

MATHEMATICAL MODELING OF COAL LIQUID

HYDROTREATMENT KINETICS

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PREFACE

This thesis work is an early portion of an effort to gain a comprehensive understanding of coal-derived liquid and other syn-fuel upgrading processes. Of the numerous individual processes taking place during this upgrading, or hydrotreatment, my attention was primarily focused on the removal of sulfur, nitrogen, and oxygen heteroatoms.

As a tool used to gain an understanding of the heteroatom removal processes I considered several types of both empirically and theoretically developed mathematical kinetic models. Using those models, I studied the reaction kinetics of the hydrotreatment of coal-derived liquids, which contain a complex mixture of reactants, and of reactant feeds containing a single model heterocompound.

Due to the theoretical nature of this study, the scarcity of applicable experimental data presented some difficulties. As a result, I limited the study of single heterocompound hydrotreatment to the hydrodesulfurization process.

I believe this work will be helpful to others in their continued effort to understand syn-fuel hydrotreatment. In as much, I know I have gained invaluable knowledge and experience through the completion of this work.

I would like to express my sincerest appreciation to my thesis advisor, Dr. Mayis Seapan, who, in addition to his instruction, has provided an unwavering source of friendly, patient support. Thanks also to Teresa Tackett for her skillful advice and production of this

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LIST OF SYMBOLS

A	pre-exponential constant in temperature dependent reaction rate and adsorption equilibrium constants, variable units
C _i	concentration of species i in liquid phase (mole% or wt%)
D	free-liquid diffusivity of heterocompound (cm ² /sec)
D _{eff}	effective diffusivity of heterocompound in catalyst pore (cm ² /sec)
E	reaction activation energy or heat of adsorption, variable units
k	reaction rate constant, variable units
k _{obs}	observed reaction rate constant (hr ⁻¹)
K _i	adsorption equilibrium constant of species i (l/mole% or l/wt%)
LHSV	liquid hourly space velocity (hr ⁻¹)
MW _L	molecular weight of solvent (g/gmole)
P _i	partial pressure of species i (psi or MPa)
P _c	critical pressure of solvent (atm)
r	reaction rate, variable units
r _{obs}	observed reaction rate (mole%/hr or wt%/hr)
R	gas constant, variable units
R _c	average catalyst particle radius (cm)
R _m	size of heterocompound molecule (angstroms)
R _p	average pore radius (angstroms)
S	solubility of hydrogen in solvent (g hydrogen/g solvent)
T	temperature (K or R)
T _c	critical temperature of solvent (K)

Tr	reduced temperature, unitless
V	reactor volume (cc)
V _L	molar volume of solvent at its normal boiling point (cc/g mole)
V _R	molar volume of heterocompound at its normal boiling point (cc/g mole)
W	weight of catalyst (g)
ε	catalyst void fraction, unitless
η	catalyst effectiveness factor, unitless
μ	viscosity of solvent (centipoise)
ρ	density of liquid (g/cc)
τ	catalyst tortuosity factor, unitless
ω	acentric factor, unitless

Superscripts

a, b, d, e, m, n	exponential power
' , "	first and second reference condition

Subscripts

A, B, D,	denotes any species A, B, D
H	denotes hydrogen
P	denotes reaction product
R	denotes reaction reactant
1, 2	denotes first or second group when used in first sublevel, denotes inlet and outlet conditions when used in second sublevel

CHAPTER I

INTRODUCTION

Upgraded coal-derived liquids can be used as petroleum liquid substitutes in such applications as power generation fuels in combustion turbines and boilers, and as refinery feedstocks. Of the raw liquid products of coal liquefaction processes, most of the distillate liquids and essentially all the residual liquids are not directly suitable for use as petroleum-derived fuel substitutes. Upgrading is achieved through a hydrotreatment process in which the concentrations of sulfur, nitrogen, oxygen, and trace metal heteroatoms are reduced. Other consequential effects of hydrotreatment are hydrogenation, hydrocracking, increased storage stability, and reduction of viscosity, aromaticity and carcinogenicity.

Hydrotreatment, as it pertains to upgrading, is a process in which the major reactions, hydrogenation and hydrogenolysis of the hydrocarbon liquid, are promoted over a catalyst bed. Commercial hydrotreatment processes incorporate mostly fixed bed continuous flow reactors operating at high temperatures and pressures. The most common systems utilize the gravity induced trickle flow of the liquid feed with cocurrent hydrogen gas flow.

The reaction kinetics of hydrocarbon liquid hydrotreatment have been the subject of a number of studies and reports published since the 1960's. These works have covered a broad range of

objectives, analysis procedures, proposed kinetic rate expressions, feed compositions, and operating and reactor conditions. However, a consensus opinion concerning hydrotreatment kinetics, especially in the case of coal-derived liquids, has not been formed and in many instances conflicting reports have been published (31).

Objectives

The objectives of this study of hydrotreatment kinetic modeling were threefold:

The first objective was to learn the reasons for the many differing and often contradictory reports concerning coal-derived liquid (CDL) hydrotreatment kinetics. Especially in question were inconsistent reports of the reaction orders and the temperature dependent Arrhenius constants.

The second objective of this work was to perform an evaluation of the kinetic rate expressions used to describe hydrotreatment processes. Specifically, these evaluations were to determine: What the various rate expressions are able to tell us through interpretation of their data fit results; determine the rate expression best suited for use in the modeling of CDL hydrotreatment kinetics; and determine the factors which have the greatest influence on the ability of a rate equation to describe hydrotreatment.

The third objective was to develop a mathematical kinetic model of the CDL hydrotreatment process. This kinetic model would use the rate expression which would allow the most accurate description of kinetic hydrotreatment data.

As a result of this work, the power-function or global models used

by numerous authors to describe kinetic hydrotreatment data were found to yield calculated parameter values which were dependent on such factors as operating conditions and data fitting procedures. These dependencies are a possible reason for some of the inconsistent kinetic reports published over the years. A hyperbolic or intrinsic expression assuming two different types of reactant adsorption sites was found to be the superior type of rate expression for use in the description of catalytic hydrotreatment kinetics. And, although the complexity of the CDL hydrotreatment process prevented the development of a mathematical kinetic model of that process, an accurate model was developed for the hydrodesulfurization of a model CDL compound, dibenzothiophene.

CHAPTER II

LITERATURE SURVEY AND PROCESS DESCRIPTION

Coal Liquids

An extensive literature survey was conducted in which information was reviewed concerning hydrocarbon liquid hydrotreatment and related subjects. Particular attention was focused on coal-derived liquids and heteroatom removal.

Coal-derived liquids are the products from any of more than twenty coal liquefaction processes. Three of the most popular processes are the Solvent Refined Coal (SRC), H-Coal, and Exxon Donor Solvent (EDS), all of which have been investigated on the pilot plant scale. Coal liquids are a complex mixture of aromatic and aliphatic hydrocarbons with sulfur, nitrogen, oxygen, and metallic compounds. Compared to petroleum liquids, they typically contain higher levels of nitrogen, oxygen and metallic heteroatoms, have a lower hydrogen content, and tend to be more viscous. Coal liquid heteroatoms are usually found in five and six member heterocycles. Sulfur is most abundant in the form of thiophene and its benzo- and dibenzo-derivatives, nitrogen in indoles, quinolines and carbazoles, and oxygen in phenols, fused ring furans, and carboxylic acids (23).

Hydrotreatment

Effects

The effects of primary concern in the hydrotreatment upgrading of hydrocarbon liquids are the removal of sulfur, nitrogen, oxygen, and metallic heteroatoms. These four heteroatom removal processes are referred to as hydrodesulfurization (HDS), hydrodenitrogenation (HDN), hydrodeoxygenation (HDO), and hydrodemetallation (HDM). Removal of these atoms is important for a number of reasons including: sensitivity and poisoning of reformer, hydrocracker, and other hydrotreatment catalysts; air pollution control standards governing combustion and catalyst regeneration gas emissions; and storage, handling, and corrosion problems. Depending upon the required specifications of the upgraded liquid, improvements in hydrogen content, storage stability, and viscosity may be of importance and can be accomplished to variable extents in the hydrotreatment process.

Reactor Systems

Several different types of batch and continuous flow reactors are used for hydrotreatment processing. Most batch reactors are used for laboratory reaction kinetic studies due to their ability to reduce flow, mass transfer, and temperature nonidealities. Conversely, nearly all commercial hydrotreatment processes incorporate continuous flow packed bed reactors, and most utilize the downward trickle flow of the liquid feed with cocurrent hydrogen gas flow.

Trickle-flow reactors have become most popular for several reasons. First, substantial savings may be realized by reduction of

expensive hydrogen gas requirements needed for the vapor phase reactions once thought necessary to achieve high heteroatom conversion and limit catalyst coking (42). Also, the liquid phase reactant mixture suppresses excessive temperatures and hot spots caused by the exothermic hydrotreatment reactions. Such high temperatures can reduce catalyst life and cause unwanted hydrocracking.

Reactor conditions in commercial hydrotreatment processes cover a broad range of operating conditions, depending primarily upon the characteristics of the feedstock. Temperatures usually fall within a range of 300 to 450 C (550-850 F), pressure from 25 to 200 atm (350-3000 psi), and liquid hourly space velocities (LHSV) from 0.5 to 15 hr⁻¹. Hydrogen consumption is highly dependent on feedstock properties and may range from less than 10 m³ H₂/m³ oil (56 std.cu.ft./bbl) for light distillate liquids to more than 1000 m² H₂/m³ oil (5600 std.cu.ft./bbl) for heavy residual liquids (12, 25).

The use of Co-Mo/Al₂O₃ or Ni-Mo/Al₂O₃ catalysts in the hydrotreatment process is almost universally accepted. The cobalt molybdate catalyst is a mixture of cobalt and molybdenum oxides dispersed in most cases over an aluminum oxide support. According to Richardson (22), the active component is a structurally unidentified cobalt-promoted MoO₃ complex, which assumes its true activated state after it sulfides. As a result of the dependence of catalyst's activity on its sulfided state, some minimal sulfur concentration must be present in the reactor at all times during the hydrotreatment process (24). This may require some hydrogen sulfide recirculation. Also, as a result of his catalyst study, Richardson reports that a Co:Mo ratio of 0.2 is desired for maximum activity. These catalyst particles are produced in

the forms of spheres, tablets, pellets, and extrudates ranging from .08 to .32 cm (1/32 to 1/8 inch) in diameter (25). Other typical catalyst characteristics, as reported by Schuit (29), are bulk density (.15-1.0 g/cc), average pore volume (.2 - .8 cc/g), specific surface area (150 - 400 m²/g), and average pore diameter (6 - 20 nm).

Hydrotreatment catalyst deactivation is principally caused by coking and poisoning. Coking causes deactivation by deposition of carbonaceous material (coke) on catalysts and plugging their pores. The catalyst may be regenerated by burning off the coke, but the extent to which this may be accomplished may be limited due to the catalyst pores being plugged to the point where they inhibit the required diffusion of oxygen (24). Irreversible catalyst poisoning occurs through deposition of metals on the catalyst surface and adsorption of nitrogenous compounds on the acidic reaction adsorption sites.

Reaction Kinetics

Global Rate Equations. The observed or global rate model is one of two common types used to describe hydrotreatment reaction kinetics. The global rate model is a power-function equation which has the general form:

$$r = kC_A^a \quad [1]$$

The rate constant, k, follows the Arrhenius temperature dependency described by the following equation:

$$k = A \exp(-E/RT) \quad [2]$$

Additional terms are sometimes included for dependence on hydrogen partial pressure and concentration of species other than the reactant. Such a rate expression could be written as follows:

$$r = k C_A^a C_B^b C_D^d P_H^e \quad [3]$$

These global equations represent the reactor contents as a single homogeneous group.

As shown in a review by Seapan and Crynes (31), global rate equations have been used by several authors to represent multicomponent hydrocarbon hydrotreatment data from continuous flow reactors. The global rate expressions used by these authors can be separated into two groups.

The first group consists of simple first or second order expressions as described by Equation [1]. A host of authors have published works in which multicomponent hydrotreatment data was fitted by one of these simple power law expressions (1, 6, 11, 12, 14, 37, 38, 41, 44). The study by White (44) was the only member of this group in which an acceptable data fit was not reported. In that publication, a break in the linear Arrhenius plot was reported near 400 C (750 F), above and below which the data could be described by two separate straight lines.

The second group is represented by first or second order expressions which have been modified in some manner. Curtin (5), Shih (32), and Angevine (2) report acceptable fits to coal liquid and shale oil hydrotreatment data by global rate expressions which include time dependent catalyst deactivation constants. Sivasubramanian (35, 36) and Mehta (17) reported that global equations incorporating a factor for incomplete catalyst wetting were able to fit hydrotreatment data acceptably well. Garg (9), Gary (10), Satchell (28), and Sooter (40) report good data fits by separating the feed mixture into separately reacting groups, each behaving according to a simple first order kinetic

expression.

A common trend concerning these global kinetic expressions was apparent to this author. Those studies using data from liquids having a boiling range less than approximately 150 C (300 F) were able to fit the data with a simple first order model. At wider boiling ranges some studies report a break in the Arrhenius temperature plot for the simple first order model, while others proposed a higher order or modified version of the global rate model. As a rule, the liquids having a wide boiling range (greater than 150 C) could not be fitted by a simple first order global rate model. This phenomena is also discussed in a theoretical work in which Weekman (43) shows that a mixture of first order reactions follows an overall observed order greater than one. In contrast to the multicomponent hydrotreatment reports, most single component studies report first order dependencies on reactant concentration.

Intrinsic Rate Equations. Intrinsic or catalyst site rate models are also commonly used to describe hydrotreatment kinetics. The Langmuir-Hinshelwood adsorption model is the most widely used and accepted type of intrinsic rate model. A set of assumptions frequently made in hydrotreatment reaction studies is:

1. Reversible adsorption of heterocompound and hydrogen reactants.
2. Irreversible reaction of adjacently adsorbed heterocompound and hydrogen molecules.
3. Reversible desorption of hydrogenated product.

The Langmuir-Hinshelwood type intrinsic rate equation resulting from these assumptions is:

$$r = \frac{k C_A C_B}{(1 + K_A C_A + K_B C_B + K_P C_P)^2} \quad [4]$$

where the reaction rate constant, k , and the adsorption equilibrium constants, K , follow the Arrhenius temperature dependencies described below:

$$k = A \exp(-E/RT) \quad [5]$$

$$K_i = A_i \exp(+E_i/RT) \quad [6]$$

The derivation of Equation [4] from the three assumptions listed above is shown in Appendix A. This type of intrinsic rate equation has many variable forms, each being individually derived from a specific set of adsorption and reaction assumptions.

A large number of hydrotreatment kinetic studies have been published in the past fifteen years, particularly of model compound hydrodesulfurization. After it became apparent to this author that a single rate equation derived from present adsorption-reaction theory would not be capable of describing the removal of all types of heteroatoms, attention was focused upon hydrodesulfurization, considered to be the most important of the heteroatom removal processes (7, 24, 30). It was thought an extensive understanding of this process would be a sound basis for the future development of an expanded model capable of describing the removal of a mixture of heteroatoms such as those found in coal derived liquids.

A number of model compound hydrodesulfurization studies were reviewed in this work. Among the most informative were reports about thiophene HDS published by Chakraborty (4), Massoth (16), and Satterfield (26, 27). In addition, several benzothiophene, dibenzothiophene, and other model compound HDS studies were reviewed (3,

7, 18, 33, 34). Most of these authors proposed intrinsic rate models that were specific forms of the generalized equation shown below:

$$r = \frac{kC_A C_B^a}{(1 + K_A C_A + K_B C_B + K_P C_P)^b} \quad [7]$$

where A, B, and P represent heterocompound, hydrogen, and hydrogen sulfide, respectively. Reaction rate resistance due to competitive adsorption of hydrocarbons free of heteroatoms was normally assumed to be negligible or possibly not occurring at all. Broderick (3) and Massoth (16) studied several specific forms of Equation [7] but found the model described by Equation [8] to be superior,

$$r = \frac{kC_A C_B}{(1 + K_A C_A + K_P C_P)(1 + K_B C_B)} \quad [8]$$

where A, B, and P again respectively represent heterocompound, hydrogen, and hydrogen sulfide. This observation was corroborated by Espino (7) and Singhal (34) in their studies of dibenzothiophene hydrodesulfurization kinetics. This model assumes the sulfur-containing molecules compete for one type of adsorption site while hydrogen molecules adsorb on a second type of site.

Several authors have suggested a two group theory could be used to describe the hydrodesulfurization of the sulfur-containing heterocompounds found in a wide boiling range liquid (9, 10, 29, 33, 40, 42). This concept involves the simultaneous first order reaction of two reactant groups, with each reaction proceeding at a rate proportional to the concentration of its group. Such an intrinsic rate expression could be written as shown in Equation [9],

$$r = \frac{\alpha k_1 C_A C_B}{(1 + K_A C_A + K_P C_P)(1 + K_H C_H)} + \frac{\beta k_2 C_B C_H}{(1 + K_B C_B + K_P C_P)(1 + K_H C_H)}$$

[9]

where α and β are the mixture fractions, and A and B represent the two reactant groups.

