimum of 300 ml of gas from a 1.6 l collection cylinder was flushed through the sampling cylinder prior to sampling. A sample was collected by sequentially closing the two stopcocks. The outer stopcock was the first closed. The clamp was

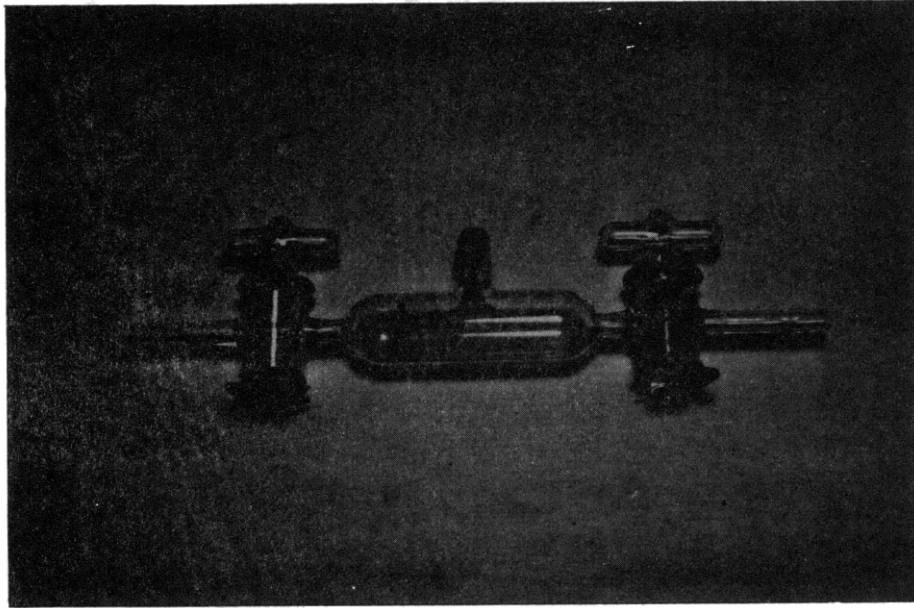


Figure 19. Gas Sampling Cylinder
(Typical)

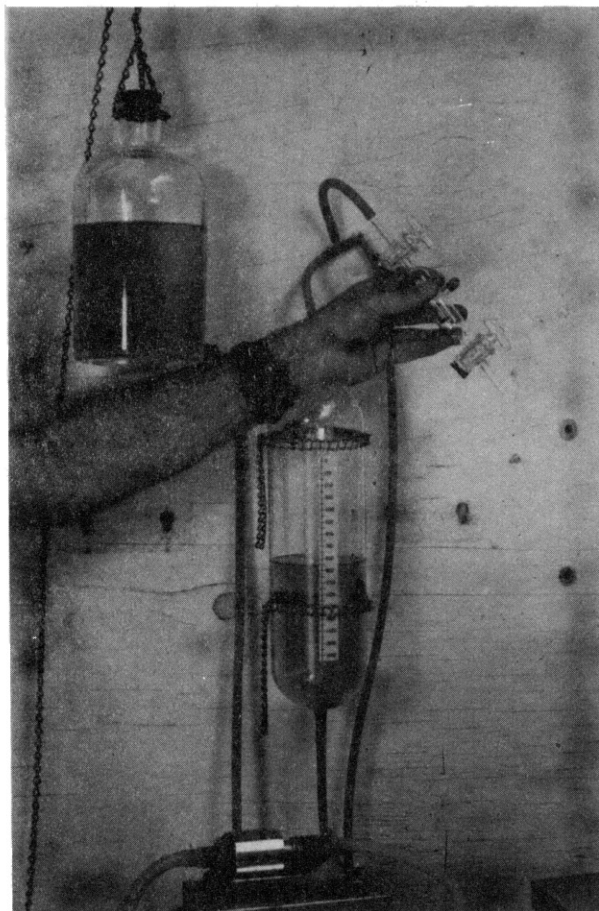


Figure 20. Positive Pressure Applied to System by Raised Aspirator Bottle and Gas Sample Being Taken

reapplied to the gas sampling outlet prior to removing the sampling cylinder.

Parameters Monitored

The 200 ml of digesting material wasted from each digester daily was analyzed to determine the digester's operating characteristics. Table XIII presents the analysis schedule for parameters monitored for each digestion system.

TABLE XIII
ANALYSIS SCHEDULE FOR PARAMETERS MONITORED
FOR EACH DIGESTION SYSTEM

Analysis	Frequency	Combined Waste	Liquid Fraction	Solid Fraction
pH	Daily	X		
Alkalinity	Daily	X		
Solids	3/Week	X	X	X
COD ML	Daily		X	
COD MLSS	3/Week	X		
NH_4^+ - N	2-3/Week		X	
Volatile Acids	1-2/Week		X	
Gas	Limited			

All analyses, except NH_4^+ - N and gas, were conducted in accordance to procedures outlined in Standard Methods for the Examination of Water and Wastewater (American Public Health Association, 1971). Alkalinity was determined by potentiometrically titrating to a pH 3.7 endpoint. Total solids, suspended solids, and dissolved solids were determined by drying samples overnight at 103°C. Liquid and solid phase separation for solids analysis was obtained by filtering samples through 0.45 μm filters. Liquid and solid phase separation of samples for COD, NH_4^+ - N and VA analyses was obtained by centrifuging. Manure samples were spun at 83 rps for 40 minutes to achieve separation. The decanted liquid fraction was filtered through a reeve angel glass fiber filter prior to analysis. The liquid fractions for VA analysis were further filtered through a 0.45 μm filter before being analyzed.

Ammonia nitrogen was determined by a procedure outlined by Ecker and Lockhart (1961). Details of the procedure are presented in Appendix B.

Gas samples were analyzed with a model LKB-9000 gas chromatograph-mass spectrometer located in the Oklahoma State University Biochemistry Department. Appendix A presents details on the LKB-9000. A 1.8 m x 0.32 cm (OD) stainless steel column packed with 80 to 100 mesh Porapak Q was used in the LKB-9000 to separate component gases. Helium carrier gas was supplied at the rate of 0.75 mL/s at 2.76×10^5 Pascals (Pa). The column and injection port were maintained at ambient temperature. A Hamilton gas tight microliter syringe was used to inject gas samples, 25 to 30 μl . Samples of research grade CO_2 (carbon dioxide), CH_4 (methane), and H_2S (hydrogen sulfide) were run to determine the retention time of each expected gas component.

Two runs were made with each anaerobic digester gas sample. The first run was made to get a chromatogram for the sample. Mass spectrometry information for each peak on the chromatogram was taken during the second run. The component gases were identified by retention times and mass spectrometry information. The areas under the peaks on chromatograms were calculated by the triangulation method. These values were used to calculate the percentage of each component gas present.

CHAPTER V

RESULTS AND DISCUSSION

Commercial Operation Characterization

Livestock Inventories

The monthly inventories during the period of January 1976 to November 1976 (Table XIV) shows the total number of animals on the farm remained relatively constant at 4232. The number of animals within the different weight-age classifications, however, varied considerably from month to month.

The birth-sales records for the same period (Table XV) show the number of pigs born on a monthly basis varied drastically with values ranging between 376 and 921. In addition, the herdsman periodically withheld animals from market because of poor prices, accounting in part for the wide range, 26 to 36 weeks, of animals in the finisher.

Lagoon System

At the start of the study, fall 1975, the herdsman was experiencing a problem with the lagoon system. Above average rainfall earlier in the year and the lack of irrigation required to remove an adequate volume of water had the lagoons filled to capacity. The lack of additional lagoon capacity meant the herdsman could not drain the pits as required. Thus, manure was accumulated in the pits. The problem was critical by

TABLE XIV

FARM'S MONTHLY LIVESTOCK INVENTORIES (JANUARY 1976 TO NOVEMBER 1976)

	Jan 1	Feb 1	Mar 1	Apr 1	May 1	June 1	July 1	Aug 1	Sept 1	Oct 1	Nov 1
Breeding Stock:											
Boars (204)*	32	32	24	22	20	17	12	15	20	19	21
Sows (182)	310	360	360	354	367	398	398	395	390	379	375
Gilts (159)	105	85	81	81	64	30	33	37	37	36	9
Breeding Hogs for Sale:											
Gilts (84)	480	505	530	536	542	575	556	585	620	730	718
Pig Inventory:											
Suckling (4)	888	499	360	515	815	746	674	449	496	452	494
Wean-23 kg (14)	736	1273	805	703	612	919	1024	656	505	546	641
23-46 kg (34)	578	514	832	715	625	527	605	854	670	666	589
46-69 kg (59)	519	578	484	689	725	700	536	660	829	681	624
69+ kg (84)	487	435	620	476	530	620	503	615	597	697	672
Total	4135	4281	4096	4091	4300	4532	4342	4266	4164	4206	4143

*Average wt, kg.

TABLE XV

FARM'S MONTHLY LIVESTOCK SALES AND BIRTH RECORDS (JANUARY 1976 TO NOVEMBER 1976)

	Jan 1	Feb 1	Mar 1	Apr 1	May 1	June 1	July 1	Aug 1	Sept 1	Oct 1	Nov 1
<u>Sales:</u>											
Butcher	?	363	333	339	296	487	267	394	251	338	509
Gilts	?	70	190	40	260	225	105	111	155	83	95
Others	?	52	6	21	21	18	21	17	23	39	1
Total*	235	485	529	400	577	730	393	522	429	460	605
<u>Births:</u>											
Litters	47	42	79	87	105	82	50	59	76	60	50
Pigs	430	376	634	707	921	661	417	512	617	495	423

*Average wt of animals 84 kg.

February 1976 because pit storage capacity was also nearly expended. A neighboring farmer pre-irrigating from the lagoons during late February and March 1976 lowered the liquid level in the lagoons by 0.8 m. The water removed was sufficient to permit the herdsman to resume draining the pits.

The lowering of the lagoon's liquid level revealed the sediment deposition patterns in the lagoons. The lagoon receiving manure directly from the production facilities had solid deposits around its edges. Because of the sediment deposits, the lagoon's capacity appeared to be reduced by one-fourth to one-third. Similar deposits were not observed in the other lagoon.

Manure Characterization

Manure samples collected prior to June were not included in the characterization study since the samples did not represent the farm's normal operating conditions. By June, the herdsman was able to re-establish a near normal draining schedule, but he was unable to drain the pits completely each time due to the limited lagoon capacity. The manure sampling period spanned the five month period between June 1, 1976 and November 1, 1976. Appendix D contains the raw manure characterization data for the individual production buildings.

Sow and Boar Barn

The sow and boar barn's pit was normally covered with a scum layer 10 to 12 cm thick. Solid particles brought to the surface by rising gas bubbles appeared to create the layer. Hair present in the manure also seemed to contribute to formation of the layer. During the warmer months

the upper surface of the layer dried forming a hard crust, occasionally creating a clogging problem when draining the pit.

Table XVI summarizes the manure characterization results for the barn. Figure 21 is a plot of TS, MLSS COD, NH_4^+ - N versus sampling date for the analyzed manure samples from the barn. The letter "D" on the plot, a notation used throughout the manure characterization presentation, indicates dates the pit was drained. The dotted line within the COD plot denotes the data point was not measured analytically but estimated. The estimated point was not used when developing Table XVI.

TABLE XVI

SOW AND BOAR BARN MANURE CHARACTERIZATION RESULTS SUMMARY
(JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	7.2-7.5	7.4	0.025
MLSS COD (mg/l)	38,000-132,000	76,000	7,500
TS (mg/l)	53,000-165,000	93,000	8,300
VS (mg/l)	33,000-104,000	59,000	5,200
NH_4^+ - N (mg/l)	720-1,730	1,120	65
% VS	61-70	64	0.51
% SS	90-97	94	0.80
% VSS	61-72	64	0.77
% CODSP	5-13	8	0.80

The TS content of the manure reflected the high bulk content in the animal feed. Manure characteristics fluctuated throughout the study as illustrated by the TS and MLSS COD plots (Figure 21). The general decline in TS and MLSS COD concentration following each pit draining was due to the herdsman adding water when draining the pit. The water added by the herdsman was used to dilute the thick scum layer and manure suspension near the standpipe and thereby maintain drainage. Although the pit was partially drained periodically, it was never completely drained during the study. Consequently, the manure level was rarely below 45 cm in the pit. Many weeks during the sampling period the manure level equaled or exceeded the standpipe height permitting overflow of the liquid fraction while retaining the solids. Therefore, a portion of the increase in TS and MLSS COD concentrations was thought to be due to overflow.

Figure 21 shows $\text{NH}_4^+ - \text{N}$ also fluctuated initially but stabilized by mid-July and remained relatively stable for the duration of the study. The $\text{NH}_4^+ - \text{N}$ concentration, unlike TS and MLSS COD concentrations, was only slightly affected by water additions during pit draining. The contrasting effects caused by water additions suggested the liquid fraction equilibrated more rapidly than the solid fraction immediately surrounding the standpipe.

Farrower

The pit of the farrowing building was periodically covered with a thin gaseous scum layer. The manure samples had a watery consistency, screened readily, and contained little or no hair. Table XVII summarizes

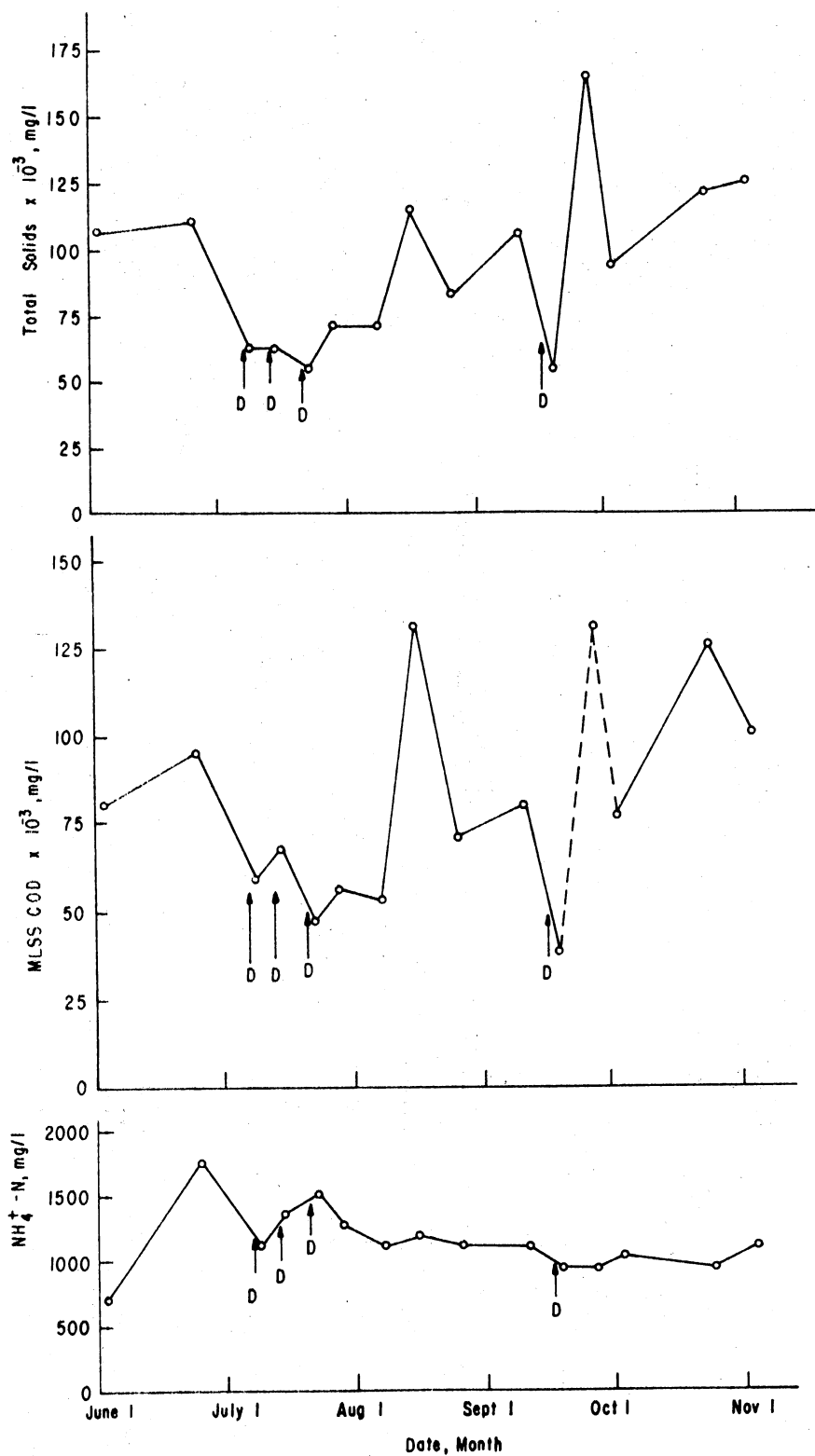


Figure 21. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Sow and Boar Barn (June 1, 1976 to November 1, 1976)

the manure characterization results for the farrowing building. Figure 22 presents a plot of TS, MLSS COD, and NH_4^+ - N versus sampling date for the manure samples.

TABLE XVII

FARROWER MANURE CHARACTERIZATION RESULTS SUMMARY
(JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	7.1-7.7	7.4	0.052
MLSS COD (mg/l)	6,000-39,000	26,000	2,400
TS (mg/l)	8,000-34,000	26,000	1,900
VS (mg/l)	5,000-26,000	18,000	1,300
NH_4^+ - N (mg/l)	200-700	380	32
% VS	60-76	72	1.3
% SS	77-95	90	1.4
% VSS	62-80	75	1.3
% CODSP	3-14	5	0.8

Figure 22 indicates TS and MLSS COD concentrations fluctuated considerably during the sampling period. The fluctuations were related to: (1) manure level, (2) pit draining, and (3) wash water additions. Prior to late August, except in mid-July when the pit was partially drained once, the manure level equaled or exceeded the standpipe height during

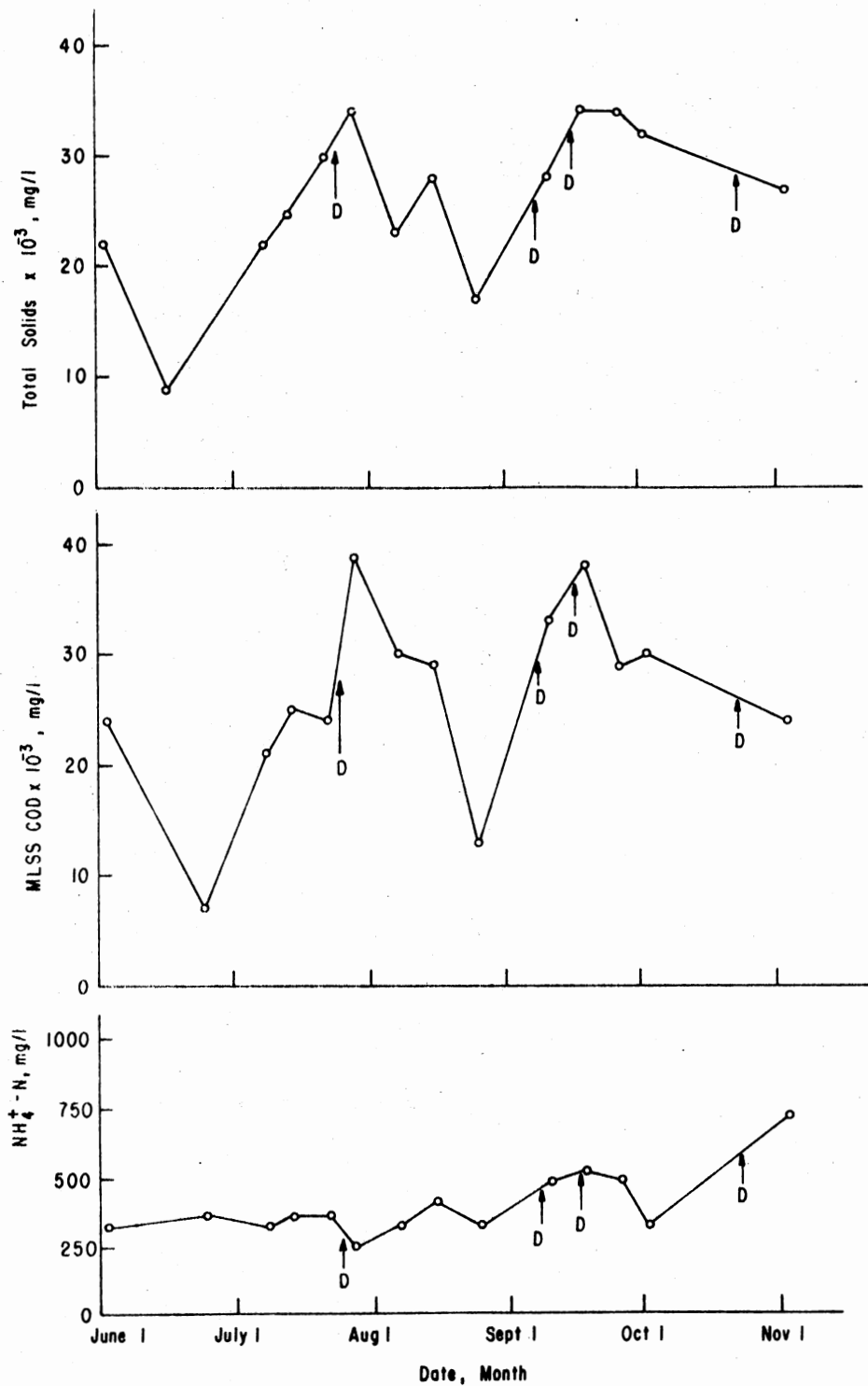


Figure 22. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from the Farrower (June 1, 1976 to November 1, 1976)

the sampling period. The elevated manure level enabled liquid to overflow the standpipe while most solids settled and were retained in the pit. Solids retention partially accounted for the increase in TS and MLSS COD concentrations noted particularly between mid-June and mid-July. The increased TS and MLSS COD concentrations observed in samples collected shortly after the pit was drained indicated settled solids were also not effectively removed when the pit was drained.

Wash water entering the pit also affected TS and MLSS COD concentrations. The herdsman washed the three farrowing rooms in rotation, one per week, utilizing approximately 19,000 l of water per washing. The extent wash water influenced TS and MLSS COD concentrations was thought to be dependent on the location of the room washed in relation to the standpipe, and on the date the room was washed in relation to the sampling date. However, correlating wash water additions to manure characteristics was not possible because detailed records on the washing schedule were not kept during the study. Wash water additions probably influenced the low TS and MLSS COD values determined for samples collected in mid-June, early and late August, and early November. The NH_4^+ - N concentration also fluctuated during the pit sampling period but not as drastically as the TS and MLSS COD concentrations. The decreased fluctuation of NH_4^+ - N was attributed to the faster equilibration of the liquid fraction with the solid fraction immediately surrounding the standpipe. The NH_4^+ - N plot (Figure 22) indicates a rapid increase in the NH_4^+ - N concentration during the final month of the study. The data collected provided no explanation for the rapid NH_4^+ - N increase.

Nursery I and II

The pit areas of the two nurseries were commonly covered with a thin gaseous scum layer. The manure samples from both buildings commonly had a watery consistency, screened readily, and contained only small quantities of hair. Tables XVIII and XIX present summaries of Nursery I and Nursery II manure characteristics, respectively. Figures 23 and 24 are plots of TS, MLSS COD, and $\text{NH}_4^+ - \text{N}$ versus sampling date for Nursery I and Nursery II manure samples, respectively. A comparison of the manure characteristics for the two nurseries revealed a wide variation in the average MLSS COD, TS, VS, and $\text{NH}_4^+ - \text{N}$ concentrations. The average MLSS COD, TS, VS, and $\text{NH}_4^+ - \text{N}$ concentrations for Nursery II were 1.4 to 2.0 times the values for Nursery I. Although variation in manure characteristics was expected over the sampling period due to washing schedule rotation, the average values were expected to be similar, since both buildings were constructed and operated identically. The variation in manure characteristics was attributed to conditions existing in the pits prior to when the study was initiated. The pit of Nursery II operated at overflow conditions from the start of the study in June through the first of September. The pit of Nursery I on the other hand was drained substantially in late June.

Nursery I. The pit of Nursery I was partially drained only once during the five month sampling period. Figure 23 shows TS and MLSS COD concentrations declined sharply prior to pit draining in late June. A rapid increase in pit manure level, 10 cm in 14 days, suggested the decline in TS and MLSS COD concentrations was primarily the result of wash water entering the pit between sample dates. The sudden rise in TS

TABLE XVIII
 NURSERY I MANURE CHARACTERIZATION RESULTS SUMMARY
 (JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	7.0-7.4	7.3	0.025
MLSS COD (mg/l)	11000-36000	19000	1500
TS (mg/l)	12000-36000	20000	1800
VS (mg/l)	8000-26000	13000	1300
NH ₄ ⁺ - N (mg/l)	470-1490	660	64
% VS	61-72	66	0.8
% SS	76-92	86	1.3
% VSS	64-75	71	0.8
% CODSP	3-26	9	1.6

TABLE XIX
 NURSERY II MANURE CHARACTERIZATION RESULTS SUMMARY
 (JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	7.1-7.5	7.3	0.025
MLSS COD (mg/l)	16000-56000	37000	2600
TS (mg/l)	19000-52000	38000	2800
VS (mg/l)	12000-34000	26000	2100
NH ₄ ⁺ - N (mg/l)	550-1140	910	46
% VS	64-70	67	0.52
% SS	87-94	91	0.52
% VSS	67-72	69	0.52
% CODSP	4-14	7	0.52

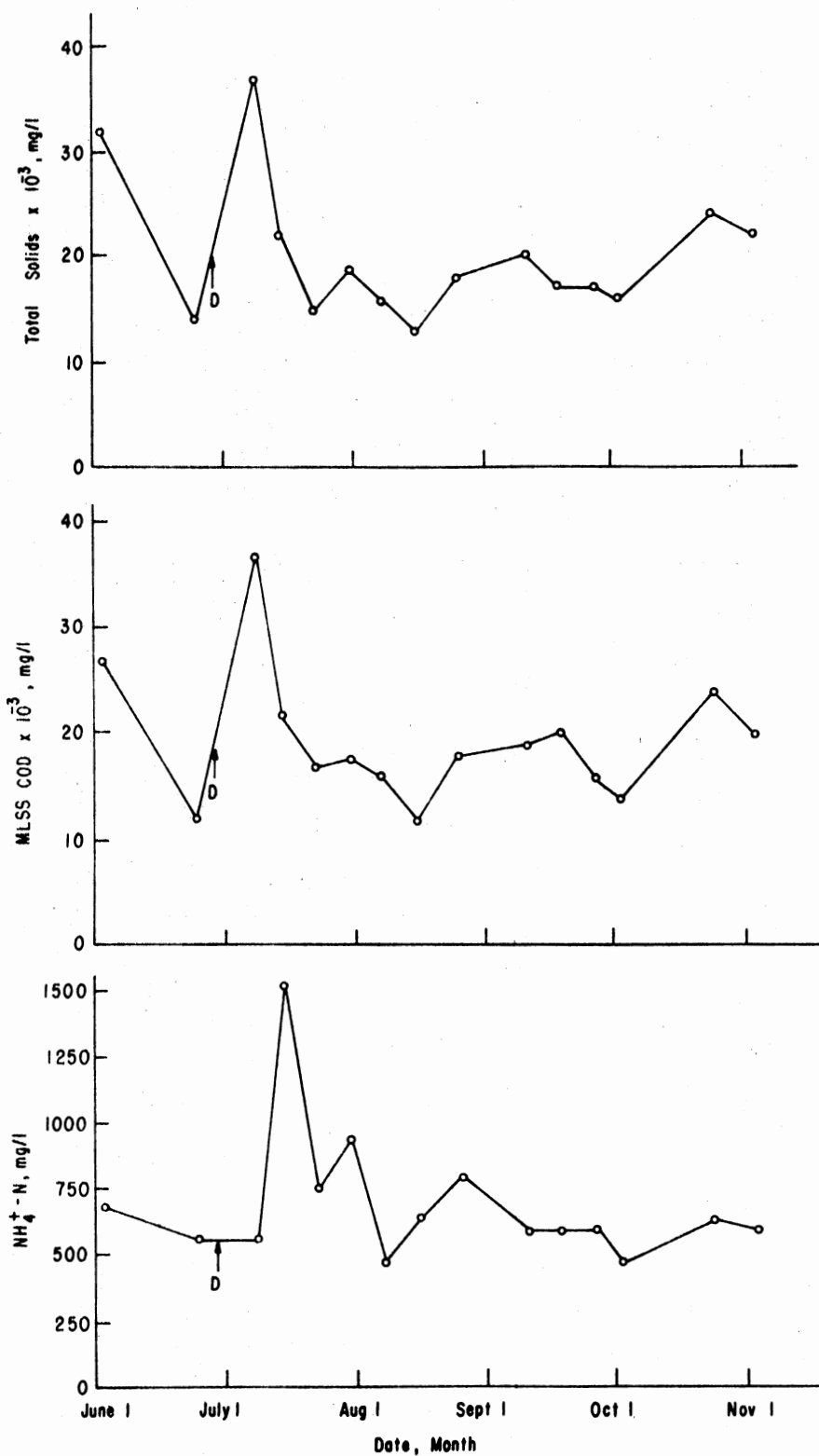


Figure 23. TS, MLSS COD, and NH_4^+ - N Versus Sampling Date for Manure Samples Collected from Nursery I (June 1, 1976 to November 1, 1976)

and MLSS COD concentrations for the sample taken shortly after the pit was drained indicated settled solids were not effectively removed during draining. The rise in TS and MLSS COD concentrations in mid-July was followed by a sharp decline in these parameters at the two subsequent samplings. Again, a rapid increase in pit manure level, 20 cm in 14 days, suggested the decline in TS and MLSS COD concentrations was primarily due to dilution caused by wash water entering the pit between samplings. Manure was overflowing the standpipe by late July and remained overflowing the remainder of the sampling period. The elevated manure level permitted liquid to overflow the standpipe while solids generally settled and were retained in the pit. As a result, the TS and MLSS COD concentrations followed a gradual increasing trend during the last three months of sampling. Although there was an increasing trend, the concentrations did fluctuate. The fluctuations in TS and MLSS COD concentrations were believed to be due to wash water periodically entering the pit similar to the farrower.

The NH_4^+ - N concentration, except for the peak occurring in mid-July, remained relatively stable throughout the sampling period. The relative stability of the NH_4^+ - N concentration was attributed to the faster equilibration of the liquid fraction than the solid fraction immediately surrounding the standpipe. The data collected provided no insight as to the cause for the rapid increase in NH_4^+ - N concentration occurring in mid-July.

Nursery II. Manure was overflowing the standpipe when sampling was initiated in June. Figure 24 indicates TS and MLSS COD concentrations increased during the first weeks of sampling. The increase in TS and

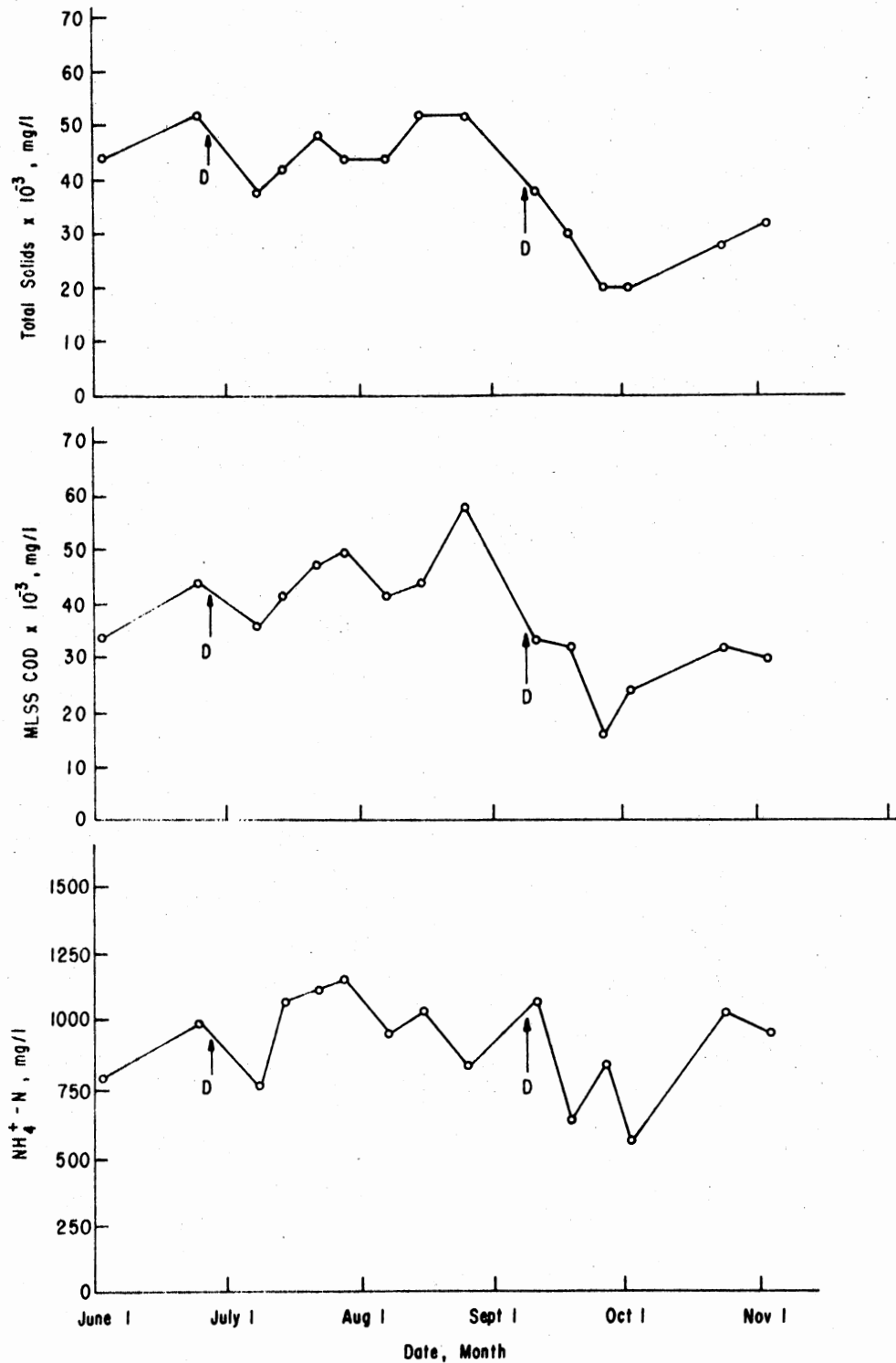


Figure 24. TS, MLSS COD, and $\text{NH}_4^+ - \text{N}$ Versus Sampling Date for Manure Samples Collected from Nursery II (June 1, 1976 to November 1, 1976)

MLSS COD concentrations was presumably due to solids being retained in the pit while the liquid fraction overflowed the standpipe. The pit was partially drained between samplings in late June. However, the manure was overflowing the standpipe again at the next sampling. The rapid return of the manure level to overflowing the standpipe and the decline in TS and MLSS COD concentrations were attributed to wash water entering the pit between samplings. The manure level equaled or exceeded the standpipe height until the pit was drained again in early September. Thus, the TS and MLSS COD concentrations followed a gradually increasing trend between late June and early September. Although there was an increasing trend, the TS and MLSS COD concentrations did fluctuate due to wash water periodically entering the pit. As indicated previously, the pit was partially drained in early September. The TS and MLSS COD concentrations declined following the pit draining. The decline in TS and MLSS COD concentrations was contrary to previous trends where the TS and MLSS COD concentrations increased rapidly when the nurseries' pits were drained. The decline in TS and MLSS COD concentrations was thought to be due to wash water entering the pit in the vicinity of the standpipe rather than the result of solids being removed efficiently during draining. The TS and MLSS COD concentrations continued to decline during the two subsequent samplings. A rapid increase in pit manure level, 28 cm in 17 days, indicated the decline in TS and MLSS COD concentrations was primarily due to dilution caused by wash water entering the pit between samplings. Manure was again overflowing the standpipe by late September and remained overflowing the remainder of the sampling period. Thus, the TS and MLSS COD concentrations exhibited a gradual increasing trend during the remainder of the study.

