

OPTIMAL CONTROL OF AN OIL REFINERY WASTE  
TREATMENT FACILITY: A TOTAL  
ECOSYSTEM APPROACH

By

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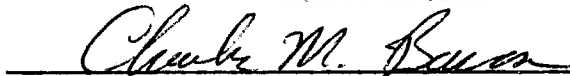
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## CHAPTER I

### INTRODUCTION

In recent years systems modeling and digital simulation have become important tools in the study of ecology. The modeling of biological populations began with the work of Lotka (20) and Volterra (34), and led to relatively recent simulations of ecosystems utilizing the digital computer (7,12,13,14,15,26,27,32,37). Referring to the synthesis of whole ecosystems, Smith (30) argues "systems oriented techniques with high speed computers offer the only means by which this can be accomplished". This is certainly not, however, the limit of digital simulation capabilities. Many authors have suggested using computer ecosystem models in studying proposed management or control policies (7,26,30). Although the efforts to date have been limited, the ultimate goal of this activity is the optimal design and control of ecological systems (27). Watt (37) treats resource management as an optimization problem: how to maximize a rate of harvest, or how to minimize the density of a pest. He used a mathematical model of the system to predict the effects of different management policies on yield (19). Davidson and Clymer (7) express the desirability of applying computer simulation to ecosystems, particularly in the area of environmental problems. An interesting application of this type would be the optimal control of a pollution abatement ecosystem. An example of this approach is the subject of this thesis.

The particular system of interest is a series of effluent holding

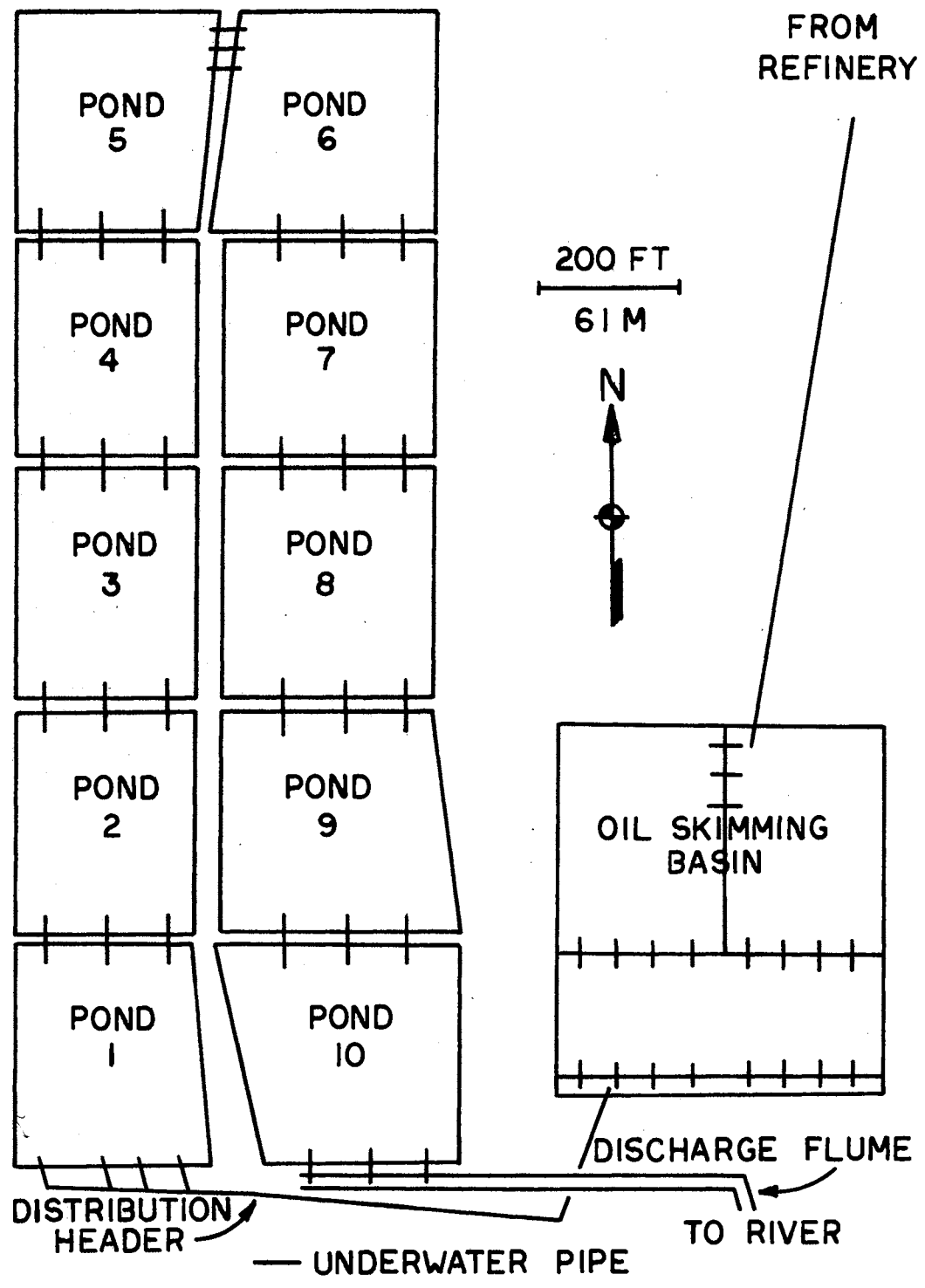


Figure 1. Holding Pond System

There has been no attempt to continuously monitor or regulate biological processes in the system. In this study a differential equation model was developed for this ecosystem and a control philosophy adopted. Control possibilities and indicators of effluent quality were reviewed, evolving into a control scheme and performance index. Digital simulation offered verification of the model and prediction of system performance was carried out by applying a search algorithm to find the minimal "cost" control policy.

Modeling of the system was carried out in three steps. First, a model for pond ten was formulated as a class project in a joint effort between the Departments of Electrical Engineering and Zoology, Oklahoma State University. Using the procedure verified by the class project, models were then developed for two upstream ponds in the system, ponds four and seven. The three models were then linked to form a series similar in function to the actual system, hopefully simulating the important biological succession effect.

Before going into some of the modeling preliminaries, a few definitions and some of the ecological terminology will be presented. The following basic concepts can be found, Odum (25).

#### Definitions

##### Ecosystem

Any unit that includes all of the organisms in a given area interacting with the physical environment so that a flow of energy leads to clearly defined trophic structure, biotic diversity, and material cycles within the system.



### Trophic Structure

The aggregation of organisms into two functional components - autotrophic and heterotrophic. The autotrophic component consists of primary producers with the heterotrophic components consisting of primary, secondary, and tertiary consumers and decomposers.

### Diversity Index

Mathematical expression describing community structure in terms of number of species and the apportionment of individuals among species. A low species diversity corresponds to a few species with many individuals, while a high diversity would be evidenced by many species with few individuals in each. Species diversity is correlated with ecosystem stability, but it is not certain to what extent this relationship is causal.

### Standing Crop

Magnitude of a particular entity in the ecosystem, indicating biotic (living) population or abiotic (non-living) intensity at a particular instant in time. Measured in units of biomass, for example, per unit area ( $\text{gm}/\text{m}^2$ ).

### Average Standing Crop

Average of the standing crop per unit time, i.e., week, month, year.

### P/R Ratio, Productivity/Respiration Ratio

The ratio of gross primary production of oxygen to community respiration including the oxygen demand of inorganic and organic compounds. This ratio should remain close to 1.0 in a steady-state ecological

system. When import of organic material occurs such as in the present study, the ratio is less than unity. However, the ratio returns to unity as oxygen demand is curbed.

#### Q-10 Factor

A factor indicating the influence of temperature on the growth of a population. Often accepted to be 2.0, so that an increase in temperature of ten degrees Centigrade would double the population's growth rate.

#### Turnover Rate

The fraction of the total amount of a substance in a compartment which leaves (or enters) in a given length of time at equilibrium. For example, assume a particular compartment has a standing crop of  $10 \text{ gm/m}^2$ . A flux of  $1 \text{ gm/day}$  out would correspond to a turnover rate of  $.1 \text{ gm/m}^2/\text{day}$ .

Of the concepts defined above, perhaps the most important is that of the ecosystem. The ecosystem is the basic functional unit in ecology, since it includes both organisms (biotic communities) and the abiotic environment, each influencing the properties of the other and both necessary for maintenance of life (25). The systems approach to ecology, fostering the ecosystem concept, results in a modeling viewpoint similar to the basic engineering systems approach. System boundaries, inputs, outputs, characteristic functions, states and system parameters are considered (30). For the submodels formulated later, the boundary of each pond ecosystem was considered as the waters edge. The primary ecosystem drivers were the inputs of light and temperature, while the ecosystem outputs consisted of the standing crop values.

As in most modeling efforts, assumptions must be made to reduce the complexity of the realization to a feasible modeling form. This should be accomplished while retaining, and hopefully exposing, the dominant characteristics controlling the system function. Patten (27) has guided much of the work in the ecosystems field and is used here as the primary source of methodology. Listed below are the assumptions made (7):

1. all variables uniformly distributed;
2. diurnal (daily) frequencies were not of interest;
3. growth and reproduction need not be distinguished; and
4. the species are divided into functional groups.

A "functional group" is a lumped set of species which have the same or similar function within the ecosystem. This approach is analogous to the "lumped parameter" assumption commonly used in engineering. An example of such lumping would be a decomposer group made up of various types of bacteria which have the same function in the ecosystem.

The concept of functional groups is further extended through the application of the compartment approach (27), wherein a compartment including several lumped species is represented by a single standing crop, expressed in units of biomass. In this way, one can systematically identify the states of the ecosystem to be modeled.

Interactions between these states are indicated as flows connecting the compartments of the model (see Figure 2). These flows arise as a result of trophic considerations, predator-prey feeding rates, mortality rates, etc. Depending on the type of model the flows can represent biomass, energy, uptake of nutrients, numbers, or any one of a number of flux types (18). In this work the flow values represent biomass fluxes based on a monthly time scale. This monthly temporal reference allows

the populations to behave like a continuous rather than discrete variable, an approach used by Ulanowicz (32).

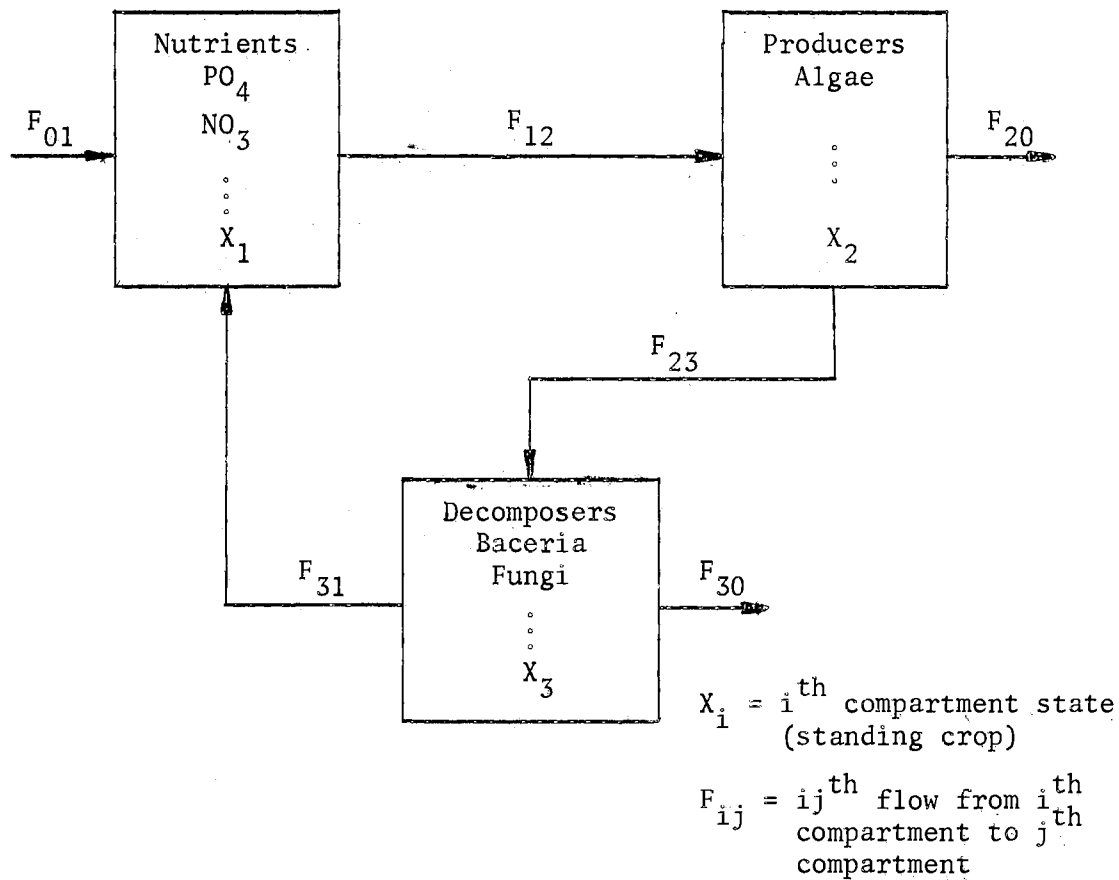


Figure 2. Simple Compartment Model

Thus far the boundaries, significant states and interactions of the ecosystem have been identified. This information is now used to formulate a differential state equation model of the form:

$$\dot{X}_i = \sum_{j=1}^n a_{ji} X_j - \sum_{j=0}^n a_{ij} X_i + b_{oi} \quad ,$$

$$i = 1, 2, \dots, n$$

$$j = 0, 1, \dots, n$$

$$a_{ji} = a_{ji}(X_i, t)$$

$$a_{ij} = a_{ij}(X_j, t)$$

This may be written compactly in the familiar matrix form:

$$\dot{\underline{X}} = \underline{A} \underline{X} + \underline{b} \quad (1)$$

describing the compartment dynamics. Presented here are some widely accepted guidelines for this formulation which follow directly from the previous modeling steps.

Consider again Figure 2 and the flows between compartments, in particular the flow from  $X_1$  to  $X_2$ .  $X_1$  in this case is the "donor" state and  $X_2$  the "recipient", for obvious reasons. To consider this flow dependent only upon the magnitude of the  $X_1$  state, or  $X_1$  standing crop, the state equation describing the simple ecosystem would be as follows:

$$\dot{X}_1 = -a_1 X_1 + F_{01}$$

$$\dot{X}_2 = a_1 X_1 - F_{23} - F_{20}$$

where

$$a_1 = \frac{F_{12}}{X_1^*}$$

Here  $X_1^*$  is defined as the average standing crop of  $X_1$ .

Through this process the resulting equation is said to be "donor controlled" for the flow from  $X_1$  to  $X_2$ . It is clear that an ecosystem model based on this type of rule will be a linear model, the  $\underline{A}$  matrix being a matrix of constants. Similarly, if the flows are defined as

being dependent upon the magnitudes of the recipient compartments ( $X_2$  in this case) the model will still be linear but the A matrix would differ. Moreover, it is clear that at the average standing crop values,  $\dot{\underline{X}} = 0$  and equilibrium is achieved.

Another variety of linear model which has been used to some extent is the combination donor-recipient controlled model, for which some types of flows are ruled donor controlled and others recipient. An example of this modeling procedure would be to let biotic flows be donor controlled and abiotic, recipient controlled.

In addition to linear models, there is another class of models whose flow descriptions are based on both standing crops, resulting in non-linear state equations. In this case, the state equations for the system shown in Figure 2 would appear as shown below:

$$\begin{aligned} \dot{X}_1 &= - a_1 X_1 X_2 + F_{01} \\ \dot{X}_2 &= a_1 X_1 X_2 - F_{23} - F_{20} \end{aligned} \quad (2)$$

where

$$a_1 = \frac{F_{12}}{X_1^* X_2^*}$$

Here it should be pointed out that there are reasons for assuming one class of models over another. The linear class is often favored in systems analysis for its mathematical simplicity and the well-developed mathematical tools which can be brought to bear on linear systems. While mathematically simple, and probably applicable in certain limited cases, it is conceptually unsatisfying to think of a predator-prey relationship as always independent of one of the interacting species. This objection is removed by invoking the Lotka-Volterra hypothesis (20) which states

that the biomass flux between two interacting populations varies as the product of the interacting biomasses (32). This, of course, leads to the nonlinear form displayed in Equation (2). The model presented in this thesis evolved into the nonlinear type.

The b vector and the addition of the effects of light and temperature will be discussed in Chapter II, which presents the details of the ecosystem model formulation. In Chapter III the control strategy and ecosystem performance index will be defined, the optimization of which will be analyzed in Chapter IV. Chapter V presents the conclusions and recommendations for further work with various simulation results given in Appendices A through C.

## CHAPTER II

### FORMULATION OF THE ECOSYSTEM MODEL

The discussion in Chapter I considered the general procedures widely used in formulation of ecosystem models. The three submodels presented in this chapter followed these guidelines. Linking of the submodels was accomplished to produce a total ecosystem model for the holding pond series. Computer simulation was performed to verify the dynamic response of the model. The simulation results for the pond ten submodel are given in Appendix B.

#### The Pond Ten Submodel

As noted previously, the submodel for pond ten was the result of a group effort involving students and faculty of the Departments of Electrical Engineering and Zoology, Oklahoma State University. Considerable amounts of data for the pond system had been accumulated by members of the Zoology Department in previous studies (3,4,11,22,28,36). This data and the general literature on zoology were the primary sources of information used to arrive at the parameters in the submodel.

Having agreed that the waters edge would be the ecosystem boundary for pond ten, the next step was to identify the system states. The functional group and compartment concepts directed this effort.

The class was divided into teams representing the different trophic levels, abiotic components, producers, herbivores, carnivores, and



decomposers. The teams worked independently and jointly confirmed their findings at regular class meetings. After identifying the system states, the teams proceeded to quantify the corresponding average standing crops.

Since light, the primary input for the ecosystem, enters on a horizontal basis, average standing crops were measured per unit area (24). The units of measurement chosen for the average standing crops were  $\text{gm/m}^2$  (dry weight). Assuming the pond depth to be an average of two meters, the average standing crop values were actually double the population densities in  $\text{gm/m}^3$  or  $\text{mg/l}$ .

Next, the teams appraised the ecosystem interactions, or flows between the model compartments. Most of the flow magnitudes were found in the literature, but some were estimated. The teams worked together in this phase and came to agreement concerning common flows. Under the assumption that the pond system was in steady-state, the sum of flows into a compartment minus the sum out was equal to zero. The pond ten submodel flow diagram is presented in Figure 3, with flow magnitudes, trophic levels, and average standing crops included. The bluegill fish compartment was added as an indicator of effluent quality.

Making use of the average standing crop and flow information available, the teams proceeded to calculate the rate parameters, or elements of the A matrix. This necessitated the decision as to what class of model to assume, basically linear or nonlinear. The group agreed to use the linear approach of the combination form, assuming that abiotic flows were recipient controlled, while biotic flows were donor controlled. The state equations arrived at are presented below:

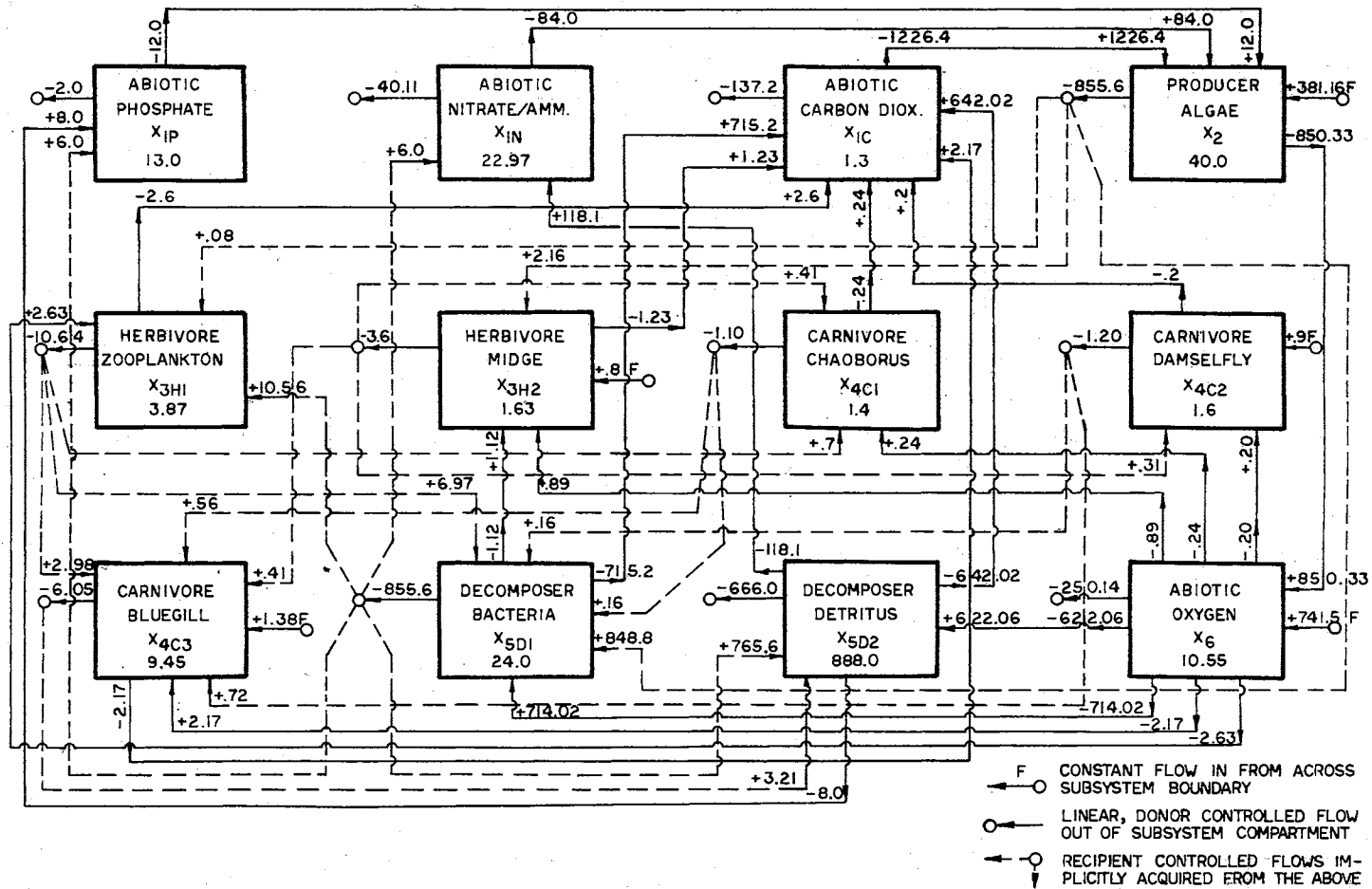


Figure 3. Pond Ten Flow Diagram

$$\dot{X}_{1P} = .25 X_{5D1} + .009 X_{5D2} - .3 X_2 - .1532 X_{1P}$$

$$\dot{X}_{1N} = .25 X_{5D1} + .133 X_{5D2} - 2.1 X_2 - 1.746 X_{1N}$$

$$\begin{aligned} \dot{X}_{1C} = & - 105.546 X_{1C} - 30.66 X_2 + .68 X_{3H1} + .745 X_{3H2} \\ & + .171 X_{4C1} + .125 X_{4C2} + .23 X_{4C3} + 29.8 X_{5D1} \\ & + .723 X_{5D2} \end{aligned}$$

$$\dot{X}_2 = - 9.529 X_2 + 381.16$$

$$\dot{X}_{3H1} = - 2.75 X_{3H1} + .44 X_{5D1} + .00206 X_2$$

$$\dot{X}_{3H2} = - 2.5 X_{3H2} + .054 X_2 + .0468 X_{5D1} + .7987$$

$$\dot{X}_{4C1} = - .789 X_{4C1} + .18 X_{3H1} + .25 X_{3H2}$$

$$\dot{X}_{4C2} = - .752 X_{4C2} + .19 X_{3H2} + .9$$

$$\begin{aligned} \dot{X}_{4C3} = & - .64 X_{4C3} + .77 X_{3H1} + .25 X_{3H2} + .4 X_{4C1} \\ & + .45 X_{4C2} + 1.38 \end{aligned}$$

$$\begin{aligned} \dot{X}_{4D1} = & - 35.65 X_{4D1} + 21.22 X_2 + 1.8 X_{3H1} + .114 X_{4C1} \\ & + .097 X_{4C2} \end{aligned}$$

$$\dot{X}_{5D2} = - .165 X_{5D2} + 31.9 X_{5D1} + .43 X_{4C3} - 623.14$$

$$\begin{aligned} \dot{X}_6 = & - 100.0 X_6 + 21.3 X_2 - .68 X_{3H1} - .548 X_{3H2} \\ & - .171 X_{4C1} - .125 X_{4C2} - .23 X_{4C3} - 29.8 X_{5D1} \\ & - .7 X_{5D2} + 1550.0 \end{aligned}$$

Note that the b vector of Equation (1) in Chapter I here can be interpreted as consisting of the balancing flow values for the compartment equations.

At this point the ecosystem model response was simulated using an IBM 360-65 digital computer and Continuous Systems Modeling Program (CSMP). The integration routine used was Runge-Kutta with variable step-size. Initial conditions were chosen reasonably close to the average standing crops (steady states). Simulation trajectories settled at the steady states, as expected, and the rate of settlement was related directly to the turnover rates. This provided a method of verifying the turnover times corresponding to the various compartments.

The diagonal terms of the A matrix correspond to the "time constant dominators" of the model, and some of these were adjusted to obtain what the teams believed to be the correct turnover rates (or reciprocal times). For example, the decoupled algae compartment's turnover time was changed to slightly less than one day by adjusting the corresponding diagonal element in the A matrix.

The "tuned" model which resulted would, given a set of initial conditions, seek the average standing crops. The next step accounted for the inputs of light and temperature determined as causal functions of time.

Light input was considered as a flow addition to the algae compartment (this proved to be in error, and will be discussed later in this chapter), thus the light influx in langleys/m<sup>2</sup>/month was merely added into the algae state equation.

Temperature influence was introduced through the Q-10 factor (27), as defined in Chapter I. A factor of the form:

$$Q-10 = 2.0 \frac{(T - T_{avg})}{10.0}$$

was used in the model. Here T designates the pond water temperature in degrees Centigrade and  $T_{avg}$  denotes the time integrated yearly average of T. All of the biotic state equations were multiplied by this factor which prescribed the temperature influence on the growth rate of a state or compartment. It is clear that, for a ten degree rise in temperature, the factor doubles, resulting in biotic growth rate doubling. This temperature dependence is usually referenced to some nominal temperature. Here, the reference used was the average pond water temperature, and at that temperature the factor is equal to unity.

With these input considerations included, the state equations [Equation (1)] become:

$$\dot{X}_{1P} = .25 X_{5D1} + .009 X_{5D2} - .3 X_2 - .1532 X_{1P}$$

$$\dot{X}_{1N} = .25 X_{5D1} + .133 X_{5D2} - 2.1 X_2 - 1.746 X_{1N}$$

$$\begin{aligned} \dot{X}_{1C} = & - 105.546 X_{1C} - 30.66 X_2 + .68 X_{3H1} + .745 X_{3H2} \\ & + .171 X_{4C1} + .125 X_{4C2} + .23 X_{4C3} + 29.8 X_{4D1} \\ & + .723 X_{5D2} \end{aligned}$$

$$\dot{X}_2 = (- 0.529 X_2 + \text{LIGHT})(Q-10)$$

$$\dot{X}_{3H1} = (- 2.75 X_{3H1} + .44 X_{5D1} + .00206 X ) (Q-10)$$

$$\dot{X}_{3H2} = (- 2.50 X_{3H2} + .054 X_2 + .0468 X_{5D1} + .7987)(Q-10)$$

$$\dot{X}_{4C1} = (- .789 X_{4C1} + .18 X_{3H1} + .25 X_{3H2})(Q-10)$$

$$\dot{X}_{4C2} = (- .752 X_{4C2} + .19 X_{3H2} + .9)(Q-10)$$

$$\begin{aligned} \dot{X}_{4C3} = & (- .64 X_{4C3} + .77 X_{3H1} + .25 X_{3H2} + .4 X_{4C1} \\ & + .45 X_{4C2} + 1.38)(Q-10) \end{aligned}$$

$$\dot{X}_{5D1} = (-35.65 X_{5D1} + 21.22 X_2 + 1.8 X_{3H1} + .114 X_{4C1} + .097 X_{4C2}) \text{ (Q-10)}$$

$$\dot{X}_{5D2} = -.165 X_{5D2} + 31.9 X_{5D1} + .43 X_{4C3} - 623.14$$

$$\begin{aligned} \dot{X}_6 &= -100.0 X_6 + 21.3 X_2 - .68 X_{3H1} - .548 X_{3H2} \\ &- 171 X_{4C1} - .125 X_{4C2} - .23 X_{4C3} - 29.8 X_{5D1} \\ &- .7 X_{5D2} + 1550.0 \end{aligned}$$

Pond water temperature and light as functions of time were generated for simulation purposes by a quadratic interpolation of the data used.

With these changes, the revised model was simulated and the trajectories checked. Computer printouts revealed that some of the abiotic states went negative and the model was unstable. Also, there was no coupling between biotic and abiotic compartments. Alleviation of these problems required that the model be changed to a nonlinear one. The abiotic flow controls were redefined to the nonlinear predator-prey type. This action led to the following submodel representation for pond ten:

$$\dot{X}_{1P} = -.1532 X_{1P} + .24 X_{5D1} + .009 X_{5D2} - .23 X_{1P} X_2$$

$$\dot{X}_{1N} = -1.746 X_{1N} + .25 X_{5D1} + .133 X_{5D2} - .0914 X_{1N} X_2$$

$$\begin{aligned} \dot{X}_{1C} &= -105.546 X_{1C} - 23.58 X_{1C} X_2 + .523 X_{1C} X_{3H1} \\ &+ .58 X_{1C} X_{3H2} + .131 X_{1C} X_{4C1} + .096 X_{1C} X_{4C2} \\ &+ .1777 X_{1C} X_{4C3} + 22.93 X_{1C} X_{5D1} + .556 X_{1C} X_{5D2} \end{aligned}$$

$$\begin{aligned} \dot{X}_{3H1} &= (-2.75 X_{3H1} + .44 X_{5D1} + .0645 X_{3H1} X_6 + .00206 X_2 \\ &- .523 X_{3H1} X_{1C}) \text{ (Q-10)} \end{aligned}$$

$$\dot{X}_{3H2} = (-2.216 X_{3H2} + .054 X_2 + .0468 X_{5D1} + .0579 X_{3H2} X_6 - .58 X_{3H2} X_{1C}) (Q-10)$$

$$\dot{X}_{4C1} = (-.789 X_{4C1} + .18 X_{3H1} + .25 X_{3H2} + .016 X_{4C1} X_{1C} - .131 X_{4C1} X_{1C}) (Q-10)$$

$$\dot{X}_{4C2} = (-.752 X_{4C2} + .19 X_{3H2} + .0118 X_{4C2} X_6 - .096 X_{4C2} X_{1C} + .9) (Q-10)$$

$$\dot{X}_{4C3} = (-.64 X_{4C3} + .77 X_{3H1} + .25 X_{3H2} + .4 X_{4C1} + .45 X_{4C2} + .0218 X_{4C3} X_6 - .1769 X_{4C3} X_{1C} + 1.38) (Q-10)$$

$$\dot{X}_{5D1} = (-35.65 X_{5D1} + 21.22 X_2 + 1.8 X_{3H1} + .114 X_{4C1} + .097 X_{4C2} + 2.82 X_{5D1} X_6 - 22.92 X_{5D1} X_{1C}) (Q-10)$$

$$\dot{X}_{5D2} = -.75 X_{5D2} - .000069 X_{5D2} X_{1P} - .0058 X_{5D2} X_{1N} - .556 X_{5D2} X_{1C} + .0664 X_{5D2} X_6 + 31.9 X_{5D1} + .43 X_{4C3}$$

$$\dot{X}_6 = -23.71 X_6 + 2.047 X_6 X_2 - .0645 X_6 X_{3H1} - .052 X_6 X_{3H2} - .0165 X_6 X_{4C1} - .0118 X_6 X_{4C2} - .0218 X_6 X_{4C3} - 2.82 X_6 X_{5D1} - .0664 X_6 X_{5D2} + 741.5$$

Simulation results now indicated that the changes were effective in eliminating the problems encountered with the linear model. Runs of approximately two years in model time showed the relative magnitudes of the standing crops and state fluctuations were as observed in the real system. However, there were phase problems (i.e., food chain lags reversed) between some compartments.