Process Models

For the purpose of use in this work, a process model was defined as an integrated plug flow design equation. The use of the ideal plug flow model implies the assumptions listed below (25):

1. No axial or radial dispersion.
2. No mass or heat transfer resistances in or between the gas, liquid and catalyst particle.
3. Catalyst particles are completely wetted.
4. Reaction occurs only at the solid-liquid interface.
5. No vaporization or condensation occurs.

Satterfield (24, 25) has indicated the nonidealities listed above do occur to varying extents, but the gas and liquid mass and heat transfer resistances are typically negligible, and, in the case of heteroatom removal, assumption of an irreversible first order reaction occurring at the solid-liquid interface is justified. Many authors have indicated significant pore diffusion resistance under some conditions. Another nonideality commonly assumed to significantly affect reactor performance is incomplete catalyst wetting. It should be noted that no multicomponent hydrotreatment process model was discovered in the

literature search conducted in this work, except those which assumed global reaction kinetics and few or no reactor nonidealities.

CHAPTER III

PROCEDURE

Evaluation of Kinetic Rate Equations

In this work the abilities of several kinetic rate expressions were investigated through the performance and subsequent evaluation of HDS, HDN, and HDO data fit calculations. Evaluations began with the simplest forms of rate expressions and proceeded according to increasing model complexity.

Heck and Stein (12) published a paper containing experimental data from the hydrotreatment of two coal-derived liquids, an SRC recycle solvent and an H-coal distillate. These HDS, HDN, and HDO data were collected from each of 60 experimental runs, using both NiMo/Al₂O₃ and CoMo/Al₂O₃ commercial catalysts. Their system, using a trickle flow reactor, was typical in most respects of commercial hydrotreatment systems. The major deviations from large scale processes were lower liquid and gas velocities inside the reactor. This is a common characteristic of experimental reactors operating at space velocities similar to those used in commercial processes due to significant differences in the reactor length to diameter ratio. Because they contained an extensive set of experimental data collected from a system typifying commercial hydrotreatment, Heck and Stein's data were utilized in the data fit calculations of the model evaluations. In their work, Heck and Stein proposed the second order pressure dependent

global rate model described in Equation [10].

$$r = A \exp(-E/RT) C_R^2 P^m \quad [10]$$

They reported the values of the model parameters which allowed the best fit to each of three data sets. Each set contained experimentally observed data for HDS, HDN, and HDO. As the first step taken to determine the reasons for the inconsistent global kinetic reports mentioned earlier, an attempt was made in this work to verify Heck and Stein's reported values of the second order model parameters. In addition, first and n-th order global models were tested and the calculated fits compared to those of the second order model. The comparative results of these three global rate models were used to determine the validity of using such simplified models to describe the intricate coal liquid heteroatom removal processes.

All the data fits in this work were calculated using a version of the Marquardt nonlinear data fit technique. This particular version was one modified by Professor John P. Chandler, of the Department of Computing and Information Sciences at Oklahoma State University. Chandler's version of the Marquardt computer program is listed in Appendix D. Output from this program includes several measures of the goodness of fit. These are: the residual mean square (rms) and minimized sum of squares (PHI), both measures of the deviation of the fitted from observed values; a correlation matrix indicating the degree of parameter interdependence; and the rescaled parameter errors, values equal to one standard deviation in the normalized distribution curve.

Evaluations similar to those of the global rate models were also

made of several Langmuir-Hinshelwood type intrinsic models. A list of the intrinsic models considered in this work appears in Table I. The hydrocarbon reactant concentration appearing as a resistance term in the denominators of Equations I-a through I-c, C'_A represented three different concentrations in three separate evaluations of each rate equation. These three groups were:

1. All sulfur-containing hydrocarbons.
2. All sulfur, nitrogen, and oxygen-containing hydrocarbons.
3. All sulfur, nitrogen, and oxygen-containing hydrocarbons plus their heteroatom-free hydrocarbon products.

The concentration of the third group was assumed to be constant and equal to the sum of the initial heterocompound concentrations. Equations I-a and I-b assume all species compete for one type of adsorption site, while equations I-c and I-d assume competition between reactant and product for one type of adsorption site and noncompetitive adsorption of hydrogen on a different type of site. Equation I-a assumes no rate resistance due to hydrogen adsorption. Equation I-d assumes two sulfur compound groups that react at different rates but by the same physical processes. The results of the data fit calculations and subsequent analyses of these intrinsic rate equations are discussed in the next chapter.

Process Model Development

An ideal process model would be one that would accurately predict the performance of a hydrotreatment reactor under all ranges of operating conditions. Noting the complexity of such an ideal process model, this work focused on the development of a simplified version

TABLE I
INTRINSIC RATE MODELS FOR HYDRODESULFURIZATION KINETICS

$r = \frac{k C_A C_H}{(1 + K_A C'_A + K_P C_P)^2}$	I-a
$r = \frac{k C_A C_H}{(1 + K_A C'_A + K_H C_H + K_P C_P)^2}$	I-b
$r = \frac{k C_A C_H}{(1 + K_A C'_A + K_P C_P)(1 + K_H C_H)}$	I-c
$r = \frac{\alpha k_1 C_A C_B}{(1 + K_A C'_A + K_P C_P)(1 + K_H C_H)} + \frac{\beta k_2 C_B C_H}{(1 + K_B C_B + K_P C_P)(1 + K_H C_H)}$	I-d

A, B - hydrocarbon reactants, P - reaction product, H - hydrogen

C'_A can represent the concentration of a species the same as or different than C_A .

Reactant group concentrations $\alpha + \beta = 1$.

which would be useful in the later elaboration of a more robust form. Therefore, a mathematical process model was developed for simulation of the hydrodesulfurization of a model sulfur compound dispersed in a liquid solvent. Attempts were made to simulate the conditions common to commercial scale upgrading of coal-derived liquids.

Although many studies have been published and much is known about the HDS of thiophene, dibenzothiophene was chosen as the model compound because it is more representative of the sulfur-containing heterocompounds found in coal-derived liquids (3). Tetralin was the choice as the model solvent for three reasons. First, tetralin is a molecule which typifies the size and cyclic structure of hydrocarbon molecules commonly found in coal-derived liquids. Second, it remains in the liquid phase, as does the largest fraction of a coal-derived liquid under the normal range of reactor operating conditions. The third reason for the selection of tetralin as a model solvent was that it, along with the dibenzothiophene reactant, describes the feed to a trickle flow reactor used by Espino (7) to collect HDS data. This description allowed Espino's experimental data to be used for a better evaluation of the model developed in this work.

This process, or reactor performance model, is yielded by the integration of the following rate equation:

$$r = \frac{k\eta C_R C_H}{(1 + K_R C_R + K_P C_P)(1 + K_H C_H)} \quad [11]$$

where R, H, and P represent dibenzothiophene, hydrogen, and hydrogen sulfide respectively. As mentioned earlier, several authors found Equation [11] to be the superior Langmuir-Hinshelwood form used to

describe the HDS adsorption reaction processes. The catalyst effectiveness factor, η , has been incorporated to account for the potentially strong resistance to dibenzothiophene pore diffusion. The derivation of Equation [11] follows a set of steps very similar to those taken in the derivation shown in Appendix A. The differences are those which result from the assumption of two types of adsorption sites, rather than a single type of site. The integrated form of the plug flow design equation incorporating Equation [11] is shown below:

$$C_{R2} = C_{R1} + \frac{(1 + K_P(C_{R1} + C_{P1}))}{(k_R \eta - K_P)} \ln \frac{C_{R1}}{C_{R2}} - \frac{K(\eta)(C_H)(W)(100)}{(1 + K_H C_H)(K_R \eta - K_P)(LHSV)(V)(\rho)} \quad [12]$$

where the subscripts 1 and 2 denote inlet and outlet conditions, and W , V , and ρ are catalyst weight, reactor volume, and liquid density respectively. The formal integration producing Equation [12] is presented in Appendix B.

Assumption of the set of sequential steps outlined below provided the basis for development of the process model expressed by Equation [12].

1. Diffusion of hydrogen (H_2) from the bulk gas to the gas-liquid interface surrounding the catalyst pellets.
2. Dissolution of H_2 in the bulk liquid.
3. Diffusion of H_2 and dibenzothiophene (DBT) from the bulk liquid to the catalyst surface.
4. Diffusion of H_2 and DBT inward through the catalyst pores.
5. Adsorption of DBT and H_2S (a reaction product) on one type of

catalyst adsorption site.

6. Adsorption of H_2 on a second type of catalyst adsorption site.
7. Reaction of DBT and H_2 adsorbed on adjacent sites.
8. Desorption of the reaction products.¹
9. Diffusion of reaction products outward through the catalyst pores.
10. Diffusion of the reaction products into the bulk liquid.
11. Diffusion of H_2S from the liquid-gas interface into the bulk gas.

As mentioned in Chapter II, there are five assumptions implied with the use of the ideal plug flow design equation. Four of those assumptions were retained in the development of the process model described by Equation [12]. The catalyst effectiveness factor was included to account for reactant pore diffusion resistance. The effects of this lone nonideality were incorporated in the process model for two reasons. First, pore diffusion resistance was found in the literature survey to be the nonideality most frequently observed and commonly reported to have significant effects on the reaction process. Second, it was believed by this author that reactor nonidealities would be better studied and modeled singularly, rather than as a group where the model factors representing them may be interdependent and simultaneously changing.

Hydrogen concentration in the liquid phase was calculated using a correlation developed in Prather (20) for the solubility of hydrogen in

¹In addition to the HDS products hydrogen sulfide, biphenyl, and cyclohexylbenzene, the hydrogenated but undesulfurized products tetrahydrodibenzothiophene and hexahydrodibenzothiophene appear to lesser extents (3).

a Solvent Refined Coal recycle solvent at high temperatures and hydrogen partial pressures. This correlation was developed assuming a linear equation for relating solubility to hydrogen partial pressure and by expressing the logarithm of the slopes of those lines as a linear function of the reciprocal absolute temperature. Hydrogen solubility was then calculated using the following equation:

$$S = \exp(-S_1 - S_2/T) P_H \quad [13]$$

where S_1 and S_2 are empirically evaluated constants. In lieu of specific values of S_1 and S_2 for the model system solvent, the values published by Prather for the SRC recycle solvent were used. The hydrogen solubility dependence on temperature and pressure, although not exactly accurate when using these values, was presumed to be satisfactorily representative for use in the process model.

The DBT effectiveness factor, η , was calculated using the following equations suggested by Froment (8) for heavy petroleum feedstocks. The values of the constants used in Equations [14-24] are listed in Table II.

$$\eta = \frac{3}{H^2} (H \coth(H) - 1) \quad [14]$$

$$H = Rc(k_{obs}/D_{eff})^{1/2} \quad [15]$$

$$r_{obs} = k_{obs} C_R \quad [16]$$

$$D_{eff} = \frac{\epsilon D}{\tau} \left(1 - \frac{R_m}{R_p}\right)^4 \quad [17]$$

The free liquid diffusivity, D , was calculated using Scheibel's correlation (21).

TABLE II

PHYSICAL CONSTANTS USED IN THE DBT PROCESS MODEL

MW_L	- tetralin molecular weight (1.32.g/mole)
P_C	- tetralin critical pressure (34.7 atm)
R_C	- average catalyst particle radius (0.0105 cm)
R_M	- DBT molecule size (10.0 angstroms)
T_C	- tetralin critical temperature (719 K)
V_L	- tetralin molar volume at normal boiling point (147.0 cc/gmole)
V_R	- DBT molar volume at normal boiling point (182.0 cc/gmole)
ϵ	- catalyst void fraction (0.5)
T	- catalyst tortuosity factor (2.5)
ω	- tetralin acentric factor (0.303)

$$D = \frac{KT}{\mu V_R^{1/3}} \quad [18]$$

where:

$$K = Z \left(1 + \left(\frac{3V_L}{V_R} \right)^{2/3} \right) \quad [19]$$

and:

$$Z = 25.2 \text{ E-8 for } V_L/V_R < 1 \quad [20]$$

$$Z = 17.5 \text{ E-8 for } 1 < V_L/V_R < 2.5 \quad [21]$$

$$Z = 8.2 \text{ E-8 for } 2.5 < V_L/V_R \quad [22]$$

The solvent viscosity, μ , was calculated using Letsou and Steil's correlation for high temperature liquids (21).

$$\mu\xi = [(\mu\xi)' + \omega(\mu\xi)''] \quad [23]$$

$$(\mu\xi)' = 0.015174 - 0.02135 T_r + 0.0075 T_r^2 \quad [24]$$

$$(\mu\xi)'' = 0.042552 - 0.07674 T_r + 0.0340 T_r^2 \quad [25]$$

$$\xi = \frac{T_c^{1/6}}{MW_L^{1/2} P_c^{1/2}} \quad [26]$$

Except for the catalyst particle and pore radii, the sensitivity of the effectiveness factor to the physical constants listed in Table II was not explored. The values of R_c and R_p , 0.0105 cm (60-80 mesh) and 14 angstroms, respectively, were adopted because they resulted in the prediction of particle size effects that most closely resembled those reported by Espino (7). A more detailed study of these physical constant effects might allow the average pore radius to fall into a more representative range (25-50 angstroms).

The liquid density, ρ , was assumed to be negligibly affected by

dissolved hydrogen and dibenzothiophene and calculated as that of the pure liquid solvent. Density values were determined by conversion of the values calculated using Gunn and Yamada's correlation for molar volume (21).

$$\frac{V'_L}{V''_L} = \frac{V_r(T'_r) [1 - \omega \Gamma(T'_r)]}{V_r(T''_r) [1 - \omega \Gamma(T''_r)]} \quad [27]$$

$$V_r(Tr) = 0.33593 - 0.33953Tr + 1.51941Tr^2 - 2.02512Tr^3 + 1.11422Tr^4 \quad [28]$$

$$\Gamma(Tr) = 0.29607 - 0.09045Tr - 0.04842Tr^2 \quad [29]$$

where ' and '' denote first and second reference conditions, respectively.

Experimental Data Fit

From the model described by Equation [12], the kinetic rate constant, k , and adsorption equilibrium constants K_H , K_R , K_P were calculated which best describe the set of dibenzothiophene HDS data published by Espino (7). This particular article was the only source uncovered in the literature survey which included the temperature, pressure, and space velocity ranges desired for such an evaluation of the process model. These data are tabulated in Appendix I. The specific values of these data points have been back calculated from a figure in the Espino paper. Other conditions desired for this model analysis and met by these data were trickle flow operation and liquid phase reaction in the catalyst. In addition, this paper included some information used to calculate hydrogen concentration, solvent density, effectiveness factor, catalyst weight, and reactor volume. These calculations, as described earlier, were performed in the first

sections of the computer programs shown in Appendices F, G, and H.

The form of the process model described by Equation [12] proved to be very awkward in the data fit calculations. The four kinetic constants k , K_H , K_R , and K_P were very difficult to handle under nonisothermal conditions due to the interdependencies of their pre-exponential and exponential constants. This necessitated the calculations be performed using isothermal data with subsequent extraction of the exponential constants from the Arrhenius plots. After many trial and error attempts, the following form of Equation [12] was found to be most suitable for use in the data fit calculations:

$$\frac{1}{x} \ln\left(\frac{1}{1-x}\right) = \frac{C_H \eta W(100) X(1)}{x \text{LHSV } C_{R1} V \rho (C_{P1}/C_{R1} + 1) (1 + X(2) C_H)} + \frac{(1 - X(3) \eta)}{(C_{P1}/C_{R1})} \quad [30]$$

where x is the fractional reactant conversion.

The fitted parameters are:

$$X(1) = k K_H K_R / K_P \quad [31]$$

$$X(2) = K_H \quad [32]$$

$$X(3) = K_R / K_P \quad [33]$$

from which three separate constants k , K_H , and K_R/K_P may be calculated.

After the pre-exponential and exponential constants were calculated from a linear regression fit of the three Arrhenius plots, the resulting six constants were included in the model equation Equation [12] and the fit over the entire set of data calculated. The n -th order global model Equation [10] was also used to fit this same set of data points and the resulting parameter values and goodness of fit compared with the intrinsic model results. These fits are discussed in the next chapter.

Parameter Sensitivity Study

In an attempt to determine the influence of operating conditions on the observed global model parameters and to determine the relationships between the global and intrinsic kinetics, a parameter sensitivity study was conducted. The process model, Equation [12], with the intrinsic kinetic parameters fixed at the values obtained from the data fit described above, was used to generate a hypothetical dibenzothiophene HDS data set which was in turn used to calculate the n -th order global model parameters (Equation [10]). This procedure, depicted by Figure 1, allowed the global model parameters to be plotted as functions of temperature, hydrogen pressure, and space velocity for a HDS system following the behavior described by Equation [12].

The ranges of the operating parameters, T , P , and $LHSV$, used in the generation of the data set were expanded from those of the DBT HDS data used in the intrinsic process model evaluation. The limits on these ranges were extended until the corresponding conversions calculated from the DBT process model became extremely high and low. The values used throughout these parameter sensitivity calculations are listed in Table III.

