SYNTHESIS TECHNIQUE FOR THE COMPENSATION OF

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ELECTROHYDRAULIC SERVOSYSTEMS WITH

DYNAMIC PRESSURE FEEDBACK

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1977

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Thesis Approved:

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NOMENCLATURE

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ABS	= Absolute Value
AE	= Cross-sectional area of spool exposed to P_3 and P_4 (in ²)
AF	= Cross-sectional area of spool exposed to P_1 and P_2 (in ²)
AG	= Area of mechanical dynamic pressure feedback piston exposed to P_1 and P_2 (in ²)
АР	= Area of mechanical dynamic pressure feedback piston exposed to P_5 and P_6 (in ²)
β	= Bulk modulus of fluid $(1b_f/in^2)$
C _D	= Orifice discharge coefficient
C _F	= Friction coefficient of the actuator
c _R	= Radial clearance between valve spool and sleeve (in)
C _S	= Slip flow coefficient of the actuator
C _{DM}	= Viscous drag coefficient of the actuator
C _V	= Velocity coefficient of the steady state flow force
D ₁	= Diameter of flapper nozzle control orifice (in)
D ₂	= Diameter of valve spool (in)
D ₃	= Diameter of fixed orifice upstream from flapper nozzle (in)
D4	= Diameter of spool area exposed to P_1 and P_2 (in)
D ₅	= Diameter of mechanical dynamic pressure feedback piston exposed to P ₅ and P ₆ (in)
D ₆	= Diameter of mechanical dynamic pressure feedback piston exposed to P_1 and P_2 (in)
D ₇	= Diameter of flapper nozzle orifice for dynamic pressure feedback control (in)
D _M	= Volumetric displacement of the actuator (in ³ /rad)

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DSET	=	Minimum desired response settling time (secs)
F ₁	=	Pressure force acting on flapper nozzle valve (1 ${ t b_f}$)
^F 2	=	Pressure force acting on flapper nozzle valve from mechanical dynamic pressure feedback unit (lb _f)
Fs	=	Spring force (1b _f)
^F T	=	Torquemotor force (1b _f)
Fv	=	Viscous damping force on valve spool (1b _f)
^F ss1, ^F ss2	=	Steady state flow forces (1b _f)
FOBJ	=	Objective function for minimization
i	=	Subscript indicating initial conditions
I	=	Step input to the system (volts)
II	=	Error signal to servoamplifier (volts)
J	=	Polar moment of inertia of the actuator (in $lb_f sec^2/rad$)
к ₁	=	Torquemotor constant (lb _f /ma)
к2	=	Torquemotor constant (lb _f /in)
к ₃	=	Spring constant of cantilever spring (lb _f /in)
К4	=	Spring constant of mechanical dynamic pressure feedback unit (lb_f/in)
ĸ _A	=	Servoamplifier gain (ma/volt)
к _D	=	Dynamic pressure feedback gain (volts in ² /1b _f)
К _F	=	Position feedback gain (volts/rad)
ĸ _P	=	Pressure feedback gain (volts in ² /lb _f)
ĸ _v	=	Servovalve gain (in/ma)
L'	=	Distance between ports for unsteady flow forces (in)
L _D	=	Spool length for viscous damping (in)
М	=	Mass of valve spool (1b _f sec ² /in)
^P 1, ^P 2	=	Load line pressures (lb _f /in ²)
^P 3, ^P 4	=	Spool control pressures (1b _f /in ²)

^P 5' ^P 6	<pre>= Pressures of mechanical dynamic pressure feedback unit (lb_f/in²)</pre>
P _D	= Dynamic pressure feedback (1b _f /in ²)
P _E	= Exhaust pressure (1b _f /in ²)
P _M	= Differential pressure of load lines $(1b_f/in^2)$
P _S	= Supply pressure (lb _f /in ²)
ρ	= Fluid density (1b _f sec ² /in ⁴)
Q_1, Q_2	= Volumetric flow through the servovalve (in ³ /sec)
Q ₃ , Q ₄	
Q_A , Q_F	<pre>= Volumetric flow through pilot stage fixed orifices (in³/sec)</pre>
Q _C , Q _D	= Volumetric flow through flapper nozzles (in ³ /sec)
$Q_{\rm H}$, $Q_{\rm J}$	= Volumetric flow from mechanical dynamic pressure feed- back unit (in ³ /sec)
Q _M	= Volumetric flow through servovalve, linearized model (in ³ /sec)
S	= Laplace variable, transformation with respect to time
s ₁ , s ₂ , s ₃ , s ₄ s ₅	<pre>Switches used for simulating the uncompensated system, mechanical pressure feedback system, electrical = pressure feedback system, mechanical dynamic pressure feedback system, and electrical dynamic pressure feed- back system, respectively</pre>
s _s	= Static stiffness (in lb _f /rad)
TL	= Load torque applied to actuator (in lb _f)
TSET	= System response settling time (secs)
τ	= Time constant of dynamic pressure feedback element (secs)
θ	= Angular displacement of the actuator (rad)
μ	= Fluid absolute viscosity (1b _f sec/in ²)
v ₁ , v ₂	= Volume of fluid under compression in right and left load lines (in ³)
Visd	= Viscous drag external to the actuator (in lb_f sec)

X = Displacement of the torquemotor (in)

 X_0 = Displacement of flapper nozzle valve at null (in)

- Y = Displacement of the valve spool (in)
- Y₀ = Effective length of the volume of oil at the right and left ends of spool (in)
- Z = Displacement of mechanical dynamic pressure feedback unit (in)

CHAPTER I

INTRODUCTION

Background

Electrohydraulic servosystems are used in many controls applications requiring position control with fast dynamic response and high stiffness. Such servosystems basically consist of a servoamplifier, servovalve, actuator, transmission lines to connect the servovalve and actuator, and a feedback mechanism to produce a position type system as Figure 1 illustrates.



Figure 1. Schematic Diagram of Electrohydraulic Position Control Servosystem

Three important criteria used to define servosystem performance are speed of response, degree of stability, and static stiffness. Speed of response and degree of stability are dynamic performance measures which can be characterized by the system rise time and settling time respectively, assuming a time-domain step input to the system. Static stiffness is a direct function of the loop gain.

Servosystem designers often compromise on one or more of the performance criteria in order to obtain acceptable system performance. It is not unusual for electrohydraulic servosystems to be lightly damped. As the servosystem loop gain is increased to meet the static stiffness performance criterion, the speed of response improves as well but this occurs at the expense of degree of stability. Often, instability results for the system loop gains which are high enough to provide adequate static stiffness.

Electrohydraulic servovalves used in a position control system typically have minimum radial clearance and underlap or overlap. These servovalves operate near the origin of the steady-state valve characteristics (pressure-flow-displacement curves) when there is no external load force applied to the system actuator. Near the origin of the steady-state valve characteristics, the slope of the curves is essentially zero. This slope is an important factor which influences the damping or degree of stability of the servosystem; for low values of slope, low damping results unless damping is provided by other means. Typical valve characteristics are shown in Figure 2.

Various means of damping enhancement such as valve spool underlap, actuator by-pass leakage, and pressure feedback have been devised to obtain better dynamic performance. The greater the valve underlap,

by-pass leakage, or pressure feedback, the steeper the effective slopes of the valve characteristic curves in the vicinity of the origin: a greater damping results. An example of the influence of valve underlap on the characteristic curves is shown in Figure 3. For all realizable values of pressure, flow, and displacement, the curves have a non-zero slope. For operation near the origin of the valve characteristic curves, the system damping is greater than in the case of a valve with minimum underlap.



Figure 2. Steady-State Valve Characteristics, Zero-Lap Valve



Figure 3. Steady-State Valve Characteristics, Maximum Valve Underlap

The introduction of damping enhancement in the system improves the degree of stability but often compromises other performance measures. Spool underlap is a simple means of enhancing damping, but it results in quiescent power loss. Flow passes through the system regardless of demand. Actuator by-pass leakage enhances damping also, but at the expense of reduction in power delivered to the load. Addition of external load damping results in the same effect. Pressure feedback produces enhanced damping without quiescent power loss. A loss of static stiffness results with the implementation of any of the above damping enhancement methods.

Advancements have been made in electrohydraulic servosystem performance through the utilization of dynamic pressure feedback. Realizable increases in performance can be produced with dynamic pressure feedback if the resulting complexity can be accepted. The appealing feature of dynamic pressure feedback is that it is active only during the transient period when damping is required. Feedback is attenuated or non-existant during steady-state operation. Thus, static stiffness is not affected but stability is enhanced. Dynamic pressure feedback is functionally a high pass filter.

Moog, Inc., has done much work with electrohydraulic servosystem design as documented by Geyer (5). Measured frequency responses for electrohydraulic position control systems with and without damping enhancement are shown in Figures 4 through 7. In all four systems, the amplifier gain was set to achieve a peak amplitude ratio of 1.25 (±2 db). In the last three cases additional damping was introduced to produce an equivalent load damping ratio of 0.6. Static stiffness for those four systems was measured by applying an external force and measuring the load deflection. A summary of results from the tests can be found in Table I. The servosystem which utilized dynamic pressure feedback produced the best dynamic and static performance.

Limited information is available in the open literature concerning the optimum design of systems with dynamic pressure feedback. Geyer (5) discussed static stiffness determination through loop gain adjustment and suggested setting the dynamic pressure feedback element time constant such that the corner frequency is about one-third the actuator-load natural frequency. Morse (9) recommended setting the corner frequency of the feedback element about a decade below the actuator-load natural frequency. An objective of this thesis was to develop a logical procedure for selecting the time constant.













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Servo Configuration	Bandwidth (±2 hz	2db) 90° Phase Lag hz	Static Load Stiffness lb _f /in
Flow Control Servovalve	0.15	0.37	9,000
Flow Control Servovalve With Bypass Orifice	8.8	5.0	5,100
PQ Servovalve	8.8	5.0	2,500
DPF Servovalve	9.2	5.0	60,000

VARIOUS POSITION SERVOS PERFORMANCE COMPARISON

Problem Statement and Scope of Study

Through the course of this study it was assumed that the basic electrohydraulic position control servosystem had already been designed and the only parameter of that servosystem which remained undetermined was the loop gain. Further, it was assumed that the system was lightly damped such that when the loop gain was increased to provide adequate static stiffness, the system transient response was too oscillatory to be useful.

The problem was to develop a logical procedure for synthesizing a dynamic pressure feedback network for compensating a lightly damped, electrohydraulic position control servosystem. The synthesis required the determination of the servosystem loop gain as well as the feedback network time constant and gain such that the three important performance criteria, static stiffness, speed of response, and degree of stability, were satisfied.

The scope of this study included:

- Derivation of a mathematical model of the existing servosystem. Due to the nature of the physical processes involved, the model includes non-linear and linear algebraic and differential equations.
- 2. Computer simulation of the basic servosystem utilizing the non-linear mathematical model. The model was structured such that the user could add mechanical and electrical pressure feedback as well as mechanical and electrical dynamic pressure feedback.
- 3. Computer simulation of the basic system utilizing a linearized mathematical model. This model was structured such that the user could add mechanical and electrical pressure feedback as well as mechanical and electrical dynamic pressure feedback.
- Validation of the models via laboratory measurements. An actual system was available in the School of Mechanical and Aerospace Engineering Systems Laboratory.
- 5. Development of a procedure to synthesize a dynamic pressure feedback network to enhance the damping of a lightly damped, electrohydraulic, position control servosystem.

Summary

A synthesis technique was developed to add dynamic pressure feedback to a lightly damped, electrohydraulic position control servosystem. In this technique the static stiffness is first satisfied and then the pressure feedback gain and time constant of the dynamic pressure feedback element are sized to satisfy the dynamic performance criteria. It is assumed that the parameters required can be achieved in actual hardware; otherwise design compromises have to be made.

The synthesis procedure is sequential. At each step of the synthesis procedure, results are compared with design specifications. If the specifications cannot be satisfied, design compromises must be made. The steps in the procedure are:

- The loop gain is determined such that the static stiffness performance criterion is satisfied.
- 2. The pressure feedback gain is determined to provide the maximum degree of stability for the system (this performance measure is characterized by the transient response settling time). For reasons explained in Chapter III, the feedback element time constant is set to infinity for this determination.
- 3. The time constant is reduced from infinity until the response settling time is equal to the maximum allowable value. Evaluate the transient speed of response (performance measure characterized by response rise time).

The feedback element corner frequency (reciprocal of time constant) range of one-third to one-tenth the actuator-load open-loop natural frequency suggested by Geyer (5) and Morse (9) did not have any particular significance in the above procedure. It appears that the time constant range could be attributed to practical limitations of hardware implementation using a mechanical, dynamic pressure feedback network.

CHAPTER II

MODEL FORMULATION

Modelling Assumptions

A system model can become unduly complex unless simplifying assumptions are made which eliminate higher order effects. Care must be exercised in making assumptions so that a loss of pertinent information does not occur. The assumptions employed in developing the models are:

- 1. The valve is symmetrical with no underlap or overlap.
- The steady-state orifice equation holds for each orifice and all discharge coefficients are constant and equal.
- All connecting passages are short in length and large in diameter, i.e., resistance and "transmission line" effects are negligble.
- 4. The supply and exhaust pressures are constant.
- The temperature, viscosity, and bulk modulus of the fluid are constant.
- 6. The change of fluid density is small compared to the density of the fluid itself. The time rate of change in density is not negligble, i.e., compressibility effects are important.
- 7. Static equations describe the torquemotor and mechanical high pass filter because their dynamics are of high enough order to be considered insignificant.

 The steady-state flow force jet angle is assumed to be constant.

System Equations

Five electrohydraulic servosystem models are developed in this section. All five models describe the same basic servosystem. One model incorporates no means of damping enhancement. The other four models incorporate damping enhancement via pressure or dynamic pressure feedback. The basic servosystem is described first since it is the basis for the remaining models. The additions and changes to the basic system equations required to describe the other four models are documented separately. Terms used in describing equations can be referenced in the section titled "Nomenclature".

Basic Servosystem

A schematic diagram of the basic servosystem is shown in Figure 8. The describing equations are as follows:

Servoamplifier error signal:

$$II = I - K_{\mu} \cdot \theta \tag{2.1}$$

Pilot stage flapper-nozzle valve force:

$$F_1 = 0.25 \cdot \pi \cdot D_1^2 \cdot (P_3 - P_4)$$
(2.2)

Cantilever spring force:

 $F_{S} = K_{3} \cdot (X - Y)$ (2.3)

Torquemotor force:

 $F_{T} = K_{1} \cdot II - K_{2} \cdot X \tag{2.4}$

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Figure 8. Schematic Diagram of Basic Servosystem

Flapper-nozzle valve orifice flow rates:

$$Q_{A} = 0.25 \cdot \pi \cdot D_{3}^{2} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{S} - P_{3})^{\frac{1}{2}}$$
(2.5)

$$Q_{C} = \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} + X) \cdot (P_{3} - P_{E})^{\frac{1}{2}}$$
(2.6)

$$Q_{F} = \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} - X) \cdot (P_{4} - P_{E})^{\frac{1}{2}}$$
(2.7)

$$Q_{\rm D} = 0.25 \cdot \pi \cdot D_3^2 \cdot C_{\rm D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{\rm S} - P_4)^{\frac{1}{2}}$$
(2.8)

Spool end chamber continuity:

$$\frac{dP_3}{dt} = \frac{\beta}{(Y_0 + Y)} \left(\frac{Q_A - Q_C}{AE} - \frac{dY}{dt} \right)$$
(2.9)

$$\frac{dP_4}{dt} = \frac{\beta}{(Y_0 - Y)} \left(\frac{Q_D - Q_F}{AE} + \frac{dY}{dt} \right)$$
(2.10)

Spool valve flow rates for X > 0:

$$Q_{2} = \pi \cdot D_{2} \cdot C_{D} \cdot Y \cdot [2 \cdot (P_{S} - P_{1})/\rho]^{\frac{1}{2}}$$
(2.11)

$$Q_{3} = \pi \cdot D_{2} \cdot C_{D} \cdot Y \cdot [2 \cdot (P_{2} - P_{E})/\rho]^{\frac{1}{2}}$$
(2.12)

Spool valve flow rates for X < 0:

$$Q_1 = -\pi \cdot D_2 \cdot C_D \cdot Y \cdot [2 \cdot (P_S - P_2)/\rho]^{\frac{1}{2}}$$
(2.13)

$$Q_{4} = -\pi \cdot D_{2} \cdot C_{D} \cdot Y \cdot [2 \cdot (P_{1} - P_{E}) / \rho]^{\frac{1}{2}}$$
(2.14)

Actuator chamber continuity:

$$\frac{dP_1}{dt} = \frac{\beta}{V_1} \left(D_M \cdot \frac{d\theta}{dt} + \frac{C_S \cdot D_M \cdot P_M}{\mu} - Q_{2,4} \right)$$
(2.15)

$$\frac{dP_2}{dt} = \frac{\beta}{v_2} \left(Q_{3,1} - D_M \cdot \frac{d\theta}{dt} - \frac{C_S \cdot D_M \cdot P_M}{\mu} \right)$$
(2.16)

Viscous damping force:

$$F_{V} = \frac{\pi \cdot \mu \cdot D_{2} \cdot L_{D}}{C_{R}} \cdot \frac{dY}{dt}$$
(2.17)

Steady-state flow forces on the valve spool:

$$F_{SS1} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot Y \cdot (P_1 - P_E + P_M) \cdot \cos 69^\circ$$
(2.18)

$$F_{SS2} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot Y \cdot (P_1 - P_E - P_M) \cdot \cos 69^\circ$$
(2.19)

Unsteady flow forces on the valve spool for X > 0:

$$F_{\text{US1}} = \rho^{\frac{1}{2}} LC_{\text{D}} \pi D_{2} \{ [2(P_{\text{S}} - P_{1})]^{\frac{1}{2}} \cdot \frac{dY}{dt} - \frac{1}{2} \cdot Y[2(P_{\text{S}} - P_{1})]^{-\frac{1}{2}} \cdot \frac{dP_{1}}{dt} \}$$
(2.20)

$$F_{\text{US2}} = -\rho^{\frac{1}{2}} LC_{\text{D}} \pi D_{2} \{ [2(P_{2} - P_{\text{E}})]^{\frac{1}{2}} \cdot \frac{dY}{dt} + \frac{1}{2} Y [2(P_{2} - P_{\text{E}})]^{-\frac{1}{2}} \cdot \frac{dP_{2}}{dt} \}$$
(2.21)

Unsteady flow forces on the valve spool for X < 0:

$$F_{\text{US1}} = -\rho^{\frac{1}{2}} LC_{\text{D}} \pi D_{2} \{ [2(P_{1} - P_{\text{E}})]^{\frac{1}{2}} \cdot \frac{dY}{dt} + \frac{1}{2} Y [2(P_{1} - P_{\text{E}})]^{-\frac{1}{2}} \cdot \frac{dP_{1}}{dt} \}$$
(2.22)

$$F_{US2} = \rho^{\frac{1}{2}} LC_{D} \pi D_{2} \{ [2(P_{S} - P_{2})]^{\frac{1}{2}} \cdot \frac{dY}{dt} - \frac{1}{2} Y [2(P_{S} - P_{2})^{-\frac{1}{2}} \cdot \frac{dP_{2}}{dt} \}$$
(2.23)

Valve spool force balance:

$$M \cdot \frac{d^2 Y}{dt^2} = F_S + (P_3 - P_4) \cdot AE + F_{US1} + F_{US2} + F_{SS1} + F_{SS2} - F_V (2.24)$$

Servoactuator torque balance:

$$J \cdot \frac{d^2 \theta}{dt^2} = (1 - C_F) \cdot P_M \cdot D_M - (C_{DM} \cdot D_M \cdot \mu + Visd) \cdot \frac{d\theta}{dt}$$
(2.25)

Basic Servosystem With Mechanical Pressure

Feedback

A schematic diagram of the basic servosystem with mechanical pressure feedback is shown in Figure 9. The system model is

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` Figure 9. Schematic Diagram of Basic Servosystem With Mechanical Pressure Feedback

identical to that of the basic servosystem except for the pressure feedback effect. Equation (2.24) must be modified to include the load differential pressure, P_M , acting on the valve spool force balance as follows:

$$M \cdot \frac{d^2 Y}{dt^2} = F_S + (P_3 - P_4)AE + P_M AF + F_{US1} + F_{US2} + F_{SS1} + F_{SS2} - F_V (2.24a)$$

Equations (2.1) through (2.25), excepting (2.24), remained unchanged to describe the servosystem with mechanical pressure feedback.

Basic Servosystem With Electrical Pressure

Feedback

Equations (2.2) through (2.25) are utilized to describe the servosystem with electrical pressure feedback. The error signal to the amplifier, equation (2.1), must be modified to include an error term proportional to the load differential pressure. The modified equation is as follows:

$$II = I - K_{\rm p} \cdot \theta - K_{\rm p} \cdot P_{\rm M}$$
(2.1a)

A schematic diagram showing the servosystem with electrical pressure feedback is shown in Figure 10.

Basic Servosystem With Mechanical Dynamic

Pressure Feedback

In this case, a "mechanical" high pass filter is added to the basic servosystem as shown schematically in Figure 11. Equations (2.1) through (2.25) are used for this system alteration.

Mechanical dynamic pressure feedback results in the addition of another force on the flapper as follows:



Figure 10. Schematic Diagram of Basic Servosystem With Electrical Pressure Feedback



Figure 11. Schematic Diagram of Servosystem With Mechanical Dynamic Pressure Feedback

$$F_2 = 0.25 \cdot \pi \cdot D_7^2 \cdot (P_5 - P_6)$$
(2.26)

Five additional equations must be added to the basic servosystem model in order to describe the filter. The flow rates into and out of the mechanical high pass filter are described by

$$Q_{\rm H} = \pi \cdot D_7 \cdot C_{\rm D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_0 + X) \cdot (P_5 - P_{\rm E})^{\frac{1}{2}}$$
, and (2.27)

$$Q_{J} = \pi \cdot D_{7} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} - X) \cdot (P_{6} - P_{E})^{\frac{1}{2}}$$
(2.28)

The velocity of the filter piston is

$$\frac{\mathrm{d}Z}{\mathrm{d}t} = \frac{\mathrm{Q}_{\mathrm{H}}}{\mathrm{AP}} = \frac{-\mathrm{Q}_{\mathrm{J}}}{\mathrm{AP}}$$
(2.29)

The force balance on the filter piston for $\frac{dZ}{dt} > 0$ is

$$P_6 \cdot AP = P_M \cdot AG - 2 \cdot K_4 \cdot Z$$
(2.30)

The force balance on the filter piston for $\frac{dZ}{dt} < 0$ is

$$P_{5} \cdot AP = 2 \cdot K_{4} \cdot Z - P_{M} \cdot AG$$
 (2.31)

Basic Servosystem With Electrical Dynamic

Pressure Feedback

A schematic diagram of the servosystem compensated with electrical dynamic pressure feedback is shown in Figure 12. Equations (2.2) through (2.25) are used to describe this system. The error signal to the servoamplifier must be altered to include an additional term. This term is proportional to the feedback passed through the filter. The modified error signal is

$$II = I - K_{\rm F} \cdot \theta - K_{\rm D} \cdot P_{\rm D}$$
 (2.1b)

An additional equation required to describe the electrical high



Figure 12. Schematic Diagram of Servosystem With Electrical Dynamic Pressure Feedback

pass filter is

$$P_{\rm D} = e^{-t/\tau} \frac{dP_{\rm M}}{dt}$$
(2.32)

Linearized Equations

Non-linear system synthesis is not a well established discipline. Most control system synthesis techniques are based on linear system concepts. The synthesis procedure developed in Chapter III is based on a linear system model.

The linearized equations which describe each of the five models are presented separately below. The method used to obtain the linearized equations about the operating point as well as the definition of each linearization constant can be found in Appendix A.