Figure 24 shows NH_4^+ - N remained relatively stable except when the pit was drained. Although the periods of greatest fluctuations of the NH_4^+ - N concentration coincided with pit draining, the fluctuations were attributed to wash water entering the pit during the same period.

Grower

The pit of the grower was normally covered with a scum layer approximately 8 to 10 cm thick. The scum layer was similar to the layer described for the sow and boar barn.

Table XX summarizes the manure characterization results for the grower. Figure 25 presents a plot of TS, MLSS COD, and NH_4^+ - N versus sampling date for the manure samples taken from the grower. The letter "L" on the plot denotes significant water leaks occurred due to broken water pipes in the grower.

The TS and MLSS COD concentrations reflect the high bulk content in the feed ration. Manure characteristics fluctuated throughout the study as exemplified by the TS, MLSS COD, and NH_4^+ - N plots (Figure 25). Fluctuations in TS, MLSS COD, and NH_4^+ - N concentrations were particularly pronounced when samples were collected shortly after the pit was drained in early August and late October. The general decline in TS, MLSS COD, and NH_4^+ - N concentrations noted following each pit draining was attributed to water added to the pit when the herdsman drained the pit. The herdsman added water to dilute the thick scum layer and manure suspension near the standpipe and thereby maintain drainage. The quantity of water added by the herdsman varied, thus contributing to the TS and MLSS COD fluctuations. The particularly rapid decline of TS, MLSS COD, and NH_4^+ - N concentrations in early August was due to

TABLE XX
 GROWER MANURE CHARACTERIZATION RESULTS SUMMARY
 (JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	7.2-7.6	7.3	0.025
MLSS COD (mg/l)	15000-62000	39000	3400
TS (mg/l)	24000-57000	43000	3100
VS (mg/l)	16000-39000	29000	2100
NH ₄ ⁺ - N (mg/l)	840-2060	1430	96
% VS	55-74	68	1.0
% SS	79-90	86	1.0
% VSS	56-77	70	1.3
% CODSP	4-21	14	1.0

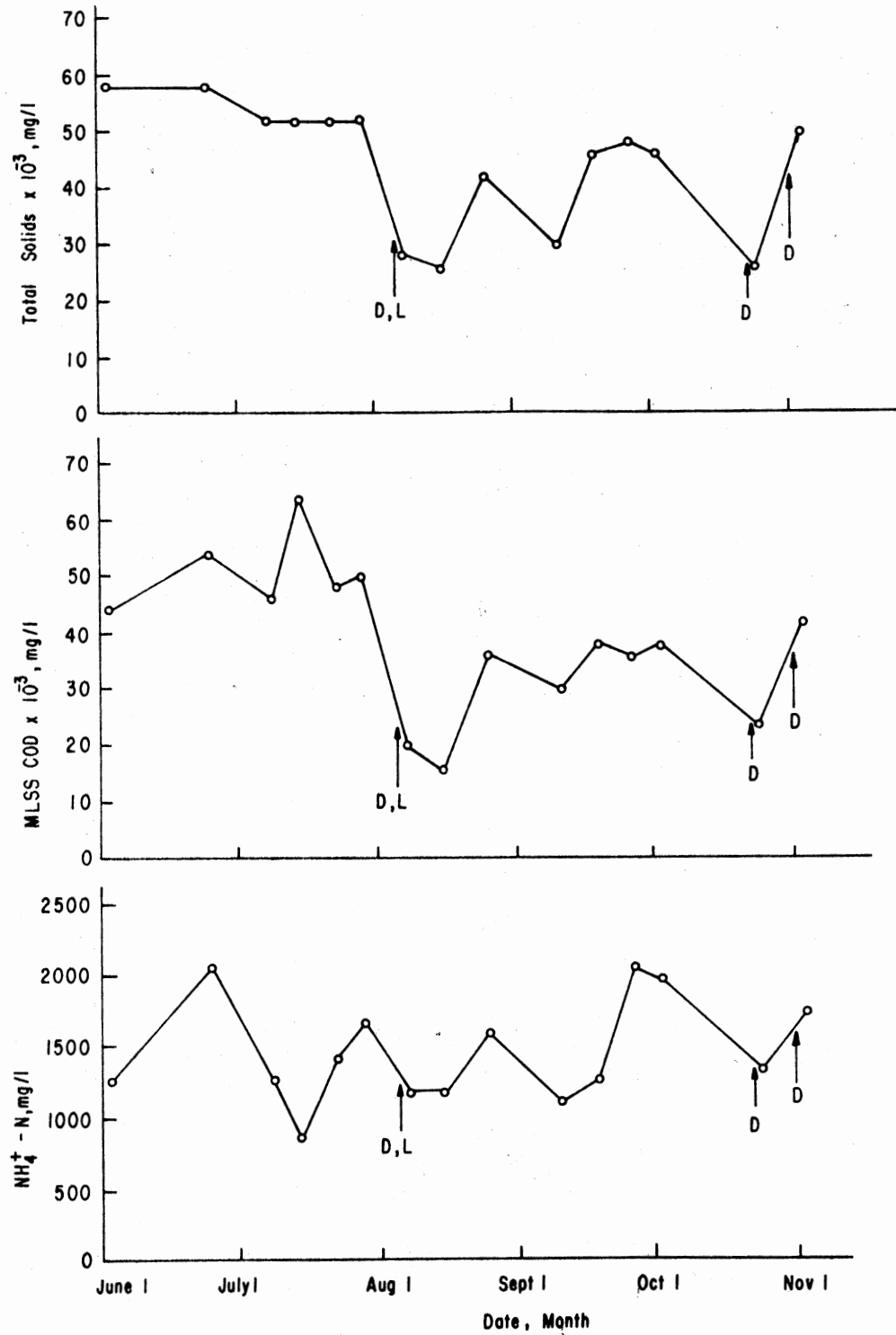


Figure 25. TS, MLSS COD, and NH₄⁺ - N Versus Sampling Date for Manure Samples Collected from the Grower (June 1, 1976 to November 1, 1976)

concurrency of water leaks with the pit draining. A rapid increase in pit manure level, 25 cm in seven days, indicated problems with the leaking water pipes persisted off and on during the week after the pit was drained in early August. The increase in TS and MLSS COD concentrations after the pit was drained in late October was contrary to previous trends. Normally, TS and MLSS COD concentrations decreased due to water additions by the herdsman when the pit was drained. The increase in TS and MLSS COD concentrations was attributed to the four day lag between draining and sampling. The four day lag allowed concentrated manure from the area surrounding the standpipe to equilibrate with the diluted manure suspension in the immediate vicinity of the standpipe. The data collected provided no explanation for the rapid NH_4^+ - N increases occurring in late June and late September.

Finisher

A scum layer 12 to 16 cm thick typically covered the pit of the finisher. The scum layer was similar to those in the sow and boar barn and the grower pits. Table XXI summarizes the manure characterization results for the finisher. Figure 26 presents a plot of TS, MLSS COD, and NH_4^+ - N versus sampling date for the manure samples taken from the finisher. The letter "L" on the plots again denotes dates significant water leaks occurred due to broken water pipes in the finisher. The fluctuations of TS, MLSS COD, and NH_4^+ - N were caused by the same factors described in the grower discussion.

Although the pit was partially drained periodically, the manure level never dropped below 45 cm in the pit. Many weeks during the sampling period the manure level equaled or exceeded the standpipe

TABLE XXI
 FINISHER MANURE CHARACTERIZATION RESULTS SUMMARY
 (JUNE 1, 1976 TO NOVEMBER 1, 1976)

Parameter	Range	Mean Value	Standard Error
pH	6.9-7.6	7.2	0.075
MLSS COD (mg/l)	53000-114000	90000	5000
TS (mg/l)	69000-129000	98000	8000
VS (mg/l)	46000-98000	65000	3500
NH_4^+ - N (mg/l)	1410-3460	2330	150
% VS	59-77	64	1.5
% SS	88-98	93	0.8
% VSS	59-78	65	1.6
% CODSP	10-43	24	2.6

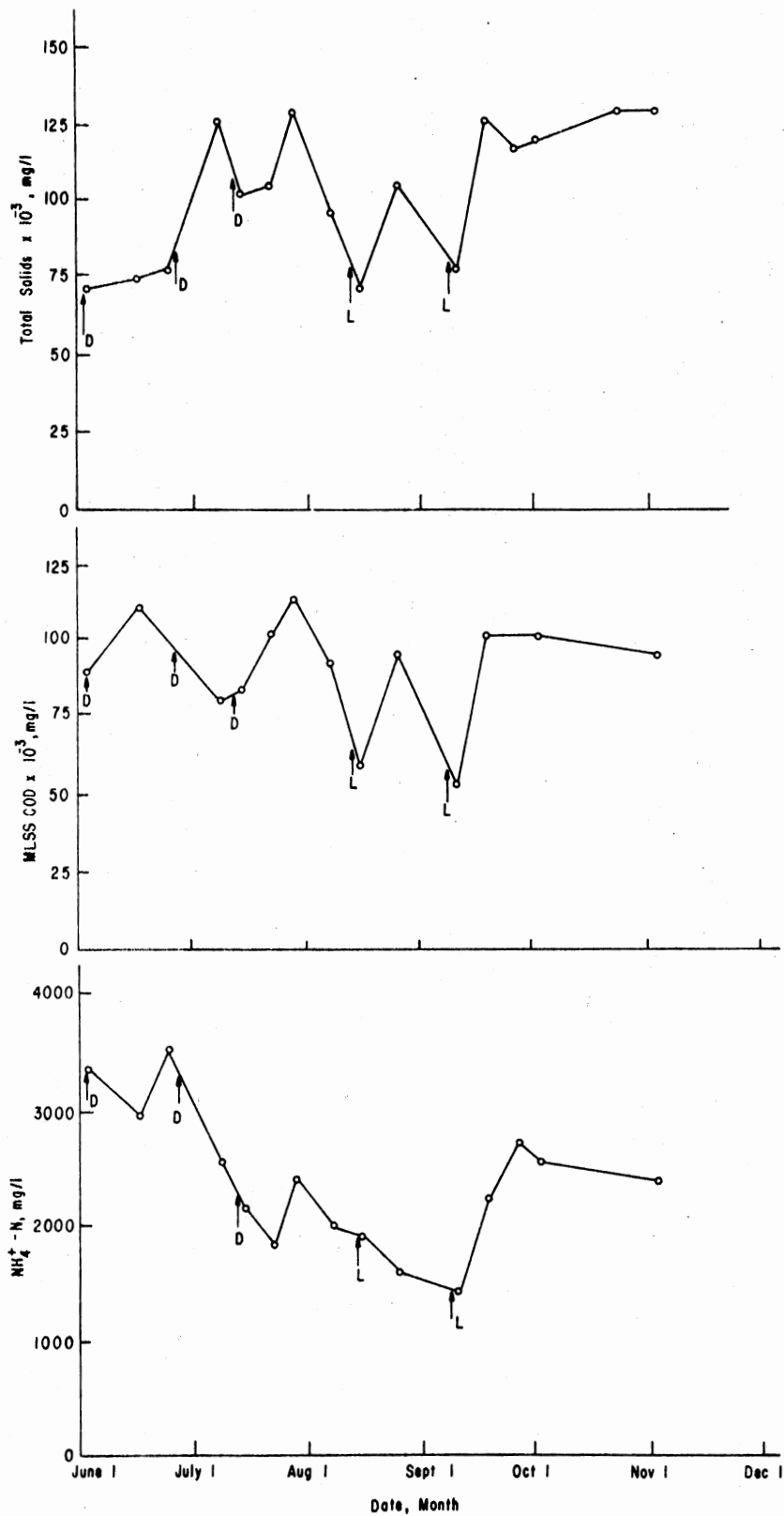


Figure 26. TS, MLSS COD, and $\text{NH}_4^+ - \text{N}$ Versus Sampling Date for Manure Samples Collected from the Finisher (June 1, 1976 to November 1, 1976)

height. Overflow of the liquid fraction was, therefore, considered to be the principle cause of the increase in TS and MLSS COD concentrations. The increased TS concentration noted following the late June pit draining was attributed to the 12 day lag between draining and sampling and to the overflowing of the liquid fraction. The 12 day lag permitted concentrated manure from the area surrounding the standpipe to equilibrate with the diluted manure suspension in the immediate vicinity of the standpipe. Also, the manure level exceeded the standpipe height at the time of sampling.

Discussion of the Commercial

Operation Characterization

The lagoon problem hampered draining manure pits for several months preceding the study. Limited lagoon capacity during the study also prevented the herdsman from draining the pits completely each time. As a result, the level of the pit in many instances exceeded the standpipe permitting the liquid fraction to overflow the standpipe while retaining the solids. Therefore, the volume of manure produced per unit of time between samplings could not be measured and compared to data available in the literature.

Numerous interesting factors caused the wide variation in daily wet manure production. Several factors noted during the study were: (1) season of the year, (2) wash water, (3) water leaks, and (4) variations in the herd size and number. Herdsman Edwards (1975-1976) indicated feed consumption was approximately one-half normal during the months of July and August when temperatures ranged between 35°C and 40°C. The reduction

in the quantity of feed consumed will affect the quantity of manure generated per day requiring treatment.

Wash water diluted the manure and increased the total volume of manure requiring treatment. Weekly additions of wash water are common with confinement operations including farrower and nursery facilities. Approximately 19000 l of water was utilized per washing at the visited production facility. However, the volume of water used per washing will vary with farm management practices. A potential problem with biological treatment systems may also exist due to disinfectants commonly used when washing.

Water leaks, like wash water, diluted the manure suspension and increased the volume of manure needing treatment. However, the occurrence of major water leaks (i.e., broken water pipes) is not predictable and the volume of water added to the manure depends on the size of the leak and the time required to correct the problem. Water leaks were periodically a problem in the grower and finisher buildings.

Plots for the six buildings revealed the manure characteristics fluctuated considerably during the sampling period. The fluctuations in values obtained for the manure characterization study did not always reflect real fluctuations in manure production. Manure characteristics were thought to be influenced by factors not common to all manure collection systems. Factors were: (1) addition of water at the standpipe by the herdsman to promote drainage, (2) retention of solids in the pit while the liquid fraction passed freely over the standpipe, and (3) retention of settled solids in the pit when the pit was partially drained. The above factors caused artificial fluctuation of the manure characteristics. Decreases in TS and MLSS COD were generally noted

when the pits were drained or water leaks occurred. The decline in TS and MLSS COD concentrations after the pits were drained was thought to be principally due to the water additions by the herdsman. The characteristics of the liquid fraction were generally not as variable due to faster equilibration. The volume of manure retained in the pits was generally of sufficient mass so as to buffer the weekly fluctuations in the manure characteristics hoped to be monitored during the study. An average value for the daily flow could not be attained due to the problem with the lagoon. The farrower, nursery I and nursery II tended to dilute the daily manure stream.

Anaerobic Digestion

Digester Response to Five Dilutions of Swine Manure

The first 20 days of operation for each digester were considered to be a stabilization period and, therefore, not included when discussing the response of the individual digesters. The discussion of digester response to the various loading rates or dilutions was limited to the twenty-first through sixtieth day of operation unless stated otherwise. Discussion of each dilution or loading rate is presented separately. Appendixes E and F contain the feed characterization and digester response data for each digester respectively.

One-Seventh Dilution

Three digesters were fed the one-seventh (1/7) dilution--two during the first segment and one during the second segment of the study.

Figures 27, 28, and 29 are plots of feed TS, digester TS, and digester gas production versus days of operation for each of the three respective digesters. Table XXII summarizes the operating characteristics of the three digesters. The variation in effluent characteristics and initial conditions of Unit 1 compared to the other two digesters was due to the initial period when Unit 1 was fed a synthetic feed. A pumping problem also occurred in Unit 1 during the fifty-first day of operation. The digester effluent characteristics beyond the fiftieth day of operation were not representative of actual operating conditions because contents of the digester were no longer completely mixed. Therefore, the analysis of results for Unit 1 was limited to the twenty-first through fiftieth day of operation.

The overall response of the digesters to the 1/7 dilution was relatively stable. The average daily gas production per individual digester was between 290 and 360 ml/day. Average alkalinity per digester was between 2500 and 3000 mg/l as CaCO_3 . The average pH per digester was between 7.4 and 7.5. Average NH_4^+ - N concentration per digester was between 280 and 380 mg/l, well within good operating conditions. No problems were encountered with VA in either of the three digesters during the study. The VA concentrations in the digesters never exceeded 260 mg/l as HAC and the average VA concentration per digester was between 170 and 180 mg/l as HAC. The digesters typically had a thin surface scum and a thin layer of solids on the bottom when dismantled at the conclusion of the run.

Unit 3 was operated for an extended period of time until gas composition data could be obtained. Operating conditions remained stable throughout the extended period of operation. Daily gas production,

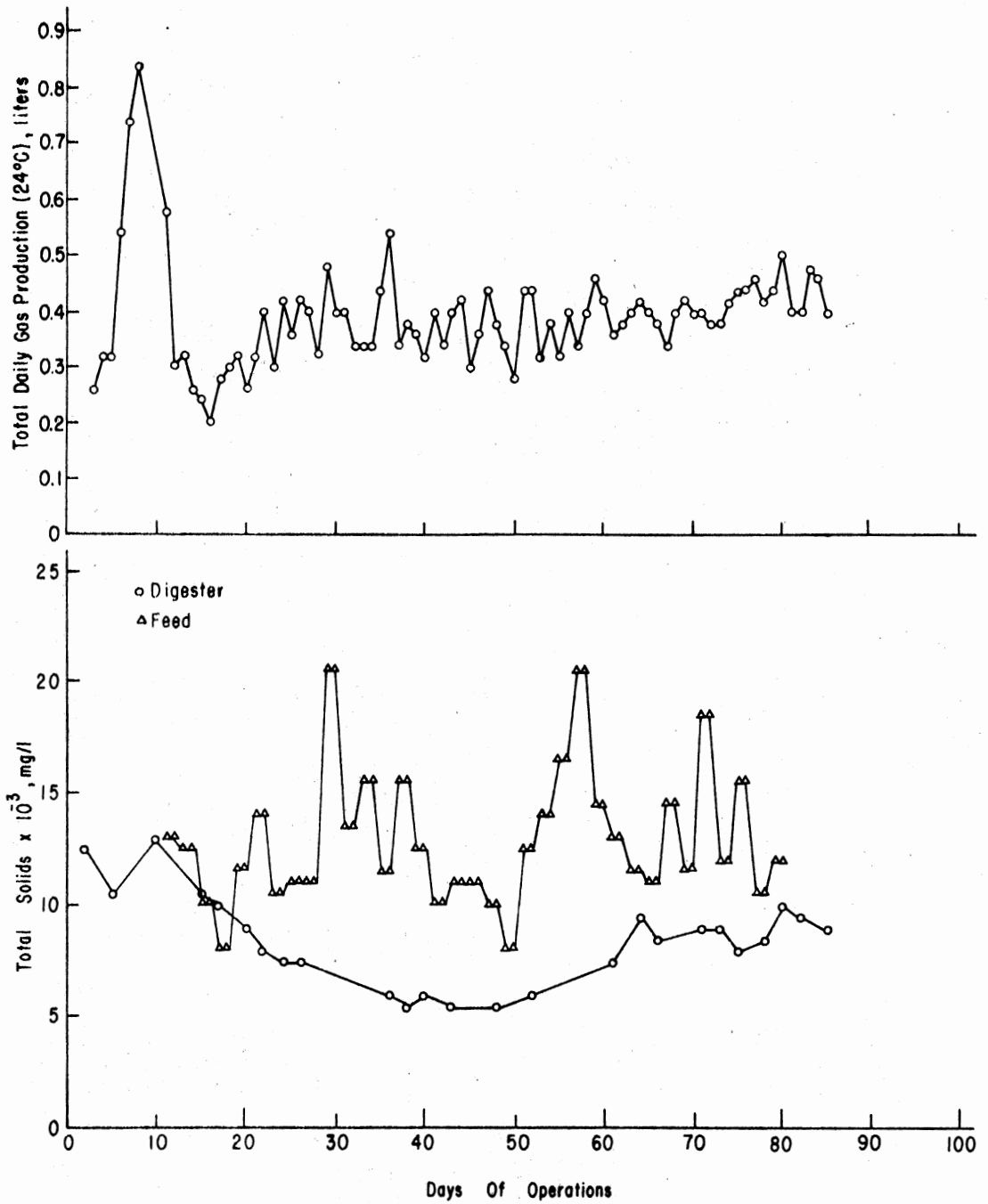


Figure 27. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on One-Seventh Dilution (March 9, 1976 to May 31, 1976)

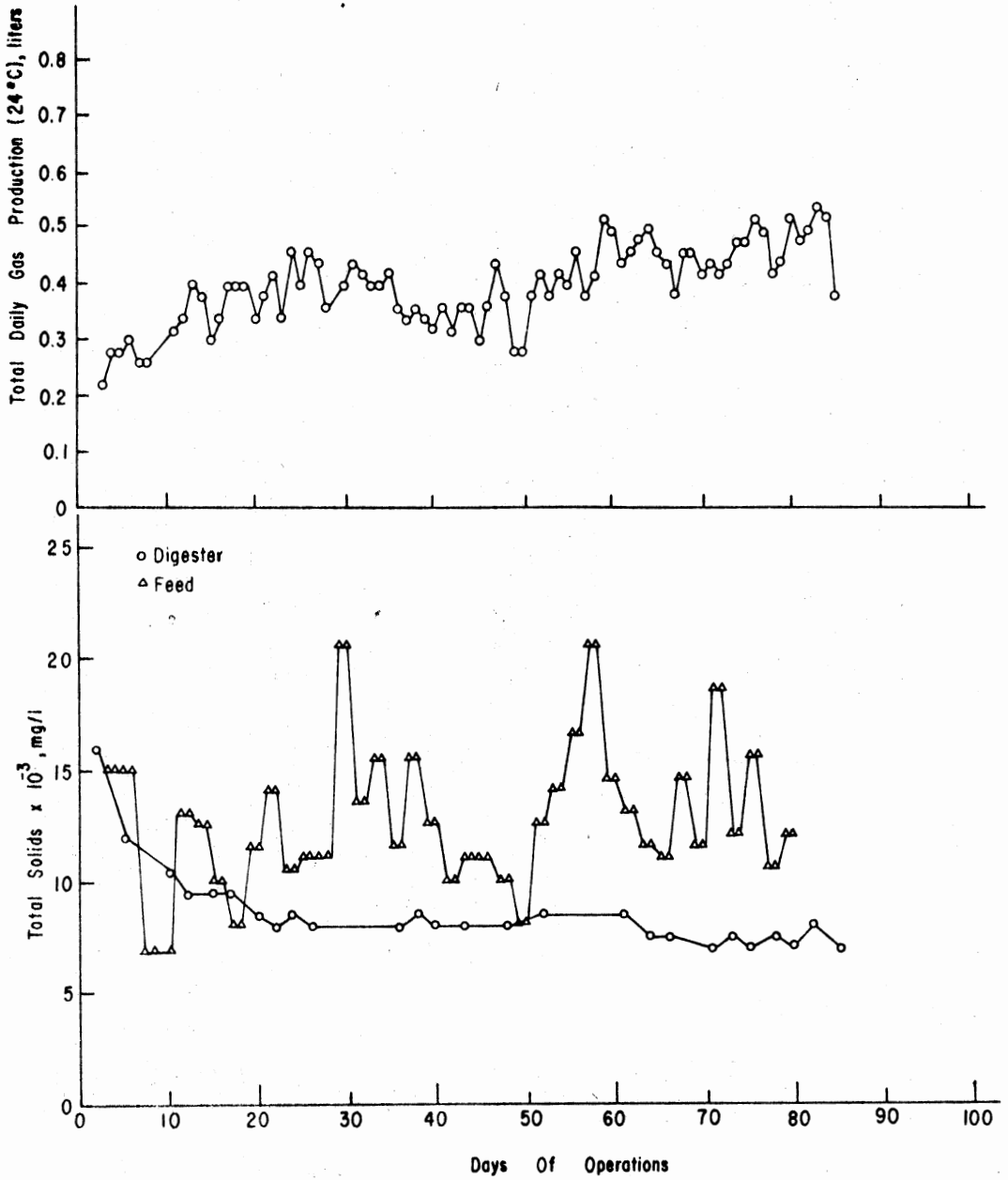


Figure 28. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Seventh Dilution (March 9, 1976 to May 31, 1976)

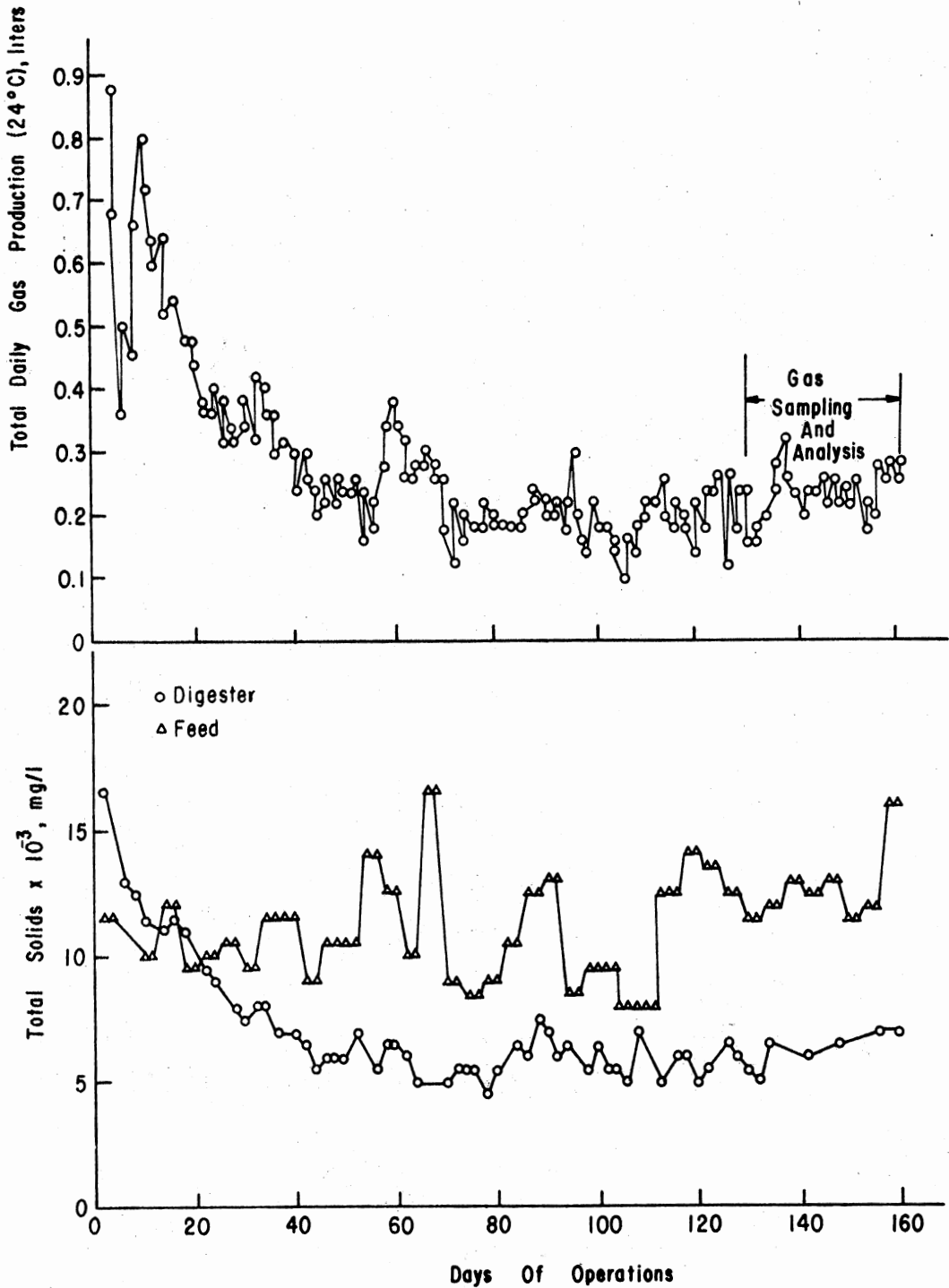


Figure 29. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the One-Seventh Dilution (June 10, 1976 to November 15, 1976)

TABLE XXII

DATA SUMMARY FOR DIGESTERS FED THE ONE-SEVENTH
DILUTION OF SWINE MANURE

Parameter	Unit #1	Unit #2	Unit #3
<u>Loading:</u>			
mg TS/l of digester/day*	550	600	550
Detention time, days	20	20	20
<u>Digester Influent:</u>			
TS, mg/l*	11000 (2000)**	12000 (3000)	11000 (1500)
VSS, mg/l*	7600 (1500)	8500 (2100)	7300 (1200)
COD MLSS, mg/l*	11000 (2000)	11400 (2000)	9500 (2200)
NH ₄ ⁺ - N, mg/l*	290 (40)	290 (40)	210 (70)
TVS, %*	72 (3)	72 (3)	74 (3)
SS, %*	85 (9)	86 (9)	88 (3)
VSS, %*	77 (6)	75 (7)	77 (3)
COD SP, %*	17 (5)	15 (5)	13 (5)
<u>Operating Conditions:</u>			
Duration, days	50	60	60
Temperature, °C*	34.6 (1.3)	34.7 (1.3)	34.5 (1.2)
Gas, ml/day*	360 (85)	360 (80)	290 (65)
pH*	7.4 (0.09)	7.5 (0.08)	7.5 (0.1)
Alkalinity, mg/l as CaCO ₃ *	2500 (180)	3000 (100)	2800 (400)
VA, mg/l as HAc*	170 (20)	180 (30)	170 (40)
<u>Digester Effluent:</u>			
TS, mg/l*	6000 (1000)	8000 (200)	7000 (1000)
VSS, mg/l*	2000 (300)	4500 (300)	4000 (600)
COD MLSS, mg/l*	3700 (600)	7600 (500)	6700 (900)
NH ₄ ⁺ - N, mg/l*	280 (40)	360 (50)	380 (80)
TVS, %*	44 (10)	63 (3)	64 (3)
SS, %*	46 (12)	79 (7)	76 (6)
VSS, %*	71 (10)	72 (7)	75 (5)
COD SP, %*	26 (2)	16 (1)	23 (3)
<u>Initial Conditions:</u>			
TS, mg/l	13000	16000	16000
VSS, mg/l	1900	5300	9500
COD MLSS, mg/l	3300	16000	15400
NH ₄ ⁺ - N, mg/l	150	340	240

*Average values.

**Value in parentheses is the standard deviation.

however, was below the expected volume. After 120 days of operation the digester was noted to be 300 to 500 ml below the 4.0 l operating level. The decline in digester volume was attributed to volume reduction due to solids degradation and spillage when servicing the stirring pump. The volume was returned to the design operating level and a slight improvement in daily gas production was noted.