At this point the group project ended, with a reasonably successful submodel for pond ten, the last in the holding pond series. The modeling

effort which follows was carried out independently with assistance and recommendations from some of the individuals of the group.

#### Formulation of the Two Upstream Submodels

Before proceeding with the development of the models for ponds four and seven, the pond ten submodel was modified slightly. The light input was reevaluated and some minor compartment changes made. These resulted in a simulated response closer to the dynamics expected from the actual ecosystem.

Considerations concerning the inclusion of light influx as a flow into the algae compartment led to somewhat of a dilemma. Light added in this manner could be interpreted as adding an energy flux into a biomass rate representation. To correct this situation light influence was changed to a form which introduced its effect by regulating algae's fixation of carbon from  $\text{CO}_2$  through the photosynthetic process. This method of representation more closely models the actual mechanism involved. A normalized light parameter (light/avg. light) multiplying the flow of  $\text{CO}_2$  to algae modulated the  $\text{CO}_2$  uptake by algae in the model. As with previous average values, the light average refers to the time integrated yearly average.

In addition to the changes concerning light input, the detritus and bacteria (actually suspended detritus and detrital sediment) compartments were lumped due to their very similar functions in the pond ten model. The revised pond ten flow diagram is shown in Figure 4 with the corresponding state equations presented on the following page.



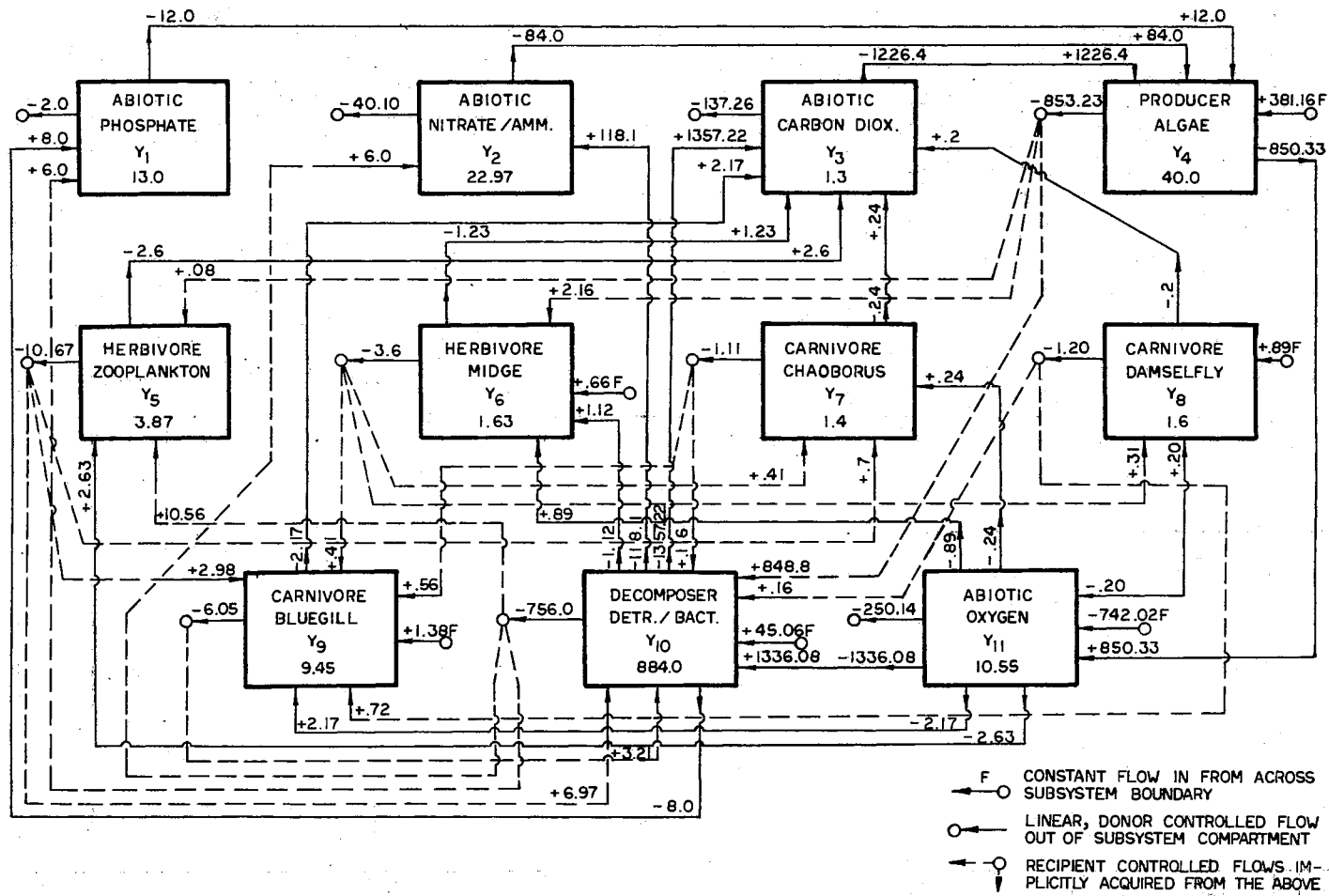


Figure 4. Pond Ten Flow Diagram (Revised)

$$\dot{Y}_1 = .15385 Y_1 - .02308 Y_1 Y_4 + .00905 Y_{10} + .00679 Y_{10}$$

$$\dot{Y}_2 = - 1.74576 Y_2 - 0.9142 Y_2 Y_4 + .13360 Y_{10} + .00679 Y_{10}$$

$$\begin{aligned} \dot{Y}_3 = & - 105.58462 Y_3 - 23.58462 Y_3 Y_4 X_4 + .17664 Y_3 Y_9 \\ & + .09615 Y_3 Y_8 + 1.18101 Y_3 Y_{10} + .13187 Y_3 Y_7 \\ & + .58046 Y_3 Y_6 + .51680 Y_3 Y_5 \end{aligned}$$

$$\begin{aligned} \dot{Y}_4 = & (23.58462 Y_3 Y_4 X_4 + .09412 Y_2 Y_4 + .02308 Y_1 Y_4 \\ & - 21.33075 Y_4 - 2.01500 Y_4 Y_{11} + 381.16) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_5 = & (- 2.75711 Y_5 - .51680 Y_3 Y_5 + .00200 Y_4 + .01195 Y_{10} \\ & + .06442 Y_5 Y_{11}) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_6 = & (- 2.20859 Y_6 - .58046 Y_3 Y_6 + .05400 Y_4 + .05175 Y_6 Y_{11} \\ & + .00127 Y_{10} + .66) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_7 = & (- .79286 Y_7 - .13187 Y_3 Y_7 + .18088 Y_5 + .25153 Y_6 \\ & + .01625 Y_7 Y_{11}) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_8 = & (- .75000 Y_8 + .01185 Y_8 Y_{11} + .19018 Y_6 - .09615 Y_3 Y_8 \\ & + .89) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_9 = & (- .64021 Y_9 + .20569 Y_{11} + .45000 Y_8 + .40000 Y_7 \\ & - .17664 Y_3 Y_9 + .25153 Y_6 + .77003 Y_5 + 1.38) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_{10} = & (- .85520 Y_{10} - .00127 Y_{10} - 1.18101 Y_3 Y_{10} - .00582 Y_{10} Y_2 \\ & + .11429 Y_7 + .14326 Y_{10} Y_{11} + 1.80103 Y_5 - .00070 Y_{10} Y_1 \\ & + 21.22000 Y_4 + .10000 Y_8 + 45.06) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_{11} = & - 23.70995 Y_{11} - .02177 Y_{11} Y_9 - .06442 Y_5 Y_{11} \\ & - .14326 Y_{10} Y_{11} - .05175 Y_6 Y_{11} - .01625 Y_7 Y_{11} \\ & - .01185 Y_8 Y_{11} + 2.01500 Y_4 Y_{11} + 742.02 \end{aligned}$$

$X_3$  represents the Q-10 factor while  $X_4$  designates the light factor in the above equations.

Simulations from this point made use of the Dynamic Simulation Program (DYSIMP) (29), available at the Oklahoma State University computer facility. This was preferred to CSMP because it offered optimization capabilities, and was less expensive. The integration routine used by this package was fixed stepsize Runge-Kutta. Due to this fixed stepsize, periodic checks were made throughout the remaining course of this work to insure numerical accuracy. The checks were made by varying the stepsize and noting the corresponding change in simulation output.

The results of the simulation showed the changes made in the pond ten submodel helped the phase situation and that the model for pond ten was essentially stable. However, initial conditions were chosen at the steady state values, since it is characteristic of nonlinear models to have system trajectories altered by a change in initial conditions. A program listing and simulation output are presented in Appendix A.

Making use of the verified submodel for pond ten, submodels for ponds four and seven were synthesized. The modeling steps established by the group effort were repeated in developing these submodels. The assumption made here was that the trophic structure in all three ponds was similar. Under this assumption, the fact that upstream ponds contained progressively fewer species and were less diverse did not lead to flow determination difficulties. In both instances, the eliminated compartments and respective flows were simply discarded while maintaining all

other flow interactions recognized in the pond ten submodel.

The modeling steps followed are outlined below:

1. determine system states;
2. find average standing crop values;
3. establish balanced flow interactions;
4. formulate the state equations;
5. test the homogeneous model (without light and temperature inputs);
6. include the effects of light and temperature; and
7. verify the final pond submodel.

Identification of the significant state variables in the upstream pond submodels demonstrated that three of the compartments included in the pond ten submodel should be eliminated in one or both of the upstream submodels. Bluegill fish and Chaoborus were excluded in both submodels, and the damselfly compartment was eliminated from the pond four submodel. The average standing crops for all three ponds are listed in Table I, with the corresponding references.

The next step in the modeling process was to determine the flows connecting the compartments in each of the submodels. The assumption of similar trophic structure fixed the flow interaction web, but to quantify the flows the following scheme was employed.

Flows in the two upstream submodels were also linear donor-recipient controlled. The donor controlled flows in ponds four and seven were scaled proportionately to the ones in ten by a ratio of the respective average standing crops. For example, assume a flow from zooplankton to Chaoborus in pond ten of  $40.0 \text{ gm/m}^2/\text{mo}$ , while the average standing crop of zooplankton there is  $20.0 \text{ gm/m}^2$ . This would imply a corresponding

flow in pond seven, where the average standing crop of zooplankton is  $10.0 \text{ gm/m}^2$ , of  $20.0 \text{ gm/m}^2/\text{mo}$ . This scheme was also used in finding the recipient controlled flow values. It was assumed the ponds were all in steady-state so that net flow into each compartment would equal zero. The flow diagrams for ponds seven and four are illustrated in Figures 5 and 6, respectively.

TABLE I  
POND AVERAGE STANDING CROPS<sup>1</sup>

Compartment	Pond 4	State	Pond 7	State	Pond 10	State	Reference
Phosphate	24.92	1	16.25	1	13.0	1	4
Nitrate/Ammonia	32.0	2	27.0	2	22.97	2	4
Carbon Dioxide	4.3	3	2.1	3	1.3	3	16
Algae	35.21	4	47.43	4	40.0	4	4, 22
Zooplankton	.99	5	3.35	5	3.87	5	22
Midges	.7	6	1.02	6	1.63	6	31
Chaoborus	-	-	-	-	1.4	7	-
Damselfly	-	-	.41	7	1.6	8	11
Bluegill Fish	-	-	-	-	9.45	9	17
Detritus/Bacteria	1722.0	7	1219.0	8	884.0	10	6, 24, 27
Oxygen	4.1	8	11.0	9	10.55	11	4

<sup>1</sup> ( $\text{gm/m}^2$ ).

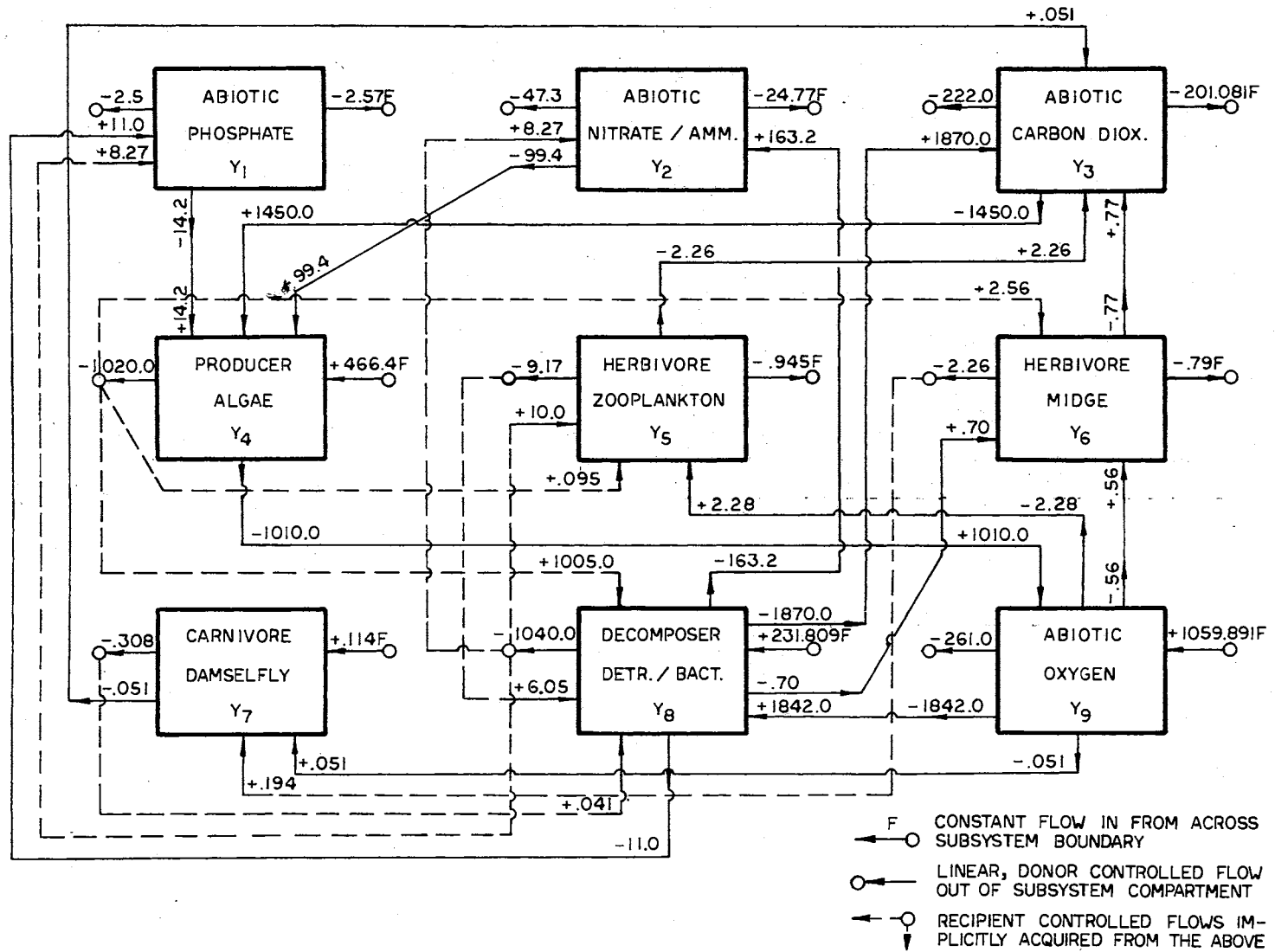


Figure 5. Pond Seven Flow Diagram

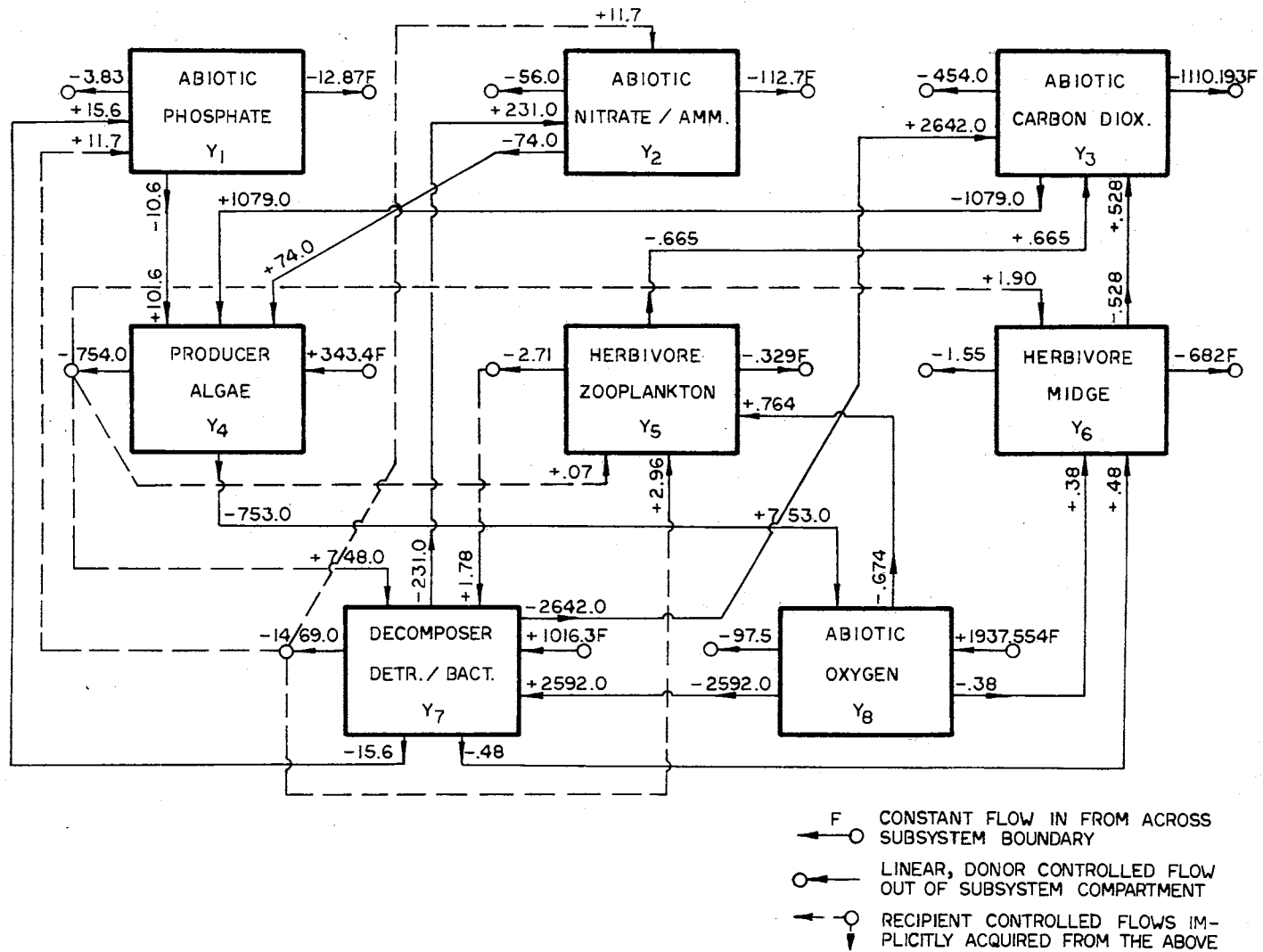


Figure 6. Pond Four Flow Diagram

By extending the concept of similar trophic structure, the assumption was made that the flow "controls", linear or nonlinear, donor or recipient, were also similar. This led to the formulation of the "undriven" state equations similar to those for the original pond ten submodel (undriven).

Testing these homogeneous submodels through simulation was performed by setting the initial conditions equal to or close to the average standing crops. Instabilities due to modeling were observed. Apparently excluding some of the state compartments and compensating for their absence led to unstable models.

The homogeneous submodels for ponds four, seven and ten (included for reference) were linearized around their respective average standing crops to resolve the stability of their equilibria (1). This is a common method used in the study of nonlinear systems which has been applied recently in the analysis of ecosystem models (33,35). The linear systems analysis program Basic Matrix (BASMAT) (21) was utilized to calculate the eigenvalues of the linearized A matrices of the three pond submodels.

It was found that instabilities in the submodels for ponds four and seven were due to the  $\text{CO}_2$  compartments, and increasing the diagonal terms in the respective locations stabilized the submodels. It should be pointed out that the stability referenced to in those linearized submodels corresponds only to local stability in the nonlinear case (1,35).

Upon elimination of the modeling stability problems, the upstream submodels were modified to include the inputs of light and temperature, just as had been done for the pond ten submodel. The representations for both of these inputs were identical to those used for the pond ten formulation. Completed state equations for the upstream pond submodels are



presented below.

Pond seven:

$$\dot{Y}_1 = - .15385 Y_1 + .00902 Y_8 + .00678 Y_8 - .01842 Y_1 Y_4 - 2.57$$

$$\dot{Y}_2 = - 1.75185 Y_2 + .00678 Y_8 - .07762 Y_2 Y_4 + .13388 Y_8 - 24.77$$

$$\begin{aligned} \dot{Y}_3 = & - 201.46714 Y_3 + 0.5923 Y_3 Y_7 - 14.55779 Y_3 Y_4 X_4 \\ & + .73050 Y_3 Y_8 + .35948 Y_3 Y_6 + .32125 Y_3 Y_5 \end{aligned}$$

$$\begin{aligned} \dot{Y}_4 = & (.01842 Y_1 Y_4 + 14.55779 Y_3 Y_4 X_4 + .07762 Y_2 Y_4 \\ & - 21.50538 Y_4 - 1.93587 Y_4 Y_9 + 466.40) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_5 = & (.00200 Y_4 - .32125 Y_3 Y_5 - 2.73731 Y_5 + .06187 Y_5 Y_9 \\ & + .00820 Y_8 - .945) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_6 = & (- 2.21569 Y_6 + .05397 Y_4 - .35948 Y_3 Y_6 + .00057 Y_8 \\ & + .04991 Y_6 Y_9 - .79) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_7 = & (- .75122 Y_7 - .05923 Y_3 Y_7 + .01131 Y_7 Y_9 + .19020 Y_6 \\ & + .114) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_8 = & (.85316 Y_8 + 21.18912 Y_4 + 1.80597 Y_5 - .00496 Y_2 Y_8 \\ & - .73050 Y_3 Y_8 - .00057 Y_8 + .13737 Y_8 Y_9 \\ & - .00056 Y_8 Y_1 + .10000 Y_7 + 231.009) (X_3) \end{aligned}$$

$$\begin{aligned} \dot{Y}_9 = & - 23.72727 Y_9 - .01131 Y_7 Y_9 - .13737 Y_8 Y_9 \\ & + 1.93587 Y_4 Y_9 - .06187 Y_5 Y_9 - .04991 Y_6 Y_9 + 1095.891 \end{aligned}$$

Pond four:

$$\dot{Y}_1 = - .15369 Y_1 + .00079 Y_7 + .00906 Y_7 - .01208 Y_1 Y_4 - 12.87$$

$$\dot{Y}_2 = - 1.75000 Y_2 + .00679 Y_7 - .06568 Y_2 Y_4 + .13415 Y_7 - 112.7$$

$$\dot{Y}_3 = - 363.76581 Y_3 - 7.12668 Y_3 Y_4 X_4 + .35681 Y_3 Y_7 \\ + .15621 Y_3 Y_5 + .17542 Y_3 Y_6$$

$$\dot{Y}_4 = (- 21.41437 Y_4 + .06568 Y_2 Y_4 + 7.12668 Y_3 Y_4 X_4 \\ + .01208 Y_1 Y_4 - 5.21609 Y_4 Y_8 - 343.40) (X_3)$$

$$\dot{Y}_5 = (-2.73737 Y_5 - .15621 Y_3 Y_5 + .00199 Y_4 + .00172 Y_7 \\ + .16606 Y_5 Y_8 - .329) (X_3)$$

$$\dot{Y}_6 = (- 2.21429 Y_6 + .05396 Y_4 - .17542 Y_3 Y_6 + .13240 Y_6 Y_8 \\ + .00029 Y_7 - .682) (X_3)$$

$$\dot{Y}_7 = (- .85308 Y_7 + 21.24396 Y_4 - .00419 Y_7 Y_2 - .35681 Y_3 Y_7 \\ + 1.79798 Y_5 + .36713 Y_7 Y_8 - .00029 Y_7 - .00036 Y_7 Y_1 \\ + 1016.3) (X_3)$$

$$\dot{Y}_8 = - 23.78049 Y_8 - .13240 Y_6 Y_8 - .16605 Y_5 Y_8 + 5.21609 Y_4 Y_8 \\ - .36713 Y_7 Y_8 + 1937.554$$

In both submodel formulations  $X_3$  is defined as the Q-10 factor and  $X_4$  indicates the light input parameter.

Light data for all three ponds were considered to be equivalent, since it was certainly reasonable to assume that light influx per unit area would be identical in each pond. However, this uniformity did not hold true for water temperature, since the flow was characteristically warmer upstream, reaching ambient as it flowed through the series (31). Thus, independent pond water temperature data was provided for each pond in degrees Fahrenheit (converted to degrees Centigrade by the model data

input routine). The data used for both inputs is condensed in Table II.

TABLE II  
WATER TEMPERATURE AND LIGHT DATA - ALL PONDS

Time (mo.) 0.0 = Oct. 1, 1961	Pond Water Temperature (31) ( $^{\circ}$ F)			Light (4) (Langleys/day/m <sup>2</sup> )
	Pond 4	Pond 7	Pond 10	
0.0	58.0	55.0	55.0	548.0
0.5	46.0	43.5	44.0	475.0
1.0	41.0	37.0	36.0	470.0
1.5	40.0	35.8	34.0	360.0
2.0	41.0	36.0	34.0	345.0
2.5	48.5	44.0	42.0	320.0
3.0	59.0	53.0	50.0	305.0
3.5	56.0	53.0	50.0	300.0
4.0	55.0	53.0	50.0	308.0
4.5	62.5	56.0	53.8	376.0
5.0	65.0	58.5	57.0	430.0
5.5	63.5	59.5	58.2	475.0
6.0	62.0	60.0	60.0	518.0
6.5	66.5	66.0	67.0	540.0
7.0	76.0	75.0	74.0	580.0
7.5	80.0	79.5	79.0	608.0
8.0	82.0	82.0	82.0	640.0
8.5	85.8	84.5	84.5	660.0
9.0	87.0	86.0	86.0	685.0
9.5	85.8	84.0	84.5	695.0
10.0	82.0	81.0	81.0	690.0
10.5	73.0	74.5	73.5	673.0
11.0	68.0	67.0	65.0	640.0
11.5	63.5	60.0	60.0	600.0
12.0	Same as 0.0, Repeat			

Linear interpolation through the data supplied the simulation with causal functions of time for light influx and the pond temperatures. Thus, the light regulator and Q-10 factors could all be calculated at each integration step.

Verification of the individual upstream submodels followed. Simulated responses matched the data and expected dynamics. The trajectories oscillated yearly around the average standing crops while magnitudes of fluctuation seemed to be reasonable. More important, phase relationships in the food chain were plausible, with algal blooms occurring when expected.

With the three submodels now complete, linking to form an overall ecosystem model for the holding pond series proceeded.

#### Linking of the Three Submodels

In choosing the linking method a compromise had to be made between depicting as nearly as possible the pond series ecosystem function and satisfying the limitations imposed by the algorithms used. Several linking attempts were evaluated before the final method was chosen. This method was to link the ponds by abiotic flows, neglecting the import or export of biotic states. These flows were delayed to produce the correct temporal relationship between the submodels, since it took approximately eight days for the effluent to flow through the pond series.

To clarify the motivation behind this modeling notion, it is necessary to look once again at the flow diagrams for ponds seven and four (Figures 5 and 6). Note that in each abiotic compartment of these submodels, there is an exiting flow proportional to the respective standing crop magnitude which is assumed to flow out of the subsystem. Certainly

a portion of this flow will enter into the adjacent downstream pond. Thus, a percentage of each of these flows proportional to the upstream standing crops, enters into the downstream pond subsystem, with an associated transport delay.

To illustrate how this action was achieved in the model, consider one of the abiotic flows from pond to pond. The upstream influence on a corresponding downstream compartment is effected by adding a flow term to that compartment which is delayed by an amount consistent with the effluent flow rate through the system. This addition, which is proportional to the upstream standing crop, must be normalized by subtracting a nominal flow from the downstream compartment, this nominal flow being proportional to the upstream average standing crop. This is necessary since merely adding a flow into the downstream compartment would unbalance the total flux at system equilibrium, which must equal zero. The pond submodel state equations would thus be revised as shown by the following example.

$$\text{Pond four: } \dot{Y}_k^t = \dots - a_{ko} Y_k$$

$$\text{Pond seven: } \dot{Y}_k = \dots + K_k a_{ko} Y_k - K_k a_{ko} Y_k^*$$

Here the  $k^{\text{th}}$  state is linked between the two ponds with  $Y_k^*$  designating the average standing crop of  $Y_k$  in pond four. Note that the linking will essentially have no effect on the ponds downstream unless the abiotic state magnitudes upstream are reasonably far from their respective average standing crops. This scheme was used to link the abiotic compartments of all three pond submodels. The overall linking mechanism is diagrammed in Figure 7.