Basic Servosystem

Servoamplifier error signal:	
$II = I + C_1 \cdot \theta$	(2.33)
Pilot stage flapper-nozzle valve force:	
$F_1 = C_2 \cdot (P_3 - P_4)$	(2.34)
Cantilever spring force:	
$F_{S} = C_{23} \cdot (X - Y)$	(2.35)
Torquemotor force:	
$F_{T} = K_{1} \cdot II - K_{2} \cdot X$	(2.36)
Flapper-nozzle valve orifice flow rates:	

$$Q_{A} = C_{6} \cdot P_{3} + C_{7}$$
(2.37)

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$$Q_{\rm C} = C_8 \cdot X + C_9 \cdot P_3 + C_{10}$$
(2.38)

$$Q_F = C_{11} \cdot X + C_{12} \cdot P_4 + C_{13}$$
 (2.39)

$$Q_{\rm D} = C_{14} \cdot P_4 + C_{15} \tag{2.40}$$

Spool end chamber continuity:

$$sP_3 = C_{34} \cdot Y + C_{35} \cdot (Q_A - Q_C) + C_{36} \cdot sY + C_{37}$$
 (2.41)

$$sP_4 = C_{38} \cdot Y + C_{39} \cdot (Q_D - Q_F) + C_{40} \cdot sY + C_{41}$$
 (2.42)

Spool valve flow rate:

$$Q_{\rm M} = C_{69} \cdot Y + C_{70} \cdot P_{\rm M}$$
 (2.43)

Actuator chamber continuity:

$$sP_1 = C_{42} \cdot s\theta + C_{43} \cdot P_M + C_{44} \cdot Q_M$$
 (2.44)

$$sP_2 = C_{45} \cdot s\theta + C_{46} \cdot P_M + C_{47} \cdot Q_M$$
 (2.45)

Viscous damping force:

$$F_{V} = C_{65} \cdot sY \tag{2.46}$$

Steady-state flow forces on the valve spool:

$$F_{SS1} = C_{16} \cdot Y + C_{17} \cdot P_{M} + C_{18}$$
(2.47)

$$F_{SS2} = C_{19} \cdot Y + C_{20} \cdot P_{M} + C_{21}$$
(2.48)

In a well designed value the unsteady flow forces effectively cancel one another. The value utilized in this study was so designed. To avoid additional complication in the linearized model the unsteady flow forces were omitted.

Valve spool force balance:

$$M \cdot s^{2}Y = F_{S} + AE \cdot (P_{3} - P_{4}) + F_{SS1} + F_{SS2} - F_{V}$$
(2.49)

Servoactuator torque balance:

$$J \cdot s^{2} \theta = (1 - C_{F}) \cdot D_{M} \cdot P_{M} - (C_{DM} \cdot D_{M} \cdot \mu + Visd) \cdot s\theta \qquad (2.50)$$
Basic Servosystem With Mechanical Pressure

Feedback

The linear system utilizes equations (2.33) through (2.50) except that equation (2.49) must be modified to include the load differential pressure in the valve spool force balance. The modified force balance is

$$M \cdot s^2 Y = F_S + AE \cdot (P_3 - P_4) + AF \cdot P_M + F_{SS1} + F_{SS2} - F_V$$
 (2.49a)

Basic Servosystem With Electrical Pressure

Feedback

Equations (2.34) through (2.35) are employed in the linear electrical pressure feedback system model. The error signal to the amplifier, equation (2.33), must be modified to include the pressure feedback effect. The modified error equation is

$$II = I + C_{1} \cdot \theta + C_{31} \cdot P_{M}$$
(2.33a)

Basic Servosystem With Mechanical Dynamic

Pressure Feedback

When the "mechanical" high pass filter is added to the servosystem equations (2.33) through (2.50) which describe the basic servosystem remain unchanged. The following equations must be included for the mechanical dynamic pressure feedback system model:

The additional force on the flapper is

$$F_2 = C_{33} \cdot (P_5 - P_6)$$
(2.51)

The flow rates into and out of the mechanical dynamic high pass

filter are

$$Q_{\rm H} = C_{59} \cdot X + C_{60} \cdot P_5 + C_{61}$$
(2.52)

$$Q_J = C_{62} \cdot X + C_{63} \cdot P_6 + C_{64}$$
 (2.53)

The velocity of the filter piston is

$$sZ = \frac{Q_H}{AP} = \frac{-Q_J}{AP}$$
(2.54)

The force balance on the filter piston for $\frac{dZ}{dt}$ > 0 is

$$P_{5} \cdot AP = 2 \cdot K_{4} \cdot Z - P_{M} \cdot AG$$
 (2.55)

The force balance on the filter piston for $\frac{dZ}{dt}$ < 0 is

$$P_6 \cdot AP = P_M \cdot AG - 2 \cdot K_4 \cdot Z$$
 (2.56)

Basic Servosystem With Electrical Dynamic

Pressure Feedback

Equations (2.34) through (2.50) are used to describe the linear system model which incorporated electrical dynamic pressure feedback. Equation (2.33) must be modified to include a term proportional to the signal passed through the high pass filter. The modified error equation is

$$II = I + C_1^{\bullet \theta} + C_{32}^{\bullet} P_D$$
 (2.33b)

The signal passed through the high pass filter is

$$P_{\rm D} = \frac{C_{48}}{\tau_{\rm s} + 1} \cdot {\rm sP}_{\rm M}$$
(2.57)

Simulation Models

The equations which describe the five servosystem models simplify

when advantage is taken of the system symmetry and the equations are linearized about the origin of the valve characteristic curves. When the simplified equations which describe the basic servosystem with or without pressure feedback were combined, an eighth-order, closed-loop transfer function was formed. Equations which describe the dynamic pressure feedback system were combined to produce a ninth-order transfer function. These models were used to observe the system transient response. The linear simulation program presented in Appendix C incorporates these transfer functions.

Model Used in Feedback Network Synthesis

One additional assumption was made to produce the procedure outlined in Chapter III to synthesize the dynamic pressure feedback network to enhance system damping. That assumption was that the dynamics of the servovalve are insignificant compared to other system dynamics. The servovalve could thus be treated as a static gain. The valve gain was obtained by combining equations (2.34) through (2.42) and equations (2.47) through (2.49) with the dynamic terms set equal to zero.

Important actuator and load dynamics include fluid compressibility and load inertia. These dynamics produce a third-order model to describe the basic closed-loop servosystem. The addition of pressure feedback does not change the order of the system model. The transfer function for either case is of the following form:

$$\frac{\theta}{I} = \frac{K}{a_3 s^3 + a_2 s^2 + a_1 s + a_0}$$
(2.58)

Dynamic pressure feedback provided by means of a high-pass filter increases the order of the closed-loop system model to four. The

transfer function is of the following form:

$$\frac{\theta}{I} = \frac{K \cdot (\tau s + 1)}{a_4 s^4 + a_3 s^3 + a_2 s^2 + a_1 a + a_0}$$
(2.59)

Definitions of the constants in equations (2.58) and (2.59) for the three system types are given in Appendix D. Block diagrams for the three system types are shown in Figures 13 through 15. For equations (2.58) and (2.59) the input torque, $T_{\rm I}$, is set equal to zero.

Static Stiffness Determination

System static stiffness was one of the important performance criteria addressed by this study. Referring to Figures 13 through 15, the static stiffness is determined by calculating the steady-state actuator deflection, θ_{SS} , for a given input torque, T_L, and for I=0.

The static stiffness for the systems studied can be calculated using the following equation:

$$S_{S} = \frac{T_{L}}{\theta} = \frac{\frac{\partial Q}{\partial Y} \cdot K_{A} \cdot K_{V} \cdot (1 - C_{F}) \cdot D_{M}}{\frac{C_{S} \cdot D_{M}}{\mu} + \frac{\partial Q}{\partial Y} \cdot K_{A} \cdot K_{V} \cdot K_{P}}$$
(2.60)

For systems which employ only the basic servosystem or the basic servosystem with dynamic pressure feedback, $K_{\rm p}$ is equal to zero.

Experimental Validation of Mathematical Models

The mathematical models presented in this chapter were derived for an actual servosystem. Both the non-linear and linear models were simulated on an IBM 3081D computer using the simulation package CSMP-360 (Continuous System Modelling Program). Program listings of the non-linear and linear model simulations can be found in Appendices



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B and C, respectively.

Without an experimental validation, it remains questionable whether or not the mathematical models adequately describe the positional response of the system to a step input. Further, the initial premise that a linear system approximation can adequately describe the non-linear system remains in question. Both of these questions were answered by comparing measured systems results with the simulation predictions.

A schematic diagram of the test set-up for the experimental study is shown in Figure 16. An electronic function generator was used to provide a time-domain step input to the system. The positional response was measured with a strip-chart recorder. No external load torque was introduced into the system.

Data from the experiment was transferred to a computer data set so that measured results could be plotted directly against simulation results. Figure 17 shows a comparison of the measured results and the computer simulations for the basic servosystem with no additional means of damping enhancement. These results indicate that the linear model is adequate within the range of variables considered.

Comparison of Damping Enhancement Via Pressure and Dynamic Pressure Feedback

The basic premise here and throughout this thesis is as follows: (1) an electrohydraulic position control system has been selected for a given application, (2) all static parameters have been selected except the loop gain, and (3) the open-loop system is so lightly damped that some means of damping enhancement is required. The problem is to





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Figure 17. Comparison of Measured Response and Computer Simulations for the Basic Servosystem

finalize the design of the system so that it will meet defined static stiffness and dynamic response requirements.

To demonstrate the benefits of dynamic pressure feedback two comparisons are presented. Transient system responses for each comparison are shown in Figures 18 and 19. Tables II and III contain system performance measurements for the comparisons shown in Figures 18 and 19, respectively. System parameters utilized in making these comparisons can be found in Appendix F.

The first comparison (see Figure 18) shows the effect on system transient response as one parameter at a time is varied to add a dynamic pressure feedback network to a lightly damped servosystem. For illustration purposes the servoamplifier gain was fixed to provide a specified static stiffness for the basic servosystem as shown in Table II. A low degree of stability often results in the achievement of that static stiffness. Pressure feedback was added to the system without changing the servoamplifier gain; the degree of stability improved but the calculated static stiffness decreased considerably. A high pass filter was then placed in the system pressure feedback. Static stiffness returned to the level of the basic servosystem without damping enhancement with an improved degree of stability.

The second comparison was made among the same three system types discussed above. The comparison was based on each system producing a fifteen percent peak overshoot. Transient response for these systems can be seen in Figure 19 and Table III shows the system performance measurements.

In this case the dynamic pressure feedback system was able to



Figure 18. Comparison of Basic Servosystem, Pressure Feedback System, and Dynamic Pressure Feedback Systems Varying One Parameter at a Time

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Figure 19. Comparison of Basic Servosystem, Pressure Feedback System, and Dynamic Pressure Feedback Systems With Constant Percent Overshoot

TABLE II

COMPARISON OF DYNAMIC PRESSURE FEEDBACK, PRESSURE FEEDBACK, AND BASIC SERVO-SYSTEMS AS ONE PARAMETER IS VARIED AT A TIME

System Type	Servoamplifier Gain ma/volt	Pressure Feedback volts/psi	Time Constant seconds	Static Stiffness in lb _f /rad	Settling Time seconds	Rise Time seconds
Basic	0.450			337	>>0.65	0.037
Pressure Feedback	0.450	3.5×10^{-2}	ω	0.34	0.40	0.132
Dynamic Pressure Feedback	0.450	3.5×10^{-2}	0.5	337	0.49	0.118

TABLE III

COMPARISON OF DYNAMIC PRESSURE FEEDBACK, PRESSURE FEEDBACK, AND BASIC SERVO-SYSTEMS WITH 15% PEAK OVERSHOOT

System Type	Servoamplifier Gain ma/volt	Pressure Feedback volts/psi	Time Constant seconds	Static Stiffness in lb _f /rad	Settling Time seconds	Rise Time seconds
Basic	0.130			97	0.60	0.063
Pressure Feedback	0.450	3.5×10^{-2}	ω	0.34	0.40	0.132
Dynamic Pressure Feedback	0.208	3.5×10^{-2}	0.5	156	0.55	0.132

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have a higher static stiffness and degree of stability than the basic servosystem with no damping enhancement. Pressure feedback produced an improved degree of stability compared to either dynamic pressure feedback or no feedback, but with inferior static stiffness.

In both comparisons it has been shown that a system which utilizes dynamic pressure feedback can provide a static stiffness at least as good as the basic servosystem with a higher degree of stability. A system with dynamic pressure feedback produces a higher static stiffness than a system with pressure feedback. Degree of stability decreases slightly with the addition of the high pass filter to the pressure feedback loop.

CHAPTER III

PROCEDURE FOR DYNAMIC PRESSURE FEEDBACK NETWORK PARAMETER DETERMINATION

Definition of Problem Class

It is assumed that the basic electrohydraulic position control system has been designed to meet all static performance requirements except stiffness. Further, it is assumed that the open-loop servosystem is lightly damped and that an increase in the loop gain to satisfy the system static stiffness requirement results in an unsatisfactory closed-loop dynamic performance. Finally, it is assumed that damping enhancement to improve the closed-loop dynamic performance is to be achieved using dynamic pressure feedback.

Assumptions to Outline Synthesis Procedure

To outline the synthesis procedure, the following assumptions were made:

- The static stiffness requirement can be decoupled from the dynamic performance requirements.
- The system maximum degree of stability occurs with an infinite feedback network time constant.
- 3. For a given loop gain, there is an optimum value of pressure feedback gain which provides the maximum degree of stability

(minimum settling time).

- 4. The pressure feedback gain which provides the maximum degree of stability for an infinite time constant also provides a near optimum degree of stability for a different time constant.
- 5. The loop gain required to provide the desired level of static stiffness is attainable.
- 6. The required pressure feedback gain is attainable.
- The required dynamic pressure feedback network time constant is attainable.

Maximum Degree of Stability Criterion - A Proof

The root locus and root contour concepts underlie the assumptions concerning the maximum degree of stability. A <u>root locus</u> can be plotted for the model of the system as loop gain is increased from zero to infinity. The closed-loop poles for a given loop gain are observed as a particular set of points on the locus. All system parameters not contributing to the loop gain are fixed at some nominal value.

When a parameter other than loop gain is of interest, a separate root locus can be drawn for each constant value of that parameter. Another way to observe the effect of parameters other than loop gain on the closed-loop poles is through a <u>root contour</u>. The effect of a parameter, for example pressure feedback gain, on the closed-loop poles can be observed if another closed-loop transfer function is defined which has the same characteristic equation as the original system. Refer to equation (2.59). The parameter of interest, K_D in this case, must replace loop gain in the transfer function open-loop gain position. The new system has the same stability properties as the original system since the same characteristic equation is used; thus, the eigenvalues are the same as well. Rules for constructing the rootcontour are the same as those employed in constructing the root locus (12).

The new closed-loop transfer function for the dynamic pressure feedback system with pressure feedback gain in the open-loop gain position is

$$1 + GH_{NEW} = 1 + \frac{K_{D} \cdot (b_{3}s^{3} + b_{2}s^{2})}{a_{4}s^{4} + a_{3}s^{3} + a_{2}s^{2} + a_{1}s + a_{0}}$$
(3.1)

The new open-loop transfer function is thus

$$GH_{NEW} = \frac{K_{D} \cdot (b_{3}s^{3} + b_{2}s^{2})}{a_{4}s^{4} + a_{3}s^{3} + a_{2}s^{2} + a_{1}s + a_{0}}$$
(3.2)

Definitions of the constants in Equations (3.1) and (3.2) are given in Appendix D.

Figures 20 through 22 each show a root contour drawn with pressure feedback gain as the adjustable parameter. Three pressure feedback network time constants are considered: infinity, 1.0 second, and 0.2 seconds. These particular time constants were chosen because they are in the vicinity of practical interest for the system under study. These figures were drawn from information obtained in the solution of the example problem in Chapter IV. Initial pole locations for the root contours (denoted by "X" in Figures 20 through 22) were established by setting the loop gain for the basic servosystem with



Figure 20. Root Contour of Dynamic Pressure Feedback Servosystem as Function of Pressure Feedback Gain, $\tau = \infty$



Figure 21. Root Contour of Dynamic Pressure Feedback Servosystem as Function of Pressure Feedback Gain, $\tau = 1.0$ seconds



Figure 22. Root Contour of Dynamic Pressure Feedback Servosystem as Function of Pressure Feedback Gain, $\tau = 0.2$ seconds

with no damping enhancement to provide adequate static stiffness. The uncompensated system is clearly unstable.

The degree of stability, which is characterized by the transient settling time, is a direct function of the real component of each closed loop pole, particularly the dominant complex conjugate pole pair. There is a <u>maximum degree of stability</u> when the dominant complex pair of poles move to their furthermost point in the left half s-plane. A comparison of the three root contours shows that the complex conjugate pair move furthermost to the left with an infinite time constant. As the time constant decreases from infinity, the minimum settling time possible increases.

There is a unique value of pressure feedback gain which produces the minimum settling time in a system with an infinite feedback network time constant. The pressure feedback gain which provides the minimum settling time for a system with a time constant other than infinity is not the same value. However, calculated results in Table IV show that the effect on the degree of stability is small if the pressure feedback gain which provides minimum settling time for an infinite time constant is used when a different time constant is employed.

Dynamic Pressure Feedback Network

Synthesis Procedure

The synthesis procedure is presented in the flow chart of Figure 23. The designer must first determine if the system performance criteria can be satisfied with no damping enhancement or with pressure feedback alone. These steps have been included in the synthesis procedure.

TABLE IV

COMPARISON OF SETTLING TIMES FOR DIFFERENT TIME CONSTANTS

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Time Constant (seconds)	Optimum Pressure Feedback Gain (volts/psi)	Minimum Settling Time (seconds)	Settling Time K _D =0.01786 volt/psi (seconds)	Settling Time Error (percent)
œ	0.01786	0.4879	0.4879	0.0
1.0				
0.6	0.01409	0.5811	0.5876	1.1
0.5	0.01404	0.5946	0.6014	1.1
0.4	0.01402	0.6148	0.6219	1.1
0.3	0.01398	0.6519	0.6597	1.2
0.2	0.01345	0.7517	0.7657	1.9

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Figure 23. Flow Chart of the Synthesis Process



Figure 23. (Continued)



Figure 23. (Continued)

Once the need for dynamic pressure feedback has been established, the designer can use the computer program in Appendix E to make the necessary calculations for the dynamic pressure feedback network parameters. A discussion of how the dynamic pressure feedback synthesis was incorporated into the computer program can be found in the following section.

Dynamic Pressure Feedback Synthesis

Implementation

For the system with dynamic pressure feedback, the loop gain required to satisfy the system static stiffness performance criterion can be determined by direct computation; but such is not the case for the parameters affecting the system dynamic performance. Near optimum values of pressure feedback gain and network time constant can be calculated using an optimization program. The optimization routine STEPIT from the Oklahoma State University WATFIV FORTRAN computer library was used in this study.

A computer program was developed to supply STEPIT with the pertinent information on system description and specifications. Further, the computer program evaluates the minimization function required by STEPIT to determine how a parameter should be adjusted. System parameters are entered into the computer program via DATA statements. More information on the main program and the associated subroutines which comprise the computer program and how they work with STEPIT can be found in Appendix E.

A minimum of two executions of the computer program are required in the synthesis process. The first execution calculates the minimum servoamplifier gain required to produce the desired static stiffness. The static stiffness is a function of the system loop gain. For this system the servoamplifier gain, position feedback gain, servoactuator volumetric displacement, and valve flow gain comprise the system parameters in the loop gain. It is assumed that the servoactuator volumetric displacement, the valve flow gain, and the position feedback gain were all predetermined when the basic servosystem was designed.

Since the loop gain is a simple product of the parameters which comprise the loop, a change can be made in the servoamplifier and position gains as long as their product remains constant. The first execution of the computer program should be redone if the position feedback gain is altered from the value initially supplied.

The equation required to calculate the servoamplifier gain is

$$K_{A} = \frac{\frac{C_{S} \cdot D_{M}}{\mu} \cdot S_{S}}{\frac{\partial Q}{\partial Y} \cdot K_{V} \cdot K_{F} \cdot (1 - C_{F}) \cdot D_{M}}$$
(3.3)

The parameters in equation (3.3) are defined in the Nomenclature. Equation (3.3) is derived from equation (2.60).

During the first execution of STEPIT, the third-order transfer function system model for a pressure feedback system, equation (2.58), i.e., the dynamic pressure feedback model with an infinite time constant, is utilized. The servoamplifier gain, K_A , and pressure feedback gain, K_p , are allowed to vary in order to determine the pressure feedback gain which produces the maximum degree of stability. The servoamplifier gain is not allowed to fall below the value calculated with equation (3.3) in order for the static stiffness requirement to be met. The initial value of the servoamplifier gain utilized is that

value calculated with equation (3.3). The initial value of pressure feedback gain is user supplied.

During the first execution of the program, STEPIT determines the pressure feedback gain necessary to minimize the settling time. The function which STEPIT attempts to minimize is the settling time.

This first program execution requires some information to be user supplied. The information is entered into the computer via four statements.

(1) The required static stiffness is entered with the statement: STIFF = AAA.A , (3.4)

where AAA.A is the desired static stiffness.

(2) The third-order pressure feedback model is selected for the first program execution by setting the following internal flag in the program:

$$SET = 3.0$$
 (3.5)

(3) The initial value of the pressure feedback gain is supplied with the statement:

X(2) = BBB.B, (3.6)

where BBB.B is the initial pressure feedback gain supplied by the user.

(4) The minimization function for STEPIT to determine the pressure feedback gain necessary to provide the minimum settling time is the statement:

$$FOBJ = TSET$$
 (3.7)

The program is submitted and the information returned includes static stiffness obtained, servoamplifier gain, position feedback gain, rise time, and settling time. If the servoamplifier gain is not

possible to implement in hardware, the other information returned would not be applicable.

The second execution of the program utilizes the dynamic pressure feedback system model. The servoamplifier gain, position feedback gain, and pressure feedback gain are fixed at the values returned by the first execution. Only the time constant is allowed to decrease from infinity such that the transient settling time can increase to its maximum allowable level. This is so the system will have the stiffness not achieveable with pressure feedback.

The function for STEPIT to minimize is changed for the second execution. The function must have its minimum value when the difference between the transient settling time and the maximum allowable settling time is zero.

The computer statements utilized in the second execution of the program follow. The internal program flag which sets up the fourthorder transfer function model, equation (2.59), for the dynamic pressure feedback system is

$$SET = 5.0$$
 (3.8)

The servoamplifier and pressure feedback gains returned by the first execution are supplied to the second run with the following statements:

$$X(1) = CCC.C$$
, (3.9)
 $X(2) = DDD.D$, (3.10)

where CCC.C and DDD.D are servoamplifier and pressure feedback gains, respectively.

To prevent K_A and K_D from changing values, the following computer statements are inserted as an indicator to STEPIT that they are not

to be varied:

MASK(1) = 1 (3.11)

MASK(2) = 1 (3.12)

The initial value of time constant is user entered with the statement

X(3) = EEE.E, (3.13)

where EEE.E is the time constant initial value.

The maximum allowable settling time for the transient response is entered with the following statement:

$$DSET = FFF.F , \qquad (3.14)$$

where FFF.F is the maximum allowable settling time.

The minimization function for the second program execution is a minimum when its value equals zero. The statement is

FOBJ = DABS(TSET - DSET)(3.15)

The program is again submitted and the pertinent information returned includes feedback network time constant, rise time, and settling time.

It appears that the time constant range suggested by Geyer (5) and Morse (9) may be related to the practical implementation of the time constant in hardware. Such a consideration was not incorporated within the computer algorithm used for the synthesis in this thesis.

CHAPTER IV

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APPLICATION OF THE SYNTHESIS

PROCEDURE - AN EXAMPLE

Problem Statement

The system considered is a lightly damped, electrohydraulic, position control servosystem. The requirements and specifications for the example are as follows:

Minimum static stiffness:	1,000 in 1b _f /rad
Maximum settling time:	0.625 seconds
Maximum rise time:	0.055 seconds
Position feedback gain:	2 volts/rad
Step input to the system:	1.5 volts
Actuator-load open-loop natural frequency:	23.0 rad/seconds
Actuator-load open-loop damping ratio:	0.3

The remaining parameters except servoamplifier gain are the same as used for the system simulation (see Chapter II) and are given in Appendix F. The servoamplifier gain has not been determined.

The static stiffness is a function of the system loop gain. For this system the servoamplifier gain, position feedback gain, servoactuator volumetric displacement, and valve flow gain comprise the system elements in the loop gain. System specifications fixed the position feedback gain. For the basic servosystem with no damping

enhancement, the static stiffness must be obtained through the adjustment of the servoamplifier gain.