Individual data fit calculations yielding values of the four global model parameters, A , E , m , and n , were performed at constant values of the operating parameter comprising the abscissas of the parameter sensitivity plots and the twenty five combinations of the two remaining operating parameters. Calculations were performed at various values of the operating parameter plotted along the abscissa for the entire range from which meaningful values of the global model parameters could be obtained. The end points of these curves were

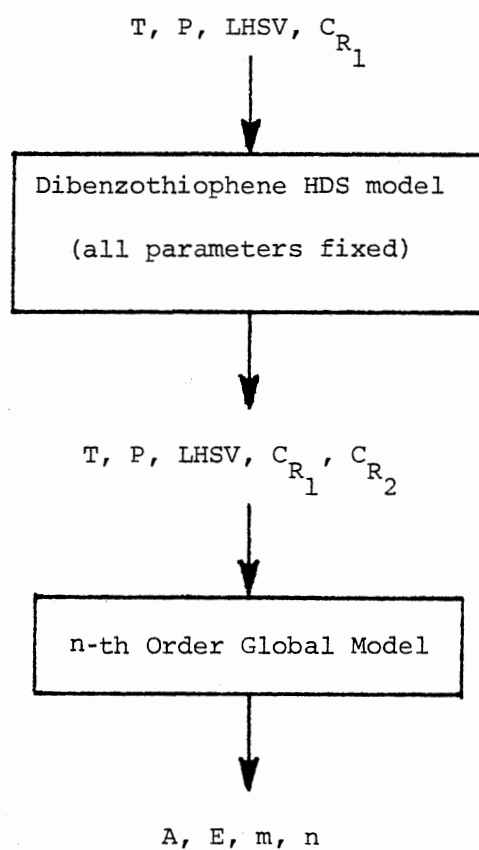


Figure 1. Parameter Sensitivity
Calculation Flow
Diagram

TABLE III
VALUES OF OPERATING PARAMETERS USED IN
PARAMETER SENSITIVITY CALCULATIONS

T F	P psi H ₂	LHSV (hr ⁻¹)
450	200	1
500	400	3
550	600	6
600	800	9
650	1000	12

usually those at which the corresponding DBT conversion was extremely high or low. The operating parameter held constant in these calculations was not confined to the ranges indicated in Table III.

The form of the n-th order global model used in these calculations is expressed by Equation [34].

$$C_{R_2} = \left[C_{R_1}^{1-X(4)} - \frac{X(1) \exp \left(\frac{X(2)}{RT} \right) P^{X(3)} (1 - X(4))}{LHSV} \right]^{1-X(4)} \quad [34]$$

where:

$$X(1) = A \quad [35]$$

$$X(2) = E \quad [36]$$

$$X(3) = m \quad [37]$$

$$X(4) = n \quad [38]$$

CHAPTER IV

DISCUSSION OF RESULTS

Global Kinetic Models

The global kinetic model described by Equation [39]

$$r = A \exp(-E/RT) C^n P^m \quad [39]$$

was analyzed by calculation of the model parameters, A, E, m, and n. The parameter calculations were performed utilizing Heck and Stein's (12) HDS, HDN, and HDO data. The Marquardt data fit program mentioned earlier was used to calculate the model parameters for the n-th order form of Equation [39] and the first and second order versions in which n is equal to 1 and 2 respectively.

The second order parameter values calculated in this work were compared to those published by Heck and Stein (see Table IV). The published values of the pre-exponential constants, activation energies, and order of hydrogen pressure dependence were duplicated with only limited precision. All of the published values were, however, within 95 percent confidence intervals of those values calculated in this work. The lack of precision may be explained by uncertainties in outlet concentration (minimum detectable limits reported at several different operational conditions) and in differences in the data fit techniques.

In addition to the comparison of the second order results, global parameters were evaluated for the first and n-th order models. These values are shown in Table V and Table VI, respectively. As expected,

TABLE IV
COMPARISON OF SECOND ORDER GLOBAL KINETIC MODEL PARAMETERS

Feed Catalyst	Heteroatom	A		E		n		Mean Deviation wt%	
		(psi ⁻ⁿ /wt%/hr)		Btu/mole					
SRC Recycle Solvent HDS-9A	Sulfur	4.46E2	3.76E2	28,960	28,380	1.37	1.36	.005	.008
	Nitrogen	1.14E9	3.58E9	59,930	64,150	0.87	0.96	.023	.024
	Oxygen	3.22E9	2.46E9	64,600	65,840	0.74	0.85	.081	.086
SRC Recycle Solvent HDS-1441A	Sulfur	5.71E6	1.25E9	45,710	55,830	1.08	0.96	.005	.007
	Nitrogen	1.91E9	1.23E9	64,750	63,980	1.03	1.04	.027	.033
	Oxygen	2.45E11	2.63E10	66,820	68,550	0.29	0.71	.148	.091
H-Coal Distillate HDS-1441A	Sulfur	2.45E5	8.52E7	31,580	45,630	0.79	0.84	.005	.008
	Nitrogen	1.81E7	1.90E7	56,390	56,750	1.29	1.30	.015	.018
	Oxygen	2.24E8	6.00E7	65,720	64,030	1.41	1.49	.061	.074

Note: The values in the first columns are those calculated in this work, the values in the second columns are those published by Heck and Stein (12).

TABLE V

FIRST ORDER GLOBAL KINETIC MODEL PARAMETERS

Feed Catalyst	Heteroatom	A (psi ^{-m} /hr)	E (Btu/lbmole)	m	Mean Deviation wt%
SRC Recycle Solvent HDS-9A	Sulfur	4.89E-2 + 2.22E-1	9,650 + 8,740	1.143 + .349	.010
	Nitrogen	5.72E3 + 2.83E4	35,820 + 9,270	0.944 + .357	.031
	Oxygen	7.92E4 + 2.27E5	39,220 + 5,280	0.776 + .206	.114
SRC Recycle Solvent HDS-1441A	Sulfur	3.92E2 + 3.26E3	26,030 + 16,220	0.889 + .374	.010
	Nitrogen	1.19E5 + 4.74E5	44,710 + 7,600	1.016 + .282	.026
	Oxygen	1.79E7 + 8.40E7	46,330 + 8,400	0.467 + .304	.160
H-Coal Distillate HDS-1441A	Sulfur	6.72E3 + 5.43E4	21,450 + 17,220	0.282 + .651	.009
	Nitrogen	5.83E3 + 2.38E4	40,290 + 9,280	1.231 + .301	.020
	Oxygen	5.87E6 + 3.80E7	55,030 + 16,530	1.223 + .542	.086

Note: The indicated error regions are 95% confidence intervals.

TABLE VI

N-th ORDER GLOBAL KINETIC MODEL PARAMETERS

Feed Catalyst	Heteroatom	A (psi ^{-m} /wt% ⁿ⁻¹ /hr)	E (Btu/lbmole)	m	n	Mean Deviation wt%
SRC Recycle Solvent HDS-9A	Sulfur	1.53E9 + 3.07E10	61,650 + 42,810	1.712 + .852	3.111 + 1.24	.003
	Nitrogen	3.73E7 + 3.46E8	53,050 + 18,660	0.885 + .396	1.765 + .543	.023
	Oxygen	4.20E6 + 1.25E7	48,910 + 6,330	0.766 + .152	1.455 + .193	.059
SRC Recycle Solvent HDS-1441A	Sulfur	8.38E9 + 1.57E11	61,860 + 39,260	1.278 + .741	2.597 + .920	.004
	Nitrogen	4.51E6 + 2.55E7	52,040 + 11,480	1.018 + .301	1.445 + .370	.023
	Oxygen	2.62E8 + 1.69E9	52,190 + 12,530	0.413 + .340	1.375 + .382	.129
H-Coal Distillate HDS-1441A	Sulfur	8.27E12 + 1.68E14	68,330 + 44,070	1.374 + .995	3.687 + 1.303	.003
	Nitrogen	1.35E6 + 6.06E6	50,810 + 10,310	1.251 + .288	1.685 + .345	.013
	Oxygen	3.88E8 + 3.80E9	67,260 + 25,280	1.430 + .607	2.075 + .672	.061

Note: The indicated error regions are 95% confidence intervals.

the additional degrees of freedom in the n-th order rate equation allow a better fit. The first order rate equation, which best describes the behavior of single reactant feeds, yields the poorest fit to the experimental data. This indicates the complexity of the reactant mixture. Equating global orders to true kinetic orders has been a common misinterpretation of data fit results. In all three global equations the hydrogen partial pressure dependencies are similar and show approximately a first order dependence with all values confined between zero and two.

Conclusions concerning activation energy were more difficult to make. The first and second order equations showed these values to increase from sulfur to nitrogen to oxygen containing compounds; whereas, the n-th order equation showed no consistent trend. Activation energies covered the broad range from 10,000 to 70,000 Btu/lbmole (75 -530 kJ/mol).

During the course of the data fit calculations it was found that in some cases the converged results were dependent upon the initial parameter guesses supplied to the program. This problem was overcome by repeating the calculations with improved guesses for the kinetic parameters until the best fit was obtained. In those calculations the best fit was obtained by minimizing the value of the following objective function:

$$FOBJ = \sum (C_{fit} - C_{calc})^2 \quad [40]$$

where C_{fit} and C_{dat} are the calculated and experimentally observed concentrations, respectively.

Another phenomena occasionally observed throughout the data fit calculations performed in this work was the ability of the model

equations to yield only a slightly poorer fit to a data set with a strikingly different set of parameter values. For instance, if the order of reactant concentration, n , is fixed at an arbitrary value far from its "best fit" value, the remaining model parameters, A , E , and m , allow the model equation enough flexibility to fit the experimental data set with nearly the same accuracy. This fact is manifested in part by the large parameter confidence regions, especially in the cases of the pre-exponential constants, in which all the confidence regions are of greater magnitude than the parameter values. Also an important fact was the observed dependence of the converged parameter values on the variable forms of the fitted function, i.e., $C_{fit} = f(A, E, m, n)$ or $0 = f(A, E, m, n)$.

These observations indicated shallow parameter surface minima, which may have been caused by poorly conditioned data or model equation (data or model equation that does not allow a sharp definition of the model parameters), or both. Because these observations generally held for all nine experimental data sets, this author believed the global model equations were the cause for these parameter calculation problems, therein lying a likely explanation for some of the discrepant literature reports mentioned earlier.

The facts that reaction orders greater than one produced more accurate results and that the values of the global parameters were scattered and inconsistent both indicated the inability of the global rate equation. Although such global rate equations are capable of describing coal liquid heterocompound conversion with good accuracy, their empirical nature keeps from yielding accurate information concerning the actual kinetic processes taking place at the reaction

sites. These observations indicated the global rate model is oversimplified for use as multicomponent hydrotreatment performance prediction tool.

Intrinsic Kinetic Models

Multicomponent Systems

An attempt was made in this work to fit the Heck and Stein (12) coal liquid hydrotreatment data with the single and two type site rate equations. An extensive effort was made to fit the data set with Equations I-a through I-c (Table I), and numerous theoretically justifiable variations of them. These rate expressions could not be used to describe coal liquid hydrotreatment satisfactorily. In most cases divergent results were obtained using a Marquardt nonlinear technique to fit these rate expressions to coal liquid data. When converged results were obtained, they were unacceptable in each case due either to physically meaningless values for the equilibrium constants, or excessively large confidence regions, or both. It was believed by this author that the complex nature of the multicomponent coal liquids did not allow them to be treated as a single group, therefore not allowing these types of single group intrinsic models to describe their kinetic data.

Several authors have suggested a two group theory could be used to describe the hydrotreatment of typical heavy petroleum and coal liquids (9, 29, 42). This concept involves the simultaneous first order reactions of two reactant groups, with each reaction proceeding at a rate proportional to the concentration of its group. Such a rate

expression is described by Equation I-d in Table I. Although this two group expression may be used to fit multicomponent feedstock HDS data, the single compound performance model should be developed to adequately account for the many system variables before an expanded version is considered. The complexity of a multicomponent systems makes preliminary understanding of the complete single component system a practical necessity.

Process Model

The process model described by Equation [12] incorporates the intrinsic kinetic rate expression, Equation [11], found to be superior for description of HDS data. The kinetic rate constant k and adsorption equilibrium constants K_H , K_R , K_P were calculated such that the process model, in the form of Equation [30], best described each of five sets of isothermal HDS data. These data were collected in a study of the hydrodesulfurization of dibenzothiophene (7). The calculated values of the kinetic constants and the average percent errors of the corresponding fits to the five isothermal data sets are shown in Table VII. The program used to perform these calculations, along with the input data and the best fit values of the parameters, are listed for each case in Appendix F. In all five sets of isothermal calculations, the process model was able to describe the data set very well. In each case the average error of the fitted outlet concentration profile values was less than two percent.

The Arrhenius plots of the three intrinsic constants k , K_H , and K_R/K_P appear in Figures 2, 3 and 4, respectively. The exponential constants were calculated via linear regression fits for each of the

TABLE VII
 DIBENZOTHIOPHENE HDS KINETIC MODEL CONSTANTS
 (ISOTHERMAL PARAMETER EVALUATIONS)

Temperature		k	K _H	K _R /K _P	Avg. % Error
°C	°F	wt%/hr	wt% ⁻¹		
285	545	8.043 E-2	1.893 E1	3.495 E-1	0.714
300	572	1.563 E-1	1.135 E1	9.355 E-1	1.098
310	590	3.136 E-1	8.177 E0	1.397 E0	1.502
325	617	8.511 E-1	5.415 E0	1.535 E0	1.279
350	662	2.648 E0	2.606 E0	2.436 E0	0.748

k - reaction rate constant

K_H - hydrogen adsorption equilibrium constant

K_R - dibenzothiophene adsorption equilibrium constant

K_P - hydrogen sulfide adsorption equilibrium constant

$$\text{Avg. \% Error} = \sum \frac{\text{ABS}(C_{\text{fit}} - C_{\text{dat}})}{C_{\text{dat}} (\text{NPTS})} \times 100\%$$