Before the completed model could be simulated, the linking

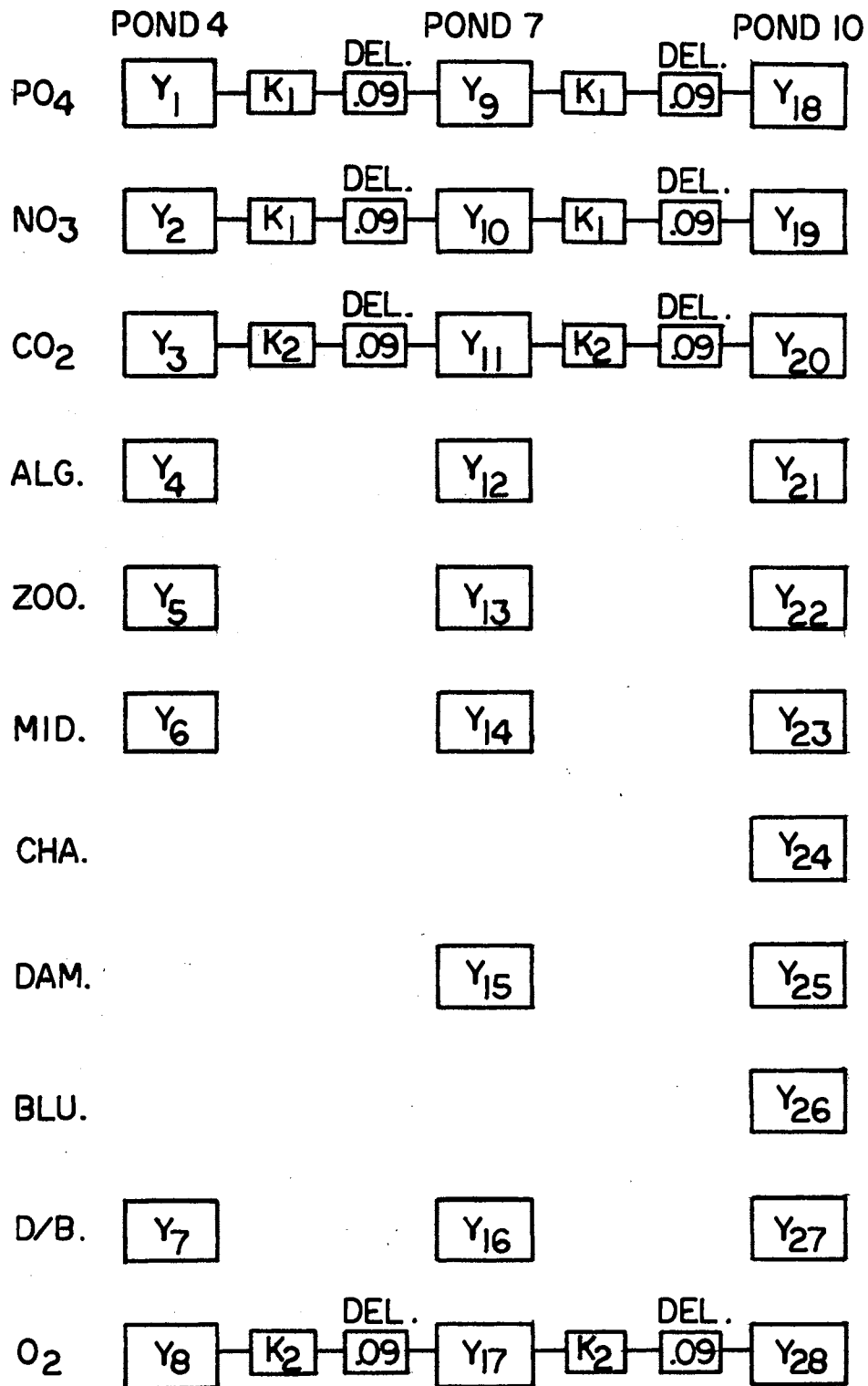


Figure 7. Pond Submodel Linking Scheme

percentages and delay duration had to be evaluated.

The linking percentages indicate the fraction of abiotic flows reaching the downstream ponds. Remembering that there are actually two ponds between each adjacent pair included in the model, the linking influence would be diminished cubically. For example, assume that 75% of the flow out of the CO<sub>2</sub> compartment in pond four reaches pond five. Then 75% of this addition would reach pond six, and so on, resulting in  $(.75)^3(100)\%$  of the original flow effecting the pond seven CO<sub>2</sub> compartment. In addition to this fact, the possibility of different percentages for different abiotic flows was considered.

Here it was assumed that the two dissolved gases, CO<sub>2</sub> and O<sub>2</sub>, could be assigned equivalent percentage rates, since both diffuse out of the pond system. Alternatively, NO<sub>3</sub> and PO<sub>4</sub> were also assigned equivalent percentage rates. The percentages were left as parameters in the model so adjustments could be facilitated. The parameter values chosen were .05 for CO<sub>2</sub> and .30 for NO<sub>3</sub> and PO<sub>4</sub>.

The delay time was assumed to be .09 mo (approximately 3 days) since the subsystems divided the pond series into three segments, and flow through the entire system took approximately eight days.

Simulation results corresponding to one year model time revealed that the model behavior closely resembled the actual pond ecosystem dynamics. Linking did have effects on the response of the downstream submodels. The completed model in this sense replicated the pond series behavior. Simulation output and program listing are included in Appendix B.

The simulations also indicated that the model was sensitive to CO<sub>2</sub> linking, the same compartment which had been adjusted previously.

Probably this was due to its highly nonlinear form and relatively quick time constants (linearization reference). This problem will be discussed further in Chapter IV.

The control scheme and performance index developments will be presented next in Chapter III.



## CHAPTER III

### CONTROL STRATEGY AND DEVELOPMENT OF THE PERFORMANCE INDEX

Formulation of the total ecosystem model for the holding pond series was presented in Chapter II. In this chapter a control philosophy is developed for the ecosystem, which is based on increasing the action of bio-degradation on the effluent water. Using the model, the resulting control scheme will be evaluated by simulation in Chapter IV. To facilitate quantification of the control strategy comparisons, a performance index is derived. The index includes both biotic indicators and control "costs" as measurements of ecosystem performance.

#### The Control Structure

There are many proven methods of management of waste treatment facilities. These include aeration, activated carbon treatment, micro-straining, effluent distribution and coagulation by polymers (9). Also, the semi-natural engineered pond ecosystem appears to be one of the most inexpensive modes of waste treatment. Although these methods have been in use for several years, testing of control schemes by ecosystem model simulations is relatively unexplored. Watt (37) has considered ecosystem management (harvest rate) through simulation while several authors (7,26, 30) have suggested the need for this type of effort in studying many of our environmental problems. Before going into the particular control

philosophy adopted in this work, some general remarks will be presented on the requirements the resulting control scheme must meet.

The control scheme must include states or inputs which can be easily measured and economically implemented in the real system, while being directly represented in the model. Controls are desired which will enhance biological action, thus improving the quality of the final effluent. The control scheme was structured with automatic control in mind, limiting direct influence to abiotic states with no biotic manipulation (i.e., dredging of detritus, fishing).

There were five basic control possibilities which could influence the biological action of the pond series and be directly represented in the model. A list of the candidate policies were:

1. lighting;
2. heating;
3. nutrient ( $\text{NO}_3$ ,  $\text{PO}_4$ ) addition;
4. aeration; and
5. flow regulation.

Three of these candidates were removed from consideration as possible controls due to their lack of feasibility. Lighting was ruled out because to effectively influence the photosynthetic process artificially would require that the pond system be virtually covered with high intensity lamps. The cost insued here would certainly be prohibitive. Both heating and nutrient addition were eliminated due to the nature of the effluent. The flow was both naturally warmer than required for biological influence and nutrient rich as a result of the refinery processes. Thus, addition of either heat or nutrients as controls to this primarily warm, eutrophic environment would be ineffective. It should be mentioned

here that although heat would improve the pond operation during a short period in the winter, at this time additional heated water from the refinery is not available.

Aeration and flow delay were included because both could economically be accomplished and had direct influence on the biological action (3, 4, 22). Aeration was controlled continuously by feedback monitoring of the oxygen standing crop in pond ten. This can be accomplished with existing oxygen level detectors (8). A feedback structure was constructed by introducing a gain which multiplied the difference between the oxygen level in pond ten and a set point which was arbitrarily chosen. This product represented the feedback aeration rate applied to pond four.

Flow delay was accomplished by allowing a variable delay of abiotic flows which linked the submodel series. This control method was also readily attainable through flow regulation in the actual system.

A diagram of the control scheme is shown in Figure 8. Now that this control scheme foundation has been defined, the performance index development will be presented.

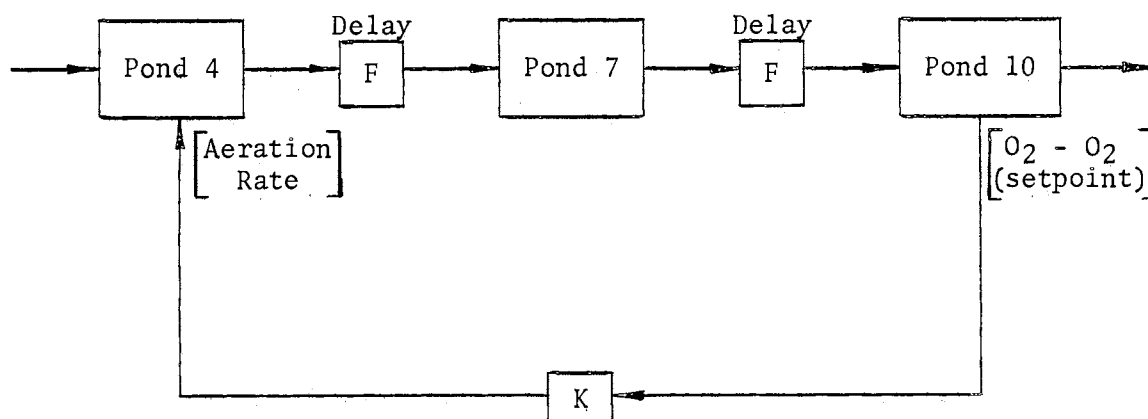


Figure 8. Control Structure

### Development of the Performance Index

A performance index (performance measure, figure of merit, cost function) is simply a number whose magnitude is an index of the merit or desirability of a solution to a problem (23). Minimizing (or maximizing) the index with respect to the control parameters corresponds to the determination of an optimum solution. Usually the performance index is manufactured to contain "trade offs" in system performance level and "cost" of control. It consists of indicators of system performance and "cost" contributions which are both scaled and weighted respectively to emphasize desired results in performance or control.

Frequently a performance index can be developed which is explicit in the parameters or variables to be optimized. This leads to the possibility of analytical solutions to the extremum problem for which there are a variety of approaches to solution (i.e., Lagrange multipliers). Usually, such an explicit formulation is not possible and a searching procedure is used to seek the optimum in an organized manner.

Optimization of the ecosystem performance with respect to the control scheme is approached here via a computer search utilizing such a performance index. Applications of this nature have been suggested by Watt (37). Minimization of the index corresponds to the lowest point on the merit surface (assuming unimodality) (38) generated by the function  $PI(X_1, X_2)$ , where  $X_1$  is the oxygen feedback gain and  $X_2$  the flow delay time. This minimum represents the best combination of the control parameters for the particular problem posed, and the lowest "cost" attained in the search.

The structure of the performance index included effluent water quality indicators and control cost rates (and penalties). These

contributions were summed by the integral form presented below:

$$PI = \int_{t_0}^{t_f} \left[ \sum_{i=1}^n (w_i u_i)^2 + \sum_{j=1}^m (w_j v_j)^2 \right] dt \quad , \quad (3)$$

where

$t_0$  = initial time;

$t_f$  = final time;

$u_i$  = the  $i^{\text{th}}$  control cost (normalized);

$w_i$  = related weight;

$v_j$  = the  $j^{\text{th}}$  system indicator (normalized);

$w_j$  = related weight;

$n$  = the number of cost contributions; and

$m$  = the number of indicator contributions.

The integral is used to provide a measure of the cumulative effects of cost, etc., while the independent summing emphasizes the individual influence of each constituent ( $u, v$ ) (23). The "trade off" here was that effluent water quality increase as a result of control effort was balanced against the costs of that effort (and penalties). The integral was included in the ecosystem model as another state equation, integrated in time along with the ecosystem simulated response.

The performance index constituents are basically of two types, effluent quality indicators and costs of control effort (or penalties).

The notion of indicators of ecosystem quality has been presented in previous studies focused on this effluent holding pond series (3,4,5,11, 22,28,31,36). As with the admissible control policies, the indicators were required to be easily measurable in the real system, and applicable in the model. The indicators used refer to pond ten only, since interest

was directed to the exiting effluent water quality. The indicators previously considered for this pond system are listed in Table III with respective references.

Many of the proposed indicators of effluent quality were disregarded for the simple reason that there was no accommodation included in the model for their computation. Ph, sulfates, chloride, dissolved solids, euphotic zone, phenol, alkalinity, chlorophyll/ash free dry weight, boron, oil, and SAR fell into this category. Many of these seem to be quite important in judging the quality of the effluent water, and the lack of their presence in the pond system model might seem unfounded. However, their effects are included implicitly in the biological actions of the model through the flow structure and data incorporated. So their exclusion does not negate the validity of the model, or its ability to resolve an optimal control strategy by predicting its effect.

The oxygen demands (BOD, COD, IOD) were excluded from consideration as effluent quality indicators because of their interpretations in the real ecosystem. It was clear that attempts to arrive at estimates for these proposed indicators from the information provided by the model would produce misleading values. Moreover, oxygen concentration was not used as an indicator since it may not reflect effluent toxicity. It is included directly as part of the control scheme, thus being indirectly used as an indicator.

Although species diversity is a good indicator of effluent quality and biotic stability, it was not used here due to the difficulty encountered in its measurement. Numerous samples are required which involve tedious identification. In this respect this proposed indicator was disregarded because of a lack of feasibility in its determination.

TABLE III  
INDICATORS OF EFFLUENT WATER QUALITY

Indicator	Desired Level	Range	Reference(s)
Species Diversity	High	5.0-7.0 Species/Cycle	11,22,28
P/R Ratio	~1.0	0.0-4.5	3,4,10,22,28
Bluegill Fish	High	0.0-10.0 gm/m <sup>3</sup>	--
Zooplankton	High	0.0-4.0 gm/m <sup>3</sup>	22,28
Bio. Ox. Demand (BOD)	Low	8.0-28.0 ppm	4,6,28
Ph	~7.0	6.9-8.6	6,22,28,36
Sulfates	Low	6.2-344.0 mg/l	6,36
Chloride	Low	20.0-1700.0 mg/l	6,36
Dissolved Solids	Low	157.0-3390.0 mg/l	36
Euphotic Zone	High	.5-1.88 m	22
Phenol	Low	0.0-1.0 ppm	4,22,28,31
Nitrate (Available Nitrogen, Ammonia)	Low	0.0-21.0 mg	4,6,28,36
Chem. Ox. Demand (COD)	Low	120.0-130.0 ppm	4,6,28
Alkalinity	Low	0.0-160.0 ppm	6,28
Chlorophyll/Ash Free Dry Weight	--	0.0-0.015	4,22
Boron	Low	0.0-0.06 mg/l	36
Oil	Low	1.0-6.0 ppm	6
Inorg. Ox. Demand (IOD)	Low	0.0-3.0 ppm	6
Dissolved Oxygen	High	2.5-6.5 ppm	6
Sodium Absorption Ratio	Low	5.4-25.0	36

Bluegill fish, heuristically included in the model for the purpose of indicating effluent water quality, depicted the long term effects of pollution. This longer sensitivity was complemented by the inclusion of zooplankton as an indicator, which possessed a relatively fast turnover rate, resulting in a quick response to "slugs" of toxic effluent (22). Both bluegill and zooplankton could easily be sampled in the real system and monitored continuously or sampled in the simulation model.

P/R ratio was used as a measure of ecosystem stability. A P/R ratio greater than one indicates an autotrophic shift with more oxygen produced than consumed while a ratio less than one indicates a heterotrophic shift or an oxygen deficit. The ratio would approach unity in a balanced steady state system with no import or export (2). However, at ecosystem equilibrium, export equals import, and their effects cancel. During periods when sufficient time was allowed for the community to stabilize the pond system was effective in treating the effluent water and the P/R ratio approached unity at the end of holding time (3,4). A graph of productivity and respiration for this pond ecosystem is shown in Figure 9 (5). Observe that productivity peaks in pond seven, and that the P/R ratio tends toward unity as the flow nears the end of the holding pond series.

The P/R ratio can be easily measured in the actual ecosystem and is obtainable from the information provided by the model. In the real system P/R could be evaluated by regular sampling or continuous monitoring of oxygen level with application of the diurnal curve method. Eley (10) provides a computer algorithm for this method which, given daily  $O_2$  data, will evaluate the P/R ratio. Note that the control structure already provides the monitoring of oxygen level required here. In the simulation



P/R can be calculated by evaluating continuously the ratio of oxygen flow from algae to oxygen (productivity) over the sum of flows of oxygen to the various compartments (respiration). Details of the procedure are presented below:

$$P/R = \frac{F_{21-28} + C}{\sum_{i=22}^{27} F_{28-i}} \quad i, 22, \dots, 27$$

$$= \frac{2.01500 Y_{21} + 46.617971}{(.021776Y_{26} + .0644164Y_{22} + .143261Y_{27} + .051755Y_{23} + .016249Y_{24} + .011848Y_{25})} \quad (4)$$

Here  $Y_{28}$  has been cancelled in both numerator and denominator;  $F_{21-28}$  represents net production, and respiration by algae is not included in the denominator. Thus, this ratio is approximately equivalent to the actual P/R ratio as per definition, since the flows involved are large. The constant in the numerator was added, so that, evaluated at the average standing crop magnitudes, the P/R ratio would equal unity.

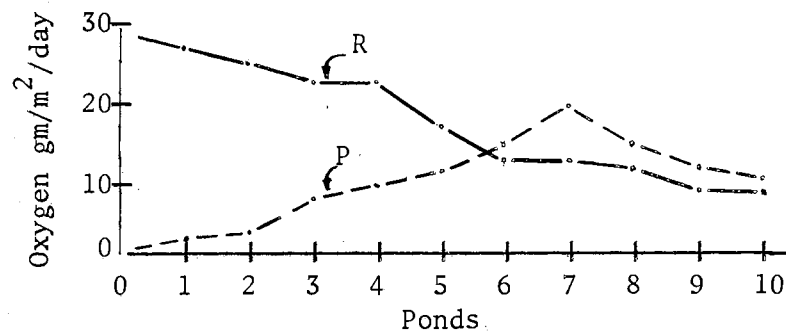


Figure 9. Productivity-Respiration for the Pond Series

Nitrate (including nitrogen contained in ammonia) was used as an indicator, being easily sampled in both pond ten and its submodel in the simulation. A maximum allowable level for this indicator has been prescribed by the State of Oklahoma (36), see Table III. It is certainly possible that in the near future, fines will be levied for violation of guidelines such as this. As an outcome of this line of thinking, the influence of nitrate (or ammonia) on the performance index consisted of introducing a set cost, representing a monthly penalty rate, when the nitrate standing crop magnitude rose above the set standard. No penalty would be introduced if the standing crop remained below the set point. In this respect, the nitrate (or ammonia) contribution to the performance index represents a penalty, or cost which can indirectly be offset by control effort. The direct costs of this control will be discussed next.

The controls which have been selected are feedback aeration and flow delay adjustment. The associated costs may readily be deduced in the ecosystem application and continuously calculated in the simulation. Aeration cost rates considered the options of mechanical or diffusion aerators and the flow delay cost allowed for the burden of low flow rate on the refinery operations.

#### Performance Contribution Weighting

With the constituents of the performance index defined, each contributor was normalized so that at ecosystem equilibrium (at the average standing crops), its value would equal one or zero. This was necessary so that weighting of the individual performance index contributions could be accomplished (38). The biotic indicators, fish and zooplankton, were normalized using the following procedure:

$$v_i = \frac{Y_i^*}{Y_i} ,$$

where

$Y_i^*$  =  $i^{\text{th}}$  average standing crop value;

$Y_i$  =  $i^{\text{th}}$  standing crop value; and

$v_i$  = as given by Equation (3).

In order to maximize  $Y_i$  one would minimize the reciprocal, and at equilibrium the indicator value would equal unity.

The ecosystem stability indicator, P/R ratio, was subtracted from one to normalize its value since its equilibrium magnitude was prescribed to be unity, and deviations far from one were undesirable. The structure of the nitrate penalty guaranteed it to equal one or zero in "normalized" form, depending on whether the limit of allowable nitrate had been exceeded or not. At ecosystem equilibrium, both of these normalized forms equaled zero.

The costs of control, as with the nitrate penalty, were already in a "normalized" form due to their direct relatibility to expense in dollars.

With the normalization forms constructed, weights were determined for the various u's and v's [see Equation (3)]. Weighting of control costs and penalty was done by setting the corresponding weight values equal to the expected costs per month. Aeration costs (mechanical, diffusion) were calculated from data provided by Davis (9). The cost of flow control and the nitrate penalty were estimated. The biotic weights (P/R, fish, zooplankton) were estimated and are subject to conjecture. The relative values of these ecosystem quality indicators has not been considered previously, but determinations of this kind are required in this type of performance index application. If the weights arrived at

for these indicators seem high, one might consider the costs of advertising which could be offset by publicity benefits of biotic quality signs (e.g., fish in the last pond). In this era of ecological emphasis, such an indication of unpolluted effluent release can easily rationalize these weights. The weight values imposed are given in Table IV. The square roots were used for the performance index weighting so that the evaluated integral would directly represent cumulative cost trade offs.

TABLE IV  
PERFORMANCE INDEX CONTRIBUTORS AND WEIGHTS

Contributor	Normalized Form	Notation (Eq. 3)	Weight (\$/mo)	Approx. $\sqrt{\text{weight}}$
Aeration Cost				
Diffusion	--	$u_1$	44.7	7.0
Mechanical	--		34.4	6.0
Flow Delay Cost	Delay/Nominal Delay	$u_2$	50.0	7.0
Nitrate (Ammonia) Penalty	--	$v_1$	30000.0	170.0
P/R	(1.0 - P/R)	$v_2$	100.0	10.0
Bluegill Fish	$Y_{26}/Y_{26}^*$	$v_3$	40.0	6.0
Zooplankton	$Y_{22}/Y_{22}^*$	$v_4$	40.0	6.0

The form and all of the components of the performance index have been defined and evaluated. Now, with all of the contributions and weights included, the index described by Equation (3) appears in the

simulation as shown below:

$$PI = \int_{t_0}^{t_f} \left\{ [P_7 \left( \frac{3.87}{Y_{22}} \right)]^2 + [P_8 \left( \frac{9.45}{Y_{26}} \right)]^2 + [P_9 (1.0 - P/R)]^2 \right. \\ \left. + [P_{10}]^2 + [P_{11} \left( \frac{P_{12}}{.090} \right)]^2 + [P_{13} X_{39}]^2 \right\} dt$$

where

$$P_7 = 40.0;$$

$Y_{22}$  = zooplankton standing crop in pond 10;

$$P_8 = 40.0;$$

$Y_{26}$  = fish standing crop in pond 10;

$$P_9 = 100.0;$$

$P/R$  = as given by Equation (4);

$$P_{10} = \begin{cases} 30000.0 & \text{if } NO_3 \text{ standing crop in pond 10 } (Y_{19}) \text{ is above the} \\ & \text{upper limit } P_{15} = 24.0 \\ 0 & \text{otherwise;} \end{cases}$$

$$P_{11} = 50.0;$$

$P_{12}$  = delay time;

$$P_{13} = 34.0; \text{ and}$$

$X_{39}$  = oxygen feedback flow ( $gm/m^2/mo$ ).

The ecosystem performance optimization utilizing this index and the control scheme presented in this chapter will be discussed in Chapter IV.

## CHAPTER IV

### ECOSYSTEM PERFORMANCE OPTIMIZATION

Using the control scheme and performance index developed in Chapter III, optimization of the ecosystem performance is discussed in this chapter. A computer search was conducted over the control parameter plane to seek the optimal control. Each evaluation of the index determining one point on the merit surface corresponded to one pair of the control parameters, and a simulation of one half year of model time. Minimization of the performance index indicated the best parameter combination and most suitable ecosystem response. The simulation listing and results of the search are presented in Appendix C.

#### Preparation of the Model for Optimization

The search procedure selected for the optimization was a Grid (23) method. This method seeks an extremum by conducting a series of alternating grid and star patterned performance index evaluations of progressively decreasing size over the control parameter plane (in this two dimensional case). There were three reasons for selecting this method. First, the nature of the merit surface was totally unpredictable; perhaps the only thing known about it was that it would be continuous. This prevented the application of many of the searching methods with faster convergence requiring knowledge or determination of derivatives. The second reason was that this search will seldom encounter numerical

difficulty or stall out. The third reason was that a Grid search by its design gives one an overall picture of the merit surface, since individual trial points are spaced relatively far apart.

Upon selection of the search algorithm, the model was prepared for the optimization simulation runs. Output limiters placing bounds on the magnitudes of the states were installed. The limiters were used because of the suspected local stability of the model, with ecosystem states remaining well behaved within a neighborhood of the equilibrium (or average standing crops). Upper bounds were chosen by considering past simulation results and minimum bounds were all set at zero. These limiters were installed merely as safeguards, and it was observed later that they did not influence the model simulation results significantly.

#### Model Sensitivity to Control

Before further optimization considerations, the ecosystem model was checked for sensitivity to control effort. This was done to determine magnitudes of the control parameters required to affect the performance "trade offs" discussed in Chapter III. Knowledge of these magnitudes would lead to suitable first guesses for the ranges over which the two parameters, aeration feedback gain and flow delay time, would be allowed to vary in the search.

The sensitivity investigations were carried out by conducting small one dimensional searches, fixing one control parameter while varying the other. In other words, the checks ran along the axes of the control parameter plane, or lines of zero control effort in one variable. From these preliminary sensitivity checks it was evident that the model was relatively insensitive to oxygen feedback of small magnitudes, and to

moderate delay parameter adjustment. These conclusions spurred an investigation of the response of the pond four submodel to oxygen addition, the function of the feedback.

The pond four submodel was unlinked from the series and simulated independently to determine the effects of adding an input flow into the oxygen compartment. Results indicated that addition of this flow, even in relatively large amounts, had a small effect on increasing the standing crop of oxygen in that pond. The supplementary flux seemed to "flow through" the oxygen compartment, with most of the subsequent biomass ending up in the detritus/bacteria compartment. This was certainly interesting but not surprising. In fact, this behavior could be expected in an ecosystem of this type. This model behavior resulted primarily from the nonlinear nature of the oxygen compartment.

Lack of response to oxygen feedback in the pond four submodel led to a far greater insensitivity in the downstream submodels. The linking diminished the effects of feedback and there resulted almost no influence on the oxygen standing crop in pond ten. To create a more sensitive model, two actions were taken. The linking parameter value for oxygen was increased to 1.0, the maximum possible, and the oxygen feedback was applied to all three ponds, not only pond four.

The  $O_2$  linking increase brought out somewhat of a problem, due to the sensitivity of the model series to  $CO_2$  linking, mentioned near the end of Chapter III. This created a conflict because the linking of both of these compartments throughout the model was controlled by a common parameter. Thus, to maintain a linking value of 1.0 for  $O_2$  while having a relatively small  $CO_2$  link for model stability, an additional linking parameter was installed for  $O_2$  alone. The value of the  $CO_2$  parameter was



left at .05, and the  $\text{NO}_3 - \text{PO}_4$  parameter was increased to .50.

The feedback modification in the control structure followed precisely the form established in Chapter III, with the exception that the feedback aeration was split between submodels. Cost weighting in the performance index corresponding to the aeration contribution was adjusted accordingly. The revised control scheme appears as shown in the following diagram (Figure 10). The model optimization program listing is presented in the first of Appendix C.

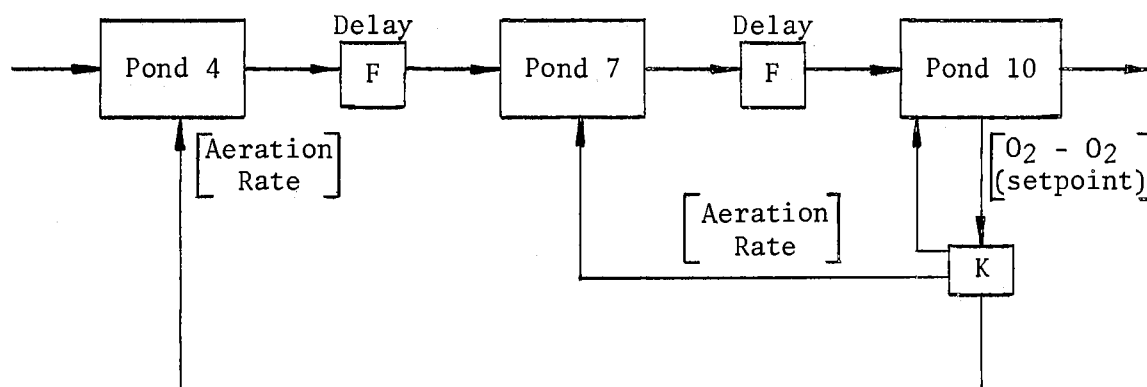


Figure 10. Modified Control Structure

With these revisions included in the model, the procedure of investigating its sensitivity to control was repeated. Results indicated the model was considerably more sensitive to control effort. Although the controls now had desirable effects on the ecosystem model response (i.e., increasing the standing crop of bluegill in pond ten), the performance index weighting was imbalanced, providing too much influence to the costs and penalty. Thus, the next action taken was to investigate the relative

ranges of fluctuation for the performance index constituents. This led to the determination of weighting modifications (or scaling) to correct the imbalance.

A small two dimensional search was conducted to evaluate the performance index contribution ranges. The simulations revealed that fluctuations of the cost of control far outweighed those of the indicator contributions, due to their respective weighting factors. This caused the search algorithm to seek the "zero control effort" corner of the control parameter plane, as the minimum performance index magnitude.

Less expensive one dimensional searches were used to pinpoint the trouble. Their results showed that varying the oxygen feedback and delay parameters over a very wide range (0.0 - 600.0; .090 - 1.0) incurred large fluctuations in cost with small fluctuations in indicator response. Observing the individual performance index contributions and noting the ranges allowed in the control inputs, the contributor sensitivities were deduced. These sensitivities are listed in Table V (a), with the weighting factors used given for later comparison.

It was obvious from this information there existed a considerable imbalance in the contributions to the performance index. To alleviate this problem the weights were modified (or scaled) so that the sensitivities listed in Table V (a) would transform into approximately equivalent contribution changes. The modified weights with resulting sensitivity values are given in Table V (b).

Simulations now indicated the weighting modifications led to the performance index "trade offs" necessary to eliminate the characteristic of minimization at the "zero control corner" of the parameter plane.

Subsequent one dimensional searches along the control plane

TABLE V  
 PERFORMANCE INDEX CONTRIBUTION SENSITIVITIES<sup>1,2</sup>

Contribution	Weight	Range	
(a) Original			
Aeration Cost	18.0	~700.0	
Flow Delay Cost	7.0	~100.0	
Nitrate Penalty	170.0	--	
P/R	10.0	~ .30	
Bluegill	6.0	~ .30	
Zooplankton	6.0	~ .45	
(b) Modified			
Contribution	Weight	Range	Scale Factor
Aeration Cost	.90	~35.0	.05
Flow Delay Cost	5.0	~72.0	.715
Nitrate Penalty	30.0	--	.176
P/R	1000.0	~30.0	100.0
Bluegill	400.0	~20.0	66.7
Zooplankton	400.0	~30.0	66.7

<sup>1</sup>To control.

<sup>2</sup>Oxygen Feedback Range = 0.0 - 600.0; Delay Range = .090 - 1.0.

boundaries were now conducted over a model time period of six months. This was done because for approximately the first six months the oxygen level in the pond ten submodel would not fall below the set point, regardless of delay parameter value. Thus, lack of oxygen feedback led to near duplication of simulated responses for the early months in all parameter variable runs. Therefore, only the last six months of the cycle were simulated only to save costs. The searches revealed that along the control boundaries, local minima were included in the large ranges of control tested. In other words, the minimum values of the performance index had been bracketed along the control parameter axes. The results are illustrated in Figure 11. Note that along the delay time axis the bracketing is implicit.

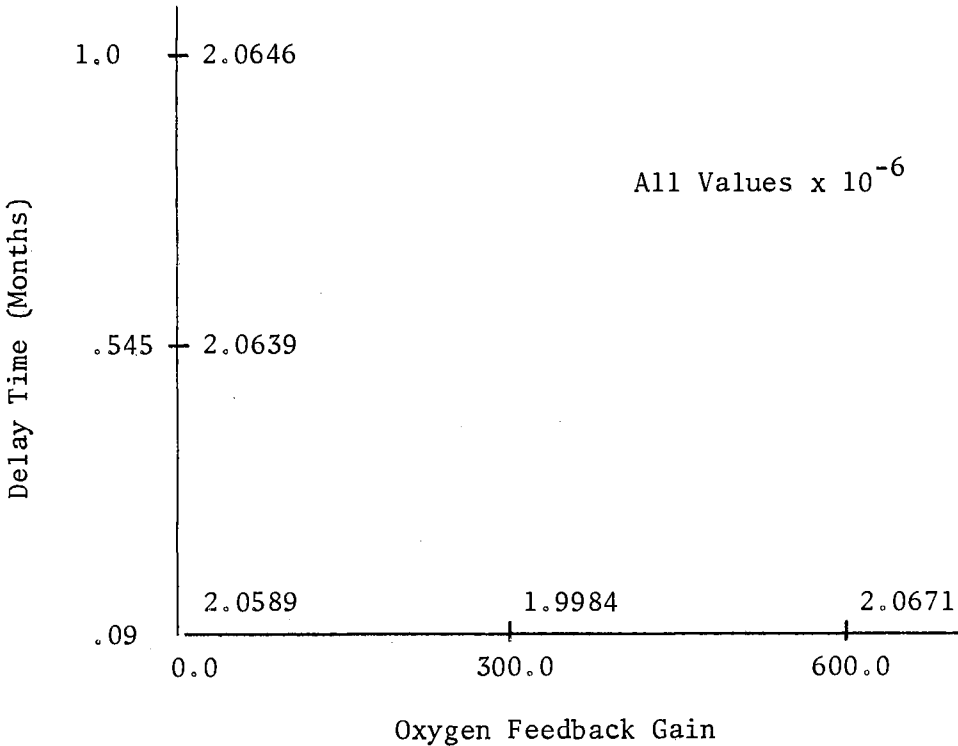


Figure 11. Boundary Minimization Bracketing

### Optimization Results

A large two parameter optimization series was now conducted. The computer output from this search is included in Appendix C. It indicated conclusively that an optimum does exist in the overall region specified. An illustration of the merit surface evaluations and their locations is provided in Figure 12.

The minimum performance index value found was  $1.9817 \times 10^6$  at (66.0, .3933). Notice that the minimum is surrounded by evaluations of higher magnitude. Converging further to the optimum by specifying a smaller fractional reduction would now be possible but was not done here. It is obvious that the location of the minimum is subject to influence by the weighting factors. Further investigation is not merited here due to question of significance of the numbers used and those which would result.

These results do show, however, that this minimization technique was successful in finding the optimal control strategy for the ecosystem problem posed. Not only was the minimum performance value bracketed by the fourth evaluation group, but by considering Figure 12 there is no implication that the merit surface is other than unimodal. Also, the applicability of ecosystem models and simulations to the study of real environmental problems is clearly demonstrated. Utilizing models to predict ecosystem control policy effects should certainly prove successful in future studies concerned with alleviating our environmental problems brought on by waste pollution. Recommendations for future work are reflected in the following chapter.

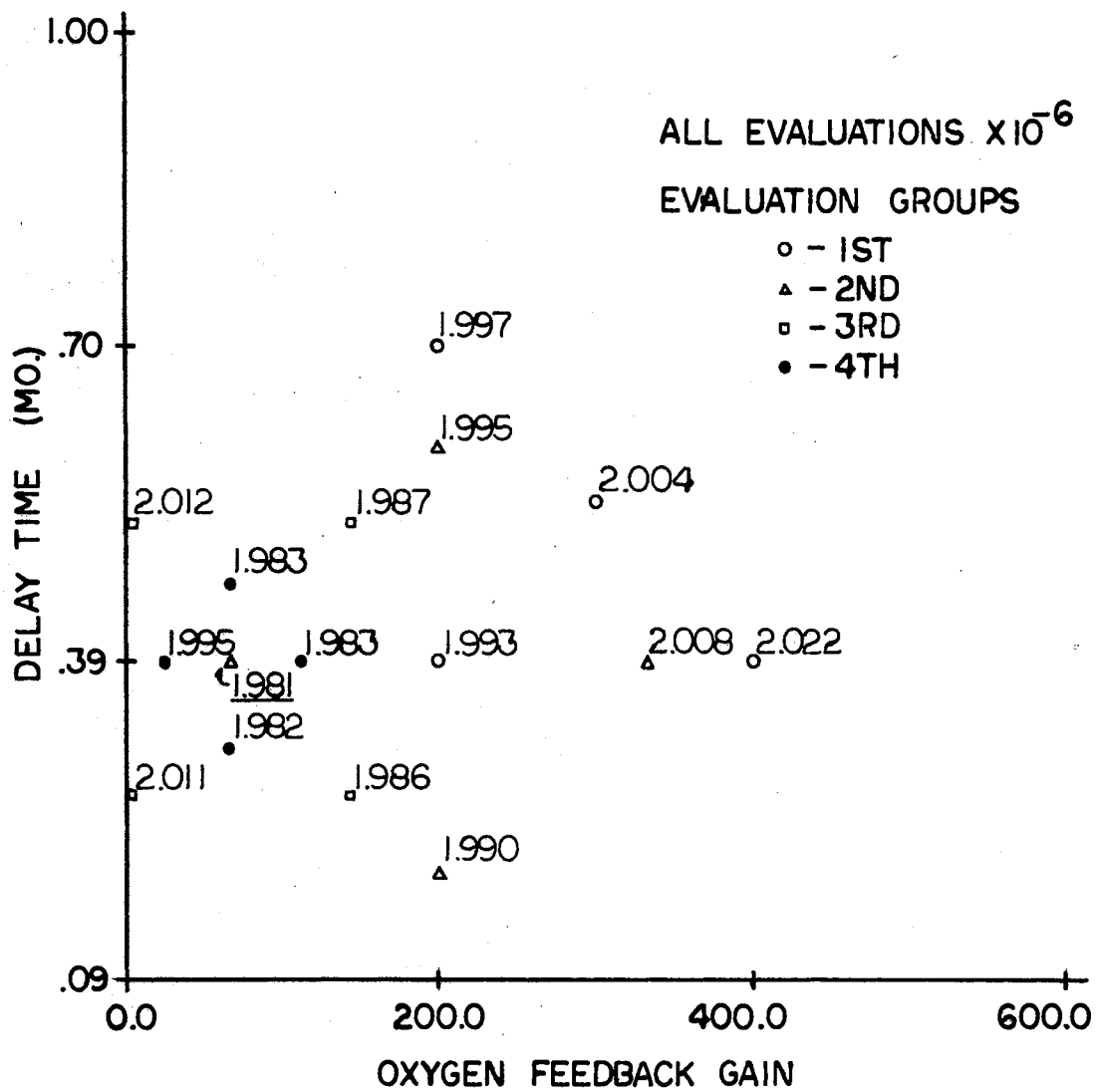


Figure 12. Optimization Results

## CHAPTER V

### CONCLUSIONS AND RECOMMENDATIONS

A total ecosystem model has been developed for a particular pollution abatement ecosystem consisting of a series of oil refinery effluent holding ponds. Simulations were performed using a digital computer, and the model response was verified with the observed behavior of the pond series.

A control philosophy and a measure of ecosystem performance were adopted. The control parameters considered were the pond series flow rate and feedback aeration, both of which influence effluent treatment by biological activity. Control costs and direct biological indicators are included as contributions to the performance index.

An optimization search utilizing the computer was conducted in order to maximize the ecosystem performance. The minimization of the performance index corresponded to attaining the optimal control parameter combination.

Although this thesis considered a particular ecosystem problem, many of the approaches taken and techniques applied here serve as a basis for extended efforts in this field. Computer simulations will surely play an increasingly important role in the study and analysis of ecological systems. The application of an ecological performance index is necessary in the evaluation of possible control schemes, and control in the environmental sense is certainly of the utmost value. However, before more

exacting work can be done in these areas, ecosystem modeling itself must be clarified and methodized. Thus, all the recommendations made here concern the ecosystem modeling process.

#### Recommendations for Further Study

The following points must be considered in further research into the topic:

1. The characteristics and attributes of ecosystem models resulting from application of the various popular modeling forms (linear, nonlinear, donor controlled, etc.) need to be studied in a comparative light. The fundamental decision of which model type can replicate actual ecosystem dynamics in general must be reconciled.

2. Much of the difficulty involved in ecological modeling is deciding which communities to include as state variables and then how to measure them efficiently. Criteria for selecting the populations which dominate the ecosystem dynamics should be outlined, so that future work in this field will be more organized.

3. In most cases to date, ecosystem models have been developed from insufficient data and partial guesswork. This emphasizes the need for refined procedures for data collection and assimilation for the modeling effort. Time series data to accomodate the ecosystem identification process undoubtedly would assist the ecosystem modeler.

4. The possibility of "fitting" ecosystem models to that data, (using tools such as the method of least squared error) as opposed to intuitive formulations needs to be explored. If conclusive evidence is found that data fitting can result in plausible ecosystem realizations, the modeling process involved will be greatly simplified.



5. Testing procedures should be developed for the purpose of model verification. Introducing inputs or disturbances which can be facilitated in both the actual ecosystem and its model counterpart would be a possible testing method.

6. It may become advantageous to consider ecosystem observability and controllability. Research in this area could directly influence work in the related fields described by recommendations 1 and 2.

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## APPENDIX A

### POND TEN SIMULATION RESULTS

The program listing and computer output for the pond ten submodel simulation are presented here. The listing provides the DYSIMP user deck (FORTRAN IV) and complete data for the simulation problem. Output is given in both graphic and tabular forms.

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      DYSIMP USER DECK

      COMMON/ ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NR,NW
      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
      READ(NR,2000) M
      DO 2002 I=1,M
10      READ(NR,2001)T(I),WT10(I),SOL(I)
11      WT10(I)=(WT10(I)-32.0)*(5.0/9.0)
12      IER=0
13      IXVAL=1
14      CALL DYSIMP(I,XVAL,IER)
15      2001 FORMAT(3F10.0)
16      2002 FORMAT(15)
17      STOP
18      END

      FUNCTION W10(TIME)
21      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
22      DO 1 J=2,M
23      IF(TIME.LT.T(J)) GO TO 2
24      IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
25      1 CONTINUE
26      IF(TIME.GE.T(M)) W10=WT10(M)
27      RETURN
28      2 W10=WT10(1)
29      RETURN
30      3 W10=WT10(J-1)+(TIME-T(J-1))*(WT10(J)-WT10(J-1))/(T(J)-T(J-1))
31      RETURN
32      END

      FUNCTION SOL1(TIME)
35      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
36      DO 1 J=2,M
37      IF(TIME.LT.T(1)) GO TO 2
38      IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
39      1 CONTINUE
40      IF(TIME.GE.T(M)) SOL1=SOL(M)
41      RETURN
42      2 SOL1=SOL(1)
43      RETURN
44      3 SOL1=SOL(J-1)+(TIME-T(J-1))*(SOL(J)-SOL(J-1))/(T(J)-T(J-1))
45      RETURN
46      END

      SUBROUTINE DERFUN
48      DIMENSION YINPUT(45),F(45)
49      COMMON/ ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NR,NW
50      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
51      EQUIVALENCE(YINPUT(1),F(1))
52      F(1)=-1.5385*Y(1)-0.2308*Y(1)*Y(4)+.00905*Y(10)+.00679*Y(10)
53      F(2)=-1.74576*Y(2)-.09142*Y(2)*Y(4)+.13360*Y(10)+.00679*Y(10)
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000000001111111122222222333333334444444455555555666666667777777788  
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CARD
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      F(3)=-105.58462*Y(3)-23.58462*Y(3)*Y(4)*X(4)+.17664*Y(3)*Y(9)
56      1+.09615*Y(3)*Y(8)+1.18101*Y(3)*Y(10)+0.13187*Y(3)*Y(7)+.58046
57      1*Y(3)*Y(6)+.51680*Y(3)*Y(5)
58      F(4)=(+23.58462*Y(3)*Y(4)*X(4)+.09412*Y(2)*Y(6)+.02308*Y(1)*Y(4)
59      1-21.33075*Y(4)-2.01500*Y(4)*Y(11)+381.16)*X(3)
60      F(5)=(-2.75711*Y(5)-.51680*Y(3)*Y(5)+.00200*Y(4)+.01195*Y(10)
61      1+.06442*Y(5)*Y(11))*X(3)
62      F(6)=(-2.20859*Y(6)-.58046*Y(3)*Y(6)+.05400*Y(4)+.05175*Y(6)
63      1*Y(11)+.00127*Y(10)+.66)*X(3)
64      F(7)=(-.79286*Y(7)-0.13187*Y(3)*Y(7)+.18088*Y(5)*.25153*Y(6)
65      1+.01625*Y(7)*Y(11))*X(3)
66      F(8)=(-.75000*Y(8)+.01185*Y(8)*Y(11)+.19018*Y(6)-.09615*Y(3)*Y(8)
67      1+.89)*X(3)
68      F(9)=(-.64021*Y(9)+.20569*Y(11)+.45000*Y(8)+.40000*Y(7)-.17664
69      1*Y(3)*Y(9)+.25153*Y(6)+.77003*Y(5)+1.381)*X(3)
70      F(10)=(-.85520*Y(10)-.00127*Y(10)-1.18101*Y(3)*Y(10)-.00582
71      1*Y(10)*Y(2)+.11429*Y(7)+.14326*Y(10)*Y(11)+1.80103*Y(5)-.00070
72      1*Y(10)*Y(11)+21.22000*Y(4)+.10000*Y(8)+45.06)*X(3)
73      F(11)=-23.70995*Y(11)-.02177*Y(11)*Y(9)-.06442*Y(5)*Y(11)
74      1-.14326*Y(10)*Y(11)-.05175*Y(6)*Y(11)-.01625*Y(7)*Y(11)-.01185
75      1*Y(8)*Y(11)+2.01500*Y(4)*Y(11)+742.02
76      DO 1 I=1,NY
77      IEU=NYP2+I
78      1 Y(IEU)=YINPUT(I)
79      RETURN
80      END

      SUBROUTINE XVAL
82      COMMON/ ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NR,NW
83      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
84      X(1)=W10(Y(NYP1))
85      X(2)=SOL(Y(NYP1))
86      X(3)=2.0*(-.16.0301-X(1))/10.0)
87      X(4)=X(2)/508.7910
88      RETURN
89      END

      SUBROUTINE INTDEL
92      COMMON/ ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NR,NW
93      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
94      COMMON/ CDELAY/OELAYV(4000),LABELD(25,4),IDTYPE(25),NO,NOY,NDMAX,
95      1 IWEIAY,TIME(25)
96      J=LABELD(1,1)
97      K=LABELD(1,2)
98      DO 1 I=J,K
99      1 OELAYV(I)=P(2)
100      RETURN
101      END

      SUBROUTINE PARADJ
103      COMMON/ ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NR,NW
104      COMMON/ MEAS/T(100),WT10(100),SOL(100),M
105      READ(NR,1) P(1)
106      1 FORMAT(1F10.0)
107      RETURN
108

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80/80 LIST

00000000111111112222222233333333444444445555555566666666777777778  
 123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890

CARD	END	DATA
109		
110		
111		
112		
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115	49	
116	0.0	55.0 548.0
117	0.5	44.0 475.0
118	1.0	30.0 420.0
119	1.5	34.0 380.0
120	2.0	34.0 345.0
121	2.5	42.0 320.0
122	3.0	50.0 305.0
123	3.5	50.0 300.0
124	4.0	50.0 308.0
125	4.5	53.8 376.0
126	5.0	57.0 430.0
127	5.5	58.2 475.0
128	6.0	60.0 518.0
129	6.5	67.0 540.0
130	7.0	74.0 580.0
131	7.5	79.0 608.0
132	8.0	82.0 640.0
133	8.5	84.5 660.0
134	9.0	86.0 685.0
135	9.5	84.5 695.0
136	10.0	81.0 690.0
137	10.5	73.5 673.0
138	11.0	65.0 640.0
139	11.5	60.0 600.0
140	12.0	55.0 548.0
141	12.5	44.0 475.0
142	13.0	36.0 420.0
143	13.5	34.0 380.0
144	14.0	34.0 345.0
145	14.5	42.0 320.0
146	15.0	50.0 305.0
147	15.5	50.0 300.0
148	16.0	50.0 308.0
149	16.5	53.8 376.0
150	17.0	57.0 430.0
151	17.5	58.2 475.0
152	18.0	60.0 518.0
153	18.5	67.0 540.0
154	19.0	74.0 580.0
155	19.5	79.0 608.0
156	20.0	82.0 640.0
157	20.5	84.5 660.0
158	21.0	86.0 685.0
159	21.5	84.5 695.0
160	22.0	81.0 690.0
161	22.5	73.5 673.0
162	23.0	65.0 640.0

80/80 LIST

00000000111111112222222233333333444444445555555566666666777777778  
 123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890

CARD	DATA	POND	TEN	SUBMODEL	RESPONSE
163	23.5	60.0	600.0		
164	24.0	55.0	566.0		
165	1 1 1 1 0 0 0 0				
166	11 4 0 40		0.3	23.9	.005
167	13.0	22.97	1.3	40.0	3.87
168	9.45	884.0	10.55		1.63 1.4 1.6
169	2 3 6 7		8 10 11		
170	1 4 5 9				
171					
172					
173					
174					
175					

DYSIMP SIMULATION PROGRAM

POND TEN SUBMODEL RESPONSE

ORDER OF SYSTEM = 11  
 NUMBER OF X'S = 4  
 NUMBER OF PARAMETERS = 0  
 OUTPUT INTERVAL = 40  
 INITIAL TIME = 3.0000E-01  
 FINAL TIME = 2.3900E 01  
 INTEGRATION STEP = 5.0000E-03

INITIAL Y VALUES

Y( 1) = 1.300000E 01    Y( 2) = 2.296999E 01    Y( 3) = 1.299999E 00    Y( 4) = 4.000000E 01    Y( 5) = 3.870000E 00  
 Y( 6) = 1.629999E 00    Y( 7) = 1.400000E 00    Y( 8) = 1.599999E 00    Y( 9) = 9.453003E 00    Y(10) = 6.840000E 02  
 Y(11) = 1.055000E 01

INITIAL X VALUES

X( 1) = 9.111113E 00    X( 2) = 5.042000E 02    X( 3) = 6.190392E-01    X( 4) = 9.909770E-01

DYSIMP SIMULATION PROGRAM

POND TEN SUBMODEL RESPONSE

TIME	Y( 1)	Y( 2)	Y( 3)	Y( 4)	Y( 5)	Y( 6)	Y( 7)	Y( 8)	Y( 9)	Y(10)	Y(11)
3.000E-01	2.296998E 01	1.299999E 00	1.629999E 00	1.399999E 00	1.599999E 00	8.640000E 02	1.054999E 01				
5.000E-01	2.252371E 01	1.545283E 00	1.629233E 00	1.398421E 00	1.598798E 00	8.787949E 02	1.140796E 01				
7.000E-01	2.180226E 01	1.683197E 00	1.629302E 00	1.395577E 00	1.596429E 00	8.721906E 02	1.226178E 01				
9.000E-01	2.104290E 01	1.892849E 00	1.627685E 00	1.391524E 00	1.594184E 00	8.634799E 02	1.328762E 01				
1.100E 00	2.027702E 01	2.122989E 00	1.623763E 00	1.386330E 00	1.590934E 00	8.528173E 02	1.446182E 01				
1.300E 00	1.960760E 01	2.354390E 00	1.618774E 00	1.379915E 00	1.587088E 00	8.401774E 02	1.567611E 01				
1.500E 00	1.896966E 01	2.637569E 00	1.605483E 00	1.372034E 00	1.582495E 00	8.247487E 02	1.719087E 01				
1.700E 00	1.835910E 01	2.943951E 00	1.588872E 00	1.362462E 00	1.577052E 00	8.062277E 02	1.889015E 01				
1.900E 00	1.776727E 01	3.316199E 00	1.565176E 00	1.350769E 00	1.570513E 00	7.836084E 02	2.096797E 01				
2.100E 00	1.718478E 01	3.719819E 00	1.532337E 00	1.336391E 00	1.562583E 00	7.559626E 02	2.328734E 01				
2.300E 00	1.666758E 01	4.089202E 00	1.488301E 00	1.317573E 00	1.552485E 00	7.211577E 02	2.539227E 01				
2.500E 00	1.615043E 01	4.448167E 00	1.423029E 00	1.292551E 00	1.539344E 00	6.771110E 02	2.762310E 01				
2.700E 00	1.567715E 01	4.848591E 00	1.342740E 00	1.260188E 00	1.523045E 00	6.254470E 02	2.880270E 01				
2.900E 00	1.522995E 01	4.791222E 00	1.249478E 00	1.219597E 00	1.503638E 00	5.689201E 02	2.934478E 01				
3.100E 00	1.477255E 01	4.743268E 00	1.148901E 00	1.170753E 00	1.481594E 00	5.111540E 02	2.917004E 01				
3.300E 00	1.437554E 01	4.556383E 00	1.058881E 00	1.119820E 00	1.460383E 00	4.624282E 02	2.823205E 01				
3.500E 00	1.401764E 01	4.390700E 00	9.620339E-01	1.068946E 00	1.440750E 00	4.226713E 02	2.747976E 01				
3.700E 00	1.373363E 01	4.076776E 00	9.201004E-01	1.019981E 00	1.423681E 00	3.928230E 02	2.627128E 01				
3.900E 00	1.354158E 01	3.817233E 00	8.733159E-01	9.742348E-01	1.409647E 00	3.722392E 02	2.527351E 01				
4.100E 00	1.345332E 01	3.329844E 00	8.411664E-01	9.325248E-01	1.399069E 00	3.609206E 02	2.377681E 01				
4.300E 00	1.368738E 01	2.711690E 00	8.311271E-01	8.971496E-01	1.394891E 00	3.658064E 02	2.134046E 01				
4.500E 00	1.417242E 01	2.310931E 00	8.390389E-01	8.676931E-01	1.395502E 00	3.825293E 02	1.955307E 01				
4.700E 00	1.481030E 01	2.072187E 00	8.590419E-01	8.438749E-01	1.399014E 00	4.065710E 02	1.827111E 01				
4.900E 00	1.553995E 01	1.867687E 00	8.908954E-01	8.260412E-01	1.404469E 00	4.357131E 02	1.718912E 01				
5.100E 00	1.634368E 01	1.723042E 00	9.301783E-01	8.148101E-01	1.411462E 00	4.686992E 02	1.606360E 01				
5.300E 00	1.717128E 01	1.599253E 00	9.745478E-01	8.105129E-01	1.419387E 00	5.033017E 02	1.513620E 01				
5.500E 00	1.801031E 01	1.484681E 00	1.022307E 00	8.130874E-01	1.428143E 00	5.388437E 02	1.425574E 01				
5.700E 00	1.884997E 01	1.384394E 00	1.072205E 00	8.222963E-01	1.437617E 00	5.748288E 02	1.344764E 01				
5.900E 00	1.968277E 01	1.291954E 00	1.123281E 00	8.378880E-01	1.447939E 00	6.108969E 02	1.269692E 01				
6.100E 00	2.049144E 01	1.228874E 00	1.174774E 00	8.596280E-01	1.458876E 00	6.464921E 02	1.207107E 01				
6.300E 00	2.119755E 01	1.189536E 00	1.228977E 00	8.885185E-01	1.470701E 00	6.821128E 02	1.158526E 01				
6.500E 00	2.183905E 01	1.150779E 00	1.285259E 00	9.251933E-01	1.483353E 00	7.177302E 02	1.112270E 01				
6.700E 00	2.250465E 01	1.082220E 00	1.341917E 00	9.700326E-01	1.497901E 00	7.538215E 02	1.056918E 01				
6.900E 00	2.322735E 01	1.019817E 00	1.396856E 00	1.022923E 00	1.513849E 00	7.896608E 02	1.004597E 01				
7.100E 00	2.395504E 01	9.704108E-01	1.448937E 00	1.082727E 00	1.530412E 00	8.239013E 02	9.598104E 00				
7.300E 00	2.468923E 01	9.322713E-01	1.496386E 00	1.146105E 00	1.547220E 00	8.545656E 02	9.240094E 00				
7.500E 00	2.520295E 01	8.962508E-01	1.537965E 00	1.210699E 00	1.563702E 00	8.814841E 02	8.925451E 00				
7.700E 00	2.576503E 01	8.578124E-01	1.572422E 00	1.273592E 00	1.579388E 00	9.045947E 02	8.635418E 00				
7.900E 00	2.630481E 01	8.219028E-01	1.599496E 00	1.332328E 00	1.593823E 00	9.238996E 02	8.382357E 00				
8.100E 00	2.680415E 01	7.943151E-01	1.620313E 00	1.385807E 00	1.606775E 00	9.396242E 02	8.182577E 00				
8.300E 00	2.720849E 01	7.737820E-01	1.636658E 00	1.432820E 00	1.617924E 00	9.518684E 02	8.046967E 00				
8.500E 00	2.755261E 01	7.542419E-01	1.648808E 00	1.473252E 00	1.627419E 00	9.614680E 02	7.911004E 00				
8.700E 00	2.788011E 01	7.310791E-01	1.656970E 00	1.507359E 00	1.635447E 00	9.692009E 02	7.784184E 00				
8.900E 00	2.820671E 01	7.089421E-01	1.661816E 00	1.535765E 00	1.642155E 00	9.754226E 02	7.669262E 00				
9.100E 00	2.851008E 01	6.937963E-01	1.664573E 00	1.559124E 00	1.647620E 00	9.801970E 02	7.585566E 00				
9.300E 00	2.872229E 01	6.818618E-01	1.667020E 00	1.577220E 00	1.651710E 00	9.836370E 02	7.537553E 00				
9.500E 00	2.889363E 01	6.768285E-01	1.668854E 00	1.591146E 00	1.654436E 00	9.858049E 02	7.495870E 00				
9.700E 00	2.896324E 01	6.805206E-01	1.670293E 00	1.601421E 00	1.657026E 00	9.870241E 02	7.500272E 00				
9.900E 00	2.896925E 01	6.843403E-01	1.672302E 00	1.608818E 00	1.658485E 00	9.876186E 02	7.511672E 00				
1.010E 01	2.892838E 01	6.933997E-01	1.674139E 00	1.613484E 00	1.659418E 00	9.876772E 02	7.541148E 00				
1.030E 01	2.880545E 01	7.074911E-01	1.676644E 00	1.616203E 00	1.659796E 00	9.871430E 02	7.595902E 00				
1.050E 01	2.864084E 01	7.222366E-01	1.679241E 00	1.617409E 00	1.659843E 00	9.863461E 02	7.653896E 00				
1.070E 01	2.839042E 01	7.323518E-01	1.682294E 00	1.617254E 00	1.659478E 00	9.848112E 02	7.767530E 00				
1.090E 01	2.805987E 01	7.447136E-01	1.686124E 00	1.615953E 00	1.658771E 00	9.828852E 02	7.895324E 00				
1.110E 01	2.769102E 01	7.522095E-01	1.690109E 00	1.613769E 00	1.657815E 00	9.805578E 02	8.045884E 00				
1.130E 01	2.725491E 01	7.666775E-01	1.694508E 00	1.610675E 00	1.656590E 00	9.776616E 02	8.228958E 00				
1.150E 01	2.678463E 01	7.846137E-01	1.698995E 00	1.606976E 00	1.655551E 00	9.743376E 02	8.431551E 00				



DYSIMP SIMULATION PROGRAM		POND TEN SUBMODEL RESPONSE										PAGE 3 OF RUN 1	
TIME	Y(12)	Y(1)	Y(2)	Y(3)	Y(4)	Y(5)	Y(6)	Y(7)	Y(8)	Y(9)	Y(10)	Y(11)	
1.170E 01	2.0241023E 01	9.0380560E 00	1.7034618E 00	1.6019220E 00	1.6531820E 00	9.7000024E 02	8.7186700E 00						
1.190E 01	2.5619598E 01	1.0014204E 00	1.7080812E 00	1.5960913E 00	1.6009256E 00	9.6479395E 02	9.0553196E 00						
1.210E 01	2.4929825E 01	1.1719275E 00	1.7121048E 00	1.5892563E 00	1.6482420E 00	9.5027637E 02	9.5118628E 00						
1.230E 01	2.4061493E 01	1.3201742E 00	1.7155094E 00	1.5814848E 00	1.6450186E 00	9.4998808E 02	1.0184430E 00						
1.250E 01	2.3092270E 01	1.5073195E 00	1.7176867E 00	1.5729416E 00	1.6413296E 00	9.4012109E 02	1.1044268E 00						
1.270E 01	2.2167984E 01	1.6778851E 00	1.7182913E 00	1.5638688E 00	1.6373701E 00	9.2950349E 02	1.1910647E 01						
1.290E 01	2.1319360E 01	1.8901777E 00	1.7181722E 00	1.5542002E 00	1.6330938E 00	9.1744800E 02	1.2971491E 01						
1.310E 01	2.0505737E 01	2.1218100E 00	1.7111855E 00	1.5439110E 00	1.6264752E 00	9.0395447E 02	1.4186135E 01						
1.330E 01	1.9809184E 01	2.3949109E 00	1.7026510E 00	1.5325670E 00	1.6233797E 00	8.8871680E 02	1.5446687E 01						
1.350E 01	1.9150070E 01	2.6412201E 00	1.6893599E 00	1.5198526E 00	1.6176205E 00	8.7060444E 02	1.7029800E 01						
1.370E 01	1.8522476E 01	2.9554367E 00	1.6702490E 00	1.5058665E 00	1.6110554E 00	8.4983081E 02	1.8813090E 01						
1.390E 01	1.7915878E 01	3.3450595E 00	1.6434412E 00	1.4888811E 00	1.6034050E 00	8.2466162E 02	2.1007525E 01						
1.410E 01	1.7320374E 01	3.7650832E 00	1.6066561E 00	1.4694338E 00	1.5943279E 00	7.9422412E 02	2.3488255E 01						
1.430E 01	1.6794159E 01	4.1999751E 00	1.5553889E 00	1.4448709E 00	1.5829000E 00	7.5610840E 02	2.5746231E 01						
1.450E 01	1.6273051E 01	4.5827524E 00	1.4485284E 00	1.4132137E 00	1.5682325E 00	7.0805518E 02	2.8155475E 01						
1.470E 01	1.5746707E 01	4.9425243E 00	1.3967056E 00	1.3732605E 00	1.5501032E 00	6.5178174E 02	2.9413345E 01						
1.490E 01	1.5228012E 01	4.9038744E 00	1.2943535E 00	1.3241405E 00	1.5265769E 00	5.9036328E 02	2.9949066E 01						
1.510E 01	1.4865914E 01	4.8443317E 00	1.1847353E 00	1.2660303E 00	1.5041809E 00	5.2784497E 02	2.9698883E 01						
1.530E 01	1.4461174E 01	4.6401072E 00	1.0872278E 00	1.2062111E 00	1.4806910E 00	4.7528662E 02	2.8630015E 01						
1.550E 01	1.4095145E 01	4.4585714E 00	1.0044060E 00	1.1490537E 00	1.4589329E 00	4.3254565E 02	2.7781357E 01						
1.570E 01	1.3803738E 01	4.1282110E 00	9.3779474E 01	1.0905190E 00	1.4399290E 00	4.0044434E 02	2.6475525E 01						
1.590E 01	1.3604836E 01	3.8570747E 00	8.8743758E 01	1.0379419E 00	1.4241657E 00	3.7814702E 02	2.5410019E 01						
1.610E 01	1.3510588E 01	3.5002467E 00	8.5253596E 01	9.9008983E 01	1.4120512E 00	3.5656549E 02	2.3649182E 01						
1.630E 01	1.3741886E 01	2.7356386E 00	8.4050689E 01	9.4917476E 01	1.4060507E 00	3.3974072E 02	2.1356873E 01						
1.650E 01	1.4224247E 01	2.3211479E 00	8.4692091E 01	9.1461742E 01	1.4058847E 00	3.2858908E 02	1.9544312E 01						
1.670E 01	1.4858524E 01	2.0796280E 00	8.6664587E 01	8.8605034E 01	1.4082775E 00	4.0949316E 02	1.8253632E 01						
1.690E 01	1.5583385E 01	1.8808889E 00	8.9674240E 01	8.6379117E 01	1.4127131E 00	4.3827979E 02	1.7098215E 01						
1.710E 01	1.6382019E 01	1.7254553E 00	9.3514812E 01	8.4844905E 01	1.4187784E 00	4.7096680E 02	1.6042969E 01						
1.730E 01	1.7204488E 01	1.6007662E 00	9.7887135E 01	8.4041733E 01	1.4258757E 00	5.0531372E 02	1.5116918E 01						
1.750E 01	1.8038818E 01	1.4656148E 00	1.0260878E 00	8.3961952E 01	1.4338923E 00	5.4063232E 02	1.4238344E 01						
1.770E 01	1.8874329E 01	1.3849649E 00	1.0755167E 00	8.4577394E 01	1.4427567E 00	5.7641724E 02	1.3432371E 01						
1.790E 01	1.9703506E 01	1.2922945E 00	1.1261806E 00	8.5859352E 01	1.4524279E 00	6.1230347E 02	1.2683758E 01						
1.810E 01	2.0509018E 01	1.2290907E 00	1.1773043E 00	8.7780166E 01	1.4628210E 00	6.4772998E 02	1.2059420E 01						
1.830E 01	2.1212173E 01	1.1896448E 00	1.2311573E 00	9.0425116E 01	1.4741249E 00	6.8318652E 02	1.1576032E 01						
1.850E 01	2.1851028E 01	1.1508207E 00	1.2871084E 00	9.3858439E 01	1.4865179E 00	7.1864404E 02	1.1115201E 01						
1.870E 01	2.2514404E 01	1.0822334E 00	1.3434544E 00	9.8122126E 01	1.5003576E 00	7.5465374E 02	1.0563525E 01						
1.890E 01	2.3235214E 01	1.0198098E 00	1.3981447E 00	1.0320826E 00	1.5156717E 00	7.9028125E 02	1.0004097E 01						
1.910E 01	2.3961288E 01	9.7040427E 01	1.4499245E 00	1.0900545E 00	1.5320435E 00	8.2439258E 02	9.5946293E 00						
1.930E 01	2.4614059E 01	9.3226641E 01	1.4971466E 00	1.1518631E 00	1.5485106E 00	8.5494531E 02	9.2374878E 00						
1.950E 01	2.5206589E 01	8.9625174E 01	1.5385408E 00	1.2151308E 00	1.5647049E 00	8.8177026E 02	8.9239055E 00						
1.970E 01	2.5767731E 01	8.5780549E 01	1.5728464E 00	1.2769442E 00	1.5801535E 00	9.0480591E 02	8.6340421E 00						
1.990E 01	2.6306793E 01	8.2189459E 01	1.5998039E 00	1.3348293E 00	1.5944004E 00	9.2405249E 02	8.3814329E 00						
2.010E 01	2.6805588E 01	7.9431087E 01	1.6205311E 00	1.3876457E 00	1.6072044E 00	9.3973145E 02	8.1819449E 00						
2.030E 01	2.7209518E 01	7.7377838E 01	1.6368103E 00	1.4341545E 00	1.6182394E 00	9.5194409E 02	8.0365141E 00						
2.050E 01	2.7553314E 01	7.5424159E 01	1.6489124E 00	1.4742069E 00	1.6276464E 00	9.6151978E 02	7.9107141E 00						
2.070E 01	2.7886000E 01	7.3108101E 01	1.6570406E 00	1.5080347E 00	1.6356096E 00	9.6923584E 02	7.7839870E 00						
2.090E 01	2.8207031E 01	7.0894057E 01	1.6618643E 00	1.5362377E 00	1.6422710E 00	9.7544580E 02	7.6691300E 00						
2.110E 01	2.8510300E 01	6.9279634E 01	1.6646051E 00	1.5594530E 00	1.6477013E 00	9.8021240E 02	7.5854810E 00						
2.130E 01	2.8722362E 01	6.8818060E 01	1.6670418E 00	1.5774508E 00	1.6517677E 00	9.8344727E 02	7.5379219E 00						
2.150E 01	2.8883372E 01	6.7882803E 01	1.6686687E 00	1.5913086E 00	1.6548767E 00	9.8581079E 02	7.4959180E 00						
2.170E 01	2.8966400E 01	6.8051666E 01	1.6703033E 00	1.6015368E 00	1.6570559E 00	9.8702905E 02	7.5002480E 00						
2.190E 01	2.8965971E 01	6.8433976E 01	1.6723089E 00	1.6087027E 00	1.6585064E 00	9.8762183E 02	7.5116549E 00						
2.210E 01	2.8928268E 01	6.9339949E 01	1.6741638E 00	1.6135454E 00	1.6594334E 00	9.8767969E 02	7.5410980E 00						
2.230E 01	2.8805406E 01	7.0749038E 01	1.6766481E 00	1.6162500E 00	1.6598120E 00	9.8714478E 02	7.5958920E 00						
2.250E 01	2.8640900E 01	7.2223008E 01	1.6792440E 00	1.6174412E 00	1.6598539E 00	9.8634766E 02	7.6538868E 00						
2.270E 01	2.8496057E 01	7.5234926E 01	1.6822508E 00	1.6172938E 00	1.6594858E 00	9.8481226E 02	7.7675209E 00						
2.290E 01	2.8065918E 01	7.8427100E 01	1.6861296E 00	1.6159773E 00	1.6587782E 00	9.8288623E 02	7.8953409E 00						

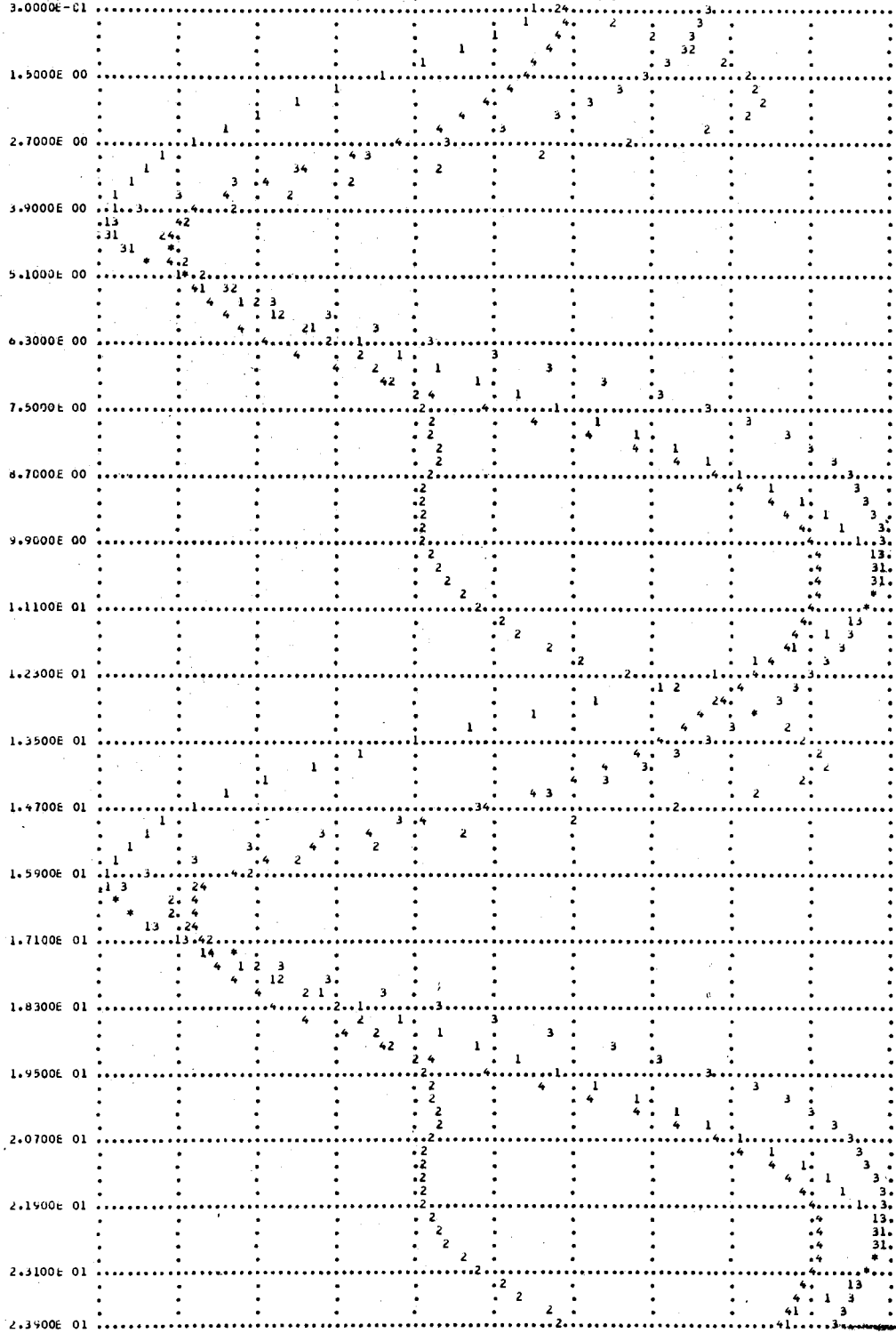
DYSIMP SIMULATION PROGRAM		POND TEN SUBMODEL RESPONSE										PAGE 4 OF RUN 1	
TIME	Y(12)	Y(1)	Y(2)	Y(3)	Y(4)	Y(5)	Y(6)	Y(7)	Y(8)	Y(9)	Y(10)	Y(11)	
2.310E 01	2.7691040E 01	8.2230365E 01	1.6901102E 00	1.6137905E 00	1.6578207E 00	9.8055884E 02	8.0458689E 00						
2.330E 01	2.7254944E 01	8.6646771E 01	1.6945095E 00	1.6106930E 00	1.6565638E 00	9.7768237E 02	8.2289753E 00						
2.350E 01	2.6784668E 01	9.1460359E 01	1.6989965E 00	1.6087829E 00	1.6550570E 00	9.7433838E 02	8.4315346E 00						
2.370E 01	2.6241669E 01	9.8379529E 01	1.7034626E 00	1.6019354E 00	1.6531858E 00	9.7000098E 02	8.7186700E 00						
2.390E 01	2.5619598E 01	1.0614204E 00	1.7080812E 00	1.5961027E 00	1.6509256E 00	9.6479466E 02	9.0553064E 00						

DYSIMP SIMULATION PROGRAM

POND TEN SUBMODEL RESPONSE

PAGE 5 OF RUN 1

Y( 1) = 8.605E 00      SYMBOL = 1,      SCALE FACTOR = 8.000E-01      Y( 1) = 1.660E 01  
 Y( 4) = 1.684E 01      SYMBOL = 2,      SCALE FACTOR = 4.000E 00      Y( 4) = 5.884E 01  
 Y( 5) = 1.595E 00      SYMBOL = 3,      SCALE FACTOR = 3.000E-01      Y( 5) = 4.955E 00  
 Y( 9) = 7.091E 00      SYMBOL = 4,      SCALE FACTOR = 4.000E-01      Y( 9) = 1.109E 01  
 TIME                      SYMBOL = \*,      FOR COINCIDENT POINTS



## APPENDIX B

### POND SERIES SIMULATION RESULTS

The program listing and computer output for the pond series model simulation are presented here. As in Appendix A, the listing includes the DYSIMP user deck and the necessary data. Two simulation runs were required to output all twenty-eight states, since the DYSIMP package allows a maximum of ten printed and ten plotted outputs.

80/80 LIST

00000000111111111122222222223333333333444444444455555555556666666666777777777788888888889999999999  
1234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890

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CARC
1
2
3      DYSIMP USER DELC
4
5
6      COMMON/ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NK,NW
7      COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
8      READ (NR,2000) M
9      DO 2002 I=1,M
10     READ(NR,2001) T(I),WT4(I),WT7(I),WT10(I),SOL(I)
11     WT4(I)=(WT4(I)-32.0)*(5.0/9.0)
12     WT7(I)=(WT7(I)-32.0)*(5.0/9.0)
13     2002 WT10(I)=(WT10(I)-32.0)*(5.0/9.0)
14     IER=0
15     IXVAL=1
16     CALL DYSIMP(IXVAL,IER)
17     2000 FORMAT(15)
18     2001 FORMAT(5F10.0)
19     STOP
20     END
21
22     FUNCTION W4(TIME)
23     COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
24     DO 1 J=2,M
25     IF(TIME.LT.T(1)) GO TO 2
26     IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
27     1 CONTINUE
28     IF(TIME.GE.T(M)) W4=WT4(M)
29     RETURN
30     2 W4=WT4(1)
31     RETURN
32     3 W4=WT4(J-1)+(TIME-T(J-1))*(WT4(J)-WT4(J-1))/(T(J)-T(J-1))
33     RETURN
34     END
35     FUNCTION W7(TIME)
36     COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
37     DO 1 J=2,M
38     IF(TIME.LT.T(1)) GO TO 2
39     IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
40     1 CONTINUE
41     IF(TIME.GE.T(M)) W7=WT7(M)
42     RETURN
43     2 W7=WT7(1)
44     RETURN
45     3 W7=WT7(J-1)+(TIME-T(J-1))*(WT7(J)-WT7(J-1))/(T(J)-T(J-1))
46     RETURN
47     END
48     FUNCTION W10(TIME)
49     COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
50     DO 1 J=2,M
51     IF(TIME.LT.T(1)) GO TO 2
52     IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
53     1 CONTINUE
54     IF(TIME.GE.T(M)) W10=WT10(M)

```

80/80 LIST

00000000111111111122222222223333333333444444444455555555556666666666777777777788888888889999999999  
1234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890

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LARU
55     RETURN
56     2 W10=WT10(1)
57     RETURN
58     3 W10=WT10(J-1)+(TIME-T(J-1))*(WT10(J)-WT10(J-1))/(T(J)-T(J-1))
59     RETURN
60     END
61     FUNCTION SOL1(TIME)
62     COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
63     DO 1 J=2,M
64     IF(TIME.LT.T(1)) GO TO 2
65     IF(TIME.GE.T(J-1).AND.TIME.LE.T(J)) GO TO 3
66     1 CONTINUE
67     IF(TIME.GE.T(M)) SOL1=SOL(M)
68     RETURN
69     2 SOL1=SOL(1)
70     RETURN
71     3 SOL1=SOL(J-1)+(TIME-T(J-1))*(SOL(J)-SOL(J-1))/(T(J)-T(J-1))
72     RETURN
73     END
74
75     SUBROUTINE DERFUN
76     COMMON/ALL/Y(92),X(50),P(50),NY,NYP1,NYP2,NYMAX,NX,NK,NW
77     COMMON/MEAS/T(100),WT4(100),WT7(100),WT10(100),SOL(100),M
78     DIMENSION YINPUT(45),F(45)
79     EQUIVALENCE(YINPUT(1),F(1))
80     F(1)=-1.5369*Y(1)+.00679*Y(7)+.00906*Y(7)-.01208*Y(1)*Y(4)-12.87)
81     F(2)=-1.75000*Y(2)+.00679*Y(7)-.00508*Y(2)*Y(4)+.13415*Y(7)
82     F(3)=-112.7)
83     F(3)=-363.76581*Y(3)-7.12668*Y(5)*Y(4)*X(2)+.35681*Y(3)*Y(7)
84     F(4)=-21.41437*Y(4)+.06568*Y(2)*Y(4)+7.12668*Y(3)*Y(4)*X(24)
85     F(5)=-2.73737*Y(5)-.15021*Y(3)*Y(5)+.00199*Y(4)+.00172*Y(7)
86     F(6)=-1.16605*Y(5)*Y(8)-329)*X(21)
87     F(6)=-2.21+29*Y(6)+.05398*Y(4)-.17542*Y(3)*Y(6)+.13240*Y(6)
88     F(7)=-.00629*Y(7)-.00219*X(21)
89     F(7)=-.85308*Y(7)+21.24396*Y(4)-.00419*Y(7)*Y(2)-.35681*Y(3)*Y(7)
90     F(8)=-1.79798*Y(8)+.56713*Y(7)*Y(8)-.00029*Y(7)-.00036*Y(7)*Y(1)
91     F(8)=-1016.3)*X(21)
92     F(8)=-23.78049*Y(8)-.13240*Y(6)*Y(8)-.16605*Y(5)*Y(8)
93     F(9)=-21.2609*Y(4)*Y(8)-.36713*Y(7)*Y(8)+.1937.554)
94     IF(Y(NYP1)-P(5)) 9,2,2
95     X(2)=-.15369*2+.92*P(3)
96     X(4)=1.75*32.0*P(3)
97     X(6)=363.76581*.43*P(4)
98     X(8)=23.78049*.41*P(4)
99     F(9)=-1.15369*Y(9)+.009072*Y(16)+.00678*Y(16)-.01842*Y(9)*Y(12)
100    F(9)=-2.57*X(2)-X(25)
101    F(10)=-1.75185*Y(10)+.00678*Y(16)-.07762*Y(10)*Y(12)+.13568
102    F(10)=-24.77*X(4)-X(26)
103    F(11)=-201.46714*Y(11)+.05925*Y(11)*Y(15)
104    F(11)=-19.55779*Y(11)*Y(12)*X(24)
105    F(12)=-.73000*Y(11)*Y(16)+.35948*Y(11)*Y(14)+.32125*Y(11)*Y(13)+X(6)
106    F(12)=-1*X(27)
107
108

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DYSLMP SIMULATION PROGRAM

SERIES POND MODEL RESPONSE

ORDER OF SYSTEM = 20
NUMBER OF PDS = 32
NUMBER OF PARAMETERS = 8
NUMBER OF DELAYS = 8
OUTPUT INTERVAL = 40
INITIAL TIME = 3.0000E-01
FINAL TIME = 1.2300E 01
INTEGRATION STEP = 2.5000E-03

INITIAL Y VALUES

Y( 1) = 2.492000E 01 Y( 2) = 3.200000E 01 Y( 3) = 4.299999E 00 Y( 4) = 3.520999E 01 Y( 5) = 9.899999E-01
Y( 6) = 7.000000E-01 Y( 7) = 1.722000E 03 Y( 8) = 4.099999E 00 Y( 9) = 1.025000E 01 Y(10) = 2.700000E 01
Y(11) = 2.099999E 00 Y(12) = 4.742555E 01 Y(13) = 3.349999E 00 Y(14) = 1.020000E 00 Y(15) = 4.100000E-01
Y(16) = 1.219000E 03 Y(17) = 1.100000E 01 Y(18) = 1.300000E 01 Y(19) = 2.296999E 01 Y(20) = 1.299999E 00
Y(21) = 4.000000E 01 Y(22) = 3.870000E 00 Y(23) = 1.629999E 00 Y(24) = 1.400000E 00 Y(25) = 1.599999E 00
Y(26) = 9.450000E 00 Y(27) = 8.840000E 02 Y(28) = 1.055000E 01

INITIAL X VALUES

X( 1) = 1.148985E 00 X( 2) = 1.148985E 00 X( 3) = 1.679999E 01 X( 4) = 1.679999E 01 X( 5) = 7.820963E 01
X( 6) = 7.820963E 01 X( 7) = 4.874998E 00 X( 8) = 4.874998E 00 X( 9) = 7.451433E-01 X(10) = 7.500182E-01
X(11) = 1.418998E 01 X(12) = 1.418998E 01 X(13) = 2.115404E 01 X(14) = 2.115404E 01 X(15) = 1.304999E 01
X(16) = 1.304999E 01 X(17) = 1.044444E 01 X(18) = 8.944445E 00 X(19) = 9.111113E 00 X(20) = 5.042000E 02
X(21) = 5.890023E-01 X(22) = 5.897395E-01 X(23) = 6.190390E-01 X(24) = 9.909770E-01 X(25) = 1.148985E 00
X(26) = 1.679999E 01 X(27) = 7.820963E 01 X(28) = 4.874998E 00 X(29) = 7.500182E-01 X(30) = 1.418998E 01

PARAMETER VALUES

P( 1) = 0.0 P( 2) = 0.0 P( 3) = 3.000000E-01 P( 4) = 5.000000E-02 P( 5) = 3.900000E-01
P( 6) = 4.800000E-01

TIME DELAYS

F( 1) = 8.999997E-02 F( 2) = 8.999997E-02 F( 3) = 8.999997E-02 F( 4) = 8.999997E-02 F( 5) = 8.999997E-02
F( 6) = 8.999997E-02 F( 7) = 8.999997E-02 F( 8) = 8.999997E-02

DYSLMP SIMULATION PROGRAM

SERIES POND MODEL RESPONSE

Table with 25 columns (Y(1) to Y(25)) and 25 rows of numerical data representing simulation results.

DYSIMP SIMULATION PROGRAM			SERIES POND MODEL RESPONSE								PAGE 3 OF RUN 1	
TIME	Y(1)	Y(3)	Y(11)	Y(20)	Y(8)	Y(17)	Y(28)	Y(24)	Y(26)			
0.000E 00	4.0000759E 00	1.9633353E 00	1.2521001E 00	4.2047921E 00	1.2239904E 01	1.2357334E 01	6.4094214E-01	7.7835026E 00				
0.100E 00	4.9913998E 00	1.9384575E 00	1.2312212E 00	4.1759882E 00	1.2018198E 01	1.2071631E 01	8.529903E-01	7.6304415E 00				
0.200E 00	3.9737234E 00	1.9150734E 00	1.2106857E 00	4.1443262E 00	1.1819251E 01	1.1818307E 01	8.669066E-01	7.8815365E 00				
0.300E 00	3.9476185E 00	1.8995216E 00	1.1895275E 00	4.1124249E 00	1.1624558E 01	1.1571918E 01	8.8273793E-01	7.9372215E 00				
0.400E 00	3.9221630E 00	1.8864249E 00	1.1690445E 00	4.0802927E 00	1.1433048E 01	1.1331736E 01	9.0053099E-01	7.9977369E 00				
0.500E 00	3.8948793E 00	1.8734953E 00	1.1487770E 00	4.0483418E 00	1.1246683E 01	1.1098604E 01	9.2024750E-01	8.0632992E 00				
0.600E 00	3.8227444E 00	1.7875652E 00	1.1123009E 00	4.0070820E 00	1.1016395E 01	1.0818480E 01	9.4212013E-01	8.1350660E 00				
0.700E 00	3.7618675E 00	1.7388430E 00	1.0777512E 00	3.9632540E 00	1.0773860E 01	1.0532953E 01	9.6600354E-01	8.2133646E 00				
0.800E 00	3.6990499E 00	1.6922808E 00	1.0449619E 00	3.9184551E 00	1.0538598E 01	1.0259141E 01	9.9188113E-01	8.2982302E 00				
0.900E 00	3.6377954E 00	1.6473799E 00	1.0134001E 00	3.8728476E 00	1.0308772E 01	9.9981232E 00	1.0196543E 00	8.3896790E 00				
1.000E 00	3.5774164E 00	1.6038427E 00	9.8317993E-01	3.8265390E 00	1.0086119E 01	9.7501116E 00	1.0491848E 00	8.4876108E 00				
1.100E 00	3.5403738E 00	1.5746880E 00	9.6236402E-01	3.7861300E 00	9.8992138E 00	9.5445518E 00	1.0799875E 00	8.5903273E 00				
1.200E 00	3.5004988E 00	1.5460157E 00	9.4260991E-01	3.7472115E 00	9.7297583E 00	9.3590221E 00	1.1115389E 00	8.6963129E 00				
1.300E 00	3.4598789E 00	1.5176926E 00	9.2307544E-01	3.7094927E 00	9.5701513E 00	9.1858768E 00	1.1435709E 00	8.8050117E 00				
1.400E 00	3.4188862E 00	1.4899101E 00	9.0428656E-01	3.6728573E 00	9.4199905E 00	9.0238800E 00	1.1758127E 00	8.9157829E 00				
1.500E 00	3.3777151E 00	1.4627123E 00	8.8605642E-01	3.6372414E 00	9.2787886E 00	8.8726444E 00	1.2079647E 00	9.0279388E 00				
1.600E 00	3.3294616E 00	1.4323959E 00	8.6592275E-01	3.6008663E 00	9.1386957E 00	8.7238216E 00	1.2396336E 00	9.1402216E 00				
1.700E 00	3.2821236E 00	1.4025707E 00	8.4660077E-01	3.5652819E 00	9.0056744E 00	8.5836954E 00	1.2703075E 00	9.2512684E 00				
1.800E 00	3.2352524E 00	1.3736620E 00	8.2789099E-01	3.5306120E 00	8.8808308E 00	8.4534950E 00	1.2998505E 00	9.3605556E 00				
1.900E 00	3.1889410E 00	1.3455582E 00	8.0978465E-01	3.496819E 00	8.7635822E 00	8.3324404E 00	1.3281137E 00	9.4676199E 00				
2.000E 00	3.1432400E 00	1.3181753E 00	7.9225910E-01	3.4639788E 00	8.653343E 00	8.2197437E 00	1.3550339E 00	9.5725010E 00				
2.100E 00	3.1166392E 00	1.3011971E 00	7.8146303E-01	3.4369946E 00	8.5692129E 00	8.1352367E 00	1.380064E 00	9.6724815E 00				
2.200E 00	3.0889511E 00	1.2848787E 00	7.7077222E-01	3.4119358E 00	8.4956493E 00	8.0618360E 00	1.4040348E 00	9.7660349E 00				
2.300E 00	3.0612717E 00	1.2683411E 00	7.6027554E-01	3.3880100E 00	8.4269753E 00	7.9935741E 00	1.4259968E 00	9.8588625E 00				
2.400E 00	3.0338259E 00	1.2523785E 00	7.5011533E-01	3.3652010E 00	8.3625231E 00	7.9302235E 00	1.4462547E 00	9.9439983E 00				
2.500E 00	3.0065794E 00	1.2365904E 00	7.4015015E-01	3.3433828E 00	8.3020000E 00	7.8710880E 00	1.4648743E 00	1.0024366E 01				
2.600E 00	2.9792324E 00	1.2172861E 00	7.2811568E-01	3.3204994E 00	8.2374773E 00	7.8079405E 00	1.4818974E 00	1.0099938E 01				
2.700E 00	2.9391651E 00	1.1984949E 00	7.1632928E-01	3.2981596E 00	8.1741800E 00	7.7467518E 00	1.4973860E 00	1.0170638E 01				
2.800E 00	2.9063177E 00	1.1799574E 00	7.0478302E-01	3.2764750E 00	8.1139307E 00	7.6888113E 00	1.5114355E 00	1.0236980E 01				
2.900E 00	2.8739471E 00	1.1617861E 00	6.9349527E-01	3.2554054E 00	8.0562487E 00	7.6337767E 00	1.5242243E 00	1.0299181E 01				
3.000E 00	2.8420391E 00	1.1439400E 00	6.8244106E-01	3.2349119E 00	8.0009775E 00	7.5813961E 00	1.5358073E 00	1.0357520E 01				
3.100E 00	2.8302641E 00	1.1368103E 00	6.7773896E-01	3.2208328E 00	7.9679270E 00	7.5521231E 00	1.5460739E 00	1.0410614E 01				
3.200E 00	2.8169012E 00	1.1291494E 00	6.7317826E-01	3.2085876E 00	7.9424299E 00	7.5290799E 00	1.5550079E 00	1.0457775E 01				
3.300E 00	2.8039608E 00	1.1220045E 00	6.6877878E-01	3.1975317E 00	7.9182339E 00	7.5073366E 00	1.5627842E 00	1.0499699E 01				
3.400E 00	2.7911978E 00	1.1149073E 00	6.6438401E-01	3.1873741E 00	7.8955975E 00	7.4869156E 00	1.5695610E 00	1.0537026E 01				
3.500E 00	2.7785473E 00	1.1078568E 00	6.6004648E-01	3.1779346E 00	7.8740902E 00	7.4674149E 00	1.5754776E 00	1.0570362E 01				
3.600E 00	2.7654185E 00	1.1010793E 00	6.5619401E-01	3.1747313E 00	7.8527827E 00	7.4484868E 00	1.5805044E 00	1.0599046E 01				
3.700E 00	2.7505054E 00	1.1141634E 00	6.6380358E-01	3.1732500E 00	7.8774481E 00	7.4744778E 00	1.5846796E 00	1.0622810E 01				
3.800E 00	2.7362036E 00	1.1170349E 00	6.6551924E-01	3.1724036E 00	7.8832417E 00	7.4812689E 00	1.5881348E 00	1.0642473E 01				
3.900E 00	2.8020077E 00	1.1200886E 00	6.6748011E-01	3.1731768E 00	7.8896141E 00	7.4884253E 00	1.5909834E 00	1.0658600E 01				
4.000E 00	2.8079147E 00	1.1234579E 00	6.6952342E-01	3.1741314E 00	7.8965311E 00	7.4959183E 00	1.5933228E 00	1.0671733E 01				
4.100E 00	2.8301525E 00	1.1345978E 00	6.7686436E-01	3.1800585E 00	7.9201889E 00	7.5198793E 00	1.5951242E 00	1.0681437E 01				
4.200E 00	2.8511696E 00	1.1464090E 00	6.8389469E-01	3.1874542E 00	7.9484568E 00	7.5482874E 00	1.5964155E 00	1.0687753E 01				
4.300E 00	2.8728037E 00	1.1583350E 00	6.9132042E-01	3.1955128E 00	7.9776011E 00	7.5773325E 00	1.5972429E 00	1.0691290E 01				
4.400E 00	2.8949213E 00	1.1707563E 00	6.9878466E-01	3.2041788E 00	8.0078516E 00	7.6071463E 00	1.5978317E 00	1.0692537E 01				
4.500E 00	2.9173651E 00	1.1831923E 00	7.0639837E-01	3.2133039E 00	8.0386942E 00	7.6375389E 00	1.598069E 00	1.0691912E 01				
4.600E 00	2.9402607E 00	1.1958476E 00	7.1423351E-01	3.2239199E 00	8.0943098E 00	7.6926165E 00	1.5980349E 00	1.0688886E 01				
4.700E 00	2.9636384E 00	1.2083268E 00	7.2265389E-01	3.2495300E 00	8.1559410E 00	7.7547054E 00	1.5976648E 00	1.0683475E 01				
4.800E 00	2.9874295E 00	1.2209730E 00	7.3126515E-01	3.2858157E 00	8.2211962E 00	7.8195801E 00	1.5970335E 00	1.0676044E 01				
4.900E 00	3.0113392E 00	1.2338620E 00	7.4013874E-01	3.28257380E 00	8.2900524E 00	7.8861427E 00	1.5961838E 00	1.0666938E 01				
5.000E 00	3.0352488E 00	1.2468304E 00	7.4878131E-01	3.3066330E 00	8.3594370E 00	7.9552908E 00	1.5951519E 00	1.0654300E 01				
5.100E 00	3.0591481E 00	1.2597861E 00	7.5749025E-01	3.3317595E 00	8.4448843E 00	8.0404549E 00	1.5939054E 00	1.0644217E 01				
5.200E 00	3.0830474E 00	1.2727433E 00	7.6617850E-01	3.3583021E 00	8.5366726E 00	8.1315746E 00	1.5924454E 00	1.0630259E 01				
5.300E 00	3.1069467E 00	1.2857006E 00	7.7492701E-01	3.3861990E 00	8.6331425E 00	8.2281284E 00	1.5907841E 00	1.0614681E 01				
5.400E 00	3.1308460E 00	1.2986579E 00	7.8367551E-01	3.4154186E 00	8.7337151E 00	8.3292646E 00	1.5889359E 00	1.0597615E 01				
5.500E 00	3.1547453E 00	1.3116152E 00	7.9242402E-01	3.4459152E 00	8.8393850E 00	8.4355049E 00	1.5869131E 00	1.0579190E 01				
5.600E 00	3.1786446E 00	1.3245725E 00	8.0117253E-01	3.4774118E 00	8.953532E 00	8.5474192E 00	1.5846558E 00	1.0558885E 01				

DYSIMP SIMULATION PROGRAM			SERIES POND MODEL RESPONSE								PAGE 4 OF RUN 1	
TIME	Y(1)	Y(3)	Y(11)	Y(20)	Y(8)	Y(17)	Y(28)	Y(24)	Y(26)			
1.170E 01	3.0763601E 00	1.6157742E 00	9.7528881E-01	3.5247316E 00	9.1270466E 00	8.7296314E 00	1.5821800E 00	1.0536659E 01				
1.180E 01	3.1777289E 00	1.6765041E 00	1.0135145E 00	3.5678043E 00	9.2895613E 00	8.8966637E 00	1.5794325E 00	1.0512607E 01				
1.190E 01	3.8853731E 00	1.7399368E 00	1.0542430E 00	3.6129904E 00	9.4628572E 00	9.0757856E 00	1.5764809E 00	1.0488828E 01				
1.200E 01	3.9972639E 00	1.8080786E 00	1.0979557E 00	3.6609012E 00	9.6484156E 00	9.2691975E 00	1.5733051E 00	1.0459361E 01				
1.210E 01	4.1818447E 00	1.9120235E 00	1.1681385E 00	3.7233782E 00	9.9106283E 00	9.5444469E 00	1.5698509E 00	1.0429724E 01				
1.220E 01	4.3533287E 00	2.0268412E 00	1.2399921E 00	3.7925940E 00	1.0216828E 01	9.8724289E 00	1.561793E 00	1.0394829E 01				
1.230E 01	4.5519886E 00	2.1532516E 00	1.3206511E 00	3.8651085E 00	1.0553557E 01	1.0240391E 01	1.5623150E 00	1.0365712E 01				



DYNSIMP SIMULATION PROGRAM

SERIES POND MODEL RESPONSE

LCRER CF SYSTEM = 24
NUMBER OF X'S = 32
NUMBER OF PARAMETERS = 6
NUMBER OF DELAYS = 8
OUTPUT INTERVAL = 40
INITIAL TIME = 3.0000E-01
FINAL TIME = 1.2300E 01
INTEGRATION STEP = 2.5000E-03

INITIAL Y VALUES

Y( 1) = 2.492000E 01 Y( 2) = 3.200000E 01 Y( 3) = 4.299999E 00 Y( 4) = 3.520999E 01 Y( 5) = 9.899999E-01
Y( 6) = 7.000000E-01 Y( 7) = 1.722000E 03 Y( 8) = 4.099999E 00 Y( 9) = 1.025000E 01 X(10) = 7.500182E-01
Y(11) = 2.099999E 00 Y(12) = 4.742999E 01 Y(13) = 3.349999E 00 Y(14) = 1.020000E 00 Y(15) = 4.100000E-01
Y(16) = 1.219000E 03 Y(17) = 1.100000E 01 Y(18) = 1.300000E 01 Y(19) = 2.296999E 01 Y(20) = 1.299999E 00
Y(21) = 4.000000E 01 Y(22) = 3.870000E 00 Y(23) = 1.629999E 00 Y(24) = 1.400000E 00 Y(25) = 1.599999E 00
Y(26) = 9.450000E 00 Y(27) = 8.840000E 02 Y(28) = 1.055000E 01

INITIAL X VALUES

X( 1) = 1.148985E 00 X( 2) = 1.148985E 00 X( 3) = 1.679999E 01 X( 4) = 1.679999E 01 X( 5) = 7.820963E 01
X( 6) = 7.820963E 01 X( 7) = 4.874998E 00 X( 8) = 4.874998E 00 X( 9) = 7.451433E-01 X(10) = 7.500182E-01
X(11) = 1.418998E 01 X(12) = 1.418998E 01 X(13) = 2.115404E 00 X(14) = 2.115404E 00 X(15) = 1.304999E 01
X(16) = 1.304999E 01 X(17) = 1.044444E 01 X(18) = 8.944444E 00 X(19) = 9.111113E 00 X(20) = 5.042000E 02
X(21) = 5.890023E-01 X(22) = 5.894759E-01 X(23) = 6.190390E-01 X(24) = 9.909770E-01 X(25) = 1.148985E 00
X(26) = 1.679999E 01 X(27) = 7.820963E 01 X(28) = 4.874998E 00 X(29) = 7.500182E-01 X(30) = 1.418998E 01
X(31) = 2.115404E 01 X(32) = 1.304999E 01

PARAMETER VALUES

P( 1) = 0.0 P( 2) = 0.0 P( 3) = 3.000000E-01 P( 4) = 5.000000E-02 P( 5) = 3.900000E-01
P( 6) = 4.800000E-01

TIME DELAYS

F( 1) = 8.999997E-02 F( 2) = 8.999997E-02 F( 3) = 8.999997E-02 F( 4) = 8.999997E-02 F( 5) = 8.999997E-02
F( 6) = 8.999997E-02 F( 7) = 8.999997E-02 F( 8) = 8.999997E-02

DYNSIMP SIMULATION PROGRAM

SERIES POND MODEL RESPONSE

Table with columns for TIME, Y(1-28), and X(1-32). It contains numerical data for 5.000E-01 to 5.500E 00, representing simulation results over time.

DYSDIP SIMULATION PROGRAM      SERIES POND MODEL RESPONSE      PAGE 3 OF RUN 1

TIME

Y(29)	Y( 2)	Y(10)	Y(19)	Y(15)	Y(25)	Y( 7)	Y(16)	Y(27)
0.00E 00	2.9441406E 01	2.3291718E 01	1.9339249E 01	2.8448361E-01	1.4500628E 00	1.5835767E 03	9.4072778E 02	6.2923926E 02
0.100E 00	2.9944916E 01	2.3867889E 01	1.9834213E 01	2.8579086E-01	1.4557781E 00	1.6041992E 03	9.6288013E 02	6.4699170E 02
0.200E 00	3.0414094E 01	2.4397566E 01	2.0293976E 01	2.8745264E-01	1.4617338E 00	1.6246099E 03	9.8486938E 02	6.6478735E 02
0.300E 00	3.0851563E 01	2.4891006E 01	2.0725861E 01	2.8949672E-01	1.4679518E 00	1.6449546E 03	1.0067278E 03	6.8262671E 02
0.400E 00	3.1270599E 01	2.5357086E 01	2.1145681E 01	2.9194272E-01	1.4744406E 00	1.6654528E 03	1.0285901E 03	7.0042407E 02
0.500E 00	3.1673920E 01	2.5801666E 01	2.1527557E 01	2.9480296E-01	1.4812012E 00	1.6854528E 03	1.0497415E 03	7.1810596E 02
0.600E 00	3.2083313E 01	2.6249878E 01	2.1920975E 01	2.9813874E-01	1.4888394E 00	1.7068247E 03	1.0717251E 03	7.3599511E 02
0.700E 00	3.2523102E 01	2.6725830E 01	2.2332092E 01	3.0199754E-01	1.4958658E 00	1.7296746E 03	1.0943301E 03	7.5290625E 02
0.800E 00	3.2987793E 01	2.7222763E 01	2.2755219E 01	3.0637074E-01	1.5037441E 00	1.7538066E 03	1.1173123E 03	7.7166797E 02
0.900E 00	3.3473770E 01	2.7734726E 01	2.3185730E 01	3.1124616E-01	1.5119362E 00	1.7790591E 03	1.1405220E 03	7.8916699E 02
1.000E 00	3.3977631E 01	2.8257004E 01	2.3619965E 01	3.1606223E-01	1.5204010E 00	1.8052778E 03	1.1637561E 03	8.0627930E 02
1.100E 00	3.4482330E 01	2.8770294E 01	2.4042953E 01	3.2229817E-01	1.5289574E 00	1.8311624E 03	1.1860217E 03	8.2251538E 02
1.200E 00	3.4969147E 01	2.9256332E 01	2.4442459E 01	3.2818848E-01	1.5374775E 00	1.8561230E 03	1.2069055E 03	8.3776733E 02
1.300E 00	3.5439926E 01	2.9718730E 01	2.4821716E 01	3.3422619E-01	1.5459309E 00	1.8802483E 03	1.2264758E 03	8.5205078E 02
1.400E 00	3.5896423E 01	3.0160950E 01	2.5183369E 01	3.4035385E-01	1.5542803E 00	1.9036067E 03	1.2447549E 03	8.6536279E 02
1.500E 00	3.6340149E 01	3.0585526E 01	2.5529373E 01	3.4650797E-01	1.5626847E 00	1.9262512E 03	1.2617751E 03	8.7770386E 02
1.600E 00	3.6777374E 01	3.0999817E 01	2.5865524E 01	3.5258245E-01	1.5706799E 00	1.9493477E 03	1.2776039E 03	8.8909399E 02
1.700E 00	3.7213318E 01	3.1409344E 01	2.6195831E 01	3.5846609E-01	1.5781422E 00	1.9698647E 03	1.2922051E 03	8.9946509E 02
1.800E 00	3.7646286E 01	3.1812546E 01	2.6519089E 01	3.6410272E-01	1.5854797E 00	1.9908215E 03	1.3056244E 03	9.0887012E 02
1.900E 00	3.8075272E 01	3.2208374E 01	2.6834671E 01	3.6944878E-01	1.5924606E 00	2.0112366E 03	1.3179622E 03	9.1737183E 02
2.000E 00	3.8499756E 01	3.2596527E 01	2.7142410E 01	3.7447125E-01	1.5990686E 00	2.0311257E 03	1.3292874E 03	9.2503394E 02
2.100E 00	3.8903671E 01	3.2960312E 01	2.7429398E 01	3.7913585E-01	1.6052160E 00	2.0498374E 03	1.3392493E 03	9.3167188E 02
2.200E 00	3.9273239E 01	3.3286911E 01	2.7686768E 01	3.8344914E-01	1.6108866E 00	2.0673296E 03	1.3481372E 03	9.3747168E 02
2.300E 00	3.9616684E 01	3.3585541E 01	2.7921494E 01	3.8742769E-01	1.6161108E 00	2.0837639E 03	1.3560383E 03	9.4255542E 02
2.400E 00	3.9939835E 01	3.3863388E 01	2.8138763E 01	3.9107794E-01	1.6209135E 00	2.0992485E 03	1.3631030E 03	9.4700928E 02
2.500E 00	4.0246933E 01	3.4125427E 01	2.8342407E 01	3.9440328E-01	1.6253166E 00	2.1138849E 03	1.3694365E 03	9.5091162E 02
2.600E 00	4.0547974E 01	3.4382278E 01	2.8540710E 01	3.9740139E-01	1.6293554E 00	2.1279746E 03	1.3752720E 03	9.5441455E 02
2.700E 00	4.0850723E 01	3.4641907E 01	2.8739517E 01	4.0006113E-01	1.6330442E 00	2.1415618E 03	1.3806433E 03	9.5751762E 02
2.800E 00	4.1153015E 01	3.4902328E 01	2.8937622E 01	4.0238690E-01	1.6364021E 00	2.1546836E 03	1.3855474E 03	9.6026074E 02
2.900E 00	4.1453629E 01	3.5162170E 01	2.9134277E 01	4.0439254E-01	1.6394520E 00	2.1673752E 03	1.3900667E 03	9.6268848E 02
3.000E 00	4.1751892E 01	3.5420624E 01	2.9329086E 01	4.0609682E-01	1.6422186E 00	2.1796682E 03	1.3942332E 03	9.6483936E 02
3.100E 00	4.2025940E 01	3.5656097E 01	2.9505783E 01	4.0749311E-01	1.6446218E 00	2.1905466E 03	1.3976006E 03	9.6647266E 02
3.200E 00	4.2257645E 01	3.5852020E 01	2.9653214E 01	4.0863281E-01	1.6466713E 00	2.1998926E 03	1.4003362E 03	9.6777954E 02
3.300E 00	4.2458435E 01	3.6019699E 01	2.9779617E 01	4.0958214E-01	1.6484413E 00	2.2080491E 03	1.4026519E 03	9.6886035E 02
3.400E 00	4.2636414E 01	3.6167496E 01	2.9890869E 01	4.1037846E-01	1.6499815E 00	2.2152759E 03	1.4046347E 03	9.6976514E 02
3.500E 00	4.2797455E 01	3.6301239E 01	2.9991211E 01	4.1104351E-01	1.6513290E 00	2.2217693E 03	1.4063745E 03	9.7053394E 02
3.600E 00	4.2923798E 01	3.6403599E 01	3.0067612E 01	4.1158617E-01	1.6524324E 00	2.2267378E 03	1.4074976E 03	9.7094751E 02
3.700E 00	4.3000870E 01	3.6461109E 01	3.0110992E 01	4.1204274E-01	1.6533117E 00	2.2302263E 03	1.4081892E 03	9.7119141E 02
3.800E 00	4.3043167E 01	3.6486954E 01	3.0130981E 01	4.1245431E-01	1.6540222E 00	2.2326011E 03	1.4086248E 03	9.7133643E 02
3.900E 00	4.3060649E 01	3.6491013E 01	3.0134521E 01	4.1283810E-01	1.6546011E 00	2.2341301E 03	1.4088733E 03	9.7140091E 02
4.000E 01	4.3060649E 01	3.6480026E 01	3.0126465E 01	4.1320121E-01	1.6550741E 00	2.2350076E 03	1.4089766E 03	9.7143140E 02
4.100E 01	4.3029205E 01	3.6441071E 01	3.0097137E 01	4.1352444E-01	1.6553974E 00	2.2347175E 03	1.4086504E 03	9.7122974E 02
4.200E 01	4.2956772E 01	3.6364212E 01	3.0039749E 01	4.1384751E-01	1.6555853E 00	2.2333818E 03	1.4080491E 03	9.7093701E 02
4.300E 01	4.2855957E 01	3.6260880E 01	2.9962662E 01	4.1416502E-01	1.6556749E 00	2.2313010E 03	1.4072894E 03	9.7059912E 02
4.400E 01	4.2735474E 01	3.6139450E 01	2.9871704E 01	4.1449058E-01	1.6556892E 00	2.2286621E 03	1.4063362E 03	9.7022827E 02
4.500E 01	4.2601242E 01	3.6003661E 01	2.9771042E 01	4.1482437E-01	1.6556444E 00	2.2256057E 03	1.4054146E 03	9.6983545E 02
4.600E 01	4.2432663E 01	3.5839493E 01	2.9645401E 01	4.1514933E-01	1.6554852E 00	2.2214089E 03	1.4039353E 03	9.6918140E 02
4.700E 01	4.2214035E 01	3.5625687E 01	2.9484238E 01	4.1547829E-01	1.6552210E 00	2.2161223E 03	1.4021829E 03	9.6842920E 02
4.800E 01	4.1961121E 01	3.5378540E 01	2.9298050E 01	4.1582537E-01	1.6548777E 00	2.2099272E 03	1.4002458E 03	9.6760767E 02
4.900E 01	4.1684357E 01	3.5109116E 01	2.9094360E 01	4.1619277E-01	1.6544743E 00	2.2029543E 03	1.3981140E 03	9.6673584E 02
5.000E 01	4.1390656E 01	3.4844783E 01	2.8878094E 01	4.1658038E-01	1.6540232E 00	2.1953040E 03	1.3958635E 03	9.6583057E 02
5.100E 01	4.1073995E 01	3.4518753E 01	2.8644531E 01	4.1697812E-01	1.6534948E 00	2.1866885E 03	1.3932442E 03	9.6474683E 02
5.200E 01	4.0727295E 01	3.4186447E 01	2.8394088E 01	4.1738707E-01	1.6528931E 00	2.1771794E 03	1.3904902E 03	9.6357174E 02
5.300E 01	4.0360916E 01	3.3835938E 01	2.8121735E 01	4.1780847E-01	1.6522555E 00	2.1668640E 03	1.3874934E 03	9.6230249E 02
5.400E 01	3.9979843E 01	3.3473099E 01	2.7842606E 01	4.1824067E-01	1.6514988E 00	2.1558035E 03	1.3843162E 03	9.6093604E 02
5.500E 01	3.9587769E 01	3.3101563E 01	2.7555847E 01	4.1868025E-01	1.6507177E 00	2.1440503E 03	1.3809590E 03	9.5947656E 02
5.600E 01	3.9167603E 01	3.2704025E 01	2.7248108E 01	4.1911608E-01	1.6498356E 00	2.1310422E 03	1.3770852E 03	9.5770068E 02

DYSDIP SIMULATION PROGRAM      SERIES POND MODEL RESPONSE      PAGE 4 OF RUN 1

TIME

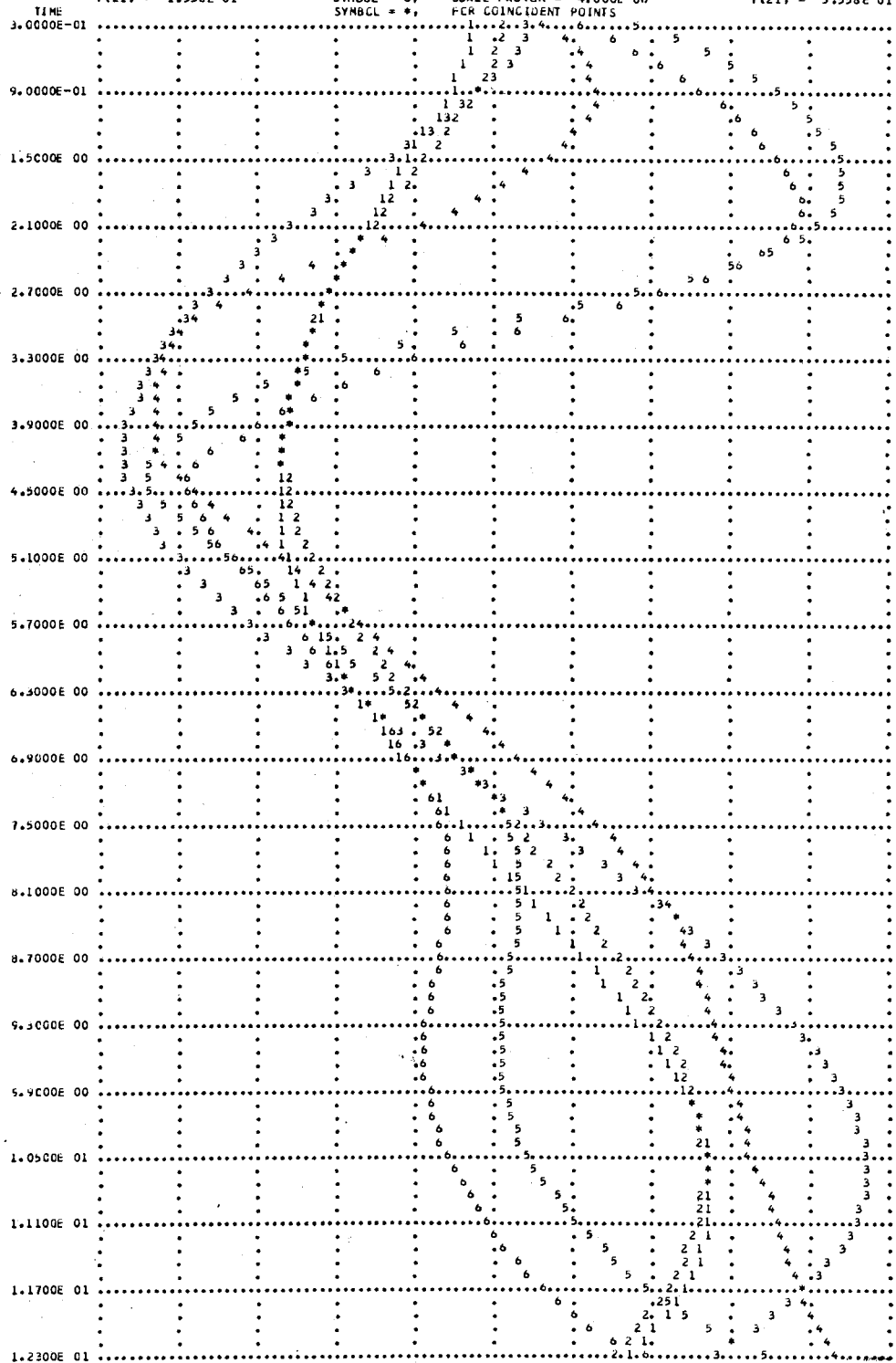
Y(29)	Y( 2)	Y(10)	Y(19)	Y(15)	Y(25)	Y( 7)	Y(16)	Y(27)
1.170E 01	3.8705826E 01	3.2267548E 01	2.6909897E 01	4.1955280E-01	1.6488523E 00	2.1159397E 03	1.3727683E 03	9.5572949E 02
1.180E 01	3.8215975E 01	3.1804504E 01	2.6550369E 01	4.1999495E-01	1.6477766E 00	2.1017766E 03	1.3680659E 03	9.5352494E 02
1.190E 01	3.7709917E 01	3.1323257E 01	2.6175476E 01	4.2044294E-01	1.6466141E 00	2.0856279E 03	1.3629902E 03	9.5121436E 02
1.200E 01	3.7181335E 01	3.0829376E 01	2.5789368E 01	4.2089438E-01	1.6453629E 00	2.0685383E 03	1.3575122E 03	9.4864000E 02
1.210E 01	3.6610764E 01	3.0289246E 01	2.5365494E 01	4.2131042E-01	1.6439571E 00	2.0497231E 03	1.3510496E 03	9.4545581E 02
1.220E 01	3.5967834E 01	2.9678223E 01	2.4885117E 01	4.2167747E-01	1.6424179E 00	2.0297268E 03	1.3439221E 03	9.4187329E 02
1.230E 01	3.5279709E 01	2.9020477E 01	2.4365707E 01	4.2200142E-01	1.6407652E 00	2.0087524E 03	1.3362649E 03	9.3795776E 02

UYSIMP SIMULATION PROGRAM

SERIES PUND MODEL RESPONSE

PAGE 5 OF RUN 1

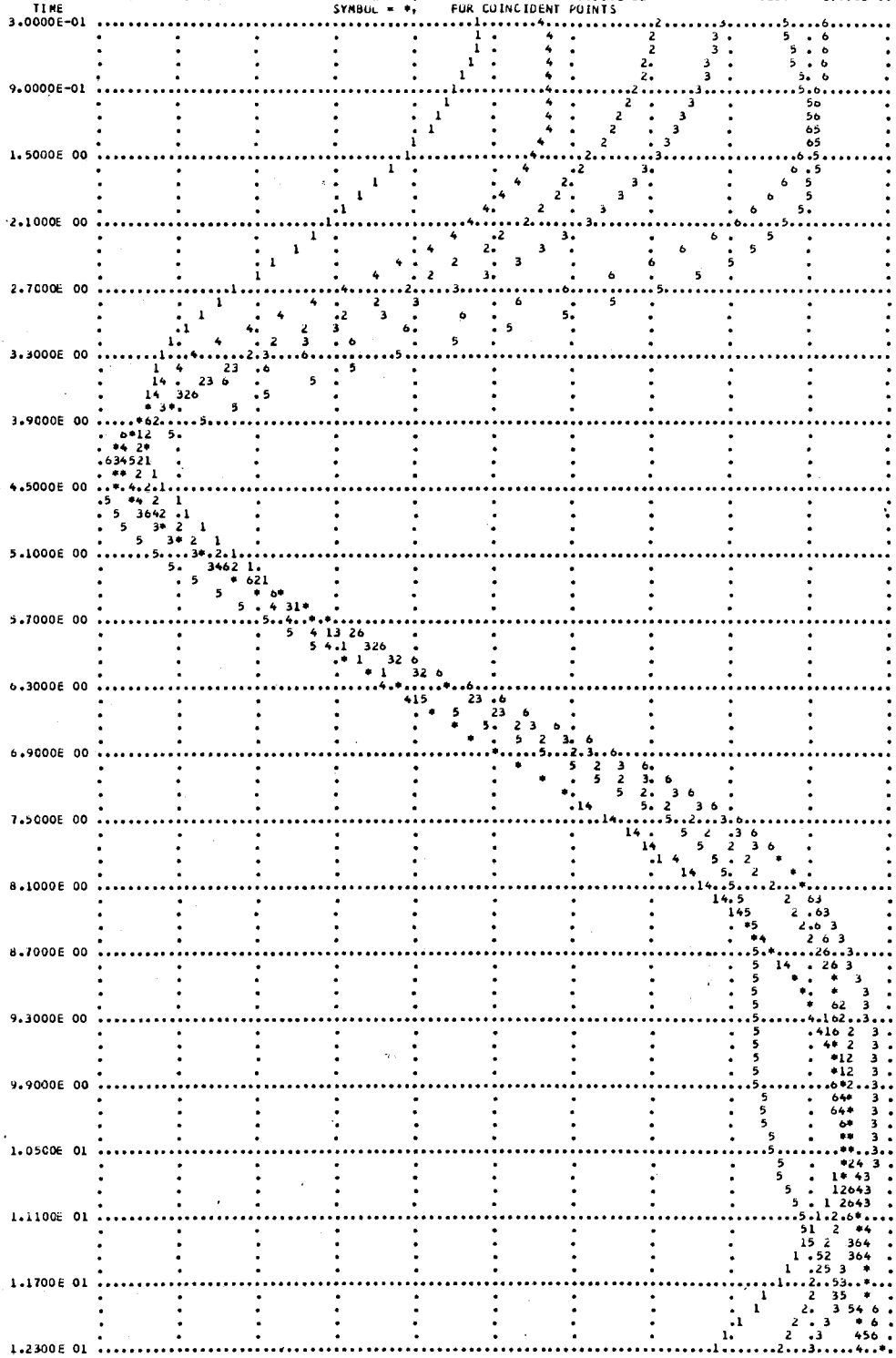
Y( 1) = 1.551E 01	SYMBOL = 1;	SCALE FACTOR = 2.000E 00	Y( 1) = 3.551E 01
Y( 9) = 6.019E 00	SYMBOL = 2;	SCALE FACTOR = 2.000E 00	Y( 9) = 2.402E 01
Y(18) = 8.097E 00	SYMBOL = 3;	SCALE FACTOR = 9.000E-01	Y(18) = 1.710E 01
Y( 4) = 1.272E 01	SYMBOL = 4;	SCALE FACTOR = 4.000E 00	Y( 4) = 5.272E 01
Y(12) = 2.019E 01	SYMBOL = 5;	SCALE FACTOR = 4.000E 00	Y(12) = 6.019E 01
Y(21) = 1.558E 01	SYMBOL = 6;	SCALE FACTOR = 4.000E 00	Y(21) = 5.558E 01
	SYMBOL = *;	FCR GOING IDENT POINTS	



DYSLMP SIMULATION PROGRAM

SERIES PUND MODEL RESPONSE

Y( 5) = 0.022E-01	SYMBOL = 1,	SCALE FACTOR = 8.000E-02	Y( 5) = 1.402E 00
Y(13) = 1.232E 00	SYMBOL = 2,	SCALE FACTOR = 3.000E-01	Y(13) = 4.232E 00
Y(22) = 1.509E 00	SYMBOL = 3,	SCALE FACTOR = 3.000E-01	Y(22) = 4.509E 00
Y( 6) = 1.928E-01	SYMBOL = 4,	SCALE FACTOR = 9.000E-02	Y( 6) = 1.093E 00
Y(14) = 3.233E-01	SYMBOL = 5,	SCALE FACTOR = 8.000E-02	Y(14) = 1.123E 00
Y(23) = 8.055E-01	SYMBOL = 6,	SCALE FACTOR = 9.000E-02	Y(23) = 1.706E 00



## APPENDIX C

### CONTROL OPTIMIZATION SIMULATION RESULTS

The program listing and computer output for the control optimization series are presented here. Notice the monitoring option of sampling is incorporated into the user deck for nitrate (or ammonia), fish, and zooplankton. The output first lists the variable parameters, then search trials and corresponding performance index values. The last evaluation returned by the search algorithm is the optimum combination found. Printed and plotted outputs correspond to this parameter combination. Here again, two runs were required to collect all of the pertinent output.





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LARK
217 1 CALL SAMPLE(Y(22),X(40),P(5),P(47),1)
218 X(53)=P(7)*(3.87)/X(40)
219 2 IF(JFSAM.EQ.1) GO TO 3
220 X(54)=P(8)*(9.45)/Y(26)
221 GO TO 4
222 3 CALL SAMPLE(Y(20),X(41),P(5),P(47),2)
223 X(34)=P(8)*(9.45)/X(41)
224 4 X(55)=P(9)*(1.0-(2.01500*Y(21)+66.6179)/(.021766*Y(26)+
225 1.084416*Y(24)+.145201*Y(27)+.051755*Y(23)+.016249*Y(24)+
226 1.011848*Y(25)))
227 IF(JAMSAM.EQ.1) GO TO 5
228 IF(Y(19).LE.P(15)) GO TO 6
229 X(36)=P(10)
230 GO TO 7
231 6 X(36)=0.0
232 GO TO 7
233 5 CALL SAMPLE(Y(19),X(42),P(45),P(48),3)
234 IF(X(42).LE.P(15)) GO TO 8
235 X(36)=P(10)
236 GO TO 7
237 8 X(36)=0.0
238 7 X(37)=P(11)*P(12)/.090
239 IF(Y(28).GT.P(16)) GO TO 15
240 X(39)=P(14)*P(16)-Y(28)
241 X(38)=P(13)*X(39)
242 GO TO 16
243 15 X(39)=0.0
244 X(38)=P(13)*X(39)
245 16 CONTINUE
246 CALL DELAY
247 P(5)=P(45)+P(12)
248 IF(Y(NYPI)-P(5)) 17,18,18
249 17 X(2)=1.5569*24.92*P(3)
250 X(4)=1.75*32.0*P(3)
251 X(6)=363.76581*4.3*P(2)
252 X(8)=23.78049*4.1*P(4)
253 18 P(6)=P(45)+2.0*P(12)
254 IF(Y(NYPI)-P(6)) 19,20,20
255 19 X(10)=1.5365*10.25*P(3)
256 X(12)=1.75185*27.0*P(3)
257 X(14)=201.46714*2.1*P(2)
258 X(16)=23.72727*11.0*P(4)
259 20 CONTINUE
260 RETURN
261 END
262
263 SUBROUTINE INTDEL
264 COMMON/ALL/Y(92),X(50),P(50),NY,NYPI,NYP2,NYMAX,NX,NR,NM
265 COMMON/CDLAY/DELAY(4000),LABELU(25,4),IOTYPE(25),ND,NDY,NOMAX,
266 IDELAY,TIME(25)
267 DD 1 I=1,ND
268 TIME(I)=P(12)
269 J=LABELU(I,1)
270 K=LABELU(I,2)

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LARK
271 DD 1 I=J,K
272 1 DELAYV(I)=0.0
273 RETURN
274 END
275 SUBROUTINE PARADJ
276 COMMON/ALL/Y(92),X(50),P(50),NY,NYPI,NYP2,NYMAX,NX,NR,NM
277 READ(NR,1) P(1)
278 1 FORMAT(1F10.0)
279 RETURN
280 END
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DATA						
2	0	0	1	29	0	1
0	0	0				
49						
289	0.0	58.0	55.0	55.0	548.0	
290	0.5	46.0	43.5	44.0	475.0	
291	1.0	41.0	37.0	36.0	420.0	
292	1.5	40.0	35.8	34.0	380.0	
293	2.0	41.0	36.0	34.0	345.0	
294	2.5	48.5	44.0	42.0	320.0	
295	3.0	58.0	53.0	50.0	305.0	
296	3.5	56.0	53.0	50.0	300.0	
297	4.0	55.0	53.0	50.0	308.0	
298	4.5	62.5	56.0	53.8	376.0	
299	5.0	65.0	58.5	57.0	430.0	
300	5.5	63.5	59.5	56.2	475.0	
301	6.0	62.0	60.0	60.0	518.0	
302	6.5	68.5	66.0	67.0	540.0	
303	7.0	76.0	75.0	74.0	580.0	
304	7.5	80.0	79.5	79.0	608.0	
305	8.0	82.0	82.0	82.0	640.0	
306	8.5	85.8	84.5	84.5	660.0	
307	9.0	87.0	86.0	86.0	685.0	
308	9.5	85.8	84.0	84.5	695.0	
309	10.0	82.0	81.0	81.0	690.0	
310	10.5	73.0	74.5	73.5	673.0	
311	11.0	68.0	67.0	65.0	640.0	
312	11.5	63.5	60.0	60.0	600.0	
313	12.0	56.0	55.0	50.0	548.0	
314	12.5	46.0	43.5	44.0	475.0	
315	13.0	41.0	37.0	36.0	420.0	
316	13.5	40.0	35.8	34.0	380.0	
317	14.0	41.0	36.0	34.0	345.0	
318	14.5	48.5	44.0	42.0	320.0	
319	15.0	58.0	53.0	50.0	305.0	
320	15.5	56.0	53.0	50.0	300.0	
321	16.0	55.0	53.0	50.0	308.0	
322	16.5	62.5	56.0	53.8	376.0	
323	17.0	65.0	58.5	57.0	430.0	
324	17.5	63.5	59.5	56.2	475.0	



80/80 LIST

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00900000011111111122222222333333334444444455555556666666777777778
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CARU
325      16.0      62.0      60.0      60.0      518.0
326      16.5      68.5      66.0      67.0      540.0
327      16.0      76.0      75.0      74.0      520.0
328      19.5      80.0      79.5      79.0      608.0
329      20.0      82.0      82.0      82.0      640.0
330      20.5      85.8      84.5      84.5      660.0
331      21.0      87.0      86.0      86.0      685.0
332      21.5      89.8      89.0      89.5      695.0
333      22.0      89.0      81.0      81.0      690.0
334      22.5      73.0      74.5      73.5      673.0
335      23.0      68.0      67.0      65.0      640.0
336      23.5      63.5      60.0      60.0      600.0
337      24.0      58.0      55.0      55.0      548.0
338      1 1 1 1 1 0 1 2 0      POND MODEL OPTIMIZATION, TZERO = 6.0
339      29 42 50 20      6.0 12.0 .0025
340      21.406 29.433 4.0072 27.791 .06081 .46192 1583.2 4.2105
341      12.403 22.075 1.9741 32.760 2.3111 .55506 28.348 941.47
342      12.253 9.5351 16.891 1.2874 26.883 2.5632 1.1394 .82379
343      1.4428 7.7877 632.83 12.595 0.0
344      0.0 .05 0.5 1.0 6.090 6.180 400.0 400.0
345      1000.0 30.0 5.0 .090 .90 0.0 24.0 10.0
346      32.3 44.0 7.4 50.0 1.5 1.2 2200.0 6.6
347      22.0 37.0 6.3 61.0 5.3 1.3 .58 1500.0
348      23.0 18.0 30.0 54.8 53.0 5.6 2.0 1.9
349      1.92 12.0 1100.0 29.8 6.0 0.0 0.0 0.0
350      0.0 0.0
351      8
352      1 2 0 0.090 3 4 0 0.090 5 6 0 0.090 7 8 0 0.090
353      9 10 0 0.090 11 12 0 0.090 13 14 0 0.090 15 16 0 0.090
354
355
356
357
358      12 .090 1.0
359      14 0.0 600.0
360      1 0 0 1 0 1 1 0 0      OPTIMAL CONTROL PARAMETER COMBINATION
361      29 42 50 20 6.0 12.0 .0025
362      1 2 0 0.090 3 4 0 0.090 5 6 0 0.090 7 8 0 0.090
363      9 10 0 0.090 11 12 0 0.090 13 14 0 0.090 15 16 0 0.090
364      3 11 20 8 17 28 24 26
365      1 9 18 4 12 21
366
367
368
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```

POND MODEL OPTIMIZATION: TZERO = 6.0

VARIABLE PARAMETER VALUES

P(12) = 8.999997E-02 TO 1.000000E 00  
 P(14) = 0.0 TO 6.000000E 02

PI = 2.047080E 06 AT

P(12) = 5.450000E-01 P(14) = 3.000000E 02

PI = 1.993078E 06 AT

P(12) = 3.933333E-01 P(14) = 2.000000E 02

PI = 1.997091E 06 AT

P(12) = 6.966665E-01 P(14) = 2.000000E 02

PI = 2.022584E 06 AT

P(12) = 3.933333E-01 P(14) = 4.000000E 02

PI = 1.995593E 06 AT

P(12) = 5.965665E-01 P(14) = 2.000000E 02

PI = 1.990439E 06 AT

P(12) = 1.900999E-01 P(14) = 2.000000E 02

PI = 2.008144E 06 AT

P(12) = 3.933333E-01 P(14) = 3.339998E 02

PI = 1.981780E 06 AT

P(12) = 3.933333E-01 P(14) = 6.599997E 01

PI = 2.011739E 06 AT

P(12) = 3.259258E-01 P(14) = 2.155559E 01

PI = 2.012992E 06 AT

P(12) = 4.607406E-01 P(14) = 2.155556E 01

PI = 1.986393E 06 AT

P(12) = 3.259258E-01 P(14) = 1.104444E 02

PI = 1.987749E 06 AT

P(12) = 4.607406E-01 P(14) = 1.104444E 02

PI = 1.982161E 06 AT

P(12) = 4.382704E-01 P(14) = 6.600000E 01

PI = 1.982840E 06 AT

P(12) = 3.483939E-01 P(14) = 6.600000E 01

PI = 1.983393E 06 AT

P(12) = 3.933333E-01 P(14) = 9.562966E 01

PI = 1.995015E 06 AT

P(12) = 3.933333E-01 P(14) = 3.637024E 01

PI = 1.981780E 06 AT

P(12) = 3.933333E-01 P(14) = 6.599997E 01

DYNSIM SIMULATION PROGRAM OPTIMAL CONTROL PARAMETER COMBINATION PAGE 1 OF RUN 1

CACER OF SYSTEM = 29  
 NUMBER OF X'S = 42  
 NUMBER OF PARAMETERS = 50  
 NUMBER OF DELAYS = 8  
 OUTPUT INTERVAL = 20  
 INITIAL TIME = 6.000E 00  
 FINAL TIME = 1.200E 01  
 INTEGRATION STEP = 2.500E-03

INITIAL Y VALUES  
 Y( 1) = 2.140599E 01 Y( 2) = 2.943300E 01 Y( 3) = 4.007199E 00 Y( 4) = 2.779099E 01 Y( 5) = 8.608100E-01  
 Y( 6) = 4.619200E-01 Y( 7) = 1.583200E 03 Y( 8) = 4.210500E 00 Y( 9) = 1.240303E 01 Y(10) = 2.207500E 01  
 Y(11) = 1.974099E 00 Y(12) = 3.275999E 01 Y(13) = 2.311099E 00 Y(14) = 5.550600E-01 Y(15) = 5.800000E-01  
 Y(16) = 9.414700E 02 Y(17) = 1.225300E 01 Y(18) = 9.535100E 00 Y(19) = 1.689099E 01 Y(20) = 1.287399E 00  
 Y(21) = 2.688300E 01 Y(22) = 2.563200E 00 Y(23) = 1.139400E 00 Y(24) = 8.237900E-01 Y(25) = 1.442800E 00  
 Y(26) = 7.787700E 00 Y(27) = 6.328298E 02 Y(28) = 1.259500E 01 Y(29) = 0.0

INITIAL X VALUES  
 X( 1) = 1.644942E 00 X( 2) = 1.914976E 00 X( 3) = 2.575386E 01 X( 4) = 2.800000E 01 X( 5) = 7.288405E 01  
 X( 6) = 7.820958E 01 X( 7) = 1.001277E 02 X( 8) = 1.074999E 01 X( 9) = 9.478989E-01 X(10) = 1.250031E 00  
 X(11) = 1.933803E 01 X(12) = 2.364990E 01 X(13) = 1.988579E 01 X(14) = 2.115404E 01 X(15) = 2.977300E 02  
 X(16) = 2.609998E 02 X(17) = 1.666666E 01 X(18) = 4.555555E 01 X(19) = 1.555555E 01 X(20) = 5.180000E 02  
 X(21) = 9.066177E-01 X(22) = 9.321382E-01 X(23) = 9.676427E-01 X(24) = 1.018100E 00 X(25) = 1.914976E 00  
 X(26) = 2.800000E 01 X(27) = 7.820958E 01 X(28) = 9.749997E 01 X(29) = 1.250031E 00 X(30) = 2.364996E 01  
 X(31) = 2.115404E 01 X(32) = 2.609998E 02 X(33) = 6.039324E 02 X(34) = 4.853806E 02 X(35) = -1.065311E 02  
 X(36) = 0.0 X(37) = 2.185185E 01 X(38) = 0.0 X(39) = 0.0 X(40) = 0.0  
 X(41) = C.0 X(42) = 0.0

PARAMETER VALUES  
 P( 1) = 0.0 P( 2) = 5.000000E-02 P( 3) = 5.000000E-01 P( 4) = 1.000000E 00 P( 5) = 6.393332E 00  
 P( 6) = 6.786666E 00 P( 7) = 4.000000E 02 P( 8) = 4.000000E 02 P( 9) = 1.000000E 03 P(10) = 3.000000E 01  
 P(11) = 3.933333E-01 P(12) = 3.933333E-01 P(13) = 9.000000E-01 P(14) = 6.600000E 01 P(15) = 2.400000E 01  
 P(16) = 1.000000E 01 P(17) = 3.200000E 01 P(18) = 4.400000E 01 P(19) = 7.299999E 00 P(20) = 5.000000E 01  
 P(21) = 1.500000E 00 P(22) = 1.200000E 00 P(23) = 2.200000E 03 P(24) = 6.599999E 00 P(25) = 2.200000E 01  
 P(26) = 3.700000E 01 P(27) = 6.299999E 00 P(28) = 6.100000E 01 P(29) = 5.299999E 00 P(30) = 1.500000E 00  
 P(31) = 5.800000E-01 P(32) = 1.500000E 03 P(33) = 2.300000E 01 P(34) = 1.800000E 01 P(35) = 3.000000E 01  
 P(36) = 5.799999E 00 P(37) = 5.300000E 01 P(38) = 5.599999E 00 P(39) = 2.000000E 00 P(40) = 1.900000E 00  
 P(41) = 1.919999E 00 P(42) = 1.200000E 01 P(43) = 1.100000E 03 P(44) = 2.979999E 01 P(45) = 6.000000E 00  
 P(46) = 0.0 P(47) = 0.0 P(48) = 0.0 P(49) = 0.0 P(50) = 0.0

TIME DELAYS  
 F( 1) = 3.933333E-01 F( 2) = 3.933333E-01 F( 3) = 3.933333E-01 F( 4) = 3.933333E-01 F( 5) = 3.933333E-01  
 F( 6) = 3.933333E-01 F( 7) = 3.933333E-01 F( 8) = 3.933333E-01

DYNSIM SIMULATION PROGRAM OPTIMAL CONTROL PARAMETER COMBINATION PAGE 2 OF RUN 1

TIME	Y(10)	Y( 3)	Y(11)	Y(20)	Y( 8)	Y(17)	Y(28)	Y(24)	Y(26)
6.000E 00	4.007199E 00	1.974099E 00	1.287399E 00	4.210499E 00	1.225299E 01	1.259499E 01	8.237899E-01	7.787699E 00	
6.050E 00	4.012391E 00	1.964330E 00	1.258559E 00	4.192445E 00	1.2154150E 01	1.217089E 01	8.300557E-01	7.809135E 00	
6.100E 00	3.989668E 00	1.953938E 00	1.242571E 00	4.176379E 00	1.205525E 01	1.203357E 01	8.367865E-01	7.831396E 00	
6.150E 00	3.983034E 00	1.942919E 00	1.226162E 00	4.161165E 00	1.195655E 01	1.191327E 01	8.440159E-01	7.855008E 00	
6.200E 00	3.973423E 00	1.931045E 00	1.214326E 00	4.144529E 00	1.185876E 01	1.179141E 01	8.517486E-01	7.879782E 00	
6.250E 00	3.959292E 00	1.918405E 00	1.205250E 00	4.128400E 00	1.176209E 01	1.167003E 01	8.598841E-01	7.906264E 00	
6.300E 00	3.947457E 00	1.905206E 00	1.194548E 00	4.112842E 00	1.166651E 01	1.155199E 01	8.687254E-01	7.933888E 00	
6.350E 00	3.935360E 00	1.891728E 00	1.183093E 00	4.096557E 00	1.157192E 01	1.143572E 01	8.779712E-01	7.962892E 00	
6.400E 00	3.921895E 00	1.878592E 00	1.172980E 00	4.080497E 00	1.147781E 01	1.132012E 01	8.873447E-01	7.993297E 00	
6.450E 00	3.908360E 00	1.864843E 00	1.162903E 00	4.064520E 00	1.137463E 01	1.120648E 01	8.979660E-01	8.025075E 00	
6.500E 00	3.894727E 00	1.852667E 00	1.152617E 00	4.048524E 00	1.127349E 01	1.109469E 01	9.087588E-01	8.058251E 00	
6.550E 00	3.881238E 00	1.841602E 00	1.143927E 00	4.032797E 00	1.118420E 01	1.098343E 01	9.200472E-01	8.093123E 00	
6.600E 00	3.867816E 00	1.831284E 00	1.135909E 00	4.017240E 00	1.099457E 01	1.088128E 01	9.318533E-01	8.129830E 00	
6.650E 00	3.854470E 00	1.821682E 00	1.128471E 00	3.995543E 00	1.082838E 01	1.068181E 01	9.441784E-01	8.168171E 00	
6.700E 00	3.841237E 00	1.812749E 00	1.121629E 00	3.974396E 00	1.067941E 01	1.049517E 01	9.570074E-01	8.208234E 00	
6.750E 00	3.828119E 00	1.804539E 00	1.115304E 00	3.953923E 00	1.054131E 01	1.032535E 01	9.703287E-01	8.249991E 00	
6.800E 00	3.815129E 00	1.796931E 00	1.109409E 00	3.934106E 00	1.041103E 01	1.017038E 01	9.841391E-01	8.293703E 00	
6.850E 00	3.802271E 00	1.790013E 00	1.103971E 00	3.914831E 00	1.029617E 01	1.002152E 01	9.981391E-01	8.339158E 00	
6.900E 00	3.789544E 00	1.783784E 00	1.100367E 00	3.896083E 00	1.018647E 01	9.900186E 00	1.013051E 01	8.384824E 00	
6.950E 00	3.776930E 00	1.778258E 00	1.095814E 00	3.877803E 00	1.008235E 01	9.817482E 00	1.028129E 01	8.432470E 00	
7.000E 00	3.764428E 00	1.773497E 00	1.091462E 00	3.859864E 00	1.018525E 01	9.741457E 00	1.043632E 01	8.482358E 00	
7.050E 00	3.752044E 00	1.769437E 00	1.087309E 00	3.842863E 00	1.012407E 01	9.677216E 00	1.059437E 01	8.533966E 00	
7.100E 00	3.739774E 00	1.765974E 00	1.083363E 00	3.826774E 00	1.006607E 01	9.613522E 00	1.075499E 01	8.586604E 00	
7.150E 00	3.727624E 00	1.763129E 00	1.079615E 00	3.811271E 00	1.000976E 01	9.552804E 00	1.091687E 01	8.640341E 00	
7.200E 00	3.715594E 00	1.760863E 00	1.076037E 00	3.796495E 00	9.954192E 00	9.492937E 00	1.108034E 01	8.695067E 00	
7.250E 00	3.703684E 00	1.759146E 00	1.072627E 00	3.782347E 00	9.898672E 00	9.434284E 00	1.124546E 01	8.750703E 00	
7.300E 00	3.691895E 00	1.757937E 00	1.069376E 00	3.768678E 00	9.844331E 00	9.376447E 00	1.141164E 01	8.807209E 00	
7.350E 00	3.680224E 00	1.757170E 00	1.066282E 00	3.755507E 00	9.790546E 00	9.319631E 00	1.157868E 01	8.864490E 00	
7.400E 00	3.668669E 00	1.756846E 00	1.063342E 00	3.742805E 00	9.737768E 00	9.263758E 00	1.174634E 01	8.922475E 00	
7.450E 00	3.657224E 00	1.756927E 00	1.060555E 00	3.730579E 00	9.685719E 00	9.208920E 00	1.191438E 01	8.981037E 00	
7.500E 00	3.645892E 00	1.757406E 00	1.057927E 00	3.718879E 00	9.634536E 00	9.155073E 00	1.2082500E 01	9.040247E 00	
7.550E 00	3.634673E 00	1.758277E 00	1.055451E 00	3.707627E 00	9.581856E 00	9.099942E 00	1.2250023E 01	9.099572E 00	
7.600E 00	3.623574E 00	1.759642E 00	1.053127E 00	3.696807E 00	9.529377E 00	9.045630E 00	1.2416058E 01	9.159326E 00	
7.650E 00	3.612594E 00	1.761504E 00	1.050953E 00	3.686400E 00	9.477736E 00	8.991853E 00	1.2580462E 01	9.218895E 00	
7.700E 00	3.601734E 00	1.763862E 00	1.048927E 00	3.676425E 00	9.427134E 00	8.939271E 00	1.274303E 01	9.278395E 00	
7.750E 00	3.591001E 00	1.766717E 00	1.047049E 00	3.666883E 00	9.377614E 00	8.887793E 00	1.290371E 01	9.337769E 00	
7.800E 00	3.580395E 00	1.770076E 00	1.045325E 00	3.657783E 00	9.328659E 00	8.837494E 00	1.3062305E 01	9.396912E 00	
7.850E 00	3.570917E 00	1.773938E 00	1.043751E 00	3.649147E 00	9.280816E 00	8.788363E 00	1.3218679E 01	9.455164E 00	
7.900E 00	3.562562E 00	1.778307E 00	1.042327E 00	3.640985E 00	9.233853E 00	8.740354E 00	1.3372726E 01	9.514580E 00	
7.950E 00	3.555342E 00	1.783182E 00	1.041053E 00	3.633205E 00	9.187775E 00	8.693460E 00	1.3524361E 01	9.572903E 00	
8.000E 00	3.549166E 00	1.788564E 00	1.039927E 00	3.625826E 00	9.142581E 00	8.647659E 00	1.367346E 01	9.630884E 00	
8.050E 00	3.543944E 00	1.794452E 00	1.038951E 00	3.618847E 00	9.104988E 00	8.602927E 00	1.381952E 01	9.688013E 00	
8.100E 00	3.539686E 00	1.757305E 00	1.038127E 00	3.612205E 00	9.069744E 00	8.573110E 00	1.3962193E 01	9.746235E 00	
8.150E 00	3.536392E 00	1.368363E 00	1.037459E 00	3.606997E 00	9.036510E 00	8.539476E 00	1.4101391E 01	9.794652E 00	
8.200E 00	3.534022E 00	1.361150E 00	1.036928E 00	3.602191E 00	9.004083E 00	8.506961E 00	1.4237070E 01	9.853670E 00	
8.250E 00	3.532573E 00	1.354027E 00	1.036421E 00	3.597683E 00	8.972091E 00	8.475550E 00	1.4369183E 01	9.906832E 00	
8.300E 00	3.532042E 00	1.346991E 00	1.035938E 00	3.593476E 00	8.940174E 00	8.443865E 00	1.4497681E 01	9.956914E 00	
8.350E 00	3.532427E 00	1.339736E 00	1.035476E 00	3.589493E 00	8.910957E 00	8.415523E 00	1.462252E 01	1.000989E 01	
8.400E 00	3.533715E 00	1.332617E 00	1.035038E 00	3.585774E 00	8.881638E 00	8.386832E 00	1.4743710E 01	1.005976E 01	
8.450E 00	3.535918E 00	1.325528E 00	1.034624E 00	3.582241E 00	8.853062E 00	8.358970E 00	1.4861231E 01	1.010850E 01	
8.500E 00	3.539045E 00	1.318457E 00	1.034230E 00	3.578861E 00	8.825220E 00	8.331903E 00	1.4975080E 01	1.015611E 01	
8.550E 00	3.543081E 00	1.311393E 00	1.033855E 00	3.575614E 00	8.799379E 00	8.303154E 00	1.5085249E 01	1.020264E 01	
8.600E 00	3.548026E 00	1.304335E 00	1.033499E 00	3.572482E 00	8.774734E 00	8.274734E 00	1.5191593E 01	1.0247981E 01	
8.650E 00	3.553879E 00	1.297273E 00	1.033161E 00	3.569464E 00	8.751843E 00	8.246467E 00	1.529622E 01	1.0292231E 01	
8.700E 00	3.560640E 00	1.290203E 00	1.032841E 00	3.566556E 00	8.730311E 00	8.219857E 00	1.5392457E 01	1.033538E 01	
8.750E 00	3.568320E 00	1.283134E 00	1.032540E 00	3.563750E 00	8.709654E 00	8.193335E 00	1.5488768E 01	1.037763E 01	
8.800E 00	3.576942E 00	1.276062E 00	1.032254E 00	3.561044E 00	8.689785E 00	8.165449E 00	1.5580864E 01	1.0418490E 01	

DYSLMP SIMULATION PROGRAM OPTIMAL CONTROL PARAMETER COMBINATION PAGE 3 OF RUN 1

TIME	Y(3)	Y(11)	Y(20)	Y(8)	Y(17)	Y(28)	Y(24)	Y(26)
8.850E 00	3.0113106E 00	1.2277734E 00	7.4702495E-01	3.4122171E 00	8.6249332E 00	8.1396675E 00	1.5669601E 00	1.0450489E 01
8.800E 00	2.9957294E 00	1.2493372E 00	7.4179578E-01	3.4023180E 00	8.5983944E 00	8.1144581E 00	1.5752262E 00	1.0497446E 01
8.950E 00	2.9802313E 00	1.2409001E 00	7.3661190E-01	3.3925190E 00	8.5823543E 00	8.0898066E 00	1.5837774E 00	1.0535502E 01
9.000E 00	2.9648094E 00	1.2326422E 00	7.3146904E-01	3.3828259E 00	8.5646787E 00	8.0656891E 00	1.5917301E 00	1.0572564E 01
9.050E 00	2.9598961E 00	1.2295876E 00	7.2921580E-01	3.3752508E 00	8.5292721E 00	8.0487814E 00	1.5993147E 00	1.0608159E 01
9.100E 00	2.9534769E 00	1.2262812E 00	7.2709787E-01	3.3687096E 00	8.5134783E 00	8.0335865E 00	1.6064854E 00	1.0644970E 01
9.150E 00	2.9469185E 00	1.2228479E 00	7.2499001E-01	3.3621283E 00	8.4995022E 00	8.0204372E 00	1.6132631E 00	1.0674091E 01
9.200E 00	2.9403595E 00	1.2194042E 00	7.2288471E-01	3.3559637E 00	8.4859122E 00	8.0080309E 00	1.6196699E 00	1.0704606E 01
9.250E 00	2.9342403E 00	1.2159243E 00	7.2078121E-01	3.3500746E 00	8.4727907E 00	7.9962587E 00	1.6257248E 00	1.0733598E 01
9.300E 00	2.9279404E 00	1.2124481E 00	7.1869272E-01	3.3444662E 00	8.4603405E 00	7.9849081E 00	1.6314478E 00	1.0761147E 01
9.350E 00	2.9216290E 00	1.2090616E 00	7.1663111E-01	3.3391079E 00	8.4483576E 00	7.973609E 00	1.6368561E 00	1.0787329E 01
9.400E 00	2.915328E 00	1.2057333E 00	7.1459407E-01	3.3339682E 00	8.4367838E 00	7.9633894E 00	1.6419668E 00	1.0812220E 01
9.450E 00	2.9091091E 00	1.2024374E 00	7.1257091E-01	3.3290272E 00	8.4255819E 00	7.9531527E 00	1.6467972E 00	1.0835990E 01
9.500E 00	2.9028816E 00	1.1991453E 00	7.1055841E-01	3.3242645E 00	8.4147282E 00	7.9432240E 00	1.6513634E 00	1.0858411E 01
9.550E 00	2.9068197E 00	1.2012491E 00	7.1135938E-01	3.3218400E 00	8.4114237E 00	7.9400673E 00	1.6556203E 00	1.0879435E 01
9.600E 00	2.9095860E 00	1.2027655E 00	7.1221477E-01	3.3200521E 00	8.4095316E 00	7.9383192E 00	1.6595736E 00	1.0898835E 01
9.650E 00	2.9119101E 00	1.2038794E 00	7.1305096E-01	3.3184357E 00	8.4094925E 00	7.9383430E 00	1.6632252E 00	1.0916713E 01
9.700E 00	2.9147892E 00	1.2051210E 00	7.1397805E-01	3.3172150E 00	8.4095821E 00	7.9388437E 00	1.6666012E 00	1.0933167E 01
9.750E 00	2.9174185E 00	1.2066154E 00	7.1497673E-01	3.3162889E 00	8.4100552E 00	7.9397306E 00	1.6697187E 00	1.0948298E 01
9.800E 00	2.9201937E 00	1.2081976E 00	7.1598089E-01	3.3156118E 00	8.4106372E 00	7.9408599E 00	1.6725900E 00	1.0962191E 01
9.850E 00	2.9230013E 00	1.2097769E 00	7.1694411E-01	3.3151712E 00	8.4119091E 00	7.9422569E 00	1.6752491E 00	1.0974934E 01
9.900E 00	2.9258385E 00	1.2112617E 00	7.1789289E-01	3.3149300E 00	8.4133568E 00	7.9438982E 00	1.6776434E 00	1.0986070E 01
9.950E 00	2.9287043E 00	1.2127838E 00	7.1885365E-01	3.3148689E 00	8.4150896E 00	7.9457398E 00	1.6799421E 00	1.0997286E 01
1.000E 01	2.9316044E 00	1.2143888E 00	7.1984100E-01	3.3149681E 00	8.4170198E 00	7.9477425E 00	1.6820107E 00	1.1007044E 01
1.005E 01	2.9427128E 00	1.2208919E 00	7.2331351E-01	3.3168192E 00	8.4248848E 00	7.9552264E 00	1.6838684E 00	1.1015626E 01
1.010E 01	2.9536040E 00	1.2258911E 00	7.2673470E-01	3.3194113E 00	8.4341898E 00	7.9637852E 00	1.6855078E 00	1.1022983E 01
1.015E 01	2.9636965E 00	1.2310772E 00	7.3002529E-01	3.3221130E 00	8.4445207E 00	7.9728541E 00	1.6869476E 00	1.1029212E 01
1.020E 01	2.9740429E 00	1.2370911E 00	7.3357725E-01	3.3249664E 00	8.4557543E 00	7.9824110E 00	1.6882067E 00	1.1034414E 01
1.025E 01	2.9847212E 00	1.2425423E 00	7.3703223E-01	3.3280354E 00	8.4666805E 00	7.9924254E 00	1.6892966E 00	1.1038686E 01
1.030E 01	2.9954281E 00	1.2482252E 00	7.4032664E-01	3.3312979E 00	8.4781914E 00	8.0060453E 00	1.6902390E 00	1.1042097E 01
1.035E 01	3.0061617E 00	1.2542553E 00	7.4392545E-01	3.3347349E 00	8.4896936E 00	8.0172911E 00	1.6910391E 00	1.1044725E 01
1.040E 01	3.0170002E 00	1.2597980E 00	7.4752915E-01	3.3383072E 00	8.5017452E 00	8.0286875E 00	1.6917124E 00	1.1046646E 01
1.045E 01	3.0279503E 00	1.2659245E 00	7.5106573E-01	3.3419971E 00	8.5138350E 00	8.0403671E 00	1.6922648E 00	1.1047915E 01
1.050E 01	3.0389933E 00	1.2717133E 00	7.5473386E-01	3.3458052E 00	8.5262260E 00	8.0521622E 00	1.6927176E 00	1.1048592E 01
1.055E 01	3.0509512E 00	1.2833989E 00	7.6282841E-01	3.3522253E 00	8.5465746E 00	8.0714397E 00	1.6930313E 00	1.1048491E 01
1.060E 01	3.0637641E 00	1.2947187E 00	7.6923281E-01	3.3589687E 00	8.5706882E 00	8.0926905E 00	1.6932163E 00	1.1047416E 01
1.065E 01	3.1064453E 00	1.3093309E 00	7.7621001E-01	3.3660040E 00	8.5938120E 00	8.1166267E 00	1.6932764E 00	1.1045605E 01
1.070E 01	3.1289358E 00	1.3188639E 00	7.8425413E-01	3.3734417E 00	8.6202555E 00	8.1399078E 00	1.6932287E 00	1.1043113E 01
1.075E 01	3.1515465E 00	1.3330120E 00	7.9083174E-01	3.3810167E 00	8.6443281E 00	8.1652632E 00	1.6930752E 00	1.1039934E 01
1.080E 01	3.1742840E 00	1.3438606E 00	7.9923671E-01	3.3886975E 00	8.6715317E 00	8.1897078E 00	1.6928282E 00	1.1036174E 01
1.085E 01	3.1973610E 00	1.3572416E 00	8.0632162E-01	3.3970470E 00	8.6970272E 00	8.2158766E 00	1.6924896E 00	1.1031828E 01
1.090E 01	3.2206907E 00	1.3700399E 00	8.1452155E-01	3.4054298E 00	8.7246456E 00	8.2414088E 00	1.6920719E 00	1.1026990E 01
1.095E 01	3.2443724E 00	1.3822489E 00	8.2251453E-01	3.4139833E 00	8.7521267E 00	8.2683525E 00	1.6915741E 00	1.1021648E 01
1.100E 01	3.2689353E 00	1.3965797E 00	8.3018762E-01	3.4227409E 00	8.7797698E 00	8.2952936E 00	1.6910066E 00	1.1015891E 01
1.105E 01	3.2938216E 00	1.4124765E 00	8.4156331E-01	3.4320778E 00	8.8129320E 00	8.3281223E 00	1.6903972E 00	1.1009359E 01
1.110E 01	3.3284779E 00	1.4296235E 00	8.5026699E-01	3.4434948E 00	8.8469076E 00	8.3596954E 00	1.6896191E 00	1.1002621E 01
1.115E 01	3.3589287E 00	1.4456767E 00	8.6141557E-01	3.4543047E 00	8.8827286E 00	8.3931456E 00	1.6888008E 00	1.0995143E 01
1.120E 01	3.3898230E 00	1.4629774E 00	8.7138897E-01	3.4652624E 00	8.9186010E 00	8.4289513E 00	1.6879005E 00	1.0987098E 01
1.125E 01	3.4210749E 00	1.4804163E 00	8.8190198E-01	3.4765463E 00	8.9554834E 00	8.4644651E 00	1.6869259E 00	1.0978563E 01
1.130E 01	3.4527464E 00	1.4975159E 00	8.9338467E-01	3.4880924E 00	8.9934425E 00	8.5012970E 00	1.6858749E 00	1.0969504E 01
1.135E 01	3.4844871E 00	1.5153535E 00	9.0584095E-01	3.4998131E 00	9.0315504E 00	8.5381102E 00	1.6847525E 00	1.0959918E 01
1.140E 01	3.5174122E 00	1.5339394E 00	9.1546363E-01	3.5118668E 00	9.0707884E 00	8.5770702E 00	1.6835604E 00	1.0949979E 01
1.145E 01	3.5504379E 00	1.5524311E 00	9.2669839E-01	3.5240728E 00	9.1108398E 00	8.6166315E 00	1.6822944E 00	1.0939558E 01
1.150E 01	3.5839167E 00	1.5711660E 00	9.3809408E-01	3.5365143E 00	9.1515770E 00	8.6566448E 00	1.6809740E 00	1.0928707E 01
1.155E 01	3.6307001E 00	1.5963287E 00	9.5507008E-01	3.5519079E 00	9.2017536E 00	8.7047272E 00	1.6793597E 00	1.0917227E 01
1.160E 01	3.6775303E 00	1.6240788E 00	9.7085267E-01	3.5672941E 00	9.2540874E 00	8.7572194E 00	1.6780539E 00	1.0905096E 01
1.165E 01	3.7242069E 00	1.6502409E 00	9.8607186E-01	3.5827570E 00	9.3099909E 00	8.8120413E 00	1.6764400E 00	1.0892402E 01

DYSLMP SIMULATION PROGRAM OPTIMAL CONTROL PARAMETER COMBINATION PAGE 4 OF RUN 1

TIME	Y(3)	Y(11)	Y(20)	Y(8)	Y(17)	Y(28)	Y(24)	Y(26)
1.170E 01	3.7709703E 00	1.6758604E 00	1.0037222E 00	3.5988910E 00	9.3678741E 00	8.8685055E 00	1.6747932E 00	1.0879114E 01
1.175E 01	3.8182392E 00	1.7024355E 00	1.0197076E 00	3.6144894E 00	9.4263210E 00	8.9277706E 00	1.6730375E 00	1.0868200E 01
1.180E 01	3.8663330E 00	1.7305346E 00	1.0369244E 00	3.6314783E 00	9.4859390E 00	8.9877501E 00	1.6712027E 00	1.0850873E 01
1.185E 01	3.9153789E 00	1.7596760E 00	1.0558453E 00	3.6484842E 00	9.5474539E 00	9.0495214E 00	1.6692867E 00	1.0835932E 01
1.190E 01	3.9661112E 00	1.7894287E 00	1.0739355E 00	3.6656704E 00	9.6106833E 00	9.1139383E 00	1.6672916E 00	1.0816057E 01
1.195E 01	4.0177479E 00	1.8195295E 00	1.0923948E 00	3.6830997E 00	9.6757441E 00	9.1800032E 00	1.6652184E 00	1.0804479E 01
1.200E 01	4.0702515E 00	1.8501310E 00	1.1120749E 00	3.7007933E 00	9.7427816E 00	9.2478828E 00	1.6630678E 00	1.0787982E 01

DYSLIM SIMULATION PROGRAM

OPTIMAL CONTROL PARAMETER COMBINATION

ORDER OF SYSTEM = 29
NUMBER OF X'S = 42
NUMBER OF PARAMETERS = 50
NUMBER OF DELAYS = 8
OUTPUT INTERVAL = 20
INITIAL TIME = 6.0000E 00
FINAL TIME = 1.2000E 01
INTEGRATION STEP = 2.5000E-03

INITIAL Y VALUES

Y( 1) = 2.140599E 01 Y( 2) = 2.943300E 01 Y( 3) = 4.007199E 00 Y( 4) = 2.779099E 01 Y( 5) = 8.608100E-01
Y( 6) = 4.619200E 03 Y( 7) = 1.583200E 03 Y( 8) = 4.210900E 00 Y( 9) = 1.240300E 01 Y(10) = 2.207500E 01
Y(11) = 1.974099E 00 Y(12) = 3.275999E 01 Y(13) = 2.311099E 00 Y(14) = 5.550600E-01 Y(15) = 5.800000E-01
Y(16) = 9.414700E 02 Y(17) = 1.225300E 01 Y(18) = 9.535100E 00 Y(19) = 1.689099E 01 Y(20) = 1.287399E 00
Y(21) = 2.583000E 01 Y(22) = 2.563200E 00 Y(23) = 1.139400E 00 Y(24) = 8.237900E-01 Y(25) = 1.442800E 00
Y(26) = 7.787700E 00 Y(27) = 6.32829E 02 Y(28) = 1.259500E 01 Y(29) = 0.0

INITIAL X VALUES

X( 1) = 1.644942E 00 X( 2) = 1.914974E 00 X( 3) = 2.575386E 01 X( 4) = 2.800000E 01 X( 5) = 7.288405E 01
X( 6) = 7.820958E 01 X( 7) = 1.001277E 02 X( 8) = 9.749997E 01 X( 9) = 9.478949E-01 X(10) = 1.250031E 00
X(11) = 1.933603E 01 X(12) = 2.364996E 01 X(13) = 1.988579E 01 X(14) = 2.115404E 01 X(15) = 2.907300E 02
X(16) = 2.609998E 02 X(17) = 1.666666E 01 X(18) = 1.555555E 01 X(19) = 1.555555E 01 X(20) = 5.180000E 02
X(21) = 9.066177E-01 X(22) = 9.321382E-01 X(23) = 9.676427E-01 X(24) = 1.018100E 00 X(25) = 1.914976E 00
X(26) = 2.800000E 01 X(27) = 7.820958E 01 X(28) = 9.749997E 01 X(29) = 1.250031E 00 X(30) = 2.364996E 01
X(31) = 2.115404E 01 X(32) = 2.609998E 02 X(33) = 6.039324E 02 X(34) = 4.853806E 02 X(35) = -1.065311E 02
X(36) = 0.0 X(37) = 2.185185E 01 X(38) = 0.0 X(39) = 0.0 X(40) = 0.0
X(41) = 0.0 X(42) = 0.0

PARAMETER VALUES

P( 1) = 0.0 P( 2) = 5.000000E-02 P( 3) = 5.000000E-01 P( 4) = 1.000000E 00 P( 5) = 6.393332E 00
P( 6) = 6.786666E 00 P( 7) = 4.000000E 02 P( 8) = 4.000000E 02 P( 9) = 1.000000E 03 P(10) = 3.000000E 01
P(11) = 5.000000E 00 P(12) = 3.933333E-01 P(13) = 9.000000E-01 P(14) = 6.600000E 01 P(15) = 2.400000E 01
P(16) = 1.000000E 01 P(17) = 3.200000E 01 P(18) = 4.400000E 01 P(19) = 7.299999E 00 P(20) = 5.000000E 01
P(21) = 1.500000E 00 P(22) = 1.200000E 00 P(23) = 2.200000E 03 P(24) = 6.599999E 00 P(25) = 2.200000E 01
P(26) = 3.700000E 01 P(27) = 6.299999E 00 P(28) = 6.100000E 01 P(29) = 5.299999E 00 P(30) = 1.500000E 00
P(31) = 5.800000E-01 P(32) = 1.500000E 03 P(33) = 2.300000E 01 P(34) = 1.800000E 01 P(35) = 3.000000E 01
P(36) = 5.799999E 00 P(37) = 5.300000E 01 P(38) = 5.599999E 00 P(39) = 2.000000E 00 P(40) = 1.900000E 01
P(41) = 1.919999E 00 P(42) = 1.200000E 01 P(43) = 1.100000E 03 P(44) = 2.979999E 01 P(45) = 6.000000E 00
P(46) = 0.0 P(47) = 0.0 P(48) = 0.0 P(49) = 0.0 P(50) = 0.0

TIME DELAYS

F( 1) = 3.933333E-01 F( 2) = 3.933333E-01 F( 3) = 3.933333E-01 F( 4) = 3.933333E-01 F( 5) = 3.933333E-01
F( 6) = 3.933333E-01 F( 7) = 3.933333E-01 F( 8) = 3.933333E-01

DYSLIM SIMULATION PROGRAM

OPTIMAL CONTROL PARAMETER COMBINATION

Table with columns: TIME, Y( 1), Y( 2), Y(10), Y(19), Y(15), Y(25), Y( 7), Y(16), Y(27). Rows contain numerical data for simulation steps from 0.000E 00 to 8.800E 00.

DYSIMP SIMULATION PROGRAM		OPTIMAL CONTROL PARAMETER COMBINATION								PAGE 3 OF RUN 1	
TIME	Y(30)	Y(2)	Y(10)	Y(19)	Y(15)	Y(25)	Y(7)	Y(16)	Y(27)		
8.850E 00	4.1749435E 01	3.6032181E 01	3.0000000E 01	4.2305511E-01	1.6509026E 00	2.2000000E 03	1.4548811E 03	1.0082632E 03			
8.900E 00	4.1913544E 01	3.6186110E 01	3.0000000E 01	4.2403901E-01	1.6522816E 00	2.2000000E 03	1.4557361E 03	1.0106897E 03			
8.950E 00	4.2076904E 01	3.6339844E 01	3.0000000E 01	4.2499077E-01	1.6548061E 00	2.2000000E 03	1.4562465E 03	1.0130193E 03			
9.000E 00	4.2239456E 01	3.6492737E 01	3.0000000E 01	4.2590851E-01	1.6566963E 00	2.2000000E 03	1.4568073E 03	1.0152561E 03			
9.050E 00	4.2395782E 01	3.6639206E 01	3.0000000E 01	4.2677903E-01	1.6584778E 00	2.2000000E 03	1.4573464E 03	1.0172703E 03			
9.100E 00	4.2538803E 01	3.6773376E 01	3.0000000E 01	4.2760146E-01	1.6601419E 00	2.2000000E 03	1.4572342E 03	1.0191030E 03			
9.150E 00	4.2670578E 01	3.6896698E 01	3.0000000E 01	4.2832275E-01	1.6617012E 00	2.2000000E 03	1.4575088E 03	1.0207820E 03			
9.200E 00	4.2792725E 01	3.7000000E 01	3.0000000E 01	4.2912859E-01	1.6631660E 00	2.2000000E 03	1.4577631E 03	1.0223303E 03			
9.250E 00	4.2906586E 01	3.7000000E 01	3.0000000E 01	4.2984182E-01	1.6645451E 00	2.2000000E 03	1.4579983E 03	1.0237644E 03			
9.300E 00	4.3013321E 01	3.7000000E 01	3.0000000E 01	4.3052441E-01	1.6658459E 00	2.2000000E 03	1.4582175E 03	1.0250955E 03			
9.350E 00	4.3113907E 01	3.7000000E 01	3.0000000E 01	4.3117744E-01	1.6670732E 00	2.2000000E 03	1.4584215E 03	1.0263347E 03			
9.400E 00	4.3209198E 01	3.7000000E 01	3.0000000E 01	4.3180168E-01	1.6682329E 00	2.2000000E 03	1.4586122E 03	1.0274922E 03			
9.450E 00	4.3298811E 01	3.7000000E 01	3.0000000E 01	4.3239748E-01	1.6693287E 00	2.2000000E 03	1.4587911E 03	1.0285769E 03			
9.500E 00	4.3384581E 01	3.7000000E 01	3.0000000E 01	4.3290516E-01	1.6703653E 00	2.2000000E 03	1.4589594E 03	1.0295964E 03			
9.550E 00	4.3464218E 01	3.7000000E 01	3.0000000E 01	4.3349814E-01	1.6713161E 00	2.2000000E 03	1.4590980E 03	1.0304346E 03			
9.600E 00	4.3526108E 01	3.7000000E 01	3.0000000E 01	4.3400016E-01	1.6721792E 00	2.2000000E 03	1.4592184E 03	1.0311467E 03			
9.650E 00	4.3578490E 01	3.7000000E 01	3.0000000E 01	4.3447846E-01	1.6729650E 00	2.2000000E 03	1.4593193E 03	1.0317559E 03			
9.700E 00	4.3612717E 01	3.7000000E 01	3.0000000E 01	4.3493682E-01	1.6736851E 00	2.2000000E 03	1.4594059E 03	1.0322805E 03			
9.750E 00	4.3641266E 01	3.7000000E 01	3.0000000E 01	4.3537843E-01	1.6743441E 00	2.2000000E 03	1.4594791E 03	1.0327344E 03			
9.800E 00	4.3662018E 01	3.7000000E 01	3.0000000E 01	4.3580514E-01	1.6749487E 00	2.2000000E 03	1.4595411E 03	1.0331260E 03			
9.850E 00	4.3676178E 01	3.7000000E 01	3.0000000E 01	4.3621790E-01	1.6755047E 00	2.2000000E 03	1.4595932E 03	1.0334629E 03			
9.900E 00	4.3684753E 01	3.7000000E 01	3.0000000E 01	4.3661726E-01	1.6760149E 00	2.2000000E 03	1.4596366E 03	1.0337505E 03			
9.950E 00	4.3688568E 01	3.7000000E 01	3.0000000E 01	4.3700349E-01	1.6764841E 00	2.2000000E 03	1.4596705E 03	1.0339946E 03			
1.000E 01	4.3688370E 01	3.7000000E 01	3.0000000E 01	4.3737674E-01	1.6769142E 00	2.2000000E 03	1.45970059E 03	1.0342000E 03			
1.005E 01	4.3680098E 01	3.7000000E 01	3.0000000E 01	4.3773019E-01	1.6772981E 00	2.2000000E 03	1.45970815E 03	1.0342744E 03			
1.010E 01	4.3658569E 01	3.7000000E 01	3.0000000E 01	4.3806481E-01	1.6776009E 00	2.2000000E 03	1.45970269E 03	1.0342698E 03			
1.015E 01	4.3626038E 01	3.7000000E 01	3.0000000E 01	4.3838412E-01	1.6778641E 00	2.2000000E 03	1.4596830E 03	1.0341999E 03			
1.020E 01	4.3584518E 01	3.7000000E 01	3.0000000E 01	4.3869221E-01	1.6780834E 00	2.2000000E 03	1.4596543E 03	1.0340759E 03			
1.025E 01	4.3535538E 01	3.7000000E 01	3.0000000E 01	4.3899077E-01	1.6782656E 00	2.2000000E 03	1.45961834E 03	1.0339119E 03			
1.030E 01	4.3480362E 01	3.7000000E 01	3.0000000E 01	4.3928081E-01	1.6784124E 00	2.2000000E 03	1.45957368E 03	1.0337001E 03			
1.035E 01	4.3420029E 01	3.7000000E 01	3.0000000E 01	4.3956333E-01	1.6785288E 00	2.2000000E 03	1.45952299E 03	1.0334646E 03			
1.040E 01	4.3358569E 01	3.7000000E 01	3.0000000E 01	4.3984047E-01	1.6786009E 00	2.2000000E 03	1.45947496E 03	1.0331958E 03			
1.045E 01	4.3287170E 01	3.7000000E 01	3.0000000E 01	4.4010699E-01	1.6786814E 00	2.2000000E 03	1.45940444E 03	1.0328989E 03			
1.050E 01	4.3215942E 01	3.7000000E 01	3.0000000E 01	4.4036859E-01	1.6787224E 00	2.2000000E 03	1.45933831E 03	1.0325478E 03			
1.055E 01	4.3135757E 01	3.7000000E 01	3.0000000E 01	4.4061720E-01	1.6787178E 00	2.2000000E 03	1.45924971E 03	1.0321130E 03			
1.060E 01	4.3039536E 01	3.7000000E 01	3.0000000E 01	4.4085449E-01	1.6786718E 00	2.2000000E 03	1.45914658E 03	1.0315840E 03			
1.065E 01	4.2930145E 01	3.7000000E 01	3.0000000E 01	4.4108474E-01	1.6785860E 00	2.2000000E 03	1.45903225E 03	1.0309750E 03			
1.070E 01	4.2809937E 01	3.6912933E 01	3.0000000E 01	4.4130999E-01	1.6784716E 00	2.2000000E 03	1.45890737E 03	1.0303381E 03			
1.075E 01	4.2680862E 01	3.6781631E 01	3.0000000E 01	4.4153273E-01	1.6783266E 00	2.2000000E 03	1.45877532E 03	1.0296431E 03			
1.080E 01	4.2544449E 01	3.6642334E 01	3.0000000E 01	4.4175279E-01	1.6781588E 00	2.2000000E 03	1.45863342E 03	1.0289242E 03			
1.085E 01	4.2401932E 01	3.6497025E 01	3.0000000E 01	4.4197190E-01	1.6779661E 00	2.2000000E 03	1.45848674E 03	1.0281528E 03			
1.090E 01	4.2254318E 01	3.6346344E 01	3.0000000E 01	4.4218880E-01	1.6777534E 00	2.2000000E 03	1.45833054E 03	1.0273665E 03			
1.095E 01	4.2102386E 01	3.6191238E 01	3.0000000E 01	4.4240487E-01	1.6775208E 00	2.2000000E 03	1.45817015E 03	1.0265344E 03			
1.100E 01	4.1946793E 01	3.6032649E 01	3.0000000E 01	4.4261891E-01	1.6772709E 00	2.2000000E 03	1.45800584E 03	1.0256909E 03			
1.105E 01	4.1785172E 01	3.5867859E 01	2.9934682E 01	4.4282877E-01	1.6769924E 00	2.2000000E 03	1.45782346E 03	1.0247546E 03			
1.110E 01	4.1614517E 01	3.5694595E 01	2.9804459E 01	4.4303501E-01	1.6766853E 00	2.2000000E 03	1.45762489E 03	1.0237593E 03			
1.115E 01	4.1436401E 01	3.5513885E 01	2.9663010E 01	4.4323844E-01	1.6763535E 00	2.2000000E 03	1.45743394E 03	1.0227239E 03			
1.120E 01	4.1252106E 01	3.5327271E 01	2.9515915E 01	4.4343978E-01	1.6759949E 00	2.2000000E 03	1.45722727E 03	1.0216252E 03			
1.125E 01	4.1062437E 01	3.5135605E 01	2.9346227E 01	4.4363886E-01	1.6756163E 00	2.2000000E 03	1.45701233E 03	1.0204998E 03			
1.130E 01	4.0864805E 01	3.4939697E 01	2.9208664E 01	4.4383603E-01	1.6752138E 00	2.2000000E 03	1.45679000E 03	1.0193105E 03			
1.135E 01	4.0671249E 01	3.4740372E 01	2.9049606E 01	4.4403112E-01	1.6747913E 00	2.2000000E 03	1.45656199E 03	1.0180881E 03			
1.140E 01	4.0470520E 01	3.4538101E 01	2.8887878E 01	4.4422382E-01	1.6743479E 00	2.2000000E 03	1.45632632E 03	1.0168208E 03			
1.145E 01	4.0267014E 01	3.4333374E 01	2.8723633E 01	4.4441402E-01	1.6738844E 00	2.2000000E 03	1.45608411E 03	1.0155034E 03			
1.150E 01	4.0061081E 01	3.4126556E 01	2.8557327E 01	4.4460142E-01	1.6734018E 00	2.2000000E 03	1.45583562E 03	1.0141506E 03			
1.155E 01	3.9848007E 01	3.3912537E 01	2.8385147E 01	4.4478190E-01	1.6728840E 00	2.2000000E 03	1.45556265E 03	1.0126563E 03			
1.160E 01	3.9621626E 01	3.3686447E 01	2.8202927E 01	4.4495702E-01	1.6723280E 00	2.2000000E 03	1.45528037E 03	1.0110537E 03			
1.165E 01	3.9384949E 01	3.3444985E 01	2.8012409E 01	4.4512743E-01	1.6717424E 00	2.1945137E 03	1.44497910E 03	1.0093911E 03			

DYSIMP SIMULATION PROGRAM		OPTIMAL CONTROL PARAMETER COMBINATION								PAGE 4 OF RUN 1	
TIME	Y(30)	Y(2)	Y(10)	Y(19)	Y(15)	Y(25)	Y(7)	Y(16)	Y(27)		
1.170E 01	3.9159434E 01	3.3204025E 01	2.7815125E 01	4.4529444E-01	1.6711245E 00	2.1862075E 03	1.44466462E 03	1.0076411E 03			
1.175E 01	3.8886551E 01	3.2951416E 01	2.7611729E 01	4.4545847E-01	1.6707679E 00	2.1776021E 03	1.44433718E 03	1.0058157E 03			
1.180E 01	3.8627800E 01	3.2692993E 01	2.7403366E 01	4.4561952E-01	1.6694800E 00	2.1687033E 03	1.44399678E 03	1.0039250E 03			
1.185E 01	3.8364120E 01	3.2429688E 01	2.7190811E 01	4.4577748E-01	1.6680950E 00	2.1595278E 03	1.44364258E 03	1.0019475E 03			
1.190E 01	3.8096268E 01	3.2162247E 01	2.6974442E 01	4.4593221E-01	1.6666307E 00	2.1500781E 03	1.44327483E 03	9.9988916E 02			
1.195E 01	3.7824814E 01	3.1891327E 01	2.6756898E 01	4.4608343E-01	1.6650987E 00	2.1403635E 03	1.44289355E 03	9.9775830E 02			
1.200E 01	3.7550247E 01	3.1617477E 01	2.6532715E 01	4.4623083E-01	1.6636861E 00	2.1303909E 03	1.44249883E 03	9.9554663E 02			

DYSIMP SIMULATION PROGRAM

OPTIMAL CONTROL PARAMETER COMBINATION

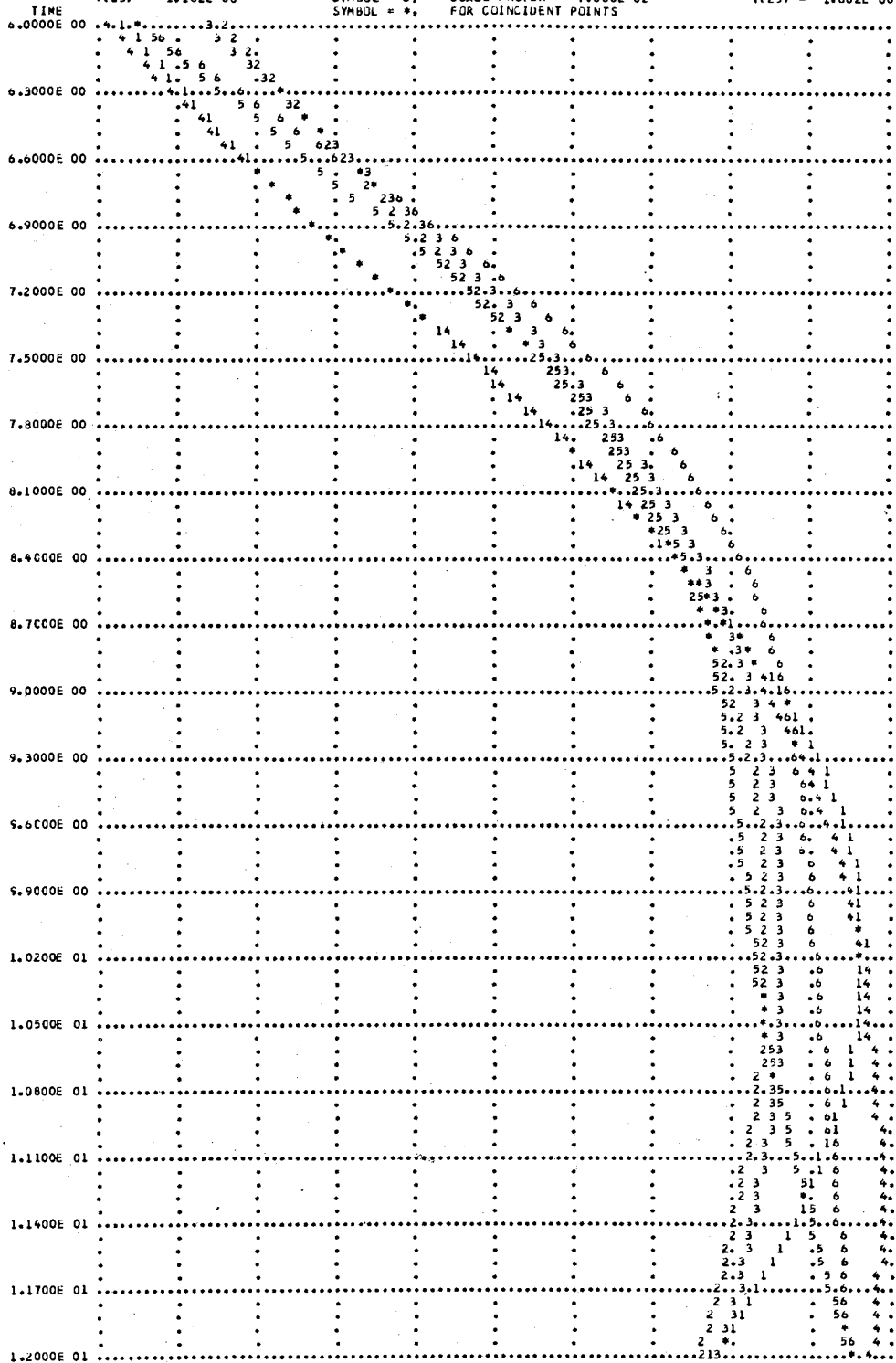
Y(1) = 2.131E 01	SYMBOL = 1,	SCALE FACTOR = 1.000E 00	Y(1) = 3.131E 01
Y(9) = 1.197E 01	SYMBOL = 2,	SCALE FACTOR = 1.000E 00	Y(9) = 2.197E 01
Y(18) = 4.284E 00	SYMBOL = 3,	SCALE FACTOR = 8.000E-01	Y(18) = 1.728E 01
Y(4) = 2.390E 01	SYMBOL = 4,	SCALE FACTOR = 3.000E 00	Y(4) = 5.390E 01
Y(12) = 2.809E 01	SYMBOL = 5,	SCALE FACTOR = 3.000E 00	Y(12) = 5.809E 01
Y(21) = 2.455E 01	SYMBOL = 6,	SCALE FACTOR = 2.000E 00	Y(21) = 4.455E 01

TIME	FOR COINCIDENT POINTS									
6.0000E 00	1	32	64	5						
6.3000E 00	1		46	5						
6.6000E 00	1		23	4	65					
6.9000E 00	1		23	4	65					
7.2000E 00	1		23	4	65					
7.5000E 00	1		23	4	65					
7.8000E 00	1		65	2	34					
8.1000E 00	1		65	2	34					
8.4000E 00	1		65	2	34					
8.7000E 00	1		65	2	34					
9.0000E 00	1		65	2	34					
9.3000E 00	1		65	2	34					
9.6000E 00	1		65	2	34					
9.9000E 00	1		65	2	34					
1.0200E 01	1		65	2	34					
1.0500E 01	1		65	2	34					
1.0800E 01	1		65	2	34					
1.1100E 01	1		65	2	34					
1.1400E 01	1		65	2	34					
1.1700E 01	1		65	2	34					
1.2000E 01	1		65	2	34					

DYSIPP SIMULATION PROGRAM

OPTIMAL CONTROL PARAMETER COMBINATION

Y( 5) = 8.399E-01	SYMBOL = 1,	SCALE FACTOR = 6.000E-02	Y( 5) = 1.440E 00
Y(13) = 1.844E 00	SYMBOL = 2,	SCALE FACTOR = 3.000E-01	Y(13) = 4.844E 00
Y(22) = 2.155E 00	SYMBOL = 3,	SCALE FACTOR = 3.000E-01	Y(22) = 5.155E 00
Y( 6) = 4.539E-01	SYMBOL = 4,	SCALE FACTOR = 7.000E-02	Y( 6) = 1.154E 00
Y(14) = 5.183E-01	SYMBOL = 5,	SCALE FACTOR = 7.000E-02	Y(14) = 1.218E 00
Y(23) = 1.102E 00	SYMBOL = 6,	SCALE FACTOR = 7.000E-02	Y(23) = 1.802E 00





VITA

Gregory Dean Martin

Candidate for the Degree of

Master of Science

Thesis: OPTIMAL CONTROL OF AN OIL REFINERY WASTE TREATMENT FACILITY:  
A TOTAL ECOSYSTEM APPROACH

Major Field: Mechanical Engineering

Biographical:

Personal Data: Born in Oklahoma City, Oklahoma, January 21, 1949,  
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the requirements for the degree of Master of Science in May,  
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Professional Experience: Special Technical Student, Western Elec-  
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to date.

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sional Engineers, Oklahoma Society of Professional Engineers  
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Institute of Aeronautics and Astronautics, Pi Tau Sigma, and  
Sigma Tau.