The basic servosystem servoamplifier gain required to maintain static stiffness is calculated with equation (3.3). For the basic servosystem, an amplifier gain of 0.667 ma/volt is required to maintain 1,000 in $1b_f/rad$ static stiffness. This gain produces a system which is unstable. The transient response for this system is shown in Figure 24.

Pressure feedback can be added to the system to improve the dynamic performance. To calculate the static stiffness for the system which employs pressure feedback, the equation used is

$$S_{S} = \frac{\frac{\partial Q}{\partial Y} \cdot K_{A} \cdot K_{V} \cdot K_{F} \cdot (1 - C_{F}) \cdot D_{M}}{\frac{C_{S} \cdot D_{M}}{\mu} + \frac{\partial Q}{\partial Y} \cdot K_{A} \cdot K_{V} \cdot K_{P}}$$
(4.1)

Figure 25 shows a plot of static stiffness versus pressure feedback gain for different values of servoamplifier gain. When the amplifier gain is increased from 0.667 ma/volt, the pressure feedback gain required to maintain the required static stiffness can be determined with equation (4.1).

If 1,000 in lb_f/rad stiffness is maintained as shown in Figure 25 and the servoamplifier gain is increased, the servoamplifier gain increases at a rate greater than the pressure feedback gain. The result is that the system is initially unstable and the degree of stability monotonically decreases. The poles of the transfer function move toward positive infinity. Pressure feedback will not suffice to satisfy both the static stiffness and degree of stability criteria.

Some means of damping enhancement is required to meet the static



Figure 24. Transient Response of System With No Damping Enhancement, $K_A = 0.667 \text{ ma/volt}$, $K_F = 2 \text{ volts/rad}$

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Figure 25. Plot of Static Stiffness Versus Pressure Feedback Gain for Pressure Feedback System in Example Problem

and dynamic specifications. Pressure feedback is not capable of producing the desired results. Dynamic pressure feedback was selected to enhance system damping and to avoid the undesirable effects introduced into the system via many other damping enhancement methods.

Problem Solution

The synthesis procedure presented in Chapter III was utilized in the design of a dynamic pressure feedback network for the example system. The static stiffness was entered into the program with the statement

$$STIFF = 1000.0$$
 (4.2)

The initial value of pressure feedback gain which is an estimate was entered as

$$X(2) = 2.5D - 02$$
 (4.3)

The output from the first execution of STEPIT can be seen in Figure 26. The key information returned is as follows:

Servoamplifier gain required for static stiffness:

0.667 ma/volt

Pressure feedback gain required for minimum settling time (infinite time constant):

0.0179 volt/psi

Transient response rise time:

0.052 seconds

Transient response settling time:

0.49 seconds

The servoamplifier gain and pressure feedback gain returned by the first execution appear to be achievable in actual hardware. The
THE MINIMUM REQUIRED STATIC STIFFNESS (IN+LBF/RAD) IS	0.10000D 04		
THE REQUIRED AMPLIFIER GAIN (MA/VOLT) IS	0.66724D 00		
THE STATIC STIFFNESS ACTUALLY OBTAINED (IN+LBF/RAD) IS	0.10000E 04		
FINAL VALUE FOR AMPLIFIER GAIN (MA/VOLT) IS	0.66724D 00		
FINAL VALUE FOR FEEDBACK GAIN (VOLT/PSI) IS	0.17862D-01		
THE CLOSED LOOP POLES ARE			
X(1)= -0.62462D 01+(0.23600D 02) I			
X(2)= -0.62462D 01+(-0.23600D 02) I			
X(3)= -0.29565D 03+(0.28106D-17) I			
STEADY STATE DISPLACEMENT (RAD) IS	0.75000D 00		
COEFFICIENT OF FIRST REAL POLE TERM IS	-0.53016D-02		
EXPONENT OF THE FIRST REAL POLE IS	0.29565D 03		
COEFFICIENT OF SINUSOIDAL TERM IS	-0.78995D OO		
EXPONENT OF SINUSOIDAL TERM IS	0.62462E 01		
RESPONSE DAMPED NATURAL FREQUENCY (RAD/SEC) IS	0.23600D 02		
PHASE SHIFT OF SYSTEM RESPONSE (RAD) IS	0.12307D 01		
RESPONSE PEAK DISPLACEMENT (RAD) IS	0.10643D 01		
TIME (SECS) PEAK DISPLACEMENT OCCURS IS	0.14753D 00		
RESPONSE RISE TIME (SECS) IS	0.52187D-01		
RESPONSE SETTLING TIME (SECS) IS	0.48791D 00		
RESPONSE ENVELOPE VALUE (RAD) AT WHICH SETTLING TIME DCCURS 0.712500 00			
THE OPEN LOOP POLES ARE			
X(1)= 0.00000D 00+(0.00000D 00) I			

X(2)≖	-0.29182D 02+(0.28227D 02) I
X(3)=	-0.29182D 02+(-0.28227D 02) I

Figure 26. Output Returned by the First Execution of STEPIT in Example Problem , ¹.

settling time obtained for the transient response more than meets the specifications. The rise time is less than the specified maximum.

For the second execution of the synthesis program, the maximum allowable settling time was entered with the statement

$$DSET = 0.625$$
 (4.4)

The servoamplifier gain and the pressure feedback gain were entered into the program prior to the second execution with the statements of

$$X(1) = 0.667$$
 , and (4.5)

$$X(2) = 0.0179$$
 (4.6)

The initial value of the feedback network time constant supplied to the program was

$$X(3) = 0.5$$
 (4.7)

Output from this execution is shown in Figure 27. The pertinent information from the output is as follows:

Feedback network time constant: 0.39 seconds

Transient response rise time: 0.050 seconds

The transient response rise time does not exceed the system specifications. The time constant is such that the corner frequency of the high pass filter is in the range of one-third to one-tenth the open-loop actuator-load natural frequency as suggested by Geyer (5) and Morse (9). It appears that the time constant could be implemented in hardware. The design of the dynamic pressure feedback network has been completed and the performance criteria satisfied. Figure 28 shows the transient response for the resulting system with dynamic pressure feedback.

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 THE MINIMUM REQUIRED STATIC STIFFNESS (1N*LBF/RAD) IS
 0.10000D 04

 THE REQUIRED AMPLIFIER GAIN (MA/VOLT) IS
 0.66724D 00

 THE STATIC STIFFNESS ACTUALLY OBTAINED (1N*LBF/RAD) IS
 0.10000E 04

 FINAL VALUE FOR AMPLIFIER GAIN (MA/VOLT) IS
 0.66724D 00

 FINAL VALUE FOR AMPLIFIER GAIN (MA/VOLT) IS
 0.66724D 00

 FINAL VALUE FOR FEEDBACK GAIN (VOLT/PSI) IS
 0.17860D-01

 FINAL VALUE OF FEEDBACK TIME CONSTANT (1/SEC) IS
 0.38846D 00

 THE CLOSED LOOP POLES ARE
 X(1)=

 -0.26552D 01+(
 0.00000D 00) I

X(2)= -0.51172D 01+(0.23397D 02) I	
X(3)= -0.51172D 01+(-0.23397D 02) I	
X(4)∗ -0.29781D 03+(-0.37321D-16) I	
STEADY STATE DISPLACEMENT (RAD) IS	0.750000 00
COEFFICIENT OF FIRST REAL POLE TÈRM IS	0.24665D-01
EXPONENT OF THE FIRST REAL POLE IS	0.26552D 01
COEFFICIENT OF SECOND REAL POLE TERM IS	-0.51484D-02
EXPONENT OF SECOND REAL POLE IS	0.29781D 03
COEFFICIENT OF SINUSOIDAL TERM IS	-0.80345D 00
EXPONENT OF SINUSOIDAL TERM IS	0.51172E 01
RESPONSE DAMPED NATURAL FREQUENCY (RAD/SEC) IS	0.23397D 02
PHASE SHIFT OF SYSTEM RESPONSE (RAD) IS	0.12791D 01
RESPONSE PEAK DISPLACEMENT (RAD) IS	0.11459D 01
TIME (SECS) PEAK DISPLACEMENT OCCURS IS	0.14674D 00
RESPONSE RISE TIME (SECS) IS	0.49969D-01
RESPONSE SETTLING TIME (SECS) IS	0.62500D 00
RESPONSE ENVELOPE VALUE (RAD) AT WHICH SETTLING TIME OCCURS	0.78750D 00
THE OPEN LOOP POLES ARE	
X(1)= 0.000000 00+(0.000000 00) I	

~(1)-	0.000000 00.0	0.000000 00) 1
X(2)=	-0.25743D 01+(0.00000D 00) I
X(3)=	-0.29182D 02+(0.28227D 02) I
X(4)=	-0.29182D 02+(-0.28227D 02) I

Figure 27. Output Returned by the Second Execution of STEPIT in Example Problem ٠...



Figure 28. Transient Response for the System With Dynamic Pressure Feedback in the Example Problem

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CHAPTER V

CONCLUSIONS AND RECOMMENDATIONS

Conclusions

A method was outlined to independently select the parameters of a dynamic pressure feedback network to compensate a lightly damped, electrohydraulic position control servosystem.

The synthesis procedure developed places no restriction on the time constant of the feedback network. It appears that the feedback network corner frequency (reciprocal of time constant) range of one-third to one-tenth the actuator-load natural frequency suggested by Geyer (5) and Morse (9) may be related to limitations of hardware implementation. The work of this study showed no special significance to this corner frequency range on system performance.

With all system parameters held constant except time constant the degree of stability (minimum settling time) increased with time constant for the class of systems considered in this study. When all system parameters were held constant except pressure feedback gain it was found that there is a unique pressure feedback gain which provides the minimum settling time as demonstrated by the root contours of Chapter III. The pressure feedback gain which produces the maximum degree of stability in systems with feedback network time constants other than infinity is close enough to that for an infinite time constant to have minimal effect on the settling time for those systems.

Recommendations

The study undertaken assumed that the significant servosystem dynamics were load inertia and fluid compressibility (in the actuator chambers). The synthesis technique should be extended to account for valve and/or transmission line dynamics.

The time constant of a mechanical dynamic pressure feedback network is a variable and is sensitive to the amplitude of the load pressure. In order to minimize the pressure feedback network sensitivity to pressure feedback amplitudes and possibly satisfy the performance criteria with less compromise the study of dynamic pressure feedback should be extended to include non-linear and optimal control theory.

BIBLIOGRAPHY

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- Blackburn, J.F., Reethof, G., and Shearer, J.L., <u>Fluid Power</u> Control, M.I.T. Press, Cambridge, Mass., 1960.
- Chandler, John P., "Instructions on Using STEPIT to Minimize or Maximize a Function", Unpublished, Stillwater, Oklahoma, Oklahoma State University, 1973.
- Dorf, Richard C., <u>Modern Control Systems</u>, Addison-Wesley, Menlo Park, California, 1974.
- "Dynamic Pressure Feedback, Controlled Damping by Use of the Dowty Moog Valve", <u>Aircraft Engineering</u>, June, 1960, pp. 171-176.
- Geyer, L.H., "Controlled Damping Through Dynamic Pressure Feedback", Moog Technical Bulletin 101, Moog, Inc., Controls Division, East Aurora, New York, 1972.
- McCloy, D., Martin, H.R., <u>The Control of Fluid Power</u>, John Wiley, New York, 1973.
- Merritt, H.D., <u>Hydraulic Control Systems</u>, John Wiley, New York, 1967.
- Meyfarth, P.F., <u>Dynamic Response Plots and Design Charts</u> for Third-Order Linear Systems, M.I.T. Dynamic Analysis and Control Laboratory, Research Memorandum. 7401-3, September, 1958.
- 9. Morse, A.C., <u>Electrohydraulic Servomechanisms</u>, McGraw-Hill, New York, 1963.
- Reid, Karl N., Classnotes for MAE 5453, Fluid Power Control I, Unpublished, Stillwater, Oklahoma, Oklahoma State University, Fall 1981.
- 11. Richardson, H.H., "The Analytical Design of Valve-Controlled Hydraulic Power and Control Systems. A Case Study", Unpublished Paper, M.I.T., Cambridge, Mass., 1962.
- 12. Rowland, James R., Linear Control Systems, Unpublished, Stillwater, Oklahoma, Oklahoma State University, 1983.

- 13. Shampine, L.F., Allen, R.C., <u>Numerical Computing: An Intro-</u> duction, Saunders Publishing Co., Philadelphia, 1973.
- 14. Speckhart, F.H., Green, W.L., <u>A Guide to Using CSMP The</u> <u>Continuous System Modelling Program</u>, Prentice-Hall, <u>Englewood Cliffs</u>, New Jersey, 1976.
- 15. Thayer, W.J., "Transfer Functions for Moog Servovalves", Moog Technical Bulletin 103, Moog, Inc., Controls Division, East Aurora, New York, 1965.

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APPENDIXES

APPENDIX A

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EQUATION LINEARIZATION

Linearization Technique

Many differential equations which describe a system are nonlinear. Linear system theory is not applicable to those equations without first transforming them into a linearized form. Once linearized the principle of superposition exists for the system equations.

The non-linear equations must be linearized about an operating point. The same non-linear equations linearized about two different operating points produces two different sets of equations.

Linearization was done about the origin of the pressure-flow curves for the position control system. A hydraulic servosystem operates about the origin of the valve pressure-flow-curves which is the point the system operates statically. The linear theory concept of the transfer function assumes that all initial conditions are zero referring to the origin of the pressure-flow curves.

Usage of derivatives and partial derivatives of the equations describing the system is part of the linearization procedure. Equation derivatives give the rate of change of a variable described by the differential equation. Small changes in the variable can be approximated by the product of the derivative and the incremental change in independent variable with which the derivative was taken.

Two examples are presented to exemplify the linearization procedure. The first example involves a function of a single variable and uses the derivative to obtain the linearization constant. The second example uses partial derivatives for a function of two or morevariables.

Example 1. Define a function of a single variable.

 $Y = f(X) \tag{A.1}$

Take the derivative of the function.

$$\frac{\mathrm{dY}}{\mathrm{dX}} = \mathrm{f}'(\mathrm{X}) \tag{A.2}$$

Multiply both sides of the equation by dX.

$$dY = f'(X) \cdot dX \tag{A.3}$$

Approximate the infinitesimal changes of the differential for small changes with Δ .

$$\Delta Y = f'(X) \cdot \Delta X \tag{A.4}$$

 ΔX and ΔY can be defined in terms of differences.

$$\Delta \mathbf{X} = \mathbf{X} - \mathbf{X}_{i} \tag{A.5}$$

$$\Delta Y = Y - Y_{i} \tag{A.6}$$

f'(X) is evaluated at the operating point and equations (A.5) and (A.6) can be substituted into equation (A.4).

$$Y - Y_{i} = f'(X_{i}) \cdot (X - X_{i})$$
 (A.7)

Regroup the terms.

$$Y = f'(X_{i}) + Y_{i} - f'(X_{i}) \cdot X_{i}$$
(A.8)

Equation (A.1) must hold true at the operating point

$$Y_{i} = f(X_{i})$$
(A.9)

Substitute equation (A.9) into equation (A.8).

$$Y = f'(X_{i}) \cdot X + f(X_{i}) - f'(X_{i}) \cdot X_{i}$$
(A.10)

The last two terms of equation (A.10) are the offset of the linearized equation from the origin. These terms will cancel if the value of the dependent variable is zero at the operating point.

Example 2. Define a function of two or more variables.

$$Y = f(X,Z) \tag{A.11}$$

Take the differential of the equation

$$dY = \frac{\partial f(X,Z)}{\partial X} \cdot dX + \frac{\partial f(X,Z)}{\partial Z} \cdot dZ$$
(A.12)

Approximate infinitesimal changes of the differential for small changes with Δ .

$$\Delta Y = \frac{\partial f(X,Z)}{\partial X} \cdot \Delta X + \frac{\partial f(X,Z)}{\partial Z} \cdot \Delta Z$$
(A.13)

 $\Delta X\,,\ \Delta Y\,,$ and ΔZ can be defined in terms of differences.

$$\Delta X = X - X_{i} \tag{A.14}$$

$$\Delta Y = Y - Y_{i} \tag{A.15}$$

$$\Delta Z = Z - Z_{1} \tag{A.16}$$

The partial derivatives are evaluated at the operating point and equations (A.14), (A.15), and (A.16) can be substituted into equation (A.13).

$$Y - Y_{i} = \frac{\partial f(X_{i}, Z_{i})}{\partial X} \cdot (X - X_{i}) + \frac{\partial f(X_{i}, Z_{i})}{\partial Z} \cdot (Z - Z_{i})$$
(A.17)

Regroup the terms of equation (A.17).

$$Y = \frac{\partial f(X_{i}, Z_{i})}{\partial X} \cdot X + \frac{\partial f(X_{i}, Z_{i})}{\partial Z} \cdot Z + Y_{i} - \frac{\partial f(X_{i}, Z_{i})}{\partial X} \cdot X_{i}$$
$$- \frac{\partial f(X_{i}, Z_{i})}{\partial Z} \cdot Z_{i}$$
(A.18)

Equation (A.11) must hold true about the operating point

$$Y_{i} = f(X_{i}, Z_{i})$$
(A.19)

Substitute equation (A.19) into (A.18).

$$Y = \frac{\partial f(X_{i}, Z_{i})}{\partial X} \cdot X + \frac{\partial f(X_{i}, Z_{i})}{\partial Z} \cdot Z + f(X_{i}, Z_{i}) - \frac{\partial f(X_{i}, Z_{i})}{\partial X} \cdot X_{i}$$
$$- \frac{\partial f(X_{i}, Z_{i})}{\partial Z} \cdot Z_{i} \qquad (A.20)$$

The last three terms of equation (A.20) may or may not cancel one another. Those terms represent the offset of the dependent variables at the operating point.

Linearized System Equations

System equations for this study were linearized using the technique presented. Algebra of combining the linearized equations was simplified by incorporating the initial conditions prior to combining them. Since the operating point was the origin of the pressure-flow curves a number of the linearization constants were equal to zero.

The initial conditions which provided the simplifications were the following:

- $X_{i} = 0 \tag{A.21}$
- $Y_{i} = 0$ (A.22)
- $sY_i = 0 \tag{A.23}$
- $P_{3i} = P_{4i}$ (A.24)
- $P_{1i} = P_{2i}$ (A.25)
- $P_{Mi} = 0 \tag{A.26}$

$$P_{6i} = P_E$$
 (A.28)

$$Q_{Ai} = Q_{Ci}$$
 (A.29)

$$Q_{\text{Di}} = Q_{\text{Fi}}$$
 (A.30)

$$sP_{1i} = 0$$
 (A.31)

$$sP_{2i} = 0$$
 (A.32)

$$sP_{3i} = 0$$
 (A.33)
 $sP_{i} = 0$ (A.34)

$$Q_{\rm H} = -Q_{\rm J} \tag{A.35}$$

$$P_5 = -P_6$$
 (A.36)

The definition of each linearization constant from the linearized equations presented in Chapter II is now presented. These constants are derivatives and partial derivatives of the equation evaluated at the operating point. The original linearized equation is also presented for the sake of continuity.

Error signal to the amplifier,

$$II = I + C_1 \cdot \theta + C_{31} \cdot P_M + C_{32} \cdot P_D$$
 (A.37)

$$C_1 = -K_F \tag{A.38}$$

$$C_{31} = -K_P \cdot S_3 \tag{A.39}$$

$$C_{32} = -K_{D} \cdot S_{5}$$
 (A.40)

Pressure forces acting on the flapper nozzle valve,

$$F_{1} = C_{2} \cdot (P_{3} - P_{4}) \tag{A.41}$$

$$F_2 = C_{33} \cdot (P_5 - P_6)$$
(A.42)

$$C_2 = 0.25 \cdot \pi \cdot D_1^2$$
 (A.43)

$$C_{33} = 0.25 \cdot \pi \cdot D_7^2$$
 (A.44)

Mechanical spring force between first and second stages,

$$F_{S} = C_{23} \cdot (X - Y)$$
 (A.45)

$$C_{23} = K_3$$
 (A.46)

Displacement of the torquemotor,

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$$X = C_3 \cdot II + C_4 \cdot Y + C_5 \cdot F_1 + C_5 \cdot F_2$$
 (A.47)

$$C_3 = K_1 \cdot K_A / (K_2 + K_3)$$
 (A.48)

$$C_4 = K_3 / (K_2 + K_3)$$
 (A.49)

$$C_5 = 1 / (K_2 + K_3)$$
 (a.50)

Flow through fixed orifice upstream of flapper valve left side,

$$Q_A = C_6 \cdot P_3 + C_7$$
 (A.51)

$$C_{6} = -0.125 \cdot \pi \cdot D_{3}^{2} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{S} - P_{3i})^{-\frac{1}{2}}$$
(A.52)

$$C_{7} = 0.125 \cdot \pi \cdot D_{3}^{2} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{S} - P_{3i})^{-\frac{1}{2}} \cdot P_{3i}$$

+ 0.25 \cdot \pi \cdot D_{3}^{2} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{S} - P_{3i})^{\frac{1}{2}} (A.53)

Flow through left side of flapper nozzle valve,

$$Q_{c} = C_{8} \cdot X + C_{9} \cdot P_{3} + C_{10}$$
 (A.54)

$$C_{8} = \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{3i} - P_{E})^{\frac{1}{2}}$$
(A.55)

$$C_{9} = 0.5 \cdot \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} + X_{1}) \cdot (P_{31} - P_{E})^{-\frac{1}{2}}$$
(A.56)

$$C_{10} = \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} + X_{i}) \cdot (P_{3i} - P_{E})^{\frac{1}{2}}$$

- $\pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{3i} - P_{E})^{\frac{1}{2}} \cdot X_{i}$
- $0.5 \cdot \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} + X_{i}) \cdot (P_{3i} - P_{E})^{-\frac{1}{2}} \cdot P_{3i}$ (A.57)

Flow through right side of flapper nozzle valve,

$$Q_F = C_{11} \cdot X + C_{12} \cdot P_4 + C_{13}$$
 (A.58)

$$C_{11} = -\pi \cdot D_1 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{41} - P_E)^{\frac{1}{2}}$$
(A.59)

$$C_{11} = -C_8$$
 (A.60)

$$C_{12} = 0.5 \cdot \pi \cdot D_1 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_0 - X_1) \cdot (P_{51} - P_E)^{-\frac{1}{2}}$$
(A.61)

$$C_{12} = C_9$$
 (A.62)

$$C_{13} = \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{4i} - P_{E})^{\frac{1}{2}} \cdot X_{i}$$

- 0.5 \cdot \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} - X_{i}) \cdot (P_{4i} - P_{E})^{-\frac{1}{2}} \cdot P_{4i}
+ \pi \cdot D_{1} \cdot C_{D} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} - X_{i}) \cdot (P_{4i} - P_{E})^{\frac{1}{2}} (A.63)
$$C_{13} = C_{13} \qquad (A.64)$$

$$C_{13} = C_{10}$$
 (A.64)

Flow through the fixed orifice upstream of right side of flapper valve,

$$Q_{\rm D} = C_{14} \cdot P_4 + C_{15} \tag{A.65}$$

$$C_{14} = -0.125 \cdot \pi \cdot D_3^2 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_S - P_{4i})^{-\frac{1}{2}}$$
(A.66)

$$C_{14} = C_6$$
 (A.67)

$$C_{15} = 0.125 \cdot \pi \cdot D_3^2 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_S - P_{4i})^{-\frac{1}{2}} \cdot P_{4i}$$

+ 0.25 \cdot \pi \cdot D_3^2 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_S - P_{4i})^{\frac{1}{2}} (A.68)

$$C_{15} = C_7$$
 (A.69)

Time rate of pressure change on left side of valve spool,

$$sP_3 = C_{34} \cdot Y + C_{35} \cdot (Q_A - Q_C) + C_{36} \cdot sY + C_{37}$$
 (A.70)

$$C_{34} = \frac{-\beta}{(Y_0 + Y_1)^2} \left(\frac{Q_{Ai} - Q_{Ci}}{AE} - sY_i \right) = 0$$
 (A.71)

$$C_{35} = \frac{\beta}{AE (Y_0 + Y_1)}$$
 (A.72)

$$C_{36} = \frac{-\beta}{(Y_0 + Y_1)}$$
 (A.73)

$$C_{37} = -C_{34} \cdot Y_{i} - C_{35} \cdot (Q_{Ai} - Q_{Ci}) - C_{36} \cdot sY_{i} + sP_{3i} = 0$$
 (A.74)

Time rate of pressure change on right side of valve spool,

$$sP_4 = C_{38} \cdot Y + C_{39} \cdot (Q_D - Q_F) + C_{40} \cdot sY + C_{41}$$
 (A.75)

$$C_{38} = \frac{\beta}{(Y_0 - Y_i)^2} \left(\frac{Q_{Di} - Q_{Fi}}{AE} + sY_i \right) = 0$$
 (A.76)

$$C_{39} = \frac{\beta}{AE (Y_0 - Y_i)}$$
 (A.77)

$$C_{39} = C_{35}$$
 (A.78)

$$C_{40} = \frac{\beta}{(Y_0 - Y_1)}$$
(A.79)

$$C_{41} = -C_{38} \cdot Y_i - C_{39} \cdot (Q_{Di} - Q_{Fi}) - C_{40} \cdot sY_i + sP_{4i} = 0$$
 (A.80)

Flow through the valve and motor,

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$$Q_{\rm M} = C_{69} \cdot Y + C_{70} \cdot P_{\rm M}$$
 (A.81)

$$C_{69} = - (QMAX \div YMAX) \cdot [1 - (P_M \div P_S)]^{\frac{1}{2}}$$
 (A.82)

$$C_{70} = - (QMAX \div P_S) \cdot (I \div IMAX) \cdot [1 - (P_M \div P_S)]^{-\frac{1}{2}}$$
 (A.83)

Time rate of pressure change in right load line,

$$sP_1 = C_{42} \cdot s\theta + C_{43} \cdot P_M + C_{44} \cdot Q_M$$
 (A.84)

$$C_{22} = \frac{C_{\rm S} \cdot D_{\rm M}}{\mu} \tag{A.85}$$

$$C_{42} = \frac{\beta \cdot D_{M}}{v_{1}}$$
(A.86)

$$C_{43} = \frac{C_{22} \cdot \beta}{V_1}$$
 (A.87)

$$C_{44} = \frac{-\beta}{v_1}$$
(A.88)

Time rate of pressure change in left load line,

$$sP_2 = C_{45} \cdot s\theta + C_{46} \cdot P_M + C_{47} \cdot Q_M$$
 (A.89)

$$C_{45} = \frac{-\beta \cdot D_{M}}{V_{2}}$$
(A.90)

$$C_{46} = \frac{-C_{22} \cdot \beta}{v_2}$$
 (A.91)

$$C_{47} = \frac{\beta}{v_2}$$
 (A.92)

The electrical dynamic pressure feedback element,

$$P_{\rm D} = \frac{C_{48} \cdot sP_{\rm M}}{\tau s + 1} \tag{A.93}$$

$$C_{48} = \tau \cdot S_5 \tag{A.94}$$

'Flow from mechanical dynamic pressure feedback unit on left side,

$$Q_{\rm H} = C_{59} \cdot X + C_{60} \cdot P_5 + C_{61}$$
 (A.95)

$$C_{59} = \pi \cdot D_7 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{5i} - P_E)^{\frac{1}{2}} = 0$$
 (A.96)

$$C_{60} = 0.5 \cdot \pi \cdot D_7 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_0 + X_1) \cdot (P_{51} - P_E)^{-\frac{1}{2}}$$
(A.97)

$$C_{60} = \infty$$
(A.98)

$$C_{61} = Q_{Hi} - \pi \cdot C_{D} \cdot D_{7} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{5i} - P_{E})^{\frac{1}{2}} \cdot X_{i}$$

$$- 0.5 \cdot \pi \cdot C_{D} \cdot D_{7} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} + X_{i}) \cdot (P_{5i} - P_{E})^{-\frac{1}{2}} P_{5i} (A.99)$$

$$C_{61} = 0$$
(A.100)

Flow from right side of mechanical dynamic pressure feedback unit,

$$Q_J = C_{62} \cdot X + C_{63} \cdot P_6 + C_{64}$$
 (A.101)

$$C_{62} = -\pi \cdot D_7 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{6i} - P_E)^{\frac{1}{2}} = 0$$
 (A.102)

$$C_{63} = 0.5 \cdot \pi \cdot D_9 \cdot C_D \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_0 - X_1) \cdot (P_{61} - P_E)^{-\frac{1}{2}}$$
(A.103)

$$C_{63} = \infty \tag{A.104}$$

$$C_{64} = Q_{Ji} + \pi \cdot C_{D} \cdot D_{7} \cdot (2/\rho)^{\frac{1}{2}} \cdot (P_{6i} - P_{E})^{\frac{1}{2}} \cdot X_{i}$$

- 0.5 \cdot \pi \cdot C_{D} \cdot D_{7} \cdot (2/\rho)^{\frac{1}{2}} \cdot (X_{0} - X_{i}) \cdot (P_{6i} - P_{E})^{-\frac{1}{2}} P_{6i} (A.105)
$$C_{ee} = 0$$
(A.106)

$$Q = Q_J = -Q_H = -C_{60} \cdot P_6$$
 (A.107)

Viscous damping force on the valve spool,

$$F_{V} = C_{65} \cdot sY \tag{A.108}$$

$$C_{65} = \mu \cdot \pi \cdot D_2 \cdot L_D / C_R$$
 (A.109)

Steady state flow forces on valve spool,

$$F_{SS1} = C_{16} \cdot Y + C_{17} \cdot P_M + C_{18}$$
 (A.110)

$$C_{16} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot (P_S - P_E + P_{Mi}) \cdot \cos 69^\circ$$
 (A.111)

$$C_{17} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot Y_i \cdot \cos 69^\circ = 0$$
 (A.112)

$$C_{18} = C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot (P_{S} - P_{E} + P_{Mi}) \cdot Y_{i}$$

- $C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot Y_{i} \cdot P_{Mi}$
+ $C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot Y_{i} \cdot (P_{S} - P_{E} + P_{Mi}) = 0$ (A.113)

$$F_{SS2} = C_{19} \cdot Y + C_{20} \cdot P_{M} + C_{21}$$
(A.114)

$$C_{19} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot (P_S - P_E - P_{Mi}) \cdot \cos 69^{\circ}$$
(A.115)

$$C_{20} = -C_V \cdot C_D \cdot \pi \cdot D_2 \cdot Y_i \cdot \cos 69^\circ = 0$$
 (A.116)

$$C_{21} = C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot (P_{S} - P_{E} - P_{Mi}) \cdot Y_{i}$$

+ $-C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot Y_{i} \cdot P_{Mi}$
+ $-C_{V} \cdot C_{D} \cdot \pi \cdot D_{2} \cdot Y_{i} \cdot (P_{S} - P_{E} - P_{Mi}) = 0$ (A.117)

Acceleration of the valve spool,

$$s^{2}Y = C_{66} \cdot F_{S} + C_{66} \cdot AE \cdot (P_{3} - P_{4}) + C_{66} \cdot AF \cdot P_{M} + C_{66} \cdot F_{SS1} + C_{66} \cdot F_{SS2} - C_{66} \cdot F_{V}$$
(A.118)

$$C_{66} = 1 / M$$
 (A.119)

Angular acceleration of the shaft,

$$s^{2}\theta = C_{67} \cdot P_{M} + C_{68} \cdot s\theta$$
 (A.120)

$$C_{67} = (1 - C_F) \cdot D_M / J$$
 (A.121)

$$C_{68} = -(C_{DM} \cdot D_{M} \cdot \mu + Visd) / J$$
 (A.122)

The linearized equations which describe the mechanical dynamic pressure feedback high pass filter are combined to form its transfer function. The constant C_{60} is the slope of the pressure-flow curve for the feedback orifices. Initially C_{60} has a value of infinity but very quickly drops to a finite value. C_{60} was assigned an effective slope for simulation purposes. The form of the feedback element

transfer function is

$$\frac{P_{\rm D}}{P_{\rm M}} = \frac{\frac{-\text{ AP} \cdot \text{AG}}{2 \cdot \text{K}_4 \cdot \text{C}_{60}} \cdot \text{s}}{\frac{\text{AP}^2}{2 \cdot \text{K}_4 \cdot \text{C}_{60}} \cdot \text{s} + 1}$$

(A.123)

APPENDIX B

NON-LINEAR SIMULATION PROGRAM

The CSMP program listing for the non-linear system simulations is contained in this appendix. Equations used in the simulation are the equations presented in Chapter II. The program includes the capabilities of adding mechanical or electrical pressure feedback, mechanical or electrical dynamic pressure feedback to the basic uncompensated servosystem.

This particular simulation solves all the system equations simultaneously. Any of the system variables is available for printer plots. Time, angular position, velocity, and acceleration are written to a TSO data set for continuous plotting purposes. Using other programs available for plotting purposes the data can be viewed as a continuous graph on a Tektronix CRT.

Basically the CSMP program consists of three main segments. These are INITIAL, DYNAMIC, and TERMINAL segments. The INITIAL segment must appear first. It sets up the information required to perform simulation and is therefore executed only once. PARAMETER, CON-STANT; and INCON statements within the INITIAL segment contain values of system parameters, constants, and initial conditions to be used in the simulation.

The DYNAMIC segment contains the equations actually used to describe the system. This program segment is continually re-executed

with a specified time step for the duration of the simulation. Integrations are performed with this segment during the course of the simulation.

The TERMINAL segment follows the DYNAMIC segment and like the INITIAL segment is executed only once. Output is set-up, integration technique defined, integration time step fixed, and simulation time duration specified. The particular integration routine used through the course of this study was a fixed step Runge-Kutta. The Runge-Kutta does quite well for general engineering work due to its low error. Close match between experimental and simulation results attest to this fact.

Additional capability is added to the CSMP simulation with MACRO statements which precede the INITIAL segment. MACRO statements are executable subprograms called by the INITIAL or DYNAMIC segments to make internal program changes during execution. When MACRO statements are included in the DYNAMIC segment they are executed as any other statement at each step of the integration.

****CONTINUOUS SYSTEM MODELING PROGRAM****

```
*** VERSION 1.3 ***
```

```
    THE MACRO MODEL SETS THE CONSTANTS TO ZERO OUT THE INCORRECT
    MODEL AND ALLOWS THE CORRECT MODEL TO BE SIMULATED
    MACRO S1, S2, S3, S4, S5=MODEL(SET)
    PROCEDURAL
    S1=1.0
    S2=0.0
    S3=0.0
    S4=0.0

                 S5=0.0
IF (SET.NE.2.0) GO TO 75
S1=0.0
S2=1.0
        $2=1.0

GO TO 105

75 IF (SET.NE.3.0) GO TO 85

S1=0.0

GO TO 105

85 IF (SET.NE.4.0) GO TO 95 -

S1=0.0

S4=1.0

GO TO 105

95 IF (SET.NE.5.0) GO TO 105

S1=0.0

S5=1.0

105 CONTINUE
        105 CONTINUE
  ENDMAC

    THE MACRO TOMP STOPS THE TORQUEMOTOR DISPLACEMENT ONCE IT REACHES
    MAXIMUM DISPLACEMENT IN EITHER DIRECTION
    MACRO XX=TOMP(X,XO)
    PROCEDURAL

       XX=X
IF (X.GE.(-1.0*X0)) GD TO 115
XX=-1.0*X0
115 IF (X.LE.X0) GD TO 125
XX=X0
125 CONTINUE
  ENDMAC

    THE MACRO GO1 DETERMINES DIRECTION OF OIL FLOW DEPENDING UPON
    THE PRESSURE DIFFERENTIAL ACROSS THE ORIFICE
    MACRO GO1=PILOT1(P1,P4P)
    PROCEDURAL
        GO1=1.0
        IF (P4P.GT.P1) GO1=-1.0

   ENDMAC

    THE MACRO GO2 DETERMINES DIRECTION OF OIL FLOW DEPENDING UPON
    THE PRESSURE DIFFERENTIAL ACROSS THE ORIFICE
    MACRO GO2=PILOT2(P4P,PE)
    PROCEDURAL
    GO2=1.0
    IE (P4P,IT PE) GO2=-1.0

                   IF (P4P.LT.PE) G02=-1.0
   ENDMAC
                THE MACRO GO3 DETERMINES DIRECTION OF OIL FLOW DEPENDING UPON
THE PRESSURE DIFFERENTIAL ACROSS THE ORIFICE
0 GO3=PILOT3(P5P,PE)
```

MACRO GO3 PROCEDURAL

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```
GO3=1.0
IF (P5P.LT.PE) GO3=-1.0
   ENDMAC
            THE MACRO GO4 DETERMINES DIRECTION OF OIL FLOW DEPENDING UPON
THE PRESSURE DIFFERENTIAL ACROSS THE ORIFICE
0 GO4=PILOT4(P1,P5P)
   ٠
   MACRO
   PROCEDURAL

G04=1.0

IF (P5P.GT.P1) G04=-1.0
                                                                                     .
٠
   ENDMAC

    THE MACRO SWITCH CHANGES THE VALVE PRESSURE DROP EQUATIONS TO
    THE APPROPRIATE PRESSURES DEPENDING UPON THE SIDE OF NULL THE
    SPOOL IS LOCATED
    MACRO A,B,SGN=SWITCH(Y)
    PROCEDURAL

         IF (Y) 35,25,25
25 A=0.0
B=1.0
               SGN=1.0
        GO TO 45
35 A×1.0
               B=0.0
               SGN=-1.0
         45 CONTINUE
   ENDMAC
            THE MACRO FILTG PREVENTS THE PRESSURE PG FROM CAVITATING
   MACRO P6P=FILT6(P6,PE)
PROCEDURAL
             P6P*P6
IF (P6.LT.PE) P6P*PE
   ENDMAC
   * THE MACRO FILT7 PREVENTS THE PRESSURE P7 FROM CAVITATING
MACRO P7P=FILT7(P7,PE)
PROCEDURAL
P7P=P7
               IF (P7.LT.PE) P7P≖PE
   ENDMAC

    THE MACRO DERI3 DETERMINES FLOW DIRECTION ACROSS ONE SPOOL LAND
    DEPENDING UPON THE PRESSURE DIFFERENTIAL
    MACRO SP=DERI3(DELP3)
    PROCEDURAL
    SP=1.0
    IF (DELP3.LT.0.0) SP=-1.0

    ENDMAC
   * THE MACRO DERI4 DETERMINES FLOW DIRECTION ACROSS ONE SPOOL LAND
* DEPENDING UPON THE PRESSURE DIFFERENTIAL
MACRO TP=DERI4(DELP4)
PROCEDURAL
TP=1.0
IF (DELP4.LT.O.O) TP=-1.0
FNDMAC
    ENDMAC

    THE MACRO FLOFOR PREVENTS THE UNSTEADY FLOW FORCES FROM GOING TO
    INFINITY AS THE PRESSURE DROP ACROSS THE LAND GOES TO ZERO
    MACRO DEL3,DEL4,C,D=FLOFOR(DELP3,DELP4)
    PROCEDURAL

               C=1.0
D=1.0
               DEL3=DELP3
               DEL4=DELP4
```

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```
IF (ABS(DEL3).GT.1.0) GO TO 55
       C=0.0
DEL3=1.0
55 IF (ABS(DEL4).GT.1.0) G0 TO 65
            D=0.0
DEL4=1.0
       65 CONTINUE
ENDMAC
          THE MACRO COUL DETERMINES THE DIRECTION OF COULOMB FRICTION
MACRO FDIR=COUL(THED)
PROCEDURAL
     IF (THED)
135 FDIR=-1.0
GD TO 165
145 FDIR=0.0
                                      135,145,155
     GO TO 165
155 FDIR=1.0
     165 CONTINUE
ENDMAC
INITIAL
           AL

THE PARAMETER SET DETERMINES WHICH MODEL IS BEING STUDIED

SET=1.0 UNCOMPENSATED MODEL

SET=2.0 MECHANICAL PRESSURE FEEDBACK MODEL

SET=3.0 ELECTRICAL PRESSURE FEEDBACK MODEL

SET=4.0 MECHANICAL DYNAMIC PRESSURE FEEDBACK MODEL

SET=5.0 ELECTRICAL DYNAMIC PRESSURE FEEDBACK MODEL

SET=5.0 ELECTRICAL DYNAMIC PRESSURE FEEDBACK MODEL

SET=5.0 SET=3.0
.
         PARAMETER
                                             SET=3.0
٠
        I - STEP INPUT TO THE SYSTEM (VOLTS)
PARAMETER I=1.5
         BETA - OIL BULK MODULUS (PSI)
MU - OIL ABSOLUTE VISCOSITY (LBF*SEC/IN**2)
PARAMETER BETA=150000.0, MU=2.0E-06,...
.
*
           CD - ORIFICE DISCHARGE COEFFICIENT
RHO - OIL DENSITY (LBF*SEC**2/IN**4)
P1 - SUPPLY PRESSURE (PSI)
CD=0.625, RHO#7.85E-05, P1=1100.0,...
*
           V1 - VOLUME UNDER COMPRESSION OF P3 (IN**3)
V2 - VOLUME UNDER COMPRESSION OF P2 (IN**3)
ANG - COS 69 DEG. USED IN STEADY STATE FLOW FORCES
V1=25.0, V2=25.0, ANG=0.3584
.
           CS - MOTOR SLIP COEFFICIENT
CV - FLUID VELOCITY COEFFICIENT FOR STEADY STATE FLOW FORCES
PARAMETER CS=0.88E-08, CV=0.98,...
*
          PARAMETER
           CF - MOTOR FRICTION COEFFICIENT

CDM - MOTOR VISCOUS DRAG COEFFICIENT

DM - MOTOR DISPACEMENT (IN**3/RAD)

CF=0.10, CDM=160000.0, DM=1.512E-02,...
٠
*
           J - MOTOR ROTARY INERTIA (IN*LBF*SEC**2/RAD)
CFRIC - COULOMB FRICTION (IN*LBF)
TL - EXTERNAL LOAD TORQUE (IN*LBF)
J=2.16E-03, CFRIC=0.0, TL=0.0,...
            VISD - VISCOUS DRAG EXTERNAL TO MOTOR (IN*LBF*SEC)
              VISD=0.018
           KWFL - SERVOAMPLIFIER GAIN (MA/VOLT)
KWFL1 UNCOMPENSATED MODEL SERVOAMPLIFIER GAIN
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KWFL2 MECHANICAL PRESSURE FEEDBACK MODEL SERVOAMPLIFIER GAIN KWFL3 ELECTRICAL PRESSURE FEEDBACK MODEL SERVOAMPLIFIER GAIN KWFL4 MECHANICAL DPF MODEL SERVOAMPLIFIER GAIN KWFL5 ELECTRICAL DPF MODEL SERVOAMPLIFIER GAIN ARAMETER KWFL1=0.667, KWFL2=0.57,... KWFL3=0.667, KWFL4=1.00, KWFL5=0.747 ٠ PARAMETER K1 - TORQUEMDTOR CONSTANT (LBF/MA) K2 - TORQUEMDTOR CONSTANT (LBF/IN) ٠ . PARAMETER K1=0.05, K2=140.0,... K3 - MECHANICAL FEEDBACK CONSTANT (LBF/IN) K5 - SPRING RATE IN MECH DPF UNIT (LBF/IN) K3=22.5, K5+200.0 ٠ D1 - FLAPPER NOZZLE DIAMETER (IN) D2 - VALVE SPOOL DIAMETER (IN) * PARAMETER D2=0.275,... D1=0.023, D3 - ORIFICE DIAMETER UPSTREAM OF FLAPPER (IN) D6 - DIAMETER OF AREA ON WHICH MECH PRESSURE FEEDBACK ACTS (IN) D7 - LARGE DIAMETER OF MECH DPF PISTON (IN) * D3=0.012, D6=0.05, D7=1.7039,... D8 - SMALL DIAMETER OF MECH DPF PISTON (IN) D9 - DIAMETER OF MECH DPF ORIFICE WHICH ACTS ON FLAPPER (IN) * D8×1.3215, D9×0.010 XO - NULL DISPLACEMENT OF FLAPPER (IN) YO - NULL LENGTH OF VOLUME ON EACH END OF SPOOL (IN) PARAMETER XO=0.0018, YO=0.40,... ٠ PARAMETER CR - VALVE SPOOL RADIAL CLEARANCE (IN) LD - SPOOL LENGTH FOR VISCOUS DAMPING (IN) L - DISTANCE BETWEEN PORTS FOR UNSTEADY FLOW FORCES (IN) CR=0.00005, LD=0.384, L=0.29,... * M - MASS OF SPOOL VALVE (LBF*SEC**2/IN**4) M=3.2071E-05 KFBK - POSITION FEEDBACK GAIN (VOLTS/RAD) KAMP - ELECTRICAL PRESSURE FEEDBACK GAIN (VOLTS/PSI) PARAMETER KFBK=2.00, KAMP≈6.5E-03,... PARAMETER KAMPD - ELECTRICAL DPF FEEDBACK GAIN (VOLTS/PSI) TAU3 - ELECTRICAL DPF TIME CONSTANT (1/SEC) KAMPD=5.0E-03, TAU3=0.32 KAMPD=5.0E-03, CONSTANT FLAG=9.8765E+00, COUNT=0.0, CYCLE=19.0 CONSTANT PI=3.14159 YDIC - INITIAL SPOOL VELOCITY (IN/SEC) YIC - INITIAL SPOOL DISPLACEMENT (IN) INCON YDIC=0.0, YIC=0.0 YIC=0.0.... THETIC - INITIAL MOTOR DISPLACEMENT (RAD) THEDIC - INITIAL MOTOR VELOCITY (RAD/SEC) CAPIC - INITAL VALUE OF REAL POLE THETIC=0.0, THEDIC=0.0, CAPIC=0.0. CAPIC=0.0.... ZIC - INITIAL MECH DPF UNIT DISPLACEMENT (IN) ZIC=0.0 PE - EXHAUST PRESSURE (PSI) PARAMETER PE≖O.O

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* P21C,P31C -INITIAL PRESSURES IN LOAD LINES (PSI) P21C=0.5*(P1+PE) P31C=0.5*(P1+PE)

S1,S2,S3,S4,S5=MODEL(SET) KWFL=KWFL1*S1+KWFL2*S2+KWFL3*S3+KWFL4*S4+KWFL5*S5 CON1=CD*P1*D2*SQRT(2.0/RH0) CON3=CD*P1*D1*SQRT(2.0/RH0) CON4=-2.0*CV*CD*P1*D2*ANG CON5=SQRT(RH0)*L*CD*P1*D2 CON6=MU*P1*D2*LD/CR CON10=0.25*P1*D1*2 CON12=0.25*P1*D1*2 CON12=0.25*P1*D9*2 CON14=CD*P1*D9*SQRT(2.0/RH0)

* AF - AREA ON SPOOL MECH PRESSURE FEEDBACK ACTS (IN**2) AF=0.25*PI*D6**2*S2

- * AE NET AREA ON SPOOL END FOR CONTROL (IN**2) AE=0.25*PI+D2**2-AF
- * AG AREA OF MECH DPF UNIT ON WHICH LINE PRESSURE ACTS (IN**2) AG=0.25*PI*DB**2
- * AP AREA OF MECH DPF UNIT WHICH HOLDS PRESSURE TO FLAPPER (IN**2) AP=D7**2*0.25*PI-AG
- * P4IC.P5IC INITIAL PRESSURE ON ENDS OF VALVE SPOOL (PSI) P4IC=(P1+D3++4+16.0+PE+D1++2+X0++2)/(D3++4+16.0+D1++2+X0++2)

P5IC=P4IC

DYNAMIC A,B,SGN≠SWITCH (Y)

 DELP3,DELP4 - PRESSURE DROP ACROSS THE TWO VALVE LANDS DELP3*(B*P1-SGN*P3P-A*PE) DELP4*(A*P1+SGN*P2P-B*PE)

DEL3,DEL4,C,D=FLOFOR(DELP3,DELP4) SP=DERI3(DELP3) TP=DERI4(DELP4)

- * QQ1,QQ4 FLOW THROUGH THE TWO LOAD LINES QQ1=-1.0*V*CON1*SORT(ABS(DELP4))*TP QQ4=-1.0*V*CON1*SORT(ABS(DELP3))*SP
- * II ERROR SIGNAL FED TO SERVOAMPLIFIER II=I-KFBK*THET-KAMP*DPM*S3-KAMPD*DPF*S5
- * X DISPLACEMENT OF TORQUEMOTOR X=(K1*KWFL*II+K3*Y+TMF1+TMF2)/(K3+K2)
- TMF1 NET FORCE ACTING ON FLAPPER BY PRESSURES ON END OF SPOOL TMF1=(P4P-P5P)*CON10
- * TMF2 NET FORCE ACTING ON FLAPPER BY MECH DPF UNIT TMF2*(P6P-P7P)*CON12

XX=TQMP(X,XO) GD1=PILDT1(P1,P4P)

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QA - FLOW THROUGH ONE FIXED ORIFICE UPSTREAM OF FLAPPER OA=CON2*SQRT(ABS(P1-P4P))*GO1

GO2=PILOT2(P4P,PE)

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QC - FLDW THROUGH DNE SIDE OF FLAPPER NOZZLE QC×CON3*(XD+XX)*SQRT(ABS(P4P-PE))*GO2

GO3×PILOT3(P5P,PE)

QF - FLOW THROUGH ONE SIDE OF FLAPPER NOZZLE QF=CON3+(XO-XX)+SQRT(ABS(P5P-PE))+GO3

GO4=PILOT4(P1,P5P)

- QD FLOW THROUGH ONE FIXED ORIFICE UPSTREAM OF FLAPPER QD=CON2+SQRT(ABS(P1-P5P))+GO4
- FSS1,FSS2 STEADY STATE FLOW FORCES ACTING ON VALVE SPOOL FSS1=CON4+Y+ABS(P1-A+P2P-B+P3P) FSS2=CON4+Y+ABS(B+P2P+A+P3P-PE)
- P4DOT TIME RATE OF CHANGE OF PRESSURE ON ONE END OF SPOOL P4DOT=BETA*((QA-QC)/AE-YDOT)/(YO+Y) P4P = INTGRL (P4IC, P4DOT)
- * P5DOT TIME RATE OF CHANGE OF PRESSURE ON ONE END OF SPOOL P5DOT=BETA*((QD-QF)/AE+YDOT)/(YO-Y) P5P = INTGRL (P5IC, P5DOT)
- FUS1,FUS2 UNSTEADY FLOW FORCES ACTING ON VALVE SPOOL FUSA1=SGN*CON5*SQRT(ABS(2.0*DELP3))*VDOT*SP FUSA2=-1.0*CON5*0.5*Y*(1.0/(SQRT(ABS(2.0*DEL3))))*P3DOT*C*SP FUS1=FUSA1+FUSA2 FUSB1=-1.0*SGN*CON5*SQRT(ABS(2.0*DELP4))*VDOT*TP FUSB2=-1.0*CON5*0.5*Y*(1.0/(SQRT(ABS(2.0*DEL4))))*P2DOT*D*TP FUS2=FUSB1+FUSB2
- P3DOT TIME RATE OF CHANGE OF ONE LOAD LINE PRESSURE P3DOT=BETA*(DM*THED+CS*DM*(P2P-P3P)/MU-QQ4)/V1 P3P=INTGRL(P3IC,P3DOT)
- P2DOT TIME RATE OF CHANGE OF ONE LOAD LINE PRESSURE P2DOT=BETA*(QQ1-DM*THED-CS*DM*(P2P-P3P)/MU)/V2 P2P*INTGRL(P2IC,P2DOT)
- DPMD TIME RATE OF CHANGE OF LOAD LINE DIFFERENTIAL PRESSURE DPMD=P2DOT-P3DOT

DPFD=DPMD+TAU3+S5

- DPF ELECTRICAL DYNAMIC PRESSURE FEEDBACK SIGNAL DPF=REALPL(CAPIC,TAU3,DPFD)
- DPM LOAD LINE DIFFERENTIAL PRESSURE DPM=P2P-P3P
- P6P=FILT6(P6,PE)
 * QI FLOW THROUGH ONE SIDE OF MECH DPF UNIT
 QI=CON14*(X0+XX)*SQRT(ABS(P6P-PE))*S4

P7P≖FILT7(P7,PE)

- QJ FLOW THROUGH ONE SIDE OF MECH DPF UNIT QJ=CON14*(XO-XX)*SORT(ABS(P7P-PE))*S4
- ZDOT TIME RATE OF DISPLACEMENT CHANGE OF MECH DPF UNIT ZDOT×(QJ/AP-QI/AP)*S4 Z=INTGRL(ZIC,ZDOT)

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P6,P7 - PRESSURE ON TWO SIDE OF MECH DPF UNIT P6=(2.0*K5*Z/AP-DPM*AG/AP) P7=(DPM*AG/AP-2.0*K5*Z/AP)

- FVD VISCOUS DAMPING FORCE ACTING ON VALVE SPOOL FVD=CON6*YDOT
- FS MECHANICAL SPRING FORCE BETWEEN FIRST AND SECOND STAGES FS=k3+(XX-Y)
- * YDDOT ACCELERATION OF VALVE SPOOL YDDOT=(FS+(P4P-P5P)*AE+(P2P-P3P)*AF+FUS1+FUS2+FSS1+FSS2-FVD)/M YDOT=INTGRL(YDIC,YDDOT) Y=INTGRL(YIC,YDOT)

FDIR=COUL(THED)

THEDD - ANGULAR ACCELERATION OF SERVOMOTOR THEDD=((1.0-CF)+DM*(P2P-P3P)-CDM+DM+MU+THED-CFRIC*FDIR-TL-VISD+... THED)/J THED=INTGRL(THEDIC.THEDD) THET=INTGRL(THETIC.THED) NOSORT

CALL DEBUG (1,0.0)

THESE STATEMENTS WRITE TO TSO DATA SET FOR PLOTTING IF (KEEP.NE.1) GO TO 500 CYCLE=CYCLE+1.0 IF (CYCLE.NE.20.0) GO TO 500 WRITE (8,600) TIME,THET,THED,THEDD 600 FORMAT (T5,4(E14.6,5X)) CYCLE=0.0 COUNT=COUNT+1.0 500 CONTINUE

TERMINAL

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TIMER FINTIM=0.65,DELT=5.0E-05,PRDEL=2.5E-03,OUTDEL=2.5E-03
WRITE (8,700) FLAG,COUNT
700 FORMAT (T5,E14.6,5X,E14.6)
METHOD RKSFX
PRTPLT THET (II,XX,DPM)
END
STOP
```

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APPENDIX C

TRANSFER FUNCTION SIMULATION

The CSMP program used to simulate the five transfer function valve models used in this study is contained in this appendix. These five models are the basic uncompensated servosystem with the means to add mechanical or electrical pressure feedback, mechanical or electrical dynamic pressure feedback to the basic system. Complete documentation is contained in the program.

Constants for the simulation are set up by the INITIAL segment. System parameters, constants, and initial conditions are entered through PARAMETER, CONSTANT, and INCON statements. Subscripted "C's" are the linearization constants defined in Appendix A. The algebra required to reduce the system equations to the transfer function is contained in the subscripted "T's" of the INITIAL segment. Constants inappropriate for a particular model are cancelled by switches set up by the MACRO MODEL.

Once the constants of the system transfer function are evaluated the dynamic response is produced by the DYNAMIC program segment. Values of time and actuator displacement are written into a TSO data set for continuous data plotting. Continuous plots are obtained through other programs.

Following the DYNAMIC segment is the TERMINAL segment. This segment sets up output, defines integration technique, sets integration

time step, and sets the simulation duration time. Runge-Kutta integration proved to be quite adequate for the transfer function as it had been with the non-linear model simulation.

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****CONTINUOUS SYSTEM MODELING PROGRAM****

*** VERSION 1.3 ***

 THE MACRO MODEL SETS THE CONSTANTS TO ZERO OUT THE INCORRECT
 MODEL AND ALLOWS THE CORRECT MODEL TO BE SIMULATED
 MACRO S1,S2,S3,S4,S5=MODEL(SET)
 PROCEDURAL 51=1.0 52=0.0 S3=0.0 S4=0.0 S5=0.0 IF (SET.NE.2.0) G0 T0 75 S1=0.0 52=1.0 GD TO 105 75 IF (SET.NE.3.0) GD TO 85 S1≠0.0 S3≖1.0 GO TO 105 85 IF (SET.NE.4.0) GO TO 95 S1=0.0 S4=1.0 GO TO 105 95 IF (SET.NE.5.0) GO TO 105 S1=0.0 S5=1.0 105 CONTINUE ENDMAC INITIAL NOSORT THE PARAMETER SET DETERMINES WHICH MODEL IS BEING STUDIED SET=1.0 UNCOMPENSATED MODEL SET=2.0 MECHANICAL PRESSURE FEEDBACK MODEL SET=3.0 ELECTRICAL PRESSURE FEEDBACK MODEL SET=5.0 MECHANICAL DYNAMIC PRESSURE FEEDBACK MODEL SET=5.0 ELECTRICAL DYNAMIC PRESSURE FEEDBACK MODEL PARAMETER SET=3.0 * * * PARAMETER I ~ STEP INPUT TO THE SYSTEM (VOLTS) PARAMETER I≈1.5 * BETA - OIL'BULK MODULUS (PSI) MU - OIL ABSOLUTE VISCOSITY (LBF*SEC/IN**2) PARAMETER BETA=150000.0, MU=2.0E-06,... * CD - ORIFICE DISCHARGE COEFFICIENT RHO - OIL DENSITY (LBF*SEC**2/IN**4) P1 - SUPPLY PRESSURE (PS1) CD=0.625, RHO=7.85E-05, P1=1100.0,... * V1 - VOLUME UNDER COMPRESSION OF P3 (IN**3) V2 - VOLUME UNDER COMPRESSION OF P2 (IN**3) ANG - COS 69 DEG. USED IN STEADY STATE FLOW FORCES V1=25.0, V2=25.0, ANG=0.3584CS - MOTOR SLIP COEFFICIENT CV - FLUID VELOCITY COEFFICIENT FOR STEADY STATE FLOW FORCES PARAMETER CS=0.88E-08, CV=0.98,... PARAMETER

CF - MOTOR FRICTION COEFFICIENT CDM - MOTOR VISCOUS DRAG COEFFICIENT DM - MOTOR DISPACEMENT (IN**3/RAD) CDM=160000.0, DM=1.512E-02,... CF=0.10. J - MOTOR ROTARY INERTIA (IN*LBF*SEC**2/RAD) J=2.16E-03 KWFL - SERVOAMPLIFIER GAIN (MA/VOLT) KWFL1 UNCOMPENSATED MODEL SERVOAMPLIFIER GAIN KWFL2 MECHANICAL PRESSURE FEEDBACK MODEL SERVOAMPLIFIER GAIN KWFL3 ELECTRICAL PRESSURE FEEDBACK MODEL SERVOAMPLIFIER GAIN KWFL4 MECHANICAL DPF MODEL SERVOAMPLIFIER GAIN KWFL5 ELECTRICAL DPF MODEL SERVOAMPLIFIER GAIN DRAMETED ARAMETER KWFL1=0.667, KWFL2=0.667 KWFL3=0.667, KWFL4=0.667, KWFL5=0.667 PARAMETER KWFL2=0.667,... K1 - TOROUEMOTOR CONSTANT (LBF/MA) K2 - TOROUEMOTOR CONSTANT (LBF/IN) PARAMETER K1=0.05, K2= PARAMETER K2=140.0.... K3 - MECHANICAL FEEDBACK CONSTANT (LBF/IN) K5 - SPRING RATE IN MECH DPF UNIT (LBF/IN) K3=22.5. K5=200.0 D1 - FLAPPER NOZZLE DIAMETER (IN) D2 - VALVE SPOOL DIAMETER (IN) PARAMETER D1=0.023, D2=0.275,... D3 - ORIFICE DIAMETER UPSTREAM OF FLAPPER (IN) D6 - DIAMETER OF AREA ON WHICH MECH PRESSURE FEEDBACK ACTS (IN) D7 - LARGE DIAMETER OF MECH DPF PISTON (IN) D6=0.05. D3=0.012. D7=1 7039 DB - SMALL DIAMETER OF MECH DPF PISTON (IN) D9 - DIAMETER OF MECH DPF ORIFICE WHICH ACTS ON FLAPPER (IN) D9=0.010 D8=1.3215, XO - NULL DISPLACEMENT OF FLAPPER (IN) YO - NULL LENGTH OF VOLUME ON EACH END OF SPOOL (IN) PARAMETER XO=0.0018, YO=0.40,... PARAMETER CR - VALVE SPOOL RADIAL CLEARANCE (IN) LD - SPOOL LENGTH FOR VISCOUS DAMPING (IN) L - DISTANCE BETWEEN PORTS FOR UNSTEADY FLOW FORCES (IN) CR=0.00005, LD=0.384, L=0.29,... M - MASS OF SPOOL VALVE (LBF*SEC**2/IN**4)
M=3.2071E-05, Z0=1.00 KFBK - POSITION FEEDBACK GAIN (VOLTS/RAD) KAMP - ELECTRICAL PRESSURE FEEDBACK GAIN (VOLTS/PSI) PARAMETER KFBK=2.000, KAMP=6.5E-03,... PARAMETER KAMPD - ELECTRICAL DPF FEEDBACK GAIN (VOLTS/PSI) TAU3 - ELECTRICAL DPF TIME CONSTANT (1/SEC) KAMPD=0.1786E-01, TAU3=0.3885 VISD - VISCOUS DRAG EXTERNAL TO MOTOR (IN+LBF+SEC) PARAMETER VISD=0.018 CONSTANT PI=3.14159

* PE - EXHAUST PRESSURE (PSI) INCON PE=0.0

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CONSTANT FLAG=9.8765E+00, COUNT=0.0, CYCLE=19.0
PARAMETER IMAX= 36.5, PM=850.0,...
YMAX=0.025
    $1,$2,$3,$4,$5*MODEL($ET)
KWFL=KWFL1*$1+KWFL2*$2+KWFL3*$3+KWFL4*$4+KWFL5*$5
 P2IC, P3IC -INITIAL PRESSURES IN LOAD LINES (PSI)
   P21C=0.5*(P1+PE)
P3IC=0.5*(P1+PE)
 P4IC,P5IC - INITIAL PRESSURE ON ENDS OF VALVE SPOOL (PSI)
P4IC=(P1*D3**4+16.0*PE*D1**2*X0**2)/(D3**4+16.0*D1**2*X0**2)
    P5IC=P4IC
    P61C=PE
     P7IC=PE
   P7IC=PE

CON1=CD+P1+D2+SQRT(2.0/RHO)

CON2=0.25+P1+D3+22+CD+SQRT(2.0/RHO)

CON3=CD+P1+D1+SQRT(2.0/RHO)

CON3=CD+P1+D1+SQRT(2.0/RHO)

CON6=MU+P1+D2+LD/CR

CON10=0.25+P1+D1+*2

CON12=0.25+P1+D3+*2

CON12=0.25+P1+05+*2
    CON14=CD+PI+D9+SQRT(2.0/RH0)-
  AF - AREA ON SPOOL MECH PRESSURE FEEDBACK ACTS (IN**2) AF=0.25*PI*D6**2*S2
  AE - NET AREA ON SPOOL END FOR CONTROL (IN**2)
AE=0.25*PI*D2**2-AF
  AG - AREA OF MECH DPF UNIT ON WHICH LINE PRESSURE ACTS (IN**2)
AG=0.25*PI*D8**2
  AP - AREA OF MECH DPF UNIT WHICH HOLDS PRESSURE TO FLAPPER (IN**2)
    AP=D7**2*0.25*PI-AG
    QMAX=PI*D2*YMAX*CD*SQRT((P1-PE)/RHO)
     C1=-1.0*KFBK
    C1=-1.0*KFBK

C2=CON10

C3=K1*KWFL/(K2+K3)

C4=K3/(K2+K3)

C5=-0.5*CON2*(SQRT(P1-P4IC))

C7=0.5*CON2*VAIC/(SQRT(P1-P4IC))+CON2*SQRT(P1-P4IC)

C8=CON3*SQRT(P4IC-PE)

C9=0.5*CON3*X0/(SQRT(P4IC-PE))

C10=CON3*X0*SQRT(P4IC-PE)-0.5*CON3*X0*P4IC/(SQRT(P4IC-PE))

C10=CON3*X0*SQRT(P4IC-PE)-0.5*CON3*X0*P4IC/(SQRT(P4IC-PE))

C12=C5*DM/MU
     C22=CS+DM/MU
     C23=K3
    C24=-1.0*CON1*SQRT(P1-P2IC)
C31=-1.0*KAMP*S3
C32=-1.0*KAMPD*S5
C33=CON12
    C34=0.0
C35=BETA/(AE*YO)
C35=BETA/(AE*YO)
C36=-1.0*BETA/YO
C42=BETA*DM/V1
C43=BETA*C22/V1
                                                               ۰.
    C43=betA*C22/V1
C44=-1.0*BETA/V1
C45=-1.0*BETA*DM/V2
C46=-1.0*BETA*C22/V2
C47=BETA/V2
     C48=TAU3*S5
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C49=AG*S4 C50=AP C51=-2.0*K5 C53+BETA/(AP+ZO) C54+-1.0+BETA/ZO C60 - EFFECTIVE SLOPE OF PRESSURE-FLOW CURVE OF MECH DPF UNIT C60=3.2824E-05 C65=CON6 C65=CON6 C66=1.0/M C67=(1.0-CF)*DM/J C69=-1.0*(CDM*DM*NU+VISD)/J C69=-VALVE FLOW GAIN C69=-1.0*(CMAX/YMAX)*SQRT(1.0-I*PM/(ABS(I)*P1))) C70=-1.0*(CMAX/YMAX)*SQRT(1.0-I*PM/(ABS(I)*P1))) T1=C43-C46+C70*(C44-C47) T2=1.0/(C67*C69*(C47-C44)) T3=(T1-C68)/(C67*C69*(C47-C44)) T4=-1.0*(T1*C68+C67*(C45-C42))/(C67*C69*(C47-C44)) T5=C1*TAU3+C31*TAU3*(C45-C42) T6=C1*(TAU3+C31*TAU3*(C45-C42)) C65×C0N6 T6=C1*(TAU3*T1+1.0)+C31*(C45-C42) T7=C1*T1 T8=C31*TAU3*(C47-C44)*C69+C32*C48*C69*(C47-C44) T9=C31*C69*(C47-C44) T9=C31*C69*(C47-C44) T10=C9*C35-C6*C35 T11=C50*C49/(2.0*K5*C60) T13=-1.0*C59*(C47-C44)*T11 T14=-1.0*T11*(C45-C42) T15=C3*T5*T12*C5*C33*T14*TAU3 T16=C3*(T6*T12*T5*T10*T12*T5)+C5*C33*T14*(T10*TAU3*1.0) T17=C3*(T5*T10+T7*T10*T12*T5)+C5*C33*T14*T10 T18=C3*(T5*110+T7*T10*T12+T6)+C5*C33*T14*T10 T 18-C3*(T6*T 10+T7*T 10*T 12+T7) T 19=C3*T7*T 10 T 20=C4*T 12*TAU3+2.0*C2*C5*C36*T 12*TAU3 120=C4*112*1AU3+2.0*C2*C5*C36*112*1AU3 121=C3*T8*T12+C4*(11*112*TAU3+112+T10*T12*TAU3+TAU3)... +2.0*C2*C5*C36*(T12*T1*TAU3+T12+TAU3)+C5*C33*T13*TAU3 122=C3*(19*T12+T8*T10*T12+T8)+C4*(T10*TAU3+T1*T12*T1*T10 *T12*TAU3+T10*T12+T1*TAU3+1.0)+2.0*C2*C5*C36*(T1*T12+T1*T10 TAU3+1.0)+C5*C33*T13*(T10*TAU3+1.0) 123=C3*(T8*T10+T9*T10*T12+T9)+C4*(T1*T10*T12+T1+T1*T10*TAU3...) +T 10)+2.0*C2*C5*C36*T 1+C5*C33*T 13*T 10 T24=C3*T9*T 10+C4*T 1*T 10 124=C3*19*110+C4*11*110 T25=T10+2.0*C2C5*C8*C35 T26=T1+T10+C65*C66 T27=T1*T10+C66*C65*(T1+T10)-2.0*C36*C66*AE+C66*C23-2.0*C16*C66 T28=C66*C65*T1*T10-2.0*C36*C66*AE*T1+C66*C23*(T1+T10)-C66*C69*AF*(C47-C44)-2.0*C16*C66*(T1+T10) T29=C66*C23*T1*T10-C66*C69*AF*(C47-C44)*T10-2.0*C16*C66*T1*T10 T30=C66*C23*T10-2.0*C8*C35*C66*AE T31=T12*TAU3 T32+T12+T25+TAU3+T12+TAU3+T12+TAU3+T26 T33+T12+T25+T25+TAU3+1.0+T26+(T12+T25+TAU3+T12+TAU3)+T27+T12+TAU3 T34+T25+T26+(T12+T26+T25+TAU3+1.0)+T27+(T12+TAU3)+T27+TAU3+ T12+TAU3)+T12+T28+TAU3 T35+T25+T26+(T12+T28+TAU3+1.0)+T28+(T12+T25+TAU3+ T12+TAU3)+T29+T12+TAU3 T36=T25+T27+T28+(T12+T25+T25+TAU3+1.0)+T29*(T12*T25*TAU3+T12+TAU3) T37=T25+T28+T29*(T12*T25+T25+TAU3+1.0) T38=T25+T29 T39=-1.0°C66*AF*(C45-C42)*T12*TAU3 T40=-1.0*C66*AF*(C45-C42)*(T10*T12*TAU3+T12*T25*TAU3+ ... T12+TAU3) T41=-1.0*C66*AF*(C45-C42)*(T10*(T12*T25*TAU3+T12+TAU3)+ ...

T12*T25+T25*TAU3+1.0) T42=-1.0*C66*AF*(C45-C42)*(T25+T10*(T12*T25+T25*TAU3+1.0)) 95

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T57=T34+T51 T58=T35+T52 T59=T36+T53 T60=T37+T54 T61=T38+T55 T62=T39+T44 T63=T40+T45 T64=T41+T46 T65=T42+T47 T66=T43+T48 T67=T2*T31 T67=T2*T31 T68=T2*T32+T3*T31 T69=T2*T56+T3*T32+T4*T31 T70=T2*T57+T3*T56+T4*T32 T71=T2*T58+T3*T56+T4*T56 T72=T2*T58+T3*T58+T4*T57 T73=T2*T60+T3*T59+T4*T58 T74=T2*T61+T3*T60+T4*T59 T75=T3*T61+T4*T60 T76=T4*T61 T77=T62+T72 T78=T63+T73 T79=T64+T74 T80=T65+T75 T81=T66+T76 1816-1951/16 182-C3+112+TAU3+C66+C23 183-C3+(130+T12+TAU3+C66+C23+(T1+T12+TAU3+T10+T12+TAU3+... T83=C3*(T30*T12*TAU3+C66*C23*(T1*T12*TAU3+T10*T12*TAU3+... T12+TAU3)) T84=C3*(T30*(T1*T12*TAU3+T12+T10*T12*TAU3+TAU3)+C66*C23*.... (T10*TAU3+T1*T12+T1*T10*T12*TAU3+T10*T12+T1*TAU3+1.0)) T85=C3*(T30*(T10*TAU3+T1*T12+T1*T10*T12*TAU3+T10*T12+T1*TAU3 +1.0)+C66*C23*(T1*T10*T12+T1*T1*T10*TAU3+T10)) T86=C3*(T30*(T1*T10*T12+T1+T1*T10*TAU3+T10)+C66*C23*T1*T10) T87=C3*T30*T1*T10 T87=C3*T30*T1 T88=T82/T87 T89=T83/T87 T90=T84/T87 T91=T85/T87 T92=T86/T87 T93=T67/T49 T94=T68/T49 T95=T69/T49 T95=T69/T49 T96=T70/T49 T97=T71/T49 T98=T77/T49 T99=T78/T49 ۰. T 100=T79/T49 T 101=T80/T49 T102=TB1/T49 DYNAMIC W1=INTGRL(0.0,W2) W2=INTGRL(0.0,W3)

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W3=INTGRL(0.0,W4)
W4=INTGRL(0.0,W5)
W5=INTGRL(0.0,W6)
W6=INTGRL(0.0,W7)
W7=INTGRL(0.0,W8)
W9=INTGRL(0.0,W100DT)
W100DT+(1-T94+W10-T95+W9-T96+W8-T97+W7-T98+W6-T99+W5-T100+W4 ...
-T101+W3-T102+W2-W1)/T93
THET=(T87/T49)+(T88+W6+T89+W5+T90+W4+T91+W3+T92+W2+W1)
RE5P+KFBK*THET/1
NOSORT
CALL DEBUG (1.0.0)
* THESE STATEMENTS WRITE TO TSO DATA SET FOR PLOTTING
IF (KEP.NE.1) GO TO 500
CYCLE=CYCLE+1.0
IF (CYCLE.NE.20.0) GO TO 500
WRITE (8,600) TIME,THET
600 FORMAT (T5.2(E14.6,5X))
CYCLE=0.0
COUNT+COUNT+1.0
500 CONTINUE
TERMINAL
WRITE (8,700) FLAG,COUNT
TIMER FINTIM=0.65,DELT+5.0E-05,PRDEL=2.5E-03,OUTDEL=2.5E-03
700 FORMAT (T5.E14.6,5X,E14.6)
METHOD RKSFX
PRTPLT THET (RESP)
END
STOP
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APPENDIX D

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TRANSFER FUNCTION CONSTANTS

Solution models for systems of the type studied are third order for uncompensated systems or systems utilizing pressure feedback. Dynamic pressure feedback system solution models are fourth order. The constants of the transfer function are terms including the various system parameters. Transfer functions for the general systems were derived for this study. Specific transfer functions for specific systems can be evaluated knowing the system parameters.

Transfer functions of the third order solution models used are of the form

$$\frac{\theta}{I} = \frac{K}{a_3 s^3 + a_2 s^2 + a_1 s + a_0}$$
(D.1)

Solution models of the fourth order dynamic pressure feedback model are of the form

$$\frac{\theta}{I} = \frac{K \cdot (\tau s + 1)}{a_4 s^4 + a_3 s^3 + a_2 s^2 + a_1 s + a_0}$$
(D.2)

The definition of each constant of (D.1) for the system with no additional compensation is described below. Subscripted "C's" represent constants from the linearized equations described in Appendix A.

$$K = (1 - C_F) \cdot D_M \cdot K_V \cdot K_A \cdot C_{69} \cdot (C_{47} - C_{44}), \qquad (D.3)$$

 K_v is the value gain.

$$a_3 = J$$
 (D.4)

$$a_2 = J \cdot [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] + (C_{DM} \cdot D_M \cdot \mu + Visd)$$
 (D.5)

$$a_{1} = [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot (C_{DM} \cdot D_{M} \cdot \mu + Visd)$$

- (1 - C_F) \cdot D_{M} \cdot (C_{45} - C_{42}) (D.6)

$$a_{0} = K_{F} \cdot K_{V} \cdot K_{A} \cdot (1 - C_{F}) \cdot D_{M} \cdot C_{69} \cdot (C_{47} - C_{44})$$
(D.7)

Systems utilizing pressure feedback also have a transfer function of the form (D.1). The definition of each transfer function constant for this system follows.

$$K = (1 - C_F) \cdot D_M \cdot K_V \cdot K_A \cdot C_{69} \cdot (C_{47} - C_{44})$$
(D.8)

$$a_3 = J$$
 (D.9)

$$a_{2} = J \cdot [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] + (C_{DM} \cdot D_{M} \cdot \mu + Visd) + J \cdot K_{P} \cdot K_{A} \cdot K_{V} \cdot C_{69} \cdot (C_{47} - C_{44})$$
(D.10)

$$a_{1} = [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot (C_{DM} \cdot D_{M} \cdot \mu + \text{Visd})$$

- $(1 - C_{F}) \cdot D_{M} \cdot (C_{45} - C_{42})$
+ $K_{P} \cdot (C_{DM} \cdot D_{M} \cdot \mu + \text{Visd}) \cdot K_{A} \cdot K_{V} \cdot C_{69} \cdot (C_{47} - C_{44})$ (D.11)

$$a_{0} = K_{F} \cdot K_{V} \cdot K_{A} \cdot (1 - C_{F}) \cdot D_{M} \cdot C_{69} \cdot (C_{47} - C_{44})$$
(D.12)

Systems utilizing pressure feedback have a transfer function of the form (D.2). The definition of each constant of the fourth order transfer function utilizing dynamic pressure feedback follows.

$$K = K_{A} \cdot K_{V} \cdot C_{69} \cdot (1 - C_{F}) \cdot D_{M} \cdot (C_{47} - C_{44})$$
(D.13)

$$a_4 = J \cdot \tau \tag{D.14}$$

$$a_{3} = \tau \cdot (J \cdot [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] + [C_{DM} \cdot D_{M} \cdot \mu + Visd])$$

+ J + K_A · K_V · K_D · C₆₉ · (C₄₇ - C₄₄) · \tau · J (D.15)
$$a_{2} = \tau \cdot ([C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot [C_{DM} \cdot D_{M} \cdot \mu + Visd]$$

- [1 - C_F] · D_M · [C₄₅ - C₄₂]) + J · [C₄₃ - C₄₆ + C₇₀ · (C₄₄ - C₄₇)]

+
$$(C_{DM} \cdot D_{M} \cdot \mu + Visd)$$

+ $K_{A} \cdot K_{V} \cdot K_{D} \cdot C_{69} \cdot (C_{47} - C_{44}) \cdot \tau \cdot (C_{DM} \cdot D_{M} \cdot \mu + Visd)$ (D.16)

$$a_{1} = [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot [C_{DM} \cdot D_{M} \cdot \mu + \text{Visd}]$$

- (1 - C_F) \cdot D_M \cdot (C_{45} - C_{42})
+ \tau \cdot K_F \cdot K_A \cdot K_V \cdot (1 - C_F) \cdot D_M \cdot C_{69} \cdot (C_{47} - C_{44}) (D.17)

$$a_{0} = K_{F} \cdot K_{A} \cdot K_{V} \cdot C_{69} \cdot (1 - C_{F}) \cdot D_{M} \cdot (C_{47} - C_{44})$$
(D.18)

When developing the root locus as a function of feedback gain the transfer function in (D.2) was rearranged with the feedback gain in the open loop gain position. The new open loop transfer function for the feedback gain is of the following form.

$$GH = \frac{K_{D} \cdot (b_{3}s^{3} + b_{2}s^{2})}{a_{4}s^{4} + a_{3}s^{3} + a_{2}s^{2} + a_{1}s + a_{0}}$$
(D.19)

The definition of each constant of the transfer function follows.

$$b_{3} = K_{A} \cdot K_{V} \cdot C_{69} \cdot (C_{47} - C_{44}) \cdot \tau \cdot J$$
 (D.20)

$$\dot{b}_{2} = K_{A} \cdot K_{V} \cdot C_{69} \cdot (C_{47} - C_{44}) \cdot \tau \cdot (C_{DM} \cdot D_{M} \cdot \mu + Visd)$$
 (D.21)

$$a_4 = J \cdot \tau \tag{D.22}$$

$$a_{3} = J + \tau \cdot (J[C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] + [C_{DM} \cdot D_{M} \cdot \mu + Visd])$$
(D.23)

$$a_{2} = J \cdot [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] + (C_{DM} \cdot D_{M} \cdot \mu + \text{Visd}) + \tau \cdot ([C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot [C_{DM} \cdot D_{M} \cdot \mu + \text{Visd}] - [1 - C_{F}] \cdot D_{M} \cdot [C_{45} - C_{42}])$$
(D.24)
$$a_{1} = [C_{43} - C_{46} + C_{70} \cdot (C_{44} - C_{47})] \cdot [C_{DM} \cdot D_{M} \cdot \mu + \text{Visd}] - [1 - C_{F}] \cdot D_{M} \cdot [C_{45} - C_{42}] + \tau \cdot K_{F} \cdot K_{A} \cdot K_{V} \cdot C_{69} \cdot (1 - C_{F}) \cdot D_{M} \cdot (C_{47} - C_{44})$$
(D.25)

$$a_{0} = K_{F} \cdot K_{A} \cdot K_{V} \cdot C_{69} \cdot (1 - C_{F}) \cdot D_{M} \cdot (C_{47} - C_{44})$$
(D.26)

APPENDIX E

PERFORMANCE OPTIMIZATION PROGRAM

A listing of the user supplied program used to determine the optimum values of the three adjustable system parameters is presented in this appendix. The program and all related subroutines are written in WATFIV FORTRAN. Computational variables are double precision to minimize round-off error in the optimization process.

A main program and five subroutines comprise the user supplied program for evaluating the objective function for minimization. SER-VO, MULER, DISP, ENVEL, and INTPOL are the five subroutines. The main program sets up the input for optimization.

Desired system static stiffness is user entered. System parameters are input into the program through DATA statements. The main program calculates the necessary servoamplifier gain required to maintain static stiffness. That amplifier gain value is assigned to XMIN(1) to prevent the gain from falling below the level required to maintain static stiffness. Simultaneously that amplifier gain is assigned to the program adjustable parameter X(1).

X(2) and X(3) represent the initial values of feedback gain and feedback time constant supplied by the user to the program. These values are not necessary for simulation. Setting MASK(1) and MASK(2) non-zero prevents the values of X(1) and X(2) from varying the second step of the synthesis process.

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The system model to be used in the optimization program is determined by the variable SET. SET equal to 1.0 models the uncompensated system, equal to 3.0 is the pressure feedback model, and equal to 5.0 the dynamic pressure feedback model. Depending upon the particular model different initial values of the system parameters are supplied.

The main program calls STEPIT which is in constant communication with SERVO. SERVO evaluates the objective function supplied for minimization. Settling time was the only value used in computing the objective function for this project but SERVO also computes rise time, peak overshoot, and time of peak overshoot. These values can be incorporated into the objective function as desired by the user.

STEPIT receives the fixed system parameters from the main program and increments the adjustable parameters in such a manner as to minimize the objective function. SERVO evaluates the system transfer function with parameter values supplied by STEPIT. SERVO in turn calls MULER to locate the transfer function poles.

MULER locates the transfer function poles using Muller's method. Determination of all the system poles is not guaranteed with Muller's method but as a general rule is quite reliable.

Nature of the poles was known through the root locus presented in Chapter III. The time solution was obtained according to the procedure outlined in Chapter III. SERVO calculates the rise time, peak displacement, and peak time utilizing the subroutines DISP and INTPOL. DISP evaluates the value of the time response for various time values. INTPOL in turn interpolates between values returned by DISP to determine the time at a specific displacement.

Simultaneously, SERVO evaluates the response settling time using

the envelope of the time response. Subroutines ENVEL and INTPOL are utilized by SERVO in obtaining the settling time. ENVEL evaluates the value of the response envelope for various time values. INTPOL in turn interpolates between values returned by ENVEL to determine the specific time settling time occurs.

STEPIT keeps track of the direction with which the objective function is changing. It increments the adjustable parameters and the process of re-evaluating the objective function begins again. Final parameter values which STEPIT returns are the starting points for system hardware selection.

	\$JOB .TIME=(1.00)
1	DOUBLE PRECISION XMAX.XMIN.DELTX.DELMN.ERR.FOBJ.X
2	DOUBLE PRECISION TRISE.TSET.DRISE.DSET.DPEAK
Э	DOUBLE PRECISION PFE.PFF.PFG.PFL.AA.BB.CC.FREQ.PHI.TIME.THET.SGN
4	DOUBLE PRECISION COE(20), ROOTR(20), ROOTI(20), XN(10), FN(10), DISL
5	DOUBLE PRECISION ABSERR, ANS, ERROR
6	DOUBLE PRECISION STIFF, CON1, CON2, CON3, CON4, CON10, P2IC, P4IC, AE,
	1 C1,C2,C4,C5,C6,C8,C9,C16,C22,C23,C24,C30,C35,C42,C44,C45,C47,
	2C69,C43,C46,C70,T1,T10.KWFL,KVAL,II,KFBK,X0,Y0,CS,CF,CDM,DM,
	3MU,P1,PE,RH0,CV,ANG,PJ,BETA,V1,V2,CD,D1,D2,D3,K1,K2,K3,PI,VISD
7	EXTERNAL SERVO
8	COMMON TRISE, TSET, DRISE, DSET
9	COMMON PFE, PFF, PFG, PFL, AA, BB, CC, FREQ, PHI, TIME, THET, SGN
10	COMMON CDE, ROOTR, ROOTI
11	COMMON XN, FN, DISL, ABSERR, ANS, ERROR
12	COMMON NT, NFAIL, IQUII, NN, MAXDEG, JJ
13	CUMMUN /PASS/PI,CI,C42,C43,C44,C45,C46,C47,C69,C70,T1,KVAL,CF,
14	10M, PU, CUM, MU, 11, UPCAK, VISU, SEICOMMON (CSTER) V(SO) VMAV(SO) VMIN(SO) DELTY(SO) DELMU(SO)
14	+ EDD(20 21) EOR INV NTDAC MATN(20), DELTA(20), DELMA(20),
	* NEWY NEL AT JUDY NYTOA KELAC NOED KEELW KW
	C SYSTEM PARAMETERS ARE ENTERED INTO THE OPTIMIZATION PROGRAM
	C THROUGH THESE DATA STATEMENTS.
15	DATA II.KFBK.X0.Y0/1.500+00.2.0000+00.1.8D-03.0.4D+00/
16	DATA CS, CF, CDM, DM, MU/O.88D-08, 1.0D-01, 1.6D+05, 1.512D-02, 2.0D-06/
17	DATA P1, PE, RHD, CV, ANG/1. 1D+03, 0. D+00, 7.85D-05, 9.8D-01, 3.584D-01/
18	DATA PJ,BETA,V1,V2,CD/2.16D-03,1.50D+05,2.5D+01,2.5D+01,6.25D-01
19	DATA D1,D2,D3,K1,K2,K3/2.3D-02,2.75D-01,1.2D-02,5.0D-02,1.4D+02,
	12.25D+01/
20	DATA PI,ABSERR/3.141592654D+00,5.0D-10/
21	DATA VISD/0.018D+00/
22	DATA IQUIT, NN, MAXDEG/0, 10, 8/
	C DRISE IS DESIRED RISE TIME.
23	DRISE=2.69217D-02
~ ~	C DSET IS DESIRED SETTLING TIME.
24	
25	UPEAR=1.0384
26	C STIFF IS THE MINIMUM STATIC STIFFNESS DESIRED.
20	C(N) = C(0, 0, 0)
28	
29	CON3 = CD + PI + DI + DSOBT(2, O/RHO)
30	CON4 = -2.0 + CV + CD + PI + D2 + ANG
31	CON10=0.25*PI*D1**2
32	P2IC=0.5*(P1+PE)
33	P4IC=(P1*D3**4+16.0*PE*D1**2*X0**2)/(D3**4+16.0*D1**2*X0**2)
34	AE=0.25*PI*D2**2
35	C1=-1.0+KFBK
36	C2=C0N10
37	C4≖K3/(K2+K3)
38	C5=1.0/(K2+K3)
39	$C6 \approx -0.5 \approx CON2/(DSQRT(P1-P4IC))$
40	CB = CUN3 = USQR1(P4IC-PE)
41	C9=0.5*CUN3*XU/(DSQR1(P4IC-PE))
42	
43	UZZ~UJ/MU (793EV3
44	C24-1 0*C0N1*DS0PT(P1-P2TC)
46	$(30 \pm 1.0)((1.0 - CE) \pm 0M)$
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C42=BETA*DM/V1 C43=C22*BETA/V1 C44=-1.0*BETA/V1 C45=-1.0*BETA*DM/V2 C45=-1.0*C22*BETA/V2 C46=-1.0*C22*BETA/V2 C47=BETA/V2 48 49 50 51 52 53 54 55 56 57 C47=BETA/V2 C69=-9.636D+02 C70=-3.9161E-03 T1=C43-C46+C70*(C44-C47) T10=C9*C35-C6*C35 KWFL=(-1.0*STIFF*(K2+K3)/(K1*C1))*((2.0*C2*C5*C8-C6+C9)/ 1(C6*C23-C9*C23+2.0*C6*AE)*((2.0*C16-C23)*C22*C30/C24) 2-C4*C22*C30/C24) 58 TC-C4+C22+C30/C24) KVAL=(K1/(K2+K3))*(T10*C23-2.0*C8*C35*AE)/(C4*(2.0*C8*C35*AE-T10*C23)+(C23-2.0*C16)*(T10+2.0*C2*C5*C8*C35)) CALL STSET 59 60 61 NTRAC=0 MARCON MASK NONZERO PROHIBITS ANY CORRESPONDING CHANGE IN X. MASK(1)=1 MASK(2)=1 C C C C C SET DETERMINES WHICH MODEL IS OF INTEREST. SET=1.0 UNCOMPENSATED SERVOSYSTEM SET=3.0 PRESSURE FEEDBACK SERVOSYSTEM. SET=5.0 DYNAMIC PRESSURE FEEDBACK SERVOSYSTEM. С С С SET=5.0 DYNAMIC PRESSURE LEGENCE SET=3.0 XMIN(1) MINIMUM VALUE DF AMPLIFIER GAIN. XMIN(2) MINIMUM VALUE OF FEEDBACK GAIN XMIN(2)=0.00 XMIN(3) MINIMUM VALUE OF FEEDBACK TIME CONSTANT XMIN(3)=1.0D-07 62 С 63 с 64 С 65 66 67 JU=0 IF (SET.NE.3.0) GO TO 25 N1=3 68 69 70 71 72 73 74 75 76 77 80 81 82 83 84 N1=3 NV=2 X(1)=KWFL X(2)=2.5D-02 X(3)=0.0 G0 T0 45 25 IF (SET.NE.5.0) G0 T0 35 N1=4 NU=2 NV=3 X(1)=KWFL X(2)=1.786D-02 X(3)=0.5 GO TO 45 35 N1=3 NV=1 X(1)=0.29 X(2)=0.0 X(3)=0.0 85 X(3)=0.0 45 CONTINUE CALL STEPIT(SERVO) WRITE (6,55) STIFF 55 FORMAT('1',T10,'THE MINIMUM REQUIRED STATIC STIFFNESS (IN*LBF/RAD) 1 IS',T70,E12.5) WRITE (6,65) KWFL 65 FORMAT(/,T10,'THE REQUIRED AMPLIFIER GAIN (MA/VOLT) IS',T70,E12.5) ST=((2.0*C16-C23)*C22*C30)/C24*(2.0*C2*C5*C8-C6+C9)/ 1(C6*C23-C9*C23+2.0*C8*AE)-C4*C22*C30/C24 86 87 88 89 90 91 92

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STIF=-1.0*K1*C1*X(1)/(ST*(K2+K3)) WRITE (6,75) STIF 75 FORMAT(/,T10,'THE STATIC STIFFNESS ACTUALLY OBTAINED (IN*LBF/RAD) 115',T70,E12.5) WRITE (6,85) X(1) 85 FORMAT(/,T10,'FINAL VALUE FOR AMPLIFIER GAIN (MA/VOLT) IS',T70, 1622 95 B5 FORMAI(/,110,'FINAL VALUE FOR AMPLIFIER GAIN (MA/VOLT) IS',T 1E12:5) IF (SET.EQ.1.0) GO TO 115 WRITE (6,95) X(2) 95 FORMAT (/,T10,'FINAL VALUE FOR FEEDBACK GAIN (VOLT/PSI) IS', 1T70,E12:5) IE (SET.EQ.2.0) CO TO 14E 11/0,E12.5) IF (SET.EQ.3.0) GO TO 115 WRITE (6,105) X(3) 105 FORMAT(/,TIO.'FINAL VALUE OF FEEDBACK TIME CONSTANT (1/SEC) IS', 1T70,E12.5) 115 CONTINUE JJ=1 UJ=1 CALL SERVO JJ=2 X(1)=0.0 CALL SERVO WRITE (6,195) 195 FORMAT ('1') STOP END SUBROUTINE SERVO THE SUBROUTINE SERVO CALCULATES THE SOLUTION OF THE SYSTEM IN THE TIME DOMAIN. FROM THIS SOLUTION THE RISE TIME AND SETTLING TIME ARE CALCULATED. С TIME DDMAIN. FROM THIS SOLUTION THE RISE TIME AND SETTLING TIME ARE CALCULATED. DOUBLE PRECISION XMAX,XMIN,DELTX,DELMN,ERR,FDBJ,X DDUBLE PRECISION MU,II,CF,CDM,DM,PI,PJ,ABSERR,KVAL,C1,C42,C43, 1C44,C45,C46,C47,C69,C70,T1,C32,VISD DDUBLE PRECISION TRISE,TSET,DRISE,DSET,DPEAK,PEAK DDUBLE PRECISION TRISE,TSET,DRISE,DSET,DPEAK,PEAK DDUBLE PRECISION TRISE,TSET,DRISE,DSET,DPEAK,PEAK DDUBLE PRECISION COE(20),RODTI(20),RODTI(20),XN(10),FN(10),DISL DOUBLE PRECISION ANS,ERROR,DC,PFH,PFJ,PFK,TIML,TIME,THET,SGN DOUBLE PRECISION ANS,ERROR,DC,PFH,PFJ,PFK,TIML,TIME,TRL,TRU COMMON TRISE,TSET,DRISE,DSET COMMON PFE,PFF,PFG,PFL,AA,BB,CC,FREQ,PHI,TIME,THET,SGN COMMON YF,FPF,PFG,PFL,AA,BB,CC,FREQ,PHI,TIME,THET,SGN COMMON YF,N,DISL,ABSERR,ANS,ERROR COMMON N,N,FN,DISL,ABSERR,ANS,ERROR COMMON N,N,FAIL,IQUIT,NN,MAXDEG,JJ COMMON /ASS/PI,C1,C42,C43,C44,C45,C46,C47,C69,C70,T1,KVAL,CF, 1DM,PJ,CDM,MU,II,DPEAK,VISD,SET COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20), * ERR(20,21),FOBJ,NV,NTRAC,MATRX,MASK(20), * NFMAX,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERFLW,KW STATEMENTS C1 THROUGH RB CALCULATES CONSTANTS DESCRIBING THE SYSTEM AND ARE USED TD DETERMINE THE COEFFICIENTS OF THE DIFFERENTIAL EQUATION. C32+-1.0*X(2) R1+(1,-CC)*DM R2+DJ*T1+(COM+DM+MU+VISD) R3=T1*(CDM+DM+MU+VISD)-(1.0-CF)*DM*(C45-C42) R4+X(1)*KVAL*R1*(C47-C44)*C69 R5×X(3)*R2+R2-X(1)*KVAL*C69*(C47-C44)*C32*X(3)*PJ R6*X(3)*R3+R2-X(1)*KVAL*C69*(C47-C44)*C32*X(3)*(CDM+DM+MU+VISD) R7*R3-C1*R4*X(3) R8+-1.0*C1*R4 С С Ċ С 131

R7=R3-C1+R4+X(3)

R8=-1.0*C1*R4

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R9=R1*R2+R4*X(2)*PU R10=R1*R3+R4*X(2)*(CDM*DM*MU+VISD) R11=-1.0*R1*R4*C1 COE(1) THROUGH COE(5) ARE THE COEFFICIENTS OF THE DIFFERENTIAL EQUATION DESCRIBING THE SYSTEM. c c EQUATION DESCRIBING THE SYSTEM. IF (SET.NE.3.0) GO TO 50 CDE(1)=PU*R1 CDE(2)=R9 CDE(3)=R10 CDE(4)=R11 GD TO 70 50 IF (SET.NE.5.0) GO TO 60 CDE(1)=X(3)*PJ CDE(2)=X(3)*R2+PJ-X(1)*KVAL*C69*(C47-C44)*C32*X(3)*PJ CDE(3)=X(3)*R3+R2-X(1)*KVAL*C69*(C47-C44)*C32*X(3)*(CDM*DM*MU+ IVISD) 148 IVISD) 1VISD) CDE(4)=R3-C1+X(3)+X(1)+KVAL+R1+(C47-C44)+C69 CDE(5)=-1.0*C1+X(1)+KVAL+R1+(C47-C44)+C69 GO TO 70 GO CDE(1)=PJ CDE(2)=R2 CDE(2)=R2 CDE(4)=-1.0*C1+R4 70 CONTINUE C THE SUBROUTINE MULER SOLVES FOR THE ROOTS OF THE EQUATION. CALL MULER IF (NFAIL.EQ.O) GD TD 140 WRITE (6,130) 130 FORMAT (//,T10,' THE SUBROUTINE MULER FAILDED TO FIND ALL ROOTS.') FOBU=0.0 FOBJ=0.0 GD TO 5BO 140 IF (JJ.EQ.0) GD TD 165 IF (JJ.EQ.1) WRITE (6,150) 150 FORMAT(/,T10,'THE CLOSED LOOP POLES ARE') IF (JJ.EQ.2) WRITE(6,151) 151 FORMAT(/,T10,'THE OPEN LOOP POLES ARE') WRITE (6,160) (I,ROOTR(I),ROOTI(I),I=1,M1) 160 FORMAT (/,15X,'X(',I1,')= ',E15.5,'+(',E15.5,') I') 165 CONTINUE IF (JJ.EQ.2) GD TD 580 IF (JJ.EQ.2) GO TO 580 KK=0 LL≇0 C THESE NEXT STATEMENTS CHECK WHETHER OR NOT THE SYSTEM IS STABLE C BY LOOKING AT THE SIGN ON THE REAL PART OF THE ROOTS OF THE EQUATION. DO 170 I*1,N1 IF (ROOTR(I).LE.O.O) GO TO 170 WRITE (6,300) 300 FORMAT (//,T10.' THE SYSTEM IS UNSTABLE.') č 178 FOBJ=0.0 WRITE (6,302) X(1),X(2),X(3) 302 FDRMAT_(T10,'X(1)= ',D14.5,5X,'X(2)= ',D14.5,5X,'X(3)= ',D14.5) GO TO 580 170 CONTINUE С THESE NEXT STATEMENTS CHECK WHETHER OR NOT THE SYSTEM IS TOO STABLE BY ALL THE ROOTS BEING REAL AND NEGATIVE NOT HAVING COMPLEX CONJUGATES С DO 310 I=1,N1 IF (DABS(ROOTI(I)).GE.1.OD-O5) GO TO 420 310 CONTINUE

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wRITE (6.320)
320 FORMAT (//,T10,' ALL ROOTS ARE REAL.')
FOBJ=0.0
GD TO 580
FIND OUT WHICK ROOTS ARE REAL AND WHICH ONES ARE COMPLEX CONJUGATES
FOR PARTIAL FRACTION EXPANSION.
CALCULATE THE VALUES REQUIRED FOR THE PARTIAL FRACTION EXPANSION.
420 DD 460 I=1,N1
IF (DABS(ROOTI(I)).GE.1.0D-05) GD TD 450
KK+K+1 С С С 420 DD 460 I=1,N1 IF (DABS(RODT1(I)).GE.1.0D-05) GD TD 450 KK+KK+1 GD TD (430,440).KK 430 AA=-1.0*RODTR(I) GD TD 460 440 BB=-1.0*RODTR(I) GD TD 460 450 LL=LL+1 IF (LL.NE.1) GD TD 460 CC=-2.0*RODTR(I) DC=RODTR(I)*2+RODTI(I)*2 460 CONTINUE IF (N1.EQ.3) GD TD 475 C PFE IS STEADY STATE VALUE. PFE=RA+II/(X(3)*AA*BB*DC*PJ) C PFG IS THE CDEFFICIENT OF ONE OF THE REAL POLES. PFFG+((AA*CC-AA*2-DC)*(RA*1I/PJ-(PFE*AA*BB*CC+PFE*AA*DC-PFE*AA 1*2*BB))+(PFE*AA*CC-PFE*AA*2)*(CC*AA*BB-AA*2*BB*BB*DC))/((AA* 2CC-AA*2-DC)*(AA*BB-BB*DC)) PFH=(FE*AA*2-PE)*(AA*BB-BB*DC)) PFH=(FFE*AA*2-PE)*AA*2*BB-BB*DC) PFH=1.0*PFE*AA*2-PFE*AA*2)*BDC PFF=1.0*PFE*AA*2-DC)* GPF= IS THE CDEFFICIENT OF ONE OF THE REAL POLES. PFF=1.0*PFE*AA*2+DFB*(BB-AA)*PFH*(CC-AA) C PFF IS THE CDEFFICIENT OF ONE OF THE REAL POLES. PFF=1.0*PFE*AA*2+DFB*AA*2+BB+ADC-BB*DC) PFH=1.0*PFE*AA*2+DFB*AA*2+BB+ADC-BB*CC-AA*2)/ 1(AA*CC-AA*2+DC) PFF=1.0*PFE*AA*2+DFB*AA*2+BB+ADC+BB*2-BB*CC-AA*2)/ 1(AA*CC-AA*2+DC) PFF=1.0*PFE*AA*DFG*(BB-AA)+PFH*(CC-AA) C PFF IS THE CDEFFICIENT OF ONE OF THE REAL POLES. PFF=1.0*PFE*AA*DFG+(BB-AA)+PFH*(CC-AA) C PFF=1.0*PFE*AA*DFG+(BB-AA)+PFH*(CC-AA) C PFF=1.0*PFE*AA*DFG+(BB-AA)+PFH*(CC-AA) C PFF=4A+1I/(PJ*AA*DC) 212 GD TD 478 475 PFG=0.0 PFE=R4+II/(PJ+AA+DC) PFH=(PFE=AA+22-PFE+AA+CC)/(AA+CC-DC-AA++2) PFJ=PFH+(CC-AA)-PFE+AA PFF=-1.0*PFE-PFH C FREQ IS THE DAMPED NATURAL FREQUENCY OF THE COMPLEX CONJUGATES. 478 FRE0=DSQRT(4.0*DC-CC+2)/2.0 PFK=(PFJ-PFH+CC/2.0)/FRE0 C PHI IS THE PHASE SHIFT IN THE SINE TERM IN THE COMPLEX CONJUGATES. PHI=DATAN(PFH/PFK) C PFI IS THE COFFFICIENT OF THE COMPLEX CONJUGATE POLES. 219 C PFL IS THE COEFFICIENT OF THE COMPLEX CONJUGATE POLES. PFL=PFK/(DCOS(PHI)) PFL=PFK/(DCOS(PHI)) IF (JJ.NE.1) GO TO 105 WRITE (6,15) PFE 15 FORMAT(/,T10,'STEADY STATE DISPLACEMENT (RAD) IS',T70,E12.5) WRITE (6,25) PFF 25 FORMAT(/,T10,'CDEFFICIENT OF FIRST REAL POLE TERM IS',T70,E12.5) WRITE (6,35) AA IF (N1.EQ.3) GO TO 58 35 FORMAT(/,T10,'EXPONENT OF THE FIRST REAL POLE IS',T70,E12.5) WRITE (6,45) PFG 45 FORMAT(/,T10,'CDEFFICIENT OF SECOND REAL POLE TERM IS',T70,E12.5) WRITE (6,55) BB 55 FORMAT(/,T10,'EXPONENT OF SECOND REAL POLE IS',T70,E12.5) 58 CCC=0.5*CC 223 225 227 229

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WRITE(6,65) PFL 65 FORMAT(/,T10,'COEFFICIENT OF SINUSOIDAL TERM IS',T70,E12.5) WRITE (6,75) CCC 75 FORMAT(/,T10,'EXPONENT OF SINUSOIDAL TERM IS',T70,E12.5) WRITE (6,85) FREQ 85 FORMAT(/,T10,'RESPONSE DAMPED NATURAL FREQUENCY (RAD/SEC) IS', 1770,E12.5) WRITE (6,95) PHI 95 FORMAT(/,T10,'PHASE SHIFT OF SYSTEM RESPONSE (RAD) IS',T70,E12.5) 105 CONTINUE M=0 M=0 C TIMP IS THE TIME WHERE THE FIRST MAXIMUM OF THE SINE TERM OCCURS. TIMP=(1.5*PI-PHI)/FREQ TIME=TIMP 246 TIME=TIMP TIML=TIMP CALL DISP PEAK=THET IF (JJ.NE.1) GO TO 145 WRITE (G.115) THET 115 FORMAT (/,T10,'RESPONSE PEAK DISPLACEMENT (RAD) IS',T70,E12.5) WRITE (G.135) TIMP 135 FORMAT(/,T10,'TIME (ŞECS) PEAK DISPLACEMENT OCCURS IS',T70,E12.5) 145 CONTINUE 250 254 145 CONTINUE IF (THET.LT.(0.9*PFE)) GO TO 497 TIME=TIMP+0.02*PI/FREQ 490 TIME=TIME-0.02*PI/FREQ 258 CALL DISP IF (THET.GE.(0.9*PFE)) GD TO 490 TIML=TIME TIML=TIME C OBTAIN DATA POINTS TO INTERPOLATE FOR 90% VALUE IN RISE TIME. DO 495 K=1,10 PK=K PK=K) FN(K)=TIML+(PK-1.0)*(0.02*PI/FREQ)/9.0 TIME=FN(K) CALL DISP XN(K)=THET 265 267 269 495 CONTINUE DISL=0.9*PFE C INTERPOLATE TO THE FIND THE 90% POINT. CALL INTPOL TRU=ANS 271 272 M=M+1 274 275 276 497 TIME=TIML 500 TIME=TIME-0.02*PI/FREQ CALL DISP IF (THET.GE.(0.1*PFE)) GO TO 500 TIME=TIME C OBTAIN DATA POINTS TO INTERPOLATE FOR 10% VALUE IN RISE TIME. DO 505 K=1,10 PK=K FN-FN FN(K)=TIML+(PK-1.0)*(0.02*PI/FREQ)/9.0 TIME=FN(K) CALL DISP XN(K)=THET 281 283 -505 CONTINUE DISL=0.1*PFE C INTERPOLATE TO FIND THE 10% POINT. CALL INTPOL 285 TRI = ANS C IN THE EVENT THAT THE SOLUTION HAS A VERY DOMINANT REAL POLE THE

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FIRST SINE PEAK MAY NOT HAVE REACHED THE 90% POINT. IF THIS IS TRUE FIND WHERE THE 90% POINT IS LOCATED. IF (M.NE.O) GO TO 520 TIME*TIMP 510 TIME*2.0*PI/FREQ с с 290 510 TIME*TIME*2.0*PI/FREQ CALL DISP IF (TIME.LT.(100.*PI/FREQ)) GD TO 525 WRITE (6,535) 535 FORMAT(//,T10,' THE RISE TIME IS TOO SLOW.') FOBJ*0.0 GO TO 580 525 IF (THET.LT.(0.9*PFE)) GO TO 510 527 TIME*TIME~0.02*PI/FREQ CALL DISP IF (THET.GE.(0.9*PFE)) GO TO 527 TIML*TIME 292 294 296 298 300 IF (THET.GE.(0.9*PFE)) GO TO 527 TIME-TIME C OBTAIN DATA POINTS TO INTERPOLATE FOR 90% VLAUE IN RISE TIME. DO 515 K=1,10 PK=K FN(K)=TIML+(PK-1.0)*(0.02*PI/FREQ)/9.0 TIME=FN(K) CALL DISP XN(K)=THET 515 CONTINUE 307 XN(K) THET 515 CONTINUE DISL=0.9*PFE C INTERPOLATE TO FIND THE 90% POINT. CALL INTPOL TRU=ANS C CALCULATE THE RISE TIME OF THE SYSTEM. IE, THE TIME TO GO FOR THE C FIRST TIME FROM THE 10% VALUE OF STEADY STATE TO THE 90% VALUE OF C STEADY STATE. 520 TRISE*TRU-TRL IF (JJ.EQ.1) WRITE(6,155) TRISE 155 FORMAT(/,T10,'RESPONSE RISE TIME (SECS) IS',T70,E12.5) C THE NEXT THING NECESSARY TO CHECK IS THE RESPONSE SETTLING TIME. C THE TIME WHEN THE BOUNDS ON THE SOLUTION COMES WITHIN 5% OF THE C STEADY STATE VALUE IS THE POINT WANTED. TIME=0.02*PI/FREQ SGN=1.0 C CHECK THE ENVELOPE OF THE SINE WAVE ON THE LOW SIDE OF STEADY STATE C VALUE. 311 314 CHECK THE ENVELOPE OF THE SINE WAVE ON THE LOW SIDE OF STEAD VALUE. 540 CALL ENVEL IF (THET.GT.(0.95*PFE)) GO TO 550 TIME*TIME+0.02*PI/FREQ IF (TIME.GT.(100.*PI/FREQ)) GD TO 545 GO TO 540 545 WRITE (6,547) 547 FORMAT (1X,'THE SETTLING TIME IS TOD LARGE.') FOBJ*0.0 GO TO 580 550 TIMU*TIME TIMU*TIME-0.02*PI/FREQ OBTAIN DATA POINTS FOR 95% ENVELOPE VALUE IN SETTLING TIME. INTERPOLATE TO FIND 95% ENVELOPE VALUE IN SETTLING TIME. INTERPOLATE TO FIND 95% ENVELOPE VALUE IN SETTLING TIME. INTERPOLATE TO FIND 95% POINT. DO 560 K=1, 10 PK=K FN(K)*TIML+(TIMU-TIML)*(PK-1.0)/9.0 С 319 325 с с 329 FN(K)=TIML+(TIMU-TIML)*(PK-1.0)/9.0 TIME=FN(K) CALL ENVEL XN(K)=THET

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334 335 560 CONTINUE DISL=0.95*PFE CALL INTPOL TSET=ANS 336 337 CHECK THE ENVELOPE OF THE SINE WAVE ON THE HIGH SIDE OF STEADY STATE VALUE. с č SGN=-1.0 TIME=TSET 338 TIME *TSET CALL ENVEL C IF THE 105% POINT DOES NOT MEET THE SETTLING TIME REQUIREMENTS C PROCEED AS BEFORE TO FIND SETTLING TIME USING THE UPPER BOUND. IF (THET.LT.(1.05*PFE)) GD TO 610 565 CALL ENVEL IF (THET.LT.(1.05*PFE)) GD TD 590 TIME=TIME+0.02*PI/FREQ IF (TIME.GT.(100.*PI/FREQ)) GD TD 545 GD TD 565 590 TIMU=TIME TIML*TIME TIML*TIME-0.02*PI/FREQ DD 600 k*1,10 PK=K 339 340 341 342 343 344 345 346 347 348 349 PK=K FN(K)=TIML+(TIMU-TIML)+(PK-1.0)/9.0 350 351 TIME=FN(K) CALL ENVEL XN(K)=THET 352 353 354 XN(K)=THET GOO CONTINUE DISL=1.05*PFE CALL INTPOL 610 TSET=ANS IF (JJ.NE.1) GO TO 185 WRITE (6,166) TSET 166 FORMAT(/,T10,'RESPONSE SETTLING TIME (SECS) IS',T70,E12.5) WRITE (6,175) DISL 175 FORMAT(/,T10,'RESPONSE ENVELOPE VALUE (RAD) AT WHICH SETTLING TIME 1 OCCURS',T70,E12.5) 185 CONTINUE 355 356 357 358 359 360 361 362 363 364 185 CONTINUE THE OBJECTIVE FUNCTION FOR MINIZATION С FOBJ×TSET FOBJ=DABS(TSET-DSET) 365 С 366 580 RETURN 367 END SUBROUTINE MULER 368 c c MULER MULER 2 3 MULER 3.0 A.N.S.I. STANDARD FORTRAN JUNE 1974 MULER c c 4 FINDS ALL ROOTS OF A POLYNOMIAL HAVING REAL COEFFICIENTS, USING 5 C C MULLER-S METHOD. MULER 67 J. P. CHANDLER, COMPUTER SCIENCE DEPT., OKLAHOMA STATE UNIVERSITY (THE ORIGINAL VERSION OF THIS ROUTINE WAS DISTRIBUTED BY -SHARE-.) MULER c c 8 9 Ċ MULER 10 MULER 11 MULLER-S METHOD GIVES SLOW CONVERGENCE AND POOR ACCURACY ON MULTIPLE OR CLUSTERED ROOTS. SO DO MOST OTHER METHODS. MULLER-S METHOD IS NOT INHERENTLY RESTRICTED TO REAL COEFFICIENTS. c c MULER 12 č MULER 13 MULER 14 15 С c P. HENRICI, -ELEMENTS OF NUMERICAL ANALYSIS- (WILEY) MULER MULER 16 MULER 17 č INPUT QUANTITIES COE(J) -- THE COEFFICIENT OF Z**(N1+1-J), J=1,...,N1+1 MULER 1

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	00000000000	N1 - IQUIT - OUTPUT QUANTIT ROOTR(K) - ROOTI(K) - NFAIL -	 THE ORDER OF THE POLYNOMIAL 1 IF MULER IS TO RETURN IMMEDIATELY UPON FINDING A ROOT THAT IS REAL AND POSITIVE, O IF MULER IS TO COMPUTE ALL ROOTS IES THE REAL PART OF THE K-TH ROOT, K=1,,N1 THE IMAGINARY PART OF THE K-TH ROOT RETURNED NONZERO IF MULER FAILED TO FIND ALL ROOTS 	MULER MULER MULER MULER MULER MULER MULER MULER MULER	19 20 21 22 23 24 25 26 27 28
	с С	ALL FLUATING-P	UINI VARIABLES ARE DOUBLE PRECISION	MULER	29
369	U	DOUBLE PREC	ISION AXI.AXR.TEM.TE1.TE2.TE3.TE4.TE5.TE6.TE7.TE8	MULER	30
370		DOUBLE PREC	ISION TE9, TE10, TE11, TE12, TE13, TE14, TE15, TE16, BELL		
371		DOUBLE PREC	ISION DE15, DE16, HELL, TEMI, TEMR, TEM1, ALP11, ALP1R, ALP21		
372		DOUBLE PREC	ISION ALP2R, ALP3I, ALP3R, ALP4I, ALP4R, BET1I, BET1R		
373		DOUBLE PREC	ISION BET2I, BET2R, BET3I, BET3R, ARG, QSQRT, DSQRT, RZERO		
374			ISION RHALF, RUNIT, RIWU, RFUUR, RSMAL, EPS, CONSA, CONSB		
376			ISION CONSC, CONSC, AA, DB, ABI, IMAX, IEM2		
	с	DOODEL THEO	1010H 002(20); NODIN(20); NODII(20)	MULER	37
377		DOUBLE PREC	ISION TRISE, TSET, DRISE, DSET, PFE, PFF, PFG, PFL, AZ		•••
378		DOUBLE PREC	ISION BZ, CZ, FREQ, PHI, TIME, THET, SGN, XN(10), FN(10)		
379		DOUBLE PREC	ISION DISL, ABSERR, ANS, ERROR		
380		COMMON TRI	SE, TSET, DRISE, DSET	•	
381		COMMON PFE	, PFF, PFG, PFL, AZ, BZ, CZ, FREQ, PHI, TIME, THET, SGN		
382			RUUIR, RUUII		
384		COMMON N1	NEATL TOUTT NN MAYDEG (1)		
	С			MULER	39
	С	QSQRT(ARG)=	SQRT (ARG)	MULER	40
385		QSQRT(ARG)=	DSQRT (ARG)	MULER	41
	С			MULER	42
	c		SET ALL CONSTANTS.	MULER	43
200	С	KH- 0	KW LOGICAL UNIT NUMBER OF THE PRINTER	MULER	44
380	c	KW=6		MULER	45
387	C		CONSA, EIC THREE STARTING PUINTS	MULER	46
388		CONSE= 85		MILLER	48
389		CONSC=.9		MULER	49
	С		RSMAL RELATIVE CONVERGENCE TOLERANCE	MULER	50
	С		FOR THE MAGNITUDE OF THE POLYNOMIAL	MULER	51
	С	RSMAL = 1.E-2	0	MULER	52
390	~	RSMAL×1.E-1	0	MULER	53
	C		EPS RELATIVE CONVERGENCE TOLERANCE	MULER	54
	č		FUR THE STEP SIZE (EPS AND RSMAL MUST	MULER	55
	č		FLOATING-DOINT ADITHMETIC USED)	MILLER	57
391	Ũ	EPS=1.0E-10)	MULLK	37
	С		CONSD RELATIVE TOLERANCE FOR CHECKING	MULER	59
	С		WHETHER A ROOT IS REAL	MULER	60
392		CONSD=1.E-5		MULER	61
	С		ITMAX MAX. NO. OF ITERATIONS PER ROOT	MULER	62
393		I I MAX = 100		MULER	63
394		RZERU=U.		MULER	64
396		RUNIT=1		MULER	66
397		RTWO=2.		MULER	67
398		RFOUR=4.		MULER	68
	С		INITIALIZE.	MULER	69

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399 400 401 402 403	NFAIL=0 MC=10 N2=N1+1 N4=0 T=N1+1	MULER 70 MULER 71 MULER 72 MULER 73
404 405 406 407 408 409	C REMOVE ANY ZERO RODTS. 100 IF(COE(I))120,110,120 110 N4=N4+1 RODTR(N4)=RZERO RODTI(N4)=RZERO I=I-1 IF(N4-N1)100,630,100	MULER 75 MULER 75 MULER 77 MULER 77 MULER 78 MULER 78 MULER 79 MULER 81
	C C COMPUTE THE FIRST THREE (POSITIVE REAL) ITERATES FOR THE N	MULER 82 IEXT ROOT. MULER 83
410 411 412 413 414 415 416 417	120 AXR=CONSA AXI=RZERO L=1 N3=1 ALP1R=AXR ALP1I=AXI M=1 GD TO 680	MULER 84 MULER 85 MULER 86 MULER 87 MULER 88 MULER 89 MULER 91 MULER 92
418 419 420 421 422 423 424 425 426 426 427	130 BEI1R=IEMR BEI1I=TEMI AXR=CONSB ALP2R=AXR ALP2I=AXI M=2 G0 T0 680 140 BET2R=TEMR BET2I=TEMI AXR=CONSC ALP2D=AXD	MULER 93 MULER 94 MULER 95 MULER 96 MULER 97 MULER 98 MULER 99 MULER 99 MULER 100 MULER 101
429 430	ALP3I=AXI M=3	MULER 103 MULER 104 MULER 105
431 432 433	C THE THREE ITERATES ARE COMPLETE. 150 BET3R*TEMR BET3I*TEMI C REGIN THE NEXT ITERATION OF MULLER-S METHOD	MULER 106 MULER 107 MULER 108 MULER 109 MULER 110
434 435 436 437 438 440 441 442 443 444 445 444 445 444 447 448 449	C COMPUTE (IN HENRICI-S NOTATION) H(N)=X(N)-X(N-1)=ALP(N)-AL C 160 TE1=ALP1R-ALP3R TE2=ALP1I-ALP3I TE5=ALP3R-ALP2I TE6=ALP3I-ALP2I TEM=TE5*TE5+TE6*TE6 IF(TEM)170,180,170 170 TE3=(TE1*TE5+TE2*TE6)/TEM TE4=(TE2*TE5-TE1*TE6)/TEM G0 T0 190 TE4=RZER0 TE4=RZER0 190 TE7=TE3+RUNIT TE9=TE3*TE3-TE4*TE4 TE10=RTW0*TE3*TE4*BET3I DE16=TE7*BET3I+TE4*BET3I DE16=TE7*BET3I+TE4*BET3R	MULER 112 MULER 113 MULER 113 MULER 114 MULER 115 MULER 117 MULER 117 MULER 117 MULER 120 MULER 122 MULER 123 MULER 125 MULER 126 MULER 126 MULER 127 MULER 128 MULER 129

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450			TF11+TF3+RFT3P-TF4+RFT31+RFT4P-DF46	
451				MULERISC
451			1012-103-00121+104-0012R+80111-0016	MULER 131
452				MULER132
453			TE1=1E9*BE12R-TE10*BET21	MULER 133
454			TE2=TE9=BET21+TE10=BET2R	MULER 134
455			TE 13=TE 1-BET 1R-TE7*BET3R+TE 10*BET3I	MULER 135
456			TE 14=TE2-BET 11-TE7+BET3I-TE 10+BET3R	MULER 136
457			TE 15=DE 15+TE3-DE 16+TE4	MULER 137
458			TE 16=DE 15*TE4+DE 16*TE3	MULER 138
459			TE 1=TE 13+TE 13-TE 14+TE 14-RFOUR+(TE 11+TE 15-TE 12+TE 16)	MULER 139
460			TE2=RTWO*TE13*TE14-RFOUR*(TE12*TE15+TE11*TE16)	MULER 140
461			TEM=QSQRT(TE1+TE1+TE2+TE2)	MULER 14
	С			MULER 143
	С		TEST THE SIGN	MULER 143
462			IF(TE1)200,200,240	MULERIA
463		200	TE4=0SORT(RHALE*(TEM-TE1))	MULEDIAE
464			IE(IE4)230 210 230	MULER 145
465		210		MULER 140
466		220	FOPMAT(1) $T(7)$	MULER 14
400		220	NEAT - (//, 12/, ERROR IN SUBROUTINE MULLER', 3220.8)	
407				MULER 149
400				MULER 150
469				MULER 15
470			GU 10 290	MULER 152
4/1		230	IE3=RHALF*IE2/IE4	MULER 153
472			GO TO 290	MULER 154
473		240	TE3=QSQRT(RHALF*(TEM+TE1))	MULER 155
	С			MULER 156
	С		TEST THE SIGN	MULER 157
474			IF(TE2)250,260,260	MULER 158
475		250	TE3=-TE3	MULER 159
476		260	IF(TE3)280,270,280	MULER 160
477		270	NFAIL=2	MULER 161
478			GO TO 630	MULER 162
479		280	TE4=RHALF+TE2/TE3	MULER 163
480		290	TE7=TE13+TE3	MULER 164
481			TE8=TE14+TE4	MULER 165
482			TE9×TE 13-TE3	MULER 166
483			TE 10=TE 14-TE4	MULER 167
484			TE1=RTWO+TE15	MULERIGA
485				MULERIGO
486			IE(T7+TF7+TF8+TF8-TF9+TF9-TF10+TF10)300 300 310	MULER 103
487		200		MULER170
407		300		MULER171
400		310		MULER 172
403		310		MULER 173
490			IF (IEM)320, 330, 320	MULER 174
491		320	1E3=(1E1+1E7+1E2+1E8)/1EM	MULER 175
492			TE4=(TE2*TE7-TE1*TE8)/TEM	MULER 176
493			GO TO 340	MULER 177
494		330	TE3=RZERO	MULER 178
495			TE4=RZERO	MULER 179
496		340	AXR*ALP3R+TE3*TE5-TE4*TE6	MULER 180
497			AXI=ALP3I+TE3*TE6+TE4*TE5	MULER 18
498			ALP4R=AXR	MULER 182
499			ALP4I=AXI	MULER 183
	С		EVALUATE THE POLYNOMIAL AT THE NEW POINT.	MULER 184
500			M=4	MULER 185
501			GD TO 680	MULER 186
502		350	N6 = 1	MULER 187
	С			MULER 188
	С	EN	D OF THIS ITERATION OF MULLER-S METHOD.	MULER 189

	С	TEST THE VALUE OF THE POL	YNOMIAL FOR CONVERGENCE.	MULER 190
	С	THE TEST FORMERLY USED HE	RE WAS IF (ABS(HELL)+ABS(BELL)-RSMAL)	MULER 191
	С	THIS IS AN ABSOLUTE TEST.	AND CAN FAIL IF THE COFFFICIENTS ARE NOT	MULER 192
	C	PROPERLY SCALED USE A R	FLATIVE TEST INSTEAD	MILLER 192
	č			MULEDIOA
	ř		TE (AMAY (ADS (HELL) ADS (DELL)) DEMAL +THAY)	MULERISA
502	c		IF (AMAXI(ADS(HELL), ADS(DELL)) - RSMAL*IMAX)	MULER 195
504		1E(AA)260 270 270		MULERISS
504		IF(AA)360,370,370		MULER 197
505		360 AA=-AA		MULER 198
506		370 BB#BELL		MULER 199
507		IF(BB)380,390,390		MULER200
508		380 BB=-BB		MULER201
509		390 IF(BB-AA)410,410,400		MULER202
510		400 AA=BB		MULER203
511		410 IF(AA-RSMAL*TMAX)530,5	30,420	MULER204
	С			MULER205
	С		TEST THE CHANGE IN Z FOR CONVERGENCE.	MULER206
	С		THIS TEST IS RELATIVE.	MULER207
	с		TE7=ABS(ALP3R-AXR)+ABS(ALP3I-AXI)	MULER208
512		420 AA=ALP3R-AXR		MULER209
513		IF(AA)430 440 440		NUL EP210
514		430 44=-44		MULED211
515		440 RB=AI P3I-AYI		MULER211
516				MULER212
517		AEO BRBR		MULER213
517				MULER214
510	~	460 TE/*AA+66		MULER215
	C		IF(TE7/(ABS(AXR)+ABS(AXI))-EPS)	MULER216
519		AA=AXR		MULER217
520		IF(AA)470,480,480		MULER218
521		470 AA=-AA		MULER219
522		480 BB=AXI		MULER220
523		IF(BB)490,500,500		MULER221
524		490 BB=-BB		MULER222
525		500 IF(TE7-EPS*(AA+BB))530	,530,510	MULER223
	С			MULER224
	С		NO CONVERGENCE. SHIFT THE ITERATES.	MULER225
526		510 N3=N3+1		MULER226
527		ALP1R=ALP2R		MULER227
528		ALP1I=ALP2I		MULER228
529		ALP2R=ALP3R		MULER229
530		AL P21 = AL P31		MULER230
531		AL P3P=AL P4P		MULEP231
532		AL DOLLAR DAT		MULER231
533		RET 1D+RETOD		MULED222
534		DET 11-DET2K		MULER233
534		BETTI-BETZI		MULER234
535		BEIZREBEIJR		MULER235
536		BE121=BE131		MULER236
537		BET3R=TEMR		MULER237
538		BET3I=TEMI		MULER238
539		IF(N3-ITMAX)160,160,52	20	MULER239
540		520 NFAIL=3		MULER240
	С		STORE THE ROOT.	MULER241
541		530 N4=N4+1	•	MULER242
542		ROOTR(N4)=ALP4R		MULER243
543		ROOTI(N4)=ALP4I		MULER244
544		N3=O		MULER245
	С		HAVE WE FOUND ALL ROOTS	MULER246
545		IF(N4-N1)540,630,630		MULER247
	С		NO. WAS THIS ROOT REAL	MULER248
	С		IF(ABS(ROOTI(N4))-CONSD*ABS(RODTR(N4)))	MULER249

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546		540	AA=RODTI(N4)		MULER250
547			IF(AA)550.560.560		MULER251
548		550	AA=-AA		MULER252
549		560	ABT=ROOTR(N4)		MULER253
550			IF (ABT) 570, 580, 580		MILLER254
551		570	ABT=-ABT		MILEP255
	С	0.0		CHECK FOR THE -LOUIT- ORTION	MULEP256
552	Ŭ	580	IF (10UIT) 600, 590, 600	SHEEK FOR THE TOUT OF TIDA.	MULEP257
	С				MULED258
553	•	590	IE(AA-CONSD+ABT) 120 120	640	MULED250
554		600	IF(AA-CONSD*ABT)610 610	640	MULER255
555		610	IE(PODTP(NA))120 120 62	0	MULER260
556		620	N1=N4		MULER201
556	r	620	141-144	THIS IS THE ONLY DETURN STATEMENT	MULER262
557	C	620	DETHION	THIS IS THE UNLE RETURN STATEMENT.	MULER203
357	~	830	RETORN	LE ONE NON-DEAL DOOT OF A CONJUGATE DATE	MULER264
	č			IF ONE NON-REAL RUUT OF A CONJUGATE PAIR	MULER265
	C	C 40	CO TO(CEO (200))	HAS BEEN FUUND,	MULER266
556	~	640	GU 10(850,120),L		MULER267
	c	650		START AT ITS COMPLEX CONJUGATE.	MULER268
559		620			MULER269
560			AXI =-ALPII		MULER270
561			ALP1I =- ALP1I		MULER271
562			M=D		MULER272
563		-	GO TO 680		MULER273
564		660	BET 1R = TEMR		MULER274
565			BETTITEMI		MULER275
	С			GET TWO OTHER ITERATES ALSO.	MULER276
566			AXR=ALP2R		MULER277
567			AXI=-ALP2I		MULER278
568			ALP2I=-ALP2I		MULER279
569			M =6		MULER280
570			GO TO 680		MULER281
571		670	BET2R=TEMR		MULER282
572			BET2I=TEMI		MULER283
573			AXR=ALP3R		MULER284
574			AXI=-ALP3I		MULER285
575			ALP3I=-ALP3I		MULER286
576			L=2		MULER287
577			M≖3		MULER288
	С				MULER289
	С	TH	IS SECTION COMPUTES THE	VALUE (TEMR, TEMI) OF THE POLYNOMIAL AT	MULER290
	С	TH	POINT (AXR, AXI) USING	HORNER-S RULE (NESTED MULTIPLICATION).	MULER291
	С				MULER292
578		680	TEMR=COE(1)		MULER293
579			TEMI = RZERO		MULER294
580			TMAX=TEMR		MULER295
581			IF(TMAX)690,700,700		MULER296
582		690	TMAX=-TMAX		MULER297
583		700	DO 710 I=1.N1		MULER298
584			TE1=TEMR*AXR-TEMI*AXI		MULER299
585			TEMI=TEMI*AXR+TEMR*AX	1	MULER300
586		710	TEMR=TE1+COE(I+1)		MULER301
	с			COMPUTE THAX. THE MAGNITUDE OF THE LARGEST	MULER302
	č			TERM IN THE POLYNOMIAL	MULER303
587	-		TE 1=RUNIT		MULER304
588			TE2=R7FR0		MULER305
589			TMAX=COE(N1+1)	· •	MULER306
590			IF (TMAX)720.730.730		MULER307
591		720	TMAX=-TMAX		MULERSOR
592		730	DO 810 I=1.N1		MULER309

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	с		(TE1.TE2) = Z**I	MULER310
593	-		TE3=AXR+TE1-AXI+TE2	MILLER311
594				MUL ED212
595			TFITTE	MULERO12
200	c			MULER313
	č			MULERSIA
506	C		ABS(COE(U)*TEZ))	MULERSIS
507				MULERJIG
500				MULER317
500		740	TE9-TE9	MULERJIO
535		750	163-163 16(169-164) 170 770 770 770	MULERJIS
600		750	Tr(163-1MAX)//0,//0	MULER320
601		760	1MAA-1E3	MULER321
602		110		MULER322
603		700	17(123)/80,810,790	MULER323
604		780		MULER324
605		/90	IF (1E 3 - IMAX) B 10, B 10, B 00	MULER325
606		800	IMAX=IE3	MULER326
607		810	CONTINUE	MULER327
608			HELL=IEMR	MULER328
609			BELL=TEMI	MULER329
610	-		IF (N4)820,860,820	MULER330
	С		DEFLATE- NUMERICALLY DIVIDE THE	MULER331
	С		POLYNOMIAL BY	MULER332
	С		(Z-ROOT(1))(Z-ROOT(N4)).	MULER333
611		820	DO 850 I=1,N4	MULER334
612			TEM1=AXR-ROOTR(I)	MULER335
613			TEM2=AXI-ROOTI(I)	MULER336
614			TE1=TEM1+TEM1+TEM2+TEM2	MULER337
615			IF(TE1)840,830,840	MULER338
616		830	NFAIL=-N4	MULER339
617			GO TO 630	MULER340
618		840	TE2=(TEMR*TEM1+TEMI*TEM2)/TE1	MULER341
619			TEMI=(TEMI+TEM1-TEMR+TEM2)/TE1	MULER342
620			TEMR=TE2	MULER343
621		850	CONTINUE	MULER344
	С		-RETURN- TO THE APPROPRIATE POINT.	MULER345
622		860	GD TD(130,140,150,350,660,670),M	MULER346
	С			MULER347
	с	EN	D MULER.	MULER348
623			RETURN	
624			END	MULER349
625			SUBROUTINE INTPOL	
	С	TH	E SUBROUTINE INTPOL WAS MODIFIED FROM A PROGRAM IN 'NUMERICAL	
	С	CO	MPUTING: AN INTRODUCTION', SHAMPINE & ALLEN, SAUNDERS PUBLISHING	
	С	CO	., PG. 227-229.	
	С			
	с	IN	FPOL CONSTRUCTS AN INTERPOLATING POLYNOMIAL USING DIVIDED	
	С	DI	FFERENCES. THE USER CAN EITHER SPECIFY THE DEGREE TO BE USED OR	
	С	A 1	FOLERANCE AND A MAXIMUM DEGREE. IN THE LATTER CASE THE CODE USES	
	С	тні	E LOWEST DEGREE POLYNOMIAL WHICH IT BELIEVES MEETS THE TOLERANCE.	
	С			
	С		N - NUMBER OF NODES. N MUST BE AT LEAST 2. THE CODE DOES NOT	
	С		TEST FOR THIS.	
	С		XN - ARRAY OF NODES. MUST BE DISTINCT. THE CODE DOES NOT TEST	
	С		FOR THIS.	
	С		FN - ARRAY OF FUNCTION VALUES CORRESPONDING TO NODES XN.	
	С		XX - POINT AT WHICH INTERPOLATING POLYNOMIAL IS TO BE EVALUATED.	
	С		ANS - VALUE OF THE INTERPOLATING POLYNOMIAL AT XX.	
	С		ERROR - ESTIMATED ERROR OF ANS. THE VALUE ANS+ERROR IS OFTEN	

N - NUMBER DF NODES. N MUST BE AT LEAST 2. THE CODE DOES NOT TEST FOR THIS.
 XN - ARRAY OF NODES. MUST BE DISTINCT. THE CODE DOES NOT TEST FOR THIS.
 FN - ARRAY OF FUNCTION VALUES CORRESPONDING TO NODES XN.
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 ERROR - ESTIMATED ERROR OF ANS. THE VALUE ANS+ERROR IS OFTEN

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	С		A MORE ACCURATE RESULT BUT NOT ALWAYS.
	č		ABSERR - THE CODE TRIES TO CHOOSE THE DEGREE OF THE INTERPOLATING
	č		POLYNOMIAL SO THAT ABS(FREDR) IF ABSERR TO SPECIFY THE
	č		DEGREE. SET ABSERR NEGATIVE AND USE MAXDEG AS DESCREED BELOW
	č		MAXDEG - UPPER BOIND ON THE DECREE OF THE INTERPOLATING DOLYNOMIAL
	č		TE TOLEDANCE IS MET THE DEGREE OF THE DOLYNOMIAL IS DETIDINED
	č		IN MAYDER OTHERWISE MAYDER DEMANS AS AN INDUIT AND THE
	č		EDDOD TOLEDANCE MAY NOT LAVE DEEN NET IN THIS CASE THE
	č		USED CHOILD CHECK THE OUTDUIT OUANTITY EDDOD TE A DOLYNOUTAL
	č		DER SHOULD CHECK THE DUTPUT QUANTIT ERKUR, IF A PULTNUMTAL
	č		DECREE AND ADSERD TO ANY NEGATIVE VALUE MAXDEG NUST BE LEEP
	č		THAN OF SOUNT TO NEW COD DECORE A TOTAL OF MAD BOILTS ADE
	č		THAN UK EQUAL TO N=2 (FOR DEGREE & A TOTAL OF K+2 PUINTS ARE
	č		REQUIRED TO EVALUATE THE PULYNOMIAL AND TO ESTIMATE THE ERKOR.
	5		IF IT EXCEEDS THIS VALUE IT IS SET EQUAL TO N-2. SINCE MAXDEG
	C		IS USED FOR OUTPUT AS WELL AS INPUT IT MUST BE A VARIABLE IN
	C		THE CALLING PROGRAM.
626			DOUBLE PRECISION AA, ABSERR, ANS, BB, CC, ERROR, FN(10), FREQ, PFE
627			DOUBLE PRECISION PFF, PFG, PFL, PHI, PROD, THET, TIME, V(10, 10)
628			DOUBLE PRECISION XN(10),XX,TRISE,TSET,DRISE,DSET,SGN
629			DOUBLE PRECISION COE(20), ROOTR(20), ROOTI(20)
630			DIMENSION INDEX(10)
631			COMMON TRISE, TSET, DRISE, DSET
632			COMMON PFE, PFF, PFG, PFL, AA, BB, CC, FREQ, PHI, TIME, THET, SGN
633			COMMON COE,ROOTR,ROOTI
634			COMMON XN,FN,XX ,ABSERR,ANS,ERROR
635			COMMON N1,NFAIL,IQUIT,N ,MAXDEG,JJ
	С		INTPOL IS WRITTEN TO HANDLE PROBLEMS WITH UP TO 10 NODES.
	С		IF MORE NODES ARE DESIRED THE DIMENSION STATEMENTS MUST BE
	С		ALTERED TO HANDLE THE INCREASED NUMBER OF NOEDS.
636			MAXDEG=MINO(MAXDEG,N-2)
637			L=MAXDEG+2
638			LIMIT=MINO(L.N-1)
	С		DETERMINE AN ORDER FOR THE NODES XN(1) (STORED IN THE ARRAY
	С		INDEX) SUCH THAT XN(INDEX(I)) IS THE NODE CLOSEST TO XX.
	č		XN(INDEX(1)) IS THE SECOND CLOSEST, ETC. THE ARRAY XN IS NOT
	С		ALTERED
	Č		EVALUATE THE INTERPOLATING POLYNOMIAL AT XX.
639			DO 100 I=1.N
640			V(1, 1) = DABS(XN(1) - XX)
641		100	
642			
643			
644			DO 110 JETRI N
645			
6/6			
647			IE(V(II - 1) E V(II + 1)) CO TO 110
647			IF(V(II, I).LE.V(IU, I)) GU (U 110 ITEMD=INDEV(I)
648			$\frac{1}{1} = \frac{1}{1} = \frac{1}$
649			INDEA(1) = INDEA(0)
650			
651		110	
652		120	
653			
654			11=1NUEX(1)
655			AN5=FN(11)
656			V(1,1)=FN(I1)
657			D0 140 K=2,L
658			IK=INDEX(K)
659			V(K,1)=FN(IK)
660			KM1≖K-1
661			DD 130 I=1,KM1

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I1=INDEX(I)
130 V(K,I+1)=(V(I,I)-V(K,I))/(XN(II)-XN(IK))
IKM1=INDEX(KM1)
PROD=(XX-XN(IKM1))*PROD
ERROR=PROD*V(K,K)
IF (DABS(ERROR).GT.ABSERR) GD TO 140
WYPOCH(CALL) MAXDEG=K-2 RETURN 140 ANS=ANS+ERROR ANS=ANS-ERROR RETURN END SUBROUTINE DISP DOUBLE PRECISION AA.ABSERR.ANS.BB.CC.DISL. ERROR.FN(10) DOUBLE PRECISION PFE.PFG.PFL.PHI.POW1.POW2.POW3.THET.TIME DOUBLE PRECISION CDE(20).ROOTI(20).ROOTI(20) DOUBLE PRECISION COE(20).ROOTI(20) COMMON TRISE.TSET.DRISE.DSET COMMON PFE.PFF.PFG.PFL.AA.BB.CC.FRE0.PHI.TIME.THET.SGN COMMON COE.ROOTR.ROOTI COMMON N1.NFAIL.IOUIT.NN.MAXDEG.JJ C CALCULATE THET EXPONENT OF ONE REAL POLE. POW1+0.0 676 ERROR, FN(10), FREQ C CALCULATE THET EXPONENT DF ONE REAL POLE. POW1=0.0 IF (IDABS(AA*TIME)).GT.100.0) GD TO 100 POW1=DEXP(-1.0*AA*TIME) C CALCULATE THE EXPONENT OF ONE REAL POLE. 100 POW2=0.0 IF (IDABS(BB*TIME)).GT.100.0) GD TO 110 POW2=DEXP(-1.0*BB*TIME) C CALCULATE THE EXPONENT OF THE COMPLEX CONJUGATE PAIR. 110 POW3=0.0 IF (IDABS(CC*TIME)).GT.100.0) GD TO 150 POW3=DEXP(-0.5*CC*TIME) 150 COF1=0.0 IF ((IDABS(PFF)).LT.1.0D-10) GD TO 130 COF1=PFF 130 COF2=0.0 130 COF2=0.0 IF ((DABS(PFG)).LT.1.0D-10) G0 T0 140 COF2=PFG 140 PSI=0.0 IF ((DABS(FREQ*TIME+PHI)).LT.1.OD-10) GO TO 120 PSI=FREQ*TIME+PHI CALCULATE THE VALUE OF THE OUTPUT FOR A GIVEN VALUE OF TIME. 120 THET=PFE+COF1*POW1+COF2*POW2+PFL*POW3*DSIN(PSI) С 705 RETURN END SUBROUTINE ENVEL DOUBLE PRECISION AA, ABSERR, ANS, BB, CC, DISL, ERROR, FN(10), FREQ, PFE DOUBLE PRECISION PFF, PFG, PFL, PHI, POW1, POW2, POW3, THET, TIME DOUBLE PRECISION XN(10), TSET, TRISE, DRISE, DSET, SGN DOUBLE PRECISION COE(20), ROOTI(20). DOUBLE PRECISION COF1, COF2 COMMON PFE, PFF, PFG, PFL, AA, BB, CC, FREQ, PHI, TIME, THET, SGN COMMON COE, ROOTR, ROOTI 708 COE, ROOTR, ROOTI XN, FN, DISL, ABSERR, ANS, ERROR COMMON

716	COMMON N1, NFAIL, IQUIT, NN, MAXDEG, JJ	
	CALCULATE THE EXPONENT OF ONE REAL POLE.	
717	POW1=0.0	
718	IF ((DABS(AA*TIME)).GT.100.0) GO TO 100	
7 19	POW1=DEXP(-1.O*AA*TIME)	
	CALCULATE THE EXPONENT OF ONE REAL POLE.	
720	100 POW2=0.0	
721	IF ((DABS(BB*TIME)).GT.100.0) GD TO 110	
722	POW2=DEXP(~1.O*BB*TIME)	
	CALCULATE THE EXPONENT OF THE COMPLEX CONJUGATE PAIR	
723	110 POW3=0.0	
724	IF ((DABS(CC*TIME)).GT.100.0) GD TD 120	
725	POW3=DEXP(~O.5*CC*TIME)	
726	120 COF1=0.0	
727	IF ((DABS(PFF)).LT.1.0D-10) GO TO 130	
728	COF 1=PFF	
729	130 COF2=0.0	
730	IF ((DABS(PFG)).LT.1.0D-10) GD TD 140	
731	COF2=PFG	
732	140 THET=PFE+COF1*POW1+COF2*POW2+SGN*PFL*POW3	
733	RETURN	
734	END	

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APPENDIX F

SYSTEM PARAMETERS IN STUDY

This appendix contains the parameters which were utilized in the linear and non-linear system simulations. The parameters were obtained from various sources. Some were from component manufacturers, others from experiments performed by the different classes which used the test set-up, and still others from textbooks on the subject.

The parameters utilized in this study can be found in Table V.

TABLE V

EXPERIMENTAL SYSTEM PARAMETERS

Parameter	Value
Fluid bulk modulus	150,000 psi
Orifice discharge coefficient	0.625
Actuator friction coefficient	0.10
Valve spool radial clearance	5.0E-05 in
Actuator slip flow coefficient	0.88E-08
Actuator viscous drag coefficient	160,000
Steady state flow force velocity coefficient	0.98
Flapper nozzle control orifice diameter	0.023 in
Valve spool diameter	0.275 in
Fixed orifice diameter upstream from flapper nozzle	0.012 in
Displacement of actuator	1.512E-02 in ³ /rad
Actuator rotary inertia	2.16E-03 in 1b _f sec ² /rad
Torquemotor constant	0.05 lb _f /ma
Torquemotor constant	140 15 _f /in
Mechanical spring rate	22.5 lb _f /in
Distance between ports for unsteady flow forces	0.29 in
Spool length for viscous damping	0.384 in
Valve spool mass	3.2071E-05
Supply pressure	1,100 psi
Exhaust pressure	0 psi
Fluid density	7.85E-05 $lb_f sec^2/in^4$
Fluid absolute viscosity	2.0E-06 lb _f sec/in ²
External viscous drag	0.018 in lb_f sec
Flapper nozzle displacement at null	0.0018 in
Length of oil volume each end of spool	0.40 in
Volume under compression each oil line	25.0 in ³

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