One-Fifth Dilution

A digester was operated on the one-fifth (1/5) dilution during both the second and third segments of the study. Figures 30 and 31 are profiles of feed TS, digester TS, and digester gas production versus days of operation for the two respective digesters. Table XXIII summarizes the feed characteristics, operating conditions, digester effluent characteristics, and initial conditions for each digester.

The average volume of gas generated daily varied drastically between the two digesters. Unit 1 averaged 500 ml of gas per day. Unit 2, however, averaged only 220 ml of gas per day. The different initial conditions for the two digesters, particularly the NH_4^+ - N concentration, was partially responsible for the variation in gas production. The initial NH_4^+ - N concentration in Unit 2 was 780 mg/l, 3.25 times greater than the initial NH_4^+ - N concentration in Unit 1. The higher initial NH_4^+ - N concentration initially inhibited Unit 2. Also, the feed TS profile for Unit 2 (Figure 31) indicates the feed suspension was relatively weak during the first half of the run. The daily gas production for Unit 2 tended to increase with increased TS concentration in the feed suspension. Daily gas production for Unit 1, however, followed a decreasing trend, but appeared to be stabilizing after 60 days of operation.

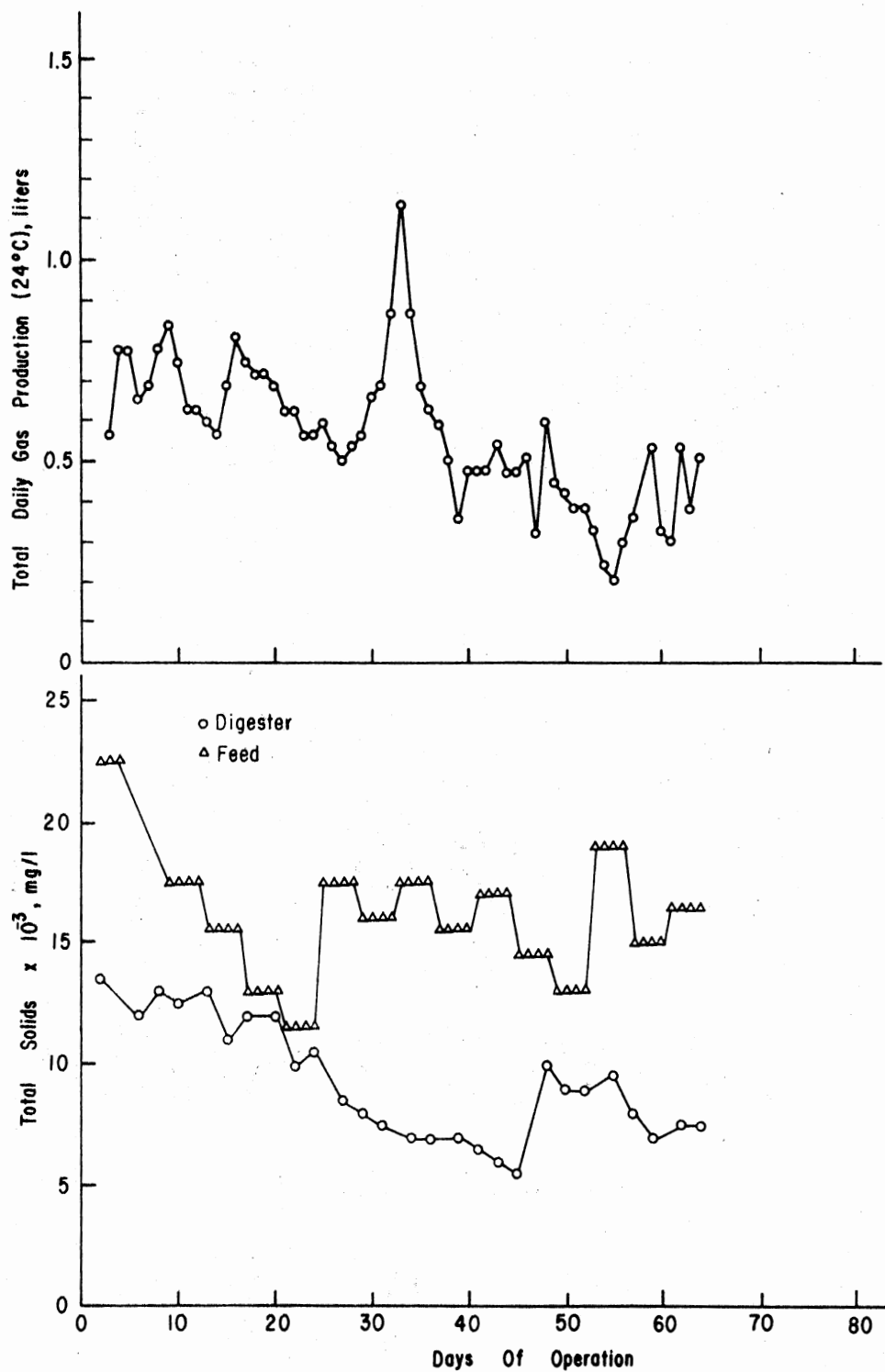


Figure 30. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Fifth Dilution (June 10, 1976 to August 11, 1976)

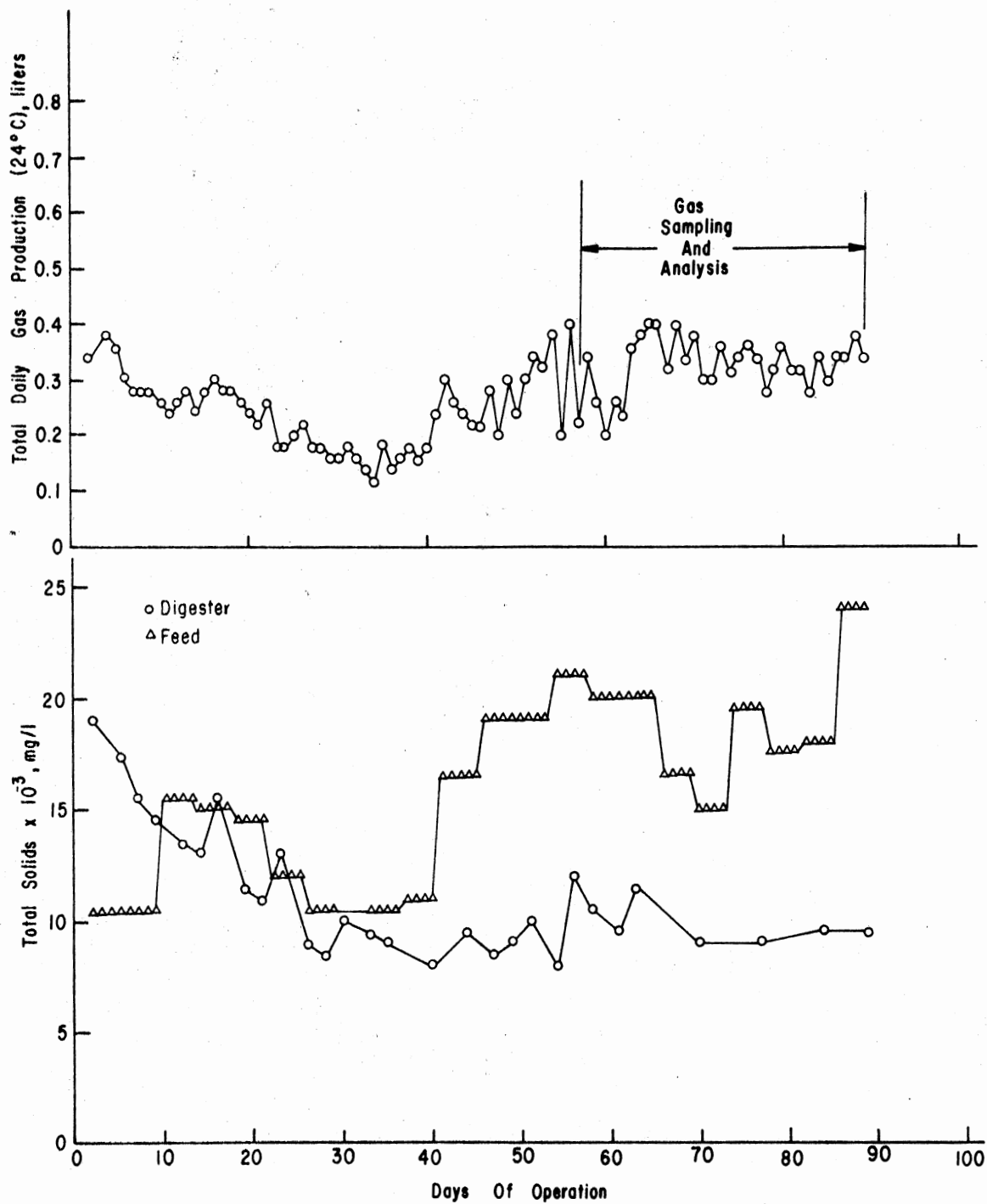


Figure 31. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Fifth Dilution (August 20, 1976 to November 15, 1976)

TABLE XXIII
 DATA SUMMARY FOR DIGESTERS FED THE ONE-FIFTH
 DILUTION OF SWINE MANURE

Parameter	Unit #1	Unit #2
<u>Loading:</u>		
mg TS/l of digester/day*	800	750
Detention time, days	20	20
<u>Digester Influent:</u>		
TS, mg/l*	16000 (1900)**	15000 (4000)
VSS, mg/l*	10000 (1600)	9700 (2900)
COD MLSS, mg/l*	13000 (2200)	13000 (4000)
NH ₄ ⁺ - N, mg/l*	300 (60)	370 (60)
TVS, %*	73 (2)	67 (2)
SS, %*	88 (7)	92 (6)
VSS, %*	79 (6)	70 (5)
COD SP, %*	14 (5)	6 (1)
<u>Operating Conditions:</u>		
Duration, days	60	60
Temperature, °C*	35.0 (1.3)	34.0 (1.1)
Gas, ml/day*	500 (170)	220 (70)
pH*	7.5 (0.2)	7.4 (0.1)
Alkalinity, mg/l as CaCO ₃ *	3200 (520)	3300 (400)
VA, mg/l as HAc*	190 (40)	190 (20)
<u>Digester Effluent:</u>		
TS, mg/l*	7700 (1400)	9400 (1400)
VSS, mg/l*	3600 (600)	6000 (1100)
COD MLSS, mg/l*	6600 (1200)	10000 (1200)
NH ₄ ⁺ - N, mg/l*	490 (80)	500 (80)
TVS, %*	57 (5)	70 (2)
SS, %*	62 (7)	84 (4)
VSS, %*	75 (7)	76 (6)
COD SP, %*	27 (4)	22 (3)
<u>Initial Conditions:</u>		
TS, mg/l	14000	19000
VSS, mg/l	6600	12000
COD MLSS, mg/l	12000	21000
NH ₄ ⁺ - N, mg/l	240	780

*Average values.

**Value in parentheses is the standard deviation.

Digester TS concentration also followed a decreasing trend during much of the run. A rapid increase in TS followed when the pump digester was cleaned after 44 days of operation. Therefore, poor mixing was thought to have influenced both the decline in digester TS concentration and gas production profiles for Unit 1.

The general operating characteristics of the two digesters were well within the range of good operating conditions. The two digesters had average alkalinities of 3200 and 3300 mg/l as CaCO_3 , respectively. The pH of the individual digesters averaged 7.4 and 7.5, respectively. Volatile acids were not a problem in either unit since the levels never exceeded 320 mg/l as HAc and averaged 190 mg/l as HAc. The NH_4^+ - N level in both digesters stabilized between 400 and 500 mg/l. A thin surface scum and a thin layer of solids on the bottom was noted with both digesters when each was dismantled at the conclusion of the run.

One-Third Dilution

Three digesters were fed the one-third (1/3) dilution of swine manure. Two digesters were operated at the 1/3 dilution during the first segment of the study and one during the second segment of the study. Plots of feed TS, digester TS, and digester gas production versus days of operation for each of the three digesters are presented in Figures 32, 33 and 34, respectively. Table XXIV summarizes the operating characteristics for the three digesters.

The three digesters functioned satisfactorily throughout the 60 day study period. Gas production by the three units was generally stable by the twenty-first day of operation. Gas production for Units 1 and 2 followed a slight increasing trend while Unit 3 maintained relatively

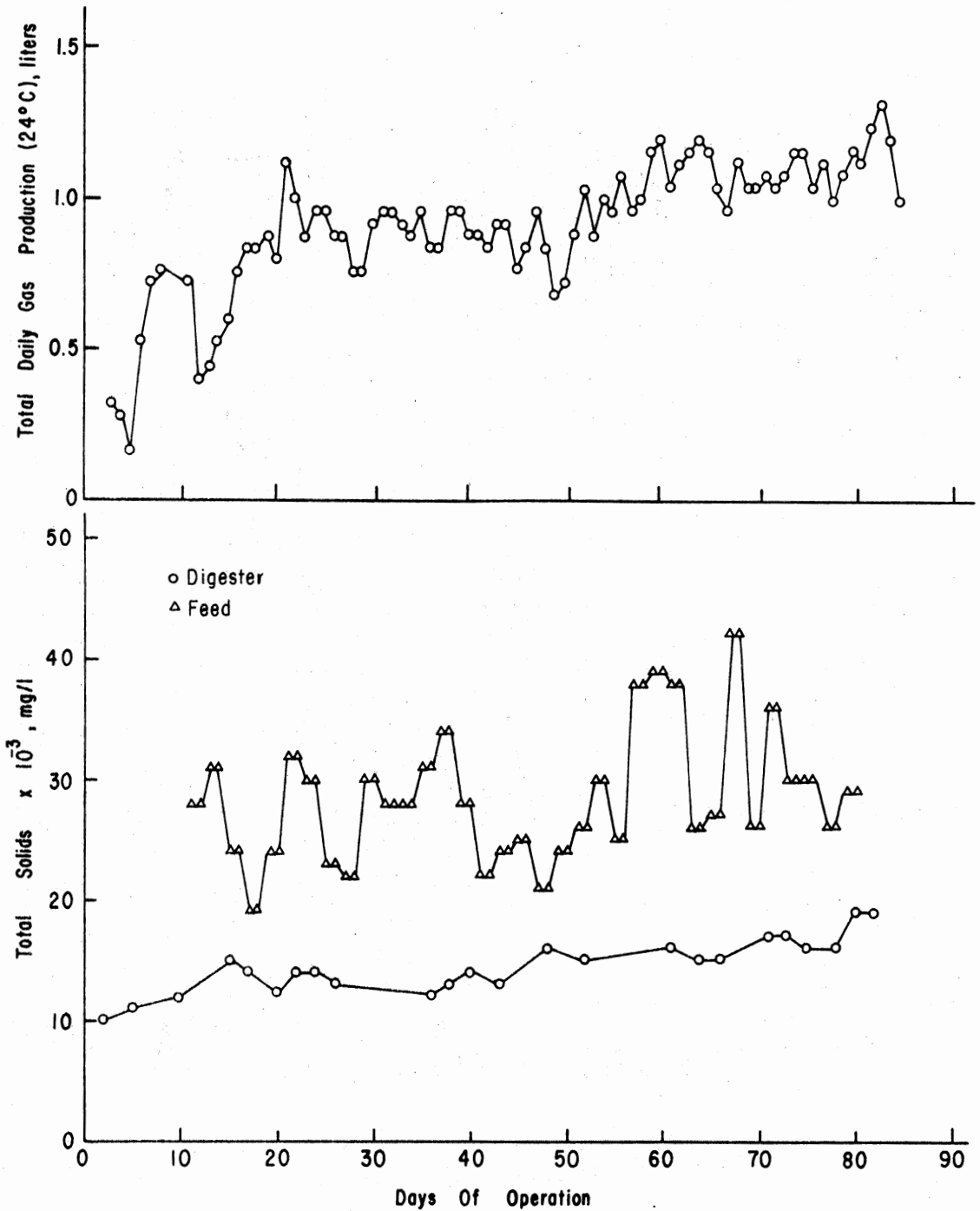


Figure 32. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Third Dilution (March 9, 1976 to May 31, 1976)

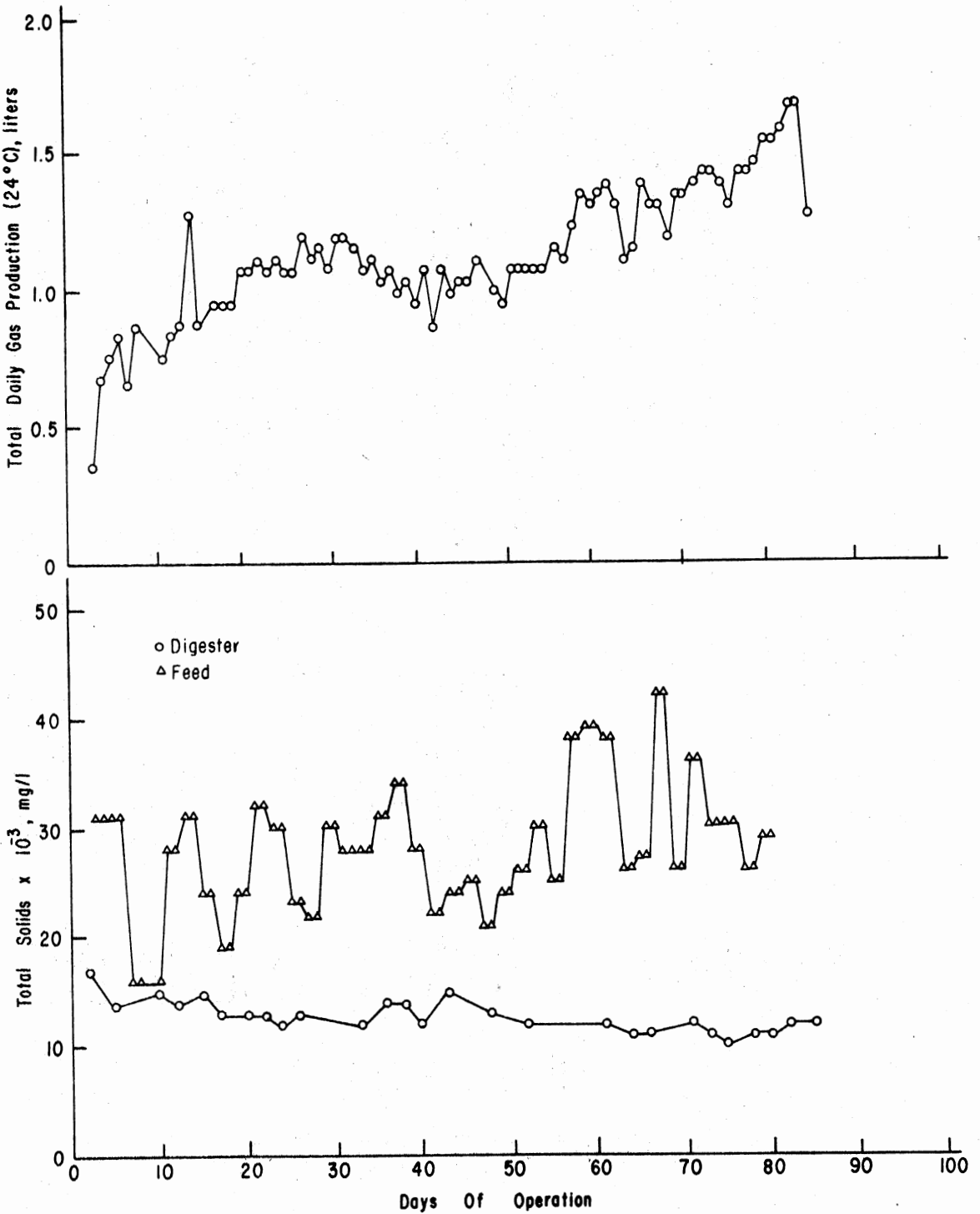


Figure 33. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Third Dilution (March 9, 1976 to May 31, 1976)

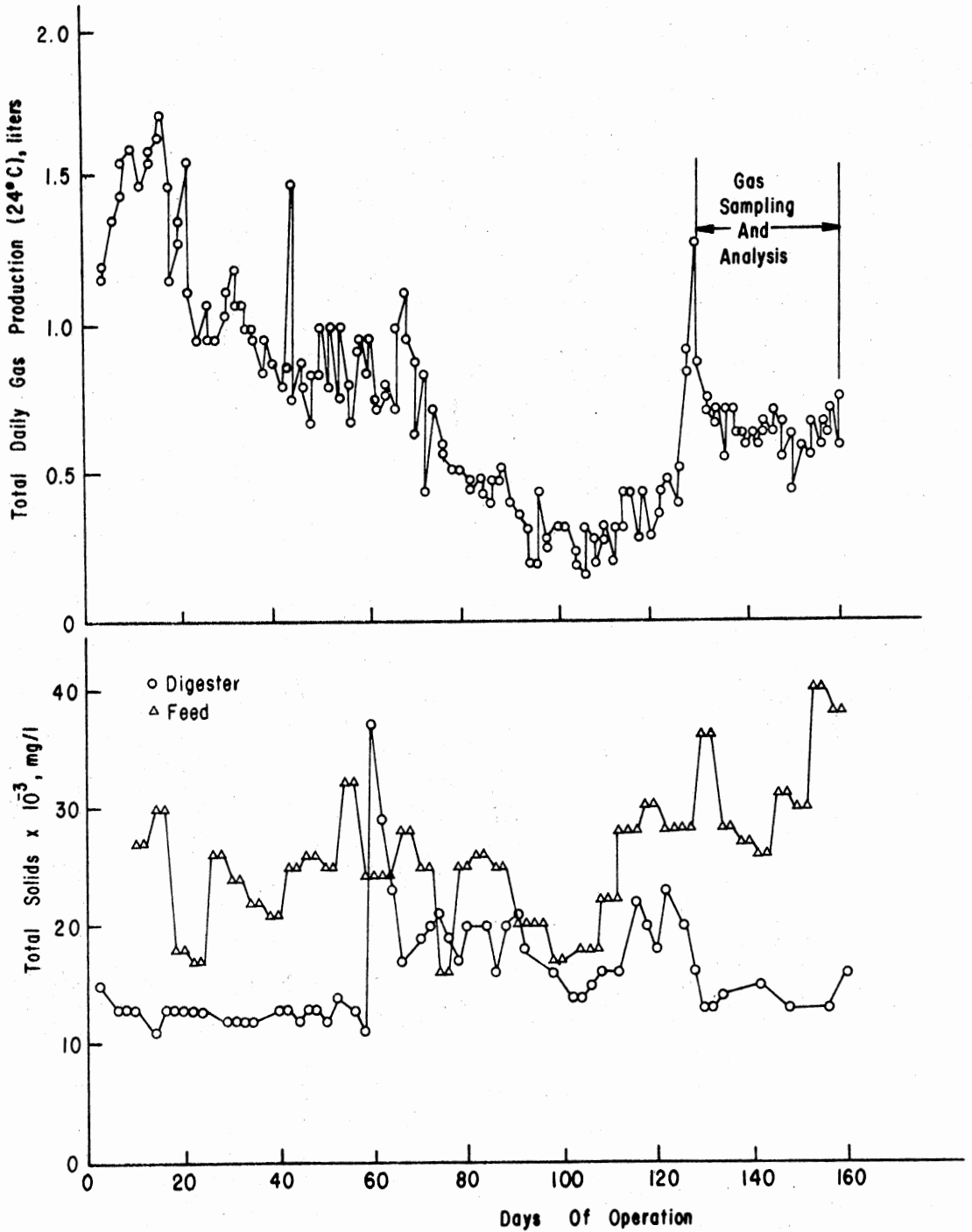


Figure 34. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the One-Third Dilution (June 10, 1976 to November 15, 1976)

TABLE XXIV

DATA SUMMARY FOR DIGESTERS FED THE ONE-THIRD
DILUTION OF SWINE MANURE

Parameter	Unit #1	Unit #2	Unit #3
<u>Loading:</u>			
mg TS/l of digester/day*	1400	1400	1200
Detention time, days	20	20	20
<u>Digester Influent:</u>			
TS, mg/l*	28000 (5000)**	28000 (5000)	24000 (3400)
VSS, mg/l*	18000 (4000)	18000 (4000)	17000 (2600)
COD MLSS, mg/l*	29000 (5000)	29000 (5000)	21000 (5500)
NH ₄ ⁺ - N, mg/l*	660 (80)	660 (80)	520 (130)
TVS, %*	70 (2)	70 (2)	72 (2)
SS, %*	89 (5)	89 (5)	92 (3)
VSS, %*	73 (7)	73 (7)	77 (6)
COD SP, %*	17 (6)	17 (6)	17 (7)
<u>Operating Conditions:</u>			
Duration, days	60	60	60
Temperature, °C*	34.8 (1.2)	34.5 (1.1)	35.5 (1.4)
Gas, ml/ day*	880 (130)	1080 (100)	920 (150)
pH*	7.6 (0.2)	7.7 (0.1)	7.5 (0.09)
Alkalinity, mg/l as CaCO ₃ *	4710 (750)	5490 (250)	5030 (400)
VA, mg/l as HAc*	170 (40)	200 (20)	210 (60)
<u>Digester Effluent:</u>			
TS, mg/l*	13000 (1400)	12000 (1000)	12000 (700)
VSS, mg/l*	6700 (2100)	7300 (1000)	7400 (700)
COD MLSS, mg/l*	11000 (2500)	11000 (600)	13000 (1400)
NH ₄ ⁺ - N, mg/l*	600 (140)	700 (90)	710 (100)
TVS, %*	57 (11)	65 (4)	69 (3)
SS, %*	65 (13)	75 (4)	80 (5)
VSS, %*	75 (8)	78 (7)	78 (4)
COD SP, %*	18 (2)	20 (4)	24 (6)
<u>Initial Conditions:</u>			
TS, mg/l	9500	16000	14000
VSS, mg/l	1400	5000	7400
COD MLSS, mg/l	3500	14000	14000
NH ₄ ⁺ - N, mg/l	160	360	230

*Average values.

**Value in parentheses is the standard deviation.

stable gas production during the 21 to 60 day period. Several of the other pertinent operational characteristics, however, took longer to fully stabilize. The average pH per digester was between 7.5 and 7.7. Alkalinity concentrations in the digesters stabilized between 5000 and 6000 mg/l as CaCO_3 . Similarly, NH_4^+ - N concentrations in the digesters stabilized between 800 and 900 mg/l. The VA concentration was typically between 170 and 210 mg/l as HAC. The average VA level per individual digester never exceeded 360 mg/l as HAC. A surface scum layer and a layer of settled solids were noted in each digester at the conclusion of run.

Unit 3 was operated beyond the 60 day test period until gas composition could be determined. Although operating conditions remained stable throughout the extended period of operation, the daily gas production profile for Unit 3 (Figure 34) indicates gas production declined substantially between 70 and 124 days of operation. The decline in gas production was due to a combination of effects. A problem was encountered with the mixing pump at the end of the 60 day test period. Failure to adequately mix digester permitted solids to settle and accounted for the high TS content in the digester effluent during the same period. Also, the feed TS profile for Unit 3 (Figure 34) shows the solid content of the feed was below average during the corresponding 54 day period. Inspection of the digester after 120 days of operation revealed the level was 500 to 600 ml below the 4.0 l mark. The decline in the digester volume was attributed to volume reduction due to solids degradation and spillage occurring when servicing the mixing pump. The volume was returned to the 4.0 l mark. The daily gas production for the digester approached normal once the level of the digester was corrected and the concentration of solids in the feed increased.

One-Half Dilution

A digester was fed the one-half (1/2) dilution during both the second and third segments of the study. Figures 35 and 36 are plots of feed TS, digester TS, and digester daily gas production versus days of operation for each unit, respectively. Table XXV summarizes the feed characteristics, operating conditions, digester effluent characteristics, and initial conditions for both digesters. The analyses of digester response data were limited to 54 days of operation for both units because of pump problems. The pump on Unit 2 was repaired and the unit was maintained until composition of the gas was determined.

The daily gas production by the two digesters was noticeably different. Unit 1 averaged 1350 ml of gas per day. A comparison of the gas production profiles for both digesters over the initial 20 days of operation indicated the seed material used to start Unit 1 was more biologically active than the seed used to start Unit 2. Daily gas production by Unit 1 was declining during the initial 20 day period but stabilized around 1300 ml/day after 20 days of operation. Daily gas production by Unit 2 increased throughout the study and did not stabilize during the 60 day test period. Gas production by Unit 2 continued to increase and was approaching the gas production rate of Unit 1 by the seventieth day of operation. The initial NH_4^+ - N concentration in Unit 2 was 990 mg/l, 3.2 times greater than the initial NH_4^+ - N concentration in Unit 1. The higher initial NH_4^+ - N inhibited Unit 2 and retarded stabilization of the system. The digester TS profile for Unit 2 (Figure 36) shows a rapid increase in TS after the pump was replaced on the fifty-fourth day of operation. The rapid rise in TS was due to solids being

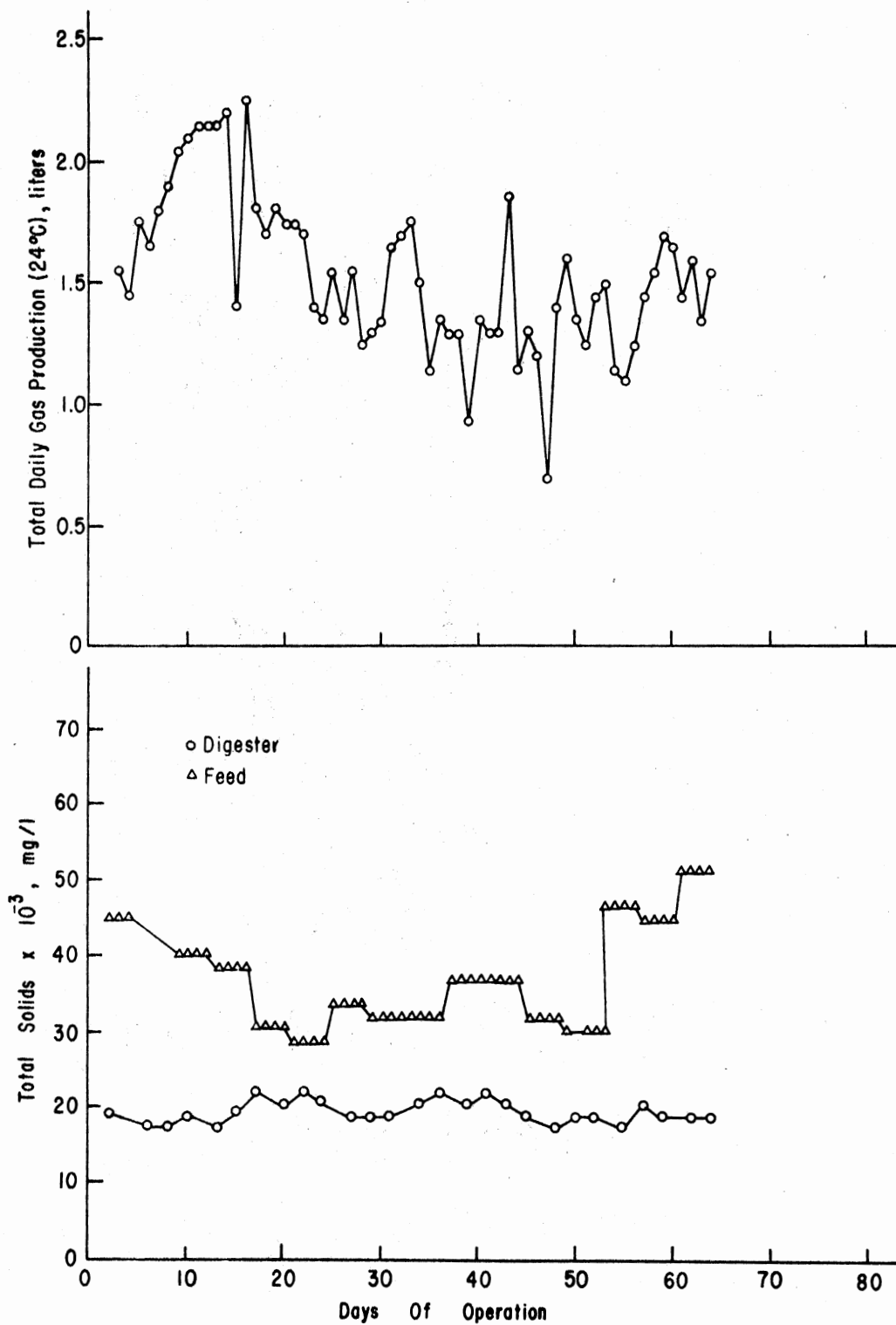


Figure 35. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the One-Half Dilution (June 10, 1976 to August 11, 1976)

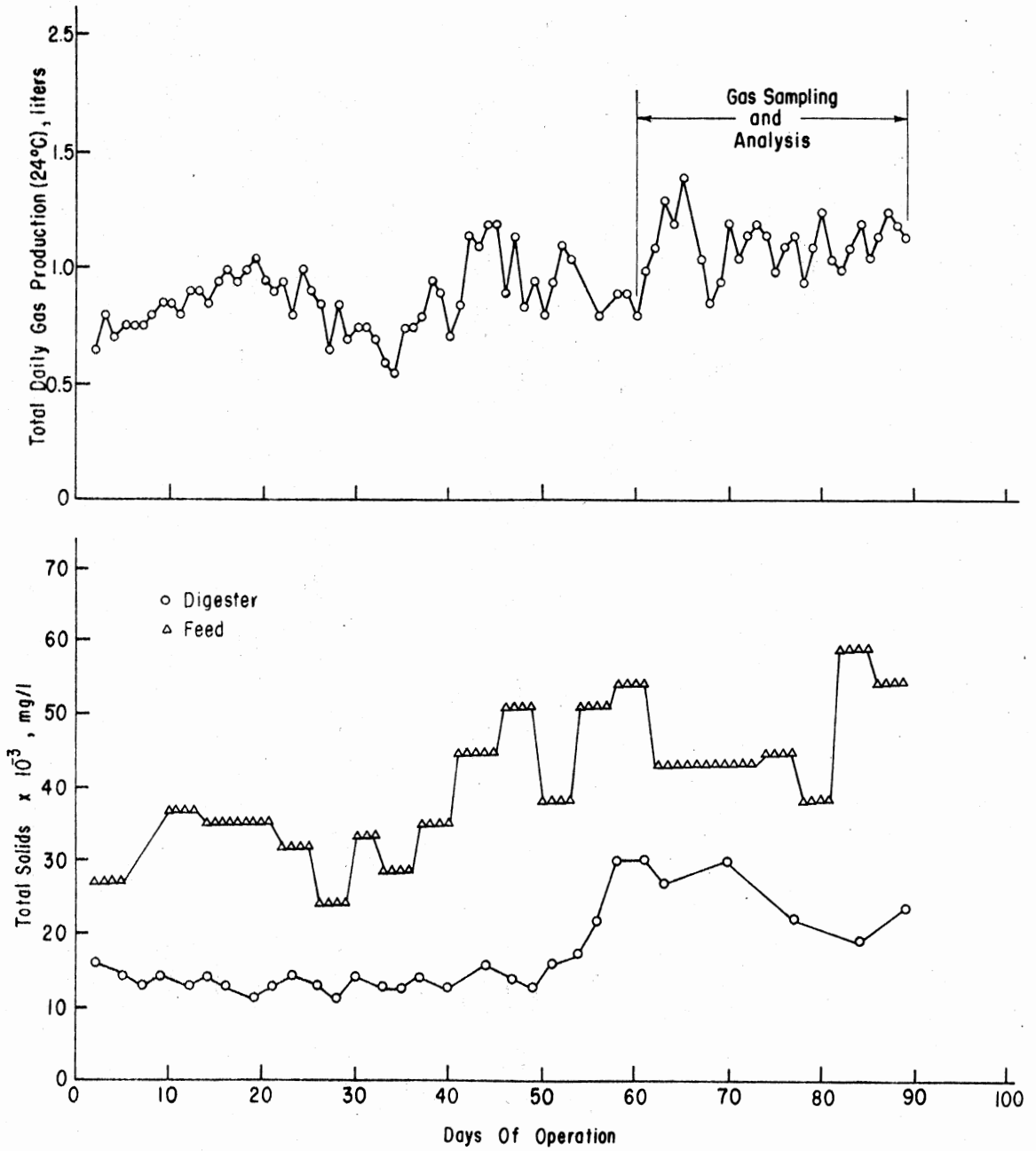


Figure 36. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the One-Half Dilution (August 20, 1976 to November 15, 1976)

TABLE XXV
 DATA SUMMARY FOR DIGESTERS FED THE ONE-HALF
 DILUTION OF SWINE MANURE

Parameter	Unit #1	Unit #2
<u>Loading:</u>		
mg TS/l of digester/day*	1650	1800
Detention time, days	20	20
<u>Digester Influent:</u>		
TS, mg/l*	33000 (4700)**	36000 (8700)
VSS, mg/l*	22000 (3400)	23000 (5500)
COD MLSS, mg/l*	31000 (5400)	30000 (5900)
NH ₄ ⁺ - N, mg/l*	810 (170)	690 (140)
TVS, %*	70 (3)	65 (3)
SS, %*	90 (2)	95 (2)
VSS, %*	74 (3)	67 (3)
COD SP, %*	19 (6)	7 (1)
<u>Operating Conditions:</u>		
Duration, days	54	54
Temperature, °C*	35.3 (1.2)	34.4 (1.4)
Gas, ml/day*	1350 (230)	860 (180)
pH*	7.7 (0.08)	7.4 (0.08)
Alkalinity, mg/l as CaCO ₃ *	7400 (560)	4900 (280)
VA, mg/l as HAc*	270 (50)	210 (30)
<u>Digester Effluent:</u>		
TS, mg/l*	19000 (1300)	13000 (1500)
VSS, mg/l*	12000 (1000)	8500 (1500)
COD MLSS, mg/l*	20000 (1400)	14000 (2200)
NH ₄ ⁺ - N, mg/l*	930 (100)	860 (80)
TVS, %*	70 (2)	71 (3)
SS, %*	82 (4)	82 (3)
VSS, %*	77 (5)	78 (5)
COD SP, %*	24 (3)	26 (3)
<u>Initial Conditions:</u>		
TS, mg/l	18000	16000
VSS, mg/l	9300	9200
COD MLSS, mg/l	16000	17000
NH ₄ ⁺ - N, mg/l	310	990

*Average values.

**Value in parentheses is the standard deviation.

picked up from the layer typically noted on the bottom of digesters by the improved circulation of the new pump. The TS level in Unit 2 stabilized again after two weeks and was comparable to the TS level in Unit 1.

General operating characteristics of the two digesters were within acceptable limits. The alkalinity and pH of the two digesters stabilized between 6500 and 7000 mg/l as CaCO_3 , and 7.5 and 7.7 respectively. The NH_4^+ - N concentrations characteristically leveled off between 850 and 950 mg/l. Volatile acids (VA) buildup posed no problem in either digester. The two digesters had average VA concentrations of 210 and 270 mg/l as HAC, respectively. The VA concentration never exceeded 440 mg/l in either unit. A gaseous scum layer of solids and a layer of settled solids were noted in each digester when dismantled at the conclusion of the run. The scum layers were also noted to contain hair.

Straight Dilution

Three digesters were fed the straight manure solution prepared to represent the daily manure flow from the farrow to finish production facilities. Two digesters were maintained on straight feed during the first segment of the study. A single digester was fed the straight feed solution during the second segment of the study. Figures 37, 38 and 39 are plots of feed TS, digester TS, and digester gas production versus days of operation for each of the three respective digesters. Table XXVI summarizes the operating characteristics for the three digesters.

The daily gas production by each of the three digesters stabilized within the first 20 days of operation. Although the daily gas production for Unit 1 appeared to be declining by the fiftieth day of

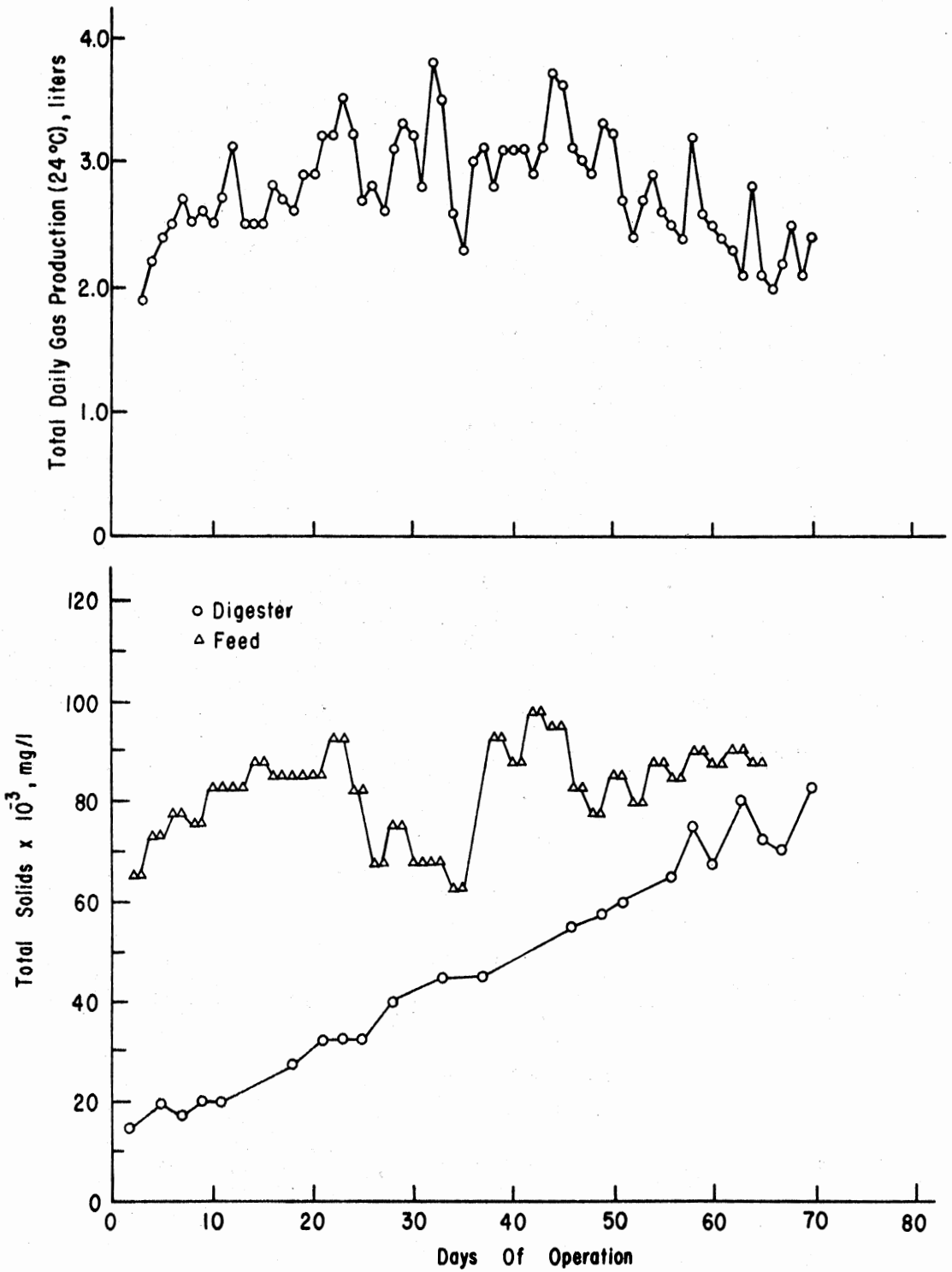


Figure 37. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the First Unit Operated on the Straight Dilution (March 24, 1976 to May 31, 1976)

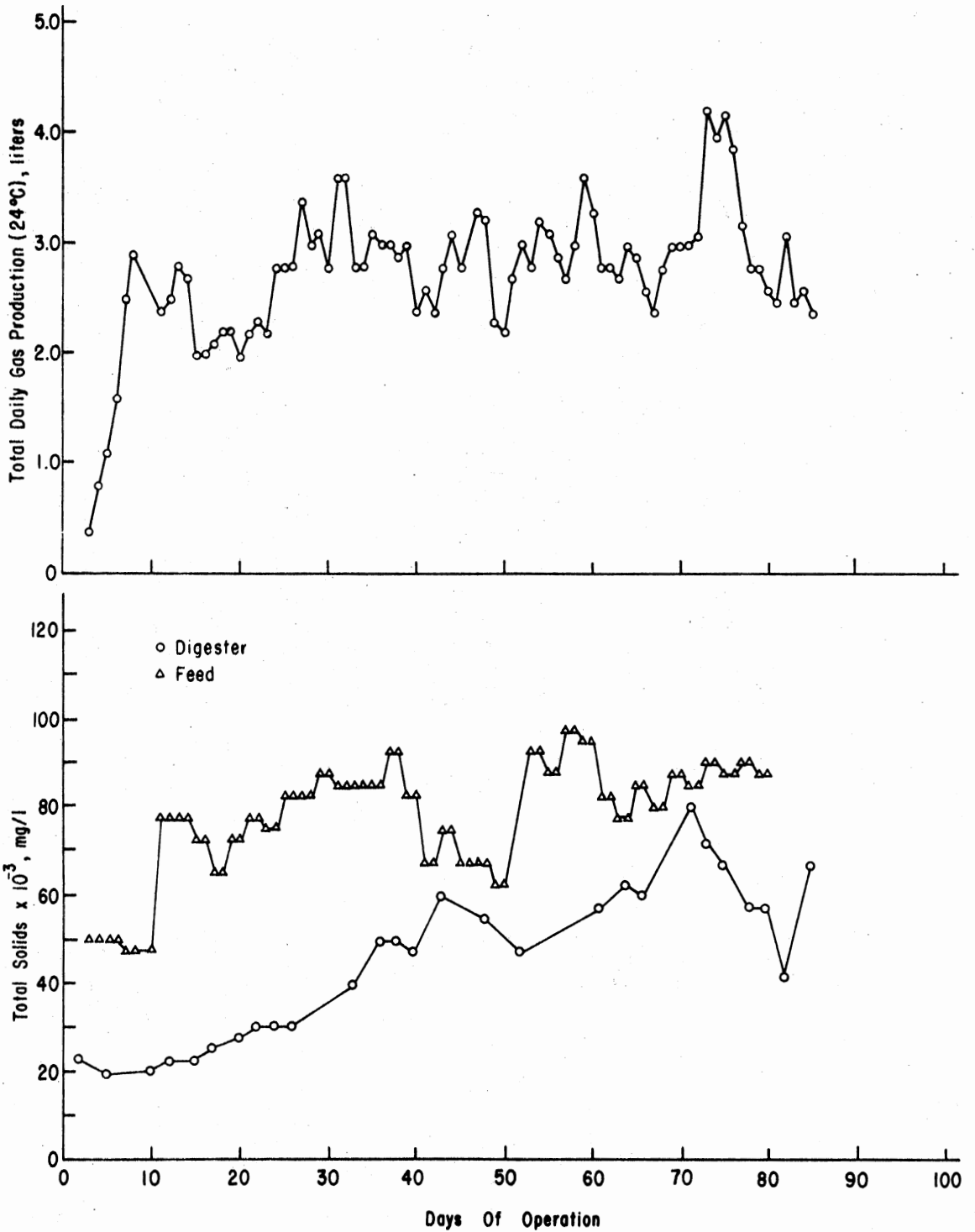


Figure 38. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Second Unit Operated on the Straight Dilution (March 9, 1976 to May 31, 1976)

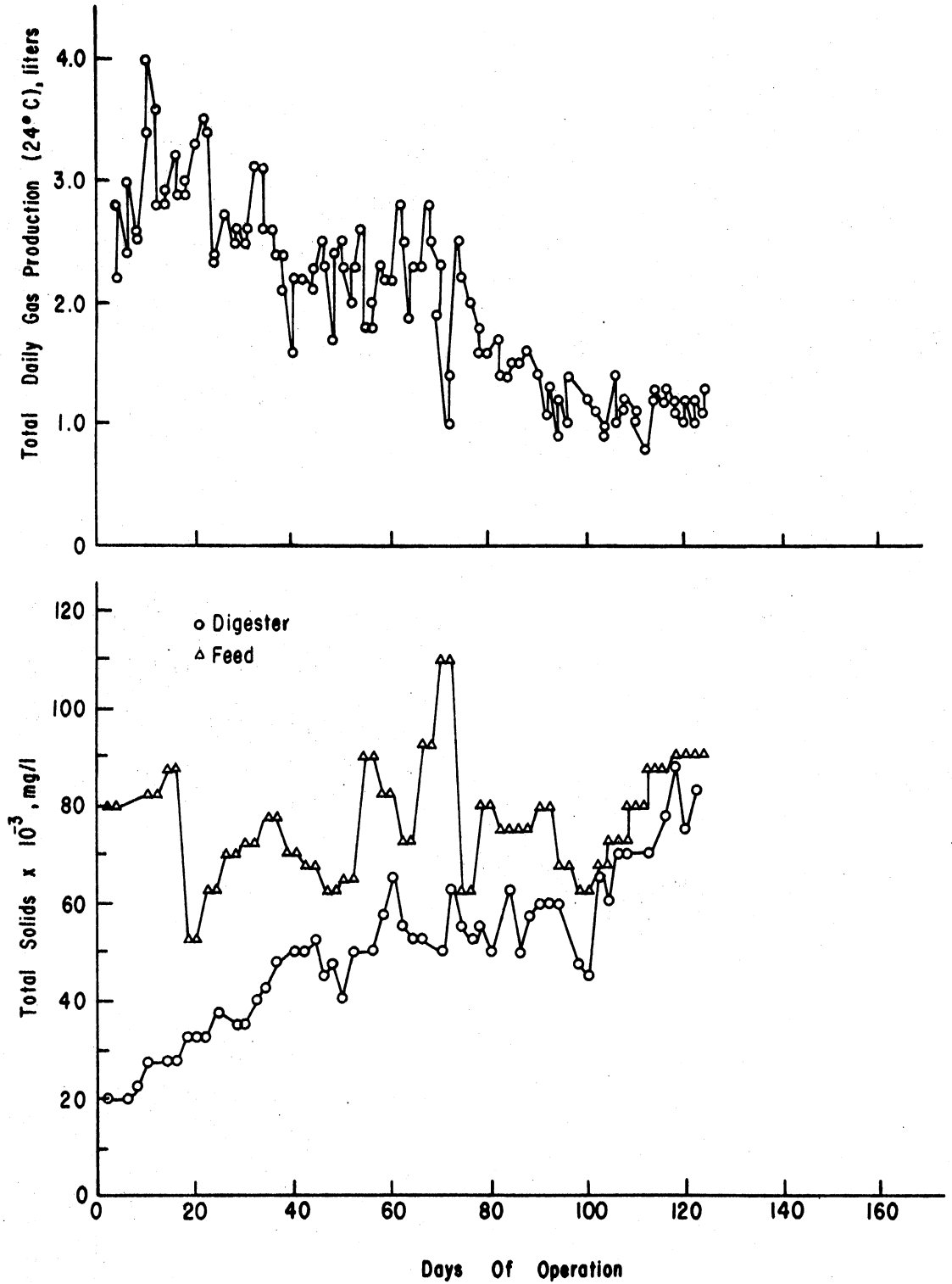


Figure 39. Feed TS, Digester TS, and Digester Gas Production Versus Days of Operation for the Third Unit Operated on the Straight Dilution (June 10, 1976 to October 7, 1976)

TABLE XXVI

DATA SUMMARY FOR DIGESTERS FED THE STRAIGHT
SWINE MANURE SUSPENSION

Parameter	Unit #1	Unit #2	Unit #3
<u>Loading:</u>			
mg TS/l of digester/day*	4100	3950	3550
Detention time, days	20	20	20
<u>Digester Influent:</u>			
TS, mg/l*	82000 (10000)**	79000 (12000)	71000 (8400)
VSS, mg/l*	53000 (6200)	52000 (6300)	45000 (5800)
COD MLSS, mg/l*	74000 (13000)	72000 (8400)	59000 (16000)
NH ₄ ⁺ - N, mg/l*	2120 (330)	2080 (360)	1630 (340)
TVS, %*	69 (1)	68 (2)	68 (2)
SS, %*	91 (2)	92 (3)	91 (3)
VSS, %*	71 (2)	70 (3)	70 (3)
COD SP, %*	24 (6)	24 (6)	20 (5)
<u>Operating Conditions:</u>			
Duration, days	60	60	60
Temperature, °C*	35.1 (1.1)	34.9 (1.4)	35.7 (1.2)
Gas, ml/day*	2800 (440)	2860 (350)	2340 (380)
pH*	8.0 (0.08)	8.0 (0.1)	7.9 (0.07)
Alkalinity, mg/l as CaCO ₃ *	17200 (2800)	16300 (2800)	14400 (900)
VA, mg/l as HAc*	2680 (1450)	1360 (900)	570 (220)
<u>Digester Effluent:</u>			
TS, mg/l*	57000 (17000)	44000 (11000)	44000 (8900)
VSS, mg/l*	38000 (12000)	27000 (8400)	29000 (6400)
COD MLSS, mg/l*	68000 (31000)	54000 (17000)	45000 (12000)
NH ₄ ⁺ - N, mg/l*	2540 (410)	2240 (510)	1790 (190)
TVS, %*	71 (3)	67 (3)	71 (1)
SS, %*	87 (5)	85 (6)	86 (5)
VSS, %*	76 (3)	71 (3)	76 (3)
COD SP, %*	25 (7)	22 (5)	21 (5)
<u>Initial Conditions:</u>			
TS, mg/l	15000	19000	19000
VSS, mg/l	6200	8900	11000
COD MLSS, mg/l	11000	18000	19000
NH ₄ ⁺ - N, mg/l	650	550	1030

*Average values.

**Value in parentheses is the standard deviation.

operation, daily gas production by Units 2 and 3 remained relatively stable throughout the 60 day test period. The TS concentrations in each of the digesters continually increased throughout the 40 day response period. The continued increase in the TS levels in the three digesters was the result of the seed material TS content being less than the normal operating TS levels. The TS concentration in the three units, as a result, were exhibiting a dilute-in phenomenon. The fluctuations in TS concentration at the end of the run in Unit 2 was due to pumping problems.

The general operating characteristics for the three units took longer than the initial 20 days to stabilize. The pH for the digesters stabilized between 7.9 and 8.0. The average alkalinity per digester was between 14400 and 17200 mg/l as CaCO_3 , but the alkalinities appeared to finally level off between 18000 and 20000 mg/l as CaCO_3 . The NH_4^+ - N concentrations stabilized in the 1800 to 2700 mg/l range. Alkalinity, pH, and NH_4^+ - N levels exceeded values accepted for correctly functioning digesters. The VA concentrations in the three units varied considerably. Unit 1 had VA concentrations ranging between 2000 and 4000 mg/l as HAC near the end of the 60 day trial. The VA concentrations in Units 2 and 3 were lower than Unit 1 and ranged between 600 and 1300 mg/l as HAC.

Each digester had a scum layer on the surface and a solids layer on the bottom when they were dismantled at the conclusion of the run. Both layers were thicker than any noted with the other digesters. The scum layer again contained hair.

Digester 3 was operated for an extended period until gas samples could be taken and analyzed for composition. However, before the gas

could be sampled, the mixing pump line broke and a large portion of the contents of the unit was lost. The volume of material lost made it impossible to restart and stabilize the unit in time for gas analyses. Inspection of the digester after the line breakage revealed the level was 500 to 700 ml below the 4.0 l operating volume. The reduced volume was attributed to solids degradation and spillage occurring when servicing the mixing pump. The pump had to be serviced frequently during the extended period because of hair clogging the pump. The reduced volume was thought to be a primary cause for the decline in gas production noted after 80 days of operation.

Finisher

A digester was fed during the second and third segment of the study manure taken directly from the finishing building. The 60 day study period, however, was too short for the digesters to achieve stability. Pumping problems were frequently experienced during both trials due to the extremely thick manure suspension and hair. Foaming was also a problem in both trials, particularly Trial 2. Pumping problems and foaming made it difficult to maintain the 4.0 l digester volume. A formal data summary for the two trials has been omitted because of aforementioned conditions and problems.

The general operating characteristics at the conclusion of the study for the two digesters were indicative of eventual digester failure. The daily gas production by the two units exhibited declining trends, particularly Unit 1. The digesters were producing 800 to 1000 ml of gas/day at the conclusion of the study. The VA concentrations in the two digesters were noticeably different. Unit 1 had a maximum VA concentration

of 10000 mg/l as HAc but the VA concentration typically ranged between 5500 and 6500 mg/l as HAc. Unit 2, however, generally had VA concentrations in the 1000 mg/l as HAc range. The variation in VA concentrations between the two units was due to a difference in biological activity. Based on the daily gas production records for the two units, Unit 2 was not as biologically active as Unit 1. The pH in the units ranged between 7.6 and 7.8. The TS and NH_4^+ - N concentrations in the digesters continually increased throughout the study and ranged between 95000 to 110000 mg/l and 3000 to 3400 mg/l, respectively, when the trials were terminated. The alkalinity in each unit also continually increased initially but appeared to stabilize between 20000 and 25000 mg/l as CaCO_3 .

The surface of each digester was covered with a two to three cm thick scum layer when the digesters were dismantled. A layer of solids was also noted at the bottom of each digester.

Gas Composition

Gas samples were analyzed for composition during the 24 days (October 8, 1976 to November 10, 1976) at the end of the third segment of the study. Procedures used to determine gas composition and raw data for the gas composition work are presented in Appendix G. Gas was sampled and analyzed eight times during the 24 day period. Samples were taken from digesters operating on 1/7, 1/5, 1/3, and 1/2 dilutions. The digester operating on the straight feed solution was lost prior to the initiation of gas analyses due to a system malfunction previously discussed. Therefore, no gas composition data is available for the straight loading rate. Gas samples, however, were taken and analyzed

for composition from a digester being fed manure taken directly from the finisher.

Table XVII is a summary of the gas composition results. The gas sample taken on October 18, 1976, from the 1/7 digester did not truly represent the gas generated due to a sampling error and the sample was therefore not included in the analyses. The data presented in Table XVII indicates gas samples taken from the 1/7 and 1/5 digesters contained a higher percentage of O_2 . The reason for the unusually high O_2 content was attributed to a sampling problem. Both digesters had the smaller 0.25 l gas collection cylinder because they typically generated less gas than the other digesters. The daily volume of gas generated by the two digesters was apparently insufficient to completely purge the sampling vessel prior to collecting the sample.

Analysis of variance (shown in Appendix H) indicated a significant difference ($\alpha = 0.01$) in percent of CH_4 content due to the different dilutions or loading rates. Duncan's new multiple range test was used to compare treatment means ($\alpha = 0.01$) (Steel and Torrie, 1960). Range test is located in Appendix H. Table XVIII summarizes the results of the multiple range test.

Figure 40 is a plot of the average CH_4 content of the digester gas versus the average daily loading rate. Linear regression was undertaken to determine the best fit equation describing the effect of average daily loading rate on methane content of digester gas. A second order polynomial was found to provide the best fit line. The equation was:

$$MC = 85.8 - 0.016 DLR + 0.0000026 DLR^2 \quad (1)$$

where MC = methane content, %; DLR = daily loading rate, mg TS/l of digester. Equation 1 had a correlation coefficient (R^2) of 0.84 and

TABLE XXVII
SUMMARY OF THE GAS COMPOSITION RESULTS

Feed Dilution	CH ₄		CO ₂		O ₂	
	Mean (%)	Standard Deviation	Mean (%)	Standard Deviation	Mean (%)	Standard Deviation
1/7	76.4	2.8	16.0	2.2	7.6	1.7
1/5	74.6	1.2	19.2	1.2	6.2	0.7
1/3	66.8	1.5	30.4	1.6	2.8	0.4
1/2	62.0	1.4	35.3	2.7	2.7	1.5
Finisher	62.9	4.4	34.6	3.8	2.5	1.2

TABLE XVIII

SUMMARY OF DUNCAN'S NEW MULTIPLE RANGE TEST OF TREATMENT MEANS FOR PERCENT METHANE IN THE DIGESTER GAS ($\alpha = 0.01$)*

Treatment			
1/7	1/5	1/3	1/2
76.2	74.6	66.8	<u>62.0</u>

*Any two means not underlined by the same line are significantly different. Any two means underlined by the same line are not significantly different.

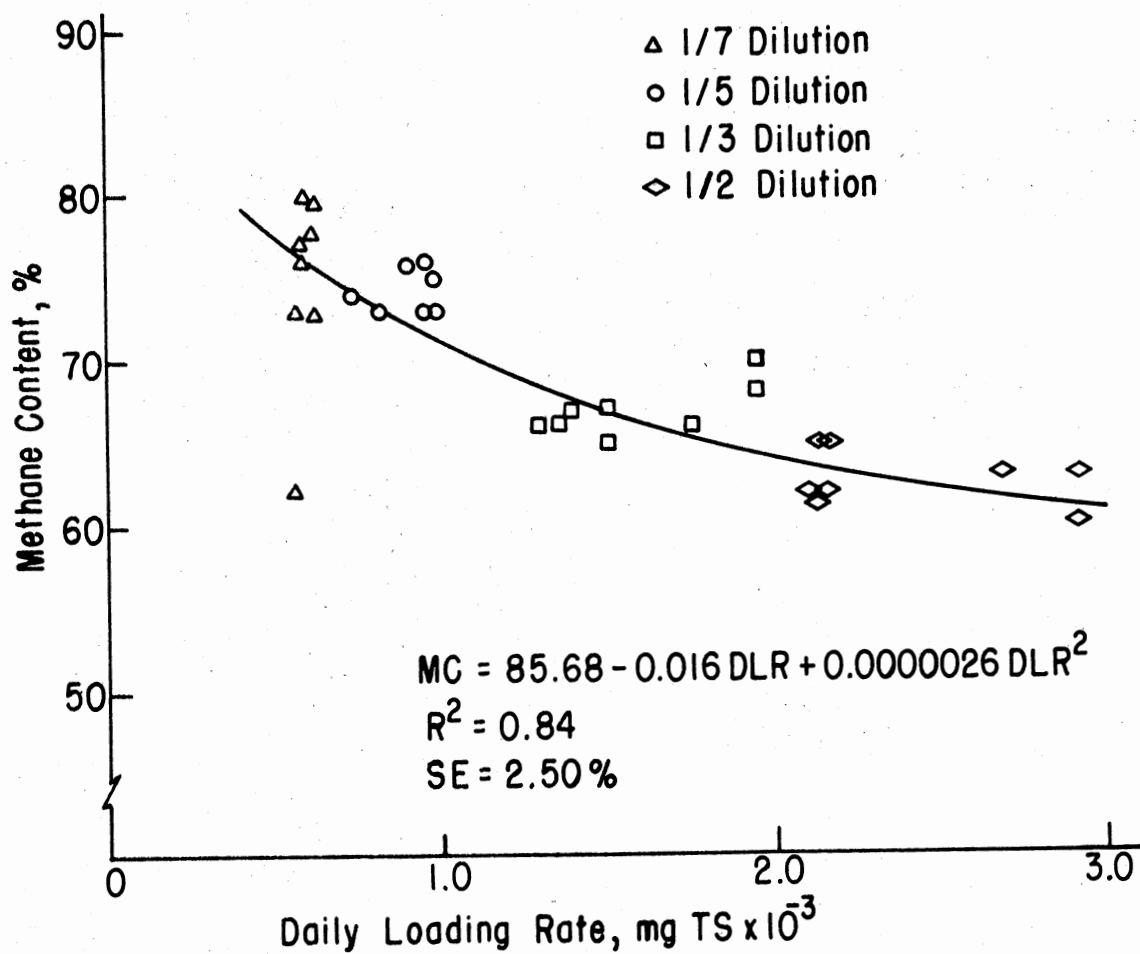


Figure 40. Methane Content Versus Daily Loading Rate

standard error of 2.50%. Analysis of variance of regression is shown in Appendix H.

Discussion of the Anaerobic

Digestion Study

Figure 41 is a plot of average daily gas production (ADGP) versus average daily loading rate (ADLR) for the digesters operated during the study. The ADGP for each digester was adjusted to a common base of 1000 mg TS feed/l of digester for the purpose of comparing the digesters. Appendix I represents a sample calculation of adjusting ADGP values.

Analysis of variance (presented in Appendix J) indicated no significant difference ($\alpha = 0.10$) in ADGP values due to the different dilutions or loading rates. The analysis included only the straight, 1/3, and 1/7 dilutions. The 1/5 and 1/2 dilutions were not included in the analysis due to the lack of adequate replications. Although the 1/2 and 1/3 dilutions appeared to give higher gas production, there were not enough trials to determine a significant relationship. Previous discussion, however, indicated digester fed the straight manure suspension had performance characteristics indicative of eventual failure.

Table XXIX summarizes data on the performance of anaerobic digesters fed swine manure under similar operating conditions. The summary indicates the loading rates of the current study were conservative when compared to loading rates attained by researchers feeding digesters swine feces without the urine included. Gramms et al. (1971) also reported a significantly higher gas production rate of 0.35 l/1000 mg TS/l of digester at a similar loading rate. The difference in loading rate and gas production was attributed primarily to the inhibition of the

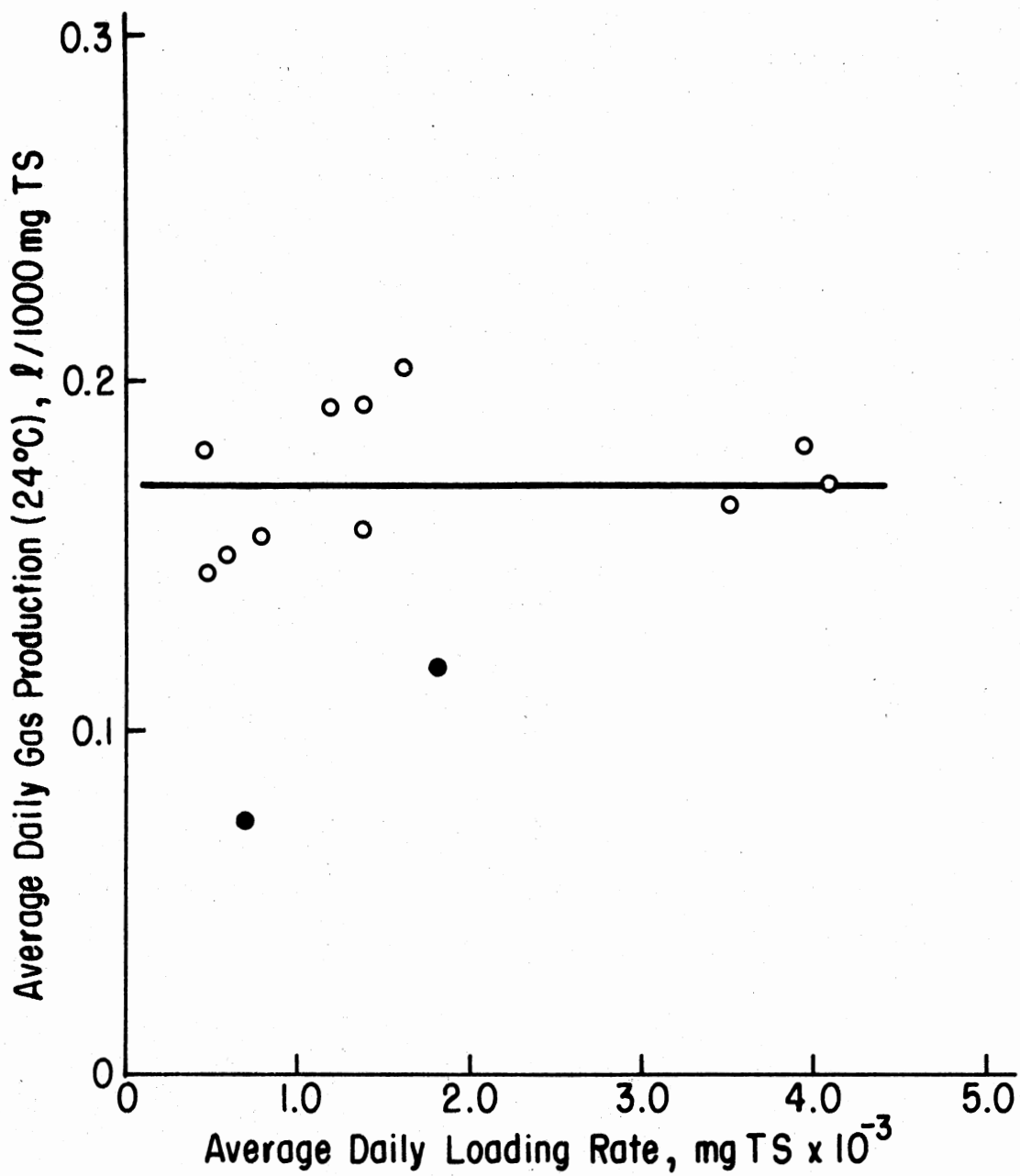


Figure 41. Average Daily Gas Production (24°C) Versus Average Daily Loading Rate

TABLE XXIX

COMPARATIVE SUMMARY OF SELECTED RESEARCH DATA ON THE PERFORMANCE
OF ANAEROBIC DIGESTERS FED SWINE MANURE

Researcher	Manure Feed		Loading Rate (mg TS/l)	Detention Time (Days)	Temp. (°C)	Gas Production (l/1000 mg TS/l)	Digester Tendency	
	Feces	Urine					Success	Failure
Jeffery et al. (1965)	X		3100 ¹	20	35	--	X	
	X		3500 ¹	20	35	--	X	
	X		3900 ¹	20	35	--		X
Cross and Duran (1970)	X		1000 ¹	15	32	--	X	
	X		2000 ¹	15	32	--	X	
	X		4000 ¹	15	32	--		X
Gramms et al. (1971)	X		2300	15	32.5	0.34	X	
	X		4600	15	32.5	0.35	X	
Taiganides (1963)		X	1500 ¹	22	34	0.46	X	
		X	2400 ¹	25	34	0.44		X
Schmid and Lipper (1969)		X	3800 ¹	20	35	--		X
Hobson and Shaw (1973)		X	1100	19	35	0.26	X	
		X	1900	14	35	0.23	X	
		X	2600	14	35	0.28	X	
		X	3300	14	35	0.27	X	
		X	3700	14	35	0.25	X	
Frey (1979)		X	500 ²	20	35	0.15	X	
		X	800 ³	20	35	0.16	X	
		X	1300 ²	20	35	0.23	X	
		X	1600 ³	20	35	0.20	X	
		X	3900 ²	20	35	0.17		X

¹Calculated assuming VS equaled 80% TS (Smith and Miner, 1975).

²Average based on the performance of three digesters.

³Based on the performance of a single digester.

digestion process due to the higher NH_4^+ - N concentrations resulting with the inclusion of urine in the manure.

The loading rates, however, were comparable to the research reported by Taiganides (1963), Schmid and Lipper (1969), and Hobson and Shaw (1973) for digesters fed swine feces and urine combined. Previous discussion also indicated digesters fed the straight manure suspension had operating characteristics indicative of eventual digester failure. The straight manure suspension corresponded to an average daily loading rate of 3900 mg TS/l of digester. The daily gas production rates were 33% to 82% below the values reported by other researchers for digesters operated at similar conditions. The noted reduction in gas production was attributed to fluctuations in the daily loading rate corresponding to variations in characteristics of the daily manure flow from the production buildings.

The gas composition analysis, however, indicated the gas generated by the digesters operated at the lower loading rates, 500 to 1300 mg TS/l of digester/day, contained a significantly higher percentage of methane. Assuming the limited gas composition data were representative of digesters operated at similar loading rates, the inclusion of the methane content data would tend to reduce the decline in gas production noted at the lower loading rates in Figure 41. The digester volume required to treat the manure production of the farm at the lower dilutions would be 1.5 to 3.5 times greater than the volume required to treat the manure at the 1/2 dilution. The higher initial cost of the larger digester and the volume of dilution water required would tend to offset any benefits associated with the increased methane content of gas generated at the lower loading rates.

CHAPTER VI

SUMMARY AND CONCLUSIONS

Summary

A commercial farrow to finish swine production facility was studied to gain a better understanding of factors affecting the volume, characteristics, and treatability of the manure produced. Manure samples from each production building were used to create manure suspensions representing the daily manure flow of the farm. Dilutions (straight, 1/2, 1/3, 1/5, and 1/7) of the manure suspension were fed to a series of digesters to determine the dilution or loading rate required to maximize methane production and minimize ammonia toxicity problems. Digester detention time and temperature were held constant at 20 days and $35 \pm 2^\circ\text{C}$, respectively. There was no significant difference in gas production due to different dilutions; however, a 1/2 dilution appeared to provide the maximum daily gas production. The gas produced at the 1/2 dilution contained between 60% and 64% methane. The daily gas production rates were 33% to 82% below the values reported by other researchers for digesters operated at similar conditions.

Conclusions

A farm with a pit manure collection system was selected to determine the variation in manure characteristics. Several factors were noted to

cause variations in the daily manure production. The factors noted included: (1) season of the year, (2) wash water, (3) water leaks, and (4) variations in herd size and number. However, quantitatively measuring the effects individually was not possible.

The lagoon problems meant the pits could not be totally drained according to the design schedule and the level of the pits in many instances exceeded the standpipes. Therefore, some fluctuations noted in the manure characterization data did not always reflect real fluctuations in manure production. Also, a value for the average daily flow from each production building was not obtained because of the problem with the lagoon. The data indicated the manure flows from the farrower and nurseries tended to dilute the daily manure flow of the farm.

There were no significant differences in gas production due to different dilutions. A 1/2 dilution, however, appeared to provide the maximum daily gas production. The daily gas production rates were 33% to 82% below the values reported by other researchers for digesters operated at similar conditions.

Methane content of the gas generated increased with a decrease in the average loading rate. The relationship is described by the following equation:

$$MC = 85.68 - 0.016 \text{ DLR} + 0.0000026 \text{ DLR}^2 \quad (2)$$

where,

MC = methane content, %

DLR = daily loading rate, mg TS/l of digester.

The higher initial cost of the digester and the volume of dilution water

required would tend to offset any benefits associated with the increased methane content of gas generated at the lower loading rates.

The operation of the production facility studied was oriented to the production of meat and not the treatment of manure. The observed fluctuations and the resultant depressed gas production indicates anaerobic digestion would not be a viable alternative unless the herdsman is willing to make a commitment to the daily operation of a digester.

Recommendations for Future Research

The characterization of the commercial farm was limited primarily to observations made on weekly or bi-monthly trips to the farm. Also, problems with the lagoon system affected the manure characterization study and tended to buffer variations in the manure characteristics. Information in more detail is needed on the causes and types of variations occurring in the daily manure production of a farrow to finish operation to: (1) aid the engineer who will design the anaerobic digestion system, and (2) guide the operator who will maintain the digestion system once operating.

The research presented was conducted with small bench scale digesters. Additional research data are needed on the response of larger anaerobic digesters (1000 l) operated under similar conditions prior to the installation of full scale on-farm digesters.

Anaerobic digestion is but a component in a manure treatment system. The effluent from the digester is still environmentally offensive and requires careful disposal. Land disposal is a common disposal technique. However, alternatives need to be explored for the extraction of additional energy prior to disposal of the digester effluent. One

alternative would be to separate the solids from the raw manure and combust under controlled conditions to generate producer gas and ultimately methanol. Alternatives need to be explored for the extraction of additional energy by combining the anaerobic digester with other energy conversion devices.

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APPENDIXES

APPENDIX A

PARTIAL LISTING OF EQUIPMENT USED
IN THE ANALYSIS OF MANURE AND
DIGESTER CHARACTERISTICS

1. The following equipment was used in the analyses for determining manure and digester characteristics:

Centrifuge-----Precision Scientific Co., Model 11-AD-10 variable speed centrifuge, maximum rps 83.

600°C Furnace-----Thermolyne, type 1500 furnace, 0 to 1200°C.

103°C Oven-----Precision Scientific Co., Type A oven, 0 to 260°C.

Spectrophotometer--Coleman Co., Model 6C Coleman Jr. Spectrophotometer with Coleman solid state regulated DC power supply.

pH Meter-----Sargent Welch, Model NX digital pH meter, relative accuracy ± 0.01 pH.

Vacuum Pump-----Welch Scientific, Model 1376 Duo-Seal vacuum pump, ultimate pressure 0.1 micron.

Gas Chromatograph--LKB Instruments, LKB-9000 Gas Chromatograph-Mass Spectrometer.

2. Detailed description of LKB-9000 Gas Chromatograph-Mass Spectrometer (Waller, 1968).

The LKB-9000 gas chromatograph-mass spectrometer was designed in 1963-64 by Dr. Waller, Oklahoma State University Biochemistry Department, Stillwater, Oklahoma, and Dr. Ryhage, Director of Mass Spectrometry Laboratory at the Karolinska Institutet, Stockholm, Sweden. A block diagram of the instrument is shown in Figure 42. The instrument was built by Dr. Ryhage for research use at Oklahoma State University. The instrument is capable of detecting 0.1 to 10 μg of compound in gas chromatography column effluent, of providing useful mass spectrum ($m/e = 12$ to 600) on a few μg of sample within 2 to 10 s, of making

Block Diagram Of LKB 9000 Gas Chromatograph – Mass Spectrometer

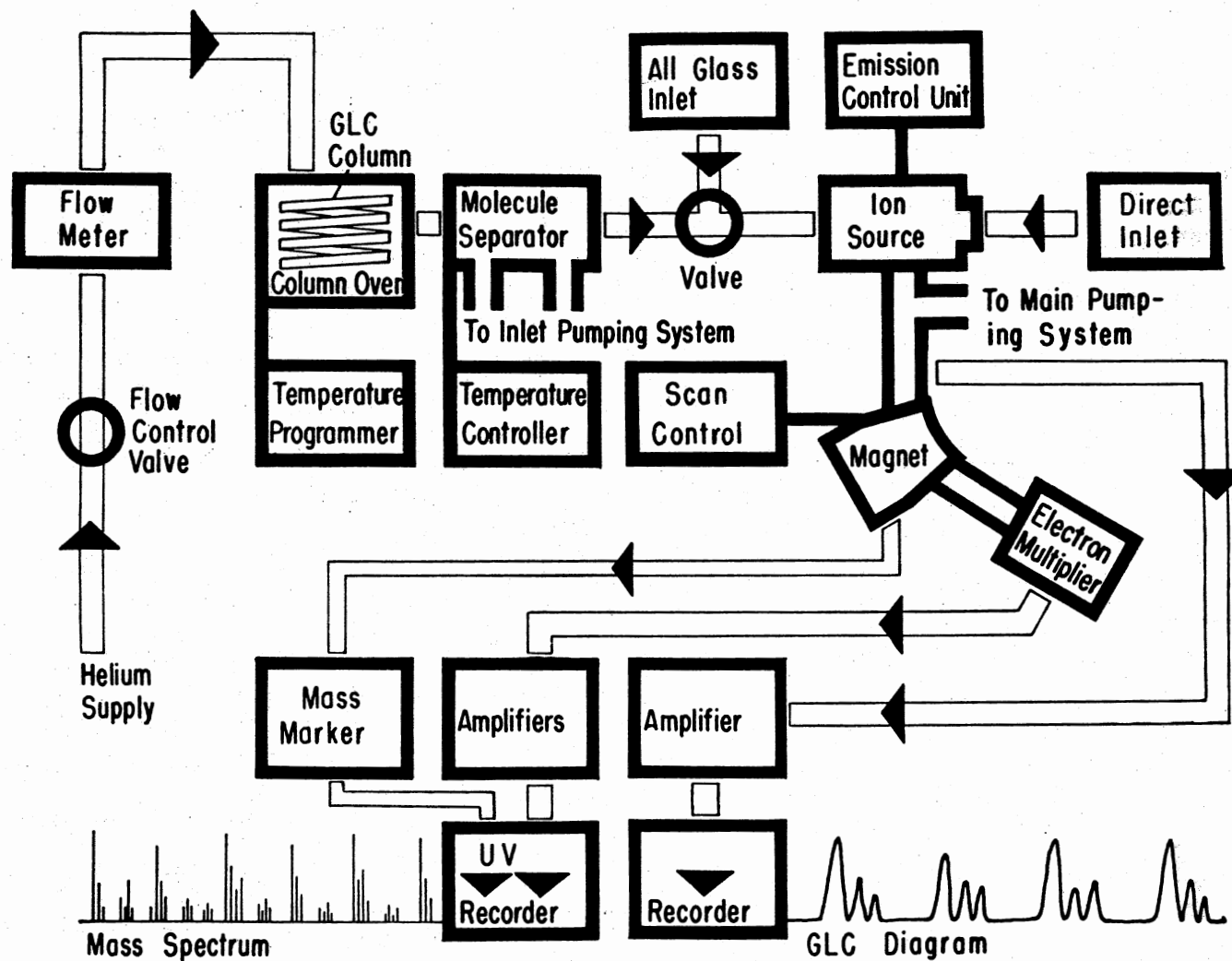


Figure 42. Block Diagram of LKB-9000(P) Gas Chromatograph-Mass Spectrometer

accurate isotope ratio measurement on compounds with m/e ratios of up to 300, and of obtaining useful spectra on submicrogram quantities of sample when the direct probe is used. Additions to the original instrument include a mass marker and double collectors for determining quantities of stable isotopes present in compounds with m/e ratios up to 300. The instrument's single-focus mass spectrometer features three different sample inlet systems: (1) a gas chromatography system (system used for gas analysis), (2) a heated glass inlet system, and (3) a direct probe.

The gas chromatography inlet system utilizes gas-liquid chromatography (GLC) to separate sample components and the mass spectrometer as the specific detector. The GLC effluent, after passing through a series of separators to remove the helium (He) carrier gas, is fed directly to an ionization chamber. Electron impact ionizes sample entering the chamber. The ions formed are accelerated and the beam collimated to its final shape using potential differences. The resulting ion beam passes through a plate (electrode) pierced centrally by a rectangular hole. The electrode collects about 10% of the positively charged ions producing an electric current. The current is amplified and finally recorded as a chromatogram using a strip chart recorder.

The remaining ions, 90%, pass through the electrode to the analyzer tube. Prior to reaching the analyzer tube, the ions go through a fixed focus and an adjustable focus control. The ions then transverse a 60° magnetic sector of the analyzer tube. The magnetic sector deflects ion groups according to m/e ratios. An ion group having equal m/e ratio is focused to impinge on the electron multiplier's collector plate. The signal produced is amplified and its intensity recorded with a high speed recording oscillograph on light sensitive photographic paper.

Each ion of a particular m/e ratio is recorded simultaneously by three galvanometers of different gains (1, 10, 100). A recording of the m/e ratios of all fragment ions of a particular sample is obtained by sweeping a range of magnetic field strengths.

APPENDIX B

SUPERNATANT AMMONIA NITROGEN

DETERMINATION PROCEDURE

A colorimetric procedure adapted by Ecker and Lockhart (1961) from Niss (1957) was used to determine supernatant NH_4^+ - N concentrations. The procedure employed two reagents. Reagent A contained: sodium citrate, 4.7 g; citric acid, 1.7 g; phenol, 9.6 g; distilled water to 480 ml. Reagent B contained: boric acid, 6.0 g; sodium hydroxide, 8.0 g; chlorox bleach, 30.0 ml; distilled water to 200 ml. Supernatant samples were diluted to give between 2 and 20 mg of NH_4^+ - N per l. To 1.0 ml samples of diluted supernatant samples were added 5.0 ml of reagent A and 2.0 ml of reagent B. Samples were mixed, capped with aluminum foil, heated in a boiling water bath for five minutes, and cooled rapidly. Optical densities of samples were determined in a spectrophotometer at 615 nm against a distilled water-reagent blank.

Optical density readings were compared to a standard curve plotted using known concentrations (2, 5, 10, 15, and 20 mg/l) of ammonium chloride. A typical standard curve is plotted in Figure 43. A new standard curve was prepared for each batch of reagents. The NH_4^+ - N concentrations read from the curve was multiplied by the dilution factor to obtain the actual supernatant NH_4^+ - N concentrations.

Sample calculation:

Given: A 1.0 ml sample of diluted (1/100) supernatant sample having an optical density reading of 0.250.

Required: NH_4^+ - N concentration.

Solution: NH_4^+ - N concentration = NH_4^+ - N concentration of diluted sample x dilution factor

NH_4^+ - N concentration = 11.3 mg/l from standard curve of diluted sample

dilution factor = 100

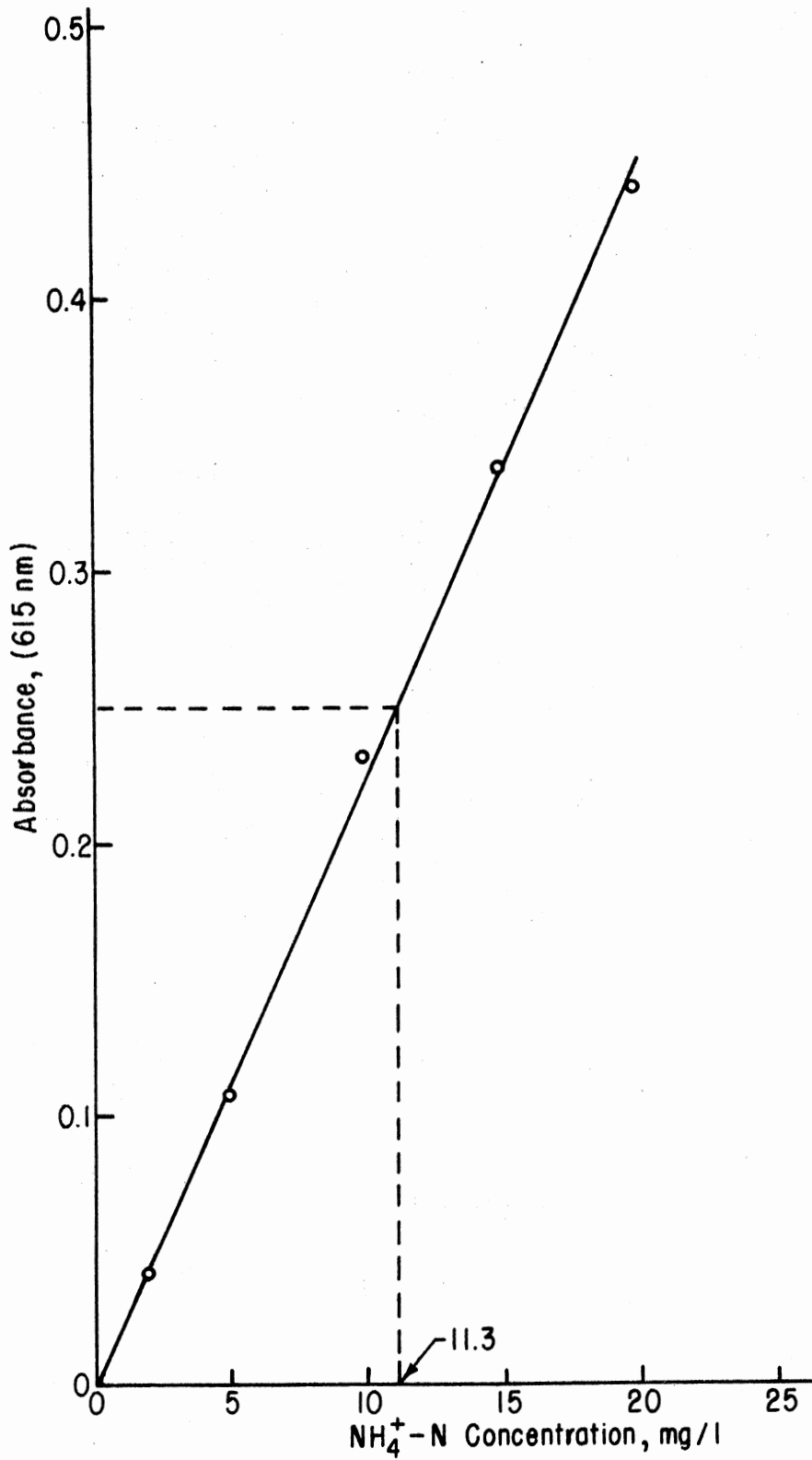


Figure 43. Standard Curve--Absorbance (615 nm)
Versus $\text{NH}_4^+ - \text{N}$ Concentration

substituting

$$\text{NH}_4^+ - \text{N concentration} = 11.3 \times 100 = 1130 \text{ mg/l.}$$

APPENDIX C

EXPECTED DAILY MANURE PRODUCTION
CALCULATIONS FOR EACH OF THE
FARM'S CONFINEMENT
BUILDINGS

Table XXX presents calculations for the daily manure production from each of the farm's confinement buildings. The calculations were based on livestock information obtained from herdsman Edward on October 23, 1975, and the mean manure production values (liquid and solids) reported by Muehling (1969). The mean manure production values reported by Muehling (1969) were specified according to livestock weight, age and classification (sow, boar, etc.).

TABLE XXX

EXPECTED DAILY MANURE PRODUCTION (SOLIDS AND LIQUID) CALCULATIONS FOR
EACH OF THE FARM'S CONFINEMENT BUILDINGS

Building	Livestock Classification	Average No. of Animals	Average Age (wks)	Average Weight		Daily Manure Product		% of Total Production (%)
				(kg/animal)	(kg)	(ℓ/animal)	(ℓ)	
Sow and Boar Barn	Sows, Boars, Gilts	250	104	181.8	45450	15.4	3785	21.5
Farrowing	Sows	48		181.8	8726	15.4	727	4.1
	+ Litters	360		1.8	648			
Nursery I and II	Sows	48		181.8	8726	15.4	727	10.1
	+ Litters	360		5.0	1800			
	Weaned Pigs	550	8	15.9	8745			
Grower	Pigs	1450	14	36.4	52780	3.8	5510	31.3
Finisher	Pigs	700	26	90.9	63630	8.3	5810	33.0
Weaning Pens	Sows	16		181.8	2909			
Dirt Breeding Pens	Gilts	30		159.1	4773			
Special Nursery	Pigs	48		4.5	216			
TOTALS		3860			198403		17604	100.0

APPENDIX D

MANURE CHARACTERIZATION DATA

SOW BARN

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.45	9091	27620	106190	55675	6153	3620	58.50	924	718
6/15/76	7.50							57.00		
6/22/76	7.50	3594	93000	103860	70440	5480	3087	56.30	2223	1732
7/ 6/76	7.53	4506	55300	67745	42550	5573	2960	58.50	1352	1051
7/13/76	7.42	4351	59500	60060	38200	6047	3040	45.00	1736	1350
7/20/76	7.32	5918	44500	54820	38200	5753	3007	52.50	1807	1467
7/27/76	7.44	7226	55500	69974	45900	5853	3033	52.00	1631	1268
8/ 5/76	7.32	4655	55500	71811	45655	4411	2100	55.00	1436	1116
8/13/76	7.39	7794	11111	11459	74180	3413	1940	54.00	1441	1120
8/24/76	7.38	3861	77000	11459	53680	3727	2147	57.00	1395	1085
9/ 8/76	7.17	6187	79000	10772	65945	3173	1967	55.50	1352	1051
9/17/76	7.51	2840	37000	53267	32815	2980	1493	51.00	1132	880
9/24/76	7.53			16500	55550			54.80	1192	927
9/30/76	7.53	5952	75397	92233	55850	3653	2147	57.50	1239	963
10/22/76	7.20	6190	12372	12216	55000	3427	2207	57.00	1202	934
11/ 1/76	7.22	4791	10114	12797	50070	3493	2200	60.00	1411	1097

FAPROWER

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.73	1230	23256	21185	16010	2430	1153	57.50	405	315
6/15/76	7.49			9130	5070	1833	647	60.50		
6/22/76	7.10	898	6202					59.90	424	329
7/ 6/76	7.26	1146	20543	21345	15415	2027	767	60.00	371	288
7/13/76	7.32	984	24900	24640	18460	2060	833	56.50	446	346
7/20/76	7.25	957	33300	29083	22795	1720	647	59.00	460	357
7/27/76	7.31	1006	39965	33435	25530	1353	553	49.50	259	201
8/ 5/76	7.33	749	29615	22210	16780	1633	647	55.50	409	318
8/13/76	7.21	934	28654	27333	20020	5187	2320	60.00	494	384
8/24/76	7.42	746	13391	16680	12400	1877	767	60.00	409	318
9/ 8/76	7.43	979	33312	27415	20210			39.00	567	441
9/17/76	7.55	1329	77305	33815	24345	1913	773	33.50	633	496
9/24/76	7.44	1230	28378	33790	23295	1987	740	37.00	610	474
9/30/76	7.26	1521	29762	31867	22694	1867	787	46.00	402	312
10/22/76	7.00							17.00		
11/ 1/76	7.31	1559	23180	26397	15813	2507	980	36.00	901	700

NURSERY I

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.32	3557	26163	31310	21280	4687	1980	45.50	851	661
6/15/76	7.14							55.50		
6/22/76	7.00	1567	11074	17595	8320	3187	1367	55.00	716	556
7/ 6/76	7.27	2009	3674	36015	25920	3247	1427	59.00	712	553
7/13/76	7.33	5707	2177	21118	14365	3127	1247	43.50	1920	1493
7/20/76	7.34	1914	1660	14336	9400	3393	1313	49.50	943	733
7/27/76	7.35	1816	1916	18270	12800	3427	1547	55.00	1211	941
8/ 5/76	7.34	1022	1177	11533	10820	2208	867	52.00	610	474
8/13/76	7.35	1206	1111	12066	7765	2500	907	52.00	800	622
8/24/76	7.37	1139	1738	17336	11460	2500	1127	53.00	979	761
9/ 8/76	7.34	944	1935	19066	12920	1955	727	54.50	760	591
9/17/76	7.45	1080	1955	16030	10785	2147	860	54.00	729	567
9/24/76	7.45	932	1544	15620	11185	2133	647	53.50	743	577
9/30/76	7.34	1092	1344	15920	10615	2233	793	54.50	605	470
10/22/76	7.21	794	2337	23377	14395	1900	680		797	619
11/ 1/76	7.12	932	1054	21450	13885	1820	693	59.00	734	570

NURSERY II

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.54	2964	33721	42250	28510	4100	1993	60.00	979	761
6/15/76	7.42							60.00		
6/22/76	7.10	3242	4224	50515	73955	3140	1547	60.00	1259	979
7/ 6/76	7.33	3043	3438	37595	24290	3800	1706	59.50	972	756
7/13/76	7.36	5551	4083	41115	28340	3611	1507	59.00	1361	1058
7/20/76	7.23	3164	4633	46338	31790	3347	1400	59.00	1426	1109
7/27/76	7.28	3301	4366	43775	30440	3467	1620	59.50	1460	1135
8/ 5/76	7.35	2490	4033	43105	30170	3393	1633	60.00	1222	950
8/13/76	7.30	2840	4260	51965	34270	2811	1293	60.00	1299	1010
8/24/76	7.32	2124	5625	50370	33855	2787	1373	59.00	1073	838
9/ 8/76	7.35	1654	3398	37975	26040	2867	1093	51.50	1366	1062
9/17/76	7.23	1693	3125	29065	19890	2333	1053	47.50	801	623
9/24/76	7.52	1091	1533	19070	12130	2327	747	59.50	1076	836
9/30/76	7.45	1448	2261	18890	12010	2427	920	59.50	711	553
10/22/76	7.24	1647	2266	26875	17975	2720	1080	60.50	1337	1039
11/ 1/76	7.23	1559	2950	31005	20575	2787	1133	53.50	1224	952

GRO-ER

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.20	9091	43411	57120	31725	7553	3887	53.00	1544	1200
6/15/76	7.41							54.50		
6/22/76	7.25	8516	52711	56790	39190	2600	4297	55.00	2651	2061
7/ 6/76	7.36	6640	44112	55025	33990	7167	3540	52.00	1608	1250
7/13/76	7.23	2205	62227	55107	35745	6277	3080	52.50	1096	844
7/20/76	7.32	4460	47104	55003	37080	5407	2560	54.00	1780	1394
7/27/76	7.24	0000	46999	55162	37880	5348	2290	54.50	2092	1697
8/ 5/76	7.25	0000	19234	22624	18125	5587	2687	22.00	1499	1165
8/13/76	7.25	1191	15500	24800	16730	1700	640	47.00	1464	1138
8/24/76	7.34	4093	34330	41300	26350	6620	3113	55.00	1984	1543
9/ 8/76	7.56	0000	99112	55093	30244	5911	1807	55.00	1420	1104
9/17/76	7.51	0000	39999	45999	31900	5022	2600	55.00	1550	1206
9/24/76	7.44	0000	34466	46555	31033	6477	4600	55.00	2590	2014
9/30/76	7.64	6644	33660	44488	29877	6677	3473	55.00	2467	1934
10/22/76	7.35	4444	22222	24444	15777	4788	2266	55.00	1706	1326
11/ 1/76	7.15	5217	40233	43945	31750	5667	2813	57.50	2162	1681

FINISHER

DATE	PH	ML COD	MLSS COD	TS	TVS	DS	VDS	DEPTH	AMMON	ANIT
6/ 1/76	7.20	37652	88274	69340	49490	1310	4990	56.00	4266	3318
6/15/76	6.89	29492	108037	77400	50730	7590	2930	72.50	3716	2890
6/22/76	6.85	0000	0000	75990	54679	9288	4675	78.50	4443	3455
7/ 6/76	6.90	27311	78013	12547	74835	8322	4330	52.50	3265	2539
7/13/76	7.04	22834	82539	10003	59190	7810	4200	46.50	2752	2140
7/20/76	7.03	29343	100014	10003	63525	8355	4014	51.00	2290	1781
7/27/76	7.00	25912	113737	12991	98192	6275	3363	49.50	3072	2399
8/ 5/76	7.04	20703	99698	92300	64935	8170	3990	50.00	5072	1969
8/13/76	7.30	11022	59527	71568	45525	4460	1750	59.00	2382	1852
8/24/76	7.37	9954	94779	10370	62410	4944	1755	54.00	2038	1595
9/ 8/76	7.43	8870	53025	77137	46452	5100	1685	54.00	1813	1410
9/17/76	7.39	13305	100390	12330	74180	5355	1970	50.50	2783	2164
9/24/76	7.40	13383	100390	118880	76340	5440	1660	54.00	3396	2641
9/30/76	7.65	12460	101369	11859	75795	6010	2980	54.00	3190	2481
10/22/76	7.54			12552	74510			61.00		
11/ 1/76	7.61	19463	94253	128650	78060			65.00	3020	2348

APPENDIX E

DIGESTER FEED CHARACTERIZATION DATA

FEED ONE-SEVENTH FIRST REP

DATE	P-	UNCSF	CLCML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT
7.15			49							124	44
7.15			49							124	44
7.10			49							124	44
7.10			49							124	44
7.11			49							124	44
7.11			49							124	44
7.14			99							124	44
7.57		1790	99							124	44
7.59		479	99							124	44
7.69		479	99							124	44
7.63											
7.75		20772	11								
7.68		19772	11								
7.53		19776	11								
7.72		20556	11								
7.67		20556	11								
7.76		20990	11								
7.62		20990	11								
7.73		20338	10								
7.64		20338	10								
7.76		20372	10								
7.63		10117	14								
7.60		10117	14								
7.76		10442	12								
7.64		10111	13								
7.74		10111	13								
7.67		10111	13								
7.75		10111	13								
7.76											
7.58											
7.68											
7.55											
7.71											
7.88											
7.60											
7.55											
7.86											
7.92											
7.71											
7.40											

FEED ONE-SEVENTH FIRST REP

OBS	DATE	PH	CO DSP	CO DML	TS	TVS	SS	VSS	OS	VDS	AMMON	ANIT
56	56		986	10895	20205	13685	19175	13325	1030	360	381	296
57	57		986	10895	20205	13685	19175	13325	1030	360	381	296
58	58	7.56	1312	10733	14440	10344	6320	9800	940	540	391	304
59	59		1312	10733	14440	10344	6320	9800	940	540	391	304
60	60	7.52	919	11823	12630	9311	4590	8490	290	800	406	315
61	61		919	11823	12630	9311	4590	8490	290	800	406	315
62	62	7.65	1012	9665	12660	8445	9800	7790	460	670	406	288
63	63		1012	9665	12660	8445	9800	7790	460	670	406	288
64	64	7.60	1455	11306	10560	7945	9850	6660	810	800	660	288
65	65	7.47	1455	11306	10560	7945	9850	6660	810	800	660	288
66	66	7.61	1354	14400	4440	11111	2995	1550	460	600	444	444
67	67		1354	14400	4440	11111	2995	1550	460	600	444	444
68	68	7.62	1160	1355	3330	11111	2995	1550	460	600	444	444
69	69		1160	1355	3330	11111	2995	1550	460	600	444	444
70	70	7.56	1600	1033	8880	11111	6760	1000	800	700	444	444
71	71		1600	1033	8880	11111	6760	1000	800	700	444	444
72	72	7.61	2222	1033	1173	11111	8890	800	700	700	444	444
73	73		2222	1033	1173	11111	8890	800	700	700	444	444
74	74	7.57	184	1447	1533	11111	4440	1110	800	800	444	444
75	75	7.52	184	1447	1533	11111	4440	1110	800	800	444	444
76	76	7.67	986	9764	11027	11111	7740	8760	640	777	444	444
77	77		986	9764	11027	11111	7740	8760	640	777	444	444
78	78	7.61	1738	9764	11027	11111	7740	8760	640	777	444	444
79	79	7.80	1738	9764	11027	11111	7740	8760	640	777	444	444
80	80	7.67	1811	9764	11027	11111	7740	8760	640	777	444	444
81	81		1811	9764	11027	11111	7740	8760	640	777	444	444
82	82	7.56	2730	1811	11895	8965	9740	8215	640	777	444	444
83	83		2730	1811	11895	8965	9740	8215	640	777	444	444

FEEB ONE-SEVENTH SECOND REP

UBS	DATE	PH	COOSP	COOHL	TS	TVS	SS	VSS	DS	VDS	AMON	ANIT
56	56		9	10895	200	13	19	133	10	360	1	1
57	57		8	10895	200	13	19	133	10	360	1	1
58	58	7.56	8	10895	200	13	19	133	10	360	1	1
59	59	7.52	8	10895	200	13	19	133	10	360	1	1
60	60		8	10895	200	13	19	133	10	360	1	1
61	61	7.65	8	10895	200	13	19	133	10	360	1	1
62	62		8	10895	200	13	19	133	10	360	1	1
63	63	7.60	8	10895	200	13	19	133	10	360	1	1
64	64	7.47	8	10895	200	13	19	133	10	360	1	1
65	65	7.61	8	10895	200	13	19	133	10	360	1	1
66	66		8	10895	200	13	19	133	10	360	1	1
67	67	7.62	8	10895	200	13	19	133	10	360	1	1
68	68		8	10895	200	13	19	133	10	360	1	1
69	69	7.56	8	10895	200	13	19	133	10	360	1	1
70	70		8	10895	200	13	19	133	10	360	1	1
71	71	7.61	8	10895	200	13	19	133	10	360	1	1
72	72		8	10895	200	13	19	133	10	360	1	1
73	73	7.57	8	10895	200	13	19	133	10	360	1	1
74	74	7.52	8	10895	200	13	19	133	10	360	1	1
75	75	7.67	8	10895	200	13	19	133	10	360	1	1
76	76		8	10895	200	13	19	133	10	360	1	1
77	77	7.61	8	10895	200	13	19	133	10	360	1	1
78	78	7.60	8	10895	200	13	19	133	10	360	1	1
79	79	7.67	8	10895	200	13	19	133	10	360	1	1
80	80		8	10895	200	13	19	133	10	360	1	1
81	81	7.56	8	10895	200	13	19	133	10	360	1	1
82	82		8	10895	200	13	19	133	10	360	1	1
83	83		8	10895	200	13	19	133	10	360	1	1

FEED ONE-SEVENTH THIRD REP

CRS	DATE	PL	CRS	CDL	TS	TVS	SS	VSS	DS	VDS	AKON	AVIT
11000	7.55	7.37	11000	7449	11000	9040	11000	8844	11000	6000	11000	11000
11001	7.55	7.39	11001	7449	11001	9040	11001	8844	11001	6000	11001	11001
11002	7.55	7.37	11002	7449	11002	9040	11002	8844	11002	6000	11002	11002
11003	7.55	7.37	11003	7449	11003	9040	11003	8844	11003	6000	11003	11003
11004	7.55	7.37	11004	7449	11004	9040	11004	8844	11004	6000	11004	11004
11005	7.55	7.37	11005	7449	11005	9040	11005	8844	11005	6000	11005	11005
11006	7.55	7.37	11006	7449	11006	9040	11006	8844	11006	6000	11006	11006
11007	7.55	7.37	11007	7449	11007	9040	11007	8844	11007	6000	11007	11007
11008	7.55	7.37	11008	7449	11008	9040	11008	8844	11008	6000	11008	11008
11009	7.55	7.37	11009	7449	11009	9040	11009	8844	11009	6000	11009	11009
11010	7.55	7.37	11010	7449	11010	9040	11010	8844	11010	6000	11010	11010
11011	7.55	7.37	11011	7449	11011	9040	11011	8844	11011	6000	11011	11011
11012	7.55	7.37	11012	7449	11012	9040	11012	8844	11012	6000	11012	11012
11013	7.55	7.37	11013	7449	11013	9040	11013	8844	11013	6000	11013	11013
11014	7.55	7.37	11014	7449	11014	9040	11014	8844	11014	6000	11014	11014
11015	7.55	7.37	11015	7449	11015	9040	11015	8844	11015	6000	11015	11015
11016	7.55	7.37	11016	7449	11016	9040	11016	8844	11016	6000	11016	11016
11017	7.55	7.37	11017	7449	11017	9040	11017	8844	11017	6000	11017	11017
11018	7.55	7.37	11018	7449	11018	9040	11018	8844	11018	6000	11018	11018
11019	7.55	7.37	11019	7449	11019	9040	11019	8844	11019	6000	11019	11019
11020	7.55	7.37	11020	7449	11020	9040	11020	8844	11020	6000	11020	11020

FEED DE-SEVENTH THIRD REP

CBS	DATE	PH	COBSP	COBML	TS	TVS	SS	VSS	DS	VDS	AREA	AZIT
111	111		555	111	111	888	111	888	000	000		000
112	111		555	111	111	888	111	888	000	000		000
113	111		555	111	111	888	111	888	000	000		000
114	111	7.46	555	111	111	888	111	888	000	000		000
115	111		555	111	111	888	111	888	000	000		000
116	111		555	111	111	888	111	888	000	000		000
117	111	7.58	555	111	111	888	111	888	000	000		000
118	111	7.58	555	111	111	888	111	888	000	000		000
119	111		555	111	111	888	111	888	000	000		000
120	111	7.70	555	111	111	888	111	888	000	000		000
121	111	7.64	555	111	111	888	111	888	000	000		000
122	111	7.73	555	111	111	888	111	888	000	000		000
123	111		555	111	111	888	111	888	000	000		000
124	111		555	111	111	888	111	888	000	000		000
125	111		555	111	111	888	111	888	000	000		000
126	111		555	111	111	888	111	888	000	000		000
127	111		555	111	111	888	111	888	000	000		000
128	111		555	111	111	888	111	888	000	000		000
129	111		555	111	111	888	111	888	000	000		000
130	111		555	111	111	888	111	888	000	000		000
131	111		555	111	111	888	111	888	000	000		000
132	111		555	111	111	888	111	888	000	000		000
133	111		555	111	111	888	111	888	000	000		000
134	111		555	111	111	888	111	888	000	000		000
135	111		555	111	111	888	111	888	000	000		000
136	111		555	111	111	888	111	888	000	000		000
137	111		555	111	111	888	111	888	000	000		000
138	111		555	111	111	888	111	888	000	000		000
139	111		555	111	111	888	111	888	000	000		000
140	111		555	111	111	888	111	888	000	000		000
141	111		555	111	111	888	111	888	000	000		000
142	111		555	111	111	888	111	888	000	000		000
143	111		555	111	111	888	111	888	000	000		000
144	111		555	111	111	888	111	888	000	000		000
145	111		555	111	111	888	111	888	000	000		000
146	111		555	111	111	888	111	888	000	000		000
147	111		555	111	111	888	111	888	000	000		000
148	111		555	111	111	888	111	888	000	000		000
149	111		555	111	111	888	111	888	000	000		000
150	111		555	111	111	888	111	888	000	000		000
151	111	7.66	555	111	111	888	111	888	000	000		000
152	111		555	111	111	888	111	888	000	000		000
153	111		555	111	111	888	111	888	000	000		000
154	111		555	111	111	888	111	888	000	000		000
155	111	7.41	555	111	111	888	111	888	000	000		000
156	111	7.50	555	111	111	888	111	888	000	000		000
157	111		555	111	111	888	111	888	000	000		000
158	111	7.68	555	111	111	888	111	888	000	000		000
159	111		555	111	111	888	111	888	000	000		000

FEED ONE-FIFTH FIRST REP

UBS	DATE	PH	COOSP	COOML	TS	TVS	SS	VSS	DS	VDS	AMON	ANIT
56	56	7.63	16225	183286	14955	10994	13790	10495	12000	4500	12000	12000
57	57	7.54	16225	183286	14955	10994	13790	10495	12000	4500	12000	12000
58	58	7.47	16225	183286	14955	10994	13790	10495	12000	4500	12000	12000
59	59	7.45	16225	183286	14955	10994	13790	10495	12000	4500	12000	12000
60	60	7.70	14699	141477	61100	10994	13790	10495	12000	4500	12000	12000
61	61	7.63	14699	141477	61100	10994	13790	10495	12000	4500	12000	12000
62	62	7.60	14699	141477	61100	10994	13790	10495	12000	4500	12000	12000
63	63	7.60	14699	141477	61100	10994	13790	10495	12000	4500	12000	12000

FEED ONE-FIFTH SECOND REP

CBS	DATE	PR	COOSP	COO-L	TS	TVS	SS	VSS	DS	VDS	AMON	ANIT
56	7.49	1200	1700	207000	197800	1875	139	1170	770	54	777	
57		1096	760	197800	197800	1875	139	1030	000	41	777	
58	7.51	1096	760	197800	197800	1875	139	1030	000	41	777	
59		1096	760	197800	197800	1875	139	1030	000	41	777	
60		1096	760	197800	197800	1875	139	1030	000	41	777	
61	7.59	1096	760	197800	197800	1875	139	1030	000	41	777	
62	7.62	1096	760	197800	197800	1875	139	1030	000	41	777	
63		1096	760	197800	197800	1875	139	1030	000	41	777	
64		1096	760	197800	197800	1875	139	1030	000	41	777	
65		1096	760	197800	197800	1875	139	1030	000	41	777	
66	7.51	1096	760	197800	197800	1875	139	1030	000	41	777	
67		1096	760	197800	197800	1875	139	1030	000	41	777	
68	7.47	1096	760	197800	197800	1875	139	1030	000	41	777	
69	7.56	1096	760	197800	197800	1875	139	1030	000	41	777	
70	7.57	1096	760	197800	197800	1875	139	1030	000	41	777	
71		1096	760	197800	197800	1875	139	1030	000	41	777	
72		1096	760	197800	197800	1875	139	1030	000	41	777	
73		1096	760	197800	197800	1875	139	1030	000	41	777	
74	7.47	1096	760	197800	197800	1875	139	1030	000	41	777	
75	7.53	1096	760	197800	197800	1875	139	1030	000	41	777	
76		1096	760	197800	197800	1875	139	1030	000	41	777	
77		1096	760	197800	197800	1875	139	1030	000	41	777	
78		1096	760	197800	197800	1875	139	1030	000	41	777	
79	7.54	1096	760	197800	197800	1875	139	1030	000	41	777	
80		1096	760	197800	197800	1875	139	1030	000	41	777	
81		1096	760	197800	197800	1875	139	1030	000	41	777	
82		1096	760	197800	197800	1875	139	1030	000	41	777	
83	7.37	1096	760	197800	197800	1875	139	1030	000	41	777	
84	7.45	1096	760	197800	197800	1875	139	1030	000	41	777	
85	7.58	1096	760	197800	197800	1875	139	1030	000	41	777	
86		1096	760	197800	197800	1875	139	1030	000	41	777	
87		1096	760	197800	197800	1875	139	1030	000	41	777	
88		1096	760	197800	197800	1875	139	1030	000	41	777	

FEEC ONE THIRD FIRST REP

CBS	DATE	FR	COOSP	COOYL	TS	TVS	SS	VSS	DS	VDS	A*NON	ANIT
1	7.11	1		49006							12	90
2	7.11	1		49006							12	90
3	7.11	1		98133							22	181
4	7.11	1		98133							22	181
5	7.11	1		92555							22	181
6	7.11	1		92555							22	181
7	7.11	1		90666							259	201
8	7.11	1		90666							259	201
9	7.11	1		44444							780	606
10	7.11	1		44444							780	606
11	7.11	1		44444							780	606
12	7.11	1		44444							780	606
13	7.11	1		44444							780	606
14	7.11	1		44444							780	606
15	7.11	1		44444							780	606
16	7.11	1		44444							780	606
17	7.11	1		44444							780	606
18	7.11	1		44444							780	606
19	7.11	1		44444							780	606
20	7.11	1		44444							780	606
21	7.11	1		44444							780	606
22	7.11	1		44444							780	606
23	7.11	1		44444							780	606
24	7.11	1		44444							780	606
25	7.11	1		44444							780	606
26	7.11	1		44444							780	606
27	7.11	1		44444							780	606
28	7.11	1		44444							780	606
29	7.11	1		44444							780	606
30	7.11	1		44444							780	606
31	7.11	1		44444							780	606
32	7.11	1		44444							780	606
33	7.11	1		44444							780	606
34	7.11	1		44444							780	606
35	7.11	1		44444							780	606
36	7.11	1		44444							780	606
37	7.11	1		44444							780	606
38	7.11	1		44444							780	606
39	7.11	1		44444							780	606
40	7.11	1		44444							780	606
41	7.11	1		44444							780	606
42	7.11	1		44444							780	606
43	7.11	1		44444							780	606
44	7.11	1		44444							780	606
45	7.11	1		44444							780	606
46	7.11	1		44444							780	606
47	7.11	1		44444							780	606
48	7.11	1		44444							780	606
49	7.11	1		44444							780	606
50	7.11	1		44444							780	606
51	7.11	1		44444							780	606
52	7.11	1		44444							780	606
53	7.11	1		44444							780	606
54	7.11	1		44444							780	606
55	7.11	1		44444							780	606
56	7.11	1		44444							780	606
57	7.11	1		44444							780	606
58	7.11	1		44444							780	606
59	7.11	1		44444							780	606
60	7.11	1		44444							780	606
61	7.11	1		44444							780	606
62	7.11	1		44444							780	606
63	7.11	1		44444							780	606
64	7.11	1		44444							780	606
65	7.11	1		44444							780	606
66	7.11	1		44444							780	606
67	7.11	1		44444							780	606
68	7.11	1		44444							780	606
69	7.11	1		44444							780	606
70	7.11	1		44444							780	606
71	7.11	1		44444							780	606
72	7.11	1		44444							780	606
73	7.11	1		44444							780	606
74	7.11	1		44444							780	606
75	7.11	1		44444							780	606
76	7.11	1		44444							780	606
77	7.11	1		44444							780	606
78	7.11	1		44444							780	606
79	7.11	1		44444							780	606
80	7.11	1		44444							780	606
81	7.11	1		44444							780	606
82	7.11	1		44444							780	606
83	7.11	1		44444							780	606
84	7.11	1		44444							780	606
85	7.11	1		44444							780	606
86	7.11	1		44444							780	606
87	7.11	1		44444							780	606
88	7.11	1		44444							780	606
89	7.11	1		44444							780	606
90	7.11	1		44444							780	606
91	7.11	1		44444							780	606
92	7.11	1		44444							780	606
93	7.11	1		44444							780	606
94	7.11	1		44444							780	606
95	7.11	1		44444							780	606
96	7.11	1		44444							780	606
97	7.11	1		44444							780	606
98	7.11	1		44444							780	606
99	7.11	1		44444							780	606
100	7.11	1		44444							780	606

FEEB ONE-THIRD FIRST REP

DBS	DATE	P.	COOSP	COOPL	TS	TVS	SS	VSS	DS	VDS	AMMUN	ANIT
56	56		3502	2992	37410	25465	35270	24555	2140	950	904	703.111
57	57		3502	2992	37410	25465	35270	24555	2140	950	904	703.111
58	58	7.42	4173	2260	38600		35597	27990	2140	1480	929	722.556
59	59		4173	2260	38600		35597	27990	2140	1480	929	722.556
60	60	7.36	2335	2260	38600		35597	27990	2140	1480	929	722.556
61	61		2335	2260	38600		35597	27990	2140	1480	929	722.556
62	62	7.46	2335	2260	38600	26610	35597	27990	2140	1480	929	722.556
63	63		2335	2260	38600	26610	35597	27990	2140	1480	929	722.556
64	64	7.36	2335	2260	38600	18440	35597	27990	2140	1480	929	722.556
65	65		2335	2260	38600	18440	35597	27990	2140	1480	929	722.556
66	66	7.44	2335	2260	38600	19780	35597	27990	2140	1480	929	722.556
67	67		2335	2260	38600	19780	35597	27990	2140	1480	929	722.556
68	68	7.42	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
69	69		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
70	70	7.46	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
71	71		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
72	72	7.46	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
73	73		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
74	74	7.43	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
75	75		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
76	76	7.44	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
77	77		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
78	78	7.44	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
79	79		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
80	80	7.50	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
81	81		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
82	82	7.35	2335	2260	38600	18080	35597	27990	2140	1480	929	722.556
83	83		2335	2260	38600	18080	35597	27990	2140	1480	929	722.556

FEED ONE-THIRD SECOND REP

SSS	DATE	PR	UOSP	COOHL	TS	TYS	SS	VSS	DS	VDS	AMMON	AVIT
56	56		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
57	57		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
58	58	7.42	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
59	59		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
60	60	7.3b	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
61	61		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
62	62	7.46	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
63	63		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
64	64	7.36	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
65	65		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
66	66	7.44	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
67	67		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
68	68	7.42	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
69	69		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
70	70	7.46	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
71	71		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
72	72	7.46	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
73	73		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
74	74	7.43	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
75	75		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
76	76	7.44	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
77	77		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
78	78	7.44	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
79	79		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
80	80	7.50	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
81	81		3500	2000	3741	25465	35270	24515	21400	950	904	703.111
82	82	7.35	3500	2000	3741	25465	35270	24515	21400	950	904	703.111
83	83		3500	2000	3741	25465	35270	24515	21400	950	904	703.111

FEED ONE-THIRD THIRD REP

UBS	DATE	P-	CDSP	CDML	TS	TVS	SS	VSS	DS	VDS	AMON	ANIT
56	56	7.50	2708	31589	2	16480	2	15730		750	4	17
57	57	7.48	2708	31589	2	16480	2	15730		750	4	17
58	58	7.46	2708	31589	2	16480	2	15730		750	4	17
59	59	7.56	2708	31589	2	16480	2	15730		750	4	17
60	60	7.57	2708	31589	2	16480	2	15730		750	4	17
61	61	7.45	2708	31589	2	16480	2	15730		750	4	17
62	62	7.67	2708	31589	2	16480	2	15730		750	4	17
63	63	7.60	2708	31589	2	16480	2	15730		750	4	17
64	64		2708	31589	2	16480	2	15730		750	4	17
65	65		2708	31589	2	16480	2	15730		750	4	17
66	66		2708	31589	2	16480	2	15730		750	4	17
67	67	7.55	2708	31589	2	16480	2	15730		750	4	17
68	68	7.56	2708	31589	2	16480	2	15730		750	4	17
69	69	7.55	2708	31589	2	16480	2	15730		750	4	17
70	70	7.56	2708	31589	2	16480	2	15730		750	4	17
71	71	7.55	2708	31589	2	16480	2	15730		750	4	17
72	72	7.72	2708	31589	2	16480	2	15730		750	4	17
73	73	7.52	2708	31589	2	16480	2	15730		750	4	17
74	74	7.50	2708	31589	2	16480	2	15730		750	4	17
75	75	7.47	2708	31589	2	16480	2	15730		750	4	17
76	76	7.25	2708	31589	2	16480	2	15730		750	4	17
77	77	7.25	2708	31589	2	16480	2	15730		750	4	17
78	78	7.31	2708	31589	2	16480	2	15730		750	4	17
79	79	7.31	2708	31589	2	16480	2	15730		750	4	17
80	80	7.48	2708	31589	2	16480	2	15730		750	4	17
81	81	7.45	2708	31589	2	16480	2	15730		750	4	17
82	82	7.49	2708	31589	2	16480	2	15730		750	4	17
83	83	7.58	2708	31589	2	16480	2	15730		750	4	17
84	84		2708	31589	2	16480	2	15730		750	4	17
85	85		2708	31589	2	16480	2	15730		750	4	17
86	86		2708	31589	2	16480	2	15730		750	4	17
87	87	7.34	2708	31589	2	16480	2	15730		750	4	17
88	88	7.36	2708	31589	2	16480	2	15730		750	4	17
89	89		2708	31589	2	16480	2	15730		750	4	17
90	90		2708	31589	2	16480	2	15730		750	4	17
91	91		2708	31589	2	16480	2	15730		750	4	17
92	92	7.39	2708	31589	2	16480	2	15730		750	4	17
93	93	7.36	2708	31589	2	16480	2	15730		750	4	17
94	94	7.69	2708	31589	2	16480	2	15730		750	4	17
95	95	7.52	2708	31589	2	16480	2	15730		750	4	17
96	96		2708	31589	2	16480	2	15730		750	4	17
97	97		2708	31589	2	16480	2	15730		750	4	17
98	98		2708	31589	2	16480	2	15730		750	4	17
99	99		2708	31589	2	16480	2	15730		750	4	17
100	100		2708	31589	2	16480	2	15730		750	4	17
101	101		2708	31589	2	16480	2	15730		750	4	17
102	102		2708	31589	2	16480	2	15730		750	4	17
103	103		2708	31589	2	16480	2	15730		750	4	17
104	104		2708	31589	2	16480	2	15730		750	4	17
105	105		2708	31589	2	16480	2	15730		750	4	17
106	106		2708	31589	2	16480	2	15730		750	4	17
107	107		2708	31589	2	16480	2	15730		750	4	17
108	108		2708	31589	2	16480	2	15730		750	4	17
109	109		2708	31589	2	16480	2	15730		750	4	17
110	110		2708	31589	2	16480	2	15730		750	4	17

FEED ONE-THIRD THIRD REP

CBS	DATE	PH	CODSP	CODPL	TS	TVS	SS	VSS	OS	VDS	AMON	ANIT
1111		7.37	1111	2200	2700	1100	2	175	14	596	787	6
1112			1111	2200	2700	1100	2	175	14	596	787	1
1113		7.42	1111	2200	2700	1100	2	175	14	596	787	2
1114			1111	2200	2700	1100	2	175	14	596	787	1
1115		7.44	1111	2200	2700	1100	2	175	14	596	787	1
1116			1111	2200	2700	1100	2	175	14	596	787	1
1117			1111	2200	2700	1100	2	175	14	596	787	1
1118			1111	2200	2700	1100	2	175	14	596	787	1
1119			1111	2200	2700	1100	2	175	14	596	787	1
1120		7.50	1111	2200	2700	1100	2	175	14	596	787	1
1121		7.56	1111	2200	2700	1100	2	175	14	596	787	1
1122		7.57	1111	2200	2700	1100	2	175	14	596	787	1
1123			1111	2200	2700	1100	2	175	14	596	787	1
1124			1111	2200	2700	1100	2	175	14	596	787	1
1125			1111	2200	2700	1100	2	175	14	596	787	1
1126		7.52	1111	2200	2700	1100	2	175	14	596	787	1
1127			1111	2200	2700	1100	2	175	14	596	787	1
1128		7.49	1111	2200	2700	1100	2	175	14	596	787	1
1129			1111	2200	2700	1100	2	175	14	596	787	1
1130			1111	2200	2700	1100	2	175	14	596	787	1
1131		7.56	1111	2200	2700	1100	2	175	14	596	787	1
1132		7.56	1111	2200	2700	1100	2	175	14	596	787	1
1133			1111	2200	2700	1100	2	175	14	596	787	1
1134		7.60	1111	2200	2700	1100	2	175	14	596	787	1
1135			1111	2200	2700	1100	2	175	14	596	787	1
1136		7.45	1111	2200	2700	1100	2	175	14	596	787	1
1137			1111	2200	2700	1100	2	175	14	596	787	1
1138		7.43	1111	2200	2700	1100	2	175	14	596	787	1
1139		7.49	1111	2200	2700	1100	2	175	14	596	787	1
1140		7.63	1111	2200	2700	1100	2	175	14	596	787	1
1141			1111	2200	2700	1100	2	175	14	596	787	1
1142			1111	2200	2700	1100	2	175	14	596	787	1
1143		7.36	1111	2200	2700	1100	2	175	14	596	787	1
1144		7.55	1111	2200	2700	1100	2	175	14	596	787	1
1145			1111	2200	2700	1100	2	175	14	596	787	1
1146			1111	2200	2700	1100	2	175	14	596	787	1
1147		7.43	1111	2200	2700	1100	2	175	14	596	787	1
1148			1111	2200	2700	1100	2	175	14	596	787	1
1149		7.30	1111	2200	2700	1100	2	175	14	596	787	1
1150		7.43	1111	2200	2700	1100	2	175	14	596	787	1
1151			1111	2200	2700	1100	2	175	14	596	787	1
1152			1111	2200	2700	1100	2	175	14	596	787	1
1153		7.54	1111	2200	2700	1100	2	175	14	596	787	1
1154			1111	2200	2700	1100	2	175	14	596	787	1
1155			1111	2200	2700	1100	2	175	14	596	787	1
1156			1111	2200	2700	1100	2	175	14	596	787	1
1157			1111	2200	2700	1100	2	175	14	596	787	1
1158			1111	2200	2700	1100	2	175	14	596	787	1
1159			1111	2200	2700	1100	2	175	14	596	787	1
1160			1111	2200	2700	1100	2	175	14	596	787	1

FEED ONE-HALF FIRST REP

DS	DATE	PT	LOOSP	COCKE	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT
56	57	7.39	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
57	58	7.45	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
58	59	7.48	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
59	60	7.52	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
60	61	7.52	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
61	62	7.61	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778
62	63	7.70	41000	45595	43350	30160	41090	28950	2460	1210	694	39.778

FEED ONE-HALF SECOND REP

UHS	DATE	PL	COOSP	COML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT
1	1	7.71	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.46	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.60	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.39	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.25	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.35	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.47	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.43	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.43	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.55	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.30	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.38	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.37	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.38	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.64	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.50	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.46	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.50	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.38	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.57	000000	000000	26460	18465	24500	17615	19600	8500	673	764
1	1	7.60	000000	000000	26460	18465	24500	17615	19600	8500	673	764

FEED STRAIGHT FIRST REP

DATE	PH	UNDOF	COPL	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT
7.12		17753	77689	63750	45235	57827	42707			20990	20990
7.15		17753	77689	63750	45235	57827	42707			20990	20990
7.50		22187	65079	70475	47570	66260	45410	5170	2160	20990	20990
7.32		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.48		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.43		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.17		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.17		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.25		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.25		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.25		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.25		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.31		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.30		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.38		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.44		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.39		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.32		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.42		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.19		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.40		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.50		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.38		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.61		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.57		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.29		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.48		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.58		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.32		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.04		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.28		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.20		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.37		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.21		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.19		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.27		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.33		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990
7.35		25591	64822	75065	46045	67970	45410	5170	2160	20990	20990

FEED STRAIGHT FIRST REP

DBS	DATE	PR	CRD SP	CUMUL	TS	TVS	SS	VSS	DS	VDS	AYMON	ANIT
56	56		22157	66106	83220	57495	77690	54055	7620	3440	3134	2437
57	57	7.34	11482	78933	87785	61725	82130	57305	8430	4420	3134	2437
58	58		11482	78933	87785	61725	82130	57305	8430	4420	3134	2437
59	59	7.20	18677	75599	87035	61120	74520	57190	7840	3940	3134	2437
60	60	7.30	18677	75599	87035	61120	74520	57190	7840	3940	3134	2437
61	61	7.31	11482	86614	86515	62235	80700	56190	8390	3880	3134	2437
62	62		11482	86614	86515	62235	80700	56190	8390	3880	3134	2437
63	63	7.32	18288	76490	86275	61870	80460	57950	7910	3920	3134	2437
64	64	7.52	18288	76490	86275	61870	80460	57950	7910	3920	3134	2437
65	65	7.33	18288								3134	2437
66	66		18288								3134	2437
67	67	7.11	21260								3134	2437
68	68		21260								3134	2437

FEED FINISHER FIRST REP

DBS	DATE	FR	COESP	COOML	TS	TVS	SS	VSS	DS	VDS	AMON	ANIT
56	7.26	7.24	33594	121705	132105	904336	127145	87806	4960	2630	2871	2233.00
57	7.28	7.28	33594	121705	132105	904336	127145	87806	4960	2630	2871	2233.00
58	7.24	7.24	33594	121705	132105	904336	127145	87806	4960	2630	2871	2233.00
59	7.27	7.27	33594	121705	132105	904336	127145	87806	4960	2630	2871	2233.00
60	7.17	7.17	20743	90698	930255	649335	84855	60945	8170	3990	2532	1969.33
61	7.29	7.29	20743	90698	930255	649335	84855	60945	8170	3990	2532	1969.33
62	7.34	7.34	20743	90698	930255	649335	84855	60945	8170	3990	2532	1969.33
63	7.25	7.25	20743	90698	930255	649335	84855	60945	8170	3990	2532	1969.33

FEED FINISHER SECOND REP

OBS	DATE	PH	COBSP	COOYL	TS	TVS	SS	VSS	DS	VDS	AMMON	A-IT
56	56											0.00
57	57											0.00
58	58											0.00
59	59		13859				64230		4710	2140	2920	2271.11
60	60		13859				64230		4710	2140	2920	2271.11
61	61		13859				64230		4710	2140	2920	2271.11
62	62											0.00
63	63											0.00
64	64											0.00
65	65											0.00
66	66	7.54										0.00
67	67											0.00
68	68	7.63										0.00
69	69	7.44			133070	79300						0.00
70	70				133070	79300						0.00
71	71				133070	79300						0.00
72	72				133070	79300						0.00
73	73				119570	69720						0.00
74	74				119570	69720						0.00
75	75				119570	69720						0.00
76	76				119570	69720						0.00
77	77											0.00
78	78											0.00
79	79	7.59										0.00
80	80											0.00
81	81		200076	94255	128650	78060					2228	1777.22
82	82	7.55	200076	94255	128650	78060					2228	1777.22
83	83	7.66	200076	94255	128650	78060					2228	1777.22
84	84		200076	94255	128650	78060					2228	1777.22
85	85	7.61	118851	94255							2228	1777.22
86	86		118851	94255							2228	1777.22
87	87		118851	94255							2228	1777.22
88	88		118851	94255							2228	1777.22

APPENDIX F

DIGESTER RESPONSE DATA

LINE=SEVENTH FIRST REP

CBS	DATE	TE	GAS	PH	ALK	CODSP	COD*ML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
1	1	7.16	2917	843	6086	12475	4375	4310	3315	7120	1060	207	161.000			
		7.13	2867	668									0.000			
		7.08	2833	248									0.000			
		7.06	2856	678	3759	10400	2735	2650	1965	6480	770	194	150.889			
		7.04	3033	599									0.000			
		7.00	3117	755									0.000			
		7.04	3267	745									0.000			
		7.13	3400	608	3529	12620	2825	2787	1933	9473	1113	196	152.000			
		7.13	3500	664									0.000			
		7.14	3535	644	3294	12605	2420	3067	1760	9538	660		0.000			
		7.14	3535	644									0.000			
		7.11	3535	644									0.000			
		7.11	3535	644	2667	10295	2400	2400	1640	7895	760		0.000		168	
		7.11	3535	644									0.000			
		7.11	3535	644	3157	9765	2770	2120	1513	7645	1257		277	221.500		
		7.11	3535	644									288	223.000	240	
		7.11	3535	644									287	223.000		
		7.11	3535	644	711									0.000		
		7.11	3535	644	751	3413	8705	2250	2260	1670	5570	580	265	206.000		
		7.11	3535	644	595									0.000		
		7.11	3535	644	790	3557	7935	2415	2930	1915	5020	500	290	225.556	144	
		7.11	3535	644	742									0.000		
		7.11	3535	644	856	3504	7390	2290	2610	1910	4310	380	362	281.556	168	
		7.11	3535	644	801									0.000		
		7.11	3535	644	875									0.000		
		7.11	3535	644	830	2957	7080	2450	2530	2110	2140	340		0.000	168	
		7.11	3535	644	850									0.000		
		7.11	3535	644	817									0.000		
		7.11	3535	644	906									0.000		
		7.11	3535	644	945									0.000		
		7.11	3535	644	957									0.000		
		7.11	3535	644	953	3658								0.000		
		7.11	3535	644	950									0.000		
		7.11	3535	644	972	3566	5910	2685	3010	1935	3100	7	327	254.333	192	
		7.11	3535	644	972									0.000		
		7.11	3535	644	902	3294	5225	2150	2170	1430	2860	720	421	327.444		
		7.11	3535	644	934									0.000		
		7.11	3535	644	950	3411	5725	3150	2160	2150	3060	1000	409	318.111		
		7.11	3535	644	950									0.000		
		7.11	3535	644	1036									0.000		
		7.11	3535	644	1080	3745	5315	2640	2500	2230	2320	410		0.000		
		7.11	3535	644	1038									0.000		
		7.11	3535	644	1080									0.000		
		7.11	3535	644	1132									0.000		
		7.11	3535	644	1111									0.000		
		7.11	3535	644	1111	4878	5455	3005	3630	2195	2120	810		0.000		
		7.11	3535	644	1149									0.000		
		7.11	3535	644	1175									0.000		
		7.11	3535	644	1201	4860	5520	2830	3500	2330	2170	500	366	284.000		
		7.11	3535	644	1201									0.000		
		7.11	3535	644	1220									0.000		
		7.11	3535	644	1235									0.000		

ONE-SEVENTH FIRST REP

UBS	DATE	TELE	GAS	PH	ALK	COOESP	COOML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
56	000000		331			1394									0,000	
57	000000		420			1295									0,000	
58	000000		420	7,63	2533										0,000	
59	000000		420	7,63											0,000	
60	000000		420	7,63	2650	1280	7360	7490	5135	5760	4385	1600	750	468	364,000	
61	000000		420	7,63	2683	1270									0,000	
62	000000		420	7,63		1255									0,000	
63	000000		420	7,63	2867	1265	10039	9100	6455	7780	5715	1830	740	466	362,444	
64	000000		420	7,63	783	1194									0,000	
65	000000		420	7,63	783	1181	7953	8445	5925	7250	5565	1480	360	485	377,222	
66	000000		420	7,63	883	1222									0,000	
67	000000		420	7,63		1167									0,000	
68	000000		420	7,63	2767	1364									0,000	
69	000000		420	7,63	717	1101									0,000	
70	000000		420	7,63	867	1236	12383	8545	6030	8230	5680	1120	350	406	315,778	
71	000000		420	7,63	867	1036									0,000	
72	000000		420	7,63	867	1036									0,000	
73	000000		420	7,63	867	1036	8560	8910		7200		1710	870	495	385,000	72
74	000000		420	7,63	867	1036									0,000	
75	000000		420	7,63	867	1036	8560	7840	5470	6490	5120	1220	350	502	390,444	240
76	000000		420	7,63	867	1036									0,000	
77	000000		420	7,63	867	1036									0,000	
78	000000		420	7,63	867	1036	11843	8105	5595	6540	5185	1260	850	438	340,667	240
79	000000		420	7,63	867	1036									0,000	
80	000000		420	7,63	867	1036	9344	9510	6710	8520	6180	1430	900	474	368,667	216
81	000000		420	7,63	867	1036									0,000	
82	000000		420	7,63	867	1036	9183	9090	6485	8180	5935	1390	550	473	367,889	216
83	000000		420	7,63	867	1036									0,000	
84	000000		420	7,63	867	1036	7782	8795	6095	7580	5155	1760	940	483	375,667	

ONE-SEVENTH SECOND REP

DBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA	
59	59	3	306	7.38	2900	1225	7680	8140	5435	7320	4775	1430	660	506	0.0000		
59	59	4	304	7.35	3000	1200									0.0000		
59	59	5	301	7.30	3017	1176								506	0.0000		
59	59	6	300	7.45		11089	7160	7320	4700	6150	3960	1700	740	542	0.5556		
59	59	7	300	7.51	2983	11083	7160	7320	4700	6150	3960	1700	740	542	0.5556		
59	59	8	300	7.50	3133	1129	7428	7450	4960	6380	4320	1440	640	538	0.0000		
59	59	9	300	7.47	2967	1167									0.0000		
59	59	10	300	7.60		1148									0.0000		
59	59	11	300	7.41	2950	1120	8047	6890	4655	5880	4335	1050	320	461	0.0000		
59	59	12	300	7.49	2967	1152								498	0.5556		
59	59	13	300	7.38	2950	1129	7938	7310	7480	5960	4180	1710	600	497	0.5556	72	
59	59	14	300	7.38	2883	1109								386	0.5556		
59	59	15	300	7.51	2733	1109	6848	6610	4230	5470	3840	1140	390	438	0.0000	120	
59	59	16	300	7.51	2667	1109									340	0.0000	
59	59	17	300	7.32		1097									0.0000		
59	59	18	300	7.40	2917	1109	7922	7345	4660	6080	4240	1270	420	520	0.0000	168	
59	59	19	300	7.40	3007	1109								408	0.4444		
59	59	20	300	7.35	3007	1109	7259	6720	4375	5440	3895	1370	480	541	0.0000	168	
59	59	21	300	7.51	3007	1109								428	0.0000		
59	59	22	300	7.51	3007	1109	7160	7775	5235	6380	4795	1430	440	472	0.0000	168	
59	59	23	300	7.51	3007	1109									360	0.0000	
59	59	24	300	7.51	3007	1109	6926	6745	4370	6000		1670		472	0.1111		

ONE-SEVENTH THIRD REP

OBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
56	56	33	272	7.37	2267	1226	6381	6235	4125	4610	3705	1360	420		0.000	144
57	57	33	272	7.50	2267	1245									0.000	
58	58	33	266	7.41	2267	1148	6070	6230	4160	5080	3760	1310	400	603	469.000	240
59	59	33	222	7.33	2267	1162								459	357.000	
60	60	33	260	7.43	2267	1167								459	357.000	
61	61	33	208	7.32	2267	1147	6549	5795	3915	5020	3545	1180	370	481	374.111	144
62	62	33	248	7.44	2267	1035								448	348.444	
63	63	33	260	7.33	2267	1062	4769	4510	2935	3160	2655	1100	280	448	348.444	168
64	64	33	296	7.44	2267										0.000	140
65	65	33	249	7.33	2167	1019								463	360.111	192
66	66	33	273	7.44											0.000	
67	67	33	256	7.33		898									0.000	
68	68	33	256	7.31	2150	927	4710	4800	3110	3490	2910	950	200	484	376.444	168
69	69	33	165	7.32	2150	827									0.000	
70	70	33	213	7.41	2150	942	5615	5060	3090	4130	2850	1010	240	478	371.778	144
71	71	33	105	7.44	2150	808									0.000	
72	72	33	150	7.33	2150	898	5444	5045	3205	4100	2965	1040	240		0.000	192
73	73	33	187	7.27	2150	904									0.000	
74	74	33	167	7.40	2150	898									0.000	
75	75	33	217	7.32	2150	872	5194	5110	3340	5610	2950	1110	390		0.000	192
76	76	33	169	7.33	2150	853								407	316.556	
77	77	33	169	7.33	2150	849	5194	4460	2900	3940	2620	1060	280	395	307.222	192
78	78	33	191	7.33	2150	906									0.000	
79	79	33	168	7.37	2150	992	6279	5095	3175	4500	2645	1160	530	437	339.889	168
80	80	33	180	7.37	2150	934									0.000	
81	81	33	167	7.37	2150	1008	7027	6155	4420	5240	4130	960	290		0.000	144
82	82	33	167	7.37	2150	888									0.000	
83	83	33	161	7.44	2150	946									0.000	
84	84	33	196	7.33	2150	917	5753	5985	4000	5030	3590	1150	410	439	341.444	156
85	85	33	215	7.33	2150	904									0.000	
86	86	33	224	7.33	2150	846	8308	7205	4850	6500	4450	900	400	411	319.667	144
87	87	33	198	7.30	2150	946									0.000	
88	88	33	204	7.30	2150	946									0.000	192
89	89	33	194	7.33	2200	891	6046	6610	4545	5420	4345	990	200	398	309.556	144
90	90	33	194	7.33	2200	935									0.000	
91	91	33	101	7.33	2200	867	7176	5860	3985	4830	3745	810	240		0.000	
92	92	33	113	7.33	2200	865									0.000	
93	93	33	169	7.33	2200	918	5703	6165	4130	4760	3830	1130	300	465	361.667	192
94	94	33	188	7.33	1933	859									0.000	
95	95	33	261	7.33	1933	859								458	356.222	
96	96	33	151	7.33	1967	859	4844	5165	3595	4560	3255	880	340	394	306.444	168
97	97	33	121	7.33	2050	798									0.000	
98	98	33	206	7.33	2050	798	5603	6075	4310	4180	4050	1000	240	413	321.222	168
99	99	33	177	7.33	2050	833									0.000	
100	100	33	177	7.33	1950	717	5349	5075	3270	4650	3080	810	190		0.000	
101	101	33	178	7.33		739									0.000	
102	102	33	158	7.33	1983	775									0.000	
103	103	33	134	7.33	1983	814	5659	5363		4870		1020	380		0.000	192
104	104	33	100	7.33	2000	833									0.000	
105	105	33	159	7.33	2000	772	5174	4970	3315	3980	3065	800	250		0.000	168
106	106	33	136	7.33	2000	772									0.000	
107	107	33	177	7.33	2000	723	5234	6595	4665	5430	4485	720	180	374	290.889	168
108	108	33	213	7.33	2000	792									0.000	
109	109	33	191	7.33	2000	734								374	290.889	
110	110	33	212	7.26	1944	811	4556	4535	2890	3920	2480	1100	410	434	337.556	216

ONE-SEVENTH THIRD REP

OBS	DATE	TEMP	GAS	PH	ALK	COOSP	CODML	TS	TVS	SS	VSS	DB	VDS	AMMON	ANIT	VA
1	7.29	09.14	07	7.29	1883	744	4903	5605	3450	4330	3140	880	310	367	0.000	168
2	7.27	09.12	07	7.27	1912	782	5469	5820	4050	4420	3640	850	410	434	0.000	168
3	7.27	09.11	07	7.27	1944	636	5714	4780	3065	4140	2555	1220	510	431	0.000	144
4	7.27	09.11	07	7.27	1920	830	5373	5020		4110		910	260	392	0.000	168
5	7.26	09.10	07	7.26	1920	765									0.000	
6	7.26	09.10	07	7.26	1920	765									0.000	
7	7.26	09.10	07	7.26	1920	765									0.000	
8	7.26	09.10	07	7.26	1920	765									0.000	
9	7.26	09.10	07	7.26	1920	765									0.000	
10	7.26	09.10	07	7.26	1920	765									0.000	
11	7.26	09.10	07	7.26	1920	765									0.000	
12	7.26	09.10	07	7.26	1920	765									0.000	
13	7.26	09.10	07	7.26	1920	765									0.000	
14	7.26	09.10	07	7.26	1920	765									0.000	
15	7.26	09.10	07	7.26	1920	765									0.000	
16	7.26	09.10	07	7.26	1920	765									0.000	
17	7.26	09.10	07	7.26	1920	765									0.000	
18	7.26	09.10	07	7.26	1920	765									0.000	
19	7.26	09.10	07	7.26	1920	765									0.000	
20	7.26	09.10	07	7.26	1920	765									0.000	
21	7.26	09.10	07	7.26	1920	765									0.000	
22	7.26	09.10	07	7.26	1920	765									0.000	
23	7.26	09.10	07	7.26	1920	765									0.000	
24	7.26	09.10	07	7.26	1920	765									0.000	
25	7.26	09.10	07	7.26	1920	765									0.000	
26	7.26	09.10	07	7.26	1920	765									0.000	
27	7.26	09.10	07	7.26	1920	765									0.000	
28	7.26	09.10	07	7.26	1920	765									0.000	
29	7.26	09.10	07	7.26	1920	765									0.000	
30	7.26	09.10	07	7.26	1920	765									0.000	
31	7.26	09.10	07	7.26	1920	765									0.000	
32	7.26	09.10	07	7.26	1920	765									0.000	
33	7.26	09.10	07	7.26	1920	765									0.000	
34	7.26	09.10	07	7.26	1920	765									0.000	
35	7.26	09.10	07	7.26	1920	765									0.000	
36	7.26	09.10	07	7.26	1920	765									0.000	
37	7.26	09.10	07	7.26	1920	765									0.000	
38	7.26	09.10	07	7.26	1920	765									0.000	
39	7.26	09.10	07	7.26	1920	765									0.000	
40	7.26	09.10	07	7.26	1920	765									0.000	
41	7.26	09.10	07	7.26	1920	765									0.000	
42	7.26	09.10	07	7.26	1920	765									0.000	
43	7.26	09.10	07	7.26	1920	765									0.000	
44	7.26	09.10	07	7.26	1920	765									0.000	
45	7.26	09.10	07	7.26	1920	765									0.000	
46	7.26	09.10	07	7.26	1920	765									0.000	
47	7.26	09.10	07	7.26	1920	765									0.000	
48	7.26	09.10	07	7.26	1920	765									0.000	
49	7.26	09.10	07	7.26	1920	765									0.000	
50	7.26	09.10	07	7.26	1920	765									0.000	
51	7.26	09.10	07	7.26	1920	765									0.000	
52	7.26	09.10	07	7.26	1920	765									0.000	
53	7.26	09.10	07	7.26	1920	765									0.000	
54	7.26	09.10	07	7.26	1920	765									0.000	
55	7.26	09.10	07	7.26	1920	765									0.000	
56	7.26	09.10	07	7.26	1920	765									0.000	
57	7.26	09.10	07	7.26	1920	765									0.000	
58	7.26	09.10	07	7.26	1920	765									0.000	
59	7.26	09.10	07	7.26	1920	765									0.000	
60	7.26	09.10	07	7.26	1920	765									0.000	
61	7.26	09.10	07	7.26	1920	765									0.000	
62	7.26	09.10	07	7.26	1920	765									0.000	
63	7.26	09.10	07	7.26	1920	765									0.000	
64	7.26	09.10	07	7.26	1920	765									0.000	
65	7.26	09.10	07	7.26	1920	765									0.000	
66	7.26	09.10	07	7.26	1920	765									0.000	
67	7.26	09.10	07	7.26	1920	765									0.000	
68	7.26	09.10	07	7.26	1920	765									0.000	
69	7.26	09.10	07	7.26	1920	765									0.000	
70	7.26	09.10	07	7.26	1920	765									0.000	
71	7.26	09.10	07	7.26	1920	765									0.000	
72	7.26	09.10	07	7.26	1920	765									0.000	
73	7.26	09.10	07	7.26	1920	765									0.000	
74	7.26	09.10	07	7.26	1920	765									0.000	
75	7.26	09.10	07	7.26	1920	765									0.000	
76	7.26	09.10	07	7.26	1920	765									0.000	
77	7.26	09.10	07	7.26	1920	765									0.000	
78	7.26	09.10	07	7.26	1920	765									0.000	
79	7.26	09.10	07	7.26	1920	765									0.000	
80	7.26	09.10	07	7.26	1920	765									0.000	
81	7.26	09.10	07	7.26	1920	765									0.000	
82	7.26	09.10	07	7.26	1920	765									0.000	
83	7.26	09.10	07	7.26	1920	765									0.000	
84	7.26	09.10	07	7.26	1920	765									0.000	
85	7.26	09.10	07	7.26	1920	765									0.000	
86	7.26	09.10	07	7.26	1920	765									0.000	
87	7.26	09.10	07	7.26	1920	765									0.000	
88	7.26	09.10	07	7.26	1920	765									0.000	
89	7.26	09.10	07	7.26	1920	765									0.000	
90	7.26	09.10	07	7.26	1920	765									0.000	
91	7.26	09.10	07	7.26	1920	765									0.000	
92	7.26	09.10	07	7.26	1920	765									0.000	
93	7.26	09.10	07	7.26	1920	765									0.	

ONE-FIFTH FIRST REP

OBS	DATE	TEMP	GAS	PH	ALK	CLDOSP	CDOXL	TS	TV8	SS	V88	DS	VDS	AMMON	ANIT	VA
1	7-1-77	100	N2	7.47	6583	412	11873	13500	7935	8670	6655	4060	1280	313	243	192
2	7-1-77	100	N2	7.47	6583	412	11260	11870	7055	8810	5645	3630	1410	678	527	192
3	7-1-77	100	N2	7.47	6583	412	10079	12505	6285	7140	5365	4680	880	949	738	192
4	7-1-77	100	N2	7.47	6583	412	11133	12165	6485	7610	5925	4030	540	839	652	192
5	7-1-77	100	N2	7.47	6583	412	11328	12515	6655	8420	6035	4130	620	764	594	192
6	7-1-77	100	N2	7.47	6583	412	9684	10655	5960	6710	5000	3660	960	800	622	192
7	7-1-77	100	N2	7.47	6583	412	11621	11850	6795	8890	6175	3420	620	779	603	192
8	7-1-77	100	N2	7.47	6583	412	6765	11660	6570	6900	5620	3210	950	766	593	192
9	7-1-77	100	N2	7.47	6583	412	9449	9800	5820	6480	4780	3260	1040	938	729	192
10	7-1-77	100	N2	7.47	6583	412	8650	10240	5375	6610	4605	2950	690	747	581	120
11	7-1-77	100	N2	7.47	6583	412	7588	8180	4635	5340	3993	2640	640	833	647	240
12	7-1-77	100	N2	7.47	6583	412	7185	7540	4285	5100	3665	2340	420	564	458	288
13	7-1-77	100	N2	7.47	6583	412	7275	7150	4085	4560	3535	2590	510	647	501	168
14	7-1-77	100	N2	7.47	6583	412	6812	6960	3990	4940	3270	2310	720	884	374	192
15	7-1-77	100	N2	7.47	6583	412	5642	6895	4010	4340	3360	2410	650	608	427	168
16	7-1-77	100	N2	7.47	6583	412	7922	6995	4335	4800	3735	2030	600	630	490	144
17	7-1-77	100	N2	7.47	6583	412	6142	6240	3735	4310	2210	2210	560	586	453	240
18	7-1-77	100	N2	7.47	6583	412	5234	5510	3135	3670	2575	2090	560	368	441	168
19	7-1-77	100	N2	7.47	6583	412	5349	5260	3055	3310	2445	1970	610	653	507	212
20	7-1-77	100	N2	7.47	6583	412	6142	9825	5040	4680	4100	3900	940	655	509	216
21	7-1-77	100	N2	7.47	6583	412	6356	8650	4616	4830	3665	3500	950	602	468	192
22	7-1-77	100	N2	7.47	6583	412	6196	8520	4435	4800	3155	3950	1280	602	468	168
23	7-1-77	100	N2	7.47	6583	412	7645	9235	5025	5720	4305	2760	720	616	479	120

ONE-FIFTH FIRST REP

OBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
56	56	33.3	348	7.28	2467	1264	5603	7805	4505	4020	3735	2800	770		0.000	162
57	57	35.0		7.53	2933	2996									0.000	
58	58	36.5	520	7.45	2467	1556	6070	6900	3820	4440	3240	2230	580	587	456.000	212
59	59	36.0	319	7.31	2717	1475								576	448.000	
60	60	34.2	300	7.32	2750	1618								620	482.000	
61	61	35.2	518	7.26	2700	1578	5137	7165	3530	4240	3100	1840	430	633	492.000	144
62	62	33.0	369	7.36	2717	1582								599	465.000	
63	63	36.0	495	7.45	2700	1448	5692	7035	4475	3630	4055	1950	420	561	436.333	264

PERFECT SECURITIES

DATE	PRICE	QTY	AMOUNT	ACCT	TYPE	DATE	PRICE	QTY	AMOUNT	ACCT	TYPE	DATE	PRICE	QTY	AMOUNT	ACCT	TYPE
57	7.03	2944	20834	10522	10035	7120	4900	653	1440	500	512	398	222	0	0	0	0
58	7.27	3053	22185	9071	9450	6815	8500	6455	1300	360	553	450	111	0	0	0	0
59	7.27	3053	22185	12782	11105	8125	9660	7485	1310	640	192	450	111	0	0	0	0
60	7.35	3083	22655											0	0	0	0
61	7.35	3083	22655											0	0	0	0
62	7.35	3083	22655											0	0	0	0
63	7.35	3083	22655											0	0	0	0
64	7.29	3109	22640	9318	8740	5950	7290	5520	1500	430	619	481	442	0	0	0	0
65	7.32	3026	22185											0	0	0	0
66	7.33	3050	22250											0	0	0	0
67	7.33	3050	22250											0	0	0	0
68	7.33	3050	22250											0	0	0	0
69	7.33	3050	22250											0	0	0	0
70	7.33	3050	22250											0	0	0	0
71	7.33	3050	22250											0	0	0	0
72	7.33	3050	22250											0	0	0	0
73	7.33	3050	22250											0	0	0	0
74	7.33	3050	22250											0	0	0	0
75	7.33	3050	22250											0	0	0	0
76	7.33	3050	22250											0	0	0	0
77	7.33	3050	22250											0	0	0	0
78	7.33	3050	22250											0	0	0	0
79	7.33	3050	22250											0	0	0	0
80	7.33	3050	22250											0	0	0	0
81	7.33	3050	22250											0	0	0	0
82	7.33	3050	22250											0	0	0	0
83	7.33	3050	22250											0	0	0	0
84	7.33	3050	22250											0	0	0	0
85	7.33	3050	22250											0	0	0	0
86	7.33	3050	22250											0	0	0	0
87	7.33	3050	22250											0	0	0	0
88	7.33	3050	22250											0	0	0	0

NAME-TIME SECOND REP

SR	DATE	TIME	SEC	REP	ALC	CSA	CSPL	TC	TVS	SS	VSS	S	VCS	END	A-IT	VA
57	57	01	00	01	3074	3060	11040	11055	7360	8600	6100	2640	1260	1140	0	0
55	55	00	01	02	3517	3451	10584	10675	6770	8270	4980	3020	1790	1143	89	0
55	55	00	01	03	5650	5635	10584	10675	6770	8270	4980	3020	1790	1143	89	0
55	55	00	01	04	5650	5635	10584	10675	6770	8270	4980	3020	1790	1143	89	0
55	55	00	01	05	5417	5284	10679	10730	7320	7230	6350	2340	970	1115	867	222
55	55	00	01	06	5750	5651	10679	10730	7320	7230	6350	2340	970	1115	867	222
55	55	00	01	07	5033	5074	11719	11560	7870	8200	7180	2250	690	1058	822	889
55	55	00	01	08	5733	5694	11719	11560	7870	8200	7180	2250	690	1058	822	889
55	55	00	01	09	5660	5604	11673	10720	6965	8150	6195	2750	770	1196	930	222
55	55	00	01	10	5660	5604	11673	10720	6965	8150	6195	2750	770	1196	930	222
55	55	00	01	11	5323	5220	10272	9775	6325	7330	5615	2100	710	930	725	333
55	55	00	01	12	5323	5220	10272	9775	6325	7330	5615	2100	710	930	725	333
55	55	00	01	13	5417	5303	11202	10895	7260	8320	6500	6460	700	1052	810	222
55	55	00	01	14	5417	5303	11202	10895	7260	8320	6500	6460	700	1052	810	222
55	55	00	01	15	5630	5580	10905	10405	6770	7960	5410	2700	960	1005	781	667
55	55	00	01	16	5630	5580	10905	10405	6770	7960	5410	2700	960	1005	781	667
55	55	00	01	17	5133	5027	9901	11565	7155	7960	6095	5030	1060	1209	940	333
55	55	00	01	18	5133	5027	9901	11565	7155	7960	6095	5030	1060	1209	940	333
55	55	00	01	19	5400	5298	14075	11270	7640	9050	4510	4190	3130	1229	955	889
55	55	00	01	20	5400	5298	14075	11270	7640	9050	4510	4190	3130	1229	955	889

ONE-THIRD THIRD-REF

CBS	DATE	TR-F	GAS	PR	ALK	COOSP	COOML	TS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
56	56		94	7.41	5583	3268	10895	10640	7320	8350	6490	2310	830		0.000	192
57	57		94	7.41	4317	2221									0.000	
58	58		94	7.34	6100	2643	37043	36475	27365	33960	26725	1510	640		0.000	143
59	59		94	7.44	4700	7943									0.000	
60	60		75	7.37	5383	2243									0.000	
61	61		77	7.36	5517	2243	29116	28600	21430	26010	20720	1790	710	878	682.889	
62	62		77	7.37	5517	2243								981	765.889	
63	63		77	7.37	5517	2243								929	723.889	144
64	64		77	7.39	4917	2243	14769	22890	16915	19930	16395	1860	520	794	617.889	192
65	65		77	7.32	5183	2243	15077	16320	10915	12160	10125	1920	700	1103	857.889	192
66	66		91	7.32		2243								921	716.333	216
67	67		90	7.33		2243									0.000	
68	68		88	7.33	5633	2243	19691	18105	12585	15860	12115	1590	470	668	519.889	120
69	69		81	7.34	5317	2243	21231	19520	13270	16530	1270	1840	570	948	737.333	204
70	70		81	7.38	6633	2243									0.000	
71	71		71	7.38	4677	2243	17117	20155	13460	17130	13030	1650	430		0.000	168
72	72		69	7.35	5717	2243									0.000	
73	73		74	7.33	5700	2243									0.000	
74	74		75	7.33	5300	2243	18450	18590	13315	17970	12595	1960	720	770	598.889	288
75	75		76	7.33	5300	2243									0.000	
76	76		76	7.33	5300	2243	18217	16430	11460	16130	10770	2120	690	891	693.000	288
77	77		78	7.40	5483	2243									0.000	
78	78		78	7.43	5190	2243	22093	19055	13570	17200	12900	1930	670		0.000	168
79	79		80	7.52	5200	2243									0.000	
80	80		80	7.53	4917	2243									0.000	
81	81		81	7.33	5400	2243	19112	19240	14085	17760	13555	1670	530	661	514.111	216
82	82		82	7.55	4690	2243									0.000	
83	83		83	7.52	4850	2243	17857	15900	11230	14350	10610	2040	620	866	673.556	312
84	84		84	7.53	5290	2243									0.000	
85	85		85	7.53	5290	2243	24038	19890	14330	17960	13500	2290	830	866	673.556	216
86	86		86	7.50	5317	2243									0.000	
87	87		87			2243									0.000	
88	88		88	7.51		2243									0.000	144
89	89		89	7.34	5333	2243	24419	20395	15015	18150	14635	1610	380	922	717.111	192
90	90		90	7.48	5267	2243									0.000	
91	91		91	7.36	4683	2243									0.000	
92	92		92	7.40	4850	2243									0.000	192
93	93		93	7.39	4683	2243	17578	19025	13875	17140	13265	1780	610	855	665.000	168
94	94		94	7.41	4700	2243									0.000	
95	95		95	7.42		2243									0.000	
96	96		96	7.43	4317	2243	14844	15700	11465	14230	10595	1640	870	775	602.778	192
97	97		97	7.36	4483	2243									0.000	
98	98		98	7.31	4467	2243	16537	16290	11865	14510	11115	1930	750	760	591.111	
99	99		99			2243									0.000	
100	100		100	7.36	3850	2243	15504	13320	9510	12100	9110	1430	400		0.000	
101	101		101			2243									0.000	
102	102		102	7.35	6217	2243									0.000	
103	103		103	7.34	3900	2243	15698	13895	9880	13100	9250	1510	630		0.000	
104	104		104	7.34	4400	2243									0.000	216
105	105		105	7.34	4199	2243	16409	14640	10500	12910	9990	1490	510		0.000	
106	106		106	7.37	4299	2243									0.000	
107	107		107	7.37	4299	2243	15820	15785	11420	14720	10990	1420	430	695	540.556	
108	108		108	7.33	4306	2243									0.000	168
109	109		109	7.33		2243									0.000	
110	110		110	7.36	4258	2243	16216	15265	11270	13870	10610	1510	660	674	524.222	
														771	599.667	

ONE-THIRD THIRD REP

OBS	DATE	TEVP	GAS	PR	ALX	COUSP	COOML	TS	TVS	SS	VSS	OS	VOS	AMMON	ANIT	VA
111	111	34	295	7.34	4209										0.000	
112	112	30	413			2901									0.000	168
113	113	35	310												0.000	
114	114	35	400	7.30	4579	3168	22763	21245	15520	18340	14930	1480	590	707	549.889	360
115	115	35	400	7.30		3053								840	653.333	
116	116	35	276	7.35	5093	3268									0.000	
117	117	35	417	7.26	5029	3398	18945	19315	13735	18250	13325	1440	410	794	617.556	
118	118	35	249	7.34	5013	3086								717	557.667	
119	119	35	260	7.25	4884	3089	20463	17675	12300	17120	11710	1460	590		0.000	216
120	120	35	55	7.39	4620	3282								788	612.889	
121	121	35	55	7.26	5302	2985	20149	22190	16540	17630	16180	1520	360		0.000	168
122	122	35	76	7.36	5109	3134									0.000	
123	123	35	38												0.000	
124	124	35	38	7.47	5061	3619	16470	19200	13845	17720	13295	1590	550	781	607.444	280
125	125	35	40	7.43	4984	3731									0.000	
126	126	35	40	7.55	4901	417	17537	15140	11380	13430	10730	1770	650	819	637.000	192
127	127	35	91	7.20	4727	3843									0.000	
128	128	35	123	7.27	4651	3806	13806	12430	9285	10750	8635	1720	650	804	625.333	
129	129	35	71	7.57	3760	3494									0.000	
130	130	35	74			234									0.000	
131	131	35	71	7.20	3867	3643	15242	12860	9630	11530	9090	1750	540	743	577.889	
132	132	35	74	7.38	3792	3727									0.000	
133	133	35	99	7.44	4033	3647	15038	13925	10590	11500	9680	1750	910	814	633.111	192
134	134	35	99												0.000	
135	135	35	99	7.26	3679										0.000	
136	136	35	99												0.000	
137	137	35	99												0.000	
138	138	35	99												0.000	
139	139	35	99												0.000	
140	140	35	10	7.33	3540										0.000	
141	141	35	10	7.41	3776	3371	14962	14300	9945	11570	9235	1520	710	921	716.333	216
142	142	35	10	7.46	3683										0.000	
143	143	35	10												0.000	
144	144	35	10												0.000	
145	145	35	10												0.000	
146	146	35	10	7.32	3917										0.000	
147	147	35	10	7.34	3833										0.000	
148	148	35	10	7.30	3750										0.000	
149	149	35	10												0.000	
150	150	35	10	7.58	3800	4000	14706	12785	9730	10180	9160	1660	570	769	598.111	216
151	151	35	10	7.29	3667										0.000	
152	152	35	10												0.000	
153	153	35	10												0.000	
154	154	35	10	7.46	4033										0.000	
155	155	35	10												0.000	
156	156	35	10	7.54	3808	4023	15970	12230	8855	11120	7975	1700	880	752	584.889	216
157	157	35	10												0.000	
158	158	35	10	7.38	4233										0.000	
159	159	35	10												0.000	
160	160	35	10												0.000	
161	161	35	10												0.000	
162	162	35	10												0.000	
163	163	35	10												0.000	
164	164	35	10												0.000	
165	165	35	10												0.000	
166	166	35	10												0.000	
167	167	35	10												0.000	
168	168	35	10												0.000	
169	169	35	10	7.42	3985	3878	18821	15625	11420	13410	10820	1940	600	814	633.111	240
170	170	35	10											852	662.667	

ONE-HALF FIRST REP

QBS	DATE	TEMP	GAS	PH	ALK	COOSP	COOML	FS	TVS	SS	VSS	DS	VDS	AMMON	ANIT	VA
1	11/11/77	57.0	1515	7.78	5683	4537	16120	18585	10525	12600	9335	4690	1190	395	307.22	204
2	11/11/77	57.0	1446	7.91	6550	4460									0.00	
3	11/11/77	57.0	1737	7.90		3487									0.00	
4	11/11/77	57.0	1627	7.90		4751									0.00	
5	11/11/77	57.0	1773	7.90	6700	4160	16794	16825	10155	12060	8985	4610	1170	1201	934.11	
6	11/11/77	57.0	1880	7.90	6800	4001									0.00	
7	11/11/77	57.0	1036	7.90	7117	4032	16403	16360	9990	11960	9070	3760	920	1294	1006.44	
8	11/11/77	57.0	1084	7.90	7167	4492									0.00	
9	11/11/77	57.0	1253	7.75	7667	5078	16602	17755	10560	13050	9550	3630	1010	1614	1255.33	
10	11/11/77	57.0	1111	7.75	7617	4070									0.00	
11	11/11/77	57.0	1111	7.72		3643									0.00	
12	11/11/77	57.0	1111	7.72		4273									0.00	
13	11/11/77	57.0	1388	7.90	7867	4273	17188	17055	10720	13340	9850	3890	870	1137	884.33	
14	11/11/77	57.0	1443	7.90	8217	4683									0.00	
15	11/11/77	57.0	1443	7.90	8100	4099	16996	19085	12290	14510	10660	4600	1630	1323	1029.00	
16	11/11/77	57.0	1770	7.77	7767	4040									0.00	
17	11/11/77	57.0	1677	7.77	7817	4707	22168	21425	14210	18130	13190	4250	1020	1412	1098.22	
18	11/11/77	57.0	1777	7.74		4569									0.00	
19	11/11/77	57.0	1749	7.74	7733	4331									0.00	
20	11/11/77	57.0	1727	7.74	7900	4331	15784	19840	13515	14700	12495	3880	1020	1005	781.67	
21	11/11/77	57.0	1727	7.74	7500	4331									0.00	
22	11/11/77	57.0	1727	7.74	4930	4331	17126	21210	14720	16450	13060	3860	1660	1164	905.33	
23	11/11/77	57.0	1727	7.74	7717	4331									0.00	
24	11/11/77	57.0	1727	7.74	7930	4331	19163	19585	13020	15840	11820	4000	1200			288
25	11/11/77	57.0	1727	7.74	7930	4331									0.00	
26	11/11/77	57.0	1727	7.74	7667	4331	18872	18600	12415	15210	11345	3730	1070	1431	1117.00	312
27	11/11/77	57.0	1727	7.74	7883	4331									0.00	
28	11/11/77	57.0	1727	7.74	7883	4331	19193	18545	12635	14220	11735	3680	900	1154	897.33	240
29	11/11/77	57.0	1630	7.74	7483	3913									0.00	
30	11/11/77	57.0	1630	7.74	7483	4427	19048	18435	12685	18860	11535	3630	1150	1109	867.00	264
31	11/11/77	57.0	1630	7.74	7817	4427									0.00	
32	11/11/77	57.0	1706	7.70	7683	4444									0.00	
33	11/11/77	57.0	1457	7.70	7850	5119	20536	19500	13720	16410	12600	3420	1120	1350	1050.00	264
34	11/11/77	57.0	1322	7.67	7650	4961									0.00	
35	11/11/77	57.0	1285	7.66	7517	4241	19747	20885	14765	17220	13615	3370	1150	1164	1074.33	240
36	11/11/77	57.0	1285	7.66	7750	4922									0.00	
37	11/11/77	57.0	950	7.64	7717	5216									0.00	
38	11/11/77	57.0	1312	7.64	7433	3647	19412	20125	14455	16530	13195	3420	1260	1271	1008.56	288
39	11/11/77	57.0	1255	7.64	7233	5020									0.00	
40	11/11/77	57.0	1255	7.64	7333	5315	21457	21100	15440	17440	14310	3250	1130	1187	923.22	360
41	11/11/77	57.0	1846	7.60	7333	5059									0.00	
42	11/11/77	57.0	1846	7.60	7150	4609	20117	19665	13395	15050	12385	3100	1010	1095	851.67	336
43	11/11/77	57.0	1556	7.60	6967	5547									0.00	
44	11/11/77	57.0	1899	7.60	7000	4690	21318	18555	13425	16430	12175	3350	1250	1071	833.00	228
45	11/11/77	57.0	1899	7.60	7183	3928									0.00	
46	11/11/77	57.0	1899	7.60	6950	2338	23031	17565	12420	14290	11190	3190	1230	1132	860.44	216
47	11/11/77	57.0	1899	7.60	6817	1118									0.00	
48	11/11/77	57.0	1899	7.60	6817	7644	18798	18235	12585	15130	11275	3270	1310	994	777.11	336
49	11/11/77	57.0	1899	7.60	6817	4922									0.00	
50	11/11/77	57.0	1899	7.60	6817	5059	20392	17850	12680	14410	11680	3150	1000		0.00	288
51	11/11/77	57.0	1899	7.60	6817	5059									0.00	
52	11/11/77	57.0	1899	7.60	6817	5059									0.00	
53	11/11/77	57.0	1899	7.60	6817	5059	20656	17015	12425	15340	11365	3130	1060	1388	1079.56	168
54	11/11/77	57.0	1899	7.60	6817	5059									0.00	
55	11/11/77	57.0	1899	7.60	6817	5059									0.00	

ONE-HALF FIRST REP

OBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	V88	DS	VDS	AMMON	ANIT	VA
56	56	33.2	1425	7.41	6767	4241	21595	19555	14505	16210	13575	2810	930		0.00	240
57	57	35.0	1535	7.56	6583	4358									0.00	
58	58	37.0	1693	7.59	6550	4202	19650	17925	13010	15070	11750	3010	1260	1521	1183.00	240
59	59	36.0	1647	7.60	6433	4629								1393	1083.44	
60	60	34.3	1431	7.53	6667	4921								1521	1183.00	
61	61	35.5	1558	7.51	6467	5118	19902	19050	14305	15650	13165	2750	1140	1323	1029.00	216
62	62	33.6	1315	7.54	6483	4766								1366	1062.44	
63	63	36.6	1545	7.54	6467	4633	19615	18790	14140	14520	13400	2580	740	1311	1016.67	240

ONE-HALF SECOND REP

DBS	DATE	TIME	LAB	PR	FLK	COOSP	COOPL	TS	TVS	SS	VSS	DS	VDS	AMHON	ANIT	VA
56	56	34.0		7.46	6250	5784									0.00	
57	57	33.9		7.56	6234	5890	33022	26890	22025	24690	21135	2730	890	1139	885.89	
58	58	34.0		7.52	6700	5651									0.00	
59	59	34.7			768	5613									0.00	
60	60	34.0		7.50	7183	6208	27138	30015	22540	27320	21760	2660	780	1204	936.44	
61	61	34.0		7.36	6941	6458									0.00	
62	62	34.0		7.62	7250	6353	25564	25920	19060	23690	18020	2630	1040	1201	934.11	216
63	63	34.0			1151										0.00	
64	64	34.0		7.47	6893										0.00	
65	65	34.0			1034										0.00	
66	66	34.7			624										0.00	
67	67	34.0		7.55	6989										0.00	
68	68	34.9		7.36	7439	5971	29167	29235	20685	25450	19625	2310	1060	1325	1030.56	216
69	69	34.0		7.54	6950										0.00	
70	70	34.0			1135										0.00	
71	71	34.0			1186										0.00	
72	72	35.0			1192										0.00	
73	73	34.0		7.53	6550										0.00	
74	74	34.0		7.56	7350										0.00	
75	75	35.8		7.53	6433										0.00	
76	76	35.0			1116	7412	23529	21990	15370	19860	14530	2460	840	1121	871.89	264
77	77	35.0		7.69	6500										0.00	
78	78	35.0		7.44	6533										0.00	
79	79	37.2			1202										0.00	
80	80	36.9		7.54	6633										0.00	
81	81	34.8			993										0.00	
82	82	35.8			1092										0.00	
83	83	35.2		7.60	6262	6973	23954	19185	13225	18820	12285	2020	940	1185	921.67	240
84	84	36.1			1038										0.00	
85	85	35.6		7.51	6750										0.00	
86	86	35.2			1123										0.00	
87	87	34.5			1200									1181	918.56	
88	88	35.0		7.63	6619	6426	24905	23360	15995	22900	15105	2370	890	1286	1000.22	288

STRAIGHT FIRST REP

DBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	DS	VDS	AMEN	AMIT	VA
65	776	5.1	N394	7.9	20733	24941									0.00	
66	776	5.1	N107	7.9	20433	14008	95720	74480	52875	68100	49665	8120	3210	3134	2437.56	680
67	776	5.1	N505	7.9		3398								3197	2642.11	
68	776	5.1	N487	7.8	20200	0392	69261	66335	47880	58590	44860	7490	3020	3557	2766.56	2480
69	776	5.1	N237	7.8	20150	1206									0.00	
69	776	5.1	N230	7.9		5483									0.00	
69	776	5.1	N223	7.9	20950	7255	158431	77765	58170	71550	55090	7210	3080	3580	2784.44	3880
69	776	5.1	N799	8.1	17967	24510									0.00	
69	776	5.1	N1968	8.0	20950	24510	67954	71836	53025	66260	49185	9130	3840	3871	3010.78	4224
69	776	5.1	N2055	7.8	21733	3339									0.00	
69	776	5.1	N197	7.7	20533	4903	77043	69770	51175	65700	47105	8900	4070	3466	2695.78	2160
69	776	5.1	N495	7.7	20750	3486									0.00	
69	776	5.1	N008	7.9	21500	6654									0.00	
69	776	5.1	N325	7.9		3930	76264	80905	57505	74220	53995	7830	3510	3547	2758.78	

STRAIGHT THIRD REP

UBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	DS	VDS	AMPOV	ANIT	VA
1	11/11/77	7.88		6600	3456	19015	19150	12500	14680	10870	4520	1630	335	260.56	192	
2	11/12/77	7.73		7000	3417									0.00		
3	11/13/77	7.92			3478									0.00		
4	11/14/77	7.77			3384									0.00		
5	11/15/77	7.65		8117	5059	20611	19700	12960	15200	11290	4300	1670	1329	1033.67		
6	11/16/77	7.67		8567	5217	22134	20645	13495	16800	12155	4430	1340	1553	1207.89		
7	11/17/77	7.73		9250	6172									0.00		
8	11/18/77	7.66		10100	6434	22656	26290	18460	22250	16240	5990	2220	1807	1405.44		
9	11/19/77	7.76		10317	6899									0.00		
10	11/20/77	7.84			6356									0.00		
11	11/21/77	7.72		11000	6719	27539	26720	18010	21040	15940	6220	2070	1447	1125.44		
12	11/22/77	7.77		11650	6905									0.00		
13	11/23/77	7.65		11750	6877	25823	26955	17210	20250	13980	6850	3230	2029	1578.11		
14	11/24/77	7.89		12100	8103									0.00		
15	11/25/77	7.85		12067	8086	32682	30655	20755	27550	18505	6350	2250	2011	1564.11		
16	11/26/77	7.85			8519									0.00		
17	11/27/77	7.74		9916	7412									0.00		
18	11/28/77	8.00		10000	7874	24967	30050	20890	20200	18670	5850	2220	1710	1330.00		
19	11/29/77	8.04		10500	8031	25197	31515	21855	24560	19115	6370	2740	2402	1868.22		
20	11/30/77	8.05		10500	7480									0.00		
21	12/01/77	8.05		10500	7354	35668	36280	25130	29290	23080	5850	2050	2434	1893.11	384	
22	12/02/77	8.04		10500	6956									0.00		
23	12/03/77	8.04		10500	6886	34241	34715	24105	28140	22195	6160	1910	2689	2091.44	840	
24	12/04/77	8.04		10500	7779									0.00		
25	12/05/77	8.04		10500	7511	34252	34870	24615	29940	22875	5410	1740	2054	1597.56	360	
26	12/06/77	8.01		10500	7303									0.00		
27	12/07/77	8.01		10500	6920	36111	37575	25680	31080	23960	5900	1720	2265	1761.67		
28	12/08/77	8.01		10500	6775									0.00		
29	12/09/77	8.01		10500	6887	41865	41875	29885	35360	27445	6340	2440	1895	1473.89	720	
30	12/10/77	8.01		10500	6827	37549	45635	32585	39240	30335	6120	2250	2018	1559.96	402	
31	12/11/77	8.01		10500	6827									0.00		
32	12/12/77	8.01		10500	6827									0.00		
33	12/13/77	8.01		10500	6827									0.00		
34	12/14/77	8.01		10500	6827									0.00		
35	12/15/77	8.01		10500	6827									0.00		
36	12/16/77	8.01		10500	6827									0.00		
37	12/17/77	8.01		10500	6827									0.00		
38	12/18/77	8.01		10500	6827									0.00		
39	12/19/77	8.01		10500	6827									0.00		
40	12/20/77	8.01		10500	6827									0.00		
41	12/21/77	8.01		10500	6827									0.00		
42	12/22/77	8.01		10500	6827									0.00		
43	12/23/77	8.01		10500	6827									0.00		
44	12/24/77	8.01		10500	6827									0.00		
45	12/25/77	8.01		10500	6827									0.00		
46	12/26/77	8.01		10500	6827									0.00		
47	12/27/77	8.01		10500	6827									0.00		
48	12/28/77	8.01		10500	6827									0.00		
49	12/29/77	8.01		10500	6827									0.00		
50	12/30/77	8.01		10500	6827									0.00		
51	12/31/77	8.01		10500	6827									0.00		
52	1/01/78	8.04		15583	10938	55598	18440		43000		5440	2200	2754	2142.00	522	

FINISHER FIRST REP

OBS	DATE	TEMP	GAS	PH	ALK	COOSP	COOML	TS	TVS	SS	VSS	DS	VLS	ATNO	ASII	VA
1	11-11-77	7.75			9717	6930		23840	15665	19440	14465	4610	1200		500	
2	11-11-77	7.77				6245									500	
3	11-11-77	7.77				8199									500	
4	11-11-77	7.64			11500	10532	33015	28490	19280	23500	16340	8040	2940	2255	1753	500
5	11-11-77	7.70			10117	10532	35573	30090	19960	24050	17180	6860	2780	2722	2117	500
6	11-11-77	7.70			10117	10532	38281	31560	21075	25820	18565	6660	2510	2672	2072	500
7	11-11-77	7.70			10117	10532	46609	39065	26556	31150	22026	8490	3730	2722	2117	500
8	11-11-77	7.70			10117	10532	52174	41600	28965	31810	23855	9630	5110	3102	2412	500
9	11-11-77	7.70			10117	10532	54492	48880	33185	42080	29895	8830	3290	2902	2257	500
10	11-11-77	7.70			10117	10532	46470	55745	40170	44430	37750	6400	2420	2853	2210	500
11	11-11-77	7.70			10117	10532	44488	58845	43310	53530	38840	8860	4470	4505	3503	500
12	11-11-77	7.70			10117	10532	62840	59770	41510	53510	37050	9890	4460	3567	2774	4776
13	11-11-77	7.70			10117	10532	65370	53800	37135	45440	33355	9360	3780	3599	2799	4296
14	11-11-77	7.70			10117	10532	75394	63070	46390	50380	42900	8070	3490	3398	2642	1520
15	11-11-77	7.70			10117	10532	64550	61090	44775	55000	41435	7750	3340	3183	2475	760
16	11-11-77	7.70			10117	10532	85450	73560	53420	65250	49350	9440	4070	3662	2448	500
17	11-11-77	7.70			10117	10532	79766	74990		65240		9750	4630	3699	2620	7120
18	11-11-77	7.70			10117	10532	83922	67270	48505	59200	43375	10470	5130	3865	2710	10492
19	11-11-77	7.70			10117	10532	93701	80465	58385	72600	53945	10280	4440	3693	2872	8568
20	11-11-77	7.70			10117	10532	71875	75400	54030	62380	49960	9630	4070	3604	2803	6920
21	11-11-77	7.70			10117	10532	123256	71200	51435	69710	46595	9830	4800	3898	3031	5760
22	11-11-77	7.70			10117	10532	86614	88980	60125	81970	55115	9410	5010	3767	2929	1968
23	11-11-77	7.70			10117	10532	78294	73160	55325	70170	49615	10730	5710	3574	2770	9840
24	11-11-77	7.70			10117	10532	94902	84390	62410	74730	60220	5640	2190			2160
25	11-11-77	7.70			10117	10532	117374	91350		82040		9310	4610	4203	3260	7880

FINISHER FIRST REP

ORS	DATE	TEMP	GAS	PH	ALK	CODSP	CODML	TS	TVS	SS	VSS	OS	VOS	AFRUX	LOTT	VA
56	56	34.0	1108	7.50	22983	40986	100589	111665	63830	88790	76740	12500	7090		0.00	
57	57	36.0	1089	7.44	23717	40358									0.00	
58	58	37.0	1048	7.78	25633	42805	101946	103535	69600	99710	62810	11480	679	4741	5687.40	1060
59	59	37.0	853	7.77	3150	43350								6203	3269.00	
60	60	36.0	742	7.77	4450	44575								6106	3195.11	
61	61	36.0	742	7.77	4467	43320	110980	106590	73425	109090	67395	11120	6730	6446	3450.56	8660
62	62	36.0	848	7.77	3067	43730								6436	3450.22	
63	63	36.0	857	7.41	27117	39897	115385	107705	77265	109040	73725	7380	5541	6589	3587.00	2520
64	64	692	692	7.60	40633	37836	133977	169200	132090	174260	128440	7580	5650	4740	3724.00	6520

FINISHER SECOND REP

DBS	DATE	TEMP	GAS	PH	ALK	CODSP	CODHL	TS	TVS	SS	VSS	DS	VDS	APHLN	AWIT	VA
086	0808	0000	1804												0.00	
085	0809	0000	588	7.50	14500	11896	43866	58205	38320	53070	36620	6140	1700	1809	1407.89	1000
084	0810	0000	655	7.60	14942	12768									0.00	
083	0811	0000	600	7.80	13898	13158	48872	52315	34935	45480	32565	6140	2370	2342	1821.56	288
082	0812	0000	931												0.00	
081	0813	0000	1174	7.56	15536										0.00	
080	0814	0000	1111												0.00	
079	0815	0000	1111												0.00	
078	0816	0000	1111												0.00	
077	0817	0000	1111												0.00	
076	0818	0000	1111												0.00	
075	0819	0000	1111												0.00	
074	0820	0000	1111												0.00	
073	0821	0000	1111												0.00	
072	0822	0000	1111												0.00	
071	0823	0000	1111												0.00	
070	0824	0000	1111												0.00	
069	0825	0000	1111												0.00	
068	0826	0000	1111												0.00	
067	0827	0000	1111												0.00	
066	0828	0000	1111												0.00	
065	0829	0000	1111												0.00	
064	0830	0000	1111												0.00	
063	0831	0000	1111												0.00	
062	0832	0000	1111												0.00	
061	0833	0000	1111												0.00	
060	0834	0000	1111												0.00	
059	0835	0000	1111												0.00	
058	0836	0000	1111												0.00	
057	0837	0000	1111												0.00	
056	0838	0000	1111												0.00	
055	0839	0000	1111												0.00	
054	0840	0000	1111												0.00	
053	0841	0000	1111												0.00	
052	0842	0000	1111												0.00	
051	0843	0000	1111												0.00	
050	0844	0000	1111												0.00	
049	0845	0000	1111												0.00	
048	0846	0000	1111												0.00	
047	0847	0000	1111												0.00	
046	0848	0000	1111												0.00	
045	0849	0000	1111												0.00	
044	0850	0000	1111												0.00	
043	0851	0000	1111												0.00	
042	0852	0000	1111												0.00	
041	0853	0000	1111												0.00	
040	0854	0000	1111												0.00	
039	0855	0000	1111												0.00	
038	0856	0000	1111												0.00	
037	0857	0000	1111												0.00	
036	0858	0000	1111												0.00	
035	0859	0000	1111												0.00	
034	0900	0000	1100	7.77	20180	28517	126996	119610	87995	115540	83795	9280	4200	3806	3009.22	1176
033	0901	0000	1100												0.00	
032	0902	0000	1100												0.00	
031	0903	0000	1100												0.00	
030	0904	0000	1100												0.00	
029	0905	0000	1100												0.00	
028	0906	0000	1100												0.00	
027	0907	0000	1100												0.00	
026	0908	0000	1100												0.00	
025	0909	0000	1100												0.00	
024	0910	0000	1100												0.00	
023	0911	0000	1100												0.00	
022	0912	0000	1100												0.00	
021	0913	0000	1100												0.00	
020	0914	0000	1100												0.00	
019	0915	0000	1100												0.00	
018	0916	0000	1100												0.00	
017	0917	0000	1100												0.00	
016	0918	0000	1100												0.00	
015	0919	0000	1100												0.00	
014	0920	0000	1100												0.00	
013	0921	0000	1100												0.00	
012	0922	0000	1100												0.00	
011	0923	0000	1100												0.00	
010	0924	0000	1100												0.00	
009	0925	0000	1100												0.00	
008	0926	0000	1100												0.00	
007	0927	0000	1100												0.00	
006	0928	0000	1100												0.00	
005	0929	0000	1100												0.00	
004	0930	0000	1100												0.00	
003	0931	0000	1100												0.00	
002	0932	0000	1100												0.00	
001	0933	0000	1100												0.00	
000	0934	0000	1100												0.00	

APPENDIX G

PROCEDURE FOR DETERMINING GAS COMPOSITION
AND GAS COMPOSITION DATA

1. Procedure used to determine gas composition.

Table XXXI presents the column retention times determined during preliminary testing for common components of digester gas. Retention time and mass spectrometer information was used to identify gas components. Figure 44 is a typical chromatogram obtained when analyzing the gas samples from the digesters. The areas under the peaks on chromatograms were calculated by the triangulation method. These values were used to calculate the percentage of each component gas present. Figure 45 shows the components of the characteristic mass spectrometer readout for the samples. The peak numbers shown in Figure 45 correspond to the peaks identified in Figure 44. The background profile of the mass spectrometer readout was subtracted from all other profiles to obtain a corrected mass spectrometer profile used to identify component gases.

2. Table XXXII presents the gas composition data.

TABLE XXXI
RETENTION TIMES OF COMMON DIGESTER GASES
IN GAS CHROMATOGRAPH COLUMN

Gases	Column Retention Time	
	Chart Travel (cm)	Elapse Time (min)
O ₂	0.6-0.7	1.0-1.2
CH ₄	1.1-1.2	1.9-2.0
CO ₂	2.2-2.3	3.8-3.9
H ₂ S	11.5-11.6	19.7-19.9

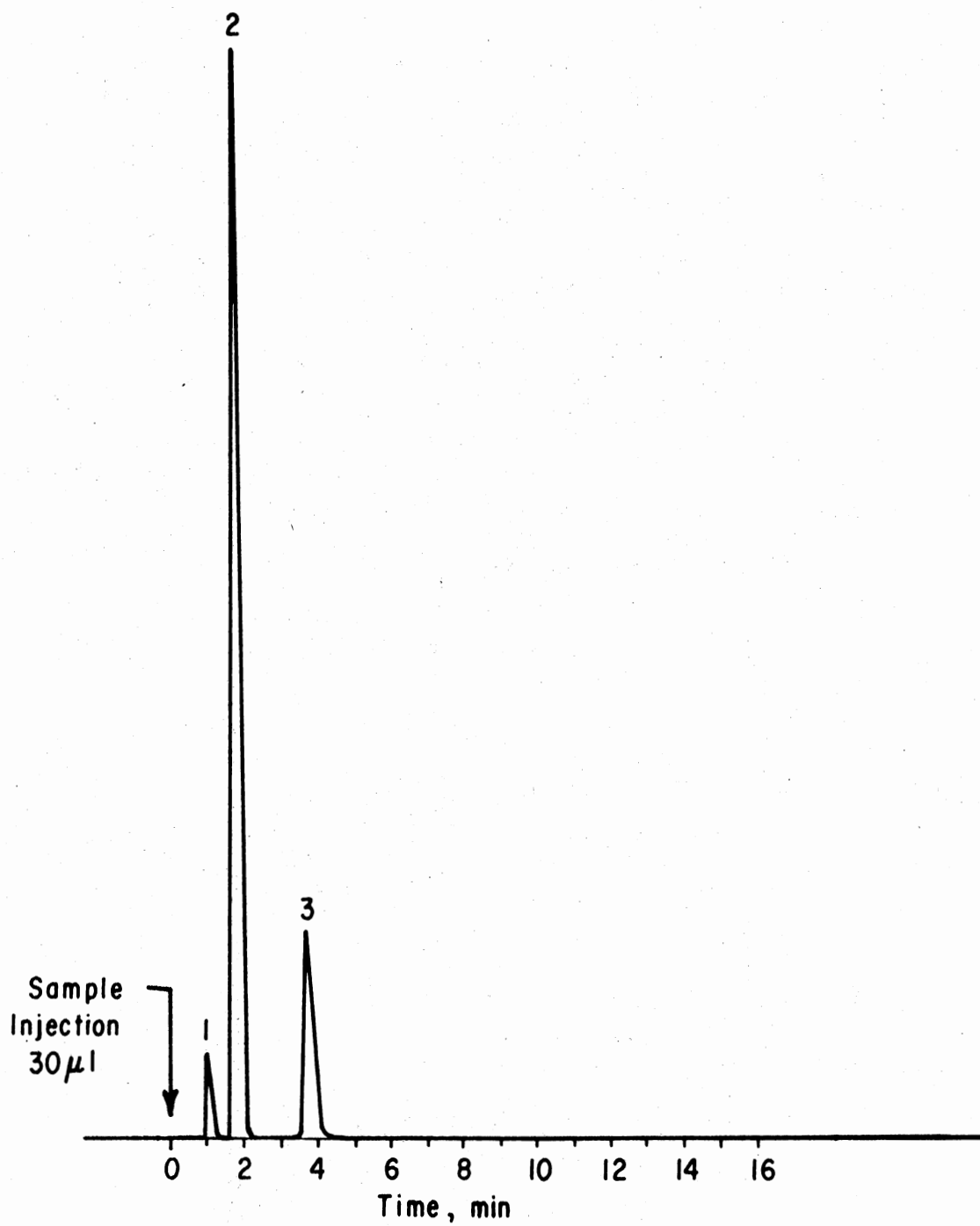


Figure 44. Typical Chromatogram for a Sample of Digester Gas

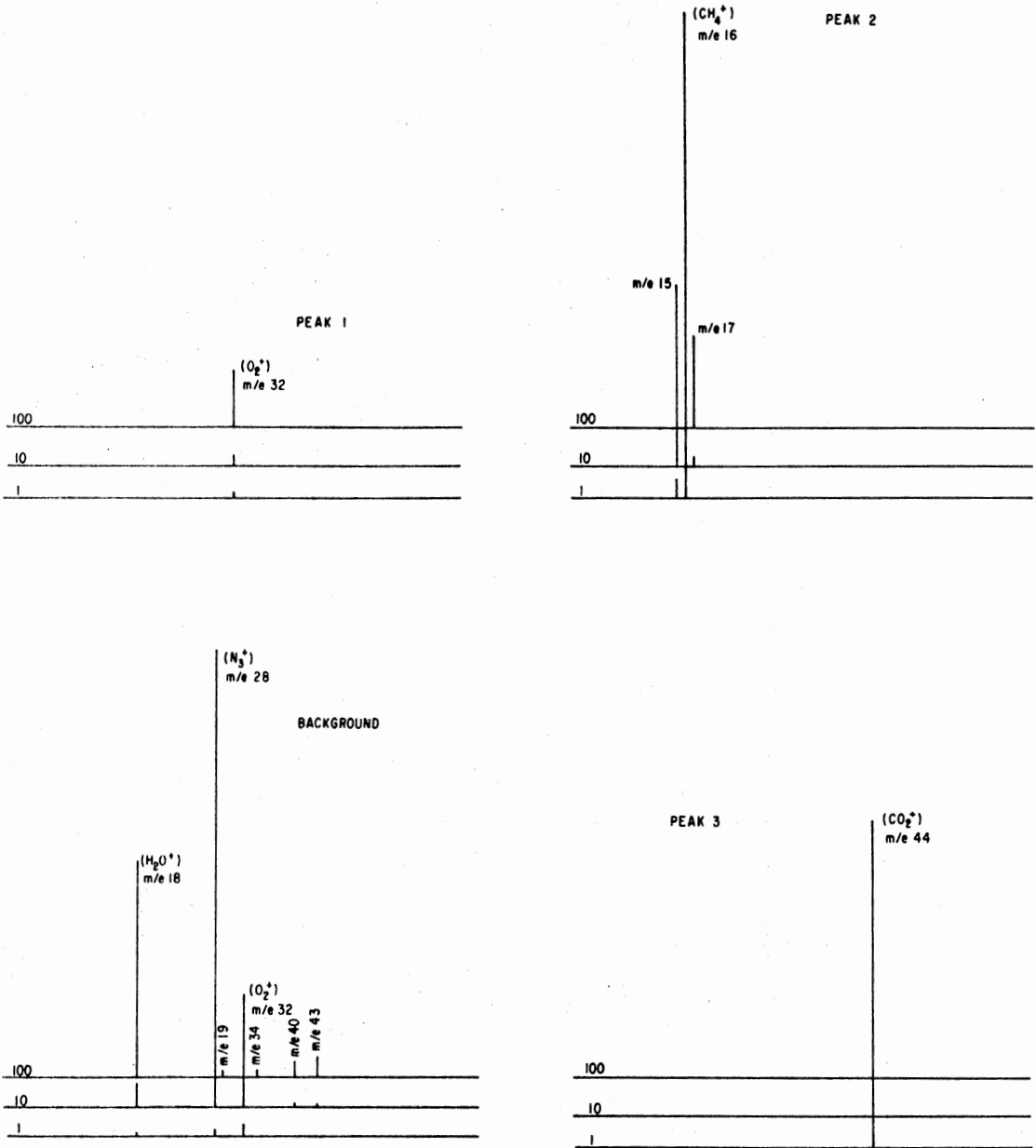


Figure 45. Characteristic Mass Spectrometer Readout for a Sample of Digester Gas

TABLE XXXII
GAS COMPOSITION DATA

Date	1/7			1/5			1/3			1/2		
	O ₂ (%)	CH ₄ (%)	CO ₂ (%)	O ₂ (%)	CH ₄ (%)	CO ₂ (%)	O ₂ (%)	CH ₄ (%)	CO ₂ (%)	O ₂ (%)	CH ₄ (%)	CO ₂ (%)
10/18/76	22.14	62.14	15.73	5.05	75.16	19.79	2.65	65.66	31.70	5.35	62.54	32.11
10/21/76	11.12	72.84	16.03	6.92	73.36	19.72	3.54	67.44	29.00	1.87	61.33	36.80
10/26/76	6.52	77.90	15.57	5.71	73.47	20.82	2.71	65.84	31.45	4.82	64.51	30.66
10/28/76	6.89	79.60	13.51	7.25	73.97	18.78	2.96	65.70	31.33	2.56	61.52	35.92
11/ 2/76	6.34	79.13	14.54	6.04	73.33	20.63	2.35	65.20	32.44	1.73	60.90	37.37
11/ 4/76	7.25	72.86	19.89	6.31	75.89	17.80	3.00	67.31	29.69	2.10	62.70	35.20
11/ 9/76	8.12	77.32	14.56	6.47	75.82	17.71	2.63	69.60	27.77	1.65	59.73	38.62
11/10/76	6.42	75.53	18.05	6.34	75.60	18.06	2.02	68.05	29.92	1.73	62.82	35.45

APPENDIX H

STATISTICAL ANALYSES RELATED TO GAS
COMPOSITION AND LOADING RATE

1.

TABLE XXXIII
ANALYSIS OF VARIANCE OF EFFECT OF DILUTION
OR LOADING RATE ON GAS METHANE CONTENT

Source	df	SS	MS	F
Total	30	1134.7	37.8	
Dilution	3	1047.9	349.3	108.6*
Error	27	86.8	3.2	

*Indicates significance at $\alpha = 0.01$.

2. Duncan's new multiple range test for making comparisons among treatment means (Steel and Torrie, 1960).

a. Determine

$$s_{\bar{x}} = \sqrt{(\text{error mean square})/r}$$

where: $s_{\bar{x}}$ = sample standard deviations

r = number of replications

$$s_{\bar{x}} = \sqrt{\frac{3.2}{2} \left(\frac{1}{7} + \frac{1}{8} \right)}$$

$s_{\bar{x}} = 0.65\%$ with error degrees of freedom = 27

Value of p	2	3	4
SSR	3.9	4.09	4.19
LSR	2.5	2.60	2.70

where: p = number of means for range being tested,

SSR = significant standard ranges, $\alpha = 0.01$,

LSR = least significant ranges ($LSR = s_{\bar{x}} \times SSR$).

b. Rank the means:

<u>1/7</u>	<u>1/5</u>	<u>1/3</u>	<u>1/2</u>
76.2	74.6	66.9	62.0

c. Test the differences:

$$1/7 - 1/2 = 14.2 > 2.7; \text{ significant}$$

$$1/7 - 1/3 = 9.4 > 2.6; \text{ significant}$$

$$1/7 - 1/5 = 1.6 < 2.5; \text{ not significant}$$

$$1/5 - 1/2 = 12.6 > 2.6; \text{ significant}$$

$$1/5 - 1/3 = 7.7 > 2.5; \text{ significant}$$

$$1/3 - 1/2 = 4.8 > 2.5; \text{ significant}$$

3. The effect of dilution or loading rate on gas methane content was described by the following polynomial regression equation.

$$MC = 85.8 - 0.016 \text{ DLR} + 0.0000026 \text{ DLR}^2 \quad (2)$$

where,

MC = methane content, %,

DLR = daily loading rate, mg TS/l of digester.

Correlation coefficient (R^2) = 0.84, and standard error = 2.50%.

Table XXXIV shows analysis of variance of regression.

TABLE XXXIV
ANALYSIS OF VARIANCE OF REGRESSION EQUATION FOR
METHANE CONTENT VERSUS DAILY LOADING RATE

Source	df	SS	MS	F
Total	30	11347333.4	4796396.0	76.5*
Regression	2	9592792.1	62662.2	
Error	28	1754541.3		

*Indicates significance at $\alpha = 0.01$.

APPENDIX I

SAMPLE CALCULATIONS FOR ADJUSTING

DAILY GAS PRODUCTION

Sample Calculations

Given: Feed TS = 61,000 mg TS/l

Gas = 850 ml/l of digester/day

Detention Time (DT) = 20 days

Required: (a) Daily Loading Rate (DLR)

(b) Adjusted Gas Production (AGP)

Solution: (a) Loading Rate

$$\text{DLR} = \frac{\text{TS}}{\text{DT}}$$

$$\text{DLR} = \frac{61,000}{20}$$

DLR = 3050 mg TS/l of digester

(c) Adjusted Gas Production

$$\text{AGP} = \text{Gas} \times \frac{1000}{\text{LR}}$$

$$\text{AGP} = 850 \times \frac{1000}{3050}$$

AGP = 279 ml or 0.28 l/1000 mg TS/l of digester/day.

APPENDIX J

STATISTICAL ANALYSES RELATED TO GAS

PRODUCTION AND LOADING RATE

TABLE XXXV
ANALYSIS OF VARIANCE OF EFFECT OF DILUTION OR LOADING
RATE ON TOTAL GAS PRODUCTION¹

Source	df	SS	MS	F
Total	8	2489	311	
Segment	1	139	139	0.45
Dilution	2	822	411	1.34
Error	5	1528	306	

¹Total gas production values were adjusted to a common base of ml/1000 TS/l of digester for the purpose of comparison. Data for the 1/5 and 1/2 dilutions were not included because of the lack of repetitions.

VITA²

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