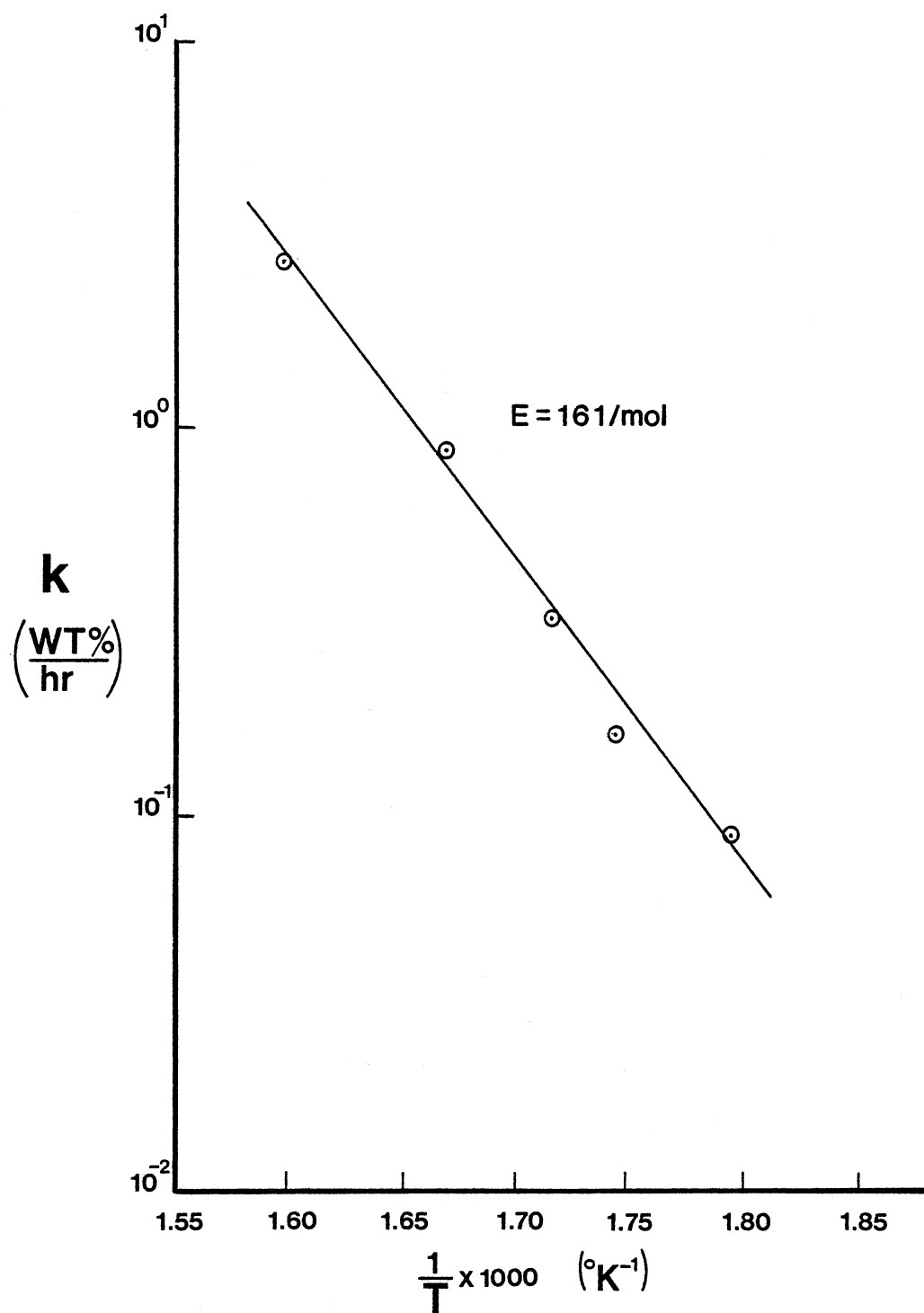


Figure 2. Arrhenius Plot of the Process Model Reaction Rate Constant

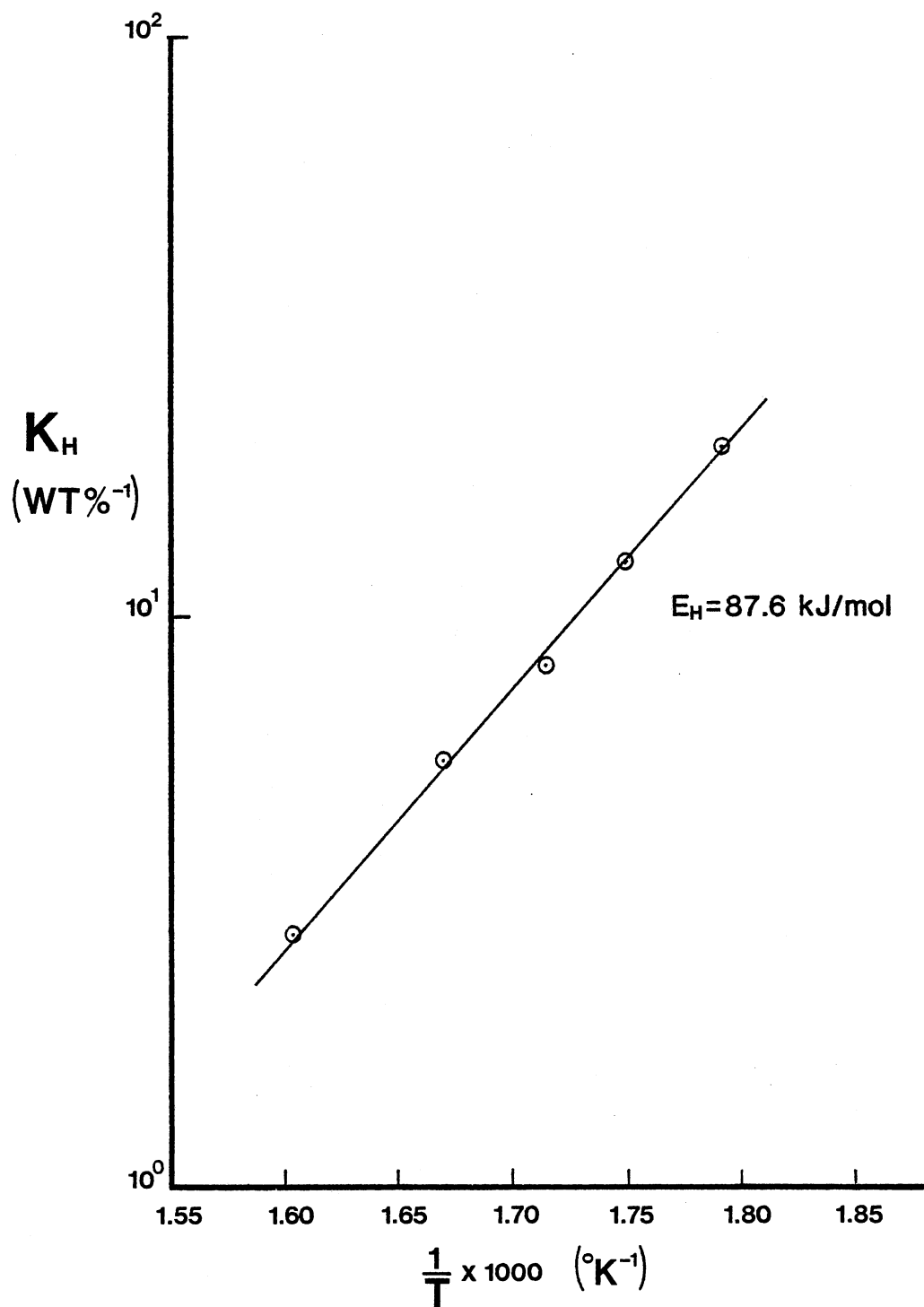


Figure 3. Arrhenius Plot of the Process Model Hydrogen Adsorption Equilibrium Constant

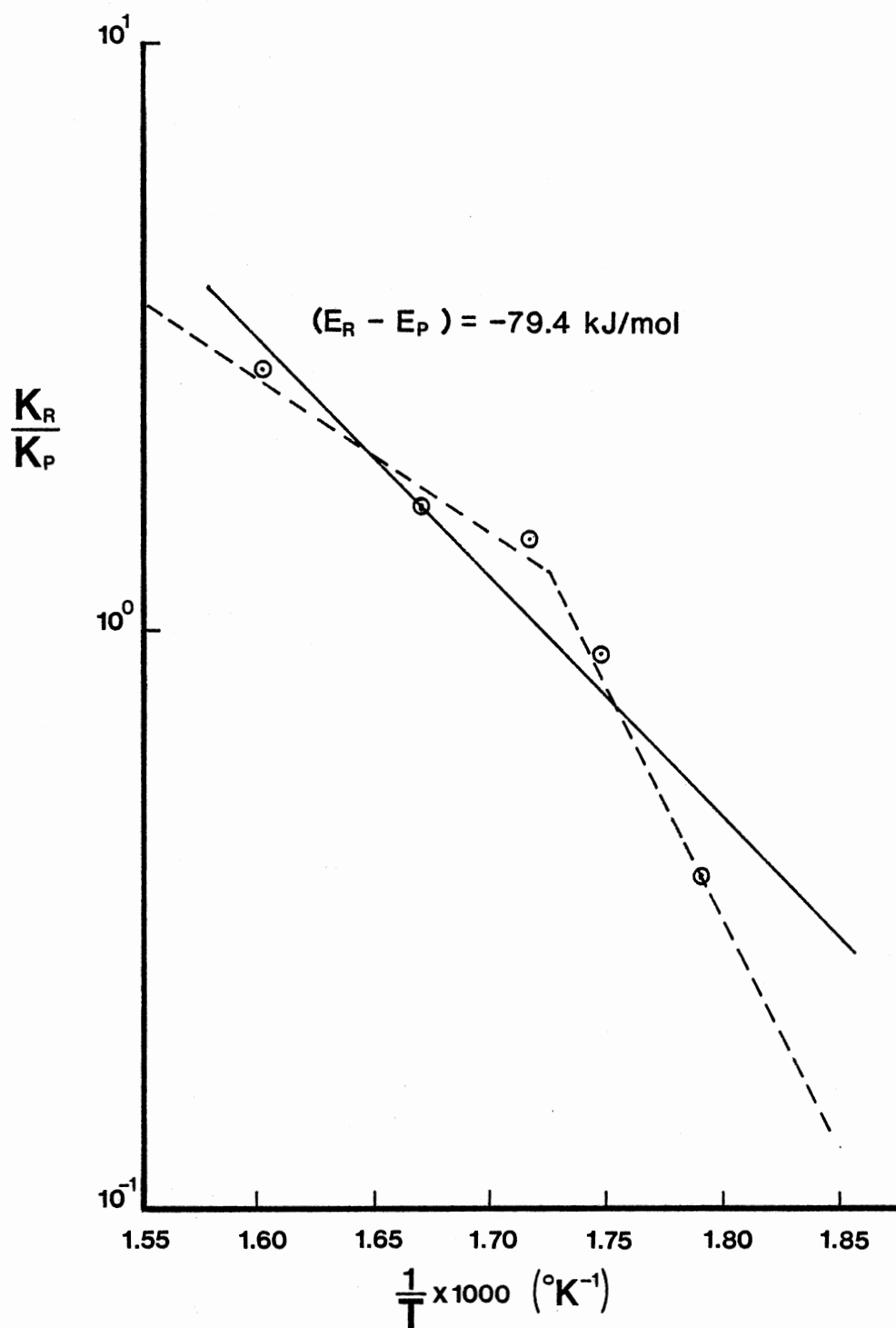


Figure 4. Arrhenius Plot of the Process Model DBT-H₂S Adsorption Equilibrium Constant Ratio

three plots. These constants are listed in Table VIII. Both the reaction rate constant and the hydrogen adsorption equilibrium constant adhered closely to the expected Arrhenius temperature dependency. The calculated reaction activation energy for the HDS of dibenzothiophene was 161 kJ/mol (21,333 BTU/lbmole), which closely compares with the values reported by Espino (7), 163 kJ/mol (21,667 BTU/lbmole), and Rollman (23), 151 kJ/mol (20,000 BTU/lbmole). The calculated heat of adsorption for hydrogen, 87 kJ/mol (11,611 BTU/lbmole), also falls within the range commonly reported in the literature (7). The ratio of dibenzothiophene to hydrogen sulfide adsorption equilibrium constants did not follow the Arrhenius temperature dependency well. The break in the Arrhenius plot (Figure 4) implies the difference in the heats of adsorption, $(E_R - E_P)$, shifts near 300 C (572 F). A likely cause for such a shift would be that, in addition to hydrogen sulfide, the other DBT HDS products, biphenyl and cyclohexylbenzene are in competition with dibenzothiophene for catalyst adsorption sites. Under these conditions, a shift in the quantity $(E_R - E_P)$ may occur with a shift in the product composition near the adsorption sites. Parallel hydrogenation-hydrogenolysis reactions of DBT which produce cyclohexylbenzene and biphenyl, respectively, have been supported in the literature (3, 7, 13). The two line segments in Figure 4 could represent these two temperature dependent DBT reactions, and thereby account for the break in the Arrhenius plot.

The ability of the dibenzothiophene HDS process model, as described by Equation [12], to fit the entire non-isothermal set of conversion data was also evaluated. The six kinetic constants, A , A_H , A_R/A_P , E , E_H , and $(E_R - E_P)$ were fixed at their respective values shown

TABLE VIII

INTRINSIC KINETIC CONSTANTS DETERMINED FROM THE ARRHENIUS
PLOTS OF k , K_H , AND K_R/K_P

	Reaction Rate Constant		Adsorption Equilibrium Constant Hydrogen		Adsorption Equilibrium Constant DBT:H ₂ S	
	$k = A \exp(-E/RT)$		$K_H = A_H \exp(E_H/RT)$		$K_R/K_P = A_R/A_P \exp((E_R - E_P)/RT)$	
Slope = E/R	-19328	(K)	10535	(K)	-9547	(K)
Standard Error	6963	(K)	7007	(K)	6076	(K)
E	160700	(J/mol)	87592	(J/mol)	-79378	(J/mol)
Intercept = ln A	32.029		-15.949		16.394	
Standard Error	11.887		11.962		10.373	
A	8.128 E13	(wt%/hr)	1.185 E-7	(wt% ⁻¹)	1.318 E7	(wt% ⁻¹)
Coeff. of det.	0.9933		0.9996		0.8668	

in Table VIII. The fitted values of the DBT concentration profile are tabulated in Appendix H. Although this model was able to describe the isothermal data very well, the non-isothermal fit was very poor. The average deviation from the experimental outlet DBT concentrations was in excess of 400%, whereas the isothermal errors were all less than 2%. By comparison, the n-th order global fit to these data points resulted in an average error of about 7%, as shown in Appendix I. The corresponding global parameters were:

$$A = 1.88 \text{ E9 (wt \% }^{1-n} \text{ /PSI }^m \text{ /hr)}$$

$$E = 5.27 \text{ E4 (BTU/lbmole)}$$

$$m = 0.82$$

$$n = 0.84$$

Obviously, the process model described by Equation [12] is completely unsatisfactory for description of non-isothermal data. This inability is due to an inadequate description of the K_R/K_P ratio as a function of temperature. The model equation is however very accurate when the data are broken down into isothermal groups. The development of an accurate product formation model, allowing the proper description of the K_R/K_P ratio as a function of temperature, and refinement of the effectiveness factor and solubility calculations would result in a very accurate and useful single component HDS model. Such a model could serve as the basis for an expanded version, perhaps in the form of a summation of individual sections, to describe multicomponent hydrotreatment.

Parameter Sensitivity Study

Parameter sensitivity calculations were performed in the manner

depicted by Figure 1. All the resulting parameter sensitivity plots include the individual points through which the curves were drawn. Although the curves are theoretical, the points were plotted to indicate the specific values of the operating parameter, T, P, or LHSV, at which the n-th order global parameters were calculated. These values of the global parameters, A, E, m, and n are tabulated in Appendix C.

The calculations performed at constant temperature and constant pressure required the following combination of parameters:

$$K_t = A \exp(-E/RT) \text{ at constant temperature} \quad [41]$$

$$K_p = AP^m \text{ at constant pressure} \quad [42]$$

The temperature and pressure related global parameters from Equations [41] and [42] were calculated from the slopes and intercepts of their respective Arrhenius and log K vs. log P plots. These plots are shown in Figures 5 and 6, and the calculated values of the corresponding global parameters, A, E, and m, tabulated in Appendix C (Tables XV and XVI).

In addition to the calculations utilizing the simple objective function equal to the sum of residual squares, Equation [40], a second set of calculations was made using the normalized objective function described by Equation [43].

$$FOBJ = \sum \left(\frac{C_{fit} - C_{dat}}{C_{dat}} \right)^2 \quad [43]$$

This function, which allowed the lower outlet concentrations to be most heavily weighted during the data fit calculations, was used to determine the dependence of the global data fit results on the form of the minimized objective function. The two curves in each of the parameter sensitivity plots represent the global parameter values calculated using the two objective functions.

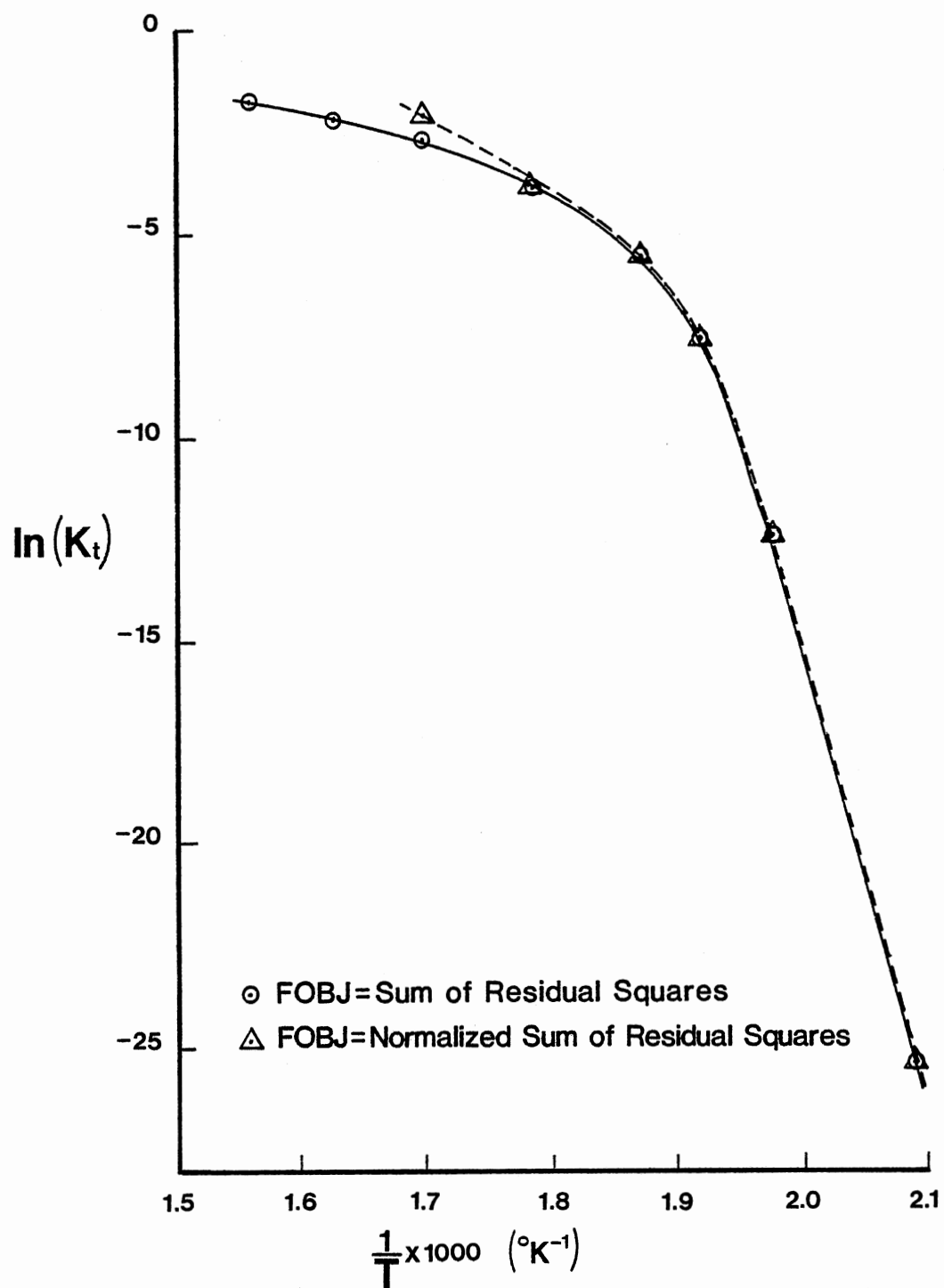


Figure 5. Arrhenius Plot of the Global Model Constant K_t

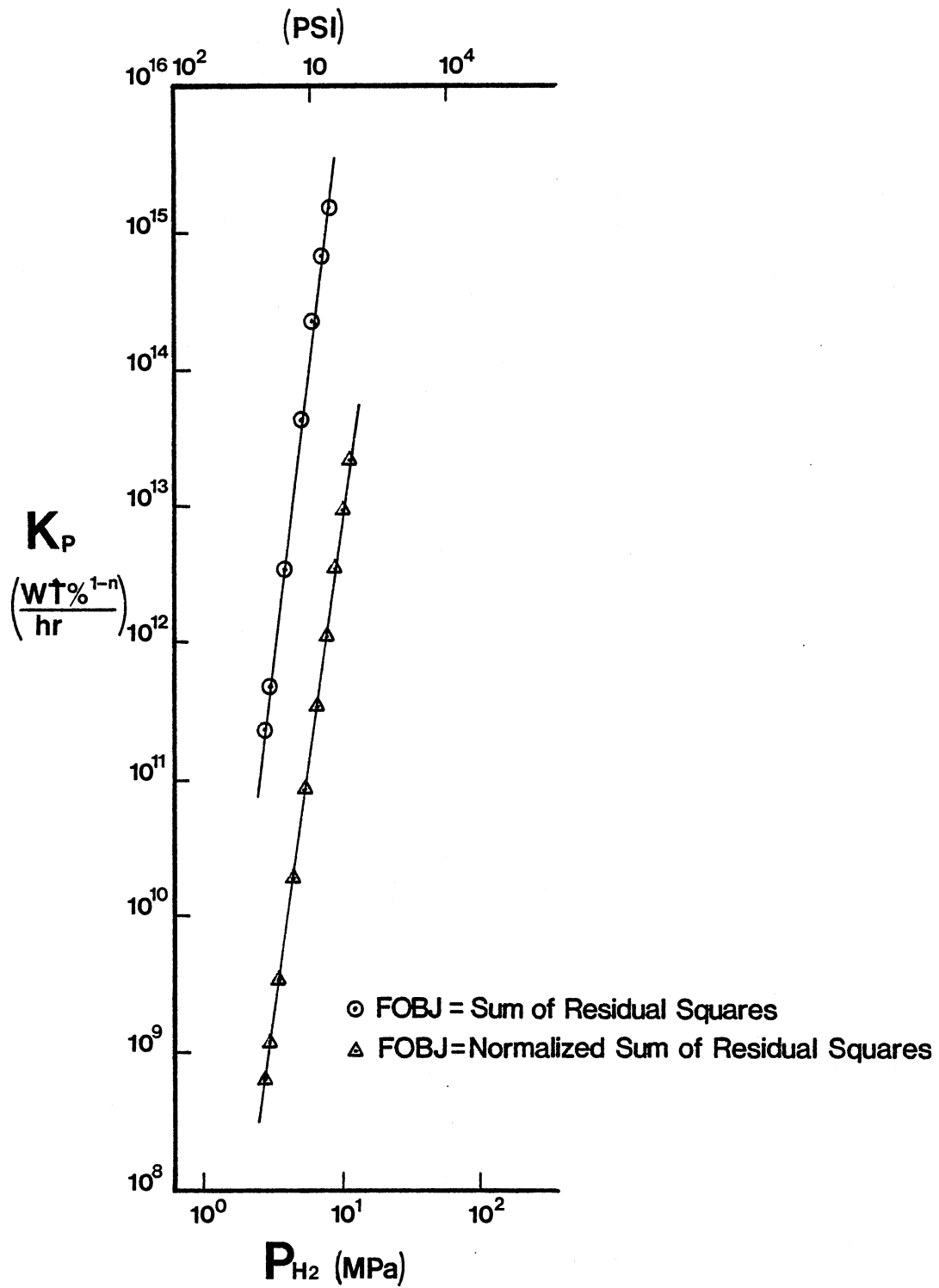


Figure 6. Global Model Constant K_p Dependence on Hydrogen Pressure

The general form of Equation [34] described below,

$$C_{R_2} = X^Y \quad [44]$$

presented problems during the course of these calculations. In some regions of the three or four dimensional surface searched by the data fit routine, X may become negative. Because Y is not an integer value, this condition resulted in a fatal computer error which halted all calculations and prevented a converged solution. Two solutions to this dilemma were considered. First, Equation [44] could be rearranged into one of several versions of Equation [45].

$$C_{R_2}^{1/Y} = X \quad [45]$$

This solution was rejected because it did not allow a direct fit to the outlet concentration profile. The second solution considered was the examination of X before the data fit program reached the exponential form (Equation [34]). In any case where X was negative it was set equal to zero, thereby eliminating the fatal program error. In a few cases where the outlet concentration was very low the data fit routine converged where X and therefore C_{R_2} remained equal to zero. These cases generally arose at or beyond the operating parameter limits discussed in Chapter III.

Another procedure which proved very helpful in obtaining meaningful converged values of the global parameters was to set a minimum limit on the concentrations included in the hypothetical data set. This precluded some of the problems encountered with the exponential form of Equation [34].

From the parameter sensitivity curves the only cases in which the

global parameter was observed as a constant function of the operating parameter were: pre-exponential constant, A, and order of hydrogen pressure dependence, m, versus hydrogen pressure. The values of these constants were calculated from the linear plots shown in Figure 6 and appear in Appendix J. The calculated orders of hydrogen pressure dependence, 7.0 and 8.0 for the two curves, are unexpected considering the first order dependence of the intrinsic process model used to generate the data set. No logical explanation for these values was apparent to this author.

In Figure 7 the two curves representing m as a function of space velocity were nearly mirror images of each other for most of the space velocity range. In both cases, however, all values of m fell within the range 0.6 to 1.0. The order of hydrogen pressure dependence was also a strong function of temperature, with both curves almost identically rising from about 0.15 at 230 C (446 F) to values approaching 1.0 as the temperature rose to 370 C (698 F) (see Figure 8). Sonnemans (39) reports that although no explanations for the effect of temperature on order of hydrogen pressure dependence were offered, several authors reported such effects.

The fluctuations of the value of m as a function of temperature and space velocity is probably not due to changes in the true order of the reaction, but to the attempt to describe the contribution of the following portion of the process model rate equation to the behavior of the hypothetical system:

$$\frac{C_H}{(1 + K_H C_H)} \quad [46]$$

Although the intrinsic model assumes first order in hydrogen pressure

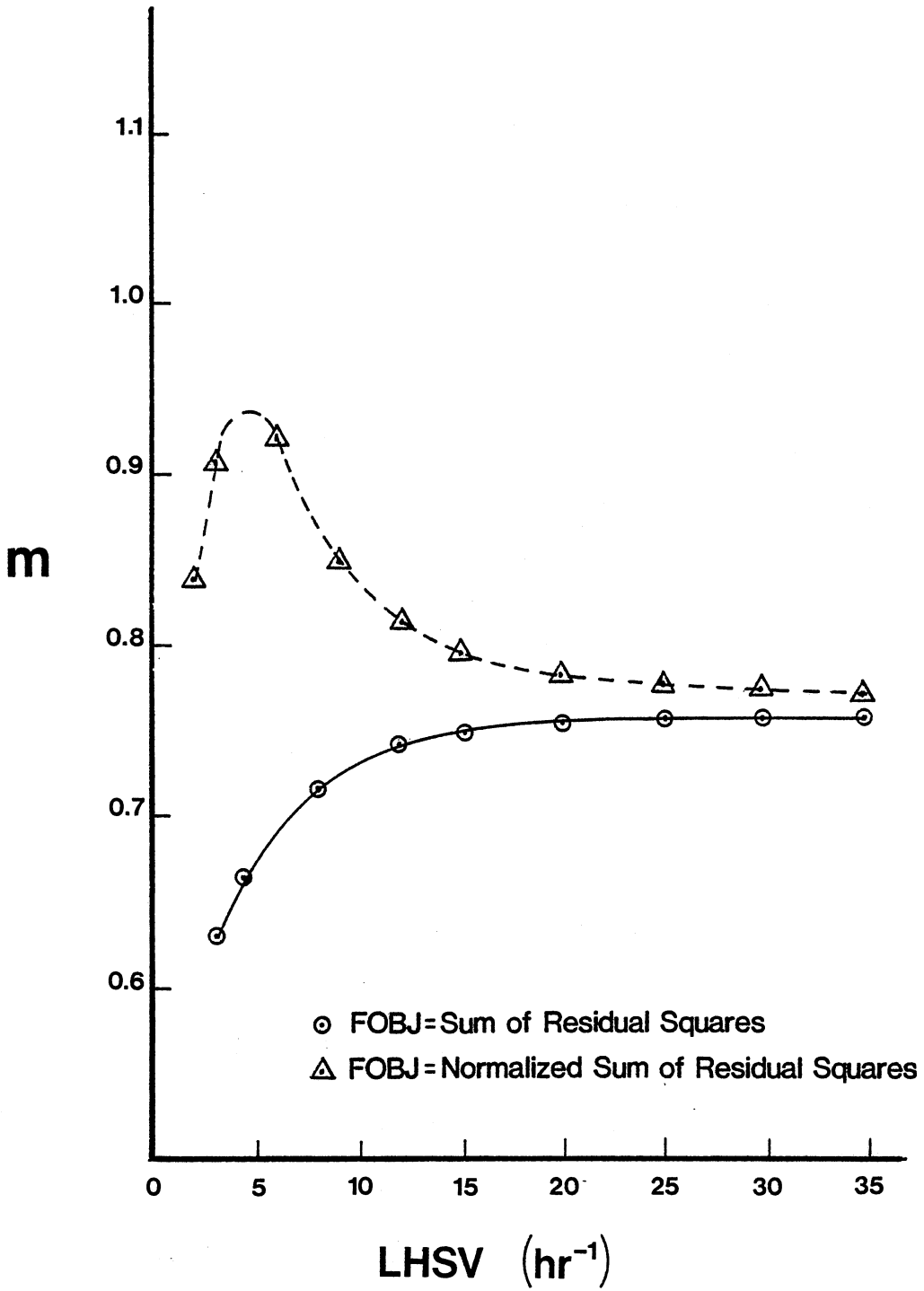


Figure 7. Global Model Order of Hydrogen Pressure Dependence on Space Velocity

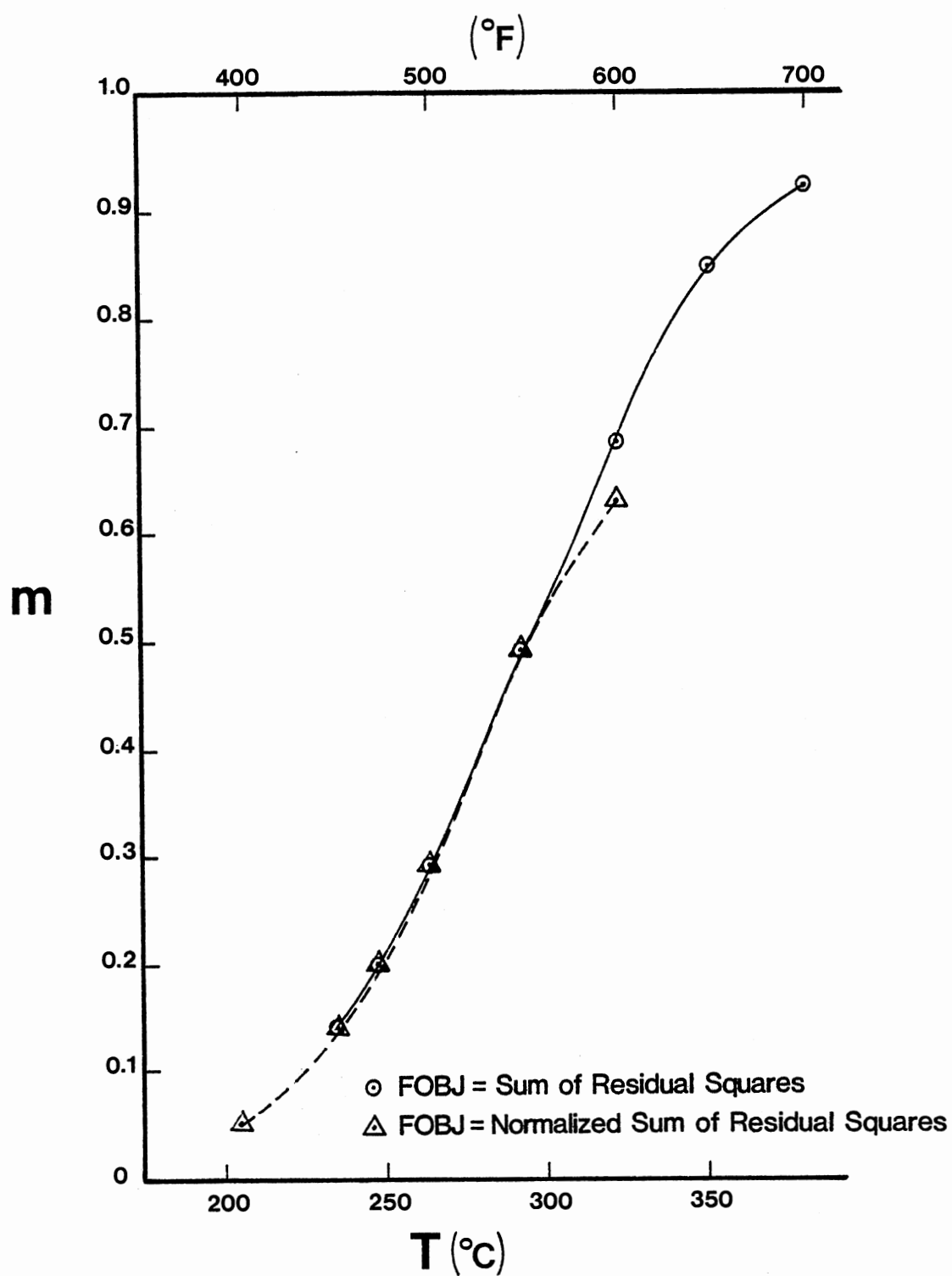


Figure 8. Global Model Order of Hydrogen Pressure Dependence on Temperature

dependence, one can see how the observed global order would vary with changes in the operating conditions, especially temperature due to its strong influence on the reaction rate and adsorption constants.

Not only the plots of m vs LHSV and m vs T , but all the parameter sensitivity curves showed how one could calculate different values for the global model parameters, depending on what objective function he chooses to use. In this case for example, if the hypothetical data were real experimental data collected at a space velocity of 6 hr^{-1} , one would calculate orders of hydrogen partial pressure dependence equal to 0.695 and 0.910 for the two respective objective functions (see Figure 7).

The global order of DBT concentration dependence, n , varied as the operating temperature, hydrogen pressure, and space velocity changed. These dependencies are indicated by the curves in Figures 9, 10, and 11, respectively. Except at temperatures below 290 C (554 F), all values of n fell somewhere in the range between 0.5 and 1.5. As in the case of the order of hydrogen pressure dependence, the variations in n with changing T , P , and LHSV can be attributed to the attempted description of the DBT concentration terms in the intrinsic rate equation by the simplified global counterpart C_R^n .

The variations in these global parameters indicate another likely reason for discrepant literature reports. As an example, if experimental data following the same behavior as this hypothetical system were collected from isothermal runs at 225 C the observed order of DBT concentration dependence, n , would be near 12.5, while isothermal runs above 300 C would result in values near one.

Likewise, the dependency of the pre-exponential constant, A , and

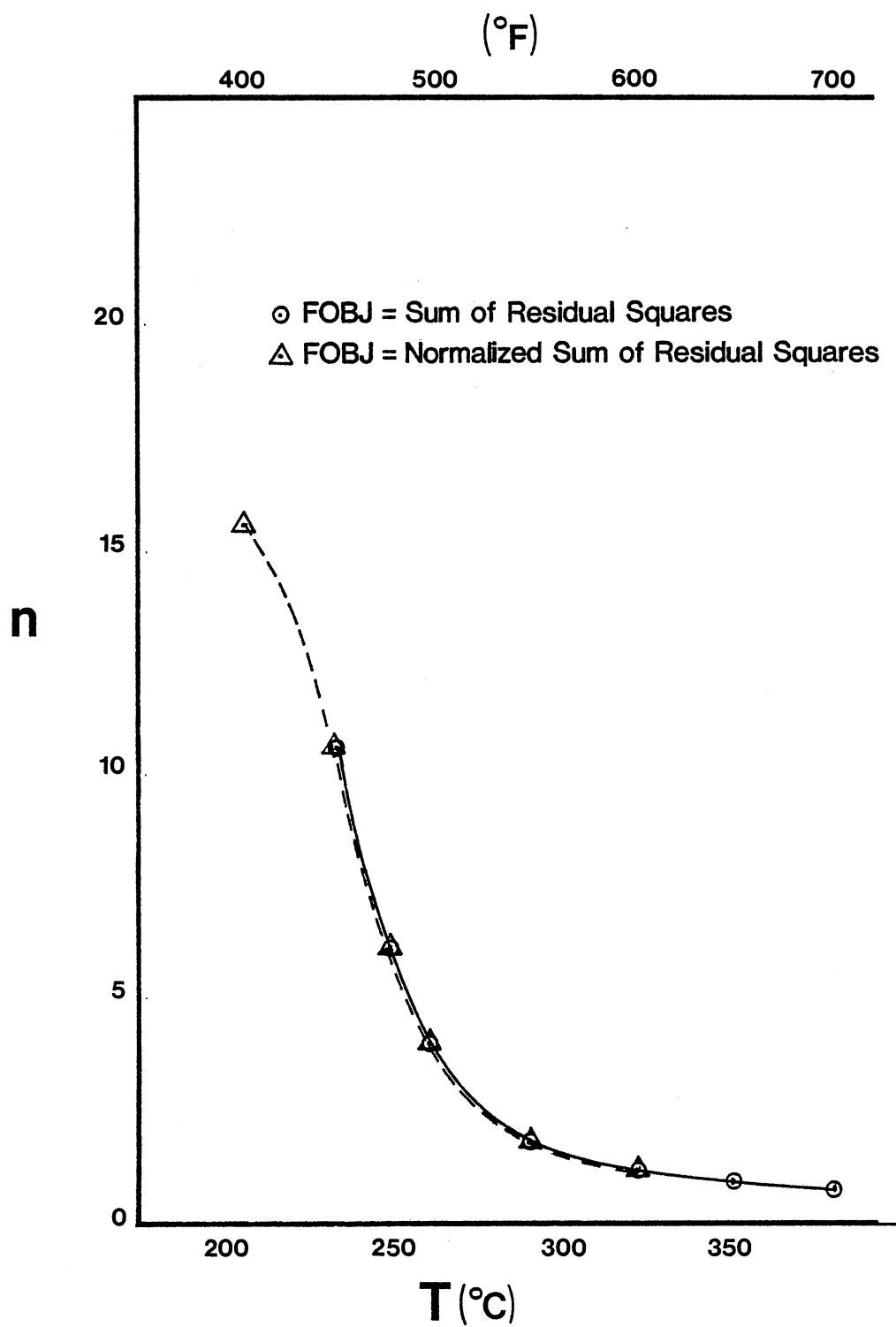


Figure 9. Global Model Order of DBT Concentration Dependence on Temperature

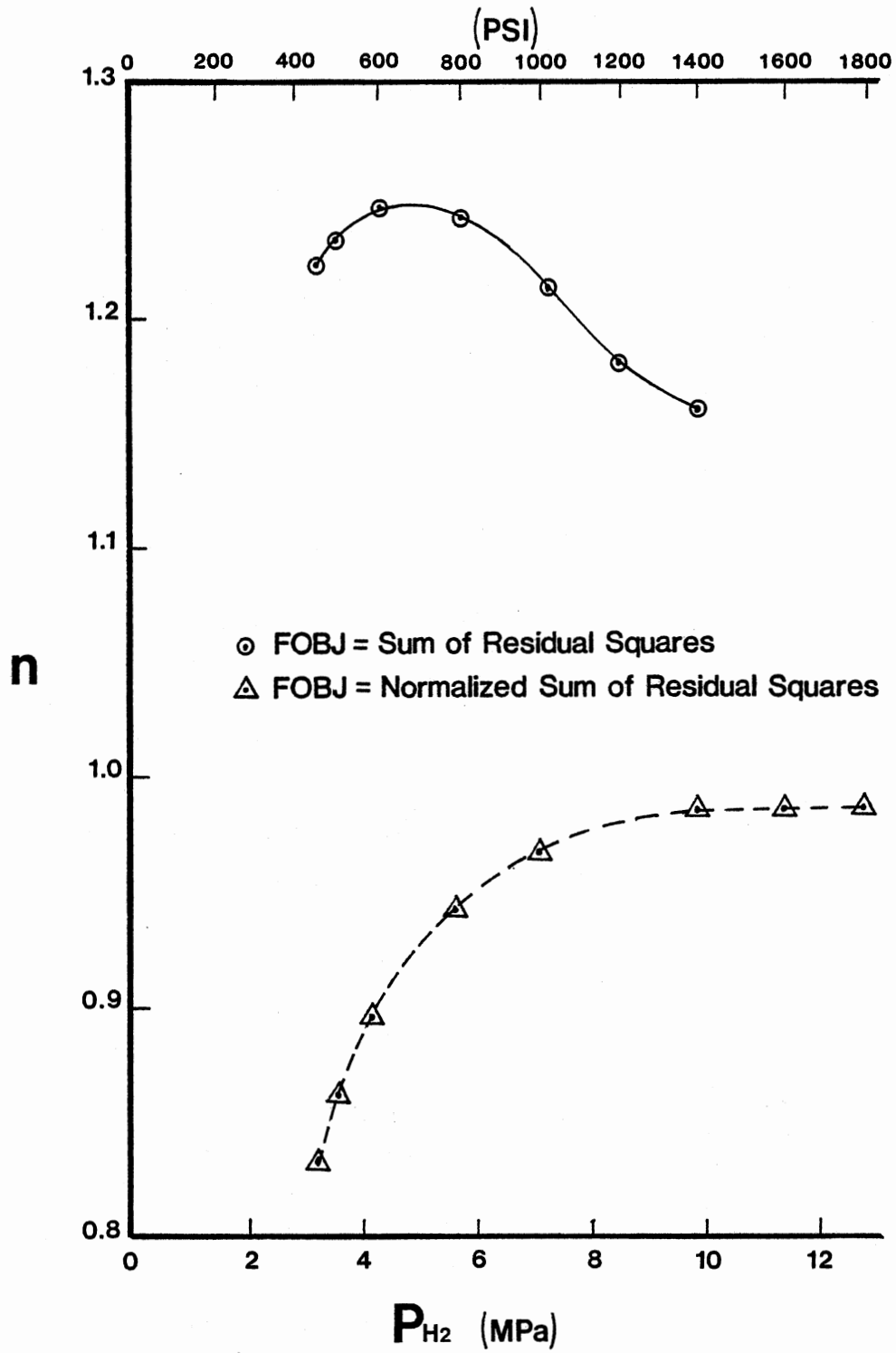


Figure 10. Global Model Order of DBT Concentration Dependence on Hydrogen Pressure

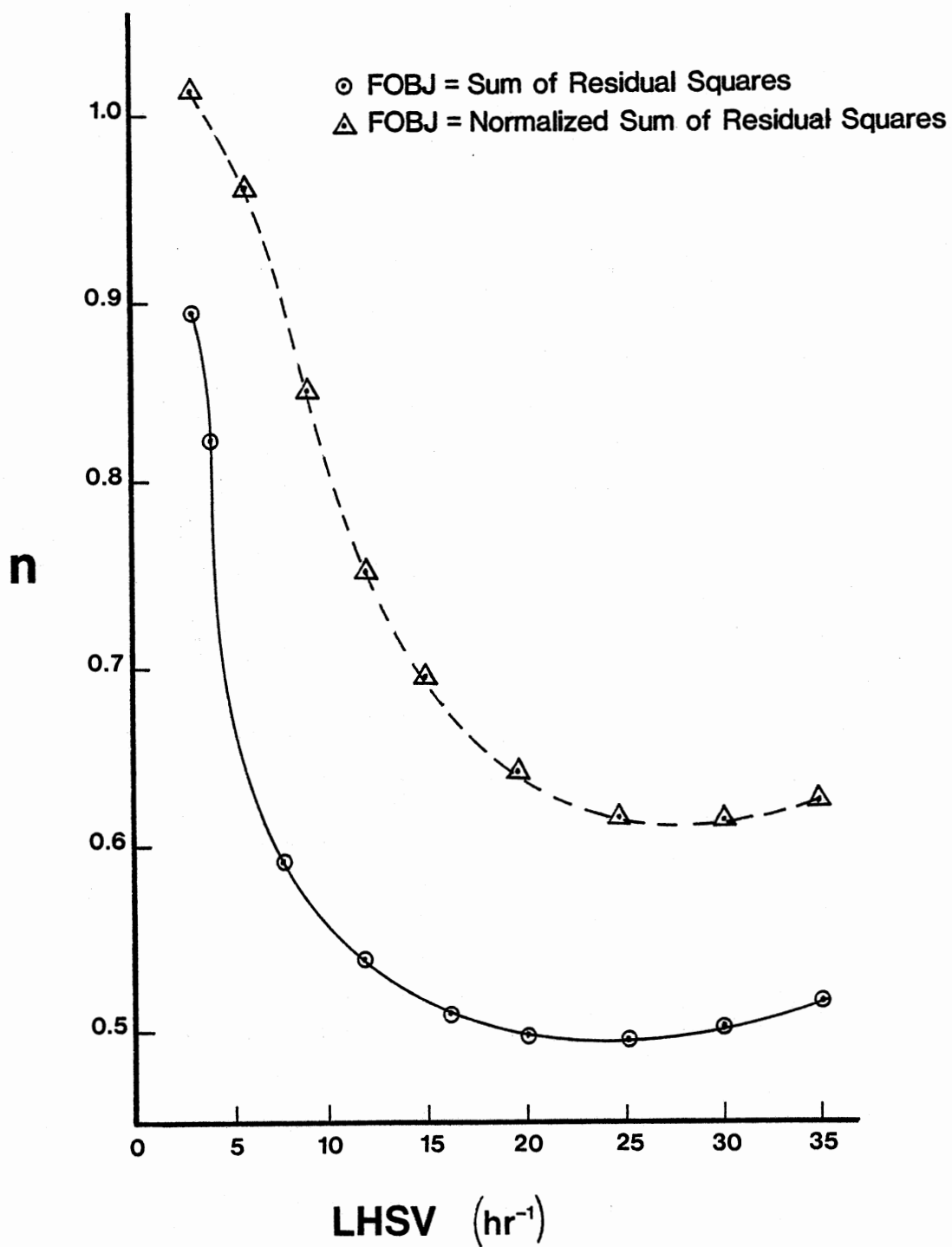


Figure 11. Global Model Order of DBT Concentration Dependence on Space Velocity

activation energy, E , on T , P , and LHSV could be attributed to the attempted description of the combined behavioral effects of the intrinsic constants k , K_H , K_R , and K_P . These plots are shown in Figures 12-16. As one would expect, temperature has a strong effect on these values while hydrogen pressure and space velocities have relatively small influences.

These operating parameter versus global parameter curves establish trends concerning their relationship to the intrinsic kinetics of the hypothetical system. A complete family of such curves, each generated under a specified set of values for the intrinsic parameters and other model constants, would allow some characteristics of the intrinsic kinetics to be recognized from such curves. Eventually, by following a similar procedure for a host of process models, developed under various assumptions concerning rate equations and the physical processes taking place inside the reactor, an analysis of appropriate global data fit calculations could provide information concerning the intrinsic kinetics of a real hydrotreatment system.

Two important observations are apparent from this parameter sensitivity study. First, due to the shallow surface minima, the calculated global parameters have large confidence regions associated with them, and are sensitive to differences in: the data set operating conditions; minimized objective functions; forms of the fitted rate equation; and data fit routines. These characteristics of the global kinetic model are a probable cause for the inconsistent values of the model parameters reported in the literature. Second, due to the empirical nature of the global models, the values of their parameters have no directly corresponding relationship to the true reaction

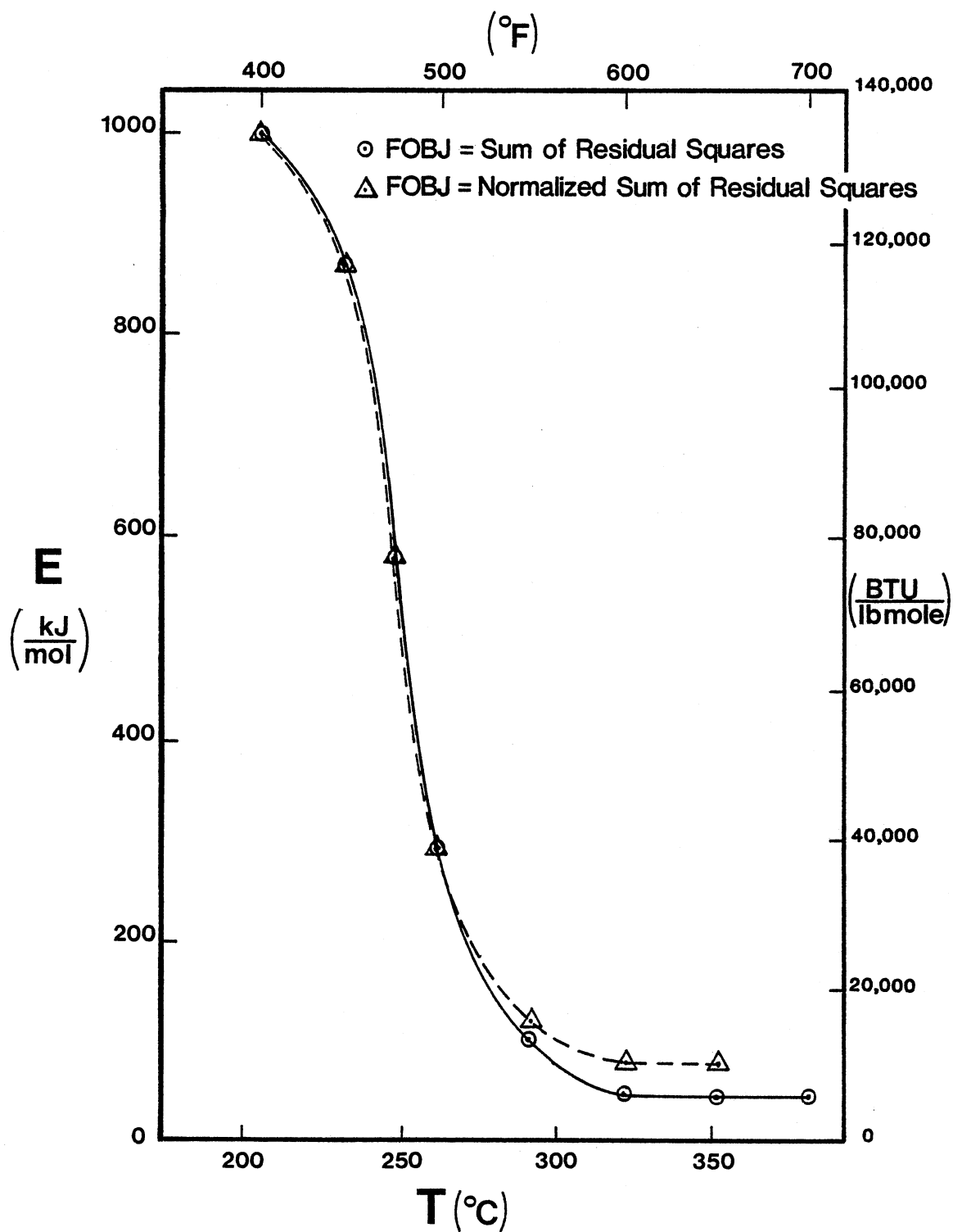


Figure 12. Global Model Activation Energy Dependence on Temperature

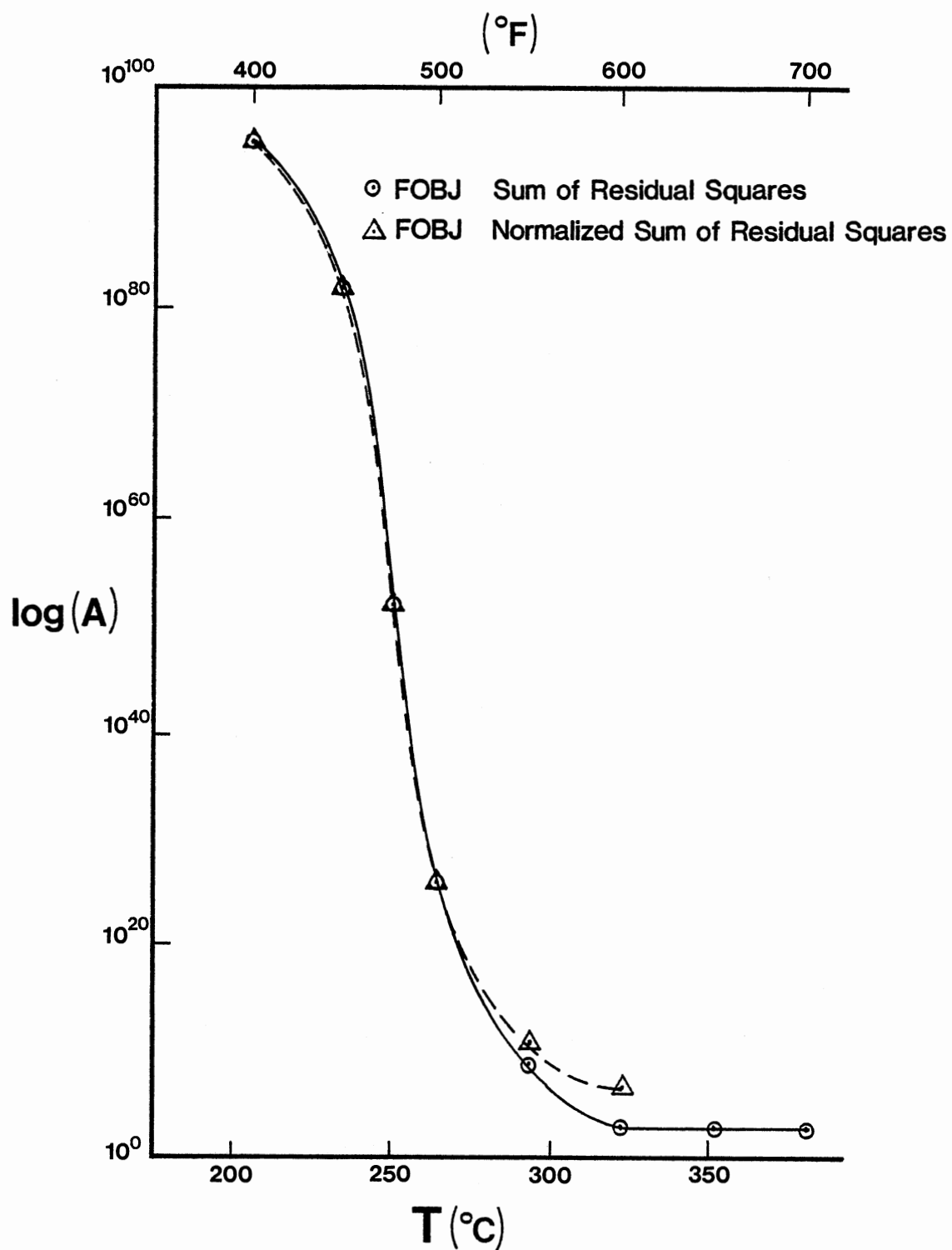


Figure 13. Global Model Pre-Exponential Constant Dependence on Temperature

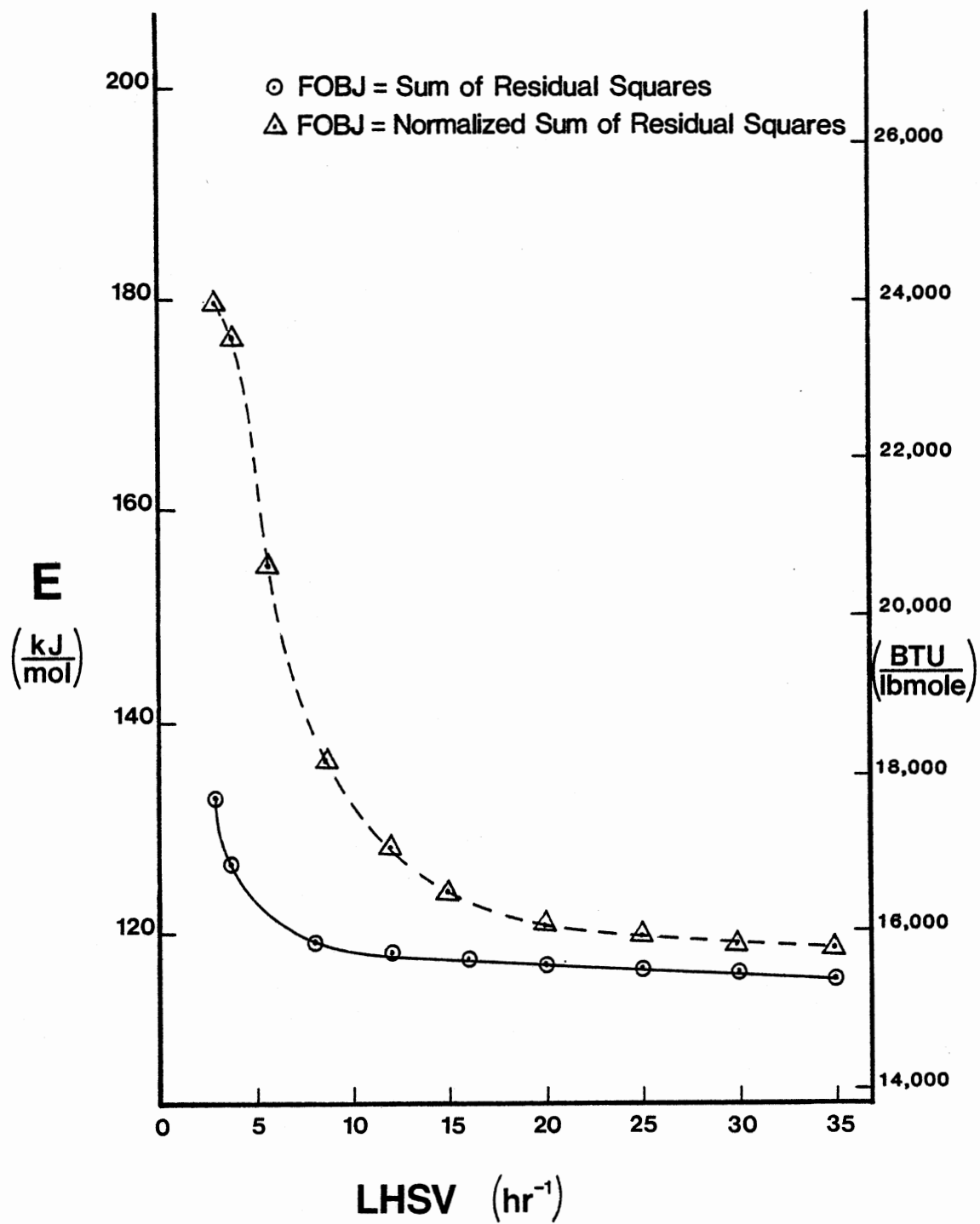


Figure 14. Global Model Activation Energy Dependence on Space Velocity

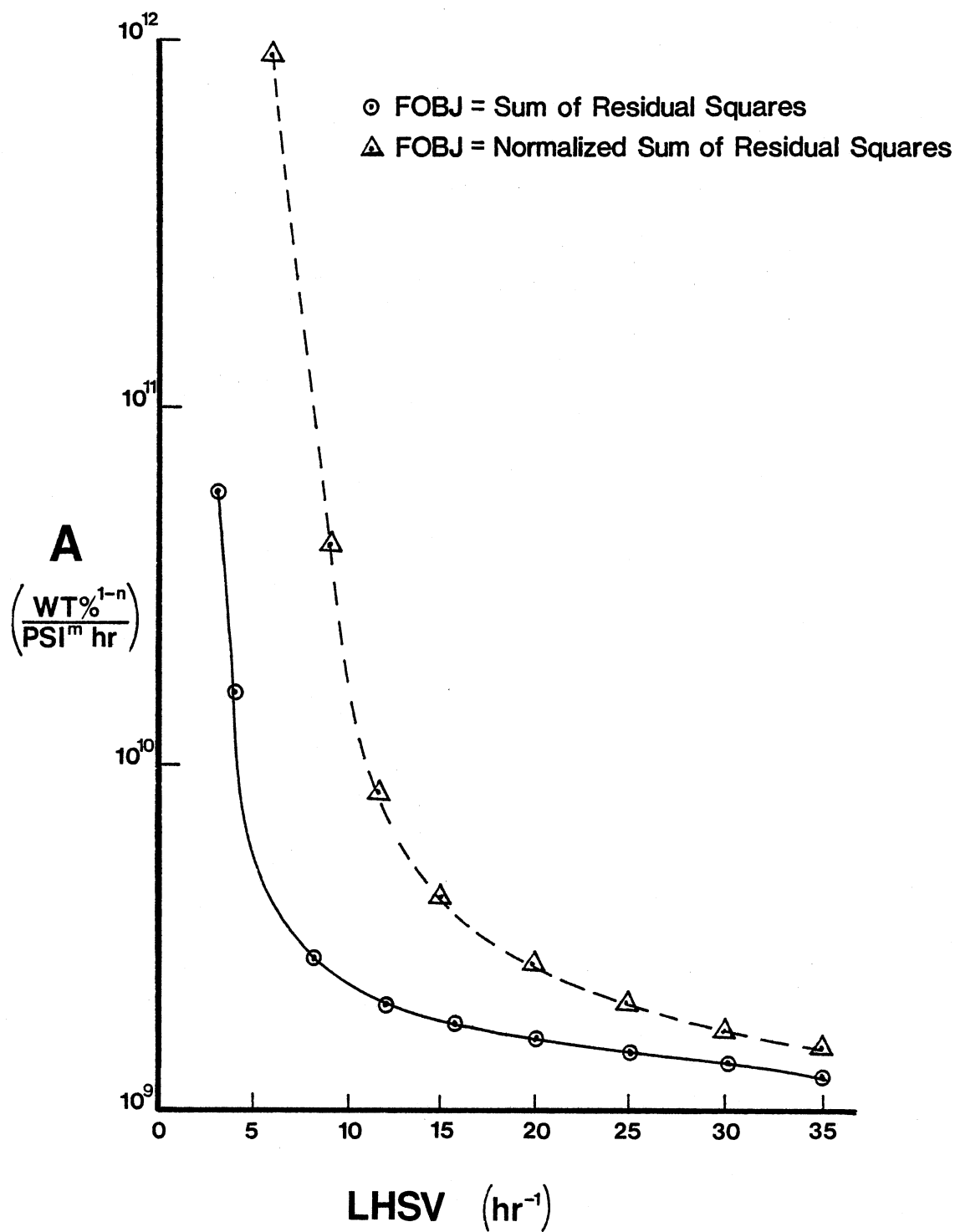


Figure 15. Global Model Pre-Exponential Constant Dependence on Space Velocity

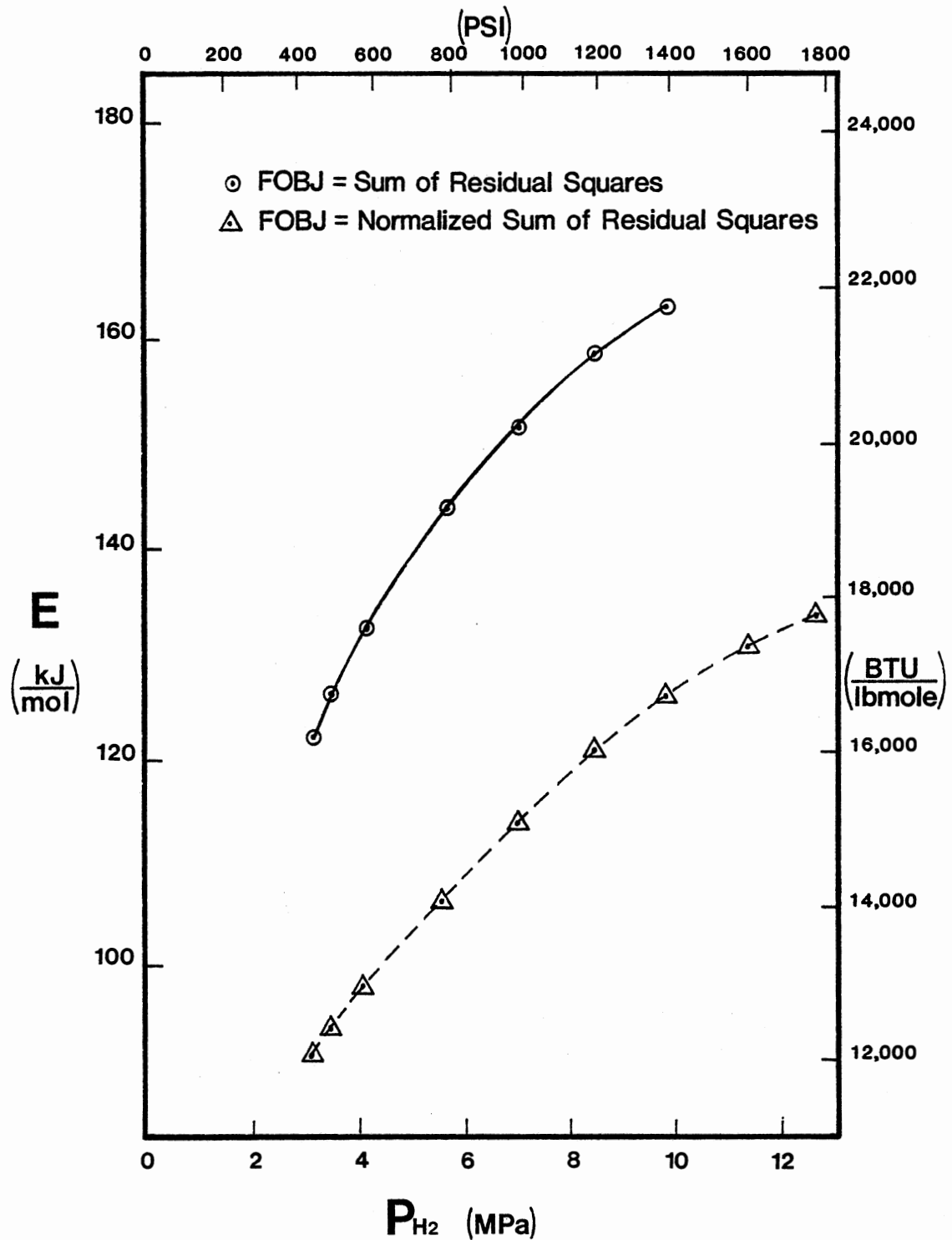


Figure 16. Global Model Activation Energy Dependence on Hydrogen Pressure

kinetics. The only such observation concerning this relationship would be that the global model parameters most closely approximate the intrinsic kinetic orders of DBT and hydrogen concentration dependence at high temperatures, high hydrogen pressures, and low space velocities.

CHAPTER V

SUMMARY AND CONCLUSIONS

Summary

An extensive survey of the literature related to the hydrotreatment of coal-derived liquids revealed a number of reports containing kinetic analyses. In these reports several different forms of global type rate equations were described from which a consensus opinion concerning their analyses was lacking. Although in most cases the authors reported acceptable data fit results for one of the global model forms, few authors made comparisons to other forms of the model. This left the determination of the best form in doubt. In many comparable studies contradictory opinions were offered.

In an attempt to learn the kinetics of CDL hydrotreatment and to resolve the questions concerning the global rate expressions raised in the literature survey, evaluations of several kinetic rate models were performed. These evaluations were obtained through the analysis of appropriate hydrotreatment data fit results.

The values of the n-th order power-law or global kinetic model parameters were calculated which best described each of three separate sets of coal-liquid HDS, HDN, and HDO data. The resulting values of the pre-exponential constants (A), activation energies (E), orders of heteroatom concentration dependence (n), and orders of hydrogen pressure dependence (m), were scattered and inconsistent. Other

observations from the global model CDL data fits were: values of n greater than one generally allowed the best fits to the experimental data; converged values of A , E , m , and n were dependent on the initial estimates of those values and on the form of the fitted function; the estimated values of the parameters included large confidence regions that were in some cases larger than the parameter value itself; and the goodness of fit was not highly dependent on the values of the model parameters, i.e., with a parameter fixed at some arbitrary value far from its "best fit" value only a slightly poorer fit resulted. These observations were concluded to be a characteristic of the global models, which are poorly conditioned for parameter estimation calculations.

The hyperbolic, or intrinsic kinetic model was unable to satisfactorily describe multiple reactant feeds unless they were treated as more than one separately reacting group. These multiple group forms were not investigated in this work.

A mathematical process model was developed to describe the HDS of a model CDL compound, dibenzothiophene. This model included the intrinsic rate expression found to be best suited for the description of the HDS of a single sulfur-containing hydrocarbon. This rate expression was derived from catalytic reaction theory in which two types of adsorption sites were assumed, one type of site for which sulfur containing molecules compete, and a second type of site on which the noncompetitive adsorption of hydrogen occurs. This process model was able to fit a set of experimental dibenzothiophene HDS data under isothermal conditions. The average deviation was less than two percent for each of five isothermal fits. This model was, however, unable to describe the same set of DBT HDS data under nonisothermal conditions

due to an inadequate description of reaction product effects.

A parameter sensitivity study was conducted in which the n-th order global model parameters were calculated which allow the best fit to a hypothetical data set described by the dibenzothiophene HDS model mentioned above, and subsequently plotted as functions of the operating temperature, hydrogen pressure, and space velocity. Several observations were apparent from these curves: the global parameters were dependent upon the minimized objective function; the global parameters were dependent on the operating conditions at which they were calculated; and the global parameters revealed no directly corresponding relationship to the intrinsic kinetics of the system.

Conclusions

The principal conclusions of this work are:

1. The global kinetic model is capable of fitting coal-derived liquid hydrotreatment data with good accuracy.
2. Global kinetic models are poorly conditioned (do not allow their parameters to be sharply defined), resulting in: shallow parameter surface minima; large parameter confidence regions; and dependence of parameter values on the operating conditions at which they were calculated, the minimized objective function, and the fitted form of the rate equation.
3. There is no direct relationship between global and intrinsic parameters, specifically reaction orders, except under certain limited ranges of the operating conditions.
4. The conventional single group intrinsic rate expression is not capable of describing the hydrotreatment of a typical coal-derived

liquid.

5. The two type adsorption site intrinsic kinetic equation may be used to develop an accurate single compound HDS model under isothermal reaction conditions.

Recommendations

Two significant recommendations for further study related to this work were apparent to this author. First, the further development of the single component process model would be valuable to better describe product formation, hydrogen solubility, diffusion and the effectiveness factor, and flow and heat nonidealities. An experimental reactor specifically used to allow collection of the data necessary for proper refinement of this model would be helpful.

Second, a properly expanded set of parameter sensitivity curves would allow recognition of the specific forms of intrinsic kinetic expressions which best describe particular processes through the analysis of the n-th order global data fit results. The possibility of eliminating the trial and error search through possible descriptive intrinsic rate equations would make such an expansion of the parameter sensitivity study worthwhile.

LIST OF REFERENCES

1. Ahmed, M. M., Ph.D. dissertation, Oklahoma State University, Stillwater (1979).
2. Angevine, P. J., Becker, M., and Callen, R. B., Electric Power Research Institute Report EPRI-AF-1255 (1979).
3. Broderick, D. H., and Gates, B. C., Amer. Chem. Soc. Div. Fuel Chem. Prepr. 25(1), 53 (1979).
4. Chakraborty, P., and Kar, A. K., Ind. Eng. Chem. Process Des. Dev., 17(3), 252 (1978).
5. Curtin, D. J., Dearth, J. D., and Everett, G. L., Amer. Chem. Soc. Div. Fuel Chem. Prepr., 23(4), 18 (1978).
6. DeRosset, A. J., U.S. Department of Energy Report FE-2010-01 (1976).
7. Espino, R. L., Sobel, J. E., Singhal, G. H., and Huff, G. A., Jr., Amer. Chem. Soc. Div. Petrol. Chem. Prepr., 23(1), 46 (1978).
8. Froment, G. F., and Bischoff, K. B., "Chemical Reactor Analysis and Design," John Wiley and Sons, New York (1979).
9. Garg, D., Tarrer, A. R., Guinn, J. A., Clinton, J. H., Curtis, C. W., and Paranjape, S. N., Fuel Process. Technol., 3, 263 (1980).
10. Gary, J. H., Golden, J. O., and Bain, R. L., U.S. Department of Energy Report FE-2047-10 (1978).
11. Heck, R. H., Proceedings of EPRI Contractor's Conf., 57 (1977).
12. Heck, R. H., and Stein, T. R., Amer. Chem. Soc. Div. Petrol. Chem. Prepr., 22(3), 948 (1977).
13. Houalla, M., Broderick, D., deBeer, V. H. J., Gates, B. C., and Kwart, H., Amer. Chem. Soc. Div. Petrol. Chem. Prepr., 22(3), 941 (1977).
14. Jacobs, H. E., Jones, J. F., and Eddinger, R. T., Ind. Eng. Chem. Process Des. Dev., 10(4), 558 (1971).
15. Levenspiel, O., "Chemical Reaction Engineering," John Wiley and Sons, New York (1972).

16. Massoth, F. E., J. Catal., 47, 316 (1977).
17. Mehta, D. C., Ph.D. dissertation, Oklahoma State University, Stillwater (1978).
18. Morooka, S., and Hamrin, C. E., Jr., Chem. Eng. Sci., 34, 521 (1979).
19. Perry, R. H., and Chilton, C. H., "Chemical Engineer's Handbook", McGraw-Hill, New York (1973).
20. Prather, J. W., Ahangar, A. N., and Pitts, W. S., Ind. Eng. Chem. Process Des. Dev., 16(3), 267 (1977).
21. Reid, R. C., Prausnitz, J. N., and Sherwood, T. K., "The Properties of Gases and Liquids," McGraw-Hill, New York (1979).
22. Richardson, J. T., Ind. Eng. Chem. Fundam., 3(2), 154 (1964).
23. Rollman, L. D., J. Catal., 46, 243 (1977).
24. Satterfield, C. N., "Heterogeneous Catalysis in Practice," McGraw-Hill, New York (1980).
25. Satterfield, C. N., AIChE J., 21(2), 209 (1975).
26. Satterfield, C. N., Modell, M., and Wilkens, J. A., Ind. Eng. Chem. Process Des. Dev., 19(1), 154 (1980).
27. Satterfield, C. N., and Roberts, G. W., AIChE J., 19(3), 417 (1973).
28. Satchell, D. P., Ph.D. dissertation, Oklahoma State University, Stillwater (1974).
29. Schuit, G. C. A., and Gates, B. C., AIChE J., 19(3), 417 (1973).
30. Schuman, S. C., and Shalit, H., Catal. Rev., 4(2), 245 (1970).
31. Seapan, M., and Crynes, B. L., U. S. Department of Energy Report BC-10306-11 (1981).
32. Shih, S. S., Angevine, P. J., and Heck, R. H., Amer. Chem. Soc. Div. Fuel Chem. Prepr., 25(1), 152 (1980).
33. Singhal, G. H., Espino, R. L., and Sobel, J. E., J. Catal., 67, 446 (1981).
34. Singhal, G. H., Espino, R. L., Sobel, J. E., and Huff, G. A., Jr., J. Catal., 67, 457 (1981).
35. Sivasubramanian, R., Ph.D. dissertation, Oklahoma State University, Stillwater (1977).

36. Sivasubramanian, R., and Crynes, B. L., Ind. Eng. Chem. Prod. Res. Dev., 18(3), 175 (1979).
37. Soni, D. S., M.S. Thesis, Oklahoma State University, Stillwater (1977).
38. Soni, D. S., and Crynes, B. L., Amer. Chem. Soc. Div. Fuel Chem. Prepr., 25(1), 176 (1981).
39. Sonnemans, J., Van Den Berg, G. H., and Mars, P., J. Catal., 31, 220 (1973).
40. Sooter, M. C., M.S. Thesis, Oklahoma State University, Stillwater (1974).
41. Stein, T. R., Cabal, R. B., and Callen, M. J., Electric Power Research Institute Report EPRI-AF-873 (1978).
42. van Deemter, J. J., 3rd Eur. Symp. Chem. Reaction Eng., 215 (1964).
43. Weekman, V. W., Ind. Eng. Chem. Process Des. Dev., 7(1), 90 (1968).
42. White, P. J., Jones, J. F., Eddinger, R. T., Hydrocarbon Processing, 47(12), 97 (1968).

APPENDIX A

DERIVATION OF A LANGMUIR-HINSHELWOOD TYPE

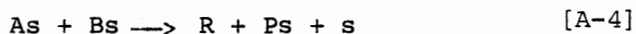
KINETIC RATE EQUATION FOR A

SOLID-CATALYZED REACTION

Consider the following irreversible chemical reaction:



Assume the following adsorption, reaction, desorption mechanism where s represents a catalyst adsorption site:



Define the following terms:

C_i = concentration of species i in the liquid near the catalyst surface.

k_{if}, k_{ir} = forward and reverse rate constants for step i

r_i = rate of step i

K_i = equilibrium constant for step i

ϕ_i = fraction of total catalyst adsorption sites occupied by species i , where $\phi_s = 1 - \sum \phi_i$

If the reaction occurs near equilibrium conditions the step rates may be expressed as:

$$r_A = k_{Af}C_A(1 - \phi_A - \phi_B - \phi_P) - k_{Ar}\phi_A \quad [A-6]$$

$$r_B = k_{Bf}C_B(1 - \phi_A - \phi_B - \phi_P) - k_{Br}\phi_B \quad [A-7]$$

$$r = k_f\phi_A\phi_B \quad [A-8]$$

$$r_P = k_{Pf}\phi_P - k_{Pr}C_P(1 - \phi_A - \phi_B - \phi_P) \quad [A-9]$$

Solving for equilibrium constants and fractional adsorption site coverages:

$$K_A = \frac{k_{Af}}{k_{Ar}} = \frac{\phi_A}{C_A(1 - \phi_A - \phi_B - \phi_P)} \quad [A-10]$$

$$\phi_A = K_A C_A (1 - \phi_A - \phi_B - \phi_P) = K_A C_A \phi_s \quad [A-11]$$

$$K_B = \frac{k_{Bf}}{k_{Br}} = \frac{\phi_B}{C_B(1-\phi_A-\phi_B-\phi_P)} \quad [A-12]$$

$$\phi_B = KBCB(1 - \phi_A - \phi_B - \phi_P) = KBCB S \quad [A-13]$$

$$K_P = \frac{k_{Pr}}{k_{Pf}} = \frac{\phi_P}{C_P(1-\phi_A-\phi_B-\phi_P)} \quad [A-14]$$

$$\phi_P = KPCP(1 - \phi_A - \phi_B - \phi_P) = KPCP\phi_S \quad [A-15]$$

The vacant catalyst site fraction may now be expressed as:

$$\phi_S = 1 - KACA\phi_S - KBCB\phi_S - KPCP\phi_S \quad [A-16]$$

Solving for ϕ_S :

$$\phi_S = \frac{1}{1 + K_A C_A + K_B C_B + K_P C_P} \quad [A-17]$$

Substituting for ϕ_S in Equations (A-11,13):

$$\phi_A = \frac{K_A C_A}{1 + K_A C_A + K_B C_B + K_P C_P} \quad [A-18]$$

$$\phi_B = \frac{K_B C_B}{1 + K_A C_A + K_B C_B + K_P C_P} \quad [A-19]$$

Substituting for ϕ_A and ϕ_B in Equation (A-8):

$$r = \frac{k_{C_A C_B}}{(1 + K_A C_A + K_B C_B + K_P C_P)^2} \quad [A-20]$$

Combining constants:

$$r = \frac{k_{C_A C_B}}{(1 + K_A C_A + K_B C_B + K_P C_P)^2} \quad [A-21]$$

APPENDIX B

INTEGRATION OF PLUG FLOW DESIGN EQUATION

WITH INTRINSIC RATE EQUATION

The ideal plug flow design equation is expressed as:

$$\frac{W}{f_{R1}} = \int_0^{X_R} \frac{dX_R}{r} \quad [B-1]$$

where W is the weight of the catalyst, f_{R1} is the reactant feed rate, X_R is the reactant conversion, and r the reaction rate. The reaction rate equation used in this model is written below:

$$r = \frac{k\eta C_R C_H}{(1 + K_R \eta C_R + K_P C_P)(1 + K_H C_H)} \quad [B-2]$$

Let:

$$X_R = 1 - C_{R2}/C_{R1} \quad [B-3]$$

$$dX_R = -dC_R/C_{R1} \quad [B-4]$$

$$\frac{-WC_{R1}}{f_{R1}} = \int_{C_{R1}}^{C_{R2}} \frac{dC_R}{r} \quad [B-5]$$

$$\frac{-WC_{R1}}{f_{R1}} = \int_{C_{R1}}^{C_{R2}} \frac{(1 + K_R \eta C_R + K_P C_P)(1 + K_H C_H)}{k\eta C_R C_H} dC_R \quad [B-6]$$

$$\frac{-WC_{R1} k C_H}{f_{R1} (1 + K_H C_H)} = \int_{C_{R1}}^{C_{R2}} \frac{(1 + K_R C_R + K_P C_P)}{C_R} dC_R \quad [B-7]$$

Define:

$$C_P = C_{R1} + C_{R2} + C_{P1} \quad [B-8]$$

$$\frac{-WC_{R1} k\eta C_H}{f_{R1} (1 + K_H C_H)} = \int_{C_{R1}}^{C_{R2}} \frac{((1 + k_P(C_{R1} + C_{P1})) + (K_R \eta - K_P)C_R)}{C_R} dC_R \quad [B-9]$$

$$\begin{aligned} \frac{-WC_{R1} k\eta C_H}{f_{R1} (1 + K_H C_H)} &= (1 + K_P(C_{R1} + C_{P1})) \ln \frac{C_{R2}}{C_{R1}} \\ &+ (K_R \eta - K_P)(C_{R2} - C_{R1}) \end{aligned} \quad [B-10]$$

Solving for outlet concentration:

$$C_{R2} = C_{R1} + \frac{(1 + K_P (C_{R1} + C_{P1}))}{(K_R \eta - K_P)} \ln \frac{C_{R1}}{C_{R2}} - \frac{WC_{R1} k \eta C_H}{f_{R1} (1 + K_H C_H) (K_R \eta - K_P)} \quad [B-11]$$

if f_{R1} and C_{R1} have units (wt/time) and (wt%) then:

$$f_{R1} = \frac{C_{R1} (\text{LHSV}) (V) (\rho)}{100} \quad [B-12]$$

Substituting for f_{R1} in Equation (B-11):

$$C_{R2} = C_{R1} + \frac{(1 + K_P (C_{R1} + C_{P1}))}{(k_R \eta - K_P)} \ln \frac{C_{R1}}{C_{R2}} - \frac{K(\eta) (C_H) (W) (100)}{(1 + K_H C_H) (K_R \eta - K_P) (\text{LHSV}) (V) (\rho)} \quad [B-13]$$

APPENDIX C

PARAMETER SENSITIVITY CALCULATION DATA

TABLE IX

PARAMETER SENSITIVITY - CONSTANT PRESSURE GLOBAL MODEL PARAMETERS

P_{H_2} psi	K_p wt% ¹⁻ⁿ /hr	E Kcal/gmole	n	Average Error %	FOBJ (wt%) ²
450	2.143 E11	2.938 E4	1.222	1.513 E1	1.064 E-1
500	5.682 E11	3.042 E4	1.233	1.856 E1	9.244 E-2
600	3.184 E12	3.227 E4	1.246	2.685 E1	7.045 E-2
800	4.172 E13	3.502 E4	1.239	4.572 E1	4.230 E-2
1000	2.241 E14	3.680 E4	1.210	5.934 E1	2.811 E-2
1200	6.983 E14	3.800 E4	1.181	6.517 E1	2.141 E-2
1400	1.580 E15	3.885 E4	1.159	6.765 E1	1.841 E-2

$$K_p = AP^m$$

$$FOBJ = \sum (c_{fit} - c_{dat})^2$$

TABLE X

PARAMETER SENSITIVITY - CONSTANT PRESSURE GLOBAL MODEL PARAMETERS
(NORMALIZED OBJECTIVE FUNCTION)

P_{H_2} psi	K_P wt% ¹⁻ⁿ /hr	E Kcal/gmole	n	Average Error %	FOBJ
450	6.272 E8	2.237 E4	8.305 E-1	1.239 E1	1.385
500	1.107 E9	2.294 E4	8.576 E-1	1.280 E1	1.430
600	3.156 E9	2.401 E4	8.970 E-1	1.343 E1	1.512
800	1.937 E10	2.590 E4	9.425 E-1	1.411 E1	1.656
1000	9.068 E10	2.753 E4	9.656 E-1	1.431 E1	1.779
1200	3.486 E11	2.898 E4	9.775 E-1	1.429 E1	1.882
1400	1.153 E12	3.029 E4	9.831 E-1	1.421 E1	1.965
1600	3.366 E12	3.148 E4	9.850 E-1	1.397 E1	2.030
1800	8.718 E12	3.254 E4	9.848 E-1	1.382 E1	2.080
2000	1.981 E13	3.346 E4	9.839 E-1	1.374 E1	2.118

$$K_P = AP^m$$

$$FOBJ = \sum \left(\frac{C_{fit} - C_{dat}}{C_{dat}} \right)^2$$

TABLE XI

PARAMETER SENSITIVITY - CONSTANT SPACE VELOCITY GLOBAL MODEL PARAMETERS

LHSV hr ⁻¹	A wt% ¹⁻ⁿ /psi ^m /hr	E Kcal/gmole	m	n	Average Error %	FOBJ (wt%) ²
3	6.030 E10	3.210 E4	6.303 E-1	8.915 E-1	3.287 E-1	3.422 E-2
4	1.562 E10	3.075 E4	6.650 E-1	8.208 E-1	1.181 E-1	3.873 E-2
8	2.557 E9	2.882 E4	7.148 E-1	5.951 E-1	3.290	3.091 E-2
12	2.004 E9	2.866 E4	7.412 E-1	5.428 E-1	1.456	1.841 E-2
16	1.645 E9	2.847 E4	7.523 E-1	5.090 E-1	9.297 E-1	1.150 E-2
20	1.452 E9	2.835 E4	7.589 E-1	4.937 E-1	7.020 E-1	2.782 E-3
25	1.314 E9	2.827 E4	7.645 E-1	4.914 E-1	5.417 E-1	5.198 E-3
30	1.227 E9	2.822 E4	7.684 E-1	5.002 E-1	4.425 E-1	3.713 E-3
35	1.163 E9	2.819 E4	7.714 E-1	5.157 E-1	3.747 E-1	2.783 E-3

$$\text{FOBJ} = \sum (C_{\text{fit}} - C_{\text{dat}})^2$$

TABLE XII

PARAMETER SