

SOME STUDIES OF SIMULATION AND ANALYSIS
OF INDICATOR REACTIONS FOR
CATALYTIC DETERMINATIONS

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LIST OF ABBREVIATIONS

- A = absorbance
- C = catalyst
- C_x = oxidized form of a catalyst
- C_X = total analytical concentration of X
- cat. = catalyzed
- Dr = reduced form of a dye
- Dx = oxidized form of a dye
- ϵ = molar absorptivity of a dye solution
- K_{eq} = equilibrium constant of first step in mechanism
- K_f = formation constant
- k = rate constant
- Ox = oxidizing agent
- Q = a reaction intermediate
- R = reducing agent
- T = transmittance
- uncat. = uncatalyzed
- [X] = concentration of X in moles/liter
- [X]₀ = total or initial concentration of X in moles/liter

CHAPTER I

INTRODUCTION

If a given sample is titrated with a species which has a catalytic effect on an independent reaction, the abrupt increase in rate of this independent reaction after the equivalence point in the titration has been reached may be used as an effective end-point detector. This method of end-point detection is referred to as catalytic end-point indication and the independent reaction is called the indicator reaction (1). This study is part of an effort to characterize these indicator reactions; particular attention has been given to a single selected chemical system.

Use of the digital computer to analyze the differential equations describing an indicator reaction allowed both the estimation of system parameters and the selection of a simplified mechanism which best described the system. Computer analysis consisted of two primary parts: (1) use of least-squares fitting to estimate rate constants assuming a particular simplified mechanism given absorbance versus time data and (2) simulation of absorbance versus time curves given system parameters and a mathematical model describing the system.

A review of existing simulators and modeling programs showed that considerable work had been done, especially in the area of bio-chemical enzyme systems. Methods of expressing and obtaining mathematical models vary, but almost all users of simulating techniques relied on one or

more differential equations to show the dynamic qualities of their systems. Programs were of two general types: (1) those which simulated reactions given system parameters (2,3,4) and (2) those which analyzed data to obtain unknown parameters (5,6).

In the first class, extensive work had been done by Garfinkel who, in one particular simulation (2), used over 80 parameters in the model to simulate the concentration of all the species present in an enzyme system. This type of simulation (i.e.-curves given parameters) was fairly well cut and dried although no reference was found wherein a concentration gradient was introduced as is done in catalytic titrations.

In the second class of papers (determination of constants given absorbance versus time data), the work reported in reference (5) seems to represent the most general and readily adaptable program available. The authors used linear regression analysis to determine the parameters of a set of differential equations. A general outline for the analysis was given along with examples of both simple systems and output of the program. Output consisted of parameters and their standard errors. As in the papers mentioned above, no concentration ramp was included in the model.

A paper by Atkinson (6) was on a somewhat more basic level and dealt with a system quite similar to those used in catalytic titrations. He presented a straight forward outline of the elucidation of rate constants using a non-linear least squares method. In addition, some discussion of flow rates and statistical analysis was given.

A review of existing computer programs for the study of chemical systems, especially bio-chemical kinetics, has been prepared by Garfinkel, et al. (7), and includes discussions of theoretical aspects,

applications, and programming languages and methodology. Childs and co-authors (8) have dealt more specifically with analytical applications of computers in their review and list at least ten references to programs dealing with reaction kinetics.

The programs which have been developed from this present study are original programs, based upon the same fundamental principals as those mentioned above. The advantages of this approach, that is development of original programs for specific problems as opposed to using an already developed "canned" program, lie chiefly in being better able to utilize computer time and storage space by omitting much of the programming necessary to make a program completely general. Thus, the work was not undertaken to offer a cure-all for all kinetic and mechanistic studies, but to develop a comparatively small and inexpensive set of programs for use only in the area of indicator reactions for catalytic end-point indication.

This study consists of two principle thrusts: (1) the use of a hypothetical chemical system for the development and testing of computer programs and (2) the application of these programs to a real system. The hypothetical system presented are not intended to approach generality, but are specific, totally hypothetical reactions used only for the purpose of developing computer programs and for showing the capabilities of those programs in the analysis of a given system. Chapter III in its entirety consists of the study of these hypothetical systems. Chapter IV, on the other hand, is devoted to showing the utility of the programs in deriving information about a real chemical system.

CHAPTER II

EXPERIMENTAL

Apparatus

Previous work in this lab involving catalytic end-point indication has been carried out using a Beckman DB spectrophotometer and a flow cell utilizing a peristaltic pump (9). However, the need for more reliable data and broader instrument response has prompted the introduction of the use of the Cary 14 spectrophotometer in the study of indicator reactions for catalytic end-point indication.

Using the Cary 14, titrations were done directly into the sample cell, thus eliminating any time lag between the introduction of the catalyst or other reactant and measurement of the resulting absorbance. Mixing of the reactants once in the cell called for a special stirring arrangement in the Cary 14 cell compartment. Such a cell holder has been designed and reported in the literature (10).

The holder, constructed mainly of phenolic resin due to its anti-magnetic properties, features a brass, thermostatable cell compartment and an eight pound block of lead to act as ballast to help cut down vibration effects. The actual stirrer is first wrapped with approximately one hundred turns of fine enameled wire then coated with silicone rubber to both hold the coil in place and to provide additional insurance against vibration. The rate of rotation of the stirrer is monitored by measuring the current output of the coil surrounding the spinning magnet.

with an ordinary ammeter having a 100 micro-amp movement. Calibration of stirring speed versus current was accomplished by connecting the output leads of the stirrer to an event counter then recording the number of "events" for a given amount of time. Details of construction and performance are given in reference 10.

The constant speed, motor driven buret used in the catalytic titrations is also described in the reference mentioned above (10).

Reagents

All reagents used were prepared as outlined by Mottola and Harrison (11) with the exception of solutions of nitrilotriacetic acid (NTA). The free acid form of NTA is not soluble in water to the degree needed to prepare a useful stock solution of $\sim 10^{-2}$ M. The NTA dissolved, however, when an excess of sodium acetate, a weak base, was added. The NTA was standardized potentiometrically by titrating the acetic acid liberated upon the dissolution of the pure NTA in sodium acetate with standard base (0.01 N NaOH).

Procedure

Preparation of Reaction Mixture

One ml of dye solution, periodate solution, and ligand solution (if any) were pipetted into a 10 ml volumetric flask. Five ml of buffer were then added and the mixture diluted to 10 ml with distilled water.

Obtaining Titration Curves

Three ml of the reaction mixture were pipetted into a one cm spectrophotometer cell which was then placed into the special cell holder

in the Cary 14. The motor driven buret containing titrant was then moved into position above the cell compartment with the tip of the buret just below liquid level in the cell. Addition of catalyst was initiated by manually turning on the power to the motor driven buret. The time at which catalyst actually reached the solution in the cell, that is, $t=0$, was determined in the following manner. The amount of time required for the catalyst solution in the syringe to travel from a given index mark to the tip of the syringe was determined in separate experiments. After turning on the buret motor, a mark was placed on the chart paper after the delay time mentioned above had elapsed.

Standardization of NTA

The amount of NTA necessary to give the desired concentration was dissolved in a sodium acetate solution containing at least an equimolar amount of sodium acetate. It was found that a 50-100 per cent excess acetate gave good results and fairly fast dissolution of the NTA. Twenty-five ml of the resulting solution was pipetted into a beaker and diluted with another 25 ml of distilled water. The solution was then titrated with standard 0.01 M sodium hydroxide while recording the pH as a function of volume. The molarity of the NTA was calculated, realizing that at the observed pH of the original NTA solution ($\text{pH} = 4.7$), two moles of acetic acid were released for each mole of NTA present.

CHAPTER III

COMPUTER PROGRAMS

Simulation Program

The original plans for this study called for the use of CSMP, a Continuous System Modeling Program available from IBM. Initial efforts at using this language proved awkward, due primarily to fairly strict format limitations as to plot dimensions, data input and output, and sub-program structure. Due to these problems, in addition to debugging problems, CSMP was dropped and a FORTRAN IV program was written to do the simulation. For the particular application being studied here, FORTRAN IV offered several advantages over the more general CSMP program, namely: (1) greater output flexibility in both plots and numerical values, (2) execution of FORTRAN IV on the WATFIV terminal was about 60-70 per cent less expensive than the same job done with CSMP, (3) the programmer could know exactly what was going on in the execution of his program since he wrote the coding himself, and (4) FORTRAN IV or some other FORTRAN dialect is available on virtually every compiler whereas CSMP is usually limited to large computer installations.

Development of Simulation Program

The heart of any simulating program is the integration of the differential equations describing the system. The method used in the present study was trapezoidal integration. When compared to plots obtained

using Runge-Kutta methods (12), the trapezoidal method gave the same results for a hypothetical system similar to the one which was chosen for study. The recursion relation for trapezoidal integration is as follows. (13):

$$\text{Predictor: } Y_{t + \Delta t}^P = Y_t + \Delta t \cdot X_t$$

$$\text{Estimator: } Y_{t + \Delta t} = Y_t + \frac{\Delta t}{2} (X_t + X_{t + \Delta t})$$

$$\text{where: } Y = f(t) \text{ and } X_t = \frac{dY}{dt} = f'(t)$$

A check of the integration technique is given in Appendix A.

A block diagram flow chart of the simulation program along with a complete print-out of the source program including definition of all FORTRAN variable names is given in Appendix B.

Application of Simulation Program to a Hypothetical System

It was felt that the best way to gain an insight into simulation applications was to use the program on a simplified hypothetical system before the study of a real experimental system. This also presented an opportunity to demonstrate the utility of the simulation program in predicting the shape of a titration curve as a function of various parameters. The following topics will be discussed in this section: (1) study of the pre-equilibrium and steady-state conditions without the presence of a complexing agent in the system, (2) study of several possibilities of three-body collisions in both the steady-state and pre-equilibrium conditions, and (3) study of steady-state and pre-equilibrium conditions in the presence of both inhibitory and rate increasing ligands.

The generalized equation of the reaction to be studied is the following:



where:

Dr = reduced form of a dye,

Ox = oxidizing agent,

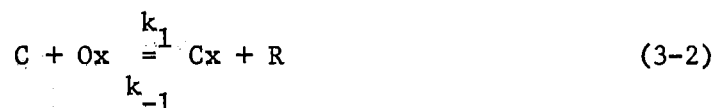
Dx = oxidized form of dye,

R = reducing agent, and

C = catalyst.

Pre-equilibrium Condition--No Complexing Agent

In the pre-equilibrium approach, the catalyzed reaction is viewed as proceeding in the following manner:



where, now, Cx = oxidized form of the catalyst and:

$$K_{\text{eq}} = \frac{[\text{Cx}]_{\text{eq}} [\text{R}]_{\text{eq}}}{[\text{C}]_{\text{eq}} [\text{Ox}]_{\text{eq}}} \quad (3-4)$$

If an equilibrium condition is assumed to exist in the first and faster step (Equation 3-2), then the second step (Equation 3-3) will be rate determining and the rate will be given by:

$$\text{rate} = -k_2[\text{Cx}][\text{Dr}] \quad (3-5)$$

Using Equation 3-2 and the stoichiometry of the system, we may express the equilibrium concentrations of the various species as functions of their initial concentrations and the instantaneous concentration of the "activated" catalyst, Cx. That is:

$$[\text{Ox}]_{\text{eq}} = [\text{Ox}]_0 - [\text{Cx}] \quad (3-6)$$

$$[\text{C}]_{\text{eq}} = [\text{C}]_0 - [\text{Cx}] \quad (3-7)$$

$$[\text{R}]_{\text{eq}} = [\text{Cx}] \quad (3-8)$$

We can then use these expressions along with Equation 3-4 to give:

$$[\text{Cx}] = \frac{([\text{C}]_0 + [\text{Ox}]_0) \pm \sqrt{([\text{C}]_0 - [\text{Ox}]_0)^2 + (4[\text{C}]_0[\text{Ox}]_0/K_{\text{eq}})}}{2(1 - 1/K_{\text{eq}})} \quad (3-9)$$

Stoichiometry requires acceptance of the positive root and substitution into Equation 3-5 gives the final form of the catalyzed rate:

$$\text{rate} = \frac{-k_2[\text{Dr}] \{ ([\text{C}]_0 + [\text{Ox}]_0) + \sqrt{([\text{C}]_0 - [\text{Ox}]_0)^2 + (4[\text{C}]_0[\text{Ox}]_0/K_{\text{eq}})} \}}{2(1 - 1/K_{\text{eq}})} \quad (3-10)$$

It can be seen that if K_{eq} is large, $1/K_{\text{eq}}$ approaches zero and Equation 3-9 reduces to:

$$[\text{Cx}] = [\text{C}]_0 \quad (3-11)$$

which leads to the simpler rate expression:

$$\text{rate} = -k_2[\text{Dr}][\text{C}]_o \quad (3-12)$$

For the special case when $K_{eq} = 1$, no second degree terms appear and the "activated" catalyst concentration is given by:

$$[\text{Cx}] = \frac{[\text{C}]_o [\text{Ox}]_o}{[\text{C}]_o + [\text{Ox}]_o} \quad (3-13)$$

The validity of the assumption leading to Equation 3-11 was verified using computer simulation. Curves were generated using Equation 3-10 as the model letting K_{eq} range from 10^8 to 10.0. No difference was observed in any of these curves.

In addition, a simulation using Equation 3-12 was identical to a curve generated from Equation 3-13 wherein there is no ambiguity in choice of root. This observation further verifies that for all K_{eq} greater than or equal to 1, the assumptions leading to Equation 3-11 are indeed valid.

Steady-State Condition--No Complex Added

In the steady-state approximation, we again look at Equations 3-1, 3-2, and 3-3. Instead of allowing an equilibrium condition to be established, however, we assume that the "activated" catalyst is consumed as rapidly as it is formed, that is:

$$\frac{d[\text{Cx}]}{dt} = 0 = k_1[\text{Ox}][\text{C}] - k_{-1}[\text{Cx}][\text{R}] - k_2[\text{Cx}][\text{Dr}] \quad (3-14)$$

which leads to:

$$[\text{Cx}] = \frac{k_1[\text{Cx}][\text{C}]}{k_{-1}[\text{R}] + k_2[\text{Dr}]} \quad (3-15)$$

Equation 3-2 is then rate determining and:

$$\text{rate} = k_1[\text{Ox}][\text{C}] - k_{-1}[\text{Cx}][\text{R}] \quad (3-16)$$

Substitution of Equation 3-15 into Equation 3-16 gives:

$$\text{rate} = \frac{-k_1 k_2 [\text{Dr}][\text{Ox}][\text{C}]}{k_{-1}[\text{R}] + k_2[\text{Dr}]} \quad (3-17)$$

Once again, stoichiometry leads to:

$$[\text{Dr}] = [\text{Dr}]_0 - ([\text{Ox}]_0 - [\text{Ox}]) \quad (3-18)$$

$$[\text{R}] = [\text{Dr}]_0 - [\text{Dr}] \quad (3-19)$$

$$[\text{Ox}] = [\text{Dr}] - [\text{Dr}]_0 + [\text{Ox}]_0 \quad (3-20)$$

Substitution into Equation 3-17 yields the final, steady-state rate expression:

$$\text{rate} = \frac{-k_1 k_2 [\text{Dr}] ([\text{Dr}] - [\text{Dr}]_0 + [\text{Ox}]_0) [\text{C}]_0}{k_{-1} ([\text{Dr}]_0 - [\text{Dr}]) + k_2 [\text{Dr}]} \quad (3-21)$$

If k_2 is much greater than k_{-1} , this expression simplifies to:

$$\text{rate} = -k_1 ([\text{Dr}] - [\text{Dr}]_0 + [\text{Ox}]_0) [\text{C}]_0 \quad (3-22)$$

Computer simulation showed that the results of using Equations 3-21 and 3-22 are identical for given values of k_1 , the rate constant for the forward and rate determining reaction. It appears from these comparisons that the expression given in Equation 3-22 is a valid model for the steady state approximation under the specified conditions.

Consideration of a Three-Body Collision in the Mechanism of Reaction

The previous discussions concerned only two-body collisions in the mechanism of reaction. If three-body collisions are considered, several possible combinations occur. The most significant possibilities are discussed.

References are made to the generalized equations:



$$K_{eq} = [Cx]^a [R]^b / [C]^a [Ox]^b \quad (3-25)$$

The procedure followed in all of the following derivations is the same as that used in the previous sections, therefore, only important results will be presented in this discussion. Complete derivations may be found in Appendix C.

Pre-equilibrium Condition-- a = 2, b = 1

In this situation, the expression for the activated catalyst concentration is a cubic equation which requires numerical solution. Using such a method, the concentration of the activated catalyst, $[Cx]$, was found to be exactly the same as the initial catalyst concentration, $[C]_0$. This is the same result obtained when assuming a two-body collision. This means that only the stoichiometry of the second reaction (Equation 3-24) affects the rate expression for the reaction. That is, if $c = 2$:

$$\text{cat. rate} = -k_2 [Cx]^2 [Dr] \quad (26)$$

and, if $c = 1$:

$$\text{cat. rate} = -k_2[\text{Cx}][\text{Dr}], \quad (3-27)$$

the same result obtained when assuming 1:1 stoichiometry for the first reaction (Equation 3-23).

Pre-equilibrium Condition-- $a = 1, b = 2$

As was the case above, a cubic equation arises giving again the same results as the 1:1 stoichiometry, $[\text{Cx}] = [\text{C}]_0$. The stoichiometry of Equation 3-24 would affect the rate in the same way as outlined above.

Steady-State Condition: $a = 2, b = 1, c = 2, d = 1$

Writing the differential rate equations, assuming no time rate of change of activated catalyst, and proper substitution yields the following expression for the catalyzed rate:

$$\text{cat. rate} = -k_2[\text{Cx}][\text{Dr}] \quad (3-28)$$

Solution of a quadratic equation in $[\text{Cx}]$ and substitution of stoichiometric equalities finally gives:

$$[\text{Cx}] = \frac{-k_2[\text{Dr}] + \sqrt{(k_2[\text{Dr}])^2 + 4k_1k_{-1}[\text{R}][\text{Ox}][\text{C}]^2}}{2k_{-1}[\text{R}]} \quad (3-29)$$

where:

$$\begin{aligned} [\text{R}] &= [\text{Dr}]_0 - [\text{Dr}] \text{ and} \\ [\text{Ox}] &= [\text{Dr}] - [\text{Dr}]_0 + [\text{Ox}]_0 . \end{aligned}$$

It can be seen that if the second term under the square root is small,

which it usually is due to the magnitude of $[R]$ and $[C]^2$, that the expression goes to zero. This is expected since one of the basic assumptions of the steady-state approximation is that the activated species is used up as soon as it is formed.

Steady-State Condition: $a = 1, b = 2, c = 1, d = 1$

This stoichiometry yields a simpler expression for the rate due to the absence of any second degree terms in the expression giving the activated catalyst concentration, $[Cx]$. The rate equation is:

$$\text{cat. rate} = -2(k_2[Cx][Dr]) \quad (3-30)$$

where:

$$[Cx] = \frac{k_1[Ox]^2[C]}{k_{-1}[R]^2 + k_2[Dr]} \quad (3-31)$$

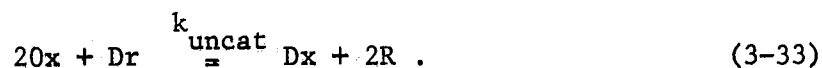
Since k_2 is much greater than k_{-1} , the rate equation can be further simplified to:

$$\text{cat. rate} = -2k_1[Ox]^2[C] \quad (3-32)$$

where:

$$[Ox] = [Ox]_0 - 2[Dr]_0 + 2[Dr]$$

The uncatalyzed reaction in this case is given by:



The uncatalyzed rate is then:

$$\text{uncat. rate} = k_{\text{uncat}} [\text{Ox}]^2 [\text{Dr}] \quad (3-34)$$

3-Body Collision Involving Three Different Species

The reactions considered here are the following:



These are discussed in the light of both the pre-equilibrium and the steady-state conditions.

Pre-equilibrium Condition

The equilibrium constant for the reaction given by Equation 3-35 is:

$$K_{\text{eq}} = [\text{Q}] / [\text{C}][\text{Dr}][\text{Ox}] \quad (3-37)$$

Substitution of stoichiometric equalities for [C], [Dr], and [Ox] into the equilibrium expression gives the following cubic equation:

$$\begin{aligned} & [\text{Q}]^3 - \{[\text{Ox}]_0 + [\text{C}]_0 + [\text{Dr}]_0\} [\text{Q}]^2 + \{[\text{Ox}]_0 ([\text{C}]_0 + [\text{Dr}]_0) + [\text{C}]_0 [\text{Dr}]_0\} \\ & + \frac{1}{K_{\text{eq}}} \} [\text{Q}] - [\text{C}]_0 [\text{Dr}]_0 [\text{Ox}]_0 = 0 \end{aligned} \quad (3-38)$$

Computer analysis of the function reveals the following. As K_{eq} becomes smaller, the curve (i.e., $f(Q)$ vs. Q) "shifts" upward along the ordin-

ate axis until there is no intersection greater than zero. This means, of course, that there will be no positive root found for these cases. Secondly, solution of the cubic equation using a numerical method shows that if K_{eq} is quite large (say, K_{eq} greater than 10^{10}), then $[Q] = [C]_0$. If this is the case, the uncatalyzed reaction remains the same as that given for the two-body collision and the rate of the catalyzed reaction becomes:

$$\text{cat. rate} = -k_2[Q] \quad (3-39)$$

and is therefore independent of the concentration of the species appearing in the expression for the uncatalyzed reaction.

Steady-State Condition

In this case, the rate is given by:

$$\text{cat. rate} = -k_2[Q] \quad (3-40)$$

Making the steady-state approximation ($d[Q]/dt = 0$) and solving for $[Q]$ gives

$$[Q] = \frac{k_1[C][Dr][Ox]}{k_2 + k_{-1}} \quad (3-41)$$

Since k_2 is much greater than k_{-1} , k_{-1} can be neglected to give finally:

$$\text{cat. rate} = -k_1[C][Dr][Ox] \quad (3-42)$$

where:

$$[C] = [C]_0 \text{ and}$$

$$[Ox] = [Ox]_0 - [Dr]_0 + [Dr].$$

The uncatalyzed reaction rate is given by:

$$\text{uncat. rate} = -k_{\text{uncat}} [\text{Ox}][\text{Dr}]$$

Computer Simulation of Curves Assuming 3-Body Collisions

As would be expected due to higher order terms in the rate controlling step, the reactions were much slower than in the case of two-body collisions. These expressions would require constants of much greater magnitude than those used in the two-body problem to approach reality. In fact, using the constants from the two-body problem, the catalyzed reaction was not always faster than the uncatalyzed reaction.

When the steady-state condition was assumed, the curves obtained considering a 3-body collision in the rate determining step were all quite similar to those obtained for the 1:1 stoichiometry. In other words, constants of about the same order of magnitude as were used in the two-body problem gave curves similar to those already reported.

By far the most interesting of the 3-body collisions were those involving the collision of three different species. Simulation of the expression obtained assuming the pre-equilibrium model resulted in a curve quite similar to those obtained when assuming the steady-state mechanism in the two-body problem. Similarly, simulation of the 3-body curve obtained using the steady-state condition produced a curve almost identical to that which resulted when considering the pre-equilibrium condition in the two-body problem. By adjusting parameters, the curve obtained using Equation 3-42 can be superimposed upon the curve resulting from the pre-equilibrium condition (see Equation 3-12).

Addition of Rate Modifying Complexing Agents

The sections preceding this one have dealt mainly with the study of a hypothetical reaction of a dye and an oxidizing agent, catalyzed by some metal ion. This reaction was assumed to take place (in aqueous media) with only the dye, oxidizing agent, catalyst, and their intermediate and final products present. At this point, consideration is given to complicating the system with the addition of a complexing agent and is presented in two main parts: (1) addition of a ligand which ties up catalyst (or catalytic species) thus inhibiting the progress of the reaction and (2) addition of a ligand which, in addition to tying up the catalyst, forms a new species which itself exerts a rate increasing effect upon the reaction. For the sake of eliminating redundancy, the "normal catalytic cycle" is considered to occur by pre-equilibrium kinetics and is assumed to be a two-body collision (see page 9, this work).

Addition of Inhibitor: Derivation of Expressions

Consider the addition to the system of a ligand, L, which forms a complex with the catalyst, C, according to the following reaction:



with

$$K_f = \frac{[CL]}{[C][L]}$$

It follows, then, that if the initial catalyst concentration is represented by $[C]_0$, the amount of catalyst, C, available for participation in the dye reaction is given by:

$$[C] \rightleftharpoons [C]_0 - [CL] \quad (3-46)$$

But, from the equilibrium expression, we have:

$$[CL] = K_f [C][L] \quad (3-47)$$

Substituting into Equation 3-46 and solving for [C] gives:

$$[C] = \frac{[C]_o}{1 + K_f [L]} \quad (3-48)$$

Further, we know that the ligand concentration, [L], can be expressed in terms of the total analytical ligand concentration, C_L , in the following manner similar to that used by Freiser and Fernando (14):

$$\alpha_L = \frac{[L]}{C_L} = \frac{1/K_f}{[C] + 1/K_f} \quad (3-49)$$

Solving for [L] gives:

$$[L] = \frac{C_L/K_f}{[C] + 1/K_f} \quad (3-50)$$

Substitution of Equation 3-50 into Equation 3-48 finally gives:

$$[C] = \frac{[C]_o}{1 + \frac{C_L}{[C] + 1/K_f}} \quad (3-51)$$

At this point, for simplification of the symbolism, we let:

$$X = [C], \quad C = [C]_o, \quad K = 1/K_f, \quad \text{and} \quad L = C_L$$

Equation 3-51 now becomes:

$$X = \frac{C}{1 + \frac{L}{X + K}} \quad (3-52)$$

Proceeding with the solution for X, we have:

$$X + \frac{XL}{X + K} = C$$

$$X^2 + KX + XL = CX + CK$$

$$X^2 + (K + L - C)X - CK = 0$$

Applying the quadratic formula, we arrive at:

$$X = \frac{-(K + L - C) \pm \sqrt{(K + L - C)^2 + 4CK}}{2} \quad (3-53)$$

or, in terms of the original symbols:

$$[C] = \frac{1}{2} \left[-(1/K_f + C_L - [C]_o) \pm \sqrt{(1/K_f + C_L - [C]_o)^2 + \frac{4[C]_o}{K_f}} \right] \quad (3-54)$$

Analysis of this expression reveals that if K_f is large, $1/K_f$ approaches zero and we may represent Equation 3-54 as:

$$[C] = \frac{1}{2} \left[-(C_L - [C]_o) \pm \sqrt{(C_L - [C]_o)^2} \right] \quad \text{or:} \quad (3-55)$$

$$[C] = \frac{1}{2} \left[([C]_o - C_L) \pm (C_L - [C]_o) \right]$$

Consideration of experimental realities leads to three possible cases:

(1) $[C]_o = C_L$, (2) $[C]_o < C_L$, or (3) $[C]_o > C_L$. Looking first at case

1, we see that if $[C]_o = C_L$, then:

$$[C] = \frac{1}{2}(0 \pm 0) = 0 \quad (5-56)$$

and there is no ambiguity in choice of positive or negative root. If $[C]_o < C_L$, however, we must choose the positive root, since the other choice leads to:

$$[C] = \frac{1}{2} ([C]_o - C_L - C_L + [C]_o) \quad \text{or:} \quad (5-57)$$

$$[C] = [C]_o - C_L$$

This, of course, is an impossibility in this case since $[C]$ cannot be less than zero. This gives then, with choice of the positive root:

$$[C] = \frac{1}{2} ([C]_o - C_L + C_L - [C]_o) = 0 \quad (5-58)$$

In the third case ($[C]_o > C_L$) either Equation 3-57 or 3-58 would fit theoretically. Equation 3-58 must be ruled out, however, since it is impossible for a given amount of ligand to tie up more than an equivalent amount of catalyst according to Equation 3-44. We then have from Equation 3-57 that:

$$[C] = [C]_o - C_L$$

These same results can be obtained numerically in the following manner: We first re-write Equation 3-55 taking only the positive root:

$$[C] = \frac{1}{2} \left[([C]_o - C_L) + \sqrt{(C_L - [C]_o)^2} \right] \quad \text{and say:} \quad (5-59)$$

$$\text{Term 1} = [C]_o - C_L \quad \text{and}$$

$$\text{Term 2} = \sqrt{(C_L - [C]_o)^2}$$

It can be seen that Term 2 will always be positive and numerically equal to the absolute value of Term 1. When $[C]_o < C_L$, Term 1 will be less than zero which leads to:

$$[C] = \frac{1}{2} [-\text{Term 1} + \text{Term 2}] = 0 \quad (3-60)$$

On the other hand, if $[C]_o > C_L$, Term 1 is positive and:

$$[C] = \frac{1}{2} [\text{Term 1} + \text{Term 2}] \quad (3-61)$$

$$= \frac{1}{2} [2 \cdot \text{Term 1}] = \text{Term 1}$$

$$[C] = [C]_o - C_L$$

This numerical analysis is necessary to accurately apply the expressions developed above to computer simulation of the resulting catalytic titration curves.

Addition of Inhibitor: Computer Analysis

The system was simulated on the computer assuming various total ligand concentrations. Results of this simulation are shown in Figure 1, a composite graph of all the curves simulated from a total analytical concentration of $C_L = 1 \times 10^{-5}$ M (code = 1) to $C_L = 8 \times 10^{-5}$ (code = 8).

It is apparent from this set of curves that the distance from the inflection point to the baseline (represented by D in Figure 1) is a direct function of ligand concentration. Indeed, this fact is the basis

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THIS CHART IS A SUMMARY OF ALL THE CURVES SIMULATED IN THIS RUN 6/26/71

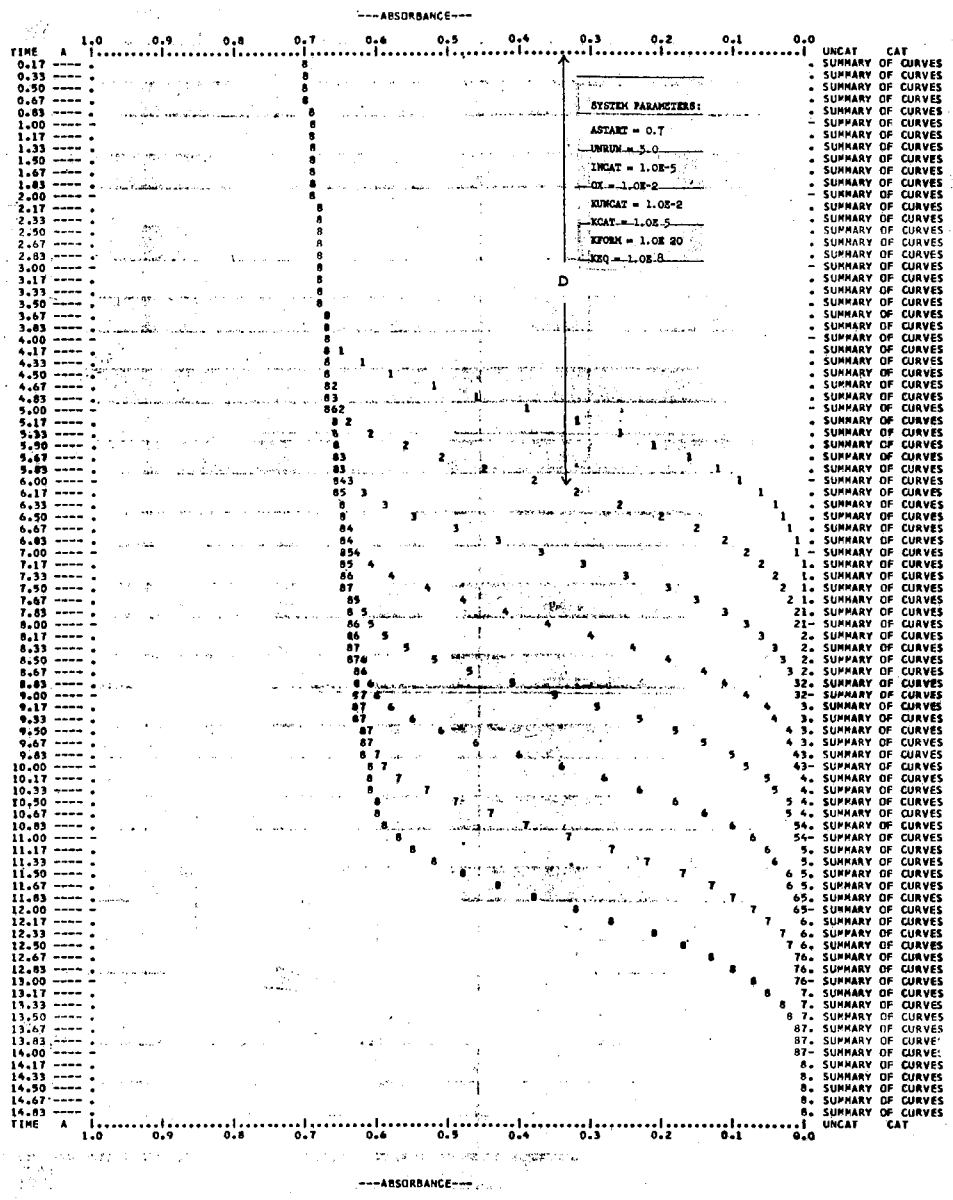


Figure 1. Computer Simulation of Hypothetical System; Effect of Rate Inhibiting Complexing Agent Concentration on Progress of Reaction

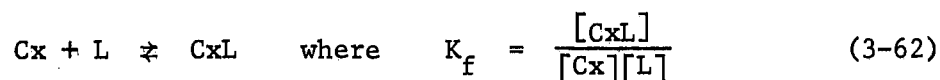
of catalytic end-point determination as discussed by Mottola (1).

Addition of Rate Increasing Ligand

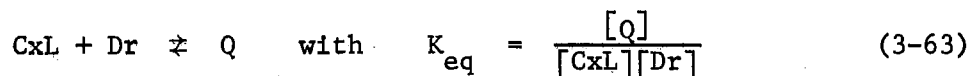
In the hypothetical reaction between a dye and an oxidizing agent, catalyzed by a metal ion, the intermediate species in all approaches is the oxidized form of the catalyst (represented by Cx). If a rate-increasing ligand is introduced, it is assumed that it forms a complex with Cx which in some way results in an increase in the rate of the overall reaction, either by true catalysis or promotion. Catalysis is the speeding up of an already existing reaction, without destruction of the catalytic species. Promotion refers to the speeding up of a reaction in such a way as to destroy the rate-increasing species (15). The differences between these two aspects are covered later. In this section, two possible approaches to rate-increase are discussed: (1) a pre-equilibrium condition and (2) a steady-state condition.

Pre-Equilibrium Condition of Rate-Increase: Derivation of Expressions

Consider the addition of a ligand, L, to a system such as described above, and the formation of the following complex:



One possible route of rate-increase is the following:



where:

P = some products of the decomposition of Q.

Here, we assume that the second step is the slow step and is irreversible. The rate of this reaction is therefore given by:

$$\text{rate}_L = k[Q] \quad (3-65)$$

where:

$\text{rate}_L \equiv$ rate due to the ligand effect. But:

$$[Q] = K_{eq}[C_xL][Dr], \quad \text{then:} \quad (3-66)$$

$$\text{rate}_L = kK_{eq}[C_xL][Dr] \quad (3-67)$$

All quantities in this equation are either known or determinable, except $[C_xL]$. An expression for $[C_xL]$ can be obtained in the following manner: From the mass balance relation for the total catalyst concentration we may write:

$$[C]_o = [C_x] + [C_xL] + [Q] \quad (3-68)$$

Then, solving for $[C_xL]$, we have:

$$[C_xL] = [C]_o - [C_x] - [Q] \quad (3-69)$$

but, $[Q] = K_{eq}[C_xL][Dr]$. This leads to:

$$[C_xL] = [C]_o - [C_x] - K_{eq}[C_xL][Dr] \quad (3-70)$$

or, solving for $[C_xL]$:

$$[C_xL] = \frac{[C]_o - [C_x]}{1 + K_{eq}[Dr]} \quad (3-71)$$

This expression, substituted into Equation 3-67 gives:

$$\text{rate}_L = \frac{kK_{eq}[\text{Dr}](\text{[C]}_o - \text{[Cx]})}{1 + K_{eq}[\text{Dr}]} \quad (3-72)$$

It now becomes necessary to obtain an expression for $[\text{Cx}]$, hereafter called the "uncomplexed catalyst concentration", meaning the concentration of "activated" catalyst available for reaction by the normal catalytic cycle.

Solving Equation 3-70 for $[\text{Cx}]$ gives:

$$[\text{Cx}] = \text{[C]}_o - [\text{CxL}] - K_{eq}[\text{CxL}][\text{Dr}] \quad \text{or:} \quad (3-73)$$

$$[\text{Cx}] = \text{[C]}_o - (1 + K_{eq}[\text{Dr}]) [\text{CxL}]$$

From the ligand mass balance, we have:

$$C_L = [\text{CxL}] + [\text{L}] + [\text{Q}] \quad (3-74)$$

But, from the appropriate equilibrium expressions we know:

$$[\text{L}] = \frac{[\text{CxL}]}{[\text{Cx}]K_f} \quad (3-75)$$

and, as before, $[\text{Q}] = K_{eq}[\text{CxL}][\text{Dr}]$. Substituting these values into Equation 3-74 yields:

$$C_L = [\text{CxL}] + \frac{[\text{CxL}]}{[\text{Cx}]K_f} + K_{eq}[\text{CxL}][\text{Dr}] \quad (3-76)$$

Proceeding with the algebra, we obtain:

$$[\text{Cx}]C_L = [\text{Cx}][\text{CxL}] + \frac{[\text{CxL}]}{K_f} + [\text{Cx}]K_{eq}[\text{CxL}][\text{Dr}]$$

$$\begin{aligned}
&= [\text{CxL}] \left\{ [\text{Cx}] + \frac{1}{K_f} + K_{eq} [\text{Dr}] [\text{Cx}] \right\} \\
&= [\text{CxL}] \left\{ \frac{1}{K_f} + (1 + K_{eq} [\text{Dr}]) [\text{Cx}] \right\}
\end{aligned}$$

Finally, solving for $[\text{CxL}]$ yields:

$$[\text{CxL}] = \frac{[\text{Cx}] C_L}{1/K_f + [1 + K_{eq} [\text{Dr}]] [\text{Cx}]} \quad (3-77)$$

Substituting into Equation 3-73, we arrive at:

$$[\text{Cx}] = [\text{C}]_o - \left\{ \frac{(1 + K_{eq} [\text{Dr}]) [\text{Cx}] C_L}{1/K_f + (1 + K_{eq} [\text{Dr}]) [\text{Cx}]} \right\} \quad (3-78)$$

Now, to simplify the algebra, let:

$$X = [\text{Cx}], \quad C = [\text{C}]_o, \quad D = K_{eq} [\text{Dr}], \quad L = C_L, \quad \text{and} \quad K = K_f$$

Equation 3-78 is re-written as:

$$X = C - \frac{(1 + D)XL}{\frac{1}{K} + (1 + D)X} \quad (3-79)$$

Proceeding with the solution:

$$(D + 1)X^2 + \frac{X}{K} = \frac{C}{K} + (D + 1)CX - (D + 1)XL$$

$$(D + 1)X^2 + \frac{X}{K} - (D + 1)CX + (D + 1)LX - \frac{C}{K} = 0$$

$$(D + 1)X^2 + \left[\frac{1}{K} - (D + 1)C + (D + 1)L \right] X - \frac{C}{K} = 0$$

$$(D + 1)X^2 + \left[\frac{1}{K} - (D + 1)(C - L) \right] X - \frac{C}{K} = 0$$

Applying the quadratic formula:

$$X = \frac{-[1/K - (D + 1)(C - L)] + \sqrt{[1/K - (D + 1)(C - L)]^2 + 4(D + 1)C/K}}{-2(D + 1)}$$

or, converting back to the original terms:

$$[Cx] = \frac{1}{2(K_{eq}[Dr] + 1)} \left\{ - \left[\frac{1}{K_f} - (K_{eq}[Dr] + 1)([C]_o - C_L) \right] + \sqrt{\left[\frac{1}{K_f} - (K_{eq}[Dr] + 1)([C]_o - C_L) \right]^2 + \frac{4(K_{eq}[Dr] + 1)[C]_o}{K_f}} \right\} \quad (3-80)$$

It should be noted that all quantities in Equation 3-80 are known with the exception of C_L , the total ligand concentration. Since Equation 3-64 is assumed to be irreversible, C_L is not constant. Let $C_L = L =$ total ligand concentration at time "t". Then:

$$\frac{dL}{dt} = \frac{-d[P]}{dt} = - \left\{ - \frac{d[Q]}{dt} \right\} = \frac{kK_{eq}([C]_o - [Cx])}{1 + K_{eq}[Dr]} \quad (3-81)$$

Or, to an approximation:

$$\Delta L = \frac{kK_{eq}([C]_o - [Cx])}{1 + K_{eq}[Dr]} \cdot \Delta t \quad \text{and:} \quad (3-82)$$

$$C_L(t + \Delta t) = C_L(t) - \Delta L \quad (3-83)$$

This expression, by no means intended to be rigorous, will yield an approximate value of the change in ligand concentration with time which can be used in computer simulation discussed in the following section.

Pre-equilibrium Condition of Rate-Increase: Computer Analysis

Using the expressions developed above to describe the system, it is both interesting and pertinent to study the effect of varying certain

parameters on the behavior of the system.

The procedure for each parameter was the following: choose reasonable values for the parameters not being studied, hold these constant, vary the parameter of interest, and observe the effect on the shapes of the resulting simulated curves. A close study of these curves can lead to valuable conclusions concerning relative magnitude of parameters and possibly give an insight into when or if a given parameter may be assumed to have no effect on the system.

In the present system under study, the following parameters were varied with respect to the remaining parameters:

K_{eq} = equilibrium constant for the formation of the complex, Q
(see Equation 3-63),

K_f = formation constant for the complex, C_xL (see Equation
3-62),

k_p = rate constant for promotion path ($k_p = k$ in Equation 3-64),
and

C_L = the concentration of total ligand in all forms at any time
(see Equation 3-28).

The results of assigning different values to these parameters can be seen in Figures 2 through 8 and are summarized in the following sections.

Each graph in this series contains a legend. However, units have been omitted for sake of simplicity. Following is a list of the FORTRAN representations of the various parameters and a short explanation of the significance of each.

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PRE-EQ MECH--COMPOSITE GRAPH SHOWING EFFECT OF VARYING K_{eq}

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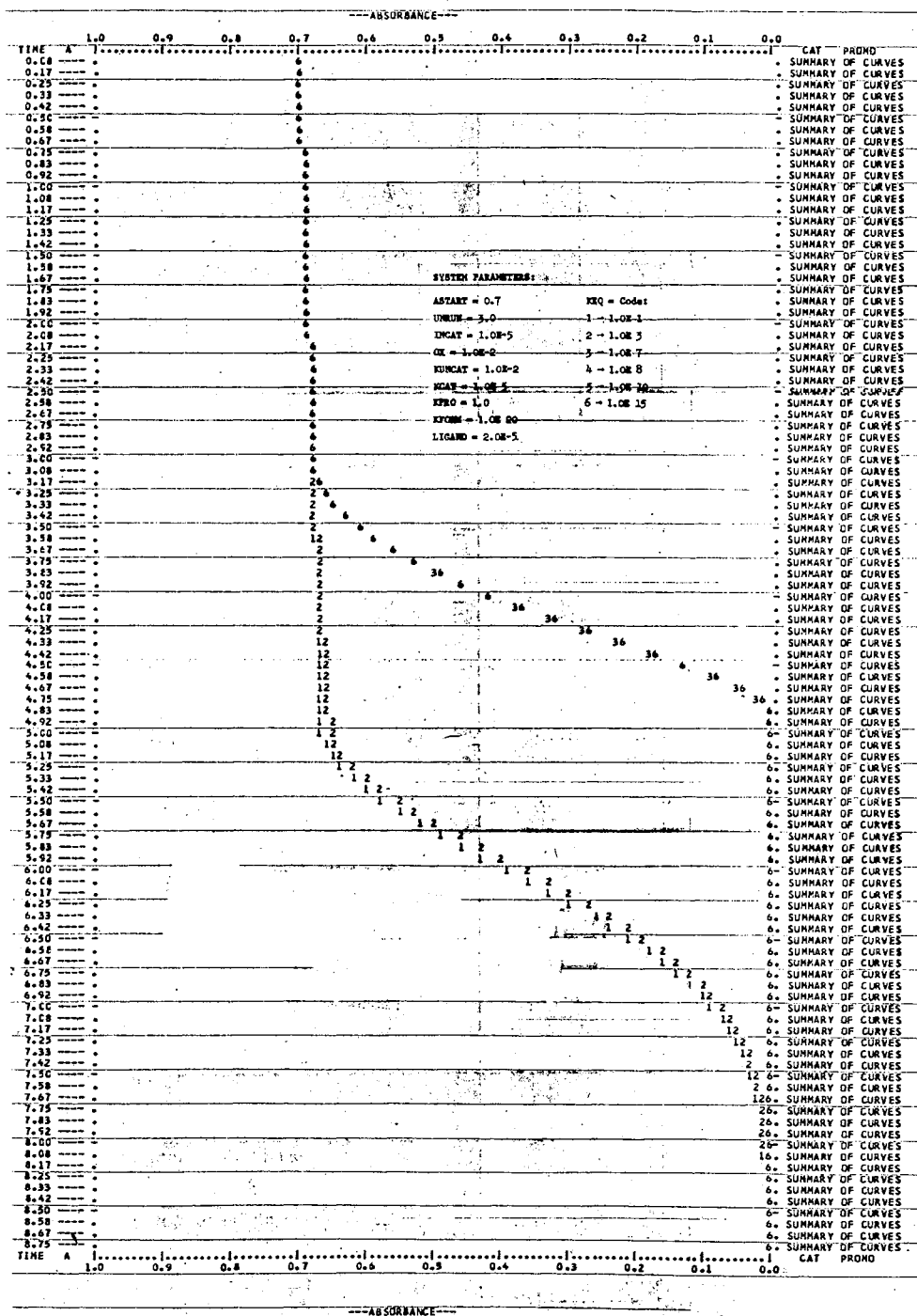


Figure 2. Computer Simulation of Hypothetical System; Addition of Rate-increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of varying K_{eq}

CPM 5000--D.L. SIMPSON

COPY 3 OF 3

PROGRAM--PRE-EQ MECH EFFELT UP VARYING KEQ 10 --> 1.0E 8

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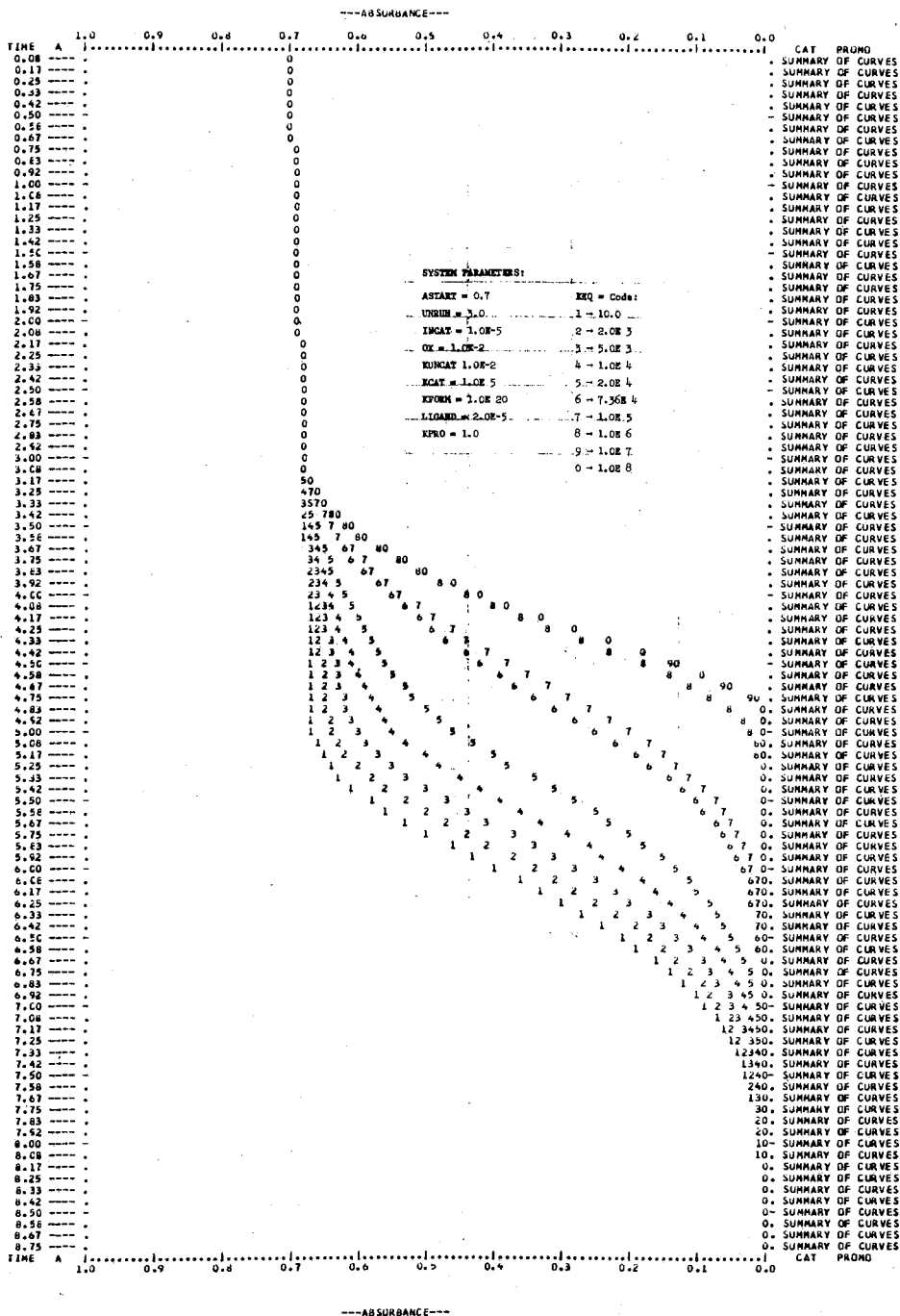


Figure 3. Computer Simulation of Hypothetical System; Addition of Rate-increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of varying K_{eq}

CHEM 5000--B.E. SIMPSON

PRE-EQ MECH--COMPOSITE GRAPH SHOWING EFFECT OF VARYING KFORM 12/22/71

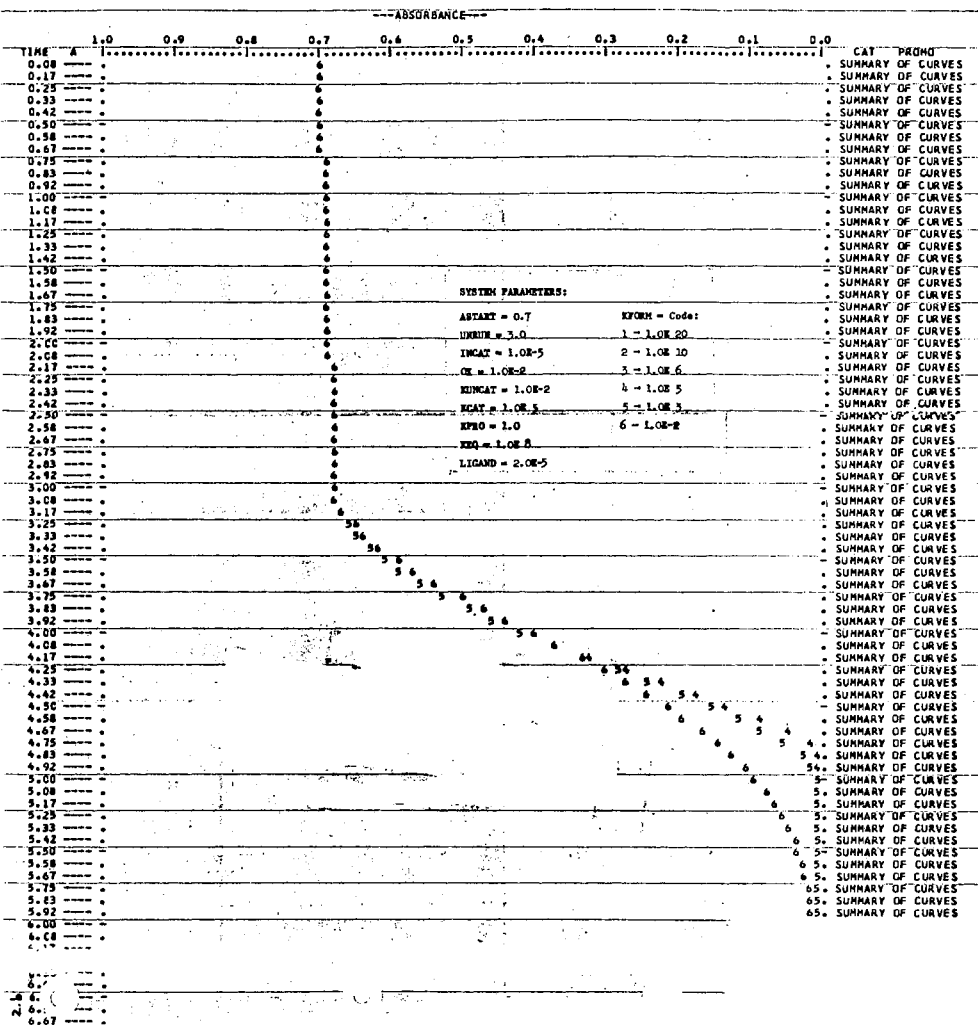


Figure 4. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of varying K_f

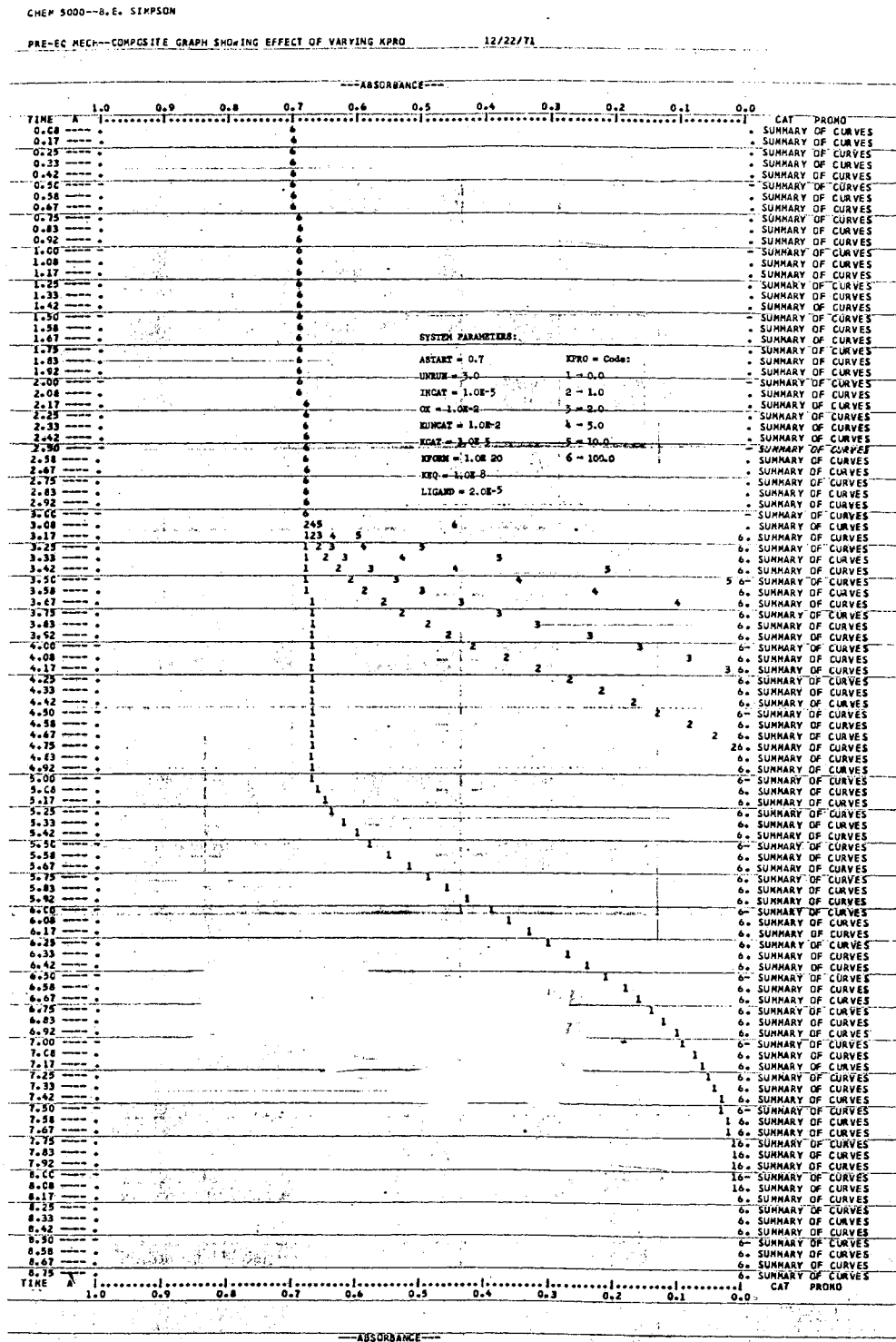


Figure 5. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of varying k_p

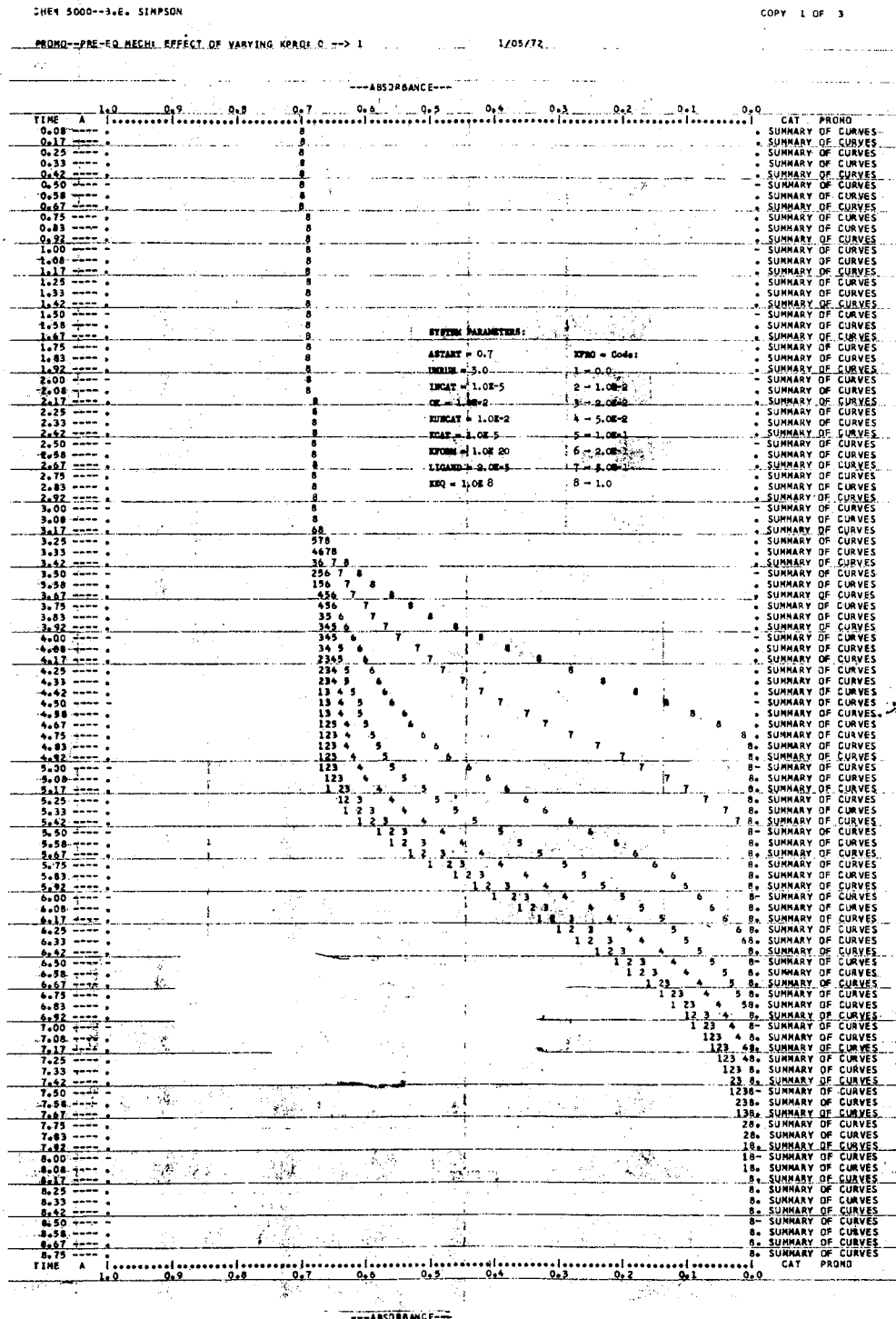


Figure 6. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of varying k_p

CHEM 5000--B.E. SIMPSON

PRE-EQ MECH--COMPOSITE GRAPH SHOWING EFFECT OF VARYING TOTAL INITI LIG 12/22/71

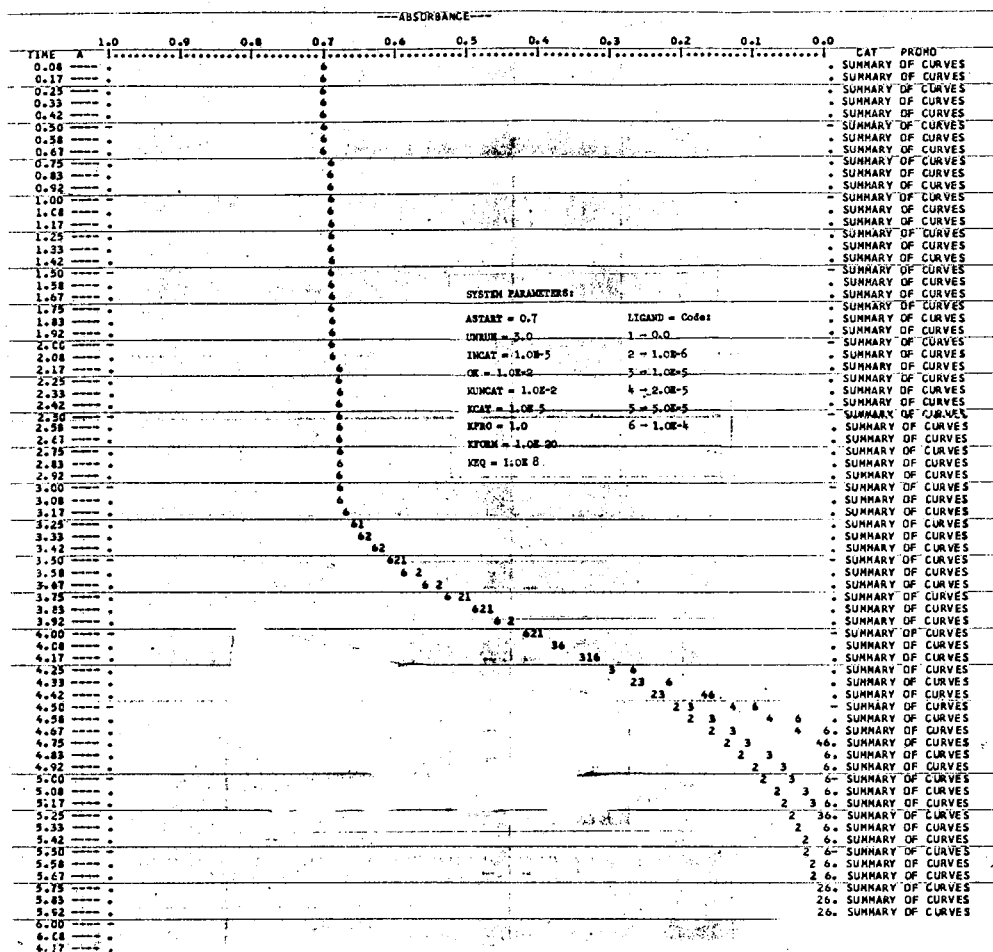


Figure 7. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of Varying Initial Ligand Concentration

CHEM 5000--R.E. SIMPSON

PRCND-PRE-EQ MECH: VARY LLG CONCEN WHEN KPRC=5

12/29/71

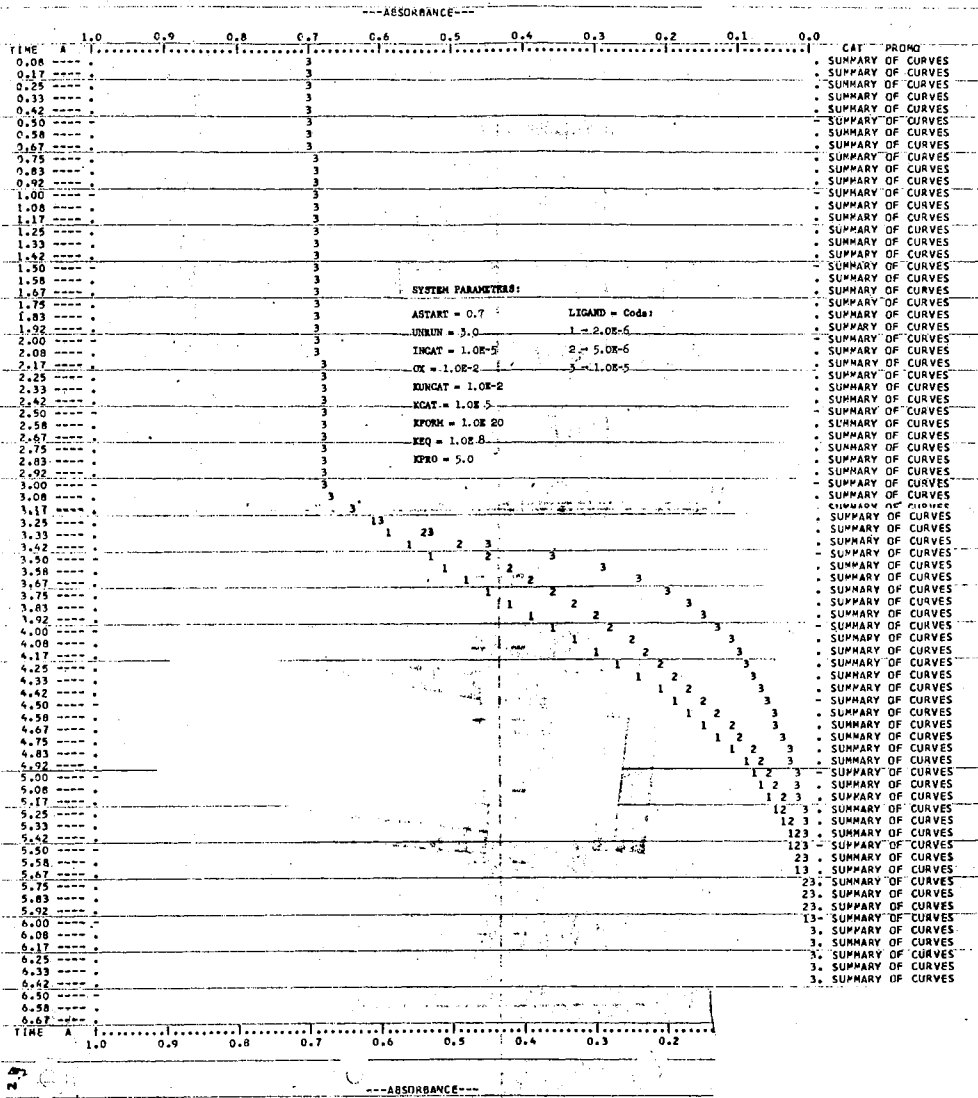


Figure 8. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition. Effect of Varying Initial Ligand Concentration

TABLE I
EXPLANATION OF VARIABLE NAMES AND UNITS OF CONSTANTS

Fortran Rep	Comment	Units
ASTART	Initial absorbance of the system at time = 0	unitless
UNRUN	Number of minutes of uncatalyzed reaction before catalyst is added	minutes
INCAT	Rate of catalyst addition	$M \cdot \text{min}^{-1}$
OX	Concentration of oxidizing agent	M
KUNCAT	Uncatalyzed rate constant	min^{-1}
KCAT	Catalyzed rate constant	$M^{-1} \text{min}^{-1}$
KPRO	Rate constant for ligand effect	min^{-1}
KFORM	Formation constant for the metal-ligand complex, CxL	M^{-1}
KEQ	Equilibrium constant for the formation of complex Q from CxL and dye	M^{-1}
LIGAND	Initial ligand concentration	M

Please note that in the following discussions, "reaction" refers to the portion of the curve after a time equal to UNRUN has elapsed; i.e., it does not refer to the uncatalyzed portion of the curve.

Variation of K_{eq}

A look at Figure 2 shows that codes 4 and 5 have been over-printed with a 6. This indicates that all values of KEQ greater than 10^8 have no effect on the system since $4 \rightarrow 10^8$. This observation is compatible with Equation 3-72. In the term $(1 + K_{eq} [Dr])$, we may neglect the value

1 if $K_{eq}[Dr]$ is large enough. If we accept a rejection criterion of 1%, then $K_{eq}[Dr] > 100$ in order to neglect the value 1. Since $[Dr] \approx 10^{-5}$, we have: $K_{eq} > 10^7$ in order to neglect 1. This agrees quite well with the simulation which shows that, under the assumed conditions, the point where K_{eq} need not be considered is somewhere between values of 10^7 and 10^8 . Under these conditions, the rate expression becomes:

$$\text{rate} = \frac{k_p K_{eq}[Dr]([C]_o - [Cx])}{K_{eq}[Dr]}$$

which simplifies to:

$$\text{rate}_p = k_p([C]_o - [Cx]) \quad (3-84)$$

It should be noted that this simplified expression is independent of dye concentration, except for the small contribution of $[Dr]$ in the expression for $[Cx]$ given by Equation 3-80.

Using the same reasoning, it can also be seen that if $K_{eq}[Dr] < 10^{-2}$ or $K_{eq} < 10^3$, then the value $K_{eq}[Dr]$ is negligible with respect to 1, and the rate expression becomes:

$$\text{rate}_p = k_p K_{eq}[Dr]([C]_o - [Cx]) \quad \text{or, letting } K^* = k_p K_{eq}: \quad (3-85)$$

$$\text{rate}_p = K^*[Dr]([C]_o - [Cx]) \quad (3-86)$$

Although in this case the value of K_{eq} still affects the behavior of the system, it would be impossible to separate the constants k_p and K_{eq} if an attempt were made to determine them given an absorbance versus time curve. It will be shown later that Equation 3-86 is in exactly the same form as the expression obtained assuming the steady-state

condition. The curves represented by 1 and 2 in Figure 2 show curves resulting when values of $K_{eq} \leq 10^3$ are used.

The region between the extremes represented by Equations 3-84 and 3-86 has been studied in Figure 3. It can be seen that as the value of K_{eq} is increased, increments of equal magnitude affect the system less and less until the point at $K_{eq} > 10^7$, after which no additional effect is observed. Also, by noticing the change in curvature near the baseline going from curve 1 to curve 8 (increasing K_{eq}), it is apparent that the effect of the dye concentrations (proportional to A) is becoming less and less. That is, in the lower curves, a decrease in absorbance causes a corresponding decrease in rate causing gentle deterioration to zero absorbance. In the higher curves at corresponding A values, the rate is still relatively fast, resulting in a rapid decrease to zero.

The breaks in the curves which are most noticeable in curves 4 and 5 are a result of different periods of domination of promotion and catalytic paths. This is due to the term $([C]_0 - [Cx])$ in the rate expression. When the reaction is just under way, $[Cx] \approx 0$ since about all Cx is tied up by the complexing agent and, consequently, promotion predominates. As time passes, however, more catalyst is added as C_L is decreasing, until a point is reached where $[C]_0 \geq C_L$ (Note: $[C]_0$ means "total catalyst added at time = t", not initial catalyst concentration) and $rate_c > rate_p$. From this point on, the catalytic path predominates.

In reality, it is usually the case that equilibrium constants of reactions we would be likely to study would be large enough to neglect, dependent upon reaction conditions, of course. Consequently, the equation which most favorably describes any given system, assuming a pre-equilibrium condition, would be Equation 3-84. In the section in which

constants are determined, we will, in any case, assume that K_{eq} is either known or independently determinable.

Variation of K_f

The effect of varying K_f can be seen in Figure 4. It is quite easy to predict the outcome of changing K_f since this basically affects only the amount of catalyst available for reaction by the catalytic path. Figure 4 shows that values of $K_f > 10^5$ have no further effect on the system, under these conditions. A look at Equation 3-80 shows why. The predominant term is:

$$\text{Term} = \frac{1}{K_f} - (K_{eq}[\text{Dr}] + 1)([C]_o - C_L) \quad (3-87)$$

Assigning reasonable values, we have:

$$\begin{aligned} \text{Term} &= \frac{1}{K_f} - (10^8 \cdot 10^{-5} + 1)(10^{-5} - 2 \times 10^{-5}) \\ &= \frac{1}{K_f} + 10^3 \cdot 10^{-5} = \frac{1}{K_f} + 10^{-2} \end{aligned}$$

Again assuming a 1% rejection criterion, we have: $\frac{1}{K_f} < 10^{-4}$ or $K_f > 10^4$ in order to neglect $\frac{1}{K_f}$ in Equation 3-87. This agrees with results observed in Figure 4.

Variation of k_p

Figures 5 and 6 show the effect of varying k_p , the rate constant for promotion cycle. Figure 5 shows variation from the point where $\text{rate}_p \approx \text{rate}_c$ (curve 2) to where $\text{rate}_p \gg \text{rate}_c$. Figure 6 covers the

region from $\text{rate}_p \ll \text{rate}_c$ to where $\text{rate}_p \approx \text{rate}_c$. The curves show that, in general, the system behaves as expected; i.e., an increase in k_p results in an increase in the reaction rate. Figure 6 shows that the break which was mentioned previously in the discussion of the equilibrium constant variation. As before, this is attributed to predominance of either rate_p or rate_c in different portions of the curve. Again, as is shown by curve 6, Figure 6, rate_p predominates early because $[\text{Cx}] \approx 0$. It is interesting to note the sensitivity of the system to even small changes in k_p as is seen in Figure 6.

Variation of Total Initial Ligand Concentration

This is probably the most interesting aspect as far as chemical analysis is concerned. If the system is sensitive to changes in ligand concentration, we have a basis for a method to determine the ligand. Figures 7 and 8 show the effects of varying initial ligand concentration. Comparison of these two sets of curves shows the difference in sensitivity caused by an increase in the rate constant for promotion. Curves 2 and 3 in Figure 7 differ by approximately the same order of magnitude of curves 1 and 3 in Figure 8, yet the effect of the same change in ligand concentration is much greater in the second case.

It is obvious from studying the figures that in the early portions of the curves, the system is practically insensitive to ligand concentration. This can be attributed to the large formation constant of the metal-ligand complex, CxL . That is: in the early stages of reaction, not much catalyst has been added, and, if ligand is present, the metal will all be complexed if K_f is large (see previous section for definition of "large"). Under these conditions, two observations can be made:

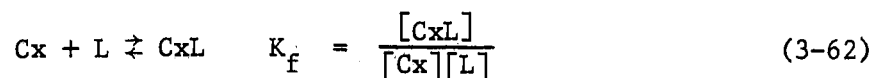
(1) no catalyst will be available for reaction by the normal catalytic path and the rate of the reaction is therefore due only to promotion caused by the complex, CxL ; and (2) as long as $C_L > C \cdot t$ where C = rate of catalyst addition and t = time, the catalyst will be the limiting factor in formation of the complex, CxL . Consequently, the resulting curve will be practically independent of C_L until enough time has passed to make $C \cdot t > C_L$. From this point on, the amount of complex formed will be negligible and catalyst will become available for reaction via the normal catalytic path. The rate will now be $rate_c + rate_p$ instead of only $rate_p$ as it was at the beginning of the reaction. The main difference, then, between two curves with a difference only in initial ligand concentration, is the amount of time it takes for enough catalyst to be added to complex all of the ligand present. This effect is especially noticeable in Figure 8.

Although this reasoning does not explain all the differences in the curves, it does account for the similarity of the reactions in the early stages. Other differences arise from the relative magnitudes of $rate_c$ and $rate_p$ which, of course, depend upon the relative size of the rate constants and the amount of rate-increasing complex, CxL , formed in the first stages of the reactions.

It should be noted at this point that almost an infinite variety of shapes and rates can be obtained by varying the different parameters of the system. Only those systems which seem reasonable when compared to existing curves from previous experiments have generally been selected for simulation.

Steady-State Condition of Rate-Increase: Derivation of Expressions

We shall now look at another possible path of reaction rate increase making use of the steady-state approximation. As in the pre-equilibrium approach, we again consider the formation of the complex CxL according to the following reaction:



Again, as in the previous discussion, we choose the following reaction path:



In this case, however, the second step is fast and the first, Equation 3-63, becomes rate determining. This is used in the following derivation.

We can write the rate of the reaction as:

$$\text{rate}_L = -\frac{d[\text{Dr}]}{dt} = k_1[\text{Dr}][\text{CxL}] - k_{-1}[\text{Q}] \quad (3-88)$$

Making the steady-state approximation:

$$\frac{d[\text{Q}]}{dt} = k_1[\text{CxL}][\text{Dr}] - k_2[\text{Q}] - k_{-1}[\text{Q}] = 0 \quad (3-89)$$

we arrive at:

$$k_1[\text{CxL}][\text{Dr}] = k_{-1}[\text{Q}] + k_2[\text{Q}] \quad (3-90)$$

Substitution of Equation 3-90 into Equation 3-88 gives:

$$\begin{aligned} \text{rate}_L &= k_{-1}[Q] + k_2[Q] - k_{-1}[Q] \quad \text{or:} \\ \text{rate}_L &= k_2[Q] \end{aligned} \quad (3-91)$$

Solving Equation 3-90 for $[Q]$ gives:

$$[Q] = \frac{k_1}{k_{-1} + k_2} [C_{xL}][Dr] \quad (3-92)$$

From the mass balance equation for total catalyst we have:

$$[C]_o = [C_{xL}] + [C_x] + [Q], \quad \text{or:} \quad (3-93)$$

$$[C_{xL}] = [C]_o - [C_x] - [Q] \quad (3-94)$$

Substitution of Equation 3-94 into Equation 3-92 gives:

$$[Q] = \frac{k_1}{k_{-1} + k_2} ([C]_o - [C_x] - [Q])[Dr] \quad (3-95)$$

Letting $\frac{k_1}{k_{-1} + k_2} = K^\ddagger$, we solve for $[Q]$:

$$[Q] = K^\ddagger[C]_o[Dr] - K^\ddagger[C_x][Dr] - K^\ddagger[Q][Dr]$$

continuing:

$$[Q] + K^\ddagger[Q][Dr] = K^\ddagger[Dr]([C]_o - [C_x]), \quad \text{and finally:}$$

$$[Q] = \frac{K^\ddagger[Dr]([C]_o - [C_x])}{1 + K^\ddagger[Dr]} \quad (3-96)$$

In this instance, k_2 is greater than k_1 for the steady-state approximation and since $k_{-1} > 0$, it can be seen that $K^\ddagger < 1$. Since in actual laboratory practice $[\text{Dr}] \approx 10^{-5}$ M, we can neglect the term $K^\ddagger[\text{Dr}]$ in the expression $(1 + K^\ddagger[\text{Dr}])$ since the term $K^\ddagger[\text{Dr}] \leq [\text{Dr}] \approx 10^{-5}$. This gives a simplified expression for $[\text{Q}]$:

$$[\text{Q}] = \frac{k_1}{k_{-1} + k_2} [\text{Dr}] ([\text{C}]_0 - [\text{Cx}]) \quad (3-97)$$

Substitution of Equation 3-97 into Equation 3-91 gives the rate expression:

$$\text{rate}_L = \frac{k_2 k_1}{k_{-1} + k_2} [\text{Dr}] ([\text{C}]_0 - [\text{Cx}]) \quad (3-98)$$

An expression for $[\text{Cx}]$ can be obtained in exactly the same way as it was for the pre-equilibrium condition if we note the similarity in Equation 3-66:

$$[\text{Q}] = K_{\text{eq}} [\text{CxL}] [\text{Dr}] \quad \text{and Equation 3-92}$$

$$[\text{Q}] = \frac{k_1}{k_{-1} + k_2} [\text{CxL}] [\text{Dr}].$$

In the expression for $[\text{Cx}]$, Equation 3-80, we simply replace K_{eq} wherever it appears with $\frac{k_1}{k_{-1} + k_2}$. Since we have already shown that this constant is less than one and that $[\text{Dr}] \approx 10^{-5}$ M, we can again neglect

$\frac{k_1}{k_{-1} + k_2} [\text{Dr}]$ when compared to 1 and Equation 3-80 simplifies to:

$$[Cx] = \frac{1}{2} \left\{ - \left[\frac{1}{K_f} - ([C]_o - C_L) \right] + \sqrt{\left[\frac{1}{K_f} - ([C]_o - C_L) \right]^2 + \frac{4}{K_f} [C]_o} \right\} \quad (3-99)$$

where, as in Equation 3-83, $\Delta C_L = \text{rate}_L \cdot \Delta t$, since Equation 3-64 is not reversible.

A closer look at Equation 3-98 shows that if $k_2 \gg k_{-1}$, we can neglect k_{-1} in the expression $(k_{-1} + k_2)$ and Equation 3-98 simplifies to:

$$\text{rate}_L = k_1 [Dr] ([C]_o - [Cx]) \quad (3-100)$$

As was mentioned previously, this equation is in the same form as Equation 3-86:

$$\text{rate}_L = K^* [Dr] ([C]_o - [Cx]) \quad \text{where } K^* = k_p K_{eq} \quad (3-86)$$

It is interesting to note the similarity of these expressions. One, Equation 3-100, is obtained assuming steady-state conditions and the other, Equation 3-86 is derived assuming the pre-equilibrium condition.

Steady-State Condition of Rate Increase: Computer Analysis

As was done with the pre-equilibrium condition, we again look at the effect that varying different parameters has on the system. The same procedure was used and units are all the same as those given in Table I, with the exception of k_p . Here, due to the presence of $[Dr]$ in Equation 3-100 k_p has units of $M^{-1} \text{min}^{-1}$. The results of varying certain parameters (k_p , K_f , and C_L) can be seen in Figures 9 through 11 and are summarized in the following paragraphs.

$$[Cx] = \frac{1}{2} \left\{ - \left[\frac{1}{K_f} - ([C]_o - C_L) \right] + \sqrt{\left[\frac{1}{K_f} - ([C]_o - C_L) \right]^2 + \frac{4}{K_f} [C]_o} \right\} \quad (3-99)$$

where, as in Equation 3-83, $\Delta C_L = \text{rate}_L \cdot \Delta t$, since Equation 3-64 is not reversible.

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COMPOSITE GRAPH SHOWING VARIATION OF CURVES WITH CHANGES IN KPRD

7/12/71

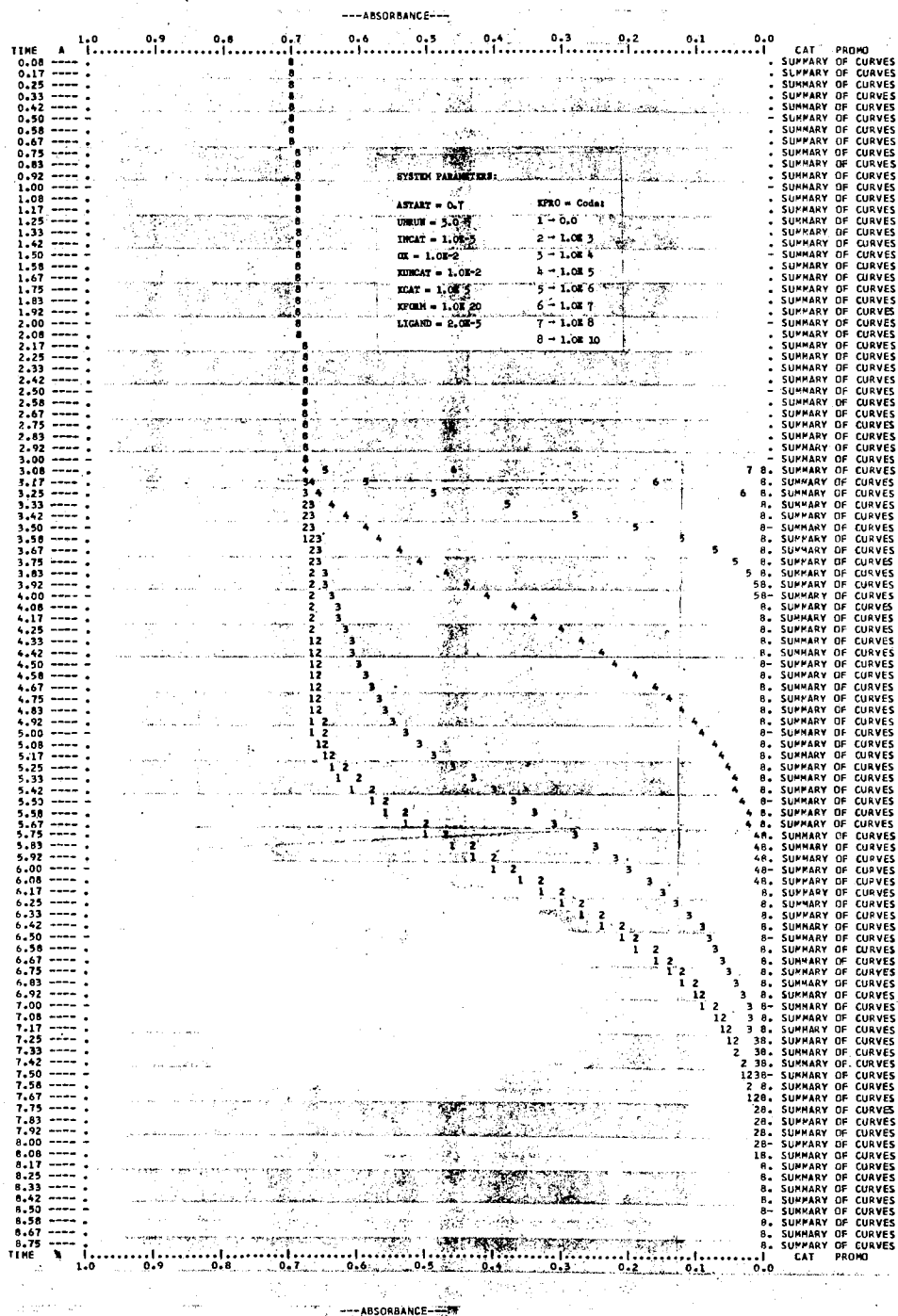


Figure 10. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Steady-State Condition. Effect of Varying k_p

CHEN 5000--R.E. SIMPSON

COMPOSITE GRAPH SHOWING VARIATION OF CURVES WITH CHANGES IN LIGAND CONC 7/12/71

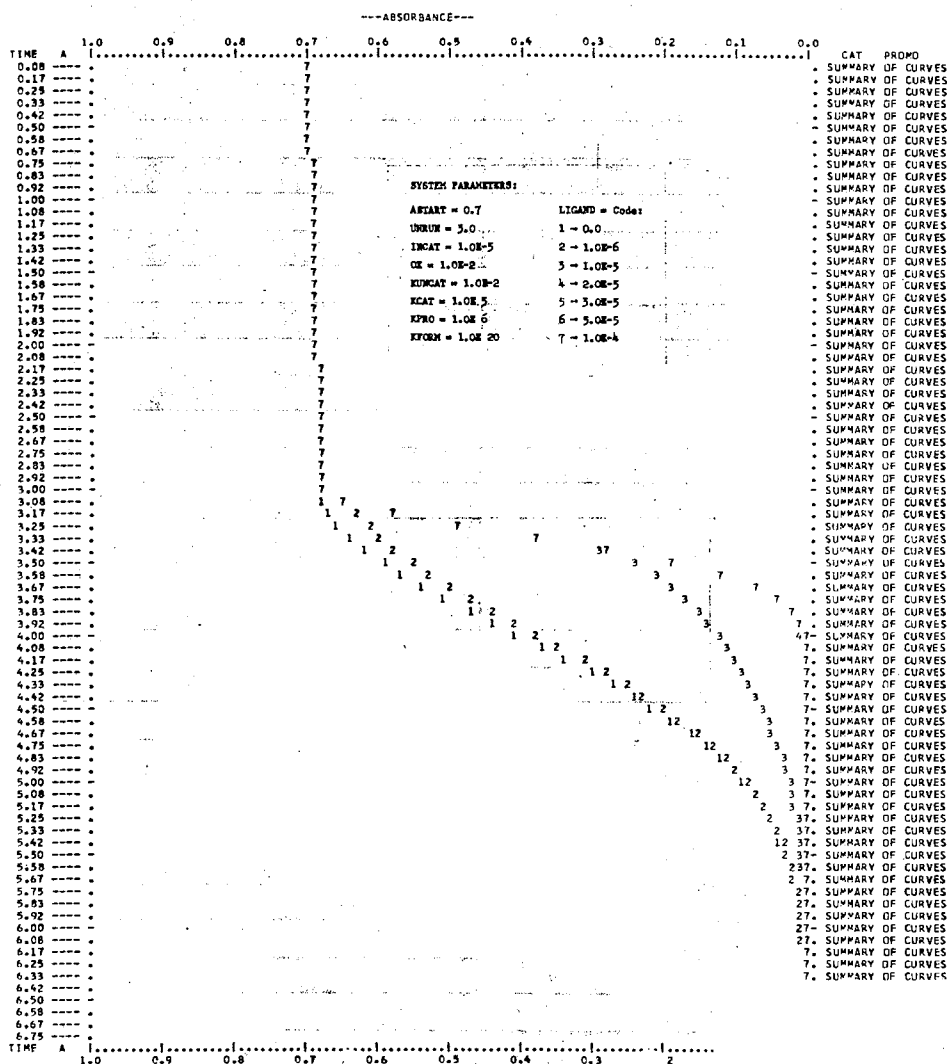


Figure 11. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Steady-State Condition. Effect Varying Initial Ligand Concentration

Variation of K_f

K_f is again the formation constant of the metal-ligand complex. Here again, its value affects most directly the amount of catalyst available for reaction by the normal catalytic cycle. That is, if K_f is large enough, practically all of the catalyst added is immediately complexed. How large must K_f be? If we look at Equation 3-99, the expression for $[Cx]$, we can see that the predominant term is:

$$\text{Term} = \frac{1}{K_f} - ([C]_0 - C_L) \quad (3-101)$$

For example, if $C_L \sim 2 \times 10^{-5}$ and $[C]_0 \sim 10^{-5}$, we have:

$$\text{Term} = \frac{1}{K_f} + 10^{-5}$$

Assuming a 1% rejection criterion, we have: $\frac{1}{K_f} < 10^{-5} \cdot 10^{-2}$ or $K_f > 10^7$ in order to neglect the term $\frac{1}{K_f}$ in Equation 3-101. This result agrees with the observation in Figure 9 in which values of $K_f \geq 10^7$ exhibit no further effect on the system.

Variation of k_p

Figure 10 shows the results of varying the rate constant for the promotion cycle. As in the pre-equilibrium condition, we again see a break in the curves where $k_p < k_c$ due to the predominance of rate p and rate c in different portions of the curve. Curve 3 especially shows the slower rate due only to promotion in the early portions of the curve where all catalyst is complexed and none is available for reaction by

the normal catalytic path. At about $t = 4.92$ minutes, however, enough catalyst has been added to overcome the amount of complexing agent present and the reaction continues in such a way that $\text{rate} = \text{rate}_c + \text{rate}_p$ instead of $\text{rate} = \text{rate}_p$ only.

Curve 4 is noteworthy in that here $k_p = k_c$. The overall rate equation used in the simulation is:

$$\frac{dA}{dt} = -k_u A - k_c A[Cx] - k_p A([C]_o - [Cx]) \quad (3-102)$$

After rearranging and grouping terms, this expression may be written as:

$$\frac{dA}{dt} = -k_u A - (k_c - k_p)A[Cx] - k_p A[C]_o$$

It can be seen that if $k_c = k_p$, the expression simplifies to:

$$\frac{dA}{dt} = -k_u A - k_p A[C]_o \quad \text{or, since } k_p = k_c: \quad (3-104)$$

$$\frac{dA}{dt} = -k_u A - k_c A[C]_o$$

This is the exact expression obtained for the pre-equilibrium mechanism assuming no complexing agent present (see: Equation 3-12). Thus, if we assume this mechanism, it would be impossible to tell promotion from ordinary metal catalysis under these conditions.

Variation of Total Initial Ligand Concentration

Figure 11 shows the same effect observed in the pre-equilibrium condition. That is, if $[C]_o < C_L$, C_L has no further effect on the system as long as it is greater than a given value. Figure 11 shows that, under this particular set of conditions, the minimum value of C_L is

2×10^{-5} M. Any concentration greater than this has no further effect on the system.

Ligand Effect: True Catalysis or Promotion

The difference between true catalysis and promotion has been mentioned earlier. The developments in the previous sections have considered only promotion. In other words, it has been assumed that $dC_L/dt \neq 0$.

If the system is truly catalyzed by the formation of a complex, we may write Equations 3-63 and 3-64 in the following manner:



The only difference in the expressions describing true catalysis and those for promotion is in the value of C_L . Before, since $\frac{dC_L}{dt} \neq 0$, it was necessary to numerically integrate the expression for $\frac{dC_L}{dt}$ to obtain a value for C_L . In the present case, however, we merely say: $C_L = \text{constant} = \text{the concentration of ligand initially added}$. The only modification to the simulating programs was the removal of the expressions giving the value of $\frac{\Delta C_L}{\Delta t}$. Results of computer simulation can be seen in Figures 12 through 17 (assuming the pre-equilibrium condition) and Figures 18 through 20 (assuming the steady-state condition). It can be seen that these curves are, in general, quite similar to their counterparts in Figures 2 through 11. There are a few subtle differences, however, and these contrasts are summarized in Table II.

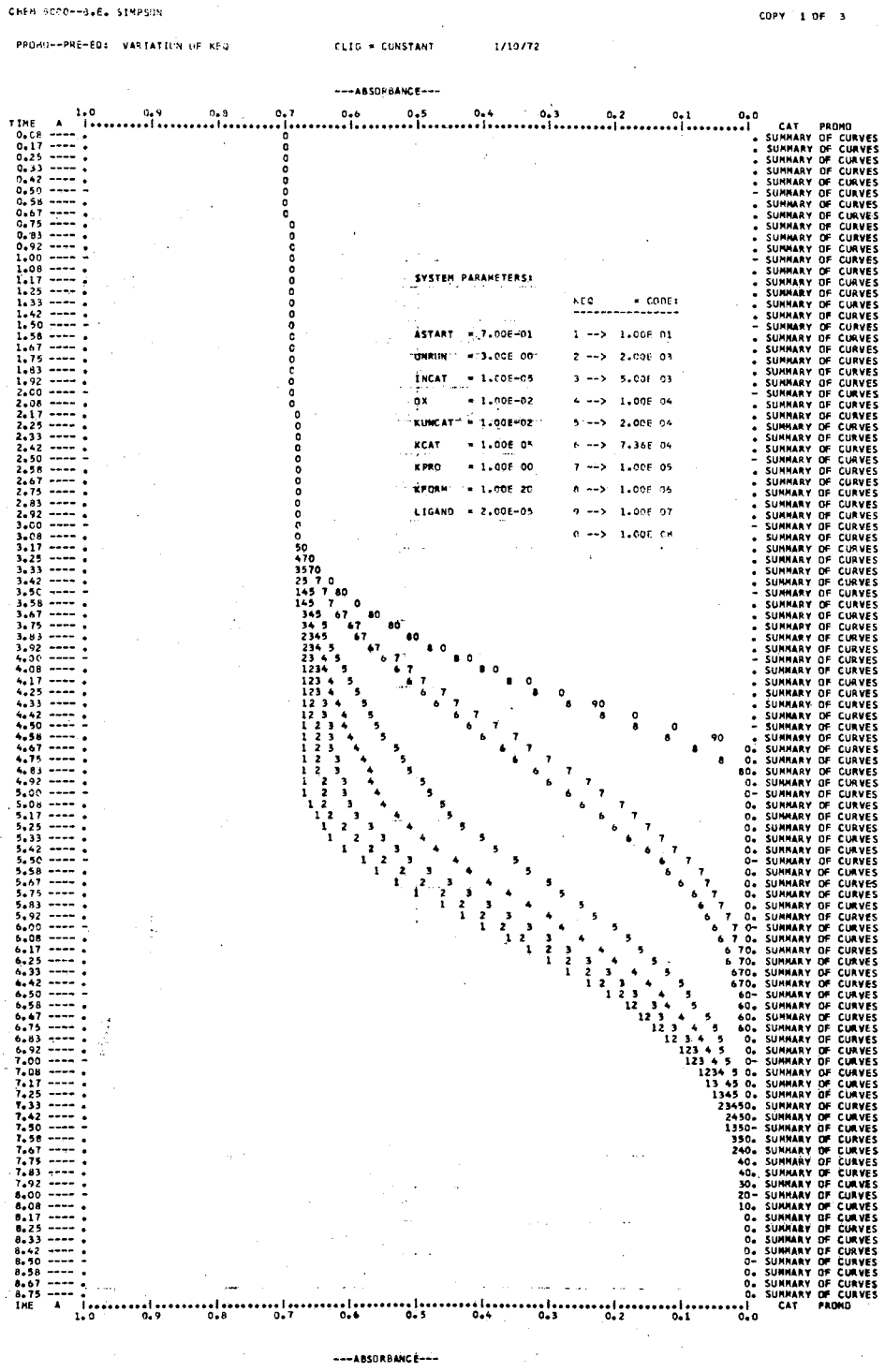


Figure 12. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition and True Catalysis. Variation of K_{eq}

PRMGD--PRE-EQ: VARIATION OF KFORM

CLIG = CONSTANT

1/10/72

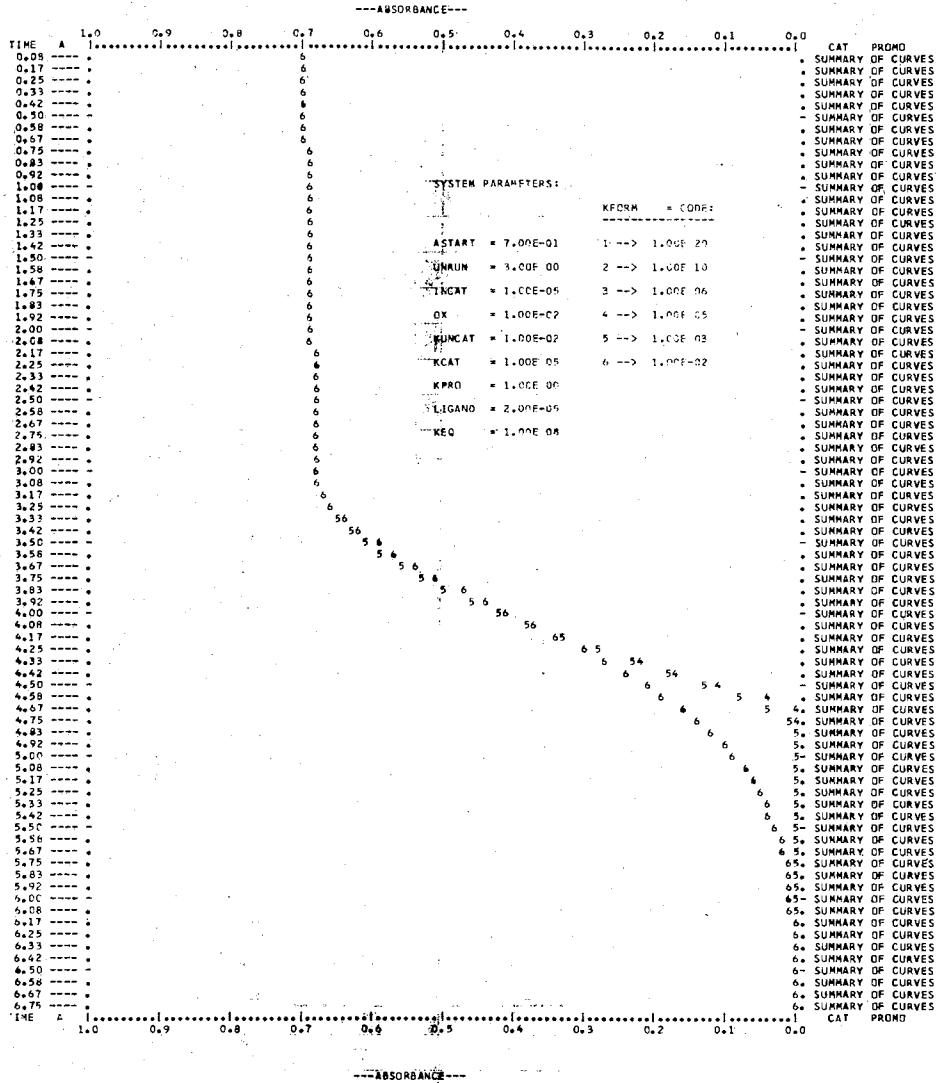


Figure 13. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition and True Catalysis. Effect of Varying K_f

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COPY 1 OF 3

PROMO--PRE-EQ: VARIATION OF CLIG(NT) WHEN KPRU = 0.02 ; CLIG = CONST 1/10/72

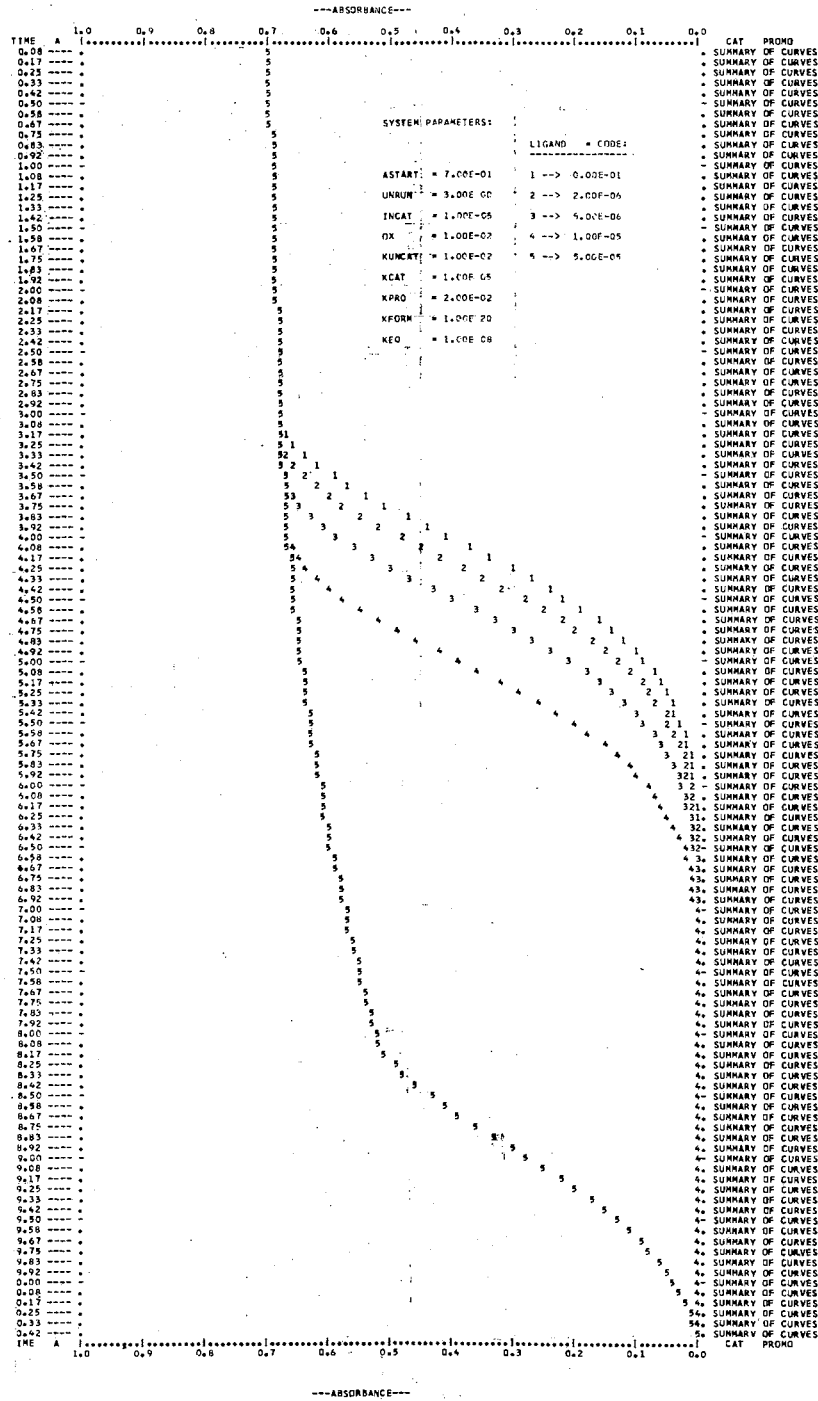


Figure 15. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition and True Catalysis. Effect Varying Initial Ligand Concentration

CHEM 5000--B.E. SIMPSON

COPY 1 OF 3

PROMO--PRE-EQ: VARIATION OF CLIG(I)INITI WHEN KPRO = 1.00 ; CLIG = CONST 1/10/72

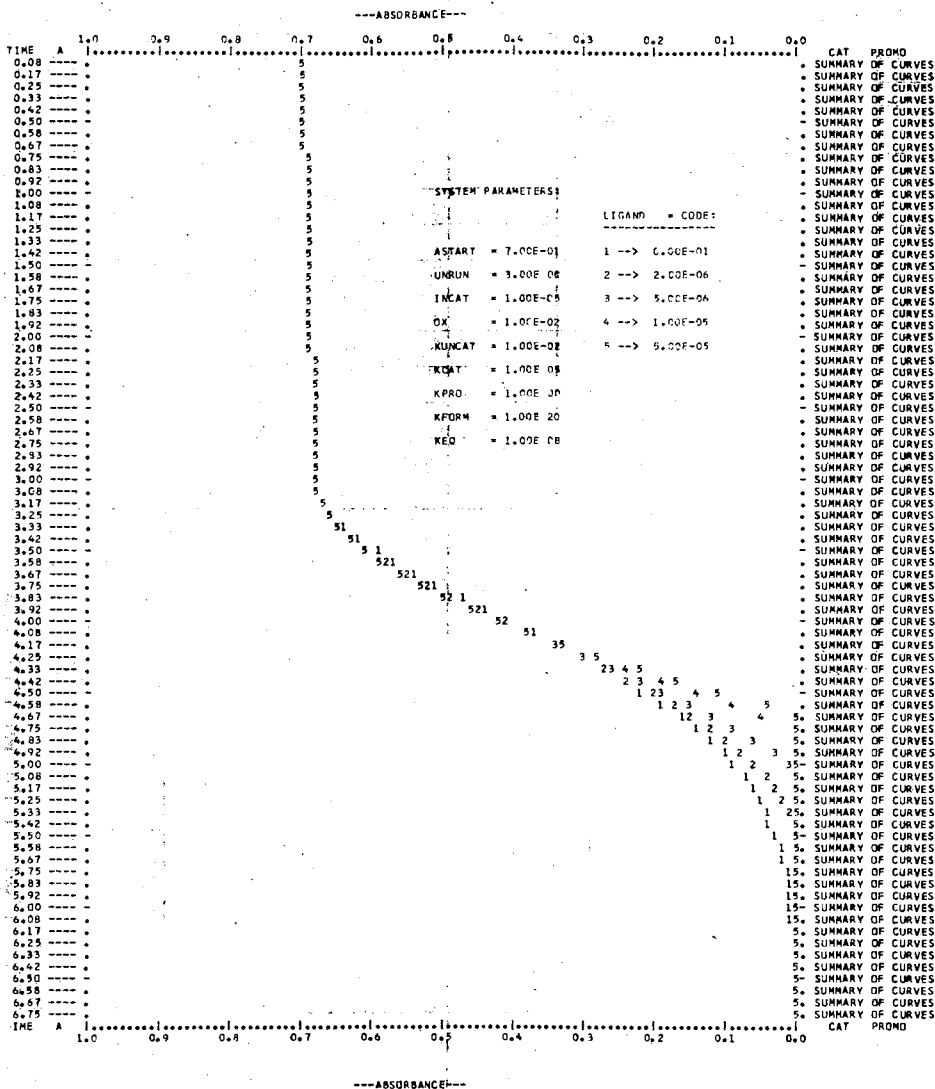


Figure 16. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition and True Catalysis. Effect Varying Initial Ligand Concentration

CHEM 500C--B.E. SIMPSON

COPY 1 OF 3

PRGM--PRE-EQ: VARIATION OF CLIG(INIT) WHEN KPRO = 5.00 ; CLIG = CONST 1/1/72

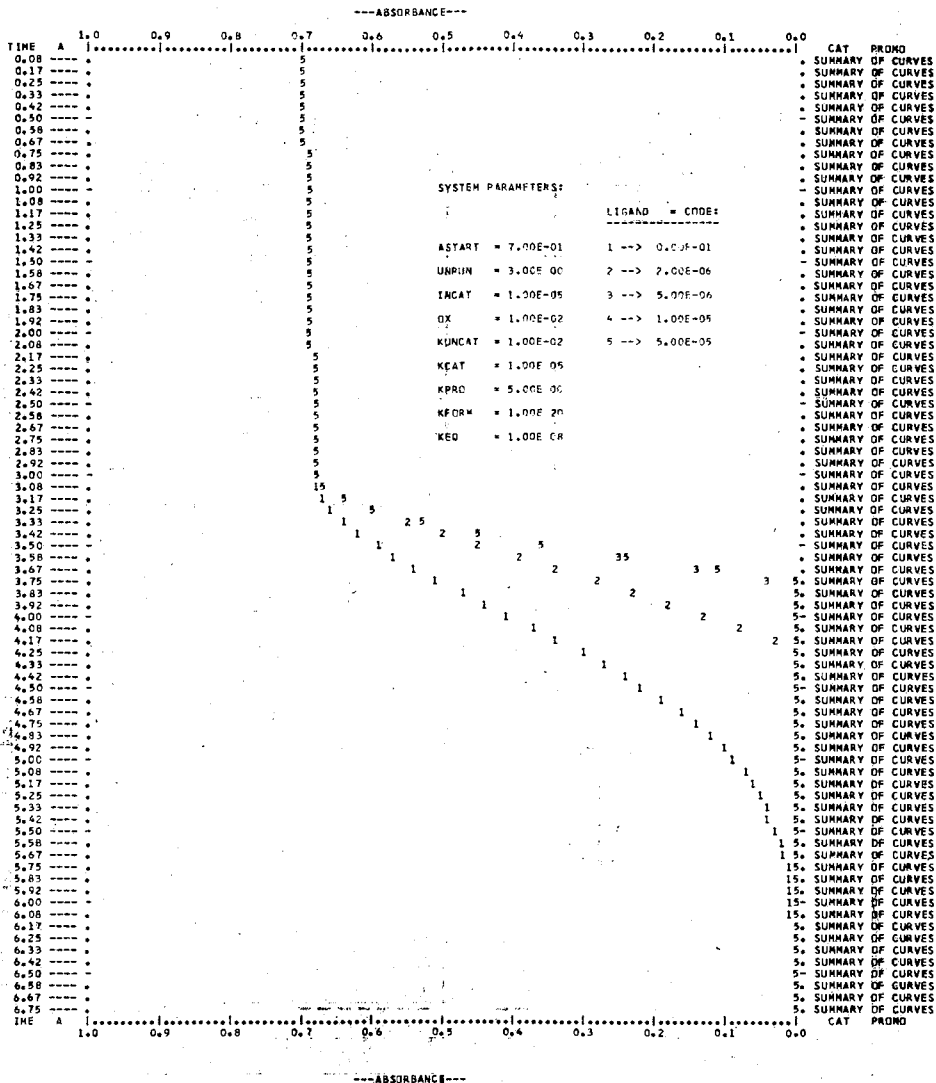


Figure 17. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Pre-equilibrium Condition and True Catalysis. Effect Varying Initial Ligand Concentration

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COPY 3 OF 3

PRMO--SI-ST: VARIATION OF KFORM; CLIG=CONST

1/13/72

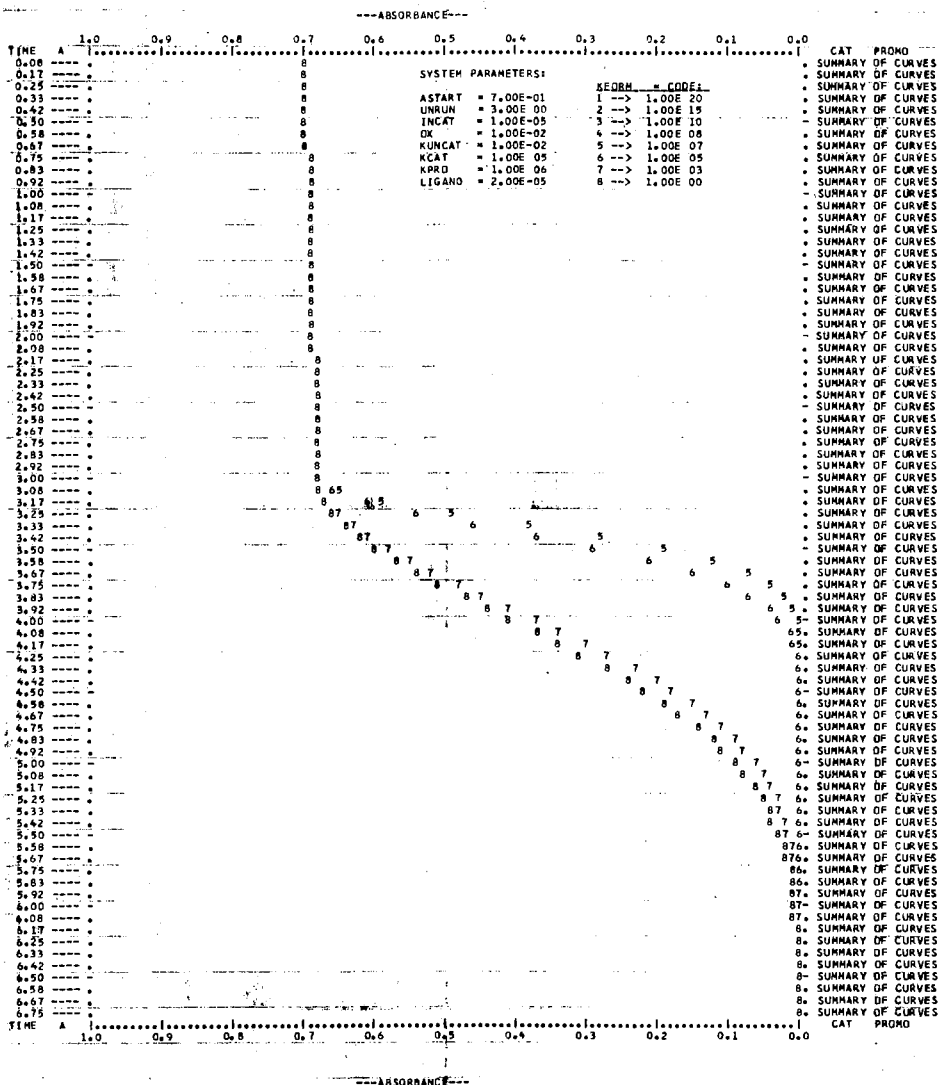


Figure 18. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Steady-State Condition and True Catalysis. Effect of Varying K_f

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COPY 3 OF 3

PROMO--ST-ST1 VARIATION OF KPRU: CLIG=CONST.

1/13/72

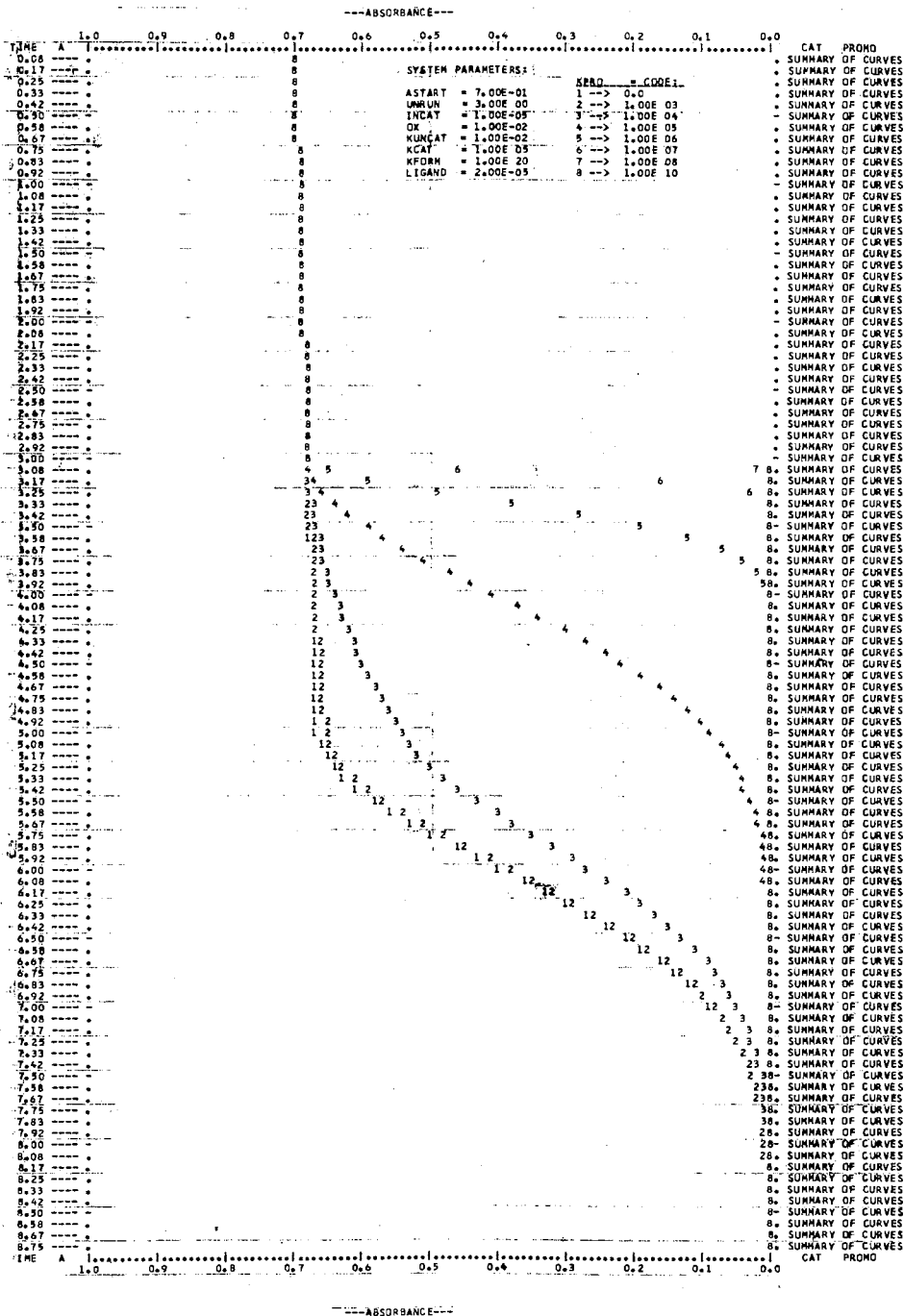


Figure 19. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Steady-State Condition and True Catalysis. Effect of Varying k_p .

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COPY 3 OF 3

PRMO--ST-ST: VARIATION OF LIGAND: CLIG=CCONSTANT

1/13/72

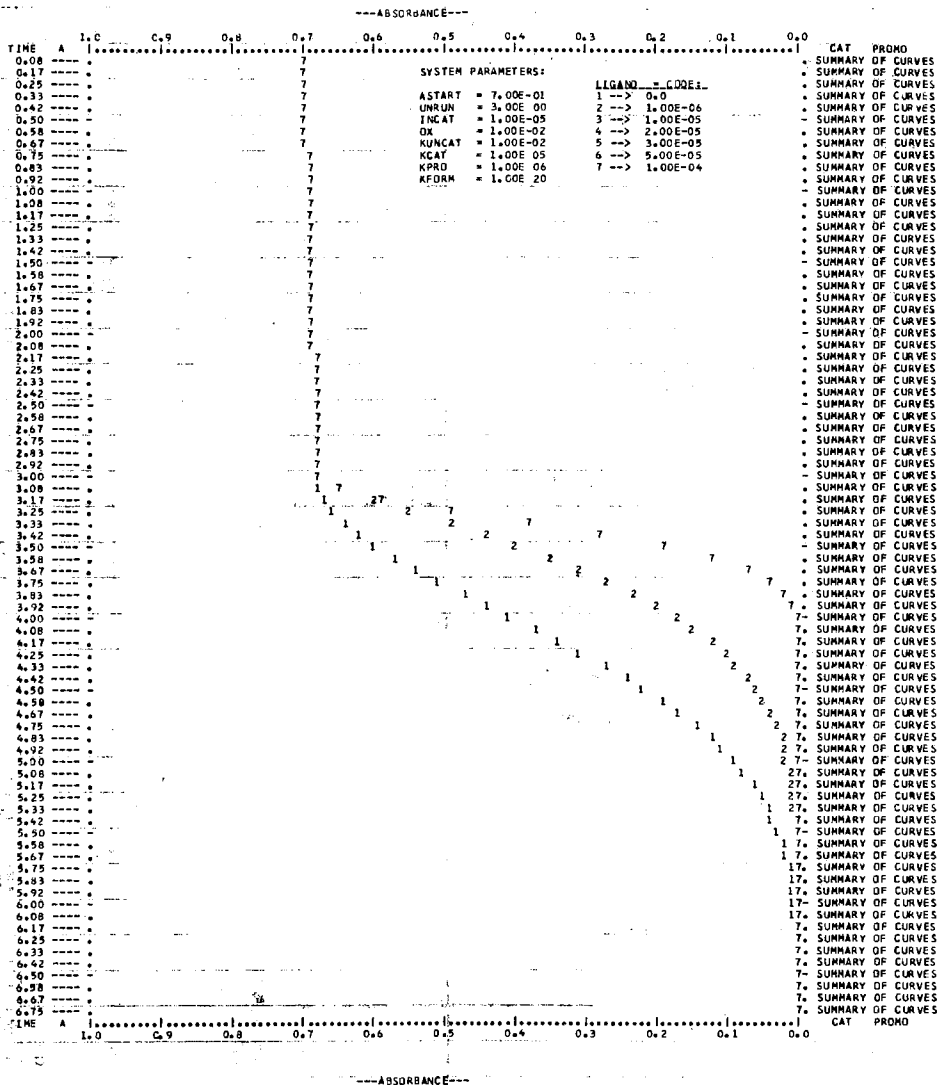


Figure 20. Computer Simulation of Hypothetical System; Addition of Rate-Increasing Complexing Agent Assuming Steady-State Condition and True Catalysis. Effect of Varying Initial Ligand Concentration

TABLE II

COMPARISON OF RESULTS OBTAINED ASSUMING TRUE CATALYSIS WITH THOSE OBTAINED ASSUMING PROMOTION

Parameter Varied	Condition Assumed	Reaction Rate Comparison			
		Catalysis	Ref. Fig:	Promotion	Ref. Fig:
		<u>Faster than Promotion When:</u>		<u>Faster than Catalysis When:</u>	
KEQ	Pre-eq.	KEQ large compared to $1/(Dr)$	12	KEQ small compared to $1/(Dr)$	2,3
KFORM	Pre-eq.	K_f larger than $1/(C)_o$	13	Never faster	4
	St-St	K_f larger than $1/(C)_o$	18	Never faster	9
KPRO	Pre-eq.	k_p larger than ϵ/k_c	14	k_p smaller than ϵ/k_c	5,6
	St-St	Never faster	19	k_p smaller than k_c	10
CLIG	Pre-eq.	Always faster	15,16,17	Never faster	7,8
	St-St	C_L much smaller than $(C)_o$	20	Never faster	11

The most drastic and, consequently, the most interesting difference in rates between true catalysis and promotion effects is observed in the case of variation of initial ligand concentration. This rather pronounced difference in effects may be explained by looking at two key expressions. Equations 3-80 and 3-99 give the amount of catalyst available for reaction by the normal catalytic cycle when assuming the pre-equilibrium and steady-state mechanisms, respectively. These expressions can in turn be analyzed in terms of a common expression:

$$\text{Term} = [C]_0 - C_L .$$

As was mentioned in earlier discussion, as long as $[C]_0 < C_L$, almost all of the available catalyst is tied up in the complex, CxL . If this is the case, the $\text{rate}_c \approx 0$ and $\text{rate}_{\text{overall}} = \text{rate}_L$ ($\text{rate}_L = \text{rate}$ due to ligand effect). It can be seen, then, that if $\frac{dC_L}{dt} = 0$ and C_L is therefore not decreasing as the reaction proceeds, catalyst will be tied up longer by a given amount of ligand added at $t = 0$. If, for a given system, the rate due to ligand effects is faster than the rate due to the normal catalytic cycle, then we would expect the faster rate to persist for a longer time if C_L is not destroyed. This accounts for the observed effect in the simulated curves. If we had chosen a system in which $\text{rate}_L < \text{rate}_c$, the opposite effect would be observed; i.e., the promotion effect would give the fastest overall rate since the slower rate (rate_L) would not be allowed to persist for as long since C_L is being destroyed as the reaction proceeds.

It is noteworthy to mention that the curves observed assuming the steady-state condition and true catalysis, most closely resemble those

shown in the literature (9).

Determination of Constants

The second phase of this study of catalytic titrations involved the elucidation of rate constants for the catalyzed and uncatalyzed portions of a given reaction from absorbance versus time data. The basic principles of the method used are the same regardless of the mechanism chosen: that is, estimates of rate constants may be obtained by plotting the instantaneous rate of a reaction, measured as the derivative of an absorbance versus time curve against some function of time and absorbance. That particular function to be used depends upon the system under study and the form of the differential equations describing the system. For this reason, a hypothetical system very similar to that described earlier (see pages 9-11 this work) was used to develop the computer programs necessary to obtain estimates of rate constants. Applications of a modified version of the program described here to a real system are discussed in the next chapter.

Consider a generalized, simplified rate expression of the following form:

$$\text{RATE} = \text{UNCATALYZED RATE} + \text{CATALYZED RATE} \quad (3-108)$$

where:

$$\text{UNCAT RATE} = \frac{dA}{dt} = -k_u A, \quad (3-109)$$

$$\text{CAT RATE} = \frac{dA}{dt} = -k_c A(C)_o, \quad (3-110)$$

$(C)_o$ = amount of catalyst added at time = t or

$(C)_o = Ct = (\text{catalyst addition rate in moles/liter} \cdot \text{min})$
(time)

and

A = absorbance of the monitored species.

It was assumed throughout this development for the sake of simplicity and clarity of illustration that k_u and k_c represented true first and second order rate constants, respectively, and that the rate of the reaction was independent of any parameters other than those given in the rate expression.

Looking first at the uncatalyzed part, it can be seen that if dA/dt is plotted as a function of A, the slope of the resulting straight line will be equal to $-k_u$. Now, taking the overall rate equation and rearranging, we get:

$$\frac{dA}{dt} + k_u A = -k_c A C t \quad (3-111)$$

Here again, knowing k_u , we can plot the quantity $(\frac{dA}{dt} + k_u A)$ versus $A C t$ and, again, obtain the slope, $-k_c$, and thus the catalyzed rate constant.

It was obvious that for this procedure to work, a reliable method of determining the derivative, dA/dt , must be used. Such a method was found in the literature (16). The method essentially consists of the following. An odd number of ordinate points is used in a "convoluting smooth" to obtain the derivative of the central point of those taken. The value of the derivative is found using the following relationship:

$$\text{derivative of central point} = \frac{\sum_{i=-m}^m C_i Y_i}{\Delta X \cdot N}$$

where:

$$Y = f(X),$$

$$m = \text{number of points taken,}$$

C_i = convoluting integers, and

N = normalizing factor.

The constants C_i and the normalizing factor N are given in tables in the reference (16).

An equally important factor, of course, is the least-squares fitting routine. The method used is the same as that outlined in an article by Sullivan, Rydberg, and Miller (17). A set of normal equations is generated and then solved by matrix inversion. The most useful portion of their work was the inclusion of a data weighting feature and a method of obtaining statistical parameters by using the diagonal elements of the inverted matrix arising from the solution of the set of normal equations.

Weighted least squares minimizes the function:

$$S = \sum_{i=1}^I W_i (Y_{i(\text{calc})} - Y_{i(\text{obs})})^2 \quad (3-113)$$

where:

S = "sum of squares",

I = no. of data points,

W_i = weights of each individual data point,

Y_{obs} = observed or experimental ordinate value, and

Y_{calc} = ordinate value calculated from results of fit.

In the present work, weights for each point were based on indeterminate errors from two sources: (1) instrumental error and (2) error in reading the chart paper from which the data was obtained. This may be represented as:

$$\text{TOTAL ERROR} = \text{INSTRUMENTAL ERROR} + \text{CHART READING ERROR} \quad (3-114)$$

An expression for instrumental error may be arrived at in the same manner as that used by Willard, Merit, and Dean (18). According to these authors:

$$\frac{\Delta C}{C} = \frac{0.4343 \Delta T}{T \log T} \quad (3-115)$$

where:

C = concentration of monitored species,

ΔC = error in C ,

T = transmittance, and

ΔT = photometric error.

But, since:

$$A = -\log T \quad (3-116)$$

where: A = absorbance, we have:

$$\frac{\Delta C}{C} = \frac{0.4343 \Delta T}{-A \cdot 10^{-A}} = \frac{0.4343 \cdot 10^A \cdot \Delta T}{-A} \quad (3-117)$$

From Beer's Law:

$$C = \frac{A}{\epsilon b} \quad \text{or} \quad \Delta C = \frac{\Delta A}{\epsilon b} \quad (3-118)$$

where:

ϵ = molar absorptivity and b = path length = 1 cm.

Then, ignoring the negative sign since error is absolute, the final expression for the relative error due to instrumental error is:

$$\text{rel. error} = \frac{\Delta A}{A} = \frac{0.4343 \cdot 10^A \cdot \Delta T}{A} \quad (3-119)$$

If the absolute error in chart reading is represented by ΔR , the overall expression for relative error becomes:

$$\text{TOTAL ERROR} = \frac{1}{A} (.4343 \cdot 10^A \cdot \Delta T + \Delta R) \quad (3-120)$$

A plot of total error versus absorbance with $\Delta T = .005$ and $\Delta R = .002$ is shown in Figure 21. A weighting function which gives almost equal weight to those points occurring in the flat portion of the curve is:

$$W_i = \left[\frac{P}{100} - (\text{total rel. error}) \right] \cdot 10 \quad (3-121)$$

where:

P = maximum acceptable per cent error.

A plot of W_i versus A with $P = 10\%$ is also shown in Figure 21. This is the weighting expression used for the determination of system parameters,

"Data" for a test run was provided by simulating a curve using the following parameters:

- A_o = initial absorbance = 0.7
- k_u = uncatalyzed rate constant = 10^{-4} /min.
- k_c = catalyzed rate constant = 10^5 L/M·min.
- C = catalyst addition rate = 10^{-5} M/L·min.

Values of absorbance thus obtained for the overall (that is, uncat + cat) portions of the curve were read into a program which does the following:

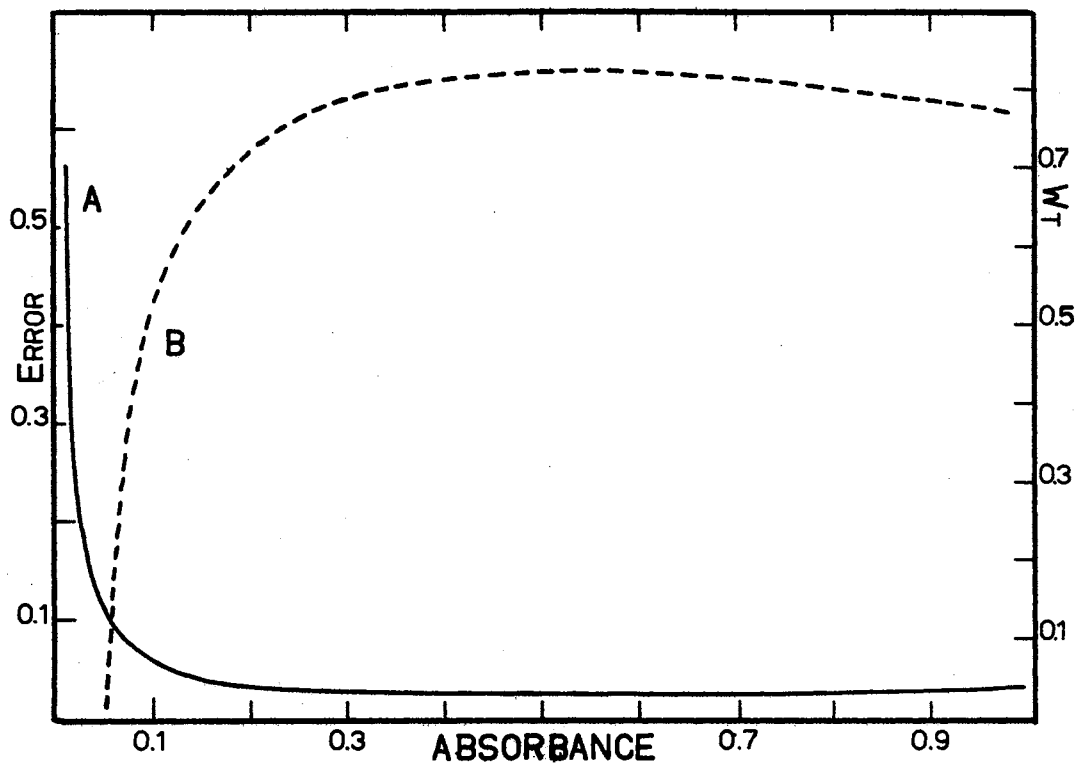


Figure 21. Error Curves for Absorbance Region 0 to 1. Curve A: Relative Error in Measurement as Function of Absorbance. Curve B: Weight Assigned to Individual Data Points Derived From Corresponding Absorbance Value

- i) determines dA/dt ,
- ii) computes the corresponding independent and dependent variables,
- iii) does a least squares fit of the function thus obtained, and
- iv) prints out the slope of the line and goodness of fit parameters.

The points obtained from the program along with the best least squares line are plotted in Figure 22. The value found by the program for the catalyzed rate constant was:

$$k_c = 1.02 \times 10^5 .$$

Compared to the 'true' value used in the simulation, this number contains an error of + 2.0%.

A complete listing of the source program along with a flow diagram and definition of all FORTRAN variables is given in Appendix D.

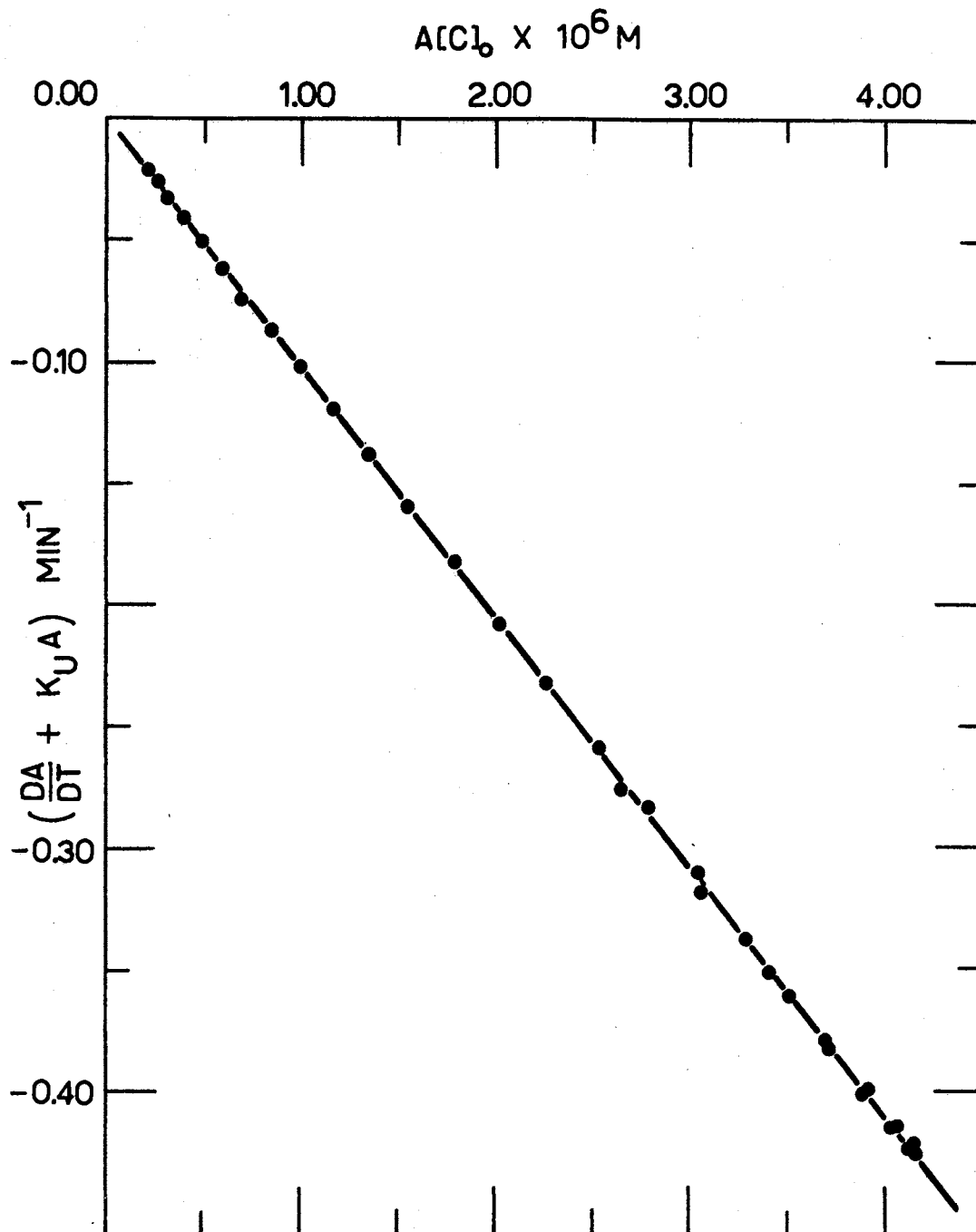


Figure 22. Determination of Rate Constants Using a Computer Simulated Catalytic Titration Curve as Data

CHAPTER IV

ANALYSIS OF A REAL SYSTEM

Catalyzed Oxidation of a Dye

The system selected for analysis was the Mn(II) catalyzed oxidation of malachite green cation (MG⁺) by periodate ions. This system was chosen for study primarily due to its relatively broad use in analytical applications (19,20). First, a set of criteria had to be set aside to decide when a given mechanism adequately "describes" the system under study. The criteria used were these: (1) values found for any rate constant must remain constant under variation of at least one major system variable (such as initial dye concentration, oxidizing agent concentration, catalyst addition rate, etc.) and (2) constants found with the program described in Chapter III must reproduce the experimental curve from which they were derived when used in the simulation program also described in Chapter III. Any mechanism which led to the satisfaction of these two points was considered to adequately describe the behavior of the system under study.

Selection of a Simplified Mechanism

The logical place to start the search for a suitable mechanism to describe the Mn(II) catalyzed oxidation was with those mechanistic assumptions discussed previously in this work in Chapter III. As has been pointed out earlier, assumption of pre-equilibrium kinetics leads to a

rate expression of the form:

$$\frac{dA}{dt} = -k_u A - k_c A [\text{Mn(II)}]_t \quad (4-1)$$

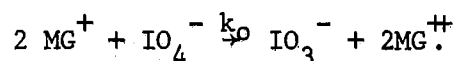
where:

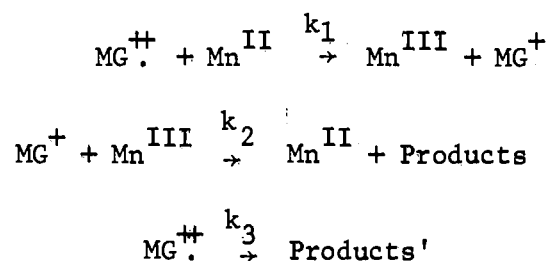
$$[\text{Mn(II)}]_t = \text{amt. of catalyst added at time} = t$$

Since the value of k_u was known from previous work (23), and was equal to $1.5 \times 10^{-3} \text{ min}^{-1}$, the contribution from the uncatalyzed reaction would be small when compared to that from the catalyzed portion. Since in this work the uncatalyzed reaction was almost imperceptible over a period of three minutes and rough calculations confirmed the order of magnitude of the reported value, the uncatalyzed contribution has been neglected in the determination of catalyzed rate constants for the sake of simplicity.

A set of experimental titration curves was obtained, the absorbance values were read and punched onto IBM data cards, and the instantaneous rate, dA/dt , was plotted as a function of the absorbance times the catalyst concentration. The plots were straight lines, but the resulting constants did not meet criterion #1, i.e.,--the values were a function of initial dye concentration. Consideration of a reverse reaction in the rate determining step succeeded in producing a better fit of the data, but failed to compensate for the dependence of rate constants upon initial dye concentration.

The possibility of a chain mechanism was also considered using the following equations to describe the system:





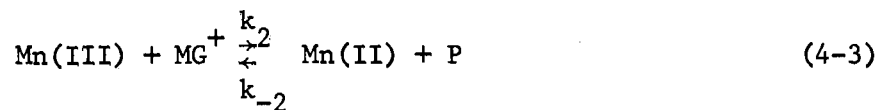
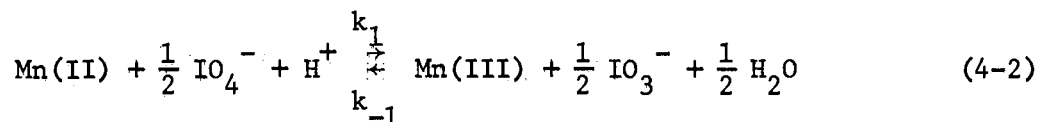
This mechanism was ruled out "on paper", however, when the derived rate equation proved to be independent of catalyst concentration, which was definitely unrealistic.

These results led to the consideration of the steady-state approximation in the reaction kinetics in hopes of obtaining a mechanism which better described the system. The apparent reliance of the observed rate upon initial dye concentration prompted the inclusion of possible reverse reactions in the development of the overall rate expressions.

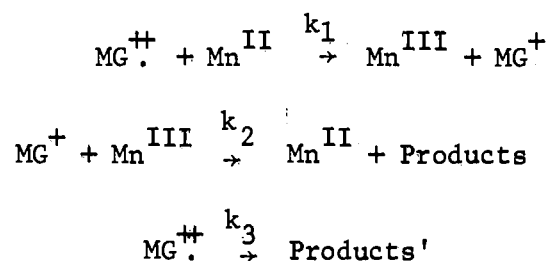
Use of the steady-state approximation led to the development of a mechanism which met both of the established criteria. Complete derivation of the final expression follows.

Development of Expressions for the Selected System

The reaction path considered was:



It was felt that Mn(III) was a reasonable choice for the reaction intermediate and was preferred over any higher oxidation states for several reasons. First, it is well known that acetate stabilizes the +3 ox-



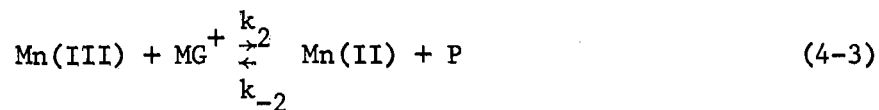
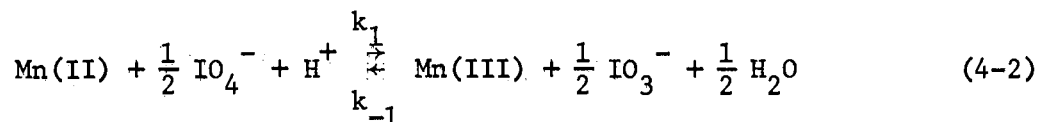
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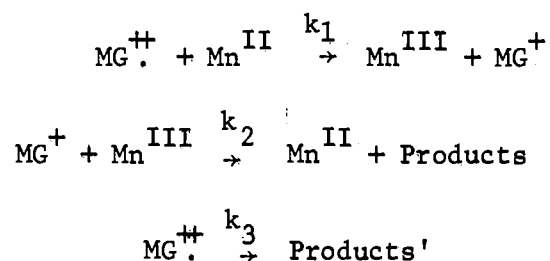
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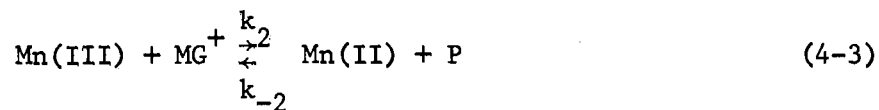
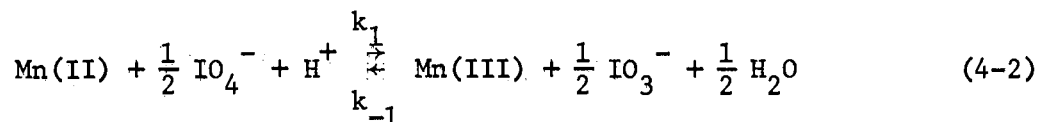
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The reaction path considered was:



It was felt that Mn(III) was a reasonable choice for the reaction intermediate and was preferred over any higher oxidation states for several reasons. First, it is well known that acetate stabilizes the +3 ox-

$$\text{Rate} = -(k_2[\text{Dr}] + k_{-2}[\text{Dx}])[\text{Cx}] + k_{-2}[\text{C}]_0[\text{Dx}] \quad (4-11)$$

Substitution of Equation 4-9 for $[\text{Cx}]$ led to:

$$\text{Rate} = \frac{-(k_2[\text{Dr}] + k_{-2}[\text{Dx}]) (k_1[\text{Ox}]^{1/2} + k_{-2}[\text{Dx}]) [\text{C}]_0}{k_{-1}[\text{R}]^{1/2} + k_1[\text{Ox}]^{1/2} + (k_2[\text{Dr}] + k_{-2}[\text{Dx}])} + k_{-2}[\text{Dx}][\text{C}]_0 \quad (4-12)$$

Proceeding with the algebra, the first term to the right of the equals sign was divided by $(k_2[\text{Dr}] + k_{-2}[\text{Dx}])$. This gave:

$$\text{Rate} = \frac{-(k_1[\text{Ox}]^{1/2} + k_{-2}[\text{Dx}]) [\text{C}]_0}{\frac{k_{-1}[\text{R}]^{1/2} + k_1[\text{Ox}]^{1/2}}{(k_2[\text{Dr}] + k_{-2}[\text{Dx}])} + 1} + k_{-2}[\text{Dx}][\text{C}]_0 \quad (4-12)$$

Since it was assumed that $k_1 \geq k_{-1}$ (the validity of this assumption can be seen later) and from stoichiometric considerations $[\text{R}] \leq [\text{Dr}]_0$, the term $k_{-1}[\text{R}]^{1/2}$ was neglected in comparison to $k_1[\text{Ox}]^{1/2}$. This simplification was entirely justified, since $[\text{Ox}]_0 = 5 \times 10^{-3}$ and $[\text{Dr}]_0 \leq 2 \times 10^{-5}$. This simplification was applied and $[\text{C}]_0$ factored out to arrive at:

$$\text{Rate} = -[\text{C}]_0 \left[\frac{(k_1[\text{Ox}]^{1/2} + k_{-2}[\text{Dx}])}{k_1[\text{Ox}]^{1/2}} - k_{-2}[\text{Dx}] \right] \frac{1}{(k_2[\text{Dr}] + k_{-2}[\text{Dx}]) + 1} \quad (4-14)$$

Clearing fractions inside the brackets gave:

$$\text{Rate} = -[\text{C}]_0 \left[\frac{k_1[\text{Ox}]^{1/2} + k_{-2}[\text{Dx}] - \frac{k_1[\text{Ox}]^{1/2} k_{-2}[\text{Dx}]}{(k_2[\text{Dr}] + k_{-2}[\text{Dx}])} - k_{-2}[\text{Dx}]}{\frac{k_1[\text{Ox}]^{1/2}}{(k_2[\text{Dr}] + k_{-2}[\text{Dx}])} + 1} \right] \quad (4-15)$$

The $k_{-2}[Dx]$ terms in the numerator cancelled and $k_1[Ox]^{1/2}$ was factored out to give:

$$\text{Rate} = -k_1[Ox]^{1/2}[C]_0 \left[\frac{1 - \frac{k_{-2}[Dx]}{(k_2[Dr] + k_{-2}[Dx])}}{1 + \frac{k_1[Ox]^{1/2}}{(k_2[Dr] + k_{-2}[Dx])}} \right] \quad (4-16)$$

Again clearing fractions in both the numerator and denominator inside the brackets and cancelling out common terms led to:

$$\text{Rate} = -k_1[Ox]^{1/2}[C]_0 \left[\frac{k_2[Dr]}{k_1[Ox]^{1/2} + k_2[Dr] + k_{-2}[Dx]} \right] \quad (4-17)$$

Mass balance requires $[Dx] = [Dr]_0 - [Dr]$. This substitution gave the final overall catalyzed rate expression:

$$\text{Rate} = \frac{-k_1k_2[Ox]^{1/2}[Dr][C]_0}{k_1[Ox]^{1/2} + k_2[Dr] + k_{-2}[Dr]_0 - k_{-2}[Dr]} \quad (4-18)$$

Testing Validity of Simplified Mechanism

Determination of Constants

Rate constants were obtained using the program described in Chapter III. The required function of absorbance to be plotted versus a function of the derivative was obtained by algebraic manipulation of the rate expression, Equation 4-18.

Equation 4-18 was first re-written in the following manner:

$$\frac{\text{Rate}}{[C]_0} = \frac{-k_1 k_2 [Ox]^{\frac{1}{2}} [Dr]}{k_1 [Ox]^{\frac{1}{2}} + k_{-2} [Dr]_0 + k_2 [Dr] - k_{-2} [Dr]} \quad (4-19)$$

Grouping similar terms and inversion of both sides of the equation gave:

$$\frac{[C]_0}{\text{Rate}} = \frac{(k_1 [Ox]^{\frac{1}{2}} + k_{-2} [Dr]_0) + (k_2 - k_{-2}) [Dr]}{-k_1 k_2 [Ox]^{\frac{1}{2}} [Dr]} \quad (4-20)$$

Dividing both terms in the numerator of the right-hand side by the denominator led to:

$$\frac{[C]_0}{\text{Rate}} = \frac{(k_1 [Ox]^{\frac{1}{2}} + k_{-2} [Dr]_0)}{-k_1 k_2 [Ox]^{\frac{1}{2}} [Dr]} + \frac{(k_2 - k_{-2})}{-k_1 k_2 [Ox]^{\frac{1}{2}}} \quad (4-21)$$

Conversion to absorbance by application of Beer's Law considering a 1 cm path length led to:

$$\frac{[C]_0}{\text{rate}} = \frac{(k_1 \epsilon [Ox]^{\frac{1}{2}} + k_{-2} A_0)}{-k_1 k_2 \epsilon [Ox]^{\frac{1}{2}}} \cdot \frac{1}{A} + \frac{(k_2 - k_{-2})}{-k_1 k_2 \epsilon [Ox]^{\frac{1}{2}}} \quad (4-22)$$

The form of equation suggested a plot of $1/A$ versus $[C]_0/\text{rate}$

should be a straight line with slope = $\frac{(k_1 \epsilon [Ox]^{\frac{1}{2}} + k_{-2} A_0)}{-k_1 k_2 \epsilon [Ox]^{\frac{1}{2}}}$ and inter-

$$\text{cept} = \frac{-(k_2 - k_{-2})}{k_1 k_2 \epsilon [Ox]^{\frac{1}{2}}}$$

A new set of titration curves were obtained according to the procedure outlined in Chapter II using the fastest chart speed possible on the Cary 14 (8 inches/min) with hopes of improving resolution and accuracy of chart reading. The data was recorded, punched on IBM data cards, and read into the program for determining rate constants. Figure 23 shows selected plots of $1/A$ vs $[C]_0/\text{rate}$ and serves to illustrate the variation of slope with changing initial dye concentration and the relatively constant value of the intercept.

Consideration of the expressions for the slope and intercept showed the dependence of the slope upon initial absorbance. Letting $C_1 = \text{intercept}$ and $C_2 = \text{slope}$, the expression for the slope was written as:

$$C_2 = \frac{k_1 \epsilon [\text{Ox}]^{1/2} + k_{-2} A_0}{-k_1 k_2 \epsilon [\text{Ox}]^{1/2}} \quad (4-23)$$

or:

$$C_2 = -\frac{1}{k_2} - \frac{k_{-2} A_0}{k_1 k_2 \epsilon [\text{Ox}]^{1/2}} \quad (4-24)$$

Since:

$$C_1 = \frac{k_2 - k_{-2}}{-k_1 k_2 \epsilon [\text{Ox}]^{1/2}} \quad (4-25)$$

an expression was obtained for k_1 :

$$k_1 = \frac{k_2 - k_{-2}}{-C_1 k_2 \epsilon [\text{Ox}]^{1/2}} \quad (4-26)$$

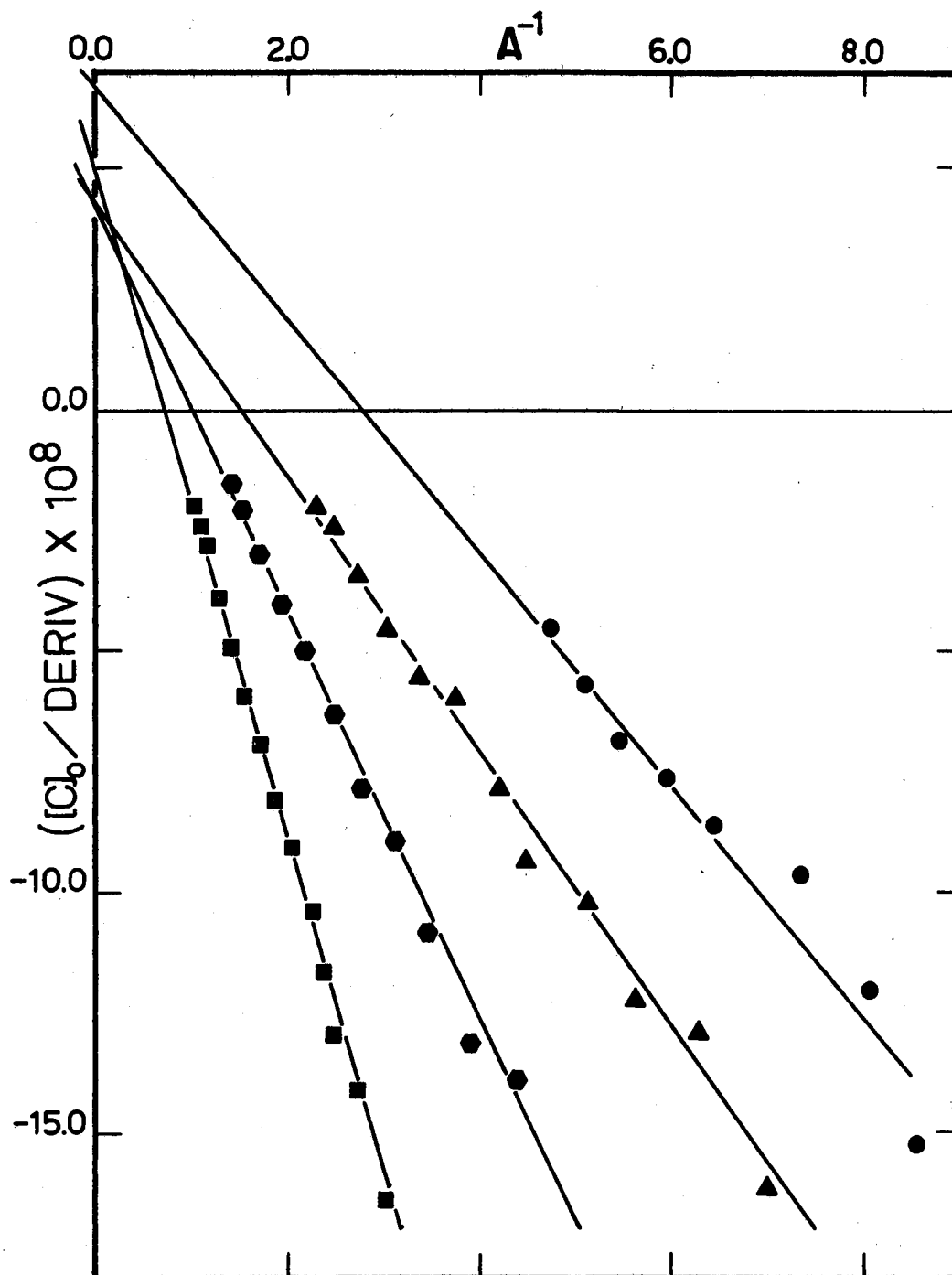


Figure 23. Variation of Slope as a Function of Initial Dye Concentration (See Appendix E, p. 124)

○ = 3.75×10^{-6} M
 △ = 7.77×10^{-6} M

◇ = 1.27×10^{-5} M
 □ = 1.68×10^{-5} M

Substitution of the expression for k_1 into Equation 4-24 led to:

$$C_2 = -\frac{1}{k_2} + \frac{k_{-2} A_o}{(k_2 - k_{-2}) C_1} \quad (4-27)$$

or finally:

$$C_2 = \frac{k_{-2}}{(k_2 - k_{-2})} \cdot C_1 A_o - \frac{1}{k_2} \quad (4-28)$$

A plot of C_2 versus $C_1 A_o$ proved to be a straight line with intercept equal to $-1/k_2$. This offered a method for the determination of k_2 . Figure 24 shows the plot used in the determination of k_2 , the forward rate constant for the reaction represented by Equation 4-5. Further, solving Equation 4-28 for k_{-2} gave:

$$k_{-2} = \frac{C_2 k_2 + 1}{C_1 A_o + C_2 + \frac{1}{k_2}} \quad (4-29)$$

This provided a method for obtaining a second constant, k_{-2} . Substitution of the values thus obtained for k_2 and k_{-2} into Equation 4-26, along with the mean value of all C_1 values gave the value for the third constant, k_1 . Complete listings of computer print-out of all the least squares fits of both raw data and for the determination of k_2 are given in Appendix E. A brief summary of the values found and their standard deviations is given in Table III.

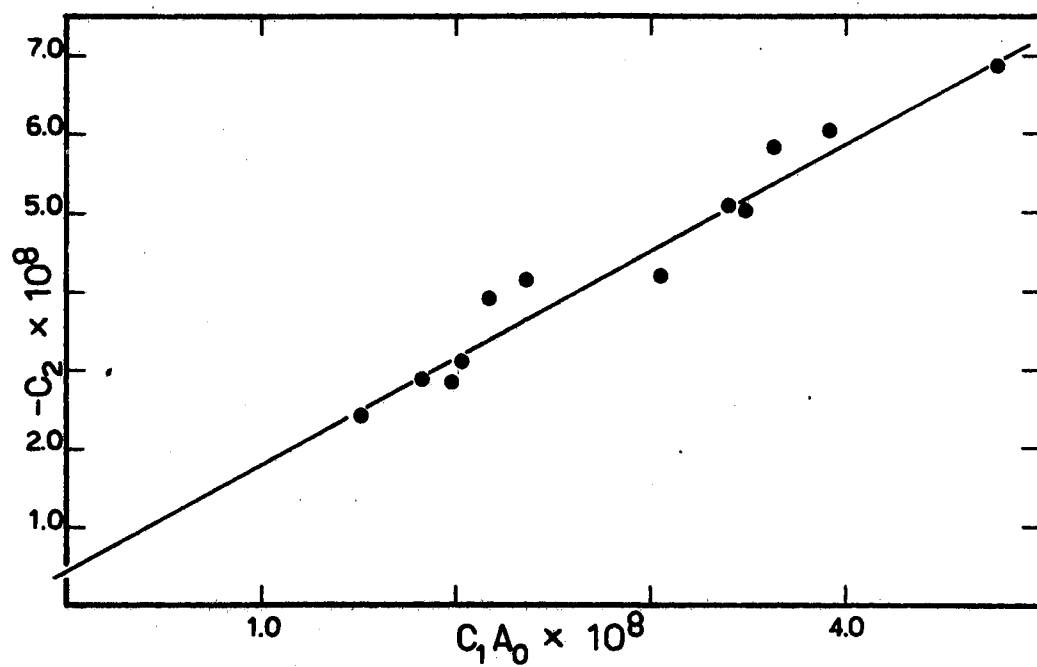


Figure 24. Determination of K_2 , the Forward Rate Constant for the Reaction Represented by Equation 4-5. Data Points Can be Found in Appendix E, p. 138

TABLE III
SUMMARY OF RATE CONSTANTS FOUND

Rate Constant	Value Found	Relative Standard Deviation (%)
k_1	$1.36 \times 10^4 \text{ M}^{-\frac{1}{2}} \text{ sec}^{-1}$	20.1
k_2	$2.24 \times 10^8 \text{ M}^{-1} \text{ sec}^{-1}$	66.2
k_{-2}	$8.43 \times 10^8 \text{ M}^{-1} \text{ sec}^{-1}$	7.58

It should be noted at this point that the large standard deviations reported here and in the NTA results to follow in the next section can be attributed to several factors, the most significant being the inherent error in using the intercept of a linear plot in the determination of parameters. Any statistics text, such as the one by Snedecor and Cochran (26) points out the poorer precision associated with the intercept of a linear plot when extrapolating long distances. Unfortunately, due to the nature of the modified rate equations, this offers the only means of obtaining an estimate of the rate constant, k_2 . Since the value found for k_2 is in turn used in the determination of the remaining system parameters, the error introduced here is carried throughout the determinations. The value reported for the standard deviation of k_{-2} is that of the slope of the linear plot mentioned above, since this is the basis of the determination of this constant. The statistical information reported for k_1 was obtained by calculating the sample standard deviation of the individual intercepts (C_1 in Equation 4-25). A recent review presents a detailed analysis of the problems encountered in using linear plots in the estimation of various parameters (27).

The assumption made earlier in the derivation of the rate expression can now be verified; i.e.--that $k_1 \geq k_{-1}$. The equilibrium constant for Equation 4-4 can be estimated from the standard potentials of the half-reactions and appears to be on the order of 10^6 . Since $K_{eq} = k_1/k_{-1}$, the values of K_{eq} and k_1 require k_{-1} to be much, much less than k_1 . The simplification made in Equation 4-14 appears as indeed valid under these conditions.

Computer Simulation of Experimental Curves

The curves used to obtain the constants discussed in the preceding section were simulated using the constants thus determined. Figure 25 shows selected curves at varying initial dye concentrations. A reasonable good fit was obtained, especially in the earlier portions of the curves. Handling of the observed induction period will be discussed in the following chapter.

Summary: Selection of a Simplified Mechanism

The steady-state approximation in the kinetics of the Mn(II) catalyzed oxidation of MG+ by periodate ion leads to an overall rate expression which satisfies both of the established criteria: (1) the constants determined are independent of initial dye concentration and (2) simulated curves match those experimental curves from which the constants were obtained.

HW(11)--PERIODATE SYSTEM: SIMULATION 35.02,03,08, & 09
DATA SET # 35.09

6/14/72

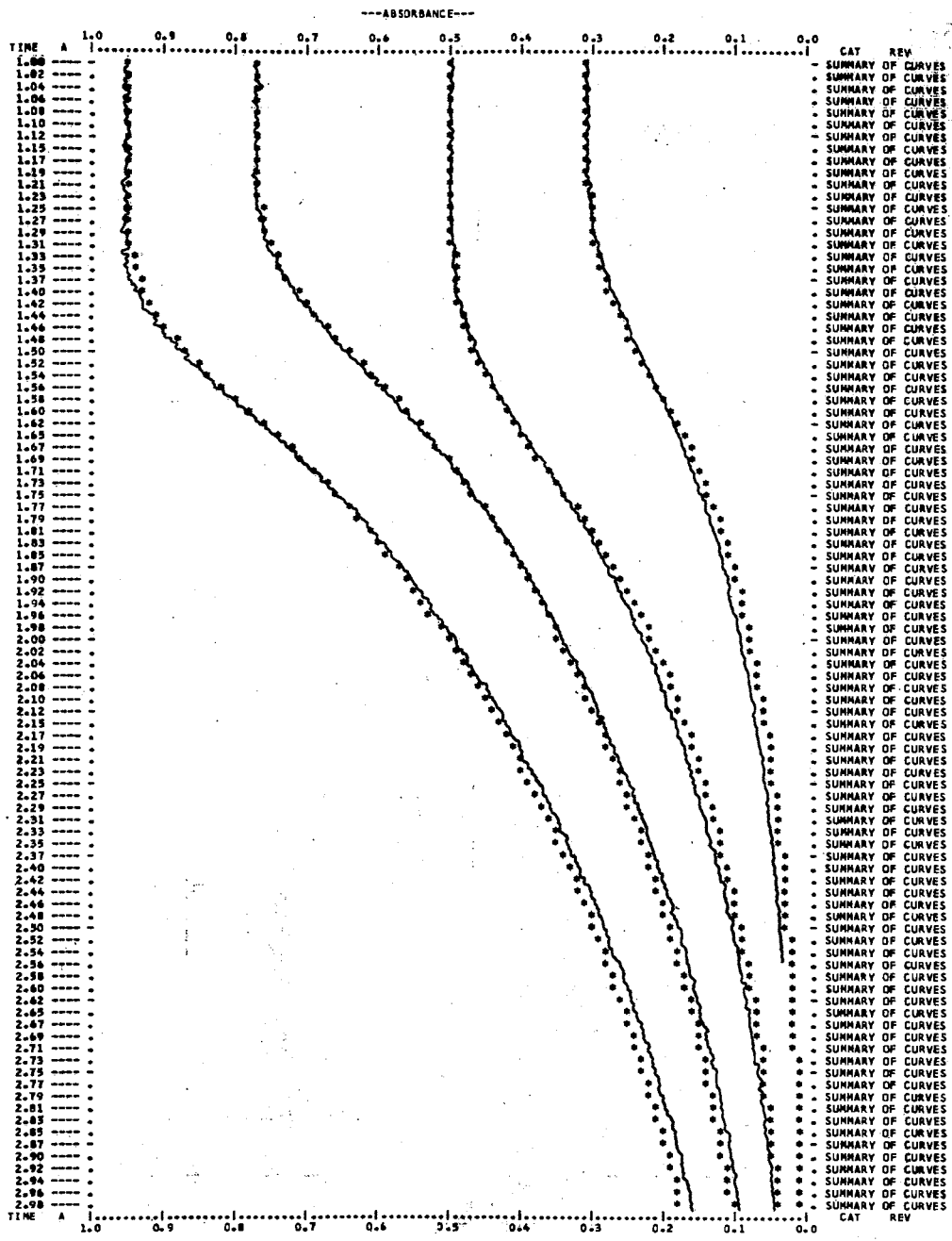


Figure 25. Computer Simulation of Experimental Curves Using Constants Obtained From Original Absorbance Versus Time Data. Solid Lines Represent Actual Experimental Curves While Asterisks Show Simulation Results. Experimental Conditions are Given in Appendix E, p. 124

The Modifying Effect of NTA on the Mn(II)
Catalyzed Oxidation of Malachite
Green Cation by Periodate Ions

Selection of a Simplified Mechanism

It was known that the addition of NTA (nitrilotriacetic acid) to the Mn(II)-MG⁺-periodate system noticeably increased the rate of the reaction (9,11,21,23). The problem was to select a simplified mechanism which could be used to describe what was occurring in the system. The large formation constant of the Mn(III)-NTA complex (28) suggested strongly the possibility that this was the active species. The mechanism selected, then, for describing the NTA effect, was exactly the same as that used when NTA was not present.

Development of Expressions for the Selected Mechanism

In this case, the reaction path was considered to be the following:



where:



This set of equations describing the mechanism of reaction was

treated in exactly the same manner as was done with the same system without NTA, with the exception that the term $[Cx]$ is replaced everywhere it appears with the term $[CxL]$. This substitution was valid due to the relatively large formation constant reported for the Mn(III)-NTA complex (28) and the magnitude of the difference between this value, $K_F = 1.8 \times 10^{20}$, and that for the formation of the Mn(III)-Acetate complex which is probably no larger than 10^{14} (see Appendix F for method of estimation). With an acetate concentration of about 0.5 M, due to the use of an acetate buffer, equilibrium calculations showed that virtually all of any Mn(III) present in the system would be complexed by the NTA as long as the formation constant for the Mn(III)-Acetate complex was no greater than about 10^{14} . Since all runs were done with an excess of NTA present, the limiting reagent in the formation of the complex was Cx, the concentration of Mn(III). Constants were also determined in an identical manner with the pertinent results summarized in Table IV. Complete listings of all computer print-out of the least square fits are given in Appendix G.

TABLE IV
SUMMARY OF RATE CONSTANTS DETERMINED FOR NTA EFFECT

Rate Constant	Value	Relative Standard Deviation (pph)
k_1^*	$4.20 \times 10^5 \text{ M}^{-1/2} \text{ sec}^{-1}$	37.7
k_2^*	$3.07 \times 10^8 \text{ M}^{-1} \text{ sec}^{-1}$	24.7
k_{-2}^*	$5.47 \times 10^9 \text{ M}^{-1} \text{ sec}^{-1}$	11.8

Figure 26 shows the results of computer simulation of the curves used to obtain the constants given above. All showed a good match when compared to the experimental curves.

Summary: Selection of Simplified Mechanism Describing NTA Effect

Making the steady-state approximation on the time-rate of change of Mn(III)-NTA complex concentration leads to an overall rate equation which meets both of the established criteria. The constants were not seen to vary with changes in dye concentration and the curves simulated by the computer matched the experimental curves. Again, the handling of the induction period will be discussed in the following chapter.

CHEM SCLD--B.E. SIMPSON

COPY 2 OF 2

MN(11)--PERIODATE SYSTEM: SIMULATION: MG-34 (INTA ADDED)

6/12/72

DATA SET = 34-14

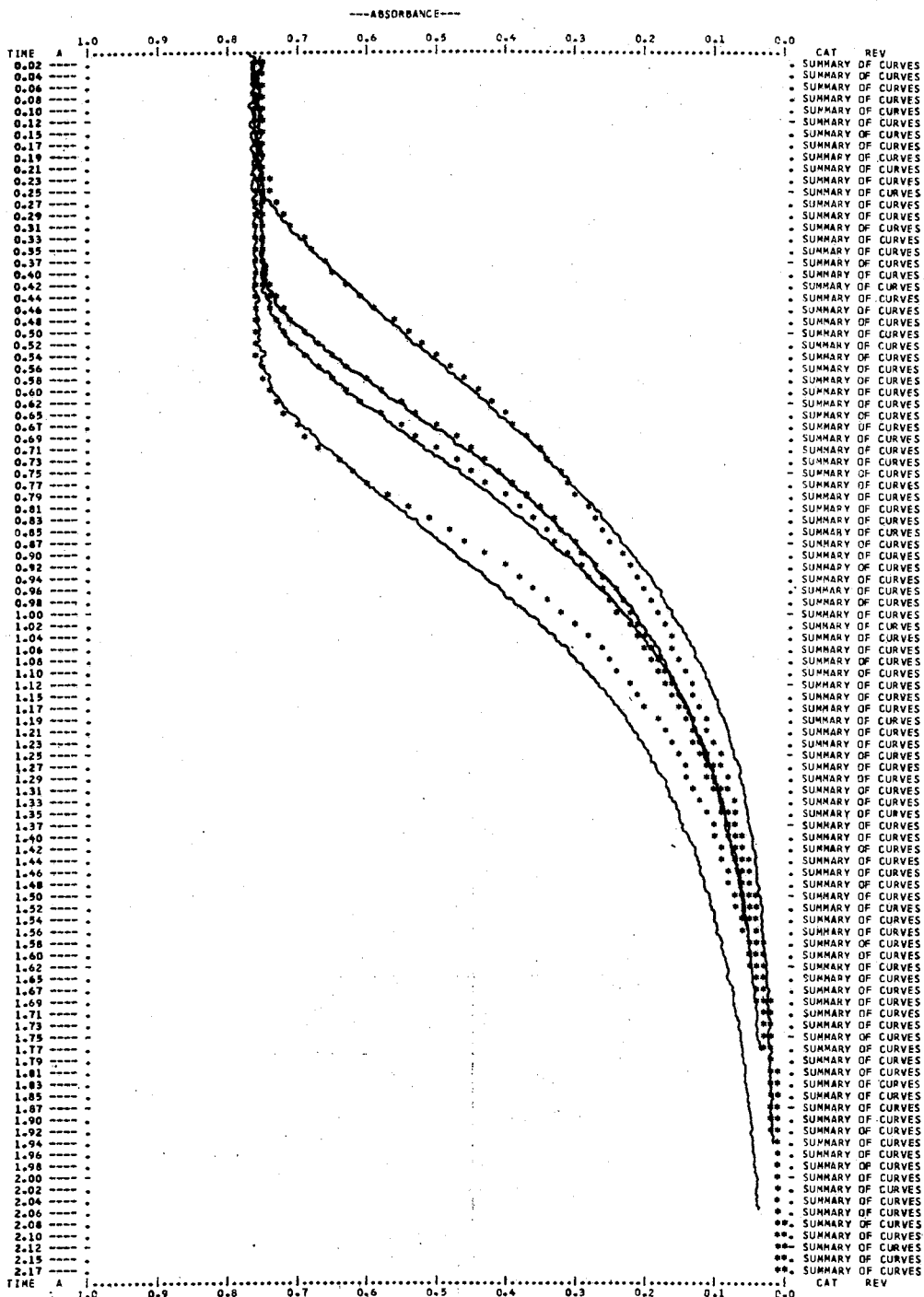


Figure 26. Computer Simulation of Experimental Curves Using Constants Obtained From Original Absorbance Versus Time Data. Solid Lines Represent Actual Experimental Curves While Asterisks Show Simulation Results. Experimental Conditions are Given in Appendix G, p. 146

CHAPTER V

SUMMARY OF RESULTS, DISCUSSIONS, AND SUGGESTIONS FOR FURTHER STUDY

Results

Most numerical results have already been presented in the text of the thesis and in the various appendices. Summarizing statements only will be presented here.

The overall goals of the study have been accomplished: i.e.--development of computer programs to determine system parameters and simulate catalytic titration curves and the application of these programs to the study of a real system. In addition, new equipment necessary to adapt catalytic titrations to the Cary 14 spectrophotometer were designed, built, and tested. The utility of using experimentally determined instantaneous derivatives to derive information from catalytic titration was demonstrated as was the application of simple, first order, linear least squares methods to the study of reaction kinetics. Further, it was shown that the programs developed can be used in attempts to test mechanistic assumptions, and, indeed, were used to show how the steady-state approximation can be used to describe a real system: namely, the Mn(II) catalyzed oxidation of MG⁺ by periodate ion both with and without the presence of a particular complexing agent, NTA.

Discussion

One problem encountered in the study was the treatment of the induction period which was observed after introduction of the catalyst. This period of time varied from a few seconds in the case of large NTA concentration to over a minute in other cases. The only correlation with any physical or chemical variable was the dependence upon NTA concentration as has already been observed by Mottola and Harrison (11). In the absence of complexing agent, however, the length of the induction period seemed to be independent of everything and would sometimes vary from one run to the next by as much as 10 - 20 seconds. Part of this variation could be attributed to error in determining exactly when the catalyst solution actually entered the system, as this was accomplished by means of a mark on the tip of the buret and a stopwatch. Error from this source, however, could not possibly contribute more than ± 3 seconds.

In the realm of possible explanations, two extremes exist: (1) the catalyst is tied up by some agent present in the system for a given amount of time, then released suddenly into the system after a period of time or (2) a given amount of catalyst equal to the rate of catalyst times the length of induction period is tied up by some agent and is never released during the reaction. The latter extreme would essentially mean that, as far as catalyst added to the system is concerned, time = 0 at the point where the break first occurs in the curve. This extreme was ruled out, since the plot of $-C_2$ vs. C_1A_0 shown in Figure 24 (see page 83, this work) did not give a slope greater than 1.0, as is required by Equation 4-28. That is, the term $\frac{k_{-2}}{k_2 - k_{-2}}$ must be larger

than 1.0 if $k_{-2} > k_2$. The negative slope of the C_2 vs. C_1A_0 verifies that $k_{-2} > k_2$, due to the term $(k_2 - k_{-2})$.

On the other hand, possibility number one gave quite good fits with the exception of the early parts of the curves. The real problem in accepting this assumption as it stood, however, was the failure in attempts to simulate experimental curves. Simulated curves showed a sharp break at the point where catalyst first became available while actual experimental curves exhibited a gentle arc (see Figure 25). Simulation, then, seemed to indicate that after a certain time, the catalyst available for reaction was indeed equal to the total amount of catalyst added, $[C]_0$, but before that time was represented by some other function. Figure 27 shows a plot of available catalyst concentration versus time superimposed over a typical absorbance versus time catalytic titration curve. In the figure, T_1 represents the time when catalyst first becomes available to the system and T_2 represents the time when the available catalyst concentration becomes equal to the total amount of catalyst added to the system. The broken line represents the amount of catalyst actually added to the system at any time. Time equals zero when the buret containing catalyst is turned on. The portion of the available catalyst curve between T_1 and T_2 was approximated empirically with the following parabolic function:

$$C = a(t - T_1)^2 \quad (5-1)$$

If $C = k_a t$ at $t = T_2$, where k_a = catalyst addition rate, then solving equation 5-1 for the constant, a , gave:

$$a = \frac{C}{(T_2 - T_1)^2} = \frac{k_a T_2}{(T_2 - T_1)^2} \quad (5-2)$$

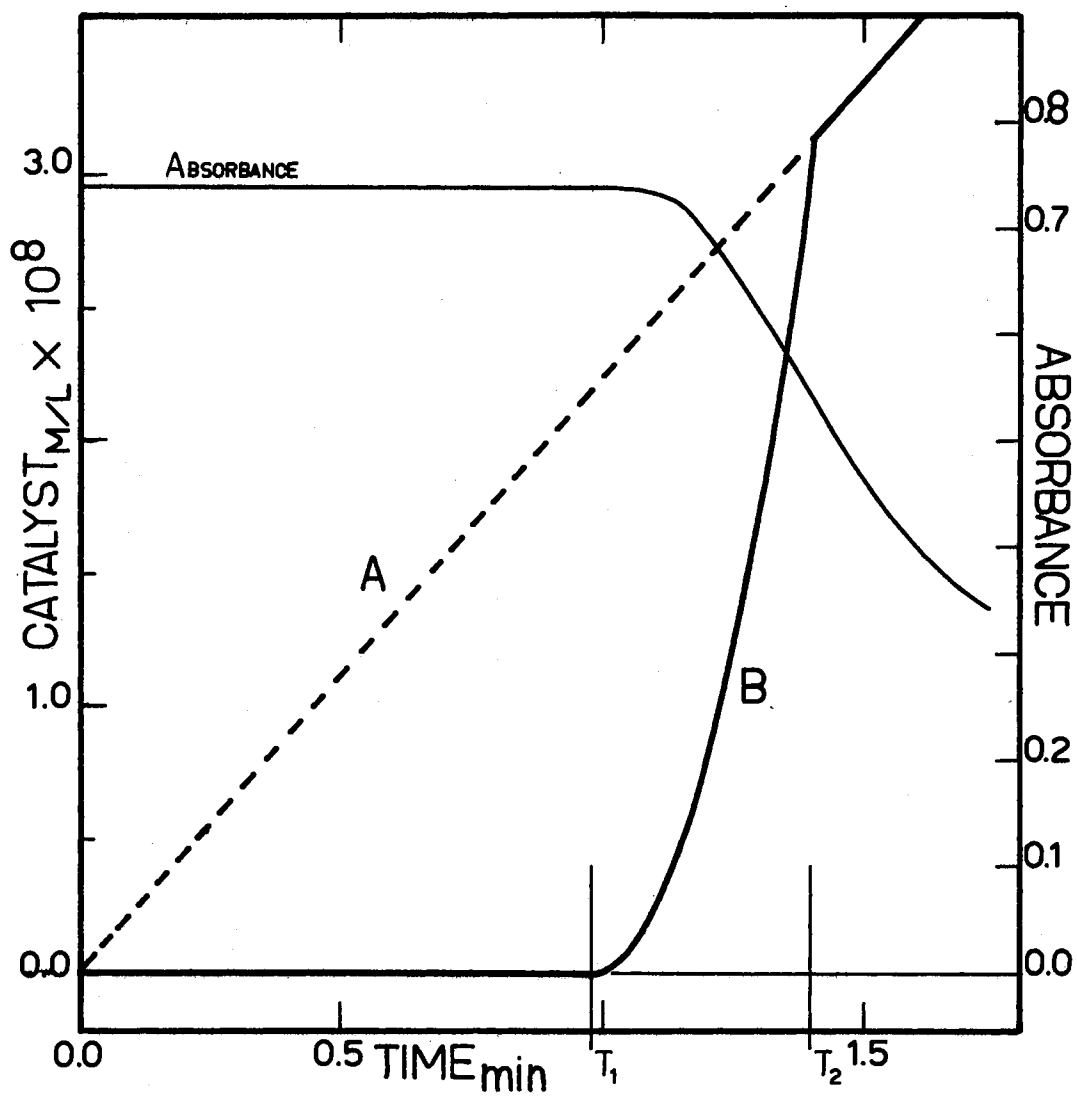


Figure 27. Available Catalyst Concentration. Curve A: Catalyst Actually Added to System. Curve B: Catalyst Available to System for Participation in Reaction. Corresponding Absorbance is Also Shown

This led to the final expression used to empirically explain the available catalyst concentration:

$$C = \frac{k_a T_2}{(T_2 - T_1)^2} (t - T_1)^2 \quad \left. \begin{array}{l} t = T_2 \\ t = T_1 \end{array} \right\} \quad (5-3)$$

The only valid defense of this approach is the fact that use of this expression led to an improved linearity in the plots of $1/A$ vs. $[C]_0/\text{rate}$ and gave an almost perfect match of simulated and experimental curves in many cases. Both T_1 and T_2 can be determined directly from experimental curves: T_1 being that time when the first deviation from the uncatalyzed reaction is observed and T_2 being the time at the point of inflection of the catalytic titration curve. The computer output given in Appendix E and referred to earlier (page 83, this work) gives the values of T_1 and T_2 used in each case.

Other empirical functions were considered, namely an exponential function of the form:

$$C = b e^{a(t - T_1)} \quad (5-4)$$

but were abandoned when they failed to give an improvement in linearity better than that achieved with the parabolic assumption.

It should be mentioned that the correction employed using T_1 and T_2 was necessary only in the case of simulation, since constants can be determined, if need be, from only the latter portions of a titration curve. For the sake of consistency, however, these corrections were included in both simulation and constant determination programs.

Suggestions for Further Work

One of the most obvious places where further study would be profitable would be in the area of the induction period. Various types of experiments done with various ligand and buffer systems similar to those conducted by Rudenko and co-authors (20) could lead to a better understanding of what is taking place. The seeming independence of the induction upon initial dye concentration and its aforementioned reliance upon NTA concentration would indicate the answer to the induction period problem lies somewhere in the formation of some metal-ligand complex which, for some reason, decays rapidly after a period of time equal to the induction period. Better knowledge of the oxidation potentials of the various reactions occurring in the system could be the key to understanding the "avalanche" change of available catalyst concentration from zero to the maximum possible in a period of a few seconds. Further, the effect caused by increasing NTA concentration would seem to be a result of mass action; as if the NTA were "taking away" the catalyst from some other species which was keeping it from participating in the catalytic cycle.

Another area where further work is called for is in the study of the effect of different ligands upon the system, especially one which inhibits the course of the reaction. A study of the pH dependence of inhibition or rate-increase would also serve to provide more information as to the "true" mechanism of ligand modification.

In conclusion, the primary analytical reasons for undertaking this study may be pin-pointed as follows. First, a study of this type can lead to better understanding of a widely used analytical system, and, consequently, to improved methods of analysis. Secondly, the area of

catalytic titration curves deserves attention. Since the introduction of these methods (1, 9, 11, 21, 22, 23), a computer study such as this present work has not been undertaken. Use of the digital computer to characterize the reactions used in catalytic end-point determination can lead to better methods of end-point determination and a more lucid interpretation of what is occurring at the theoretical equivalence point.

Third, and finally, a study such as this seems to lend itself to the tracing of metal chelate catalysis, promotion, and inhibition which is of much importance not only in the area of analytical chemistry, but also in bio-chemical applications in which oxygen and nitrogen containing ligands play an important role. It is hoped that the computer programs, methods of analysis, and technical apparatus presented in this work will make a valid contribution to the above mentioned areas.

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APPENDIXES

APPENDIX A

CHECK OF INTEGRATION TECHNIQUE

Check of Simulation

In order to check the accuracy of the simulated curves, a differential rate equation was solved rigorously and the resulting function of time, t , plotted. The test equation used was that developed in Chapter III to express the rate of the reaction assuming the pre-equilibrium mechanism:

$$\begin{aligned} \text{Rate} &= \text{uncatalyzed rate} + \text{catalyzed rate} \\ &= \frac{dA}{dt} = -k_u A - k_c A(C)_o \end{aligned} \quad (\text{A-1})$$

where:

$$\begin{aligned} A &= \text{absorbance} \\ k_u &= k_{\text{uncat}}(Ox) = \text{constant (since } (Ox) \text{ is constant),} \\ k_c &= k_2 = \text{catalyzed rate constant, and} \\ (C)_o &= Ct = \text{(catalyst addition rate)(time).} \end{aligned}$$

Proceeding with the solution:

$$\frac{dA}{dt} = -k_u A - k_c A C t \quad (\text{A-2})$$

$$\frac{dA}{A} = -k_u dt - k_c C t dt \quad (\text{A-3})$$

$$\int \frac{dA}{A} = -k_u \int dt - k_c C \int t dt \quad (\text{A-4})$$

$$\ln A + \ln B = -k_u t - \frac{1}{2} k_c C t^2 \quad (\text{A-5})$$

where: $\ln B$ contains all constants of integration

$$\ln AB = -k_u t - \frac{1}{2} k_c C t^2 \quad (\text{A-6})$$

$$AB = e^{-k_u t} \cdot e^{-\frac{1}{2} k_c C t^2} \quad (\text{A-7})$$

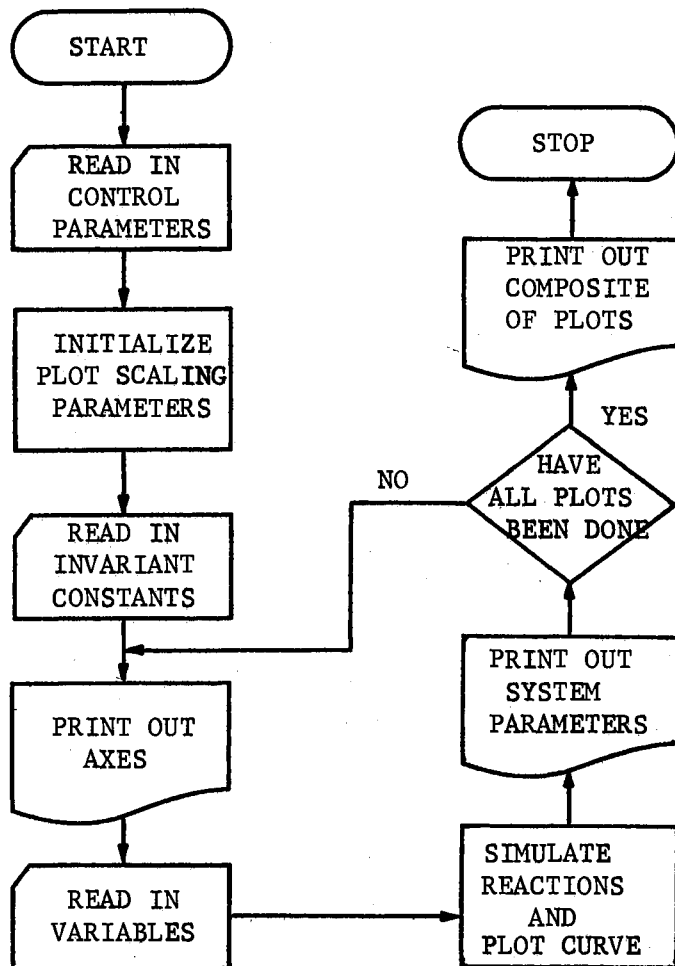
At $t = 0$, $B = \frac{1}{A} = \frac{1}{A_0}$, therefore:

$$A = A_0 (e^{-k_u t} \cdot e^{-\frac{1}{2} k_c C t^2}) \quad (\text{A-8})$$

Comparison of the curve plotted with this function with one simulated using the same parameters showed that they are identical. This favorable comparison shows that the integration technique used in the simulation does a good job of producing a curve, given a differential equation expressing the rate.

APPENDIX B

FLOW DIAGRAM AND SOURCE PROGRAM FOR SIMULATION



GIVEN THE SYSTEM PARAMETERS, THIS PROGRAM SIMULATES A CATALYTIC TITRATION CURVE BY PRODUCING A PLOT OF ABSORBANCE VS. TIME. THE PRINTOUT IS A 1:1 REPRODUCTION OF THE STRIPCHART FROM THE CARY 14 SPECTROPHOTOMETER. VALUES OF TIME, ABSORBANCE, AND CONTRIBUTIONS OF BOTH THE FORWARD AND REVERSE REACTIONS TO THE OVERALL RATE ARE ALSO TABULATED FOR EACH POINT.

A BREAKDOWN OF THE PROGRAM SEGMENTS AND THEIR FUNCTION FOLLOWS:

MAIN: 1) READS IN THE NUMBER OF PLOTS TO BE DONE.
2) CALLS ALL OTHER SUB-PROGRAMS.
3) HANDLES TIME INCREMENTING AND KEEPS TRACK OF THE DEPENDENT VARIABLE.

AINPUT: 1) READS IN ALL PARAMETERS WHICH DO NOT VARY WITH SUCCESSIVE PLOTS.

BINPUT: 1) READS IN THOSE PARAMETERS WHICH CHANGE WITH SUCCESSIVE PLOTS.

AXIS: 1) READS IN AND PRINTS OUT THE LABEL FOR EACH PLOT.
2) PRINTS OUT OPINATE AXES BEFORE AND AFTER EACH PLOT.

PLOT: 1) DOES THE ACTUAL PLOTTING OF POINTS.
2) PRINTS OUT TIME, ABSORBANCE, FORWARD REACTION CONTRIBUTION, AND REVERSE REACTION CONTRIBUTION.

AMODEL: 1) DEFINES THE SYSTEM MODEL.
2) CONTAINS THE INTEGRATION TECHNIQUE.

OUTPUT: 1) PRINTS OUT THE SYSTEM PARAMETERS.

CHART: "SAVES" EACH INDIVIDUAL PLOT AND PRINTS OUT A COMPOSITE GRAPH.

SEE SUB-PROGRAMS FOR FURTHER COMMENTS AND DEFINITION OF VARIABLES.

DEFINITION OF VARIABLES APPEARING IN MAIN PROGRAM:

A: ABSORBANCE AT ANY TIME
A1: CORRECTED ABSORBANCE (EQUALS A -1.0 IF A.GT.1.0)
ASTART: INITIAL ABSORBANCE OF THE DYE IN SOLUTION
ADELT: INCREMENT IN ABSORBANCE PER UNIT OF TIME RESULTING FROM PROGRESS OF REACTION
CAT: FORWARD CONTRIBUTION TO THE OVERALL RATE
CATCON: CATALYST CONCENTRATION AVAILABLE TO THE SYSTEM AT ANY TIME
CATREV: CONTRIBUTION TO OVERALL RATE FROM REVERSE REACTION
CHECK: VARIABLE USED TO DETERMINE MAGNITUDE OF STEP SIZE IN INTEGRATION ROUTINE (USED ONLY WHEN KPROD.GT.0)
CLIG: CONCENTRATION OF LIGAND AT ANY TIME (USED ONLY WHEN CONTRIBUTION EXPECTED FROM BOTH LIGAND EFFECT AND NORMAL PATH)
CLIG1: INITIAL CONCENTRATION OF LIGAND ADDED TO SYSTEM (USED UNDER SAME CONDITIONS AS CLIG)
DELTIM: VALUE COMPUTED FROM "TDELTM" WHEN VARIABLE STEP SIZE REQUIRED BY THE PROGRAM
EPS: MOLAR ABSORPTIVITY OF THE DYE BEING USED
IGRID: ARRAY FOR SAVING THE INDIVIDUAL PLOTS
INCAT: RATE OF CATALYST ADDITION IN MOLES/LITER.MIN
ISCALE: DESIRED SCALE OF PLOT IN INCHES PER MINUTE
KEQ: EQUILIBRIUM CONSTANT (USED ONLY WHEN PRE-EQUILIBRIUM MECH ASSUMED)
KFORM: FORMATION CONSTANT OF COMPLEX OF LIGAND WITH CATALYST (USED ONLY WHEN CONTRIBUTION EXPECTED FROM BOTH LIGAND EFFECT AND NORMAL CATALYTIC CYCLE)
KICK: VARIABLE USED TO ADJUST STEP SIZE IN INTEGRATION ROUTINE
KNEG2: RATE CONSTANT FOR REVERSE REACTION IN SECOND STEP OF MECHANISM
KPRO: RATE CONSTANT FOR PROMOTION REACTION (USED ONLY WHEN A CONTRIBUTION FROM BOTH LIGAND EFFECT AND NORMAL CATALYTIC CYCLE IS EXPECTED)
KUNCAT: RATE CONSTANT FOR UNCATALYZED REACTION
K1: RATE CONSTANT FOR FIRST STEP IN REACTION MECHANISM
K2: RATE CONSTANT FOR FORWARD REACTION IN SECOND STEP OF MECHANISM
LABEL: ANY LABEL UP TO 80 CHARACTERS LONG TO BE PRINTED WITH PLOT
MAXTIM: MAXIMUM TIME ALLOWED FOR A GIVEN PLOT
OX: CONCENTRATION OF OXIDIZING AGENT IN MOLES/LITER
PROMO: RATE CONTRIBUTION DUE TO PROMOTION OF THE LIGAND (USED ONLY WHEN CONTRIBUTION EXPECTED FROM BOTH LIGAND AND NORMAL CYCLES)
REF: DATA IDENTIFIER

SAVE,SAVE1,SAVE2,SAVE3: VARIABLES USED TO SAVE THE VALUES OF GIVEN PARAMETERS WHICH MUST BE SET TO ZERO DURING ANY UNCATALYZED PORTION OF THE REACTION.
STD: ARRAY CONTAINING VALUES ASSIGNED TO VARIABLES IN "VAR"
TERM: VARIABLE NEED IN SYSTEM MODEL--CALCULATED IN MAIN PROGRAM TO SAVE EXECUTION TIME
TDELTM: TIME INCREMENT USED IN THE INTEGRATION ROUTINE
TIME: TIME FROM INTRODUCTION OF CATALYST INTO SYSTEM
T1: TIME WHEN CATALYST FIRST BECOMES AVAILABLE TO THE SYSTEM
T2: TIME WHEN TOTAL ANALYTICAL CATALYST CONCENTRATION IS AVAILABLE
UNRUN: THE NUMBER OF MINUTES OF UNCATALYZED REACTION TO BE SIMULATED
VAR: ARRAY CONTAINING STANDARD VALUES OF GIVEN PARAMETERS TO BE VARIED DURING A RUN

IMPLICIT REAL*8(A-H,O-Z)
REAL*8 KUNCAT,K1,K2,KNEG2,KEQ,INCAT,KPRO,KFORM
REAL*4 LABEL,VAR,STD
COMMON OX,CLIG,CLIG1,EPS,TDELTM,INCAT,ASTART,KUNCAT,K1,K2,KNEG2,
KPRO,KFORM,KEQ,UNRUN,DELTIN,T1,T2,ISCALE,MAXTIM
DIMENSION IGRID(200,10),STD(10),VAR(10,2),LABEL(20)
DATA IGRID/200*10/
A1=1.0
DD 15 IREAD=1,10
15 READ(5,253)VAR(IREAD,1),VAR(IREAD,2),STD(IREAD)
READ(5,251)NSETS,NUMCOP
CALL AINPUT
SCALE=ISCALE
MAX=MAXTIM*6*ISCALE
MAXUN=(UNRUN+0.0001)*6*ISCALE
INNERI=24/ISCALE
LOCATE=1
DO 10DD ISETS=1,NSETS
LINE5=1
READ(5,252)NUMRUN,LABEL
DO 111 IRUN=1,NUMRUN
CATCON=0.000
CAT=0.000
PROMO=0.000
CATREV=0.000
K=0
KK=0
WRITE(6,300)
CALL BINPUT(REF)
CALL AXIS(LABEL,REF,LOCATE)
TERM=K1*EPS*DSQRT(OX)
A=ASTART
TIME=0.000
SAVE=TERM
SAVE1=KPRO
SAVE2=KNEG2
SAVE3=K2
TERM=0.00
KPRO=0.000
KNEG2=0.00
K2=C.00
IF(MAXUN.EQ.C)GO TO 9
INNER=INNERI
TDELTM=DELTIM
6 DD 7 ILDOP=1,MAXUN
DD 8 IDELT=1,INNER
TIME=TIME+TDELTM
CALL AMODEL(A,CATCON,UNCAT,CAT,CATREV,PROMO,ADELT,TIME,TERM)
8 A=A+DELT
CALL PLOT(A,K,TIME,CAT,CATREV)
A1=A
IF(A1.GT.1.00)A1=A1-1.00
IGRID(ILDOP,IRUN)=101.49999-A1*100.
7 CONTINUE

```

9 MLOOP=MAXUN+1
  TERM=SAVE
  KPRO=SAVE1
  KNEG2=SAVE2
  K2=SAVE3
  CHECK=KPRO
  IF(K2.GT.KPRO)CHECK=K2
  KICK=(DLOG10(CHECK)-6.000)
  IF(KICK.LT.1)KICK=1
  IF(KICK.GT.10)KICK=10
  KICK=2
  INNER=INNER1*KICK
  TDEL=DELTIM/KICK
  DO 10 ILOOP=MLOOP,MAX
  DO 11 IDELT=1,INNER
  TIME=TIME+TDELT
  CATCON=INCAT*T2*(TIME-T1)**2/(T2-T1)**2
  IF(TIME.LT.T1)CATCON=0.00
  IF(TIME.GE.T2)CATCON=INCAT*TIME
  CALL AMODEL(A,CATCON,UNCAT,CAT,CATREV,PROMO,ADELT,TIME,TERM)
  A=A+ADELT
  IF(ADELT.GT.0.000)GO TO 12
11 CONTINUE
  CALL PLOT(A,K,TIME,CAT,CATREV)
  IF((DABS(A1-A).LT.1.D-4).AND.((TIME-UNRUN).GT.4.00))GO TO 12
  IF(A.LT.0.00500)GO TO 12
  A1=A
  IF(A1.GT.1.00)A1=A1-1.00
  IGRID(ILOOP,IRUN)=101.49999-A1*100.
13 CONTINUE
12 IF(ILOOP.GT.LINES)LINES=ILOOP
  CALL PLOT(A,K,TIME,CAT,CATREV)
  CALL AXIS(LABEL,REF,LOCATE)
  CALL OUTPUT(IRUN,INNER)
111 CONTINUE
  IF(NUMCDP.EQ.0)GO TO 1000
  DO 112 KOPY=1,NUMCDP
  WRITE(6,301)KOPY,NUMCDP
  CALL AXIS(LABEL,REF,LOCATE)
  CALL CHART(IGRID,NUMRUN,LINES,SCALE,VAR,STD,KOPY)
  CALL AXIS(LABEL,REF,LOCATE)
112 CONTINUE
  DO 1001 ISTUFF=1,LINES
  DO 1001 JSTUFF=1,NUMRUN
  IGRID(ISTUFF,JSTUFF)=101
1001 CONTINUE
1000 CONTINUE
  WRITE(6,300)
  STOP
251 FORMAT(2I3)
252 FORMAT(1I3/20A4)
253 FORMAT(2A4,E10.3)
300 FORMAT(1H1,'CHEM 5000--B.E. SIMPSON'//)
301 FORMAT(1H1,'CHEM 5000--B.E. SIMPSON',T115,'COPY',I3,' OF',I3//)
  END

```

SUBROUTINE AINPUT

THIS SUB-PROGRAM READS IN THOSE VARIABLES WHICH ARE CONSTANT FOR A GIVEN SET OF DATA. VARIABLE NAMES ARE THE SAME AS THOSE LISTED IN THE MAIN PROGRAM.

```

IMPLICIT REAL*8(A-H,O-Z)
REAL*8 KUNCAT,K1,K2,KNEG2,KEQ,INCAT,KPRO,KFORM
COMMON DX,CLIG,CLIG1,EPS,TDELT,INCAT,ASTAR,KUNCAT,K1,K2,KNEG2,
$KPRO,KFORM,KEQ,UNRUN,DELTIM,T1,T2,ISCALE,MAXTIM
READ(5,252)ISCALE,MAXTIM,DELTIM,INCAT,KUNCAT,DX,EPS,KPRO,KFORM,
$KEQ,UNRUN,K1,K2,KNEG2
CLIG1=D.D0
CLIG=D.D0
252 FORMAT(2I3/(E10.3))
RETURN
END

```

SUBROUTINE BINPUT(REF)

THIS SUB-PROGRAM READS IN THOSE VARIABLES WHICH CHANGE WITH SUCCESSIVE PLOTS. SEE MAIN PROGRAM COMMENTS FOR VARIABLE NAMES DEFINITION.

```

IMPLICIT REAL*8(A-H,O-Z)
REAL*8 KUNCAT,K1,K2,KNEG2,KEQ,INCAT,KPRO,KFORM
COMMON DX,CLIG,CLIG1,EPS,TDELT,INCAT,ASTAR,KUNCAT,K1,K2,KNEG2,
$KPRO,KFORM,KEQ,UNRUN,DELTIM,T1,T2,ISCALE,MAXTIM
READ(5,250)REF,ASTAR,T1,T2
250 FORMAT(F10.0/F10.0/2F10.0)
RETURN
END

```

SUBROUTINE OUTPUT(IRUN,INNER)

THIS SUB-PROGRAM PRINTS OUT SELECTED SYSTEM PARAMETERS. SEE MAIN PROGRAM FOR VARIABLE NAME DEFINITION.

```

IMPLICIT REAL*8(A-H,O-Z)
REAL*8 KUNCAT,K1,K2,KNEG2,KEQ,INCAT,KPRO,KFORM
REAL*4 KSTAR
COMMON DX,CLIG,CLIG1,EPS,TDELT,INCAT,ASTAR,KUNCAT,K1,K2,KNEG2,
$KPRO,KFORM,KEQ,UNRUN,DELTIM,T1,T2,ISCALE,MAXTIM
KODE=IRUN
IF(KODE.EQ.10)KODE=0
WRITE(6,350)TDELT,INNER,INCAT,ASTAR,KUNCAT,KPRO,K1,K2,KNEG2
$KEQ,KFORM,DX,UNRUN,KODE
350 FORMAT(1H1,10X,'SYSTEM PARAMETERS:'//)
$11X,'TDEL=' ,I PD13.6//
$11X,'NUMBER OF ITERATIONS FOR EACH POINT=' ,I3//
$11X,'INCAT=' ,D13.6//
$11X,'ASTAR=' ,D13.6//
$11X,'KUNCAT=' ,D13.6//
$11X,'KPRO=' ,D13.6//
$11X,'K1=' ,D13.6//
$11X,'K2=' ,D13.6//
$11X,'K-2=' ,D13.6//
$11X,'KEQ=' ,D13.6//
$11X,'KFORM=' ,D13.6//
$11X,'DX=' ,D13.6//
$11X,'NUMBER OF MINUTES OF UNCATALYZED REACTION=' ,DPP6.3//
$11X,'THE CODE FOR THIS REACTION ON THE COMPOSITE' ,/11X,'GRAPH AT' ,
$' THE END OF THIS SET OF OUTPUT IS: >>>---> ',I2)
RETURN
END

```

```

C
C
C
C
C
SUBROUTINE AXIS(TITLE,REF,LOCATE)
    THIS SUB-PROGRAM PRINTS THE PROPER LABELS AND AXES FOR EACH PLOT.

    DIMENSION TITLE(20)
    GO TO (20,30),LOCATE
20  WRITE(6,295)TITLE,REF
    WRITE(6,296)
    WRITE(6,297)
    WRITE(6,305)
    LOCATE=2
    GO TO 40
30  WRITE(6,305)
    WRITE(6,297)
    WRITE(6,296)
    LOCATE=1
40  RETURN
295 FORMAT(1X,20A4,/,1X,'DATA SET = ',F10.2)
296 FORMAT(1X,F5.0,' ---ABSORBANCE---/')
297 FORMAT(11X,'1.0      0.9',
$      ' 0.8      0.7      0.6      0.5      0.4      0.3',
$      ' 0.2      0.1      0.0')
305 FORMAT(1X,'TIME  A |.....|.....|.....|.....|',
$      '.....|.....|.....|.....|.....|',
$      '.....| CAT  REV *')
END

C
C
C
C
C
SUBROUTINE PLOT(A,K,TIME,UNCAT,CAT)
    THIS SUB-PROGRAM TAKES ABSORBANCE VALUES FROM THE MAIN PROGRAM AND
    PLOTS THEM ON A SCALE MATCHING THE PRINTOUT OF THE CARY 14 .

    REAL*8 A,TIME,UNCAT,CAT,B
    DIMENSION PLT(102)
    DATA PLT,STAR,BLANK,DOT,BAR/102* ' ',' ',' ',' ',' ',' ',' ',' ',' /
    B=A
    IF(B.GT.1.00)B=B-1.00
    K=K+1
    INDEX=101.499999-B*100.
    IF(INDEX.GT.101)INDEX=101
    IF(INDEX.LT.2)INDEX=2
    PLT(INDEX)=STAR
    IF(K.EQ.6)GO TO 495
    PLT(1)=DOT
    PLT(102)=DOT
    GO TO 496
495  PLT(1)=BAR
    PLT(102)=BAR
    K=0
496  WRITE(6,201)TIME,A,PLT,UNCAT,CAT
201  FORMAT(1X,F5.2,1X,F5.3,102A1,1P9.2,1X,1P9.2)
    PLT(INDEX)=BLANK
    RETURN
END

```

```

C
C
C
C
C
SUBROUTINE CHART(IGRID,NUMRUN,LINE ,SCALE,VAR,STD,KOPY)
    THIS SUB-PROGRAM ACCEPTS ARRAY IGRID FROM THE MAIN PROGRAM CONTAINING
    ALL THE PREVIOUS PLOTS IN THIS DATA SET AND PRINTS A COMPOSIT GRAPH.

    REAL*8 SCALE
    DIMENSION IGRID(200,10),GRID(102),VAL(10),STD(10),VAR(10,2),
    $STAR(10)
    DATA GRID,STAR,BLANK,DOT,BAR/102* ' ',' ',' ',' ',' ',' ',' ',' /
    IF(KOPY.GT.1)GO TO 10
    DO 11 J=7,10
11  CONTINUE
10  DENOM=6.*SCALE
    TIME=0.0
    K=0
    LINES=LINE-1
    DO 300 I=1,LINES
    TIME=TIME+1./DENOM
    K=K+1
    DO 200 J=1,NUMRUN
    GRID(IGRID(I,J))=STAR(J)
    IF(K.EQ.6)GO TO 205
    GRID(1)=DOT
    GRID(102)=DOT
    GO TO 206
205  GRID(1)=BAR
    GRID(102)=BAR
    K=0
206  WRITE(6,301)TIME,GRID
    WRITE(6,410)TIME,GRID
410  FORMAT(1H,F5.2,1X,'---- ',102A1)
299  DO 300 J=1,NUMRUN
300  GRID(IGRID(I,J))=BLANK
    RETURN
301  FORMAT(1X,F5.2,1X,'---- ',102A1,' SUMMARY OF CURVES')
    END

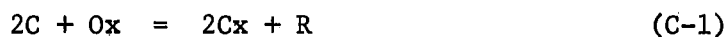
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APPENDIX C

DETAILED DERIVATION OF EQUATIONS

Complete derivations of cases discussed in the text of this report. Derivations are in the same order as the discussions appear in the paper.

Pre-equilibrium Condition (Case 1)



$$K_{eq} = [Cx]^2[R]/[C]^2[Ox] \quad (C-3)$$

Solving for $[Cx]^2$:

$$[Cx]^2 = K_{eq}[C]^2[Ox]/[R] \quad (C-4)$$

From stoichiometric considerations:

$$[Ox] = [Ox]_0 - \frac{1}{2}[Cx]$$

$$[C] = [C]_0 - [Cx]$$

$$[Cx] = 2[R]$$

Now, let: $X = [Cx]$, $C = [C]_0$, $\phi = [Ox]_0$, and $K = K_{eq}$

Substituting the above relations into Equation C-4 gives:

$$X^2 = \frac{K(C - X)^2(\phi - \frac{1}{2}X)}{\frac{1}{2}X} \quad (C-5)$$

Multiplying both sides by X and the right-hand side by $\frac{2}{\phi}$ gives:

$$\begin{aligned} X^3 &= K(C - X)^2(2\phi - X) \\ &= (KC^2 - 2KCX + KX^2)(2\phi - X) \\ &= 2\phi KC^2 - 4\phi KCX + 2\phi KX^2 - KX^3 \\ &\quad - KC^2X + 2KCX^2 \end{aligned}$$

Collecting terms:

$$(K + 1)X^3 = 2K(\phi + C)X^2 - KC(C + 4\phi)X + 2\phi KC^2$$

Dividing both sides by K and transferring to the left side:

$$\left(1 + \frac{1}{K}\right)X^3 - 2(C + \phi)X^2 + C(C + 4\phi)X - 2C^2\phi = 0 \quad (C-6)$$

Conversion back to the original variables gives the final equation expressing the activated catalyst concentration, $[Cx]$, in a cubic polynomial:

$$\left(1 + \frac{1}{K}\right)[Cx]^3 - 2([C]_o + [Ox]_o)[Cx]^2 + [C]_o([C]_o + 4[Ox]_o)[Cx] - 2[C]_o^2[Ox]_o = 0 \quad (C-7)$$

Pre-equilibrium Condition (Case 2)

$$C + 2Ox = Cx + 2R \quad (C-8)$$

$$Cx + Dr = Dx + C \quad (C-9)$$

$$K_{eq} = \frac{[Cx][R]^2}{[C][Ox]^2} \quad (C-10)$$

Solving for $[Cx]$:

$$[Cx] = K_{eq} [C][Ox]^2/[R]^2 \quad (C-11)$$

From stoichiometric considerations:

$$[Ox] = [Ox]_0 - 2[Cx] \quad (C-12)$$

$$[C] = [C]_0 - [Cx] \quad (C-13)$$

$$[R] = 2[Cx] \quad (C-14)$$

Again, letting: $X = [Cx]$, $C = [C]_0$, $\phi = [Ox]_0$, and $K = K_{eq}$ and substituting into Equation C-11 gives:

$$X = \frac{K(C - X)(\phi - 2X)^2}{4X^2} \quad (C-15)$$

Multiplying both sides by $4X^2/K$:

$$\begin{aligned} \frac{4X^3}{K} &= (C - X)(\phi - 2X)^2 \\ &= (C - X)(\phi^2 - 4\phi X + 4X^2) \\ &= C\phi^2 - 4C\phi X + 4CX^2 \\ &\quad - \phi^2 X + 4\phi X^2 - 4X^3 \end{aligned}$$

Collection of terms and transferring to the left side gives the final form of the expression for $[Cx]$:

$$4\left(1 + \frac{1}{K}\right)X^3 - 4(C + \phi)X^2 + (4C + \phi)\phi X - C\phi^2 = 0 \quad (C-16)$$

Or, in terms of the original variables:

$$4\left(1 + \frac{1}{K}\right)[C_x]^3 - 4([C]_0 + [O_x]_0)[C_x]^2 + (4[C]_0 + [O_x]_0)[O_x]_0[C_x] - [C]_0[O_x]_0^2 = 0 \quad (C-17)$$

Steady-State Condition (Case 1)

$$2C + O_x \stackrel{k_1}{=} 2C_x + R \quad (C-18)$$

$$2C_x + Dr \stackrel{k_2}{=} 2C + Dx \quad (C-19)$$

Equation C-18 represents the rate-determining step.

$$\text{rate} = -\frac{d[Dr]}{dt} = -\frac{d[O_x]}{dt} = k_1[O_x][C]^2 - k_{-1}[C_x]^2[R] \quad (C-20)$$

Making the steady-state approximation:

$$\frac{1}{2} \frac{d[C_x]}{dt} = k_1[O_x][C]^2 - k_{-1}[C_x]^2[R] - k_2[C_x][Dr] = 0 \quad (C-21)$$

From Equation C-21 we get the following two relationships:

$$k_1[O_x][C]^2 = k_{-1}[C_x]^2[R] + k_2[C_x][Dr] \quad (C-22)$$

and, using the quadratic formula:

$$[C_x] = \frac{-k_2[Dr] + \sqrt{(k_2[Dr])^2 + 4k_1k_{-1}[R][O_x][C]^2}}{2k_{-1}[R]} \quad (C-23)$$

Substitution of Equation C-22 into Equation C-20 gives:

$$\text{rate} = -k_2[C_x][Dr] \quad (C-24)$$

Taking the following stoichiometric relations:

$$[R] = [Dr]_0 - [Dr] \quad (C-25)$$

$$[Ox] = [Dr] - [Dr]_0 + [Ox]_0 \quad (C-26)$$

and Equation C-23 in Equation C-24 gives the final rate expression:

$$\text{rate} = -k_2[Dr] \left(\frac{-k_2[Dr] + \sqrt{(k_2[Dr])^2 + 4k_1k_{-1}[R][Ox][C]^2}}{2k_{-1}[R]} \right) \quad (C-27)$$

Steady-State Mechanism (Case 2)



$$\text{rate} = \frac{-d[Dr]}{dt} = -\frac{1}{2} \frac{d[Ox]}{dt} = k_1[Ox]^2[C] - k_{-1}[Cx][R]^2 \quad (C-30)$$

Making the steady-state approximation:

$$\frac{d[Cx]}{dt} = k_1[Ox]^2[C] - k_{-1}[Cx][R]^2 - k_2[Cx][Dr] = 0 \quad (C-31)$$

Rearrangement of Equation C-31 gives the following two relations:

$$k_1[Ox]^2[C] = k_{-1}[Cx][R]^2 + k_2[Cx][Dr] \quad (C-32)$$

and, using the quadratic formula:

$$[Cx] = \frac{k_1 [Ox]^2 [C]}{k_{-1} [R]^2 + k_2 [Dr]} \quad (C-33)$$

Substitution of Equation C-32 into Equation C-30 gives:

$$\text{rate} = -2(k_2 [Cx] [Dr]) \quad (C-34)$$

Replacing $[Cx]$ by Equation C-33

$$\text{rate} = \frac{-2k_1 k_2 [Ox]^2 [Dr] [C]}{k_{-1} [R]^2 + k_2 [Dr]} \quad (C-35)$$

but, since k_2 is much greater than k_{-1} and

$$[Ox] = [Ox]_o - 2[Dr]_o + 2[Dr]$$

we have:

$$\text{rate} = -2k_1 ([Ox]_o - 2[Dr]_o + 2[Dr])^2 [C]_o, \quad (C-36)$$

the final expression for the catalyzed rate.

Special Case: 3 Different Species



Pre-equilibrium Mechanism

$$K_{eq} = [Q] / [C][Dr][Ox] \quad (C-39)$$

Solving for $[Q]$ gives:

$$[Q] = K_{eq}[C][Dr][Ox] \quad (C-40)$$

Stoichiometric considerations give:

$$[Ox] = [Ox]_o - [Q] \quad (C-41)$$

$$[C] = [C]_o - [Q] \quad (C-42)$$

$$[Dr] = [Dr]_o - [Q] \quad (C-43)$$

Letting $Q = [Q]$, $C = [C]_o$, $D = [Dr]_o$, $\phi = [Ox]_o$, and $K = K_{eq}$ and substituting into Equation C-40 gives:

$$Q = K(C - Q)(D - Q)(\phi - Q) \quad (C-44)$$

$$Q/K = (CD - (C + D)Q + Q^2)(\phi - Q)$$

$$\frac{Q}{K} = CD\phi - \phi(C + D)Q + \phi Q^2 - CDQ + (C + D)Q^2 - Q^3$$

Collection of terms and transferring to the left side gives:

$$Q^3 - (\phi + C + D)Q^2 + (\phi(C + D) + CD + \frac{1}{K})Q - CD\phi = 0 \quad (C-45)$$

Substitution of the original variables gives Equation 3-38 in text.

Steady-State Condition

Referring to Equations C-37 and C-38

$$\text{rate} = -\frac{d[Dr]}{dt} = -k_{-1}[Q] + k_1[C][Dr][Ox] \quad (C-46)$$

Making the steady-state approximation:

$$\frac{d[Q]}{dt} = k_1[C][Dr][Ox] - k_2[Q] - k_{-1}[Q] = 0 \quad (C-47)$$

Equation C-47 yields the following two relations:

$$k_1[C][Dr][Ox] = k_2[Q] + k_{-1}[Q] \quad \text{and} \quad (C-48)$$

$$[Q] = \frac{k_1[C][Dr][Ox]}{k_2 + k_{-1}} \quad (C-49)$$

Substitution of Equation C-48 into Equation C-46 gives:

$$\text{rate} = -k_2[Q] \quad (C-50)$$

Equation C-49 in Equation C-50 gives:

$$\text{rate} = \frac{-k_1 k_2 [C][Dr][Ox]}{k_2 + k_{-1}} \quad (C-51)$$

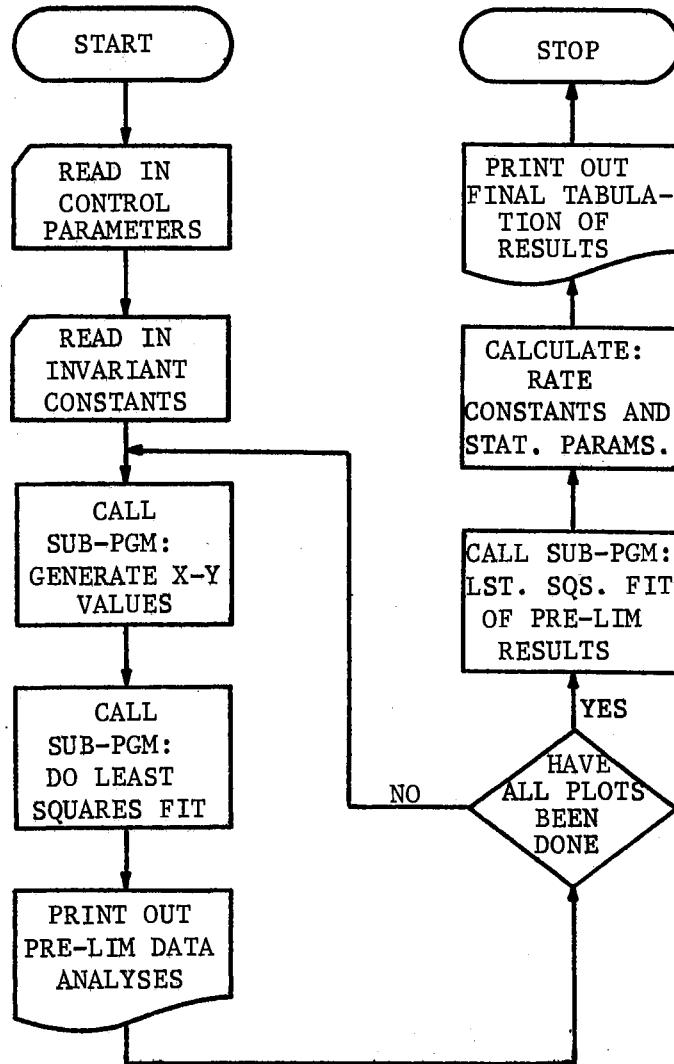
But, since k_2 is much greater than k_{-1} , $[C] = [C]_0$ and $[Ox] = [Ox]_0 - [Dr]_0 + [Dr]$, we have finally:

$$\text{rate} = -k_1[Dr][C]_0([Ox]_0 - [Dr]_0 + [Dr]) \quad (C-52)$$

This is the final expression for the catalyzed rate when considering the collision of three different species and assuming the steady-state mechanism.

APPENDIX D

FLOW DIAGRAM AND SOURCE PROGRAM FOR DETERMINATION
OF SYSTEM PARAMETERS



THIS PROGRAM ACCEPTS ABSORBANCE VS. TIME DATA AND CALCULATES RATE
CONSTANTS BY DOING A LEAST SQUARES FIT OF THE MODIFIED RATE EQUATION.
A BREAKDOWN OF THE INDIVIDUAL PROGRAM SEGMENTS AND THEIR FUNCTION
FOLLOWS:

MAIN: 1) READS IN PARAMETERS WHICH DO NOT VARY FROM RUN TO RUN
2) CALLS ALL OTHER SUB-PROGRAMS
3) COLLECTS RESULTS OF LEAST SQUARES FITS AND CALCULATES
MEAN VALUES AND STATISTICAL PARAMETERS FOR THE RATE
CONSTANTS DETERMINED

POINTS: 1) READS IN ABSORBANCE VS. TIME DATA AND OTHER CONTROL
PARAMETERS
2) CALCULATES THE DERIVATIVE OF EACH POINT
3) GENERATES THE ABSCISSA AND ORDINATE VALUES FOR THE
LEAST SQUARES ROUTINE
4) PRINTS OUT INPUT PARAMETERS, DERIVATIVES, AND WEIGHTS

FIT: CALCULATES ORDINATE VALUES PREDICTED BY THE FITTED EQUATION

OUTPUT: GENERATES THE OUTPUT OF THE LEAST SQUARES ROUTINE

MTXGEN: GENERATES THE AUGMENTED MATRIX NECESSARY TO DO GAUSSIAN
ELIMINATION

WEIGHT: 1) SOLVES THE SYSTEM OF SIMULTANEOUS EQUATIONS NECESSARY
TO DO LINEAR LEAST SQUARES FITTING
2) GENERATES THE INVERSE OF THE AUGMENTED MATRIX NECESSARY
TO CALCULATE STATISTICAL PARAMETERS

DEFINITION OF VARIABLES APPEARING IN MAIN PROGRAM:

AKNEG2: REVERSE RATE CONSTANT FOR REACTION OF CATALYST WITH DYE
AK1: FORWARD RATE CONSTANT FOR THE OXIDATION OF CATALYST
AK2: FORWARD RATE CONSTANT FOR THE REACTION OF OXIDIZED CATALYST
WITH DYE
AMTX: ARRAY CONTAINING THE AUGMENTED MATRIX GENERATED BY "MTXGEN"
Astart: INITIAL ABSORBANCE
CATIN: CATALYST ADDITION RATE IN MOLES/LITER*MIN
CONST: ARRAY CONTAINING RESULTS OF THE LEAST SQUARE FITTING
DEV: ARRAY CONTAINING THE ABSOLUTE DEVIATION OF EACH OBSERVED
ORDINATE VALUE FROM THE CORRESPONDING CALCULATED VALUE
EPS: MOLAR ABSORPTIVITY OF THE DYE BEING USED
LABEL: ANY 80 CHARACTER LABEL TO BE PRINTED AT THE TOP OF EACH TABLE
N: NUMBER OF POINTS CONTAINED IN ARRAYS X, Y, AND W
OMEGA: SUM OF THE SQUARES OF THE VALUES IN "DEV"
UX: CONCENTRATION OF THE OXIDIZING AGENT IN MOLES/LITER
PCTDEV: ARRAY CONTAINING THE RELATIVE DEVIATIONS OF EACH OBSERVED
ORDINATE VALUE FROM THE CALCULATED VALUE
RCNST: ARRAY CONTAINING CALCULATED RATE CONSTANTS (USED ONLY WHEN
INDIVIDUAL CONSTANTS ARE CALCULATED, THEN AVERAGED)
SD: ARRAY CONTAINING THE STANDARD DEVIATIONS OF THE RESULTS OF THE
LEAST SQUARE FITTING
SOLN: ARRAY CONTAINING SOLUTIONS TO THE SIMULTANEOUS EQUATIONS
SOLVED BY SUB-PROGRAM WEIGHT
TABLE: ARRAY CONTAINING DATA IDENTIFIER, INITIAL DYE CONCENTRATION,
AND CATALYST ADDITION RATE
T1: TIME WHEN CATALYST FIRST BECOMES AVAILABLE TO SYSTEM
T2: TIME WHEN AVAILABLE CATALYST EQUALS TOTAL ANALYTICAL CATALYST
CONCENTRATION
W: ARRAY CONTAINING THE WEIGHTS OF EACH CORRESPONDING ORDINATE POINT
WINV: ARRAY CONTAINING THE DIAGONAL ELEMENTS OF THE INVERSE OF
THE AUGMENTED MATRIX
WTFAC: DIAGONAL ELEMENT OF THE INVERSE OF THE AUGMENTED MATRIX
CORRESPONDING TO "SOLN(I)"
X: ARRAY CONTAINING ABSCISSA VALUES FOR LEAST SQUARE FITTING
Y: ARRAY CONTAINING ORDINATE VALUES FOR LEAST SQUARE FITTING
YCAL: ARRAY CONTAINING ORDINATE VALUES CALCULATED FROM RESULTS
OF LEAST SQUARE FITTING

IMPLICIT REAL*8(A-H,O-Z)
COMMON X(100),Y(100),W(100),N
DIMENSION SOLN(6),AMTX(6,7),YCAL(100),RCNST(20,2),SD(20,2)
S,W,WINV(6),CONST(20,2),PCTDEV(100),DEV(100)
REAL*4 LABEL(20),TABLE(20,3)
DATA MFIT/1/

/2/TIM AT AD
DU 3000 MASTER=1,2

READ(5,997)NUMRUN,AKUN,CRIT,EPS,UX
DO 1000 KOUNT=1,NUMKUN
READ(5,995)TABLE(KOUNT,1)
READ(5,998)LABEL
LUOP=1
CALL POINTS
S(LOOP,ASTART,CATIN,EPS,UX,T1,T2,LABEL)
CALL MTXGEN(MFIT,AMTX,NROW)
CALL WEIGHT(MFIT,AMTX,WINV,SOLN,KODE)
IF(KODE.EQ.1)GO TO 1010
CALL FIT(YCAL,PCTDEV,DEV,OMEGA,SOLN,MFIT)
DO 2001 ISTAT=1,2
KEY=ISTAT
CONST(IKOUNT,ISTAT)=SOLN(ISTAT)
WTFAC=DABS(WINV(KEY))
2001 SD(IKOUNT,ISTAT)=DSQRT(OMEGA*WTFAC)
CALL OUTPUT(LABEL,YCAL,PCTDEV,DEV,OMEGA,SOLN,WINV,MFIT)
GO TO 1020
1010 WRITE(6,350)MFIT,LOOP
END INSERT * * * * *

CONTINUE
TABLE(KOUNT,2)=ASTART/EPS
TABLE(KOUNT,3)=CATIN
1000 CONTINUE
DO 1070 I=1,NUMRUN
ABSORB=TABLE(I,2)*EPS
X(I)=ABSORB*CONST(I,1)
W(I)=1.0-8*(1.0-(12.1715D-3*1.01**ABSORB+2.0-3)/ABSORB))/SD(I,2)
1070 Y(I)=CONST(I,2)
READ(5,998)LABEL
N = NUMKUN
CALL MTXGEN(MFIT,AMTX,NROW)
CALL WEIGHT(MFIT,AMTX,WINV,SOLN,KODE)
IF(KODE.EQ.1)GO TO 1095
CALL FIT(YCAL,PCTDEV,DEV,OMEGA,SOLN,MFIT)
CALL OUTPUT(LABEL,YCAL,PCTDEV,DEV,OMEGA,SOLN,WINV,MFIT)
WTFAC=DABS(WINV(1))
AK2=1.0D0/SOLN(1)
SD2=DSQRT(OMEGA*WTFAC)*AK2/(1-SOLN(1))
WRITE(6,352)
C2 = 1.0-8*SOLN(2) + SOLN(1)
AKNEG2=(C2*AK2 + 1.0D0/1.0-8 + C2 - SOLN(1))
WTFAC=DABS(WINV(2))
SD3=DSQRT(OMEGA*WTFAC)*AKNEG2/(1-SOLN(2))
SUM1=0.0D0
DO 1081 I=1,NUMRUN
SUM1=SUM1 + CONST(I,1)
1081 CONTINUE
C1BAR=SUM1/NUMRUN
AK1=(AKNEG2-AK2)/(C1BAR*AK2*EPS*DSQRT(UX))
SUMS1=0.0D0
DO 1090 I=1,NUMRUN
SUMS1=SUMS1 + (C1BAR-CONST(I,1))**2
1090 CONTINUE
REALN=NUMRUN - 1
RELS01=DSQRT(SUMS1/REALN)*1.0D2/C1BAR
SD1=AK1*RELS01/1.02
RELS02=1.02*SD2/AK2
RELS03=1.02*SD3/AKNEG2
WRITE(6,355)AK1,SD1,RELS01,AK2,SD2,RELS02,AKNEG2,SD3,RELS03
GO TO 1099

```

1095 WRITE(6,356)
1099 WRITE(6,351)
3000
      STOP
497 FORMAT(13,4E10.3)
495 FUMMAT(F10.0)
496 FUMMAT(20A4)
450 FUMMAT(1M1,'SINGULAR MATRIX ENCOUNTERED FOR DEGREE ',I2//
      $IX,'LOOP= ',I3)
351 FUMMAT(1M1,'END OF OUTPUT')
352 FUMMAT(1M1,T8,'DETERMINATION OF SYSTEM PARAMETERS--SUMMARY OF',
      $' RESULTS'//)
355 FUMMAT(///IX,T8,'MEAN VALUES OF RATE CONSTANTS:////
      $IX,T12,'CONSTANT      VALUE      STD DEV      REL STD DEV(PH)')
      $/IX,T15,'K1'          ,T24,2(1PD11.4,3X),OPF10.5/
      $/IX,T15,'K2'          ,T24,2(1PD11.4,3X),OPF10.5/
      $/IX,T15,'K-2'        ,T24,2(1PD11.4,3X),OPF10.5/
356 FUMMAT(///IX,'***** SINGULAR MATRIX ENCOUNTERED
      $ UN THIS STEP *****')
      END

```

CONTINUE

SUBROUTINE POINTS
\$(LOOP,ASTART,CATIN,EPS,OX,T1,T2,LABEL)

THIS SUB-PROGRAM GENERATES THE ABSCISSA AND ORDINATE VALUES FOR THE
LEAST SQUARES ROUTINE.

DEFINITION OF VARIABLES NOT APPEARING IN THE MAIN PROGRAM:

ABS: ARRAY CONTAINING INPUT ABSORBANCE VALUES
 ABSORB: ABSORBANCE FOR THE I*TH POINT
 DCHECK: VARIABLE USED IN FINDING POINT WITH LARGEST DERIVATIVE
 DEL: EQUALS TDEL (NECESSARY WHEN VARIABLE STEP SIZE USED)
 DERIV: ARRAY CONTAINING CALCULATED DERIVATIVE VALUES FOR EACH POINT
 SLOPE: CHANGE IN INPUT ABSORBANCE PER UNIT OF TIME (USED AS A ROUGH
 CHECK ON THE DERIVATIVE VALUE FOR EACH POINT)
 TDEL: TIME INCREMENT BETWEEN INPUT ABSORBANCE VALUES
 TSTART: TIME CORRESPONDING TO FIRST INPUT ABSORBANCE VALUE

```

IMPLICIT REAL*8 (A-H,C-Z)
REAL*4 LABEL(20)
COMMON X(100),Y(100),W(100),N
DIMENSION ABSB(100), DERIV(100)
IF(LOOP.GT.1)GO TO 15
JUMP=5
READ(5,100)NUM,KDROP
READ(5,2999)T1
READ(5,101)TDEL,TSTART,CATIN,ASTART,(ABS(B(K),K=1,NUM)
DEL=TDEL
IF(KDROP.EQ.0)GO TO 12
NUM=NUM - KDROP
TSTART=TSTART + KDROP*TDEL
DO 13 I=1,NUM
13 ABSB(I) = ABSB(I) + KDROP
12 CONTINUE

```

```

TIME=TSTART + JUMP*DEL
NSTOP=NUM - 2*JUMP
N = NSTOP
WRITE(6,302)LABEL
DCHECK=0.00
DO 30 I=1,NSTOP
  ABSORB=ABSB(I + JUMP)
  SLOPE=(ABSORB - ABSB(I + JUMP -1))/DEL
  W(I)=1.0/PE(1000-(12.17150-3*1.01**ABSORB + 2.0-3)/ABSORB))
  IF(W(I).LT.D.DC)W(I)=0.00
  DERIV(I)=
  $ (300.*ABSB(I)-294.*ABSB(I+1)-532.*ABSB(I+2)-503.*ABSB(I+3)
  $-296.*ABSB(I+4)+296.*ABSB(I+6)+503.*ABSB(I+7)+532.*ABSB(I+8)
  $+294.*ABSB(I+9)-300.*ABSB(I+10))/(5148.*DEL)
  IF(DERIV(I).GT.DC)DCHECK=GO TO 25
  DCHECK=DERIV(I)
  T2=TIME
25 JUMP=1+JUMP
  WRITE(6,301)I,TIME,ABSB(JUMP),DERIV(I),SLOPE,W(I)
30 TIME=TIME + DEL
  WRITE(6,354)INUM,KDROP,DEL,TSTART,CATIN,ASTART,T1,T2
15 TIME=TSTART + JUMP*DEL
  DCHECK=0.00
  DO 40 I=1,NSTOP
    ABSORB=ABSB(I + JUMP)
    X(I) = 1.00/ABSORB
    CATCON=CATIN*T2*(TIME-T1)**2/(T2-T1)**2
    IF(TIME.LT. T1)CATCON=0.00
    IF(TIME.GE.T2)CATCON=CATIN*TIME
    Y(I)=CATCON/DERIV(I)
40 TIME = TIME + DEL
11 RETURN
100 FORMAT(2 I3)
101 FORMAT(4E10.3/18F10.0)
301 FORMAT(4X, I3,5(3X,F10.5))
302 FORMAT(1M1,T5,20A4///IX,T5,'DETERMINATION OF DERIVATIVE USING ',
      $ '11-POINT CUBIC SMOOTH'///IX,T5,'NO. TIME ',
      $ 'ABSORBANCE DERIVATIVE SLOPE WEIGHT')
354 FORMAT(///IX,T5,'VALUES OF OTHER INPUT PARAMETERS:////IX,T5,
      $'NUM=',I4,3X,'KDROP=',I3,3X,'TDEL= ',1PD11.4,3X,'TSTART= ',D11.4,
      $/IX,T5,'CATIN= ',D11.4,3X,'ASTART= ',OPF6.3,3X,'T1= ',F7.4,
      $3X,'T2= ',F7.4)
2999 FORMAT(2F10.0)
      END

```

```

SUBROUTINE MTXGEN(M,G,MPI)
C
C THIS SUB-PROGRAM TAKES THE X(I) AND Y(I) VALUES AND BUILDS THE
C AUGMENTED MATRIX NECESSARY TO DO GAUSSIAN ELIMINATION.
C
C PARAMETERS REQUIRED:
C
C     M=THE DEGREE OF THE POLYNOMIAL TO BE FIT.
C
C VALUES RETURNED:
C
C     G=THE AUGMENTED MATRIX CONTAINING THE COEFFICIENTS OF THE
C     SIMULTANEOUS EQUATIONS TO BE SOLVED.
C
C     MPI=THE NUMBER OF SIMULTANEOUS EQUATIONS TO BE SOLVED.
C
C NOTE: THIS SUB-PROGRAM WAS WRITTEN BY T.E. BAILEY.
C
IMPLICIT REAL*8 (A-H,U-Z)
COMMON X(100),Y(100),M(100),N
DIMENSION G(6,7),SUMX(11),SUMY(6)
MPZ=M+2
MPI=M+1
M2P1=M*2+1
SUMX(1)=0.00
DO 9 I=1,N
9 SUMX(1)=SUMX(1)+M(I)
DO 7 I=2,M2P1
7 SUMX(I)=0.
DO 6 I=1,MPI
6 SUMY(I)=0.
DO 1 I=2,M2P1
DO 1 K=1,M
1 SUMX(I)=SUMX(I)+M(K)*X(K)**(I-1)
DO 2 K=1,N
2 SUMY(I)=SUMY(I)+M(K)*Y(K)
DO 3 I=2,MPI
DO 3 K=1,N
3 SUMY(I)=SUMY(I)+M(K)*Y(K)*X(K)**(I-1)
C GENERATE THE AUGMENTED MATRIX.
INDEX=0
DO 5 J=1,MPI
DO 4 I=1,MPI
4 I(I,J)=SUMX(I+INDEX)
5 INDEX=INDEX+1
DO 6 I=1,MPI
6 I(MP2)=SUMY(I)
C THE AUGMENTED MATRIX IS NOW GENERATED AND READY FOR SOLUTION.
RETURN
END

```

```

SUBROUTINE WEIGHT(MFIT,AUG,MINV,SOLN,KODE)
C
C THIS SUB-PROGRAM ACCEPTS AN AUGMENTED MATRIX FROM THE MAIN PROGRAM
C CONSTITUTING A SET OF SIMULTANEOUS LINEAR EQUATIONS AND RETURNS THE
C SOLUTIONS TO THE EQUATIONS ALONG WITH AN ARRAY(MINV) CONTAINING THE
C DIAGONAL ELEMENTS OF THE INVERSE OF THE AUGMENTED MATRIX.
C
C SEE MAIN PROGRAM FOR VARIABLE DEFINITION
C
IMPLICIT REAL*8(A-H,U-Z)
DIMENSION AUG(6,7),VAL(6,13),MINV(6),SOLN(6)
KODE=0
NSIZE=MFIT+1
NIDENT=NSIZE+1
NNSIZE=2*NSIZE+1
DO 7 I=1,NSIZE
DO 7 J=NIDENT,NNSIZE
VAL(I,J)=0.00
IF(I.EQ.(J-NSIZE))VAL(I,J)=1.00
7 CONTINUE
DO 8 J=1,NSIZE
DO 8 I=1,NSIZE
8 VAL(I,J)=AUG(I,J)
DO 11 I=1,NSIZE
11 VAL(I,NSIZE)=AUG(I,NIDENT)
DO 1 IA=1,NSIZE
CK=0.00
DO 10 IR=IA,NSIZE
IF(ABS(VAL(IR,IA)).LE.DABS(CK))GO TO 10
CK=VAL(IR,IA)
KR=IR
10 CONTINUE
DO 20 J=1,NNSIZE
R=VAL(KR,J)
VAL(KR,J)=VAL(IA,J)
20 VAL(IA,J)=R
GPIVT=VAL(IA,IA)
IF(ABS(GPIVT).LT.1.0-60)GO TO 30
DO 2 NI=1,NNSIZE
2 VAL(IA,NI)=VAL(IA,NI)/GPIVT
DO 3 N2=1,NSIZE
IF(N2.EQ.1)GO TO 3
D=VAL(N2,IA)
DO 4 N3=1,NNSIZE
4 VAL(N2,N3)=VAL(N2,N3)-VAL(IA,N3)*D
3 CONTINUE
1 CONTINUE
DO 9 I=1,NSIZE
SOLN(I)=VAL(I,NNSIZE)
9 MINV(I)=VAL(I,(I+NSIZE))
GO TO 40
30 KODE=1
40 RETURN
END

```

```

C
C
C
SUBROUTINE FIT(YCAL,PCTDEV,DEV,OMEGA,C,M)
    THIS SUB-PROGRAM CALCULATES THE ORDINATE VALUES PREDICTED BY THE
    FITTED EQUATION.
    IMPLICIT REAL*8 (A-H,U-Z)
    COMMON X(100),Y(100),W(100),N
    DIMENSION C(6),YCAL(100),PCTDEV(100),DEV(100)
    DO 1 I=1,N
        YCAL(I)=C(1)
        DO 1 K=1,M
            YCAL(I)=YCAL(I)+C(K+1)*X(I)**K
        SUMCHI=0.0
        SUMSQ=0.0
        DO 10 I=1,N
            UEV(I)=Y(I)-YCAL(I)
            PCTDEV(I)=DEV(I)*100./YCAL(I)
10    SUMSQ = SUMSQ + W(I)*DEV(I)**2
        RM=N
        IF(N.EQ.2)RN=3.00
        RM=N+1
        OMEGA = SUMSQ/(N-RM)
    RETURN
    END

```

```

C
C
C
SUBROUTINE OUTPUT(LABEL,YCALC,PCTDEV,DEV,OMEGA,C,M,INV,M)
    THIS SUB-PROGRAM GENERATES THE OUTPUT OF THE LEAST SQUARES PORTION
    OF THE PROGRAM. SPECIFICLY, IT PRINTS OUT:
    X(I)=THE ABSCISSA VALUE FED INTO THE LEAST SQUARES PORTION.
    Y(I)=Y(OBS)=ORDINATE VALUE FED INTO THE LEAST SQUARES PORTION
    OF THE PROGRAM.
    YCALC(I)=THE ORDINATE VALUE CALCULATED FROM THE EQUATION
    GENERATED BY THE LEAST SQUARES SEGMENT.
    DEV(I)=THE DEVIATION OF Y(OBS) FROM THE FITTED CURVE.
    PCTDEV=PER CENT DEVIATION OF Y(OBS) FROM THE FITTED CURVE.
    CHISQ(I)=TERM CONTRIBUTING TO THE OVERALL CHI SQUARED
    GOODNESS OF FIT CRITERION: CHISQ(I)=UEV**2/ABS(YCALC(I)).
    OMEGA=THE SAMPLE VARIANCE OF THE LEAST SQUARES FIT.
    SUMCHI=THE SUM OF THE INDIVIDUAL CHI SQUARED TERMS: A MEASURE
    OF THE GOODNESS OF FIT OF THE CURVE TO THE DATA.
    IMPLICIT REAL*8(A-H,U-Z)
    COMMON X(100),Y(100),W(100),N
    DIMENSION C(6),YCALC(100),PCTDEV(100),DEV(100),W(INV(6))
    REAL*4 LABEL(20)
    WRITE(6,10)LABEL
    DO 1 I=1,N
1    WRITE(6,11)X(I),Y(I),YCALC(I),DEV(I),PCTDEV(I),W(I)
    MPI=M+1
    WRITE(6,14)OMEGA
    WRITE(6,15)M
    DO 20 I=1,MPI
        WTFAC=DABS(W(INV(I)))
        SDOF=DSQRT(OMEGA*WTFAC)
        RELSDO=SDOF*1.02/C(I)
20    WRITE(6,16)I,C(I),SDOF,RELSDO
    RETURN
10  FORMAT(1H1,///1H ,10X,20A4,///1H ,14X,*X          Y(OBS)*,
        $*   Y(CALC)*,
        $*   DEV(Y)   $ DEV(Y)   WEIGHT(Y)*/)
11  FORMAT(1H ,9X,3(1P10.3,2X),D10.3,2X,0PF10.5,2X,F11.4)
14  FORMAT(///15X,*GOODNESS OF FIT:          GAUSS CRITERION,  OMEGA=*,1X
        $,1P10.3)
15  FORMAT(///1X,T15,*CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF *,
        $*DEGREE *,I1,* *///1X,T20,*CONSTANT   VALUE          STD DEV   *,
        $*REL STD DEVI(PHI)*/)
16  FORMAT(1X,T23,*C(*,I1,*)*,T30,2(1P11.4,2X),0PF10.4/)
    END

```

APPENDIX E

COMPLETE LISTING OF OUTPUT FROM DETERMINATION OF
SYSTEM PARAMETERS PROGRAM--NO NTA PRESENT

MN(III)--PERIODATE SYSTEM: 34.01 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

MN(III)--PERIODATE SYSTEM: 34.01 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.00617	0.21100	-0.26013	-0.19200	0.73792
2	1.02900	0.20300	-0.30724	-0.38400	0.73077
3	1.04963	0.19700	-0.33980	-0.28800	0.72498
4	1.07067	0.19000	-0.35701	-0.33600	0.71772
5	1.09150	0.18300	-0.35244	-0.33600	0.70986
6	1.11233	0.17400	-0.33608	-0.45200	0.69876
7	1.13317	0.16800	-0.33117	-0.28800	0.69065
8	1.15400	0.16200	-0.31992	-0.28800	0.68190
9	1.17463	0.15500	-0.30424	-0.33600	0.67078
10	1.19567	0.14900	-0.30219	-0.28800	0.66038
11	1.21650	0.14200	-0.30907	-0.33600	0.64709
12	1.23733	0.13600	-0.28794	-0.28800	0.63456
13	1.25817	0.13100	-0.26465	-0.24000	0.62320
14	1.27900	0.12400	-0.23807	-0.33600	0.60572
15	1.29983	0.12000	-0.20672	-0.19200	0.59478
16	1.32067	0.11700	-0.19421	-0.14400	0.58608
17	1.34150	0.11200	-0.19000	-0.24000	0.57050
18	1.36233	0.10900	-0.18075	-0.14400	0.56046
19	1.38317	0.10500	-0.17752	-0.19200	0.54615
20	1.40400	0.10000	-0.17619	-0.24000	0.52662
21	1.42483	0.09700	-0.16960	-0.14400	0.51392
22	1.44567	0.09500	-0.16804	-0.09600	0.50500
23	1.46650	0.09100	-0.15897	-0.19200	0.48597
24	1.48733	0.08600	-0.15545	-0.24000	0.45965
25	1.50817	0.08400	-0.15300	-0.09600	0.44823
26	1.52900	0.08100	-0.15249	-0.14400	0.43003
27	1.54983	0.07800	-0.13841	-0.14400	0.41042
28	1.57067	0.07500	-0.14379	-0.14400	0.38922
29	1.59150	0.07200	-0.14498	-0.14400	0.36624

VALUES OF OTHER INPUT PARAMETERS:

NUM= 39 KORUP= 0 TDELTA= 2.08330-02 TSTART= 9.04000-01
 CATIN= 2.24000-08 ASTART= 0.225 T1= 0.8620 T2= 1.0707

X	Y(OBS)	Y(CALC)	DEVI(Y)	Z DEVI(Y)	WEIGHT(Y)
4.7390 00	-4.5240-08	-4.7550-08	2.3140-09	-4.86665	0.7379
4.9260 00	-5.0000-08	-5.2070-08	2.0690-09	-3.97376	0.7308
5.0760 00	-5.7190-08	-5.5690-08	-1.4490-09	2.68243	0.7250
5.2630 00	-6.7180-08	-6.0220-08	-6.9610-09	11.56024	0.7177
5.4640 00	-6.9370-08	-6.5080-08	-4.2890-09	6.58946	0.7099
5.7470 00	-7.4140-08	-7.1920-08	-2.2210-09	3.08889	0.6988
5.9520 00	-7.6650-08	-7.6680-08	2.3390-10	-0.30430	0.6906
6.1730 00	-8.0800-08	-8.2210-08	1.4090-09	-1.71396	0.6819
6.4520 00	-8.6500-08	-8.8950-08	2.4530-09	-2.75720	0.6708
6.7110 00	-8.8630-08	-9.5230-08	6.6020-09	-6.93289	0.6604
7.0420 00	-8.8170-08	-1.0320-07	1.5060-08	-14.59313	0.6471
7.3530 00	-9.6260-08	-1.1070-07	1.4480-08	-13.07821	0.6346
7.6340 00	-1.0650-07	-1.1750-07	1.1040-08	-9.39096	0.6232
8.0650 00	-1.2030-07	-1.2790-07	7.6050-09	-9.94374	0.6057
8.3330 00	-1.4080-07	-1.3440-07	-6.4020-09	4.76171	0.5948
8.5470 00	-1.5230-07	-1.3960-07	-1.2710-08	9.10627	0.5861
8.9290 00	-1.5820-07	-1.4880-07	-9.3230-09	6.26410	0.5705
9.1740 00	-1.6480-07	-1.5480-07	-1.4060-08	9.08232	0.5605
9.5240 00	-1.7450-07	-1.6320-07	-1.1300-08	6.92566	0.5462
1.0000 01	-1.7850-07	-1.7470-07	-3.7610-09	2.15240	0.5266
1.0310 01	-1.8820-07	-1.8220-07	-5.9630-09	3.27257	0.5139
1.0530 01	-1.9270-07	-1.8750-07	-5.2470-09	2.79902	0.5050
1.0990 01	-2.0660-07	-1.9870-07	-7.9940-09	4.02432	0.4860
1.1630 01	-2.1430-07	-2.1410-07	-2.2250-10	0.10393	0.4596
1.1900 01	-2.2080-07	-2.2080-07	-1.4170-11	0.00482	0.4482
1.2350 01	-2.2460-07	-2.3150-07	6.8570-09	-2.96248	0.4300
1.2820 01	-2.5080-07	-2.4290-07	-7.8970-09	3.25063	0.4104
1.3330 01	-2.4470-07	-2.5530-07	1.0640-08	-4.10766	0.3892
1.3890 01	-2.4590-07	-2.6880-07	2.2870-08	-8.50884	0.3662

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 4.3940-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STO DEV	REL STD DEV(PPH)
C(1)	6.70320-08	5.28870-09	7.8898
C(2)	-2.41770-08	6.24480-10	-2.5829

MN(11)--PERIODATE SYSTEM: 34.02 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

MN(11)--PERIODATE SYSTEM: 34.02 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.97917	0.43500	-0.42532	-0.38400	0.81811
2	1.00000	0.42800	-0.46491	-0.33600	0.81734
3	1.02083	0.41600	-0.51990	-0.57600	0.81588
4	1.04167	0.40300	-0.56065	-0.62400	0.81409
5	1.06250	0.39400	-0.58519	-0.43200	0.81270
6	1.08333	0.38200	-0.59875	-0.57600	0.81065
7	1.10417	0.36600	-0.59388	-0.76800	0.80755
8	1.12500	0.35500	-0.60416	-0.52800	0.80514
9	1.14583	0.34500	-0.60568	-0.48000	0.80273
10	1.16667	0.33000	-0.56955	-0.72000	0.79871
11	1.18750	0.31900	-0.56324	-0.52800	0.79541
12	1.20833	0.30700	-0.53693	-0.57600	0.79143
13	1.22917	0.29700	-0.49277	-0.48000	0.78778
14	1.25000	0.28900	-0.47139	-0.43200	0.78421
15	1.27083	0.27700	-0.48947	-0.52800	0.77945
16	1.29167	0.26700	-0.47924	-0.48000	0.77469
17	1.31250	0.25900	-0.46211	-0.38400	0.77056
18	1.33333	0.24600	-0.42389	-0.62400	0.76317
19	1.35417	0.23800	-0.38430	-0.38400	0.75814
20	1.37500	0.23500	-0.35633	-0.24000	0.75479
21	1.39583	0.22500	-0.34048	-0.38400	0.74909
22	1.41667	0.21800	-0.33900	-0.33600	0.74370
23	1.43750	0.21000	-0.36862	-0.38400	0.73706
24	1.45833	0.20300	-0.36155	-0.33600	0.73077
25	1.47917	0.19500	-0.32343	-0.38400	0.72296
26	1.50000	0.18800	-0.30504	-0.33600	0.71554
27	1.52083	0.18200	-0.28691	-0.28800	0.70869
28	1.54167	0.17800	-0.28237	-0.19200	0.70384
29	1.56250	0.17200	-0.28113	-0.28800	0.69612
30	1.58333	0.16400	-0.28849	-0.38400	0.68489
31	1.60417	0.15900	-0.27776	-0.24000	0.67726
32	1.62500	0.15300	-0.27039	-0.28800	0.66741
33	1.64583	0.14800	-0.24696	-0.24000	0.65857
34	1.66667	0.14300	-0.23074	-0.24000	0.64907
35	1.68750	0.13900	-0.23585	-0.19200	0.64096

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
2.2990 00	-2.0150-08	-2.2700-08	2.5450-09	-11.21161	0.8181
2.3360 00	-2.1960-08	-2.3760-08	1.8060-09	-7.60141	0.8173
2.4040 00	-2.3060-08	-2.5670-08	2.6160-09	-10.19047	0.8159
2.4810 00	-2.4810-08	-2.7870-08	3.0620-09	-10.98517	0.8141
2.5380 00	-2.7300-08	-2.9480-08	2.1800-09	-7.93436	0.8127
2.6180 00	-3.0370-08	-3.1740-08	1.3700-09	-4.31685	0.8107
2.7320 00	-3.4580-08	-3.4980-08	4.0620-10	-1.16099	0.8075
2.8170 00	-3.8120-08	-3.7380-08	-7.3330-10	1.96145	0.8051
2.8990 00	-4.2380-08	-3.9700-08	-2.6770-09	6.74234	0.8027
3.0300 00	-4.5880-08	-4.3440-08	-2.4490-09	5.63789	0.7987
3.1350 00	-4.8970-08	-4.6400-08	-2.5680-09	5.53415	0.7954
3.2570 00	-5.0410-08	-4.9870-08	-5.3760-10	1.07794	0.7914
3.3670 00	-5.5870-08	-5.2980-08	-2.8920-09	5.45926	0.7878
3.4720 00	-5.9400-08	-5.5960-08	-3.4350-09	6.13690	0.7842
3.6100 00	-5.8160-08	-5.9870-08	1.1710-09	-2.86700	0.7795
3.7450 00	-6.0370-08	-6.3710-08	3.3340-09	-5.23317	0.7747
3.8610 00	-6.3620-08	-6.6990-08	3.3660-09	-5.02516	0.7706
4.0650 00	-7.0460-08	-7.2770-08	2.3140-09	-3.17966	0.7632
4.2020 00	-7.8930-08	-7.6650-08	-2.2850-09	2.98106	0.7581
4.2920 00	-8.6440-08	-7.9200-08	-7.2340-09	9.13396	0.7548
4.4440 00	-9.1830-08	-8.3530-08	-8.3030-09	9.83966	0.7491
4.5870 00	-9.3610-08	-8.7580-08	-6.0320-09	6.88777	0.7437
4.7620 00	-8.7350-08	-9.2530-08	5.1770-09	-5.59448	0.7371
4.9260 00	-9.0350-08	-9.7190-08	6.8340-09	-7.03167	0.7308
5.1280 00	-1.0240-07	-1.0290-07	4.6690-10	-0.45366	0.7230
5.3190 00	-1.1020-07	-1.0830-07	-1.8220-09	1.68152	0.7155
5.4950 00	-1.1870-07	-1.1330-07	-5.4350-09	4.79721	0.7087
5.6180 00	-1.2230-07	-1.1680-07	-5.4970-09	4.70598	0.7038
5.8140 00	-1.2450-07	-1.2240-07	-2.1400-09	1.74876	0.6961
6.0980 00	-1.2290-07	-1.3040-07	7.4620-09	-5.72268	0.6849
6.2890 00	-1.2940-07	-1.3580-07	6.4690-09	-4.76221	0.6773
6.5360 00	-1.3460-07	-1.4280-07	8.2070-09	-5.74602	0.6674
6.7570 00	-1.4930-07	-1.4910-07	-1.6520-10	0.13094	0.6586
6.9930 00	-1.6180-07	-1.5580-07	-6.0100-09	3.85770	0.6491
7.1940 00	-1.6030-07	-1.6150-07	1.2220-09	-0.75689	0.6410

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 1.341D-17

VALUES OF OTHER INPUT PARAMETERS:

ALM= 45 KXDP= 0 TDEL= 2.0833D-02 TSTART= 8.7500D-01
 CATIN= 2.2400D-08 ASTART= 0.466 TI= 0.7510 T2= 1.1458

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.24810-08	2.17630-09	5.1231
C(2)	-2.83520-08	4.94750-10	-1.7450

MN(11)--PERIODATE SYSTEM: 34.03 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

MN(11)--PERIODATE SYSTEM: 34.03 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.17917	0.70800	-0.48725	-0.48000	0.81517
2	1.20000	0.69900	-0.58807	-0.43200	0.81605
3	1.22083	0.68300	-0.66294	-0.76800	0.81749
4	1.24167	0.67000	-0.70381	-0.62400	0.81855
5	1.26250	0.65400	-0.74685	-0.76800	0.81973
6	1.28333	0.63800	-0.77087	-0.76800	0.82076
7	1.30417	0.62400	-0.80232	-0.72000	0.82154
8	1.32500	0.60600	-0.83031	-0.86400	0.82236
9	1.34583	0.58700	-0.83725	-0.91200	0.82300
10	1.36667	0.57100	-0.85433	-0.76800	0.82335
11	1.38750	0.55100	-0.86554	-0.96000	0.82355
12	1.40833	0.53700	-0.82754	-0.67200	0.82351
13	1.42917	0.51800	-0.78769	-0.91200	0.82321
14	1.45000	0.50000	-0.75673	-0.86400	0.82266
15	1.47083	0.48500	-0.72800	-0.72000	0.82198
16	1.49167	0.47400	-0.71347	-0.52800	0.82135
17	1.51250	0.45800	-0.67663	-0.76600	0.82022
18	1.53333	0.44200	-0.66939	-0.76800	0.81881
19	1.55417	0.42800	-0.66092	-0.67200	0.81734
20	1.57500	0.41600	-0.63337	-0.57600	0.81588
21	1.59583	0.40400	-0.56477	-0.57600	0.81423
22	1.61667	0.39100	-0.53423	-0.62400	0.81221
23	1.63750	0.38000	-0.51802	-0.52800	0.81029
24	1.65833	0.37000	-0.50063	-0.48000	0.80837
25	1.67917	0.36200	-0.47709	-0.38400	0.80670
26	1.70000	0.34900	-0.46257	-0.62400	0.80372
27	1.72083	0.34000	-0.47027	-0.43200	0.80145
28	1.74167	0.33100	-0.46908	-0.43200	0.79899
29	1.76250	0.32200	-0.44123	-0.43200	0.79634
30	1.78333	0.31200	-0.42480	-0.48000	0.79314
31	1.80417	0.30200	-0.42562	-0.48000	0.78965
32	1.82500	0.29500	-0.40447	-0.33600	0.78701
33	1.84583	0.28800	-0.38192	-0.33600	0.78421
34	1.86667	0.27700	-0.37495	-0.52800	0.77945
35	1.88750	0.27100	-0.37104	-0.28800	0.77665
36	1.90833	0.26400	-0.35263	-0.33600	0.77318
37	1.92917	0.25600	-0.32858	-0.38400	0.76894
38	1.95000	0.24800	-0.32786	-0.38400	0.76438
39	1.97083	0.24300	-0.24603	-0.24000	0.76133
40	1.99167	0.23700	-0.33391	-0.28800	0.75748
41	2.01250	0.22800	-0.32461	-0.43200	0.75128
42	2.03333	0.22000	-0.31611	-0.38400	0.74528
43	2.05417	0.21500	-0.31792	-0.24000	0.74128

VALUES OF OTHER INPUT PARAMETERS:

NUM= 53 KDRUP= 0 IDELT= 2.08330-02 TSTART= 1.07500 00
 CATIN= 2.24000-08 ASTART= 0.757 T1= 0.9600 T2= 1.3875

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT (Y)
1.4120 00	-1.6760-08	-1.7740-08	9.7890-10	-5.51664	0.8152
1.4310 00	-1.6660-08	-1.8510-08	1.8500-09	-9.99378	0.8160
1.4640 00	-1.7450-08	-1.9910-08	2.4600-09	-12.35564	0.8175
1.4930 00	-1.9170-08	-2.1110-08	1.9350-09	-9.18765	0.8186
1.5290 00	-2.0840-08	-2.2640-08	1.8000-09	-7.95366	0.8197
1.5670 00	-2.3060-08	-2.4250-08	1.1830-09	-4.87738	0.8208
1.6030 00	-2.5110-08	-2.5120-08	6.1460-10	-2.38930	0.8215
1.6500 00	-2.7290-08	-2.7720-08	4.3220-10	-1.55931	0.8224
1.7040 00	-3.0240-08	-2.9960-08	-2.7780-10	0.92730	0.8230
1.7510 00	-3.2920-08	-3.1960-08	-9.5680-10	2.99352	0.8234
1.8150 00	-3.5910-08	-3.4630-08	-1.2780-09	3.68986	0.8235
1.8620 00	-3.8120-08	-3.6620-08	-1.5060-09	4.11166	0.8235
1.9310 00	-4.0640-08	-3.9480-08	-1.1600-09	2.93839	0.8232
2.0000 00	-4.2920-08	-4.2400-08	-5.2380-10	1.23539	0.8227
2.0620 00	-4.5260-08	-4.4990-08	-2.6310-10	0.58474	0.8220
2.1100 00	-4.6830-08	-4.7000-08	1.6910-10	-0.35975	0.8214
2.1830 00	-5.0090-08	-5.0090-08	6.9250-12	-0.01382	0.8202
2.2620 00	-5.1310-08	-5.3410-08	2.0990-09	-3.93072	0.8188
2.3360 00	-5.2670-08	-5.6510-08	3.8410-09	-6.79685	0.8173
2.4040 00	-5.5700-08	-5.9340-08	3.6410-09	-6.15556	0.8159
2.4750 00	-6.3290-08	-6.2340-08	-9.5480-10	1.53164	0.8142
2.5580 00	-6.7790-08	-6.5790-08	-1.9940-09	3.03097	0.8122
2.6320 00	-7.0810-08	-6.8900-08	-1.9090-09	2.77089	0.8103
2.7030 00	-7.4200-08	-7.1480-08	-2.3180-09	3.22441	0.8084
2.7620 00	-7.8840-08	-7.4390-08	-4.4560-09	5.95027	0.8067
2.8650 00	-8.2320-08	-7.8710-08	-3.6160-09	4.59368	0.8037
2.9410 00	-8.1970-08	-8.1890-08	-7.8810-11	0.09624	0.8014
3.0210 00	-8.3170-08	-8.5240-08	2.0750-09	-2.43414	0.7990
3.1060 00	-8.9480-08	-8.8790-08	-6.8930-10	0.77632	0.7963
3.2050 00	-9.4040-08	-9.2960-08	-1.0720-09	1.15284	0.7931
3.3110 00	-9.4950-08	-9.7420-08	2.4660-09	-2.53165	0.7896
3.3900 00	-1.0110-07	-1.0070-07	-3.5720-10	0.35470	0.7870
3.4720 00	-1.0830-07	-1.0420-07	-4.0880-09	3.92474	0.7842
3.6100 00	-1.1150-07	-1.1000-07	-1.5610-09	1.41983	0.7795
3.6900 00	-1.1390-07	-1.1130-07	-6.3940-10	0.56427	0.7766
3.7880 00	-1.2120-07	-1.1740-07	-3.8080-09	3.24330	0.7732
3.9060 00	-1.3150-07	-1.2240-07	-9.1330-09	7.46289	0.7689
4.0320 00	-1.3320-07	-1.2770-07	-5.5570-09	4.35298	0.7644
4.1150 00	-1.2760-07	-1.3120-07	3.5720-09	-2.72349	0.7613
4.2190 00	-1.3360-07	-1.3550-07	1.9150-09	-1.41271	0.7575
4.3860 00	-1.3890-07	-1.4250-07	3.6350-09	-2.55093	0.7513
4.5450 00	-1.4410-07	-1.4920-07	5.1190-09	-3.43120	0.7453
4.6510 00	-1.4470-07	-1.5360-07	8.5070-09	-5.79725	0.7413

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 7.5670-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.15210-08	1.39440-09	3.3584
C(2)	-4.19590-08	4.92110-10	-1.1728

PN(III)--PERIODATE SYSTEM: 34.04 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.10417	0.97500	-0.35501	-0.38400	0.76923
2	1.12500	0.97000	-0.39392	-0.24000	0.77046
3	1.14583	0.95900	-0.43624	-0.52800	0.77311
4	1.16667	0.95100	-0.46475	-0.38400	0.77499
5	1.18750	0.94000	-0.50971	-0.52800	0.77752
6	1.20833	0.93000	-0.53076	-0.48000	0.77976
7	1.22917	0.91700	-0.54819	-0.24000	0.78258
8	1.25000	0.90700	-0.58761	-0.48000	0.78668
9	1.27083	0.89300	-0.63659	-0.67200	0.78754
10	1.29167	0.88200	-0.68240	-0.52800	0.78970
11	1.31250	0.86500	-0.71942	-0.81600	0.79291
12	1.33333	0.85000	-0.73011	-0.72000	0.79561
13	1.35417	0.83300	-0.74284	-0.81600	0.79852
14	1.37500	0.82000	-0.74736	-0.62400	0.80065
15	1.39583	0.80400	-0.75147	-0.76800	0.80313
16	1.41667	0.79000	-0.75429	-0.67200	0.80520
17	1.43750	0.77000	-0.75685	-0.96000	0.80796
18	1.45833	0.75700	-0.74974	-0.62400	0.80965
19	1.47917	0.74000	-0.72521	-0.81600	0.81171
20	1.50000	0.72800	-0.71445	-0.57600	0.81308
21	1.52083	0.71100	-0.68602	-0.81600	0.81487
22	1.54167	0.69800	-0.66730	-0.62400	0.81614
23	1.56250	0.68300	-0.61791	-0.72000	0.81749
24	1.58333	0.67000	-0.59620	-0.62400	0.81855
25	1.60417	0.66000	-0.58855	-0.48000	0.81931
26	1.62500	0.64800	-0.60975	-0.57600	0.82014
27	1.64583	0.63500	-0.62984	-0.62400	0.82094
28	1.66667	0.62000	-0.63246	-0.72000	0.82174
29	1.68750	0.60600	-0.61287	-0.67200	0.82236
30	1.70833	0.59500	-0.57641	-0.52800	0.82276
31	1.72917	0.58300	-0.55703	-0.57600	0.82310
32	1.75000	0.57400	-0.54439	-0.43200	0.82330
33	1.77083	0.56100	-0.52225	-0.62400	0.82349
34	1.79167	0.54900	-0.50327	-0.57600	0.82355
35	1.81250	0.53800	-0.49981	-0.52800	0.82352
36	1.83333	0.53000	-0.49138	-0.38400	0.82343
37	1.85417	0.52200	-0.47404	-0.38400	0.82330
38	1.87500	0.50900	-0.48114	-0.62400	0.82297
39	1.89583	0.49700	-0.49238	-0.57600	0.82254
40	1.91667	0.49000	-0.47222	-0.33600	0.82223
41	1.93750	0.48000	-0.44483	-0.48000	0.82171
42	1.95833	0.47000	-0.42831	-0.48000	0.82109
43	1.97917	0.46100	-0.45069	-0.43200	0.82045
44	2.00000	0.45400	-0.45776	-0.33600	0.81990
45	2.02083	0.44200	-0.43516	-0.57600	0.81881
46	2.04166	0.43300	-0.41734	-0.43200	0.81789
47	2.06250	0.42400	-0.39532	-0.43200	0.81688
48	2.08333	0.41800	-0.38750	-0.28800	0.81614
49	2.10416	0.41000	-0.36360	-0.38400	0.81508
50	2.12500	0.40200	-0.36691	-0.38400	0.81394
51	2.14583	0.39400	-0.35261	-0.38400	0.81270
52	2.16666	0.38500	-0.34267	-0.43200	0.81118
53	2.18750	0.38100	-0.33269	-0.19200	0.81047
54	2.20833	0.37300	-0.34106	-0.38400	0.80896
55	2.22916	0.36700	-0.35277	-0.28800	0.80775
56	2.25000	0.35800	-0.35810	-0.43200	0.80582
57	2.27083	0.35000	-0.35368	-0.36400	0.80396
58	2.29166	0.34300	-0.33346	-0.33600	0.80223
59	2.31250	0.33700	-0.32104	-0.28800	0.80065
60	2.33333	0.33100	-0.31863	-0.28800	0.79899
61	2.35416	0.32400	-0.32928	-0.33600	0.79695
62	2.37500	0.31600	-0.33099	-0.38400	0.79445
63	2.39583	0.31000	-0.32995	-0.28800	0.79246
64	2.41666	0.30200	-0.30947	-0.38400	0.78965
65	2.43750	0.29700	-0.29930	-0.24000	0.78778
66	2.45833	0.29100	-0.29804	-0.28800	0.78543
67	2.47916	0.28400	-0.29453	-0.33600	0.78254
68	2.50000	0.27900	-0.28986	-0.24000	0.78035

VALUES OF OTHER INPUT PARAMETERS:

NUM= 78 KDROP= 0 TDELTA= 2.08330-02 TSTART= 1.00000 00
 CATIN= 2.24000-08 ASTART= 1.006 T1= 0.8050 T2= 1.4375

MNI(1)--PERIODATE SYSTEM: 34.04 INCLUDES ALLOWANCE FOR INDUCTION PERIOD 6/6/72

X	Y(OBS)	Y(LALC)	DEV(Y)	4 DEV(Y)	WEIGHT(Y)	
1.0260	00	-2.0290-08	-2.2880-08	2.5840-09	-11.29536	0.7692
1.0310	00	-2.0920-08	-2.3240-08	2.3150-09	-9.76377	0.7705
1.0430	00	-2.1430-08	-2.4050-08	2.6170-09	-10.88099	0.7731
1.0520	00	-2.2050-08	-2.4650-08	1.9990-09	-8.10850	0.7750
1.0640	00	-2.2310-08	-2.5500-08	2.3940-09	-9.38822	0.7775
1.0750	00	-2.2670-08	-2.6280-08	1.6130-09	-6.13622	0.7798
1.0910	00	-2.2640-08	-2.7330-08	9.1220-10	-3.33795	0.7826
1.1030	00	-2.7120-08	-2.8150-08	1.0390-09	-3.68894	0.7847
1.1200	00	-2.7440-08	-2.9340-08	1.9040-09	-6.48889	0.7875
1.1340	00	-2.7940-08	-3.0300-08	2.3640-09	-7.80181	0.7897
1.1560	00	-2.8820-08	-3.1830-08	3.0140-09	-9.46960	0.7929
1.1760	00	-3.0770-08	-3.3230-08	2.4570-09	-7.39501	0.7956
1.2000	00	-3.2680-08	-3.4880-08	2.2010-09	-6.30919	0.7985
1.2200	00	-3.4990-08	-3.6180-08	1.1940-09	-3.29895	0.8006
1.2440	00	-3.7390-08	-3.7850-08	4.6090-10	-1.21770	0.8031
1.2660	00	-3.9920-08	-3.9360-08	-5.5960-10	1.42169	0.8052
1.2990	00	-4.2540-08	-4.1620-08	-9.2380-10	2.21960	0.8080
1.3210	00	-4.5570-08	-4.3150-08	-4.1840-10	0.96951	0.8096
1.3510	00	-4.5690-08	-4.5240-08	-4.5240-10	1.00003	0.8117
1.3740	00	-4.7030-08	-4.6760-08	-2.6450-10	0.56550	0.8131
1.4060	00	-4.9660-08	-4.9020-08	-6.3960-10	1.30478	0.8149
1.4330	00	-5.1750-08	-5.0820-08	-9.3330-10	1.83648	0.8161
1.4640	00	-5.6640-08	-5.2980-08	-3.6650-09	6.91785	0.8175
1.4930	00	-5.9490-08	-5.4930-08	-4.5610-09	8.30280	0.8186
1.5150	00	-6.1050-08	-5.6480-08	-4.5740-09	8.09805	0.8193
1.5430	00	-5.9700-08	-5.8410-08	-1.2900-09	2.20854	0.8201
1.5750	00	-5.8530-08	-6.0580-08	2.0420-09	-3.37029	0.8209
1.6130	00	-5.9030-08	-6.3190-08	4.1620-09	-6.58598	0.8217
1.6500	00	-6.1680-08	-6.5750-08	4.0710-09	-6.19247	0.8224
1.6810	00	-6.6390-08	-6.7840-08	1.4550-09	-2.14494	0.8228
1.7150	00	-6.9540-08	-7.0220-08	6.8190-10	-0.97115	0.8231
1.7420	00	-7.2010-08	-7.2060-08	5.7220-11	-0.07940	0.8233
1.7830	00	-7.5950-08	-7.4840-08	-1.1180-09	1.49419	0.8235
1.8210	00	-7.9740-08	-7.7510-08	-2.2340-09	2.88260	0.8236
1.8590	00	-8.1230-08	-8.0070-08	-1.1630-09	1.45283	0.8235
1.8870	00	-8.3570-08	-8.1990-08	-1.5820-09	1.92923	0.8234
1.9160	00	-8.7620-08	-8.3980-08	-3.6370-09	4.33101	0.8233
1.9650	00	-8.7290-08	-8.7340-08	4.3930-11	-0.05031	0.8230
2.0120	00	-8.6250-08	-9.0590-08	4.3460-09	-4.79743	0.8225
2.0410	00	-9.0920-08	-9.2570-08	1.6480-09	-1.77992	0.8222
2.0830	00	-9.7570-08	-9.5490-08	-2.0800-09	2.17821	0.8217
2.1280	00	-1.0240-07	-9.8530-08	-3.8900-09	3.94819	0.8211
2.1690	00	-9.8370-08	-1.0140-07	3.0110-09	-2.97034	0.8205
2.2030	00	-9.7870-08	-1.0370-07	5.8090-09	-5.60271	0.8199
2.2620	00	-1.0400-07	-1.0780-07	3.7580-09	-3.48714	0.8188
2.3090	00	-1.0960-07	-1.1100-07	1.4270-09	-1.28581	0.8179
2.3580	00	-1.1690-07	-1.1440-07	-2.4930-09	2.17936	0.8169
2.3920	00	-1.2040-07	-1.1670-07	-3.7320-09	3.19818	0.8161
2.4390	00	-1.2960-07	-1.1990-07	-9.7260-09	8.11191	0.8151
2.4880	00	-1.2970-07	-1.2320-07	-6.4970-09	5.27187	0.8139
2.5380	00	-1.3630-07	-1.2670-07	-9.6150-09	7.58887	0.8127
2.5970	00	-1.4160-07	-1.3080-07	-1.0860-08	8.30288	0.8112
2.6250	00	-1.4730-07	-1.3260-07	-1.4640-08	11.03384	0.8105
2.6810	00	-1.4500-07	-1.3650-07	-8.5240-09	6.24425	0.8090
2.7250	00	-1.4150-07	-1.3950-07	-2.0230-09	1.45020	0.8078
2.7930	00	-1.4070-07	-1.4420-07	3.4800-09	-2.41319	0.8058
2.8570	00	-1.4380-07	-1.4860-07	4.7850-09	-3.22006	0.8040
2.9150	00	-1.5390-07	-1.5260-07	-1.3340-09	0.87417	0.8022
2.9670	00	-1.6130-07	-1.5620-07	-5.1750-09	3.31369	0.8007
3.0210	00	-1.6400-07	-1.5990-07	-4.1700-09	2.60844	0.7990
3.0860	00	-1.6010-07	-1.6430-07	4.1980-09	-2.55443	0.7969
3.1650	00	-1.6070-07	-1.6970-07	8.9820-09	-5.29276	0.7945
3.2260	00	-1.6270-07	-1.7390-07	1.1260-08	-6.47674	0.7925
3.3110	00	-1.7490-07	-1.7980-07	4.8610-09	-2.70378	0.7896
3.3670	00	-1.8240-07	-1.8360-07	1.1830-09	-0.64455	0.7878
3.4360	00	-1.8480-07	-1.8840-07	3.6130-09	-1.91802	0.7854
3.5210	00	-1.8860-07	-1.9420-07	5.6380-09	-2.90342	0.7825
3.5840	00	-1.9320-07	-1.9850-07	5.3210-09	-2.68052	0.7804

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 1.6490-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.75340-08	1.56040-09	3.2827
C(2)	-6.86490-08	7.37240-10	-1.0739

MN(11)--PERIODATE SYSTEM: 35.02 INDUCTION PERIOD CONSIDERED

6/7/72

MN(11)--PERIODATE SYSTEM: 35.02 INDUCTION PERIOD CONSIDERED

6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.31217	0.29600	-0.16860	-0.09600	0.78816
2	1.33300	0.29200	-0.19968	-0.28800	0.78583
3	1.35383	0.28800	-0.22656	-0.19200	0.78421
4	1.37467	0.28400	-0.27071	-0.19200	0.78254
5	1.39550	0.27700	-0.30135	-0.33600	0.77945
6	1.41633	0.27200	-0.31568	-0.24000	0.77713
7	1.43717	0.26400	-0.34313	-0.38400	0.77318
8	1.45800	0.25500	-0.34839	-0.43200	0.76838
9	1.47883	0.25000	-0.35457	-0.24000	0.76554
10	1.49967	0.24300	-0.36388	-0.33600	0.76133
11	1.52050	0.23400	-0.36433	-0.43200	0.75548
12	1.54133	0.22700	-0.37647	-0.33600	0.75056
13	1.56217	0.21800	-0.38496	-0.43200	0.74370
14	1.58300	0.21100	-0.38741	-0.33600	0.73792
15	1.60383	0.20300	-0.38444	-0.38400	0.73077
16	1.62467	0.19500	-0.38517	-0.38400	0.72296
17	1.64550	0.18700	-0.35730	-0.38400	0.71443
18	1.66633	0.17800	-0.34891	-0.43200	0.70384
19	1.68717	0.17300	-0.32332	-0.24000	0.69745
20	1.70800	0.16600	-0.30913	-0.33600	0.68780
21	1.72883	0.16100	-0.29741	-0.24000	0.68037
22	1.74967	0.15200	-0.29202	-0.43200	0.66569
23	1.77050	0.14800	-0.29827	-0.19200	0.65857
24	1.79133	0.14100	-0.28929	-0.33600	0.64508
25	1.81217	0.13600	-0.26842	-0.24000	0.63456
26	1.83300	0.13000	-0.24952	-0.28800	0.62083
27	1.85383	0.12400	-0.24650	-0.28800	0.60572
28	1.87467	0.12000	-0.20900	-0.19200	0.59478
29	1.89550	0.11700	-0.19454	-0.14400	0.58608
30	1.91633	0.11100	-0.17973	-0.28800	0.56722
31	1.93717	0.10800	-0.17791	-0.14400	0.55698
32	1.95800	0.10600	-0.18268	-0.09600	0.54983
33	1.97883	0.10000	-0.18854	-0.28800	0.52662
34	1.99967	0.09700	-0.18080	-0.14400	0.51392
35	2.02050	0.09300	-0.19085	-0.19200	0.49569

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
3.3560 00	-3.4010-08	-3.8040-08	4.0080-09	-10.68356	0.7882
3.4250 00	-3.5660-08	-4.0220-08	4.5610-09	-11.34030	0.7858
3.4720 00	-3.8210-08	-4.1700-08	3.4880-09	-8.36421	0.7842
3.5210 00	-3.8210-08	-4.3220-08	5.0090-09	-11.58919	0.7825
3.6100 00	-4.0420-08	-4.5980-08	5.5630-09	-12.09873	0.7795
3.6760 00	-4.4880-08	-4.8040-08	3.1670-09	-6.59160	0.7771
3.7880 00	-4.7510-08	-5.1900-08	3.9910-09	-7.74937	0.7732
3.9220 00	-5.3360-08	-5.3660-08	2.2980-09	-4.12962	0.7684
4.0000 00	-5.9300-08	-5.8090-08	-1.2060-09	2.07677	0.7655
4.1150 00	-6.4890-08	-6.1670-08	-3.2190-09	-5.21889	0.7613
4.2740 00	-7.2320-08	-6.6590-08	-5.7330-09	-8.60965	0.7555
4.4050 00	-7.7660-08	-7.0680-08	-6.9750-09	-9.86719	0.7506
4.5870 00	-8.3630-08	-7.6330-08	-7.4990-09	-9.82399	0.7437
4.7390 00	-9.1530-08	-8.1060-08	-1.0470-08	12.91117	0.7379
4.9260 00	-9.3450-08	-8.6860-08	-6.5860-09	-6.58600	0.7308
5.1280 00	-9.4490-08	-9.3140-08	-1.3430-09	-1.44166	0.7230
5.3480 00	-1.0320-07	-9.9960-08	-3.2050-08	-3.20506	0.7144
5.6180 00	-1.0700-07	-1.0840-07	1.3800-09	-1.27356	0.7038
5.7800 00	-1.1690-07	-1.1340-07	-3.4880-09	-3.07563	0.6974
6.0240 00	-1.2380-07	-1.2100-07	-2.7910-09	-2.30739	0.6878
6.2110 00	-1.3020-07	-1.2680-07	-3.4260-09	-2.70219	0.6804
6.5790 00	-1.3420-07	-1.3820-07	3.9980-09	-2.89243	0.6657
6.7570 00	-1.3300-07	-1.4370-07	1.0770-08	-7.49145	0.6586
7.0920 00	-1.3870-07	-1.5420-07	1.5450-08	-10.02118	0.6451
7.3530 00	-1.5120-07	-1.6230-07	1.1030-08	-6.79576	0.6346
7.6920 00	-1.6460-07	-1.7280-07	8.2440-09	-4.77069	0.6208
8.0650 00	-1.6850-07	-1.8440-07	1.5900-08	-8.62272	0.6057
8.3330 00	-2.0090-07	-1.9270-07	-8.2130-09	-4.26186	0.5948
8.5470 00	-2.1830-07	-1.9930-07	-1.8910-08	-9.44861	0.5861
9.0090 00	-2.3860-07	-2.1370-07	-2.5140-08	11.76199	0.5672
9.2590 00	-2.4390-07	-2.2150-07	-2.2430-08	10.12540	0.5570
9.4340 00	-2.4010-07	-2.2690-07	-1.3190-08	-5.81361	0.5498
1.0000 01	-2.3510-07	-2.4450-07	9.3860-09	-3.83913	0.5266
1.0310 01	-2.4770-07	-2.5410-07	6.3500-09	-2.49899	0.5139
1.0750 01	-2.3710-07	-2.6790-07	3.0730-08	-11.47081	0.4957

VALUES OF OTHER INPUT PARAMETERS:

NUM= 45 KDROP= 0 TDILT= 2.08330-02 TSTART= 1.20800 00
 CATI= 2.24000-08 ASTAKT= 0.307 T1= 1.1300 T2= 1.5830

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 7.2600-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	6.61660-08	5.01290-09	7.5763
C(2)	-3.10650-08	8.10990-10	-2.6106

PN(II)--PERIQUATE SYSTEM: 35.03

INDUCTION PERIOD CONSIDERED

6/7/72

PN(II)--PERIQUATE SYSTEM: 35.03

INDUCTION PERIOD CONSIDERED

6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSCISSANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.39617	0.49200	-0.06777	-0.04800	0.82233
2	1.41700	0.49000	-0.10748	-0.09600	0.82223
3	1.43783	0.48800	-0.15101	-0.09600	0.82214
4	1.45867	0.48400	-0.19954	-0.19200	0.82193
5	1.47950	0.48000	-0.23027	-0.19200	0.82171
6	1.50033	0.47300	-0.26460	-0.33600	0.82129
7	1.52117	0.46800	-0.29785	-0.24000	0.82096
8	1.54200	0.46200	-0.32305	-0.28800	0.82053
9	1.56283	0.45600	-0.35769	-0.28800	0.82006
10	1.58367	0.44600	-0.40402	-0.48000	0.81919
11	1.60450	0.43800	-0.44649	-0.38400	0.81842
12	1.62533	0.42900	-0.47680	-0.43200	0.81745
13	1.64617	0.41800	-0.48272	-0.52800	0.81614
14	1.66700	0.40700	-0.50651	-0.52800	0.81466
15	1.68783	0.39800	-0.53149	-0.43200	0.81333
16	1.70867	0.38600	-0.54572	-0.57600	0.81136
17	1.72950	0.37600	-0.55062	-0.48000	0.80954
18	1.75033	0.36100	-0.55582	-0.72000	0.80648
19	1.77117	0.35200	-0.54792	-0.43200	0.80444
20	1.79200	0.34000	-0.52923	-0.57600	0.80145
21	1.81283	0.33000	-0.50927	-0.48000	0.79871
22	1.83367	0.31900	-0.47848	-0.52800	0.79541
23	1.85450	0.30900	-0.47378	-0.48000	0.79212
24	1.87533	0.29900	-0.44792	-0.48000	0.78854
25	1.89617	0.29100	-0.43313	-0.38400	0.78543
26	1.91700	0.28200	-0.43555	-0.43200	0.78167
27	1.93783	0.27200	-0.43217	-0.48000	0.77713
28	1.95867	0.26400	-0.41933	-0.38400	0.77318
29	1.97950	0.25500	-0.40203	-0.43200	0.76838
30	2.00033	0.24500	-0.38672	-0.48000	0.76256
31	2.02117	0.24000	-0.37120	-0.24000	0.75943
32	2.04200	0.23200	-0.35596	-0.38400	0.75411
33	2.06283	0.22400	-0.33909	-0.38400	0.74834
34	2.08367	0.21600	-0.30994	-0.38400	0.74209
35	2.10450	0.21100	-0.30015	-0.24000	0.73792
36	2.12533	0.20500	-0.27249	-0.28800	0.73261
37	2.14617	0.19900	-0.27925	-0.28800	0.72695
38	2.16700	0.19500	-0.30068	-0.19200	0.72296
39	2.18783	0.18600	-0.31071	-0.43200	0.71331
40	2.20867	0.18100	-0.30832	-0.24000	0.70750
41	2.22950	0.17300	-0.28936	-0.38400	0.69745
42	2.25033	0.16800	-0.25599	-0.24000	0.69065
43	2.27117	0.16400	-0.22708	-0.19200	0.68489
44	2.29200	0.15800	-0.22284	-0.28800	0.67567
45	2.31283	0.15500	-0.21628	-0.14400	0.67078
46	2.33366	0.15000	-0.23133	-0.24000	0.66218
47	2.35450	0.14400	-0.23579	-0.28800	0.65103

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
2.0330	00	-4.9380-08	-3.6790-08	-1.2580-08	34.19744
2.0410	00	-4.0640-08	-3.7140-08	-3.5020-09	9.43084
2.0490	00	-3.6590-08	-3.7490-08	8.9320-10	-2.38291
2.0660	00	-3.4180-08	-3.8190-08	4.0110-09	-10.50395
2.0830	00	-3.5820-08	-3.8900-08	3.0760-09	-7.90625
2.1140	00	-3.7090-08	-4.0180-08	3.0840-09	-7.67681
2.1370	00	-3.8670-08	-4.1110-08	2.4480-09	-5.95492
2.1650	00	-4.1340-08	-4.2260-08	9.2670-10	-2.19267
2.1930	00	-4.2850-08	-4.3440-08	5.9280-10	-1.36440
2.2420	00	-4.3160-08	-4.5480-08	2.3230-09	-5.10826
2.2830	00	-4.4080-08	-4.7180-08	3.0970-09	-6.56399
2.3310	00	-4.6270-08	-4.9160-08	2.8900-09	-5.87808
2.3920	00	-5.0920-08	-5.1710-08	7.8490-10	-1.51793
2.4570	00	-5.3770-08	-5.4390-08	6.1740-10	-1.13524
2.5130	00	-5.6490-08	-5.6690-08	1.9910-10	-0.35120
2.5910	00	-6.0380-08	-5.9930-08	-4.5120-10	0.75285
2.6600	00	-6.5400-08	-6.2780-08	-2.6170-09	4.16894
2.7700	00	-7.0570-08	-6.7360-08	-3.2030-09	4.75547
2.8410	00	-7.2410-08	-7.0300-08	-2.1120-09	3.00392
2.9410	00	-7.5850-08	-7.4450-08	-1.3950-09	1.87301
3.0300	00	-7.8740-08	-7.8150-08	-1.5900-09	2.03493
3.1350	00	-8.5840-08	-8.2480-08	-3.3660-09	4.08066
3.2360	00	-8.7680-08	-8.6680-08	-9.9760-10	1.15086
3.3440	00	-9.3780-08	-9.1170-08	-2.6170-09	2.87028
3.4360	00	-9.8060-08	-9.4980-08	-3.0860-09	3.24879
3.5460	00	-9.8590-08	-9.9520-08	5.3400-10	-0.93850
3.6760	00	-1.0040-07	-1.0490-07	4.4850-09	-4.27459
3.7880	00	-1.0460-07	-1.0950-07	4.9140-09	-4.48600
3.9220	00	-1.1030-07	-1.1510-07	4.7930-09	-4.16449
4.0820	00	-1.1590-07	-1.2170-07	5.8530-09	-4.80889
4.1670	00	-1.2200-07	-1.2520-07	3.2740-09	-2.61452
4.3100	00	-1.2850-07	-1.3120-07	2.6980-09	-2.05628
4.4640	00	-1.3630-07	-1.3760-07	1.3060-09	-0.94929
4.6300	00	-1.5060-07	-1.4440-07	-6.1620-09	4.26654
4.7390	00	-1.5710-07	-1.4900-07	-8.0820-09	5.42517
4.8780	00	-1.7470-07	-1.5470-07	-1.9990-08	12.91685
5.0250	00	-1.7220-07	-1.6080-07	-1.1340-08	7.04997
5.1380	00	-1.6140-07	-1.6510-07	3.6650-09	-2.21426
5.3760	00	-1.5770-07	-1.7540-07	1.7650-08	-10.06417
5.5250	00	-1.6050-07	-1.8150-07	2.1070-08	-11.60454
5.7800	00	-1.7260-07	-1.9210-07	1.9530-08	-10.16530
5.9520	00	-1.9690-07	-1.9920-07	2.3380-09	-1.17325
6.0980	00	-2.2400-07	-2.0530-07	-1.8770-08	9.14587
6.3290	00	-2.3040-07	-2.1490-07	-1.5530-08	7.22641
6.4520	00	-2.3950-07	-2.1990-07	-1.9600-08	8.91156
6.6670	00	-2.2600-07	-2.2890-07	2.8780-09	-1.25776
6.9440	00	-2.2370-07	-2.4040-07	1.8680-08	-6.94064

GOODNESS OF FIT: GAUSS CRITERION, DMGA= 5.4660-17

VALUES OF OTHER INPUT PARAMETERS:

NUM= 57 KURUP= 0 TUELT= 2.08330-02 TSTART= 1.29200 00
 CATIN= 2.24000-08 ASTART= 0.497 T1= 1.2500 T2= 1.7503

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.74410-08	3.31170-09	6.9808
C(2)	-4.14440-08	8.50680-10	-2.0526

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT	X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1	1.31217	0.66000	-0.09883	-0.09600	0.81931	1.5150 00	-2.9780-08	-2.3320-08	-6.4650-09	27.72590	0.8193
2	1.33300	0.65800	-0.14971	-0.09600	0.81945	1.5200 00	-2.5710-08	-2.3550-08	-2.1620-09	9.18331	0.8195
3	1.35383	0.65500	-0.20558	-0.14400	0.81966	1.5270 00	-2.3600-08	-2.3900-08	-2.9450-10	-1.23244	0.8197
4	1.37467	0.64800	-0.27149	-0.33600	0.82014	1.5430 00	-2.2190-08	-2.4720-08	-2.5340-09	-10.25064	0.8201
5	1.39550	0.64600	-0.32360	-0.19200	0.82039	1.5530 00	-2.2540-08	-2.5200-08	-2.6650-09	-10.57448	0.8204
6	1.41633	0.63500	-0.37882	-0.43200	0.82094	1.5750 00	-2.2920-08	-2.6300-08	-3.3810-09	-12.85474	0.8209
7	1.43717	0.62700	-0.42108	-0.38400	0.82138	1.5950 00	-2.4210-08	-2.7310-08	-4.0980-09	-11.34399	0.8214
8	1.45800	0.61800	-0.44228	-0.43200	0.82183	1.6180 00	-2.6740-08	-2.6470-08	-1.7290-09	-6.07218	0.8218
9	1.47883	0.60900	-0.48877	-0.43200	0.82223	1.6420 00	-2.7790-08	-2.9670-08	-1.8810-09	-6.33926	0.8222
10	1.49967	0.59700	-0.52084	-0.57600	0.82269	1.6750 00	-2.9680-08	-3.1320-08	-1.6440-09	-5.24808	0.8227
11	1.52050	0.59700	-0.57105	-0.48000	0.82303	1.7040 00	-3.0570-08	-3.2750-08	-2.1850-09	-6.67293	0.8230
12	1.54133	0.57600	-0.61219	-0.52800	0.82326	1.7360 00	-3.1970-08	-3.4380-08	-2.4090-09	-7.00582	0.8233
13	1.56217	0.56000	-0.63291	-0.76800	0.82350	1.7860 00	-3.4460-08	-3.6860-08	-2.4010-09	-6.51236	0.8235
14	1.58300	0.54800	-0.63539	-0.57600	0.82355	1.8250 00	-3.8040-08	-3.8820-08	-7.7800-10	-2.00403	0.8236
15	1.60383	0.53400	-0.63119	-0.67200	0.82348	1.8730 00	-4.2230-08	-4.1220-08	-1.0110-09	-2.49385	0.8235
16	1.62467	0.52100	-0.64928	-0.62400	0.82328	1.9190 00	-4.5060-08	-4.3560-08	-1.5040-09	-3.45405	0.8233
17	1.64550	0.50900	-0.66165	-0.57600	0.82297	1.9650 00	-4.8330-08	-4.5820-08	-2.5130-09	-5.48546	0.8230
18	1.66633	0.49500	-0.69021	-0.67200	0.82246	2.0200 00	-5.0460-08	-4.8600-08	-1.8540-09	-3.81472	0.8225
19	1.68717	0.48000	-0.69135	-0.72000	0.82171	2.0830 00	-5.4660-08	-5.1760-08	-2.9010-09	-5.60508	0.8217
20	1.70800	0.46200	-0.68040	-0.86400	0.82053	2.1650 00	-5.6230-08	-5.5830-08	-4.0290-10	-0.72164	0.8205
21	1.72883	0.45200	-0.65097	-0.48000	0.81973	2.2120 00	-5.4490-08	-5.6220-08	-1.2650-09	-2.17240	0.8197
22	1.74967	0.43800	-0.60244	-0.67200	0.81842	2.2830 00	-6.5060-08	-6.1770-08	-3.2900-09	-5.32735	0.8184
23	1.77050	0.42600	-0.57169	-0.57600	0.81711	2.3470 00	-6.9370-08	-6.4990-08	-4.3860-09	-6.74937	0.8171
24	1.79133	0.41400	-0.58123	-0.57600	0.81562	2.4150 00	-6.9040-08	-6.8390-08	-6.4400-10	-0.94160	0.8156
25	1.81217	0.40200	-0.57906	-0.57600	0.81394	2.4880 00	-7.3100-08	-7.2000-08	-1.9010-09	-2.64031	0.8139
26	1.83300	0.39100	-0.55217	-0.52800	0.81221	2.5580 00	-7.4360-08	-7.5510-08	-1.1460-09	-1.51752	0.8122
27	1.85383	0.37800	-0.52701	-0.62400	0.80992	2.6460 00	-7.8790-08	-7.9910-08	-1.1150-09	-1.39482	0.8099
28	1.87467	0.36600	-0.48706	-0.57600	0.80755	2.7320 00	-8.6220-08	-8.4250-08	-1.9440-09	-2.33159	0.8075
29	1.89550	0.36000	-0.47263	-0.28800	0.80626	2.7780 00	-8.9840-08	-8.6530-08	-3.3030-09	-3.81722	0.8063
30	1.91633	0.34800	-0.46884	-0.57600	0.80526	2.8740 00	-9.1950-08	-9.1330-08	-6.2310-10	-0.66232	0.8035
31	1.93717	0.34000	-0.45100	-0.38400	0.80348	2.9410 00	-9.6210-08	-9.4710-08	-1.5010-09	-1.58436	0.8014
32	1.95800	0.33000	-0.45765	-0.48000	0.79871	3.0300 00	-9.5840-08	-9.9170-08	-3.3400-09	-3.36738	0.7987
33	1.97883	0.31800	-0.44475	-0.57600	0.79509	3.1450 00	-9.8780-08	-1.0490-07	6.1230-09	-5.83714	0.7951
34	1.99967	0.31000	-0.40013	-0.33600	0.79280	3.2150 00	-1.1190-07	-1.0840-07	-3.5010-09	-3.22811	0.7928
35	2.02050	0.30400	-0.38766	-0.33600	0.79037	3.2890 00	-1.1680-07	-1.1220-07	-4.6000-09	-4.10180	0.7904
36	2.04133	0.29400	-0.38401	-0.48000	0.78662	3.4010 00	-1.2560-07	-1.1780-07	-7.8840-09	-6.67881	0.7866
37	2.06217	0.28600	-0.35667	-0.28800	0.78421	3.4720 00	-1.2950-07	-1.2130-07	-8.2090-09	-6.76787	0.7842
38	2.08300	0.28100	-0.37618	-0.33600	0.78124	3.5590 00	-1.2400-07	-1.2560-07	-1.5960-09	-1.27041	0.7812
39	2.10383	0.27100	-0.38349	-0.48000	0.77665	3.6900 00	-1.2290-07	-1.3220-07	-9.3180-09	-7.04820	0.7766
40	2.12467	0.26500	-0.37090	-0.28800	0.77369	3.7740 00	-1.2630-07	-1.3660-07	-8.0720-09	-5.91867	0.7737
41	2.14550	0.25700	-0.35108	-0.38400	0.76948	3.8910 00	-1.3690-07	-1.4230-07	-5.3790-09	-3.78094	0.7695
42	2.16633	0.24800	-0.33517	-0.43200	0.76436	4.0320 00	-1.4480-07	-1.4490-07	-4.5600-09	-3.05339	0.7644
43	2.18717	0.24200	-0.31237	-0.28800	0.76070	4.1320 00	-1.5680-07	-1.5430-07	-2.4950-09	-1.61639	0.7607
44	2.20800	0.23800	-0.30146	-0.19200	0.75814	4.2020 00	-1.6410-07	-1.5780-07	-6.2410-09	-3.95664	0.7581
45	2.22883	0.23100	-0.29133	-0.33600	0.75341	4.3290 00	-1.7140-07	-1.6420-07	-7.1760-09	-4.37048	0.7534
46	2.24966	0.22200	-0.29954	-0.43200	0.74683	4.5050 00	-1.8820-07	-1.7300-07	-4.7520-09	-2.74719	0.7468
47	2.27050	0.21900	-0.29910	-0.14400	0.74500	4.5660 00	-1.7000-07	-1.7610-07	-6.0300-09	-3.42448	0.7450
48	2.29133	0.21200	-0.29031	-0.33600	0.73677	4.7170 00	-1.7660-07	-1.8360-07	-6.8260-09	-3.71752	0.7368
49	2.31216	0.20500	-0.26574	-0.33600	0.73261	4.8780 00	-1.9490-07	-1.9170-07	-3.2110-09	-1.67516	0.7326
50	2.33300	0.20000	-0.26259	-0.24000	0.72792	5.0000 00	-1.9900-07	-1.9780-07	-1.2220-09	-0.61761	0.7279
51	2.35383	0.19600	-0.25742	-0.19200	0.72398	5.1020 00	-2.0680-07	-2.0290-07	-1.9240-09	-0.94940	0.7240
52	2.37466	0.18900	-0.24443	-0.33600	0.71664	5.2910 00	-2.1760-07	-2.1240-07	-5.2590-09	-2.47631	0.7166
53	2.39550	0.18500	-0.24896	-0.19200	0.71218	5.4650 00	-2.4550-07	-2.1810-07	-2.5550-09	-1.17176	0.7122

GOODNESS OF FIT: GAUSS CRITERION, UMEGA= 1.3000-17

VALUES OF OTHER INPUT PARAMETERS:

NUM= 63 KUR0P= 0 TDEL= 2.08330-02 TSTART= 1.20800 00
CATIN= 2.24000-06 ASTART= 0.665 T1= 1.1670 T2= 1.6872

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	5.23420-08	1.47700-09	2.8112
C(2)	-5.00660-08	4.79780-10	-0.9583

MN(II)--PERIODATE SYSTEM: 35.05 INDUCTION PERIOD CONSIDERED 6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.43717	0.62700	-0.36052	-0.36400	0.79952
2	1.45800	0.62400	-0.41272	-0.24000	0.80033
3	1.47893	0.61200	-0.45698	-0.48000	0.80191
4	1.49967	0.79900	-0.49639	-0.62400	0.80388
5	1.52050	0.79200	-0.54587	-0.36600	0.80491
6	1.54133	0.78000	-0.59933	-0.57600	0.80661
7	1.56217	0.76500	-0.60560	-0.72000	0.80862
8	1.58300	0.75400	-0.64412	-0.57600	0.81015
9	1.60383	0.73900	-0.68870	-0.67200	0.81183
10	1.62467	0.72400	-0.71973	-0.72000	0.81351
11	1.64550	0.71200	-0.75589	-0.57600	0.81477
12	1.66633	0.69200	-0.79961	-0.96000	0.81670
13	1.68717	0.67600	-0.82293	-0.76800	0.81807
14	1.70800	0.65800	-0.82230	-0.86400	0.81945
15	1.72883	0.64300	-0.80070	-0.72000	0.82046
16	1.74967	0.62500	-0.76534	-0.86400	0.82149
17	1.77050	0.60900	-0.77710	-0.76800	0.82223
18	1.79133	0.59500	-0.74025	-0.67200	0.82276
19	1.81217	0.57900	-0.71871	-0.76800	0.82320
20	1.83300	0.56300	-0.68940	-0.76800	0.82347
21	1.85383	0.54800	-0.66787	-0.72000	0.82355
22	1.87467	0.53900	-0.64603	-0.43200	0.82352
23	1.89550	0.52200	-0.62284	-0.81600	0.82330
24	1.91633	0.51000	-0.60270	-0.57600	0.82300
25	1.93717	0.49800	-0.58245	-0.57600	0.82258
26	1.95800	0.48500	-0.57326	-0.62400	0.82198
27	1.97883	0.47400	-0.54521	-0.52800	0.82135
28	1.99967	0.46400	-0.54439	-0.48000	0.82068
29	2.02050	0.45200	-0.53126	-0.57600	0.81973
30	2.04133	0.43900	-0.52315	-0.62400	0.81852
31	2.06217	0.43000	-0.51309	-0.43200	0.81757
32	2.08300	0.42000	-0.49525	-0.48000	0.81639
33	2.10383	0.40900	-0.47774	-0.52800	0.81494
34	2.12467	0.39900	-0.46411	-0.48000	0.81348
35	2.14550	0.39000	-0.46434	-0.43200	0.81204
36	2.16633	0.38000	-0.44757	-0.48000	0.81029
37	2.18717	0.37100	-0.42349	-0.43200	0.80857
38	2.20800	0.36300	-0.41350	-0.38400	0.80691
39	2.22883	0.35300	-0.39097	-0.48000	0.80467
40	2.24967	0.34600	-0.37256	-0.33600	0.80298
41	2.27050	0.33900	-0.36993	-0.33600	0.80119
42	2.29133	0.33000	-0.36948	-0.43200	0.79871
43	2.31217	0.32400	-0.36035	-0.28800	0.79695
44	2.33300	0.31500	-0.37870	-0.43200	0.79413
45	2.35383	0.30700	-0.37456	-0.38400	0.79163
46	2.37467	0.30000	-0.36878	-0.33600	0.78891
47	2.39550	0.29300	-0.37196	-0.33600	0.78623
48	2.41633	0.28300	-0.35241	-0.48000	0.78211
49	2.43717	0.27800	-0.33703	-0.24000	0.77990
50	2.45800	0.27000	-0.33303	-0.38400	0.77617
51	2.47883	0.26300	-0.31878	-0.33600	0.77267
52	2.49966	0.25800	-0.31125	-0.24000	0.77003
53	2.52050	0.25100	-0.30556	-0.33600	0.76612
54	2.54133	0.24300	-0.27175	-0.38400	0.76133
55	2.56216	0.23900	-0.25553	-0.19200	0.75879

MN(II)--PERIODATE SYSTEM: 35.05 INDUCTION PERIOD CONSIDERED 6/7/72

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.2090 00	-2.5800-08	-2.7590-08	1.7840-09	-6.46722	0.7995
1.2110 00	-2.8920-08	-2.8020-08	1.3000-09	-3.35250	0.8003
1.2320 00	-2.7830-08	-2.8890-08	1.0580-09	-3.66254	0.8019
1.2520 00	-2.9460-08	-3.0060-08	5.9260-10	-1.97155	0.8039
1.2630 00	-3.0530-08	-3.0700-08	1.6940-10	-0.55165	0.8049
1.2820 00	-3.1440-08	-3.1840-08	3.9710-10	-1.24727	0.8066
1.3070 00	-3.4920-08	-3.3300-08	-1.0220-09	4.87145	0.8086
1.3280 00	-3.6620-08	-3.4510-08	-2.1090-09	6.11041	0.8101
1.3530 00	-3.7990-08	-3.5980-08	-2.0090-09	5.58489	0.8118
1.3810 00	-4.0110-08	-3.7610-08	-2.4990-09	6.64357	0.8135
1.4040 00	-4.1950-08	-3.8970-08	-2.9810-09	7.64939	0.8148
1.4450 00	-4.3380-08	-4.1340-08	-2.0400-09	4.93554	0.8167
1.4790 00	-4.5920-08	-4.3330-08	-2.5930-09	5.98411	0.8181
1.5200 00	-4.6530-08	-4.5690-08	-8.3720-10	1.83224	0.8195
1.5550 00	-4.8360-08	-4.7760-08	-6.0830-10	1.27367	0.8205
1.6000 00	-5.1210-08	-5.0370-08	-8.4160-10	1.67086	0.8215
1.6420 00	-5.1030-08	-5.2820-08	1.7830-09	-3.37566	0.8222
1.6810 00	-5.4210-08	-5.5070-08	8.6420-10	-1.56922	0.8228
1.7270 00	-5.6480-08	-5.7780-08	1.2970-09	-2.24455	0.8232
1.7760 00	-5.9560-08	-6.0640-08	1.0800-09	-1.78112	0.8235
1.8250 00	-6.2180-08	-6.3470-08	1.2950-09	-2.04082	0.8236
1.8550 00	-6.5000-08	-6.5250-08	2.4740-10	-0.37917	0.8235
1.9160 00	-6.8170-08	-6.8770-08	6.0000-10	-0.87253	0.8233
1.9610 00	-7.1220-08	-7.1400-08	1.7520-10	-0.24540	0.8230
2.0080 00	-7.4500-08	-7.4150-08	-3.4840-10	0.46979	0.8226
2.0620 00	-7.6510-08	-7.7290-08	7.8010-10	-1.00939	0.8220
2.1100 00	-8.1300-08	-8.0080-08	-1.2220-09	1.52657	0.8214
2.1550 00	-8.2260-08	-8.2730-08	4.4810-10	-0.54161	0.8207
2.2120 00	-8.3190-08	-8.4060-08	8.7150-10	-1.01267	0.8197
2.2780 00	-8.7400-08	-8.8880-08	2.4770-09	-2.75622	0.8185
2.3260 00	-9.0030-08	-9.2660-08	2.4330-09	-2.84161	0.8176
2.3810 00	-9.4210-08	-9.5890-08	1.6760-09	-1.74777	0.8164
2.4450 00	-9.8640-08	-9.9620-08	9.7850-10	-0.98225	0.8149
2.5060 00	-1.0250-07	-1.0320-07	6.4760-10	-0.62753	0.8135
2.5640 00	-1.0350-07	-1.0660-07	3.0630-09	-2.87454	0.8120
2.6320 00	-1.0850-07	-1.1050-07	2.0270-09	-1.83459	0.8103
2.6990 00	-1.1570-07	-1.1420-07	-1.4700-09	1.28691	0.8086
2.7350 00	-1.1960-07	-1.1770-07	-1.9300-09	1.63983	0.8069
2.8330 00	-1.2770-07	-1.2220-07	-5.6800-09	4.47198	0.8047
2.8920 00	-1.3530-07	-1.2560-07	-9.6900-09	7.71661	0.8030
2.9500 00	-1.3750-07	-1.2900-07	-8.4340-09	6.53553	0.8012
3.0300 00	-1.3890-07	-1.3370-07	-5.1740-09	3.86891	0.7987
3.0880 00	-1.4370-07	-1.3700-07	-6.7170-09	4.90263	0.7969
3.1750 00	-1.3800-07	-1.4210-07	4.1550-09	-2.92289	0.7941
3.2570 00	-1.4080-07	-1.4700-07	6.2020-09	-4.22007	0.7914
3.3330 00	-1.4420-07	-1.5140-07	7.1640-09	-4.73180	0.7889
3.4130 00	-1.4430-07	-1.5600-07	1.1780-08	-7.55189	0.7862
3.5340 00	-1.5380-07	-1.6310-07	9.4860-09	-5.81693	0.7821
3.5970 00	-1.6200-07	-1.6680-07	4.7950-09	-2.87689	0.7799
3.7040 00	-1.6530-07	-1.7300-07	7.6600-09	-4.42817	0.7762
3.8020 00	-1.7420-07	-1.7870-07	4.5530-09	-2.54752	0.7727
3.8760 00	-1.7990-07	-1.8300-07	3.1330-09	-1.71173	0.7700
3.9840 00	-1.8240-07	-1.8930-07	6.9560-09	-3.67419	0.7661
4.1150 00	-2.0950-07	-1.9700-07	-1.2500-08	6.34708	0.7613
4.1840 00	-2.2460-07	-2.0100-07	-2.3610-08	11.74481	0.7588

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.3040-17

VALUES OF OTHER INPUT PARAMETERS:

NUM= 65 KURUP= 0 IOELT= 2.08330-02 TSTART= 1.33300 00
 CATIN= 2.24000-06 ASTART= 0.846 TI= 1.1910 T2= 1.6872

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.28950-08	2.03960-09	4.7548
C(2)	-5.82890-08	8.24440-10	-1.4144

MN(11)--PERIODATE SYSTEM: 35.06

INDUCTION PERIOD CONSIDERED

6/7/72

MN(11)--PERIODATE SYSTEM: 35.06

INDUCTION PERIOD CONSIDERED

6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NG.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.22917	0.41000	-0.15220	-0.09600	0.81508
2	1.25000	0.40400	-0.22187	-0.28800	0.81423
3	1.27083	0.40000	-0.27403	-0.19200	0.81304
4	1.29167	0.39300	-0.31399	-0.33600	0.81254
5	1.31250	0.38800	-0.35649	-0.24000	0.81170
6	1.33333	0.37700	-0.40438	-0.54800	0.80973
7	1.35417	0.37100	-0.44626	-0.28800	0.80857
8	1.37500	0.36100	-0.46091	-0.48000	0.80648
9	1.39583	0.34900	-0.49616	-0.57600	0.80372
10	1.41667	0.33500	-0.52232	-0.48000	0.80119
11	1.43750	0.33000	-0.55773	-0.43200	0.79871
12	1.45833	0.31800	-0.57601	-0.57600	0.79509
13	1.47917	0.30300	-0.59872	-0.72000	0.79001
14	1.50000	0.29200	-0.60848	-0.52800	0.78583
15	1.52083	0.28000	-0.57863	-0.57600	0.78080
16	1.54167	0.26700	-0.54157	-0.62400	0.77469
17	1.56250	0.25700	-0.49518	-0.48000	0.76948
18	1.58333	0.24700	-0.46263	-0.48000	0.76377
19	1.60417	0.23800	-0.43755	-0.43200	0.75814
20	1.62500	0.22800	-0.40797	-0.48000	0.75128
21	1.64583	0.22200	-0.39716	-0.28800	0.74683
22	1.66667	0.21200	-0.38986	-0.48000	0.73877
23	1.68750	0.20300	-0.39340	-0.43200	0.73077
24	1.70833	0.19800	-0.38642	-0.24000	0.72597
25	1.72917	0.18800	-0.36332	-0.48000	0.71554
26	1.75000	0.18000	-0.34581	-0.38400	0.70629
27	1.77083	0.17300	-0.33056	-0.33600	0.69745
28	1.79167	0.16800	-0.31443	-0.24000	0.69065
29	1.81250	0.16200	-0.28525	-0.28800	0.68190
30	1.83333	0.15300	-0.28773	-0.43200	0.66741
31	1.85417	0.15000	-0.27705	-0.14400	0.66218
32	1.87500	0.14300	-0.27525	-0.33600	0.64907
33	1.89583	0.13800	-0.26184	-0.24000	0.63886
34	1.91667	0.13200	-0.25097	-0.28800	0.62555
35	1.93750	0.12800	-0.24060	-0.19200	0.61595

X	Y(OBS)	Y(CALC)	DEV(Y)	Δ DEV(Y)	WEIGHT(Y)
2.4390 00	-2.7120-08	-2.6320-08	-8.0130-10	3.04394	0.8151
2.4750 00	-2.4290-08	-2.7370-08	3.0780-09	-11.24698	0.8142
2.5000 00	-2.4680-08	-2.8080-08	3.2030-09	-11.40548	0.8136
2.5450 00	-2.6800-08	-2.9360-08	2.5680-09	-8.74578	0.8125
2.5770 00	-2.6590-08	-3.0310-08	1.7000-09	-5.80551	0.8117
2.6530 00	-2.5940-08	-3.2480-08	2.5320-09	-7.79522	0.8097
2.6950 00	-3.1680-08	-3.3710-08	1.8730-09	-5.55669	0.8086
2.7700 00	-3.5750-08	-3.5860-08	1.1810-10	-0.32937	0.8065
2.8650 00	-3.8110-08	-3.8610-08	4.9550-10	-1.28346	0.8037
2.9500 00	-4.1190-08	-4.1040-08	-1.4220-10	0.34648	0.8012
3.0300 00	-4.3540-08	-4.3360-08	-1.7640-10	0.40682	0.7987
3.1450 00	-4.7260-08	-4.6660-08	-5.9950-10	1.28448	0.7951
3.3000 00	-5.0820-08	-5.1140-08	3.2210-10	-0.62979	0.7900
3.4250 00	-5.5400-08	-5.4730-08	-6.7440-10	1.23232	0.7858
3.5710 00	-5.8870-08	-5.8960-08	8.2120-11	-0.13929	0.7808
3.7490 00	-6.3770-08	-6.3970-08	2.0240-10	-0.31661	0.7747
3.8910 00	-7.0680-08	-6.8170-08	-2.5140-09	3.68748	0.7695
4.0490 00	-7.8660-08	-7.2710-08	-3.9560-09	5.44056	0.7638
4.2020 00	-8.2120-08	-7.7120-08	-5.0050-09	6.44973	0.7581
4.3860 00	-8.9220-08	-8.2430-08	-6.7920-09	8.23918	0.7513
4.5050 00	-9.2830-08	-8.5850-08	-6.9800-09	8.13117	0.7468
4.7170 00	-9.5760-08	-9.1970-08	-3.7930-09	4.12366	0.7388
4.9260 00	-9.6090-08	-9.8000-08	1.9100-09	-1.94942	0.7308
5.0510 00	-9.9040-08	-1.0160-07	2.5530-09	-2.51364	0.7260
5.3190 00	-1.0660-07	-1.0930-07	2.7130-09	-2.48175	0.7155
5.5560 00	-1.1340-07	-1.1610-07	2.7730-09	-2.39214	0.7063
5.7880 00	-1.2000-07	-1.2260-07	2.6130-09	-2.13134	0.6974
5.9520 00	-1.2760-07	-1.2760-07	-6.5640-11	0.05146	0.6906
6.1730 00	-1.4230-07	-1.3390-07	-8.4070-09	6.27750	0.6819
6.5360 00	-1.4270-07	-1.4440-07	1.6620-09	-1.15102	0.6674
6.6670 00	-1.4990-07	-1.4820-07	-1.7550-09	1.18471	0.6622
6.9930 00	-1.5260-07	-1.5760-07	4.9740-09	-3.15676	0.6491
7.2460 00	-1.6220-07	-1.6490-07	2.6740-09	-1.62208	0.6389
7.5760 00	-1.7110-07	-1.7440-07	3.2810-09	-1.88173	0.6255
7.8130 00	-1.8040-07	-1.8120-07	7.9150-10	-0.43685	0.6160

GOODNESS OF FIT: GAUSS CRITERION, UMEGA = 7.6870-18

VALUES OF OTHER INPUT PARAMETERS:

NUM= 45 NURGP= 0 TDEL= 2.08330-02 TSTART= 1.12500 00
 CAT IN= 2.24000-08 ASTART= 0.415 T1= 1.0830 T2= 1.5000

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPM)
C(1)	4.39650-08	1.54290-09	3.5094
C(2)	-2.88180-08	3.38600-10	-1.1750

MN(11)--PERIODATE SYSTEM: 35.07 INDUCTION PERIOD CONSIDERED

6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	HEIGHT
1	1.43717	0.56800	-0.33929	-0.28800	0.82340
2	1.45800	0.55900	-0.40022	-0.43200	0.82350
3	1.47883	0.55100	-0.43399	-0.38400	0.82355
4	1.49967	0.54200	-0.47309	-0.43200	0.82354
5	1.52050	0.53100	-0.52142	-0.52800	0.82345
6	1.54133	0.52000	-0.56753	-0.52800	0.82326
7	1.56217	0.50900	-0.62282	-0.52800	0.82297
8	1.58300	0.49300	-0.67990	-0.76800	0.82237
9	1.60383	0.48000	-0.71135	-0.62400	0.82171
10	1.62467	0.46500	-0.73276	-0.72000	0.82075
11	1.64550	0.44900	-0.71182	-0.76800	0.81946
12	1.66633	0.43300	-0.70136	-0.76800	0.81789
13	1.68717	0.42100	-0.68634	-0.57600	0.81651
14	1.70800	0.40600	-0.67325	-0.72000	0.81452
15	1.72883	0.39400	-0.65649	-0.57600	0.81270
16	1.74967	0.37700	-0.63705	-0.81600	0.80973
17	1.77050	0.36700	-0.58540	-0.48000	0.80775
18	1.79133	0.35200	-0.52173	-0.72000	0.80444
19	1.81217	0.34400	-0.49549	-0.38400	0.80246
20	1.83300	0.33400	-0.49088	-0.48000	0.79983
21	1.85383	0.32600	-0.49398	-0.38400	0.79755
22	1.87467	0.31300	-0.48504	-0.62400	0.79347
23	1.89550	0.30100	-0.48916	-0.57600	0.78928
24	1.91633	0.29200	-0.45494	-0.43200	0.78583
25	1.93717	0.28500	-0.42243	-0.28800	0.78338
26	1.95800	0.27500	-0.40861	-0.52800	0.77853
27	1.97883	0.26700	-0.40366	-0.38400	0.77469
28	1.99967	0.25900	-0.40670	-0.38400	0.77056
29	2.02050	0.25000	-0.37803	-0.43200	0.76554
30	2.04133	0.24100	-0.35136	-0.43200	0.76007
31	2.06217	0.23700	-0.34052	-0.19200	0.75748
32	2.08300	0.22800	-0.32909	-0.43200	0.75128
33	2.10383	0.22300	-0.31290	-0.24000	0.74759
34	2.12467	0.21400	-0.31133	-0.43200	0.74045
35	2.14550	0.20900	-0.32306	-0.24000	0.73619
36	2.16633	0.20200	-0.30619	-0.33600	0.72983
37	2.18717	0.19700	-0.31020	-0.24000	0.72498
38	2.20800	0.18900	-0.30340	-0.38400	0.71664
39	2.22883	0.18200	-0.29468	-0.33600	0.70869
40	2.24967	0.17800	-0.27565	-0.19200	0.70384
41	2.27050	0.17100	-0.26777	-0.33600	0.69478

VALUES OF OTHER INPUT PARAMETERS:

NUM= 51 KOROP= 0 TDEL= 2.08330-02 TSTART= 1.33300 00
 CATIN= 2.24000-08 ASTART= 0.586 T1= 1.2300 T2= 1.6247

MN(11)--PERIODATE SYSTEM: 35.07

INDUCTION PERIOD CONSIDERED

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X	Y(OBS)	Y(CALC)	DEV(Y)	DEV(Y)	WEIGHT(Y)
1.7610 00	-2.9550-08	-3.2180-08	2.6250-09	-6.15768	0.8234
1.7890 00	-3.0350-08	-3.3290-08	2.9420-09	-6.83708	0.8235
1.8150 00	-3.3330-08	-3.4310-08	9.7140-10	-2.83156	0.8235
1.8450 00	-3.5910-08	-3.5490-08	-4.2820-10	1.20056	0.8235
1.8830 00	-3.7810-08	-3.6980-08	-8.3250-10	2.25112	0.8234
1.9230 00	-3.9900-08	-3.8540-08	-1.3630-09	3.53518	0.8233
1.9650 00	-4.1390-08	-4.0170-08	-1.2220-09	3.04244	0.8230
2.0280 00	-4.2820-08	-4.2660-08	-1.5610-10	0.36593	0.8224
2.0830 00	-4.5900-08	-4.4820-08	-1.0860-09	2.42261	0.8217
2.1510 00	-4.9670-08	-4.7450-08	-2.2190-09	4.67601	0.8207
2.2270 00	-5.1780-08	-5.0450-08	-1.3340-09	2.64533	0.8195
2.3090 00	-5.3220-08	-5.3670-08	4.4970-10	-0.83792	0.8179
2.3750 00	-5.5230-08	-5.6250-08	1.0210-09	-1.81506	0.8165
2.4630 00	-5.6830-08	-5.9680-08	2.8540-09	-4.78213	0.8145
2.5380 00	-5.8990-08	-6.2620-08	3.6290-09	-5.79526	0.8127
2.6530 00	-6.1520-08	-6.7100-08	5.5780-09	-8.31268	0.8097
2.7250 00	-6.7750-08	-6.9930-08	2.1320-09	-3.11969	0.8078
2.8410 00	-7.6910-08	-7.4470-08	-2.4350-09	3.26991	0.8044
2.9070 00	-8.1920-08	-7.7060-08	-4.8630-09	6.31081	0.8025
2.9940 00	-8.3640-08	-8.0470-08	-3.1750-09	3.94582	0.7998
3.0670 00	-8.4060-08	-8.3350-08	-7.1920-10	0.86297	0.7975
3.1950 00	-8.6580-08	-8.8330-08	1.7570-09	-1.98875	0.7935
3.3220 00	-8.8800-08	-9.3320-08	6.5190-09	-6.98834	0.7893
3.4250 00	-9.4360-08	-9.7330-08	2.9730-09	-3.05447	0.7858
3.4970 00	-1.0270-07	-1.0010-07	-2.5790-09	2.57548	0.7834
3.6360 00	-1.0730-07	-1.0560-07	-1.7820-09	1.63025	0.7785
3.7450 00	-1.0980-07	-1.0990-07	7.1090-11	-0.06470	0.7747
3.8610 00	-1.1010-07	-1.1440-07	4.2730-09	-3.73515	0.7706
4.0000 00	-1.1970-07	-1.1990-07	1.3010-10	-0.10858	0.7655
4.1490 00	-1.3010-07	-1.2570-07	-4.4400-09	3.53188	0.7601
4.2190 00	-1.3570-07	-1.2840-07	-7.2090-09	5.61265	0.7575
4.3860 00	-1.4180-07	-1.3500-07	-6.8180-09	5.05206	0.7513
4.4840 00	-1.5060-07	-1.3880-07	-1.1800-08	8.49965	0.7476
4.6730 00	-1.5290-07	-1.4620-07	-6.6720-09	4.56373	0.7405
4.7850 00	-1.4880-07	-1.5060-07	1.8100-09	-1.20237	0.7362
4.9500 00	-1.5850-07	-1.5710-07	-1.4170-09	0.90234	0.7298
5.0760 00	-1.5790-07	-1.6200-07	4.0460-09	-2.49765	0.7250
5.2910 00	-1.6300-07	-1.7040-07	7.3810-09	-4.33182	0.7166
5.4950 00	-1.6940-07	-1.7840-07	8.5370-09	-5.01040	0.7087
5.6180 00	-1.6280-07	-1.8320-07	3.8060-10	-0.20776	0.7038
5.8480 00	-1.8990-07	-1.9220-07	2.2620-09	-1.17697	0.6948

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 1.3050-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	3.67470-08	1.84790-09	5.0288
C(2)	-3.91500-08	5.32560-10	-1.3603

MN(11)--PERIODATE SYSTEM: 35.08

INDUCTION PERIOD CONSIDERED

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MN(11)--PERIODATE SYSTEM: 35.08

INDUCTION PERIOD CONSIDERED

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DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	1.31217	0.75500	-0.33051	-0.24030	0.80990
2	1.33300	0.74300	-0.42120	-0.57600	0.81136
3	1.35383	0.73800	-0.50479	-0.93800	0.81218
4	1.37467	0.72400	-0.57368	-0.57600	0.81351
5	1.39550	0.71400	-0.59916	-0.48000	0.81457
6	1.41633	0.69600	-0.62308	-0.86400	0.81633
7	1.43717	0.68600	-0.67480	-0.48000	0.81723
8	1.45800	0.67100	-0.71409	-0.72000	0.81848
9	1.47883	0.65800	-0.75465	-0.62400	0.81945
10	1.49967	0.64000	-0.78311	-0.86400	0.82064
11	1.52050	0.62200	-0.82449	-0.86400	0.82164
12	1.54133	0.60500	-0.80682	-0.81800	0.82240
13	1.56217	0.59000	-0.79912	-0.72000	0.82291
14	1.58300	0.57300	-0.77383	-0.81600	0.82332
15	1.60383	0.55700	-0.74694	-0.76800	0.82352
16	1.62467	0.54200	-0.74340	-0.72000	0.82354
17	1.64550	0.52500	-0.72688	-0.81600	0.82336
18	1.66633	0.51200	-0.68461	-0.62400	0.82306
19	1.68717	0.49900	-0.65153	-0.62400	0.82262
20	1.70800	0.48200	-0.60885	-0.81600	0.82182
21	1.72883	0.47200	-0.58295	-0.48000	0.82123
22	1.74967	0.46100	-0.58709	-0.52800	0.82045
23	1.77050	0.44800	-0.57567	-0.62400	0.81938
24	1.79133	0.43700	-0.57291	-0.52800	0.81831
25	1.81217	0.42300	-0.57374	-0.67200	0.81676
26	1.83300	0.41100	-0.54296	-0.57600	0.81522
27	1.85383	0.40200	-0.49808	-0.43200	0.81394
28	1.87467	0.39100	-0.47292	-0.52800	0.81221
29	1.89550	0.38200	-0.44525	-0.43200	0.81065
30	1.91633	0.37200	-0.44502	-0.48000	0.80876
31	1.93717	0.36400	-0.43718	-0.38400	0.80713
32	1.95800	0.35300	-0.41704	-0.52800	0.80467
33	1.97883	0.34500	-0.41100	-0.58400	0.80273
34	1.99967	0.33800	-0.42077	-0.33600	0.80092
35	2.02050	0.32800	-0.43365	-0.48000	0.79813
36	2.04133	0.32000	-0.42685	-0.38400	0.79572
37	2.06217	0.31000	-0.41994	-0.48000	0.79246
38	2.08300	0.30000	-0.38189	-0.48000	0.78891
39	2.10383	0.29400	-0.33458	-0.28800	0.78662
40	2.12467	0.28800	-0.31546	-0.28800	0.78421
41	2.14550	0.28100	-0.31777	-0.33600	0.78124
42	2.16633	0.27500	-0.34781	-0.28800	0.77853
43	2.18717	0.26700	-0.36836	-0.38400	0.77469
44	2.20800	0.25900	-0.36394	-0.38400	0.77056
45	2.22883	0.25000	-0.34937	-0.43200	0.76594
46	2.24966	0.24400	-0.32657	-0.28800	0.76194
47	2.27050	0.23900	-0.28936	-0.24000	0.75879
48	2.29133	0.23200	-0.27324	-0.33600	0.75411
49	2.31216	0.22600	-0.26731	-0.28800	0.74983

VALUES OF OTHER INPUT PARAMETERS:

NUM= 55 KDRDP= 0 IDELT= 2.0833D-02 TSTART= 1.20800 00
 CATIN= 2.2400D-08 ASTART= 0.772 T1= 1.1320 T2= 1.5205

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.3250 00	-2.2160-08	-2.3460-08	1.2980-09	-5.53243	0.8099
1.3460 00	-2.1640-08	-2.4550-08	2.9050-09	-11.83418	0.8114
1.3690 00	-2.2000-08	-2.5200-08	3.2010-09	-12.70202	0.8122
1.3810 00	-2.3160-08	-2.6350-08	3.1860-09	-12.09036	0.8135
1.4010 00	-2.6150-08	-2.7330-08	1.1850-09	-4.33397	0.8146
1.4370 00	-2.9250-08	-2.9180-08	-1.0010-10	0.34296	0.8163
1.4540 00	-3.1140-08	-3.0250-08	-8.9400-10	2.96246	0.8172
1.4900 00	-3.3580-08	-3.1910-08	-1.6780-09	5.25882	0.8185
1.5200 00	-3.5970-08	-3.3410-08	-2.5650-09	7.67712	0.8195
1.5630 00	-3.8950-08	-3.5580-08	-3.3700-09	9.46976	0.8206
1.6080 00	-4.1310-08	-3.7890-08	-3.4230-09	9.03511	0.8216
1.6530 00	-4.2790-08	-4.0190-08	-2.6050-09	6.48221	0.8224
1.6950 00	-4.3790-08	-4.2330-08	-1.4610-09	3.45145	0.8229
1.7450 00	-4.5820-08	-4.4890-08	-9.3350-10	2.07959	0.8233
1.7950 00	-4.8100-08	-4.7440-08	-6.5440-10	1.37936	0.8235
1.8450 00	-4.8950-08	-4.9970-08	1.0190-09	-2.04001	0.8235
1.9050 00	-5.0710-08	-5.3020-08	2.3090-09	-4.35427	0.8234
1.9530 00	-5.4520-08	-5.5480-08	9.5900-10	-1.72858	0.8231
2.0040 00	-5.8010-08	-5.8070-08	6.7050-11	-0.11546	0.8226
2.0750 00	-6.2860-08	-6.1670-08	-1.1850-09	1.92152	0.8218
2.1190 00	-6.6500-08	-6.3910-08	-2.5880-09	4.04864	0.8212
2.1690 00	-6.6760-08	-6.6490-08	-2.7090-10	0.40743	0.8205
2.2320 00	-6.8890-08	-6.9690-08	8.0130-10	-1.14973	0.8194
2.2830 00	-7.0040-08	-7.2550-08	2.5160-09	-3.46731	0.8183
2.3640 00	-7.0750-08	-7.6410-08	5.6630-09	-7.41052	0.8168
2.4330 00	-7.5620-08	-7.9930-08	4.3070-09	-5.38873	0.8152
2.4880 00	-8.3370-08	-8.2700-08	-6.6860-10	0.80839	0.8139
2.5580 00	-8.8790-08	-8.6270-08	-2.5250-09	2.92741	0.8122
2.6180 00	-9.3260-08	-8.9340-08	-3.9270-09	4.39614	0.8107
2.6880 00	-9.6660-08	-9.2920-08	-3.5370-09	3.80657	0.8088
2.7470 00	-9.9260-08	-9.5930-08	-3.3250-09	3.46639	0.8071
2.8330 00	-1.0520-07	-1.0030-07	-4.8750-09	4.86056	0.8047
2.8990 00	-1.0780-07	-1.0360-07	-4.2100-09	4.06237	0.8027
2.9540 00	-1.0650-07	-1.0670-07	2.4070-10	-0.22557	0.8009
3.0490 00	-1.0440-07	-1.1130-07	6.9220-09	-6.22011	0.7981
3.1250 00	-1.0710-07	-1.1520-07	8.0590-09	-6.99725	0.7957
3.2260 00	-1.1000-07	-1.2030-07	1.0310-08	-8.56824	0.7925
3.3330 00	-1.2220-07	-1.2580-07	3.6060-09	-2.86670	0.7889
3.4010 00	-1.3920-07	-1.2920-07	-9.9360-09	7.68735	0.7866
3.4720 00	-1.5090-07	-1.3290-07	-1.8010-08	13.55433	0.7842
3.5590 00	-1.5120-07	-1.3730-07	-1.3970-08	10.17958	0.7812
3.6360 00	-1.3950-07	-1.4120-07	1.7030-09	-1.20612	0.7785
3.7450 00	-1.3300-07	-1.4680-07	1.3770-08	-9.38174	0.7747
3.8610 00	-1.3590-07	-1.5270-07	1.6760-08	-10.98168	0.7706
4.0000 00	-1.4290-07	-1.5970-07	1.6840-08	-10.54227	0.7655
4.0980 00	-1.5430-07	-1.6480-07	1.0450-08	-6.34048	0.7619
4.1840 00	-1.7580-07	-1.6910-07	-6.6430-09	3.92813	0.7588
4.3100 00	-1.8780-07	-1.7560-07	-1.2290-08	7.00122	0.7541
4.4250 00	-1.9380-07	-1.8140-07	-1.2370-08	6.82252	0.7498

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 3.8060-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.40060-08	2.87100-09	6.5241
C(2)	-5.09370-08	1.08070-09	-2.1217

MN(III)--PERIODATE SYSTEM: 35.09 INDUCTION PERIOD CONSIDERED

6/7/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SCOPE	WEIGHT
1	1.39617	0.93700	-0.40861	-0.448000	0.77820
2	1.41700	0.92900	-0.51564	-0.384000	0.77998
3	1.43783	0.91500	-0.56276	-0.672000	0.78901
4	1.45667	0.90300	-0.65340	-0.576000	0.78551
5	1.47495	0.89000	-0.66985	-0.624000	0.78813
6	1.50033	0.87500	-0.74608	-0.720000	0.79104
7	1.52117	0.86000	-0.78737	-0.720000	0.79382
8	1.54200	0.84000	-0.85437	-0.960000	0.79734
9	1.56283	0.82700	-0.90019	-0.624000	0.79952
10	1.58367	0.80100	-0.94497	-1.248000	0.80359
11	1.60450	0.78700	-0.95364	-0.672000	0.80563
12	1.62533	0.76400	-0.93529	-1.104000	0.80875
13	1.64617	0.74500	-0.92741	-0.912000	0.81112
14	1.66700	0.72500	-0.86988	-0.960000	0.81340
15	1.68783	0.71000	-0.87740	-0.720000	0.81497
16	1.70867	0.69100	-0.86137	-0.912000	0.81679
17	1.72950	0.67200	-0.84852	-0.912000	0.81840
18	1.75033	0.65700	-0.82400	-0.720000	0.81952
19	1.77117	0.63600	-0.78506	-1.008000	0.82086
20	1.79200	0.62100	-0.73731	-0.720000	0.82169
21	1.81283	0.61000	-0.69736	-0.524000	0.82219
22	1.83367	0.59300	-0.67291	-0.816000	0.82282
23	1.85450	0.58000	-0.64901	-0.624000	0.82318
24	1.87533	0.56500	-0.63525	-0.720000	0.82344
25	1.89617	0.55400	-0.60225	-0.528000	0.82354
26	1.91700	0.54000	-0.57279	-0.672000	0.82353
27	1.93783	0.52400	-0.56240	-0.528000	0.82342
28	1.95867	0.51900	-0.58113	-0.480000	0.82324
29	1.97950	0.50500	-0.56192	-0.672000	0.82284
30	2.00033	0.49200	-0.54463	-0.624000	0.82233
31	2.02117	0.46100	-0.52729	-0.528000	0.82177
32	2.04200	0.47200	-0.52387	-0.432000	0.82123
33	2.06283	0.46300	-0.50356	-0.432000	0.82060
34	2.08367	0.44900	-0.50882	-0.672000	0.81946
35	2.10450	0.44000	-0.51047	-0.432000	0.81882
36	2.12533	0.42700	-0.47768	-0.624000	0.81723
37	2.14617	0.42100	-0.42984	-0.288000	0.81651
38	2.16700	0.41000	-0.42284	-0.528000	0.81508
39	2.18783	0.40200	-0.43052	-0.384000	0.81394
40	2.20867	0.39500	-0.43030	-0.336000	0.81286
41	2.22950	0.38400	-0.45288	-0.528000	0.81101
42	2.25033	0.37200	-0.43605	-0.576000	0.80876
43	2.27117	0.36700	-0.42458	-0.240000	0.80775
44	2.29200	0.35700	-0.39534	-0.480000	0.80559
45	2.31283	0.34800	-0.36751	-0.442000	0.80348
46	2.33367	0.34200	-0.36767	-0.288000	0.80197
47	2.35450	0.33400	-0.38079	-0.384000	0.79983
48	2.37533	0.32600	-0.37419	-0.384000	0.79755
49	2.39617	0.31800	-0.37932	-0.384000	0.79509
50	2.41700	0.31000	-0.37864	-0.384000	0.79246
51	2.43783	0.30200	-0.35332	-0.384000	0.78965
52	2.45867	0.29500	-0.31715	-0.336000	0.78701
53	2.47950	0.28900	-0.30144	-0.240000	0.78452
54	2.50033	0.28200	-0.30956	-0.336000	0.78167
55	2.52117	0.27700	-0.32573	-0.240000	0.77945
56	2.54200	0.27100	-0.33747	-0.288000	0.77665
57	2.56283	0.26100	-0.32477	-0.480000	0.77162

VALUES OF OTHER INPUT PARAMETERS:

NUM= 07 KURUP= 0 TDELTA= 2.08330-02 TSTART= 1.29200 00

LATIN= 2.24000-06 ASTART= 0.955 T1= 1.1910 T2= 1.6045

MN(III)--PERIODATE SYSTEM: 35.09

INDUCTION PERIOD CONSIDERED

6/7/72

X	Y(OBS)	Y(CALL)	DEV(Y)	% DEV(Y)	WEIGHT (Y)
1.0670 00	-2.1650-08	-2.3330-08	1.6790-09	-7.19451	0.7782
1.0760 00	-2.0820-08	-2.3890-08	3.0660-09	-12.83533	0.7800
1.0930 00	-2.1980-08	-2.4880-08	2.9050-09	-11.67401	0.7830
1.1070 00	-2.3050-08	-2.5760-08	2.7110-09	-10.52349	0.7855
1.1240 00	-2.6120-08	-2.6730-08	6.1390-10	-2.29038	0.7881
1.1450 00	-2.6460-08	-2.7690-08	9.3550-10	-3.35357	0.7910
1.1630 00	-2.9100-08	-2.9100-08	-5.3030-12	0.01823	0.7938
1.1900 00	-3.0300-08	-3.0770-08	4.6250-10	-1.80320	0.7973
1.2090 00	-3.2280-08	-3.1900-08	-3.8930-10	1.22043	0.7995
1.2480 00	-3.4300-08	-3.4260-08	-3.4580-11	0.10091	0.8036
1.2710 00	-3.7690-08	-3.5600-08	-2.0850-09	5.85649	0.8056
1.3090 00	-3.8930-08	-3.7910-08	-1.0160-09	2.68015	0.8088
1.3420 00	-3.9760-08	-3.9920-08	1.6360-10	-0.40984	0.8111
1.3790 00	-4.2930-08	-4.2160-08	-7.6880-10	1.82366	0.8134
1.4080 00	-4.3090-08	-4.3920-08	8.2470-10	-1.87802	0.8150
1.4470 00	-4.4430-08	-4.6250-08	1.8170-09	-3.92895	0.8168
1.4880 00	-4.5860-08	-4.8720-08	3.0630-09	-6.28603	0.8184
1.5220 00	-4.7880-08	-5.0770-08	3.1870-09	-6.27707	0.8195
1.5720 00	-5.0540-08	-5.3800-08	3.2640-09	-6.06674	0.8209
1.6100 00	-5.4440-08	-5.6090-08	1.6480-09	-2.93893	0.8217
1.6390 00	-5.8230-08	-5.7840-08	-3.8750-10	0.66997	0.8222
1.6860 00	-6.1040-08	-6.0680-08	-3.6180-10	0.59621	0.8228
1.7240 00	-6.4010-08	-6.2980-08	-1.0490-09	1.66671	0.8232
1.7700 00	-6.6120-08	-6.5720-08	-4.0470-10	0.81581	0.8234
1.8050 00	-7.0530-08	-6.7840-08	-2.6880-09	3.96213	0.8235
1.8520 00	-7.4470-08	-7.0660-08	-4.3060-09	6.09440	0.8235
1.8900 00	-7.4480-08	-7.2980-08	-1.4490-09	2.05169	0.8234
1.9270 00	-7.5500-08	-7.5180-08	-3.1730-10	0.42206	0.8232
1.9800 00	-7.8910-08	-7.8400-08	-5.0640-10	0.64592	0.8228
2.0330 00	-8.2270-08	-8.1560-08	-7.1320-10	0.87444	0.8223
2.0790 00	-8.5960-08	-8.4360-08	-1.4490-09	1.77675	0.8218
2.1190 00	-8.7310-08	-8.6750-08	-5.5940-10	0.64477	0.8212
2.1600 00	-9.1760-08	-8.9240-08	-2.5230-09	2.82739	0.8206
2.2270 00	-9.1730-08	-9.3300-08	1.5700-09	-1.68306	0.8195
2.2750 00	-9.2350-08	-9.6050-08	3.7010-09	-3.85285	0.8186
2.3420 00	-9.9660-08	-1.0020-07	5.5770-10	-0.55649	0.8172
2.3750 00	-1.1180-07	-1.0220-07	-9.6070-09	9.39741	0.8165
2.4390 00	-1.1480-07	-1.0610-07	-8.7170-09	8.21718	0.8151
2.4880 00	-1.1380-07	-1.0900-07	-4.8270-09	4.42791	0.8139
2.5320 00	-1.1500-07	-1.1170-07	-3.3090-09	2.96318	0.8129
2.6060 00	-1.1050-07	-1.1800-07	5.7860-09	-4.96697	0.8110
2.6880 00	-1.1560-07	-1.2110-07	5.5070-09	-4.54702	0.8088
2.7250 00	-1.1980-07	-1.2330-07	3.4940-09	-2.83354	0.8078
2.8010 00	-1.2990-07	-1.2790-07	-1.9450-09	1.52019	0.8056
2.8740 00	-1.4400-07	-1.3230-07	-8.6800-09	6.56114	0.8035
2.9240 00	-1.4220-07	-1.3530-07	-6.8440-09	5.05701	0.8020
2.9940 00	-1.3850-07	-1.3960-07	1.0530-09	-0.75485	0.7998
3.0670 00	-1.4220-07	-1.4400-07	1.7950-09	-1.24645	0.7975
3.1450 00	-1.4150-07	-1.4860-07	7.1420-09	-4.80461	0.7951
3.2360 00	-1.4300-07	-1.5350-07	1.0930-08	-6.87124	0.7925
3.3110 00	-1.5460-07	-1.5870-07	4.1350-09	-2.60558	0.7896
3.3900 00	-1.7370-07	-1.6340-07	-1.0220-08	6.25525	0.7870
3.4600 00	-1.8430-07	-1.6770-07	-1.6580-08	9.88629	0.7846
3.5460 00	-1.8090-07	-1.7290-07	-8.0700-09	4.66639	0.7817
3.6100 00	-1.7340-07	-1.7670-07	3.3390-09	-1.88958	0.7795
3.6900 00	-1.6870-07	-1.8150-07	1.2810-08	-7.00820	0.7766
3.8310 00	-1.7680-07	-1.9010-07	1.3310-08	-7.00122	0.7716

GODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.1800-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE OF DEGREE 1:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	4.10420-08	1.95340-09	4.7594
C(2)	-6.03200-08	8.63050-10	-1.4408

HN(II)--PERIODATE SYSTEM: DETA OF K2 FROM PLOT OF SLOPE VS AZERO

X	Y(OBS)	Y(CALC)	DEV(Y)	X DEV(Y)	WEIGHT(Y)
1.5080-08	-2.4180-08	-2.5010-08	8.2800-10	-3.51133	1.1995
1.9600-08	-2.8350-08	-3.1430-08	3.0740-09	-9.78019	1.6591
3.0600-08	-4.1960-08	-4.6140-08	4.1840-09	-9.06671	1.6502
4.7620-08	-6.8650-08	-6.9600-08	9.4460-10	-1.36019	1.0326
2.0510-08	-4.1070-08	-3.2130-08	1.0650-09	-3.31428	0.9759
2.3580-08	-4.1440-08	-3.6580-08	-4.8060-09	13.30454	0.9669
3.4940-08	-5.0070-08	-5.2050-08	1.9670-09	-3.81748	1.7069
3.6240-08	-5.8290-08	-5.3890-08	-4.3980-09	8.16103	0.9659
1.8250-08	-2.8620-08	-2.9310-08	4.9570-10	-1.69088	2.4092
2.1530-08	-3.9150-08	-3.3790-08	-5.3570-09	15.85364	1.5454
3.3470-08	-5.0940-08	-5.0740-08	-2.0140-10	0.39705	0.7474
3.9200-08	-6.0320-08	-5.7850-08	-2.4700-09	4.26973	0.8969

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 1.4e20-17

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	-4.46180-09	2.95190-09	-66.1583
C(2)	-1.36210 00	1.03230-01	-7.5784

DETERMINATION OF SYSTEM PARAMETERS--SUMMARY OF RESULTS

MEAN VALUES OF RATE CONSTANTS:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
K1	1.36240 04	2.74370 03	20.13963
K2	2.24120 08	1.48280 08	66.15834
K-2	8.43090 08	6.38930 07	7.57842

APPENDIX F

ESTIMATION OF K_{Ac}

Relationships between the stability constants of complexes and the characteristic properties of their constituents give information on the nature of the chemical bonding in complexes and may be used to make possible estimation of unknown stability constants.⁽²⁹⁾ A few linear plots of $\log K - \log K'$ can be found in the literature. Irving and Rossotti⁽³⁰⁾ and Freiser et al.⁽³¹⁾ found linear relationships between the stability constants of complexes of two metal ions with a series of related ligands. Irving and Rossotti also pointed out that the logarithm of the stability constants of the corresponding metal complexes formed with another but analogous ligand give straight lines.

In a search for an approximate value for the stability constant of the manganese (III)-acetate complex ($M\text{L}_3$), a few correlating plots were tried. The main difficulty is the lack of data for the formation constant of trivalent metal cations. Plotting the $\log M(\text{II})$ vs. $\log M(\text{III})$ for the chelates of iron and manganese with a series of aminopolycarboxylic acids, (Figure 28) roughly a straight line relationship is obtained. If the value for the manganese (II)-acetate complex, MnA_2 , is entered in this plot, $\log K$ for MnA_3 would seem to have a value of 13.8. It is of interest to observe that by means of this plot the $\log K$ for $\text{Mn}(\text{III})$ -NTA complex is equal to 19.5, in reasonable good agreement with a recently reported value of 20.25.⁽²⁸⁾ In Figure 29 $\log K$ of the

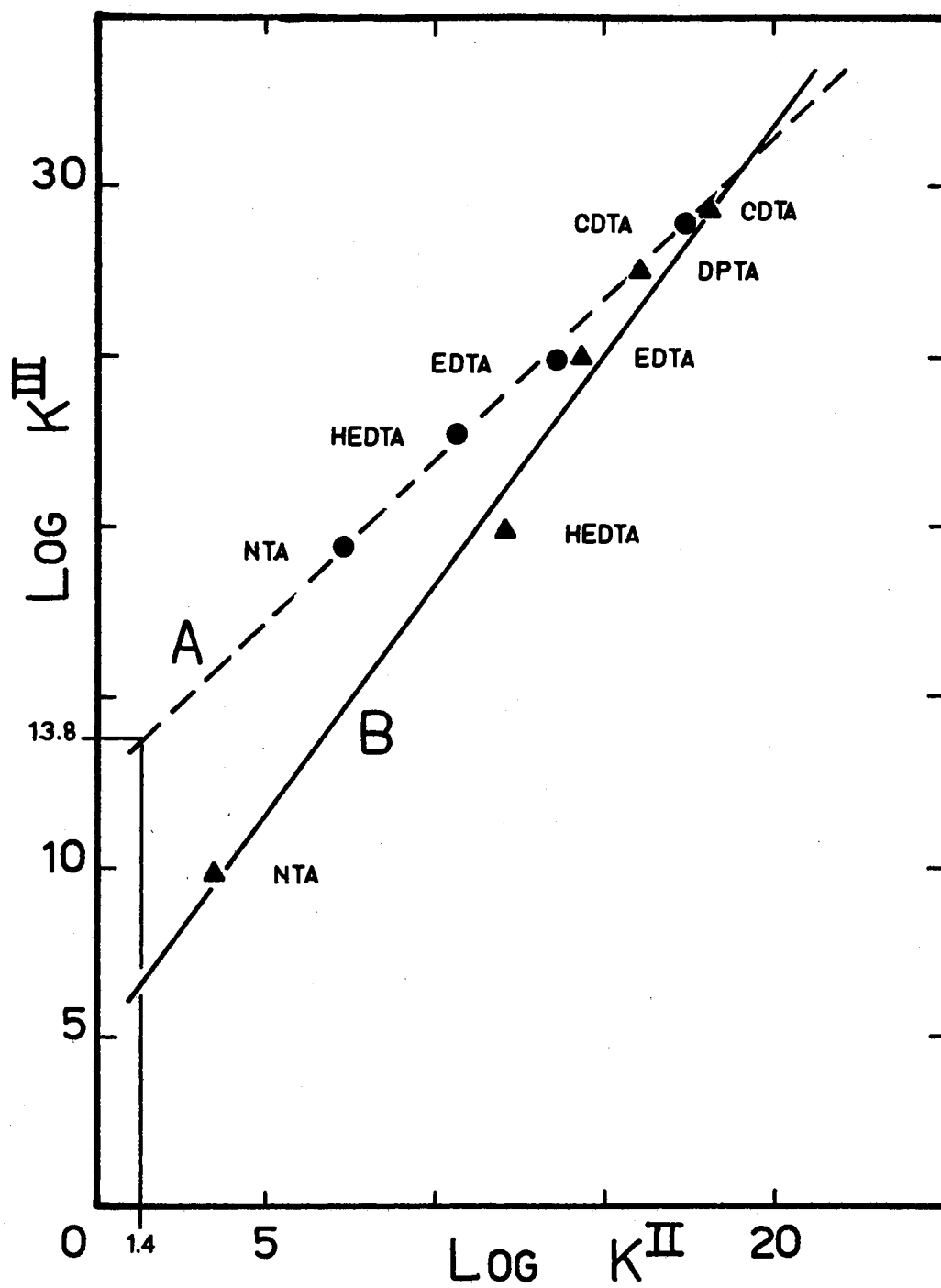


Figure 28. Estimation of Formation Constant of Mn(III)-Acetate Complex. Curve A: Manganese Complexes. Curve B: Iron Complexes. Constants From Ringbom (32) and Hamm (33)

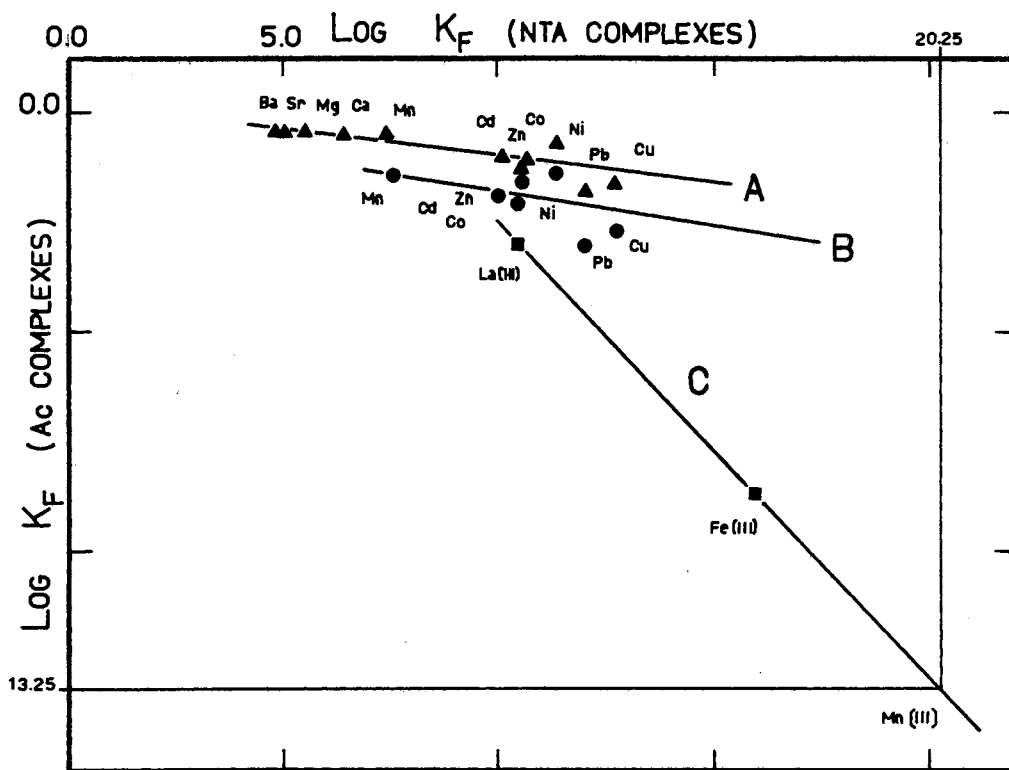
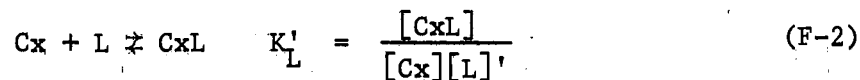
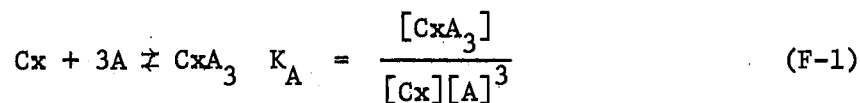


Figure 29. Estimation of Formation Constant of Mn(III)-Acetate Complex. Curve A: Monovalent Metal Complexes. Curve B: Divalent Metal Complexes. Curve C: Trivalent Metal Complexes. Constants From Ringbom (32)

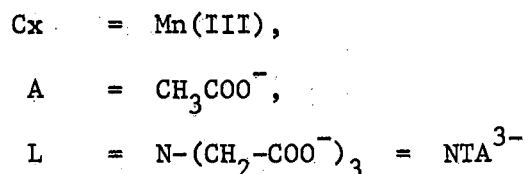
MA complexes for a series of bivalent cations are plotted against the corresponding log K for the NTA complexes. A definite trend which could be roughly fitted by a straight line is observed. The MA₂ complexes seem to follow the same trend with a slightly steeper slope. The only two trivalent cations which could be used to construct a similar plot for the MA₃ complexes are iron (III) and lanthanum (III). Recognizing that is rather brave to fit a straight line through these two points, when this is done though, and the value for Mn(III)-NTA is entered, a value of log K = 13.25 is obtained which coincidentally or surprisingly agrees very well with the value obtained in the plot of aminopolycarboxylate complexes. In light of these observations, a reasonable maximum limit for the value of log K for the Mn(III)-Acetate complex can be set at $K_F^{Ac^-} \leq 10^{14}$.

Having this estimate in hand, the competition of NTA and Acetate for any Mn(III) present in a given system can be represented in the following manner:



(Note: 3:1 Ac complex is preferred due to large concn. of Ac⁻)

where:



- K_A = formation constant for the Mn(III)-acetate complex,
 K'_L = conditional formation constant for the Mn(III)-NDA³⁻
 complex (32), and
 $[L]'$ = all forms of the ligand present not complexed with
 Mn(III) (32).

From the required mass balance:

$$[C]_0 = [Cx] + [CxA_3] + [CxL] \quad (F-3)$$

where:

$$[C]_0 = \text{total catalyst added to the system.}$$

From the formation constant expressions:

$$[CxA_3] = K_A [Cx][A]^3 \text{ and} \quad (F-4)$$

$$[CxL] = K'_L [Cx][L]' \quad (F-5)$$

Substitution of these expressions into Equation (F-3) and solving for [Cx] gives:

$$[Cx] = \frac{[C]_0}{1 + K_A [A]^3 + K'_L [L]'} \quad (F-6)$$

Substitution of Equation [F-6] into Equation [F-5] leads to:

$$[CxL] = \frac{K'_L [L]' [C]_0}{1 + K_A [A]^3 + K'_L [L]'} \quad (F-7)$$

But, from mass balance:

$$[L]' = C_L - [CxL] \quad (F-8)$$

Substitution of this expression into Equation [F-7] yields:

$$[C_{xL}] = \frac{K'_L (C_L - [C_{xL}])[C]_o}{1 + K_A[A]^3 + K'_L (C_L - [C_{xL}])} \quad (F-9)$$

Letting $x = [C_{xL}]$ to simplify the algebra somewhat and proceeding with the solution:

$$x + K_A[A]^3 x + K'_L C_{Lx} - K'_L x^2 = K'_L C_L [C]_o - K'_L [C]_o x \quad (F-10)$$

$$K'_L x^2 - (1 + K_A[A]^3 + K'_L C_L + K'_L [C]_o)x + K'_L C_L [C]_o = 0 \quad (F-11)$$

$$K'_L x^2 - (1 + K_A[A]^3 + (C_L + [C]_o)K'_L)x + K'_L C_L [C]_o = 0 \quad (F-12)$$

Application of the quadratic formula and selection of the negative root since this gives the proper result when $C_L = 0.0$, leads to the final expression for concentration of Mn(III)-complex:

$$[C_{xL}] = \left[\frac{[1 + K_A[A]^3 + (C_L + [C]_o)K'_L] - \sqrt{[1 + K_A[A]^3 + (C_L + [C]_o)K'_L]^2 - 4K'_L{}^2 C_L [C]_o}}{2 K'_L} \right] \quad (F-13)$$

According to Ringbom (32), a value for K'_L may be obtained from the expression:

$$K'_L = \frac{K_L}{\alpha_L(H)}$$

where:

- K_L = the formation constant for Mn(III)-NTA³⁻ complex and
 $\alpha_L(H)$ = the inverse of the fraction of NTA present in the N-(CH₂-COO⁻)₃ form.

Since $K_L = 10^{20.25} = 1.8 \times 10^{20}$ and, from Table A.4c in Ringbom's book, $\alpha_L(H)$ for NTA at pH = 4.7 can be interpolated as $\alpha_L(H) = 5.1$, the final value for the conditional formation constant obtained was: $K'_L = 3.5 \times 10^{19}$.

Looking at the term

$$T = 1 + K_A[A]^3 + (C_L + [C]_o) K'_L$$

in Equation [F-13] and assigning the following values used in obtaining titration curves:

$$[A] = 0.5, C_L = 10^{-5}, [C]_o = 10^{-8}, \text{ and } K'_L = 3.5 \times 10^{19}$$

leads to:

$$\begin{aligned} T &= 1 + K_A(.125) + 10^{-5}(3.5 \times 10^{19}) \\ &\approx (.125) K_A + 3.5 \times 10^{14} \end{aligned} \quad (\text{F-15})$$

Since a maximum value of 10^{14} has been set for K_A , the above expression becomes:

$$T = (.125 \times 10^{14}) + (3.5 \times 10^{14}) \quad (\text{F-16})$$

It can be seen, then, that a value of $K_A = 10^{14}$, under the conditions specified, introduces an "acetate effect" of only $\frac{.125}{3.5} \times 100\%$ or 3.6%. In light of the satisfactory results obtained and considering the magnitude of other errors introduced in estimation, it seems reasonable to assume that, for all practical purposes, all of the Mn(III) present in the system will be complexed by NTA.

APPENDIX G

COMPLETE LISTING OF OUTPUT FROM DETERMINATION
OF SYSTEM PARAMETERS--NTA PRESENT

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.47917	0.72600	-0.57482	-0.48000	0.81308
2	0.50000	0.71600	-0.73657	-0.57600	0.81436
3	0.52083	0.69700	-0.82420	-0.91200	0.81624
4	0.54167	0.67900	-0.93649	-0.86400	0.81783
5	0.56250	0.65600	-0.99540	-1.10400	0.81959
6	0.58333	0.63800	-1.03721	-0.86400	0.82076
7	0.60417	0.62000	-1.05320	-0.86400	0.82174
8	0.62500	0.59000	-1.07595	-1.44000	0.82291
9	0.64583	0.57100	-1.11265	-0.91200	0.82335
10	0.66667	0.54700	-1.15308	-1.15200	0.82355
11	0.68750	0.52500	-1.15620	-1.05600	0.82336
12	0.70833	0.50000	-1.16133	-1.20000	0.82266
13	0.72917	0.47300	-1.15072	-1.29600	0.82129
14	0.75000	0.45100	-1.10904	-1.05600	0.81964
15	0.77083	0.42800	-1.07223	-1.10400	0.81734
16	0.79167	0.40600	-1.03406	-1.05600	0.81452
17	0.81250	0.38900	-1.03013	-0.81600	0.81187
18	0.83333	0.36200	-1.02480	-1.29600	0.80670
19	0.85417	0.34300	-0.98444	-0.91200	0.80223
20	0.87500	0.32200	-0.96306	-1.00800	0.79634
21	0.89583	0.30200	-0.91846	-0.96000	0.78965
22	0.91667	0.28600	-0.85958	-0.76800	0.78338
23	0.93750	0.26800	-0.81961	-0.86400	0.77519
24	0.95833	0.24800	-0.77291	-0.96000	0.76436
25	0.97917	0.23500	-0.72593	-0.62400	0.75615
26	1.00000	0.22000	-0.68727	-0.72000	0.74528
27	1.02083	0.20800	-0.63895	-0.57600	0.73531
28	1.04167	0.19200	-0.58809	-0.76800	0.71986
29	1.06250	0.18200	-0.56464	-0.48000	0.70869
30	1.08333	0.16900	-0.51922	-0.62400	0.69204
31	1.10417	0.16000	-0.47883	-0.43200	0.67883
32	1.12500	0.15200	-0.43340	-0.38400	0.66569
33	1.14583	0.14000	-0.40845	-0.57600	0.64304
34	1.16667	0.13300	-0.37758	-0.33600	0.62785
35	1.18750	0.12600	-0.36617	-0.33600	0.61092

X	Y(OBS)	Y(CALC)	DEV(Y)	Z DEV(Y)	WEIGHT(Y)
1.3740 00	-1.0020-08	-6.7510-09	-3.2650-09	48.36313	0.8131
1.3970 00	-8.7630-09	-6.9630-09	-1.4190-09	26.12642	0.8144
1.4350 00	-8.7200-09	-7.3150-09	-1.4060-09	19.21817	0.8162
1.4730 00	-8.5600-09	-7.6660-09	-8.9500-10	11.67519	0.8178
1.5240 00	-8.8940-09	-8.1420-09	-7.5180-10	9.23342	0.8196
1.5670 00	-9.3610-09	-8.3390-09	-8.4250-10	9.86714	0.8208
1.6130 00	-1.0110-08	-8.9590-09	-1.1530-09	12.86933	0.8217
1.6950 00	-1.0790-08	-9.7150-09	-1.0750-09	11.06584	0.8229
1.7510 00	-1.1340-08	-1.0240-08	-1.0990-09	10.73993	0.8234
1.8280 00	-1.1840-08	-1.0940-08	-8.9770-10	8.20205	0.8236
1.9050 00	-1.2700-08	-1.1650-08	-1.0970-09	9.41723	0.8234
2.0000 00	-1.3660-08	-1.2530-08	-1.1320-09	9.03477	0.8227
2.1140 00	-1.4190-08	-1.3580-08	-6.1010-10	4.49138	0.8213
2.2170 00	-1.5150-08	-1.4540-08	-6.1280-10	4.21617	0.8196
2.3360 00	-1.6100-08	-1.5630-08	-4.6870-10	2.99777	0.8173
2.4630 00	-1.7150-08	-1.6800-08	-3.4610-10	2.05983	0.8145
2.5710 00	-1.7670-08	-1.7800-08	1.2840-10	-0.72241	0.8119
2.7620 00	-1.8210-08	-1.9570-08	1.3510-09	-6.90284	0.8067
2.9150 00	-1.9440-08	-2.0980-08	1.5420-09	-7.34897	0.8022
3.1060 00	-2.0350-08	-2.2730-08	2.3800-09	-10.46990	0.7963
3.3110 00	-2.1850-08	-2.4630-08	2.7810-09	-11.29302	0.7896
3.4970 00	-2.3890-08	-2.6340-08	2.4510-09	-9.30641	0.7834
3.7310 00	-2.5620-08	-2.8510-08	2.8840-09	-10.11627	0.7752
4.0320 00	-2.7770-08	-3.1280-08	3.5080-09	-11.21480	0.7644
4.2550 00	-3.0210-08	-3.3340-08	3.1260-09	-9.37707	0.7562
4.5450 00	-3.2590-08	-3.6020-08	3.6250-09	-9.50919	0.7453
4.8080 00	-3.5790-08	-3.8440-08	2.6490-09	-6.89221	0.7353
5.2080 00	-3.9680-08	-4.2130-08	2.4540-09	-5.83320	0.7199
5.4950 00	-4.2150-08	-4.4770-08	2.6240-09	-5.86056	0.7087
5.9170 00	-4.6740-08	-4.8670-08	1.9370-09	-3.98021	0.6920
6.2500 00	-5.1650-08	-5.1750-08	9.1340-11	-0.17652	0.6788
6.5790 00	-5.8140-08	-5.4780-08	-3.3640-09	6.14142	0.6657
7.1430 00	-6.2840-08	-5.9980-08	-2.8560-09	4.76053	0.6430
7.5190 00	-6.4210-08	-6.3450-08	-5.7610-09	9.07863	0.6279
7.9370 00	-7.2640-08	-6.7310-08	-5.3360-09	7.92825	0.6109

GOODNESS OF FIT: GAUSS CRITERION: OMEGA= 4.2430-18

VALUES OF OTHER INPUT PARAMETERS:

NUM= 45 KDRCP= 0 TDILT= 2.08330-02 TSTART= 3.75000-01
 CATIN= 2.24000-08 ASTART= 0.755 T1= 0.1320 T2= 0.7083

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STO DEV	REL STD DEV(PPH)
C(1)	5.92370-09	8.02260-10	13.5433
C(2)	-9.22710-09	2.12700-10	-2.3052

MN(III)--PERIODATE SYSTEM: 34.12 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

MN(III)--PERIODATE SYSTEM: 34.12 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.43717	0.71400	-0.76689	-0.76800	0.81457
2	0.45800	0.69200	-0.91215	-1.05600	0.81670
3	0.47883	0.67500	-1.00113	-0.81600	0.81816
4	0.49967	0.65200	-1.08644	-1.10400	0.81987
5	0.52050	0.63300	-1.08827	-0.91200	0.82105
6	0.54133	0.60500	-1.11681	-1.34400	0.82240
7	0.56217	0.58400	-1.15438	-1.00800	0.82308
8	0.58300	0.55800	-1.16238	-1.24800	0.82351
9	0.60383	0.53800	-1.16470	-0.96000	0.82352
10	0.62467	0.51000	-1.17639	-1.34400	0.82300
11	0.64550	0.48600	-1.18524	-1.15200	0.82204
12	0.66633	0.46200	-1.15844	-1.15200	0.82053
13	0.68717	0.43900	-1.11273	-1.10400	0.81852
14	0.70800	0.41300	-1.03019	-1.24800	0.81549
15	0.72883	0.39600	-0.97768	-0.81600	0.81302
16	0.74967	0.37400	-0.93640	-1.05600	0.80916
17	0.77050	0.35700	-0.90610	-0.81600	0.80559
18	0.79133	0.33800	-0.88824	-0.91200	0.80092
19	0.81217	0.31900	-0.85281	-0.91200	0.79541
20	0.83300	0.30000	-0.80403	-0.91200	0.78891
21	0.85383	0.28500	-0.76113	-0.72000	0.78296
22	0.87467	0.27000	-0.71435	-0.72000	0.77617
23	0.89550	0.25600	-0.67118	-0.57600	0.77003
24	0.91633	0.24000	-0.64486	-0.86400	0.75943
25	0.93717	0.22900	-0.63153	-0.52800	0.75200
26	0.95800	0.21500	-0.60069	-0.67200	0.74128

VALUES OF OTHER INPUT PARAMETERS:

NUM= 36 KOKOP= 0 TDELTA= 2.08330-02 TSTART= 3.33000-01
LATIN= 2.24000-08 ASTART= 0.757 T1= 0.2460 T2= 0.6455

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.4010 00	-4.3170-09	-4.9040-09	5.8700-10	-11.97001	0.8146
1.4450 00	-4.4640-09	-5.3380-09	8.7420-10	-16.37676	0.8167
1.4810 00	-4.9060-09	-5.6930-09	7.8700-10	-13.82412	0.8182
1.5340 00	-5.3660-09	-6.2020-09	8.3630-10	-13.48447	0.8199
1.5800 00	-6.2730-09	-6.6510-09	3.7790-10	-5.88252	0.8211
1.6530 00	-7.0750-09	-7.3630-09	2.8770-10	-3.90708	0.8224
1.7120 00	-7.8450-09	-7.9420-09	9.7320-11	-1.22536	0.8231
1.7920 00	-8.8520-09	-8.7200-09	-1.3180-10	1.51117	0.8235
1.8590 00	-9.9600-09	-9.3690-09	-5.9090-10	6.30702	0.8235
1.9610 00	-1.1040-08	-1.0360-08	-6.7910-10	6.55308	0.8230
2.0580 00	-1.2200-08	-1.1310-08	-8.9230-10	7.89146	0.8220
2.1650 00	-1.2880-08	-1.2350-08	-5.3570-10	4.33825	0.8205
2.2780 00	-1.3830-08	-1.3450-08	-3.7940-10	2.81982	0.8185
2.4210 00	-1.5390-08	-1.4850-08	-5.4320-10	3.65762	0.8155
2.5290 00	-1.6700-08	-1.5800-08	-8.3490-10	5.26004	0.8130
2.6740 00	-1.7430-08	-1.7310-08	-6.1990-10	3.58109	0.8092
2.8010 00	-1.9050-08	-1.8550-08	-4.9540-10	2.67029	0.8056
2.9590 00	-1.9960-08	-2.0090-08	1.3070-10	-0.65081	0.8009
3.1350 00	-2.1330-08	-2.1800-08	4.7160-10	-2.16294	0.7954
3.3330 00	-2.3210-08	-2.3740-08	5.3160-10	-2.23933	0.7889
3.5090 00	-2.5130-08	-2.5450-08	3.2000-10	-1.25763	0.7830
3.7040 00	-2.7430-08	-2.7350-08	-7.9160-11	0.28946	0.7762
3.8760 00	-2.9890-08	-2.9030-08	-8.5990-10	2.96234	0.7700
4.1670 00	-3.1830-08	-3.1860-08	2.9350-11	-0.09213	0.7594
4.3670 00	-3.3240-08	-3.3810-08	5.6880-10	-1.68222	0.7521
4.6510 00	-3.5720-08	-3.6580-08	8.5650-10	-2.34137	0.7413

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.9330-19

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPM)
C(1)	8.74390-09	3.36680-10	3.8504
C(2)	-9.74480-09	1.23540-10	-1.2678

MN(III)--PERIODATE SYSTEM: 34.13 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

AC.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.18747	0.74700	-0.32179	-0.14400	0.81088
2	0.20830	0.74000	-0.40345	-0.33600	0.81171
3	0.22913	0.72700	-0.60542	-0.62400	0.81319
4	0.24997	0.71100	-0.71838	-0.76800	0.81487
5	0.27080	0.69600	-0.79328	-0.72000	0.81633
6	0.29163	0.68000	-0.83750	-0.76800	0.81774
7	0.31247	0.66200	-0.85045	-0.86400	0.81916
8	0.33330	0.64500	-0.86919	-0.81600	0.82033
9	0.35413	0.62500	-0.89054	-0.96000	0.82149
10	0.37497	0.60600	-0.88723	-0.91200	0.82236
11	0.39580	0.59000	-0.88450	-0.76800	0.82291
12	0.41663	0.57000	-0.89842	-0.96000	0.82337
13	0.43747	0.55100	-0.92347	-0.91200	0.82355
14	0.45830	0.53300	-0.94239	-0.86400	0.82347
15	0.47913	0.51200	-0.96742	-1.00800	0.82306
16	0.49997	0.49100	-0.97063	-1.00800	0.82228
17	0.52080	0.47100	-0.96893	-0.96000	0.82116
18	0.54163	0.45300	-0.96424	-0.86400	0.81981
19	0.56247	0.43000	-0.96252	-1.10400	0.81757
20	0.58330	0.41200	-0.94203	-0.86400	0.81535
21	0.60413	0.39300	-0.91827	-0.91200	0.81254
22	0.62497	0.37200	-0.88541	-1.00800	0.80876
23	0.64580	0.35400	-0.83144	-0.86400	0.80490
24	0.66663	0.34000	-0.82162	-0.67200	0.80145
25	0.68747	0.32100	-0.79236	-0.91200	0.79603
26	0.70830	0.30500	-0.78578	-0.76800	0.79075
27	0.72913	0.29000	-0.77898	-0.72000	0.78503
28	0.74997	0.27100	-0.74992	-0.91200	0.77665
29	0.77080	0.25800	-0.70674	-0.62400	0.77003
30	0.79163	0.24200	-0.68973	-0.76800	0.76070
31	0.81247	0.23000	-0.66495	-0.57600	0.75271
32	0.83330	0.21600	-0.63300	-0.67200	0.74209
33	0.85413	0.20200	-0.61348	-0.57200	0.72983
34	0.87497	0.18900	-0.57542	-0.62400	0.71664

VALUES OF OTHER INPUT PARAMETERS:

NUM= 44 KORUP= 0 TUFLT= 2.08330-D2 TSTART= 8.33000-D2
 CATIN= 2.24000-D4 ASTAKT= 0.760 T1= 0.0280 T2= 0.5000

MN(III)--PERIODATE SYSTEM: 34.13 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEV(Y)	Δ DEV(Y)	WEIGHT(Y)
1.3390 00	-3.9730-D9	-4.6200-D9	6.6680-10	-13.99999	0.8109
1.3510 00	-3.5270-D9	-4.7180-D9	1.1910-09	-25.25238	0.8117
1.3760 00	-3.3600-D9	-4.9050-D9	1.5460-09	-31.50987	0.8132
1.4000 00	-3.4480-D9	-5.1450-D9	1.6970-D9	-32.97842	0.8149
1.4370 00	-3.7360-D9	-5.3800-D9	1.6430-09	-30.94769	0.8163
1.4710 00	-4.1720-D9	-5.6410-D9	1.4690-09	-26.04097	0.8177
1.5110 00	-4.7840-D9	-5.9510-D9	1.1670-09	-19.61399	0.8192
1.5500 00	-5.3910-D9	-6.2590-D9	8.6800-10	-13.86669	0.8203
1.6000 00	-6.0050-D9	-6.6440-D9	6.3880-10	-9.61515	0.8215
1.6500 00	-6.8220-D9	-7.0320-D9	2.1030-10	-2.99008	0.8224
1.6950 00	-7.6890-D9	-7.3790-D9	-3.1070-10	4.21025	0.8229
1.7540 00	-8.4520-D9	-7.8390-D9	-6.1280-10	7.81745	0.8234
1.8150 00	-9.1280-D9	-8.3060-D9	-8.2020-10	9.87308	0.8235
1.8780 00	-9.8780-D9	-8.7830-D9	-1.0960-09	12.47581	0.8235
1.9530 00	-1.0530-D8	-9.3780-D9	-1.1980-09	12.77842	0.8231
2.0370 00	-1.1540-D8	-1.0030-D8	-1.5130-D9	15.08825	0.8223
2.1230 00	-1.2040-D8	-1.0700-D8	-1.3450-D9	12.57316	0.8212
2.2080 00	-1.2580-D8	-1.1350-D8	-1.2340-D9	10.87271	0.8198
2.3260 00	-1.3090-D8	-1.2260-D8	-8.2680-D9	6.74248	0.8176
2.4270 00	-1.3870-D8	-1.3050-D8	-8.2000-10	6.28342	0.8154
2.5450 00	-1.4740-D8	-1.3960-D8	-7.7840-D9	5.57630	0.8125
2.6880 00	-1.5810-D8	-1.5070-D8	-7.3990-10	4.90925	0.8088
2.8250 00	-1.7400-D8	-1.6130-D8	-1.2690-09	7.86643	0.8049
2.9610 00	-1.8170-D8	-1.7030-D8	-1.1640-09	6.71666	0.8014
3.1150 00	-1.9440-D8	-1.8360-D8	-1.0570-D9	5.75283	0.7960
3.2790 00	-2.0190-D8	-1.9640-D8	-5.4670-10	2.78319	0.7907
3.4480 00	-2.0970-D8	-2.0960-D8	-8.8580-12	0.04227	0.7850
3.6900 00	-2.2400-D8	-2.2830-D8	4.2890-10	-1.87867	0.7766
3.8760 00	-2.4430-D8	-2.4270-D8	-1.6010-10	0.65954	0.7700
4.1320 00	-2.5710-D8	-2.6250-D8	5.4530-10	-2.07681	0.7607
4.3480 00	-2.7370-D8	-2.7920-D8	5.5530-10	-1.98859	0.7527
4.6300 00	-2.9490-D8	-3.0110-D8	6.1890-10	-2.05583	0.7421
4.9500 00	-3.1090-D8	-3.2590-D8	1.5060-09	-4.62177	0.7298
5.2910 00	-3.4060-D8	-3.5230-D8	1.1690-09	-3.31695	0.7166

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 8.9490-19

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	5.74770-D9	4.49500-10	7.8206
C(2)	-7.74460-D9	1.63840-10	-2.1156

PA(III)--PERIODATE SYSTEM: 34.14 DETN OF CONSTANT FOR NTA EFFECT

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MNE(III)--PERIODATE SYSTEM: 34.14 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.56217	0.74200	-0.21585	-0.24000	0.81146
2	0.58300	0.73600	-0.30090	-0.28800	0.81218
3	0.60383	0.73100	-0.42270	-0.24000	0.81274
4	0.62467	0.71900	-0.54277	-0.57600	0.81405
5	0.64550	0.70900	-0.66540	-0.48000	0.81508
6	0.66633	0.69200	-0.77708	-0.81600	0.81670
7	0.68717	0.67300	-0.86070	-0.91200	0.81832
8	0.70800	0.65700	-0.92485	-0.76800	0.81952
9	0.72883	0.63700	-0.89454	-0.96000	0.82082
10	0.74967	0.61800	-0.88767	-0.91200	0.82183
11	0.77050	0.59800	-0.89970	-0.96000	0.82266
12	0.79133	0.57900	-0.93940	-0.91200	0.82320
13	0.81217	0.56800	-0.99269	-0.52800	0.82340
14	0.83300	0.53600	-1.05218	-1.53600	0.82350
15	0.85383	0.51800	-1.09399	-0.86400	0.82321
16	0.87467	0.49300	-1.11715	-1.20000	0.82237
17	0.89550	0.47000	-1.08114	-1.10400	0.82109
18	0.91633	0.45000	-1.00709	-0.96000	0.81955
19	0.93717	0.42800	-1.00846	-1.05600	0.81734
20	0.95800	0.40700	-0.96308	-1.00800	0.81466
21	0.97883	0.38900	-0.94496	-0.86400	0.81187
22	0.99967	0.36800	-0.93630	-1.00800	0.80796
23	1.02050	0.34900	-0.90245	-0.91200	0.80372
24	1.04133	0.33100	-0.85836	-0.86400	0.79899
25	1.06217	0.31300	-0.82289	-0.86400	0.79347
26	1.08300	0.29500	-0.76882	-0.86400	0.78701
27	1.10383	0.28200	-0.74310	-0.82400	0.78167
28	1.12467	0.26700	-0.71151	-0.72000	0.77469
29	1.14550	0.25000	-0.68102	-0.81600	0.76554
30	1.16633	0.23800	-0.66056	-0.57600	0.75814
31	1.18717	0.22300	-0.62318	-0.72000	0.74759
32	1.20800	0.21200	-0.56305	-0.52800	0.73877
33	1.22883	0.20000	-0.52634	-0.57600	0.72792
34	1.24967	0.18900	-0.48124	-0.52800	0.71666
35	1.27050	0.18100	-0.43773	-0.38400	0.70750
36	1.29133	0.17100	-0.40830	-0.48000	0.69478
37	1.31217	0.16200	-0.37930	-0.43200	0.68190
38	1.33300	0.15700	-0.36912	-0.24000	0.67407

VALUES OF OTHER INPUT PARAMETERS:

NUM= 48 KOROP= 0 TDELTA= 2.08330-02 TSTART= 4.58000-01
 CATIN= 2.24000-08 ASTART= 0.760 T1= 0.6170 T2= 0.8747

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.3480 00	-9.1320-09	-6.9660-09	-2.1660-09	31.09213	0.8115
1.3590 00	-8.5660-09	-7.1110-09	-1.4550-09	20.45328	0.8122
1.3680 00	-7.7240-09	-7.2340-09	-4.9000-10	6.77305	0.8127
1.3910 00	-7.4320-09	-7.5360-09	1.0430-10	-1.36365	0.8140
1.4100 00	-7.3400-09	-7.7960-09	4.5600-10	-5.84958	0.8151
1.4450 00	-7.4830-09	-8.2540-09	7.7090-10	-9.33921	0.8167
1.4860 00	-7.9320-09	-8.7940-09	8.6120-10	-9.79355	0.8183
1.5220 00	-8.5650-09	-9.2720-09	7.0760-10	-7.63098	0.8195
1.5700 00	-1.0170-08	-9.9040-09	-2.6390-10	2.66458	0.8208
1.6180 00	-1.1660-08	-1.0540-08	-1.1190-09	10.61620	0.8218
1.6720 00	-1.2990-08	-1.1260-08	-1.7340-09	15.39927	0.8227
1.7270 00	-1.3950-08	-1.1980-08	-1.9690-09	16.42910	0.8232
1.7610 00	-1.4710-08	-1.2430-08	-2.2860-09	18.41243	0.8234
1.8660 00	-1.5380-08	-1.3820-08	-1.5680-09	11.55138	0.8235
1.9310 00	-1.6320-08	-1.4670-08	-1.6420-09	11.19108	0.8232
2.0280 00	-1.7540-08	-1.5970-08	-1.5700-09	9.82901	0.8224
2.1280 00	-1.8550-08	-1.7480-08	-1.2730-09	7.36382	0.8211
2.2220 00	-2.0360-08	-1.8530-08	-1.8500-09	9.49801	0.8196
2.3360 00	-2.0820-08	-2.0040-08	-7.7400-10	3.86165	0.8173
2.4570 00	-2.2280-08	-2.1640-08	-6.4500-10	2.98122	0.8147
2.5710 00	-2.3200-08	-2.3140-08	-6.2480-11	0.26998	0.8119
2.7170 00	-2.3920-08	-2.5080-08	1.1650-09	-4.64326	0.8080
2.8650 00	-2.5330-08	-2.7040-08	1.7070-09	-6.31356	0.8037
3.0210 00	-2.7170-08	-2.9100-08	1.9230-09	-6.60833	0.7990
3.1950 00	-2.8910-08	-3.1400-08	2.4820-09	-7.90629	0.7935
3.3900 00	-3.1550-08	-3.3970-08	2.4200-09	-7.12304	0.7870
3.5460 00	-3.3270-08	-3.6040-08	2.7660-09	-7.67556	0.7817
3.7450 00	-3.5410-08	-3.8680-08	3.2680-09	-8.44940	0.7747
4.0000 00	-3.7680-08	-4.2040-08	4.3660-09	-10.38353	0.7655
4.2020 00	-3.9550-08	-4.4710-08	5.1600-09	-11.53986	0.7581
4.4840 00	-4.2670-08	-4.8450-08	5.7760-09	-11.92215	0.7476
4.7170 00	-4.8060-08	-5.1530-08	3.4670-09	-6.72927	0.7388
5.0000 00	-5.2300-08	-5.5270-08	2.5720-09	-5.37725	0.7279
5.2910 00	-5.8170-08	-5.9120-08	9.4980-10	-1.60656	0.7166
5.5250 00	-6.5020-08	-6.2210-08	-2.8060-09	4.51069	0.7075
5.8480 00	-7.0840-08	-6.6480-08	-4.3620-09	6.56091	0.6948
6.1730 00	-7.7490-08	-7.0780-08	-6.7120-09	9.48244	0.6819
6.3690 00	-8.0890-08	-7.3380-08	-7.5140-09	10.23926	0.6741

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 6.1960-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	1.08580-08	9.86450-10	9.0854
C(2)	-1.32250-08	3.07510-10	-2.3252

MN(11)--PERIODATE SYSTEM: 35.13 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NC.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.64617	0.59000	-0.50564	-0.24000	0.82291
2	0.66700	0.57600	-0.69909	-0.67200	0.82326
3	0.68783	0.55700	-0.83443	-0.91200	0.82352
4	0.70867	0.54000	-0.93276	-0.81600	0.82353
5	0.72950	0.51800	-0.95431	-1.05600	0.82321
6	0.75033	0.50000	-0.97471	-0.86400	0.82266
7	0.77117	0.48100	-0.96180	-0.91200	0.82177
8	0.79200	0.45800	-0.99735	-1.10400	0.82022
9	0.81283	0.44100	-1.02369	-0.81600	0.81872
10	0.83367	0.41400	-1.02415	-1.29600	0.81562
11	0.85450	0.40000	-0.97694	-0.67200	0.81364
12	0.87533	0.37200	-0.94746	-1.34400	0.80876
13	0.89617	0.35600	-0.91457	-0.76800	0.80536
14	0.91700	0.34100	-0.83424	-0.72000	0.80171
15	0.93783	0.32200	-0.81059	-0.91200	0.79634
16	0.95867	0.30200	-0.75081	-0.96000	0.78965
17	0.97950	0.29000	-0.74634	-0.57600	0.78503
18	1.00033	0.27700	-0.68065	-0.62400	0.77945
19	1.02117	0.25900	-0.62307	-0.86400	0.77056
20	1.04200	0.24800	-0.58957	-0.52800	0.76436
21	1.06283	0.23600	-0.57645	-0.57600	0.75682
22	1.08367	0.22600	-0.55052	-0.48000	0.74983
23	1.10450	0.21300	-0.52659	-0.62400	0.73962
24	1.12533	0.20300	-0.52432	-0.48000	0.73077
25	1.14617	0.19100	-0.48870	-0.57600	0.71880
26	1.16700	0.18100	-0.44901	-0.48000	0.70750
27	1.18783	0.17400	-0.39153	-0.33600	0.69876
28	1.20867	0.16500	-0.36173	-0.43200	0.68636
29	1.22950	0.15800	-0.34405	-0.33600	0.67567
30	1.25033	0.15100	-0.34711	-0.33600	0.66395
31	1.27117	0.14500	-0.35179	-0.28800	0.65295
32	1.29200	0.13600	-0.33678	-0.43200	0.63456
33	1.31283	0.12900	-0.31653	-0.33600	0.61841

VALUES OF OTHER INPUT PARAMETERS:

NUM= 43 KDRDP= 0 IUFLT= 2.08330-02 TSTART= 5.42000-01
 CATIN= 2.24000-08 ASTART= 0.010 T1= 0.4580 T2= 0.8337

MN(11)--PERIODATE SYSTEM: 35.13 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEVI(Y)	4 DEVI(Y)	WEIGHT(Y)
1.6950 00	-9.2660-09	-6.7900-09	-2.4760-09	36.46654	0.8229
1.7360 00	-8.2680-09	-7.3780-09	-8.9020-10	12.06602	0.8233
1.7950 00	-8.3770-09	-8.2230-09	-1.5370-10	1.86910	0.8235
1.8520 00	-8.9140-09	-9.0300-09	1.1600-10	-1.28477	0.8235
1.9310 00	-1.0220-08	-1.0150-08	-6.8400-11	0.67378	0.8232
2.0000 00	-1.1600-08	-1.1140-08	-4.5720-10	4.10213	0.8227
2.0790 00	-1.3490-08	-1.2270-08	-1.2210-09	9.94769	0.8218
2.1830 00	-1.4800-08	-1.3760-08	-1.0380-09	7.54522	0.8202
2.2680 00	-1.6270-08	-1.4980-08	-1.3110-09	8.76234	0.8187
2.4150 00	-1.8230-08	-1.7070-08	-1.1590-09	6.79006	0.8156
2.5000 00	-1.9590-08	-1.8280-08	-1.3110-09	7.17370	0.8136
2.6880 00	-2.0690-08	-2.0970-08	2.7220-10	-1.29838	0.8088
2.8090 00	-2.1950-08	-2.2690-08	7.4230-10	-3.27139	0.8054
2.9330 00	-2.4620-08	-2.4460-08	-1.6710-10	0.68312	0.8017
3.1060 00	-2.5920-08	-2.6920-08	1.0090-09	-3.74690	0.7963
3.3110 00	-2.8600-08	-2.9860-08	1.2590-09	-4.21708	0.7896
3.4480 00	-2.9400-08	-3.1820-08	2.4190-09	-7.60158	0.7850
3.6100 00	-3.2920-08	-3.4130-08	1.2060-09	-3.53323	0.7795
3.8610 00	-3.6710-08	-3.7710-08	9.9540-10	-2.43971	0.7706
4.0320 00	-3.9590-08	-4.0150-08	5.6210-10	-1.39999	0.7644
4.2370 00	-4.1300-08	-4.3080-08	1.7780-09	-4.12755	0.7568
4.4250 00	-4.4090-08	-4.5750-08	1.6610-09	-3.63080	0.7498
4.6950 00	-4.6980-08	-4.9610-08	2.6260-09	-5.29412	0.7396
4.9260 00	-4.8080-08	-5.2910-08	4.8340-09	-9.13535	0.7308
5.2360 00	-5.2540-08	-5.7330-08	4.7920-09	-8.35935	0.7188
5.5230 00	-5.8220-08	-6.1460-08	3.2370-09	-5.26795	0.7075
5.7470 00	-6.7960-08	-6.4630-08	-3.3290-09	5.15167	0.6988
6.0610 00	-7.4850-08	-6.9100-08	-5.7420-09	6.38890	0.6864
6.3290 00	-8.0050-08	-7.2940-08	-7.1130-09	9.75297	0.6757
6.6230 00	-8.0690-08	-7.7120-08	-3.5650-09	4.62203	0.6639
6.8970 00	-8.0940-08	-8.1040-08	9.3790-11	-0.11574	0.6530
7.3530 00	-8.5930-08	-8.7550-08	1.6170-09	-1.84672	0.6346
7.7520 00	-9.2910-08	-9.3240-08	3.3960-10	-0.36418	0.6184

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 4.7270-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	1.74630-08	1.02250-09	5.8754
C(2)	-1.42740-08	2.48030-10	-1.7377

MN(11)--PERIODATE SYSTEM: 35.14 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

ETERPINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.60417	0.58300	-0.55578	-0.48000	0.82310
2	0.62500	0.56800	-0.73645	-0.72000	0.82340
3	0.64583	0.55000	-0.87354	-0.86400	0.82355
4	0.66667	0.53300	-0.93797	-0.81600	0.82347
5	0.68750	0.51000	-0.98179	-1.10400	0.82300
6	0.70833	0.49100	-0.99600	-0.91200	0.82228
7	0.72917	0.47100	-1.02882	-0.96000	0.82116
8	0.75000	0.45000	-1.05243	-1.00800	0.81955
9	0.77083	0.42500	-1.06214	-1.20000	0.81899
10	0.79167	0.40600	-1.04727	-0.91200	0.81452
11	0.81250	0.38100	-1.02340	-1.20000	0.81047
12	0.83333	0.36200	-0.98224	-0.91200	0.80670
13	0.85417	0.34200	-0.93396	-0.96000	0.80197
14	0.87500	0.32500	-0.91182	-0.81600	0.79725
15	0.89583	0.30200	-0.87390	-1.10400	0.78965
16	0.91667	0.28700	-0.85219	-0.72000	0.78380
17	0.93750	0.27000	-0.79327	-0.81600	0.77617
18	0.95833	0.25200	-0.73526	-0.86400	0.76669
19	0.97917	0.23800	-0.67197	-0.67200	0.75814
20	1.00000	0.22500	-0.64423	-0.62400	0.74909
21	1.02083	0.21300	-0.58476	-0.57600	0.73962
22	1.04167	0.20000	-0.54610	-0.62400	0.72792
23	1.06250	0.18900	-0.51287	-0.52800	0.71664
24	1.08333	0.17800	-0.48763	-0.52800	0.70384
25	1.10417	0.17000	-0.44792	-0.38400	0.69342
26	1.12500	0.16000	-0.41369	-0.48000	0.67883
27	1.14583	0.15200	-0.39546	-0.38400	0.66569
28	1.16667	0.14200	-0.39664	-0.48000	0.64709
29	1.18750	0.13700	-0.37865	-0.24000	0.63672
30	1.20833	0.12800	-0.36405	-0.43200	0.61595

VALUES OF OTHER INPUT PARAMETERS:

NUM= 40 KDRUP= 0 TDEL= 2.08330-02 TSTART= 5.00000-01
 CATIN= 2.24000-08 ASTART= 0.610 T1= 0.4580 T2= 0.7708

MN(11)--PERIODATE SYSTEM: 35.14 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.7150 00	-6.7820-09	-6.6380-09	-1.4440-10	2.17511	0.8231
1.7610 00	-6.6810-09	-7.1570-09	4.6540-10	-6.93145	0.8234
1.8180 00	-7.1280-09	-7.7940-09	6.6820-10	-8.57289	0.8235
1.8760 00	-8.1900-09	-8.4460-09	2.5560-10	-3.02376	0.8235
1.9610 00	-9.4650-09	-9.3960-09	-6.8900-11	0.73323	0.8230
2.0370 00	-1.1100-08	-1.0250-08	-8.5220-10	8.31544	0.8223
2.1230 00	-1.2610-08	-1.1220-08	-1.3900-09	12.38529	0.8212
2.2200 00	-1.4290-08	-1.2330-08	-1.9610-09	15.89638	0.8196
2.3530 00	-1.6260-08	-1.3800-08	-2.4540-09	17.78350	0.8170
2.4630 00	-1.6930-08	-1.5040-08	-1.8940-09	12.59184	0.8145
2.6250 00	-1.7780-08	-1.6850-08	-9.2910-10	5.51215	0.8105
2.7620 00	-1.9000-08	-1.8900-08	-6.0160-10	3.26933	0.8067
2.9240 00	-2.0490-08	-2.0220-08	-2.6880-10	1.32944	0.8020
3.0770 00	-2.1500-08	-2.1940-08	4.4040-10	-2.00776	0.7972
3.3110 00	-2.2960-08	-2.4570-08	1.6060-09	-6.53834	0.7896
3.4840 00	-2.4090-08	-2.6510-08	2.4180-09	-9.11991	0.7838
3.7040 00	-2.6470-08	-2.8980-08	2.5050-09	-8.64386	0.7762
3.9680 00	-2.9200-08	-3.1950-08	2.7530-09	-8.61805	0.7667
4.2020 00	-3.2640-08	-3.4570-08	1.9320-09	-5.88813	0.7581
4.4440 00	-3.4770-08	-3.7300-08	2.5300-09	-6.78172	0.7491
4.6950 00	-3.9100-08	-4.0110-08	1.0080-09	-2.51287	0.7396
5.0000 00	-4.2730-08	-4.3540-08	8.1370-10	-1.86886	0.7279
5.2910 00	-4.6610-08	-4.6810-08	4.0470-10	-0.86453	0.7166
5.6180 00	-4.9760-08	-5.0480-08	7.1910-10	-1.42444	0.7038
5.8820 00	-5.5220-08	-5.3450-08	-1.7650-09	3.30108	0.6934
6.2500 00	-6.0920-08	-5.7580-08	-3.3310-09	5.78452	0.6788
6.5790 00	-6.4900-08	-6.1280-08	-3.6230-09	5.91264	0.6657
7.0420 00	-6.5890-08	-6.6490-08	5.9910-10	-0.90107	0.6471
7.2990 00	-7.0250-08	-6.9370-08	-8.7710-10	1.26436	0.6367
7.8130 00	-7.4350-08	-7.5140-08	7.8940-10	-1.05055	0.6160

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.1850-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	1.26330-08	7.18340-10	5.6864
C(2)	-1.12350-08	1.74130-10	-1.5499

MN(11)--PERIODATE SYSTEM: 35.15 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.60417	0.58500	-0.61001	-0.48000	0.82305
2	0.62500	0.56900	-0.84418	-0.76800	0.82339
3	0.64583	0.54800	-1.04086	-1.00800	0.82355
4	0.66667	0.52500	-1.16972	-1.10400	0.82336
5	0.68750	0.50100	-1.24427	-1.15200	0.82270
6	0.70833	0.47100	-1.27656	-1.14400	0.82116
7	0.72917	0.44800	-1.25727	-1.10400	0.81938
8	0.75000	0.42200	-1.19606	-1.24800	0.81664
9	0.77083	0.39500	-1.16394	-1.29600	0.81286
10	0.79167	0.37200	-1.13924	-1.10400	0.80876
11	0.81250	0.35200	-1.11571	-0.96000	0.80444
12	0.83333	0.32900	-1.08117	-1.10400	0.79842
13	0.85417	0.30100	-1.03481	-1.34400	0.78928
14	0.87500	0.28300	-0.99352	-0.86400	0.78211
15	0.89583	0.26500	-0.92572	-0.86400	0.77369
16	0.91667	0.24400	-0.82416	-1.00800	0.76194
17	0.93750	0.23000	-0.74730	-0.67200	0.75271
18	0.95833	0.21200	-0.70885	-0.86400	0.73877
19	0.97917	0.19900	-0.66137	-0.62400	0.72695
20	1.00000	0.18800	-0.62310	-0.52800	0.71554
21	1.02083	0.17400	-0.59704	-0.67200	0.69876
22	1.04167	0.16100	-0.53368	-0.62400	0.68037
23	1.06250	0.14900	-0.49444	-0.57600	0.66038
24	1.08333	0.14100	-0.44124	-0.38400	0.64508
25	1.10417	0.13300	-0.39419	-0.38400	0.62785

VALUES OF OTHER INPUT PARAMETERS:

NUM= 35 KDNOP= 0 TDELTA= 2.08330-02 TSTART= 5.00000-01
 CATIN= 2.24000-08 ASTART= 0.610 T1= 0.4760 T2= 0.7083

MN(11)--PERIODATE SYSTEM: 35.15 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(W)
1.7090 00	-7.9150-09	-6.9330-09	-9.8250-10	14.17113	0.8231
1.7570 00	-7.7300-09	-7.3360-09	-3.9460-10	5.37947	0.8234
1.8250 00	-8.1450-09	-7.9000-09	-2.4530-10	3.10493	0.8236
1.9050 00	-9.1350-09	-8.5700-09	-5.6530-10	6.59625	0.8234
1.9960 00	-1.0570-08	-9.3350-09	-1.2330-09	13.20344	0.8227
2.1230 00	-1.2430-08	-1.0400-08	-2.0290-09	19.50784	0.8212
2.2320 00	-1.2990-08	-1.1310-08	-1.6770-09	14.82495	0.8194
2.3700 00	-1.4050-08	-1.2470-08	-1.5800-09	12.67207	0.8166
2.5320 00	-1.4830-08	-1.3820-08	-1.0110-09	7.31230	0.8129
2.6880 00	-1.5570-08	-1.5140-08	-4.3030-10	2.84297	0.8088
2.8410 00	-1.6310-08	-1.6420-08	1.0330-10	-0.62906	0.8044
3.0400 00	-1.7270-08	-1.8080-08	8.1490-10	-4.50691	0.7984
3.3220 00	-1.8490-08	-2.0450-08	1.9600-09	-9.58449	0.7893
3.5340 00	-1.9730-08	-2.2220-08	2.4930-09	-11.21862	0.7821
3.7740 00	-2.1680-08	-2.4230-08	2.5550-09	-10.54494	0.7737
4.0980 00	-2.4910-08	-2.6950-08	2.0400-09	-7.56746	0.7619
4.3480 00	-2.8100-08	-2.9040-08	9.4360-10	-3.24874	0.7527
4.7170 00	-3.0240-08	-3.2140-08	1.8550-09	-5.77078	0.7388
5.0250 00	-3.3160-08	-3.4720-08	1.5580-09	-4.44879	0.7270
5.3190 00	-3.5950-08	-3.7180-08	1.2360-09	-3.32266	0.7155
5.7470 00	-3.8300-08	-4.0770-08	2.4710-09	-6.06164	0.6988
6.2110 00	-4.3720-08	-4.4660-08	9.3920-10	-2.10293	0.6804
6.7110 00	-4.8130-08	-4.8850-08	7.1820-10	-1.47010	0.6604
7.0920 00	-5.5000-08	-5.2040-08	-2.9520-09	5.67221	0.6451
7.5190 00	-6.2750-08	-5.5620-08	-7.1340-09	12.82603	0.6279

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 3.3340-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	KEL STD DEVI(PPH)
C(1)	7.39300-09	9.75920-10	13.2005
C(2)	-8.38070-09	2.42630-10	-2.8952

PH(II)--PERIODATE SYSTEM: 35.16 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.43717	0.59200	-0.42946	-0.33600	0.82285
2	0.45800	0.57900	-0.56348	-0.62400	0.82320
3	0.47483	0.56600	-0.70198	-0.62400	0.82343
4	0.49367	0.54800	-0.81660	-0.86400	0.82355
5	0.52020	0.53500	-0.87611	-0.62400	0.82349
6	0.54133	0.51500	-0.92139	-0.96000	0.82314
7	0.56217	0.49300	-0.94146	-1.05600	0.82237
8	0.58300	0.47300	-0.93340	-0.96000	0.82129
9	0.60363	0.45600	-0.92354	-0.81600	0.82006
10	0.62467	0.43600	-0.90244	-0.96000	0.81821
11	0.64550	0.41900	-0.91119	-0.81600	0.81627
12	0.66633	0.39900	-0.92523	-0.96000	0.81348
13	0.68717	0.37900	-0.92154	-0.96000	0.81010
14	0.70800	0.35900	-0.89102	-0.96000	0.80604
15	0.72883	0.34200	-0.86008	-0.81600	0.80197
16	0.74967	0.32500	-0.81616	-0.81600	0.79725
17	0.77050	0.30800	-0.79264	-0.81600	0.79178
18	0.79133	0.29200	-0.75213	-0.76800	0.78583
19	0.81217	0.27600	-0.73077	-0.76800	0.77899
20	0.83300	0.26100	-0.69164	-0.72000	0.77162
21	0.85383	0.24700	-0.65391	-0.67200	0.76377
22	0.87467	0.23600	-0.61922	-0.52800	0.75682
23	0.89550	0.22000	-0.59591	-0.76800	0.74528
24	0.91633	0.21000	-0.57318	-0.48000	0.73706
25	0.93717	0.19800	-0.53794	-0.57600	0.72597
26	0.95800	0.18700	-0.50022	-0.52800	0.71443
27	0.97883	0.17600	-0.45473	-0.52800	0.70133
28	0.99967	0.16800	-0.42642	-0.38400	0.69065
29	1.02050	0.16000	-0.38521	-0.38400	0.67883
30	1.04133	0.15100	-0.37144	-0.43200	0.66395
31	1.06217	0.14400	-0.36900	-0.33600	0.65103
32	1.08300	0.13700	-0.36291	-0.33600	0.63672
33	1.10383	0.12900	-0.34684	-0.38400	0.61841

VALUES OF OTHER INPUT PARAMETERS:

NUM= 43 KDRUP= 0 TDELTA= 2.0833D-02 TSTART= 3.3300D-01
 CATIN= 2.2400D-08 ASTART= 0.610 T1= 0.3040 T2= 0.5622

PH(II)--PERIODATE SYSTEM: 35.16 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.6890 00	-7.802D-09	-7.246D-09	-5.558D-10	7.07132	0.8229
1.7270 00	-7.952D-09	-7.640D-09	-3.121D-10	4.08527	0.8232
1.7670 00	-8.227D-09	-8.052D-09	-1.748D-10	2.17124	0.8234
1.8250 00	-8.654D-09	-8.655D-09	-2.029D-10	2.34446	0.8236
1.8690 00	-1.011D-08	-9.116D-09	-9.922D-10	10.88404	0.8235
1.9420 00	-1.155D-08	-9.870D-09	-1.680D-09	17.02036	0.8231
2.0280 00	-1.338D-08	-1.077D-08	-2.605D-09	24.18644	0.8224
2.1140 00	-1.399D-08	-1.166D-08	-2.329D-09	19.97290	0.8213
2.1930 00	-1.465D-08	-1.248D-08	-2.165D-09	17.34498	0.8201
2.2940 00	-1.551D-08	-1.353D-08	-1.979D-09	14.63238	0.8182
2.3870 00	-1.587D-08	-1.449D-08	-1.375D-09	9.48995	0.8163
2.5000 00	-1.613D-08	-1.574D-08	-3.958D-10	2.51538	0.8135
2.6390 00	-1.670D-08	-1.711D-08	4.074D-10	-2.38126	0.8101
2.7860 00	-1.780D-08	-1.864D-08	6.391D-10	-4.50187	0.8060
2.9240 00	-1.898D-08	-2.008D-08	1.095D-09	-5.45320	0.8020
3.0770 00	-2.058D-08	-2.167D-08	1.091D-09	-5.03533	0.7972
3.2470 00	-2.177D-08	-2.343D-08	1.656D-09	-7.06890	0.7918
3.4250 00	-2.357D-08	-2.528D-08	1.712D-09	-6.77186	0.7858
3.6230 00	-2.489D-08	-2.734D-08	2.447D-09	-8.95078	0.7790
3.8310 00	-2.698D-08	-2.951D-08	2.528D-09	-8.56709	0.7716
4.0490 00	-2.925D-08	-3.176D-08	2.514D-09	-7.91607	0.7638
4.2370 00	-3.164D-08	-3.372D-08	2.083D-09	-6.17613	0.7568
4.5450 00	-3.366D-08	-3.693D-08	3.264D-09	-8.83995	0.7453
4.7620 00	-3.581D-08	-3.917D-08	3.364D-09	-8.58766	0.7371
5.0510 00	-3.902D-08	-4.217D-08	3.150D-09	-7.46902	0.7260
5.3480 00	-4.290D-08	-4.526D-08	2.361D-09	-5.21655	0.7144
5.6820 00	-4.822D-08	-4.873D-08	5.169D-10	-1.06074	0.7013
5.9520 00	-5.251D-08	-5.153D-08	-9.668D-10	1.87561	0.6906
6.2500 00	-5.934D-08	-5.464D-08	-4.704D-09	8.60879	0.6788
6.6230 00	-6.280D-08	-5.851D-08	-4.289D-09	7.33103	0.6639
6.9440 00	-6.448D-08	-6.185D-08	-2.625D-09	4.24308	0.6510
7.2990 00	-6.685D-08	-6.554D-08	-1.305D-09	1.99132	0.6367
7.7520 00	-7.129D-08	-7.024D-08	-1.043D-09	1.48488	0.6184

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 3.511D-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1:

CONSTANT	VALUE	STO DEV	REL STD DEV(PPH)
C(1)	1.0307D-08	8.5766D-10	8.3215
C(2)	-1.0391D-08	2.1324D-10	-2.0521

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.60417	0.58200	-0.76233	-0.62400	0.82313
2	0.62500	0.56200	-0.99640	-0.96000	0.82348
3	0.64583	0.53800	-1.17809	-1.15200	0.82352
4	0.66667	0.51300	-1.27927	-1.20000	0.82309
5	0.68750	0.48400	-1.33958	-1.39200	0.82193
6	0.70833	0.45800	-1.34196	-1.24800	0.82022
7	0.72917	0.43000	-1.32615	-1.34400	0.81757
8	0.75000	0.40200	-1.32929	-1.34400	0.81394
9	0.77083	0.37300	-1.29514	-1.39200	0.80896
10	0.79167	0.35000	-1.28062	-1.10400	0.80396
11	0.81250	0.32200	-1.24769	-1.34400	0.79634
12	0.83333	0.29400	-1.20309	-1.34400	0.78662
13	0.85417	0.27400	-1.13029	-0.96000	0.77807
14	0.87500	0.24700	-1.05142	-1.29600	0.76377
15	0.89583	0.22700	-0.96569	-0.96000	0.75056
16	0.91667	0.20900	-0.91144	-0.86400	0.73619
17	0.93750	0.19200	-0.85357	-0.81600	0.71986
18	0.95833	0.17300	-0.77238	-0.91200	0.69745
19	0.97917	0.15600	-0.71875	-0.81600	0.67244
20	1.00000	0.14300	-0.62840	-0.62400	0.64907
21	1.02083	0.13200	-0.52634	-0.52800	0.62555
22	1.04167	0.12100	-0.45419	-0.52800	0.59759
23	1.06250	0.11200	-0.41551	-0.43200	0.57050
24	1.08333	0.10500	-0.37965	-0.33600	0.54615
25	1.10417	0.09700	-0.34586	-0.38400	0.51392
26	1.12500	0.08800	-0.32355	-0.43200	0.47054

VALUES OF OTHER INPUT PARAMETERS:

NLM= 3c KDR0P= 0 TUFLT= 2.08330-02 TSTART= 5.0000-01
 CATIN= 2.24000-08 ASTART= 0.610 T1= 0.5140 T2= 0.7083

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.7180 00	-4.4810-05	-4.6480-09	1.6720-10	-3.59651	0.8231
1.7790 00	-5.1950-09	-5.0760-09	-1.1940-10	2.35312	0.8235
1.8590 00	-6.1980-09	-5.6310-09	-5.6680-10	10.04563	0.8235
1.9490 00	-7.6540-05	-6.2630-09	-1.3890-09	22.17199	0.8231
2.0660 00	-9.4410-09	-7.0830-09	-2.3580-09	33.29510	0.8219
2.1830 00	-1.1820-08	-7.9040-09	-3.9200-09	49.59334	0.8202
2.3260 00	-1.2320-08	-8.8990-09	-3.4180-09	38.40386	0.8176
2.4880 00	-1.2640-08	-1.0030-08	-2.6060-09	25.97258	0.8139
2.6810 00	-1.3330-08	-1.1390-08	-1.9460-09	17.08700	0.8090
2.8570 00	-1.3850-08	-1.2620-08	-1.2280-09	9.73193	0.8040
3.1060 00	-1.4590-08	-1.4360-08	-2.2860-10	1.59210	0.7963
3.4010 00	-1.5520-08	-1.8430-08	9.1280-10	-5.55644	0.7866
3.6500 00	-1.6930-08	-1.8170-08	1.2380-09	-6.81662	0.7781
4.0490 00	-1.8640-08	-2.0960-08	2.3170-09	-11.05570	0.7638
4.4050 00	-2.0780-08	-2.3460-08	2.6760-09	-11.40691	0.7506
4.7850 00	-2.2540-08	-2.6110-08	3.5820-09	-13.71950	0.7362
5.2080 00	-2.4600-08	-2.9080-08	4.4730-09	-15.38463	0.7199
5.7800 00	-2.7790-08	-3.3080-08	5.2870-09	-15.98183	0.6974
6.4100 00	-3.0520-08	-3.7490-08	6.9720-09	-18.59900	0.6724
6.9930 00	-3.5650-08	-4.1570-08	5.9210-09	-14.24475	0.6491
7.5760 00	-4.3440-08	-4.5650-08	2.2010-09	-4.82261	0.6255
8.2640 00	-5.1370-08	-5.0470-08	-9.0700-10	1.79727	0.5976
8.9290 00	-5.7280-08	-5.5110-08	-2.1650-09	3.92815	0.5705
9.5240 00	-6.3920-08	-5.9280-08	-4.6380-09	7.82455	0.5462
1.0310 01	-7.1640-08	-6.4780-08	-6.8590-09	10.58784	0.5139
1.1360 01	-7.7890-08	-7.2160-08	-5.7270-09	7.93707	0.4705

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 8.5880-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPM)
C(1)	7.37830-09	1.30060-09	17.6276
C(2)	-6.99920-09	2.52400-10	-3.6061

MN(11)--PERIODATE SYSTEM: 35.18 DETN OF CONSTANT FOR NTA EFFECT

6/8/72

DETERMINATION OF DERIVATIVE USING 11-POINT CUBIC SMOOTH

NO.	TIME	ABSORBANCE	DERIVATIVE	SLOPE	WEIGHT
1	0.52117	0.59200	-0.63415	-0.46000	0.82285
2	0.54200	0.57100	-0.84591	-1.00800	0.82335
3	0.56283	0.55200	-1.03574	-0.91200	0.82354
4	0.58367	0.53000	-1.15533	-1.05000	0.82343
5	0.60450	0.50700	-1.18782	-1.10400	0.82291
6	0.62533	0.48000	-1.21123	-1.29600	0.82171
7	0.64617	0.45300	-1.22672	-1.29600	0.81981
8	0.66700	0.43000	-1.21051	-1.10400	0.81757
9	0.68783	0.40600	-1.19098	-1.15200	0.81452
10	0.70867	0.37900	-1.16414	-1.29600	0.81010
11	0.72950	0.35700	-1.15554	-1.05600	0.80559
12	0.75033	0.33200	-1.12400	-1.20000	0.79928
13	0.77117	0.30900	-1.05900	-1.10400	0.79212
14	0.79200	0.28800	-0.99389	-1.00800	0.78421
15	0.81283	0.26700	-0.93968	-1.00800	0.77469
16	0.83367	0.25000	-0.86804	-0.81600	0.76554
17	0.85450	0.23200	-0.80083	-0.86400	0.75411
18	0.87533	0.21500	-0.74912	-0.81600	0.74128
19	0.89617	0.20000	-0.69293	-0.72000	0.72792
20	0.91700	0.18700	-0.64312	-0.62400	0.71443
21	0.93783	0.17500	-0.58637	-0.57600	0.70005
22	0.95867	0.16100	-0.51593	-0.67200	0.68037
23	0.97950	0.15200	-0.46836	-0.43200	0.66569
24	1.00033	0.14200	-0.44234	-0.48000	0.64709
25	1.02117	0.13400	-0.41680	-0.38400	0.63012

VALUES OF OTHER INPUT PARAMETERS:

NUM= 35 KDRUP= 0 TUEL= 2.08330-02 TSTART= 4.17000-01
 CATIN= 2.24000-08 ASTART= 0.615 T1= 0.3850 T2= 0.6462

MN(11)--PERIODATE SYSTEM: 35.18 DELTA CF CONSTANT FOR NTA EFFECT

6/8/72

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
1.6890 00	-6.2040-09	-5.4340-09	-7.7010-10	14.17012	0.8229
1.7510 00	-6.1830-09	-5.9250-09	-2.5840-10	4.36097	0.8234
1.8120 00	-6.4790-09	-6.4010-09	-7.8200-11	1.22163	0.8235
1.8870 00	-7.2490-09	-6.9950-09	-2.5430-10	3.63520	0.8234
1.9720 00	-8.0070-09	-7.6710-09	-9.3640-10	12.20645	0.8229
2.0630 00	-1.0120-08	-8.5470-09	-1.5720-09	14.39249	0.8217
2.2080 00	-1.1800-08	-9.5280-09	-2.2710-09	23.83426	0.8198
2.3260 00	-1.2340-08	-1.0460-08	-1.8820-09	17.98945	0.8176
2.4630 00	-1.2940-08	-1.1550-08	-1.3900-09	12.04120	0.8145
2.6390 00	-1.3640-08	-1.2930-08	-7.0350-10	5.44010	0.8101
2.8010 00	-1.4140-08	-1.4220-08	7.5280-11	-0.52953	0.8056
3.0120 00	-1.4950-08	-1.5880-08	9.2930-10	-5.85111	0.7993
3.2360 00	-1.6310-08	-1.7650-08	1.3420-09	-7.59980	0.7921
3.4720 00	-1.7850-08	-1.9520-08	1.6670-09	-8.54185	0.7842
3.7450 00	-1.9380-08	-2.1670-08	2.2980-09	-10.40199	0.7747
4.0000 00	-2.1510-08	-2.3690-08	2.1730-09	-9.17237	0.7655
4.3100 00	-2.3900-08	-2.6140-08	2.2360-09	-8.55322	0.7541
4.6510 00	-2.6170-08	-2.8830-08	2.6550-09	-9.20801	0.7413
5.0000 00	-2.8970-08	-3.1580-08	2.6140-09	-8.27617	0.7279
5.3480 00	-3.1940-08	-3.4330-08	2.3900-09	-6.96064	0.7144
5.7140 00	-3.5830-08	-3.7230-08	1.3990-09	-3.75794	0.7001
6.2110 00	-4.1620-08	-4.1150-08	-4.7270-10	1.14870	0.6804
6.5790 00	-4.8850-08	-4.4050-08	-2.7920-09	6.33766	0.6657
7.0420 00	-5.0660-08	-4.7710-08	-2.9630-09	6.16759	0.6471
7.4630 00	-5.4990-08	-5.1030-08	-3.9510-09	7.74264	0.6301

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.8110-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	7.90710-09	8.90590-10	11.2632
C(2)	-7.89820-09	2.23530-10	-2.8302

MN(11)--PERIODATE SYSTEM: NTA ADDED, DETN OF RATE CONSTANT FOR NTA EFFECT 6/13

X	Y(OBS)	Y(CALC)	DEV(Y)	% DEV(Y)	WEIGHT(Y)
4.4720-09	-9.2270-09	-7.9930-09	-1.2340-09	15.43959	3.8078
6.6190-09	-9.7450-09	-1.0270-08	5.2290-10	-5.09222	6.5535
4.3080-09	-7.7450-09	-7.8830-09	1.3800-10	-1.75126	4.9392
3.2520-09	-1.3240-08	-1.2000-08	-1.2280-09	10.23339	2.6317
1.0620-08	-1.4270-08	-1.4500-08	2.2870-10	-1.57069	3.3149
7.7000-09	-1.1230-08	-1.1420-08	1.8440-10	-1.61457	4.7217
4.5100-09	-8.3810-09	-8.0330-09	-3.4810-10	4.33364	3.3886
6.2870-09	-1.0390-08	-9.9160-09	-4.7530-10	4.79310	3.8557
4.5010-09	-6.9990-09	-8.0230-09	1.0240-09	-12.76169	3.2576
4.8630-09	-7.8980-09	-8.4070-09	5.0860-10	-6.04953	3.6772

GOODNESS OF FIT: GAUSS CRITERION, OMEGA= 2.204D-18

CONSTANTS FOUND FOR POLYNOMIAL CURVE FIT OF DEGREE 1 :

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
C(1)	-3.25420-09	8.04760-10	-24.7299
C(2)	-1.05960 00	1.24970-01	-11.7943

DETERMINATION OF SYSTEM PARAMETERS--SUMMARY OF RESULTS

MEAN VALUES OF RATE CONSTANTS:

CONSTANT	VALUE	STD DEV	REL STD DEV(PPH)
K1	4.19650 05	1.58140 05	37.68275
K2	3.07290 08	7.59940 07	24.72994
K-2	5.46620 09	6.44700 08	11.79426

VITA²

Benny Edward Simpson

Candidate for the Degree of

Master of Science

Thesis: SOME STUDIES OF SIMULATION AND ANALYSIS OF INDICATOR REACTIONS FOR CATALYTIC DETERMINATIONS

Major Field: Chemistry

Biographical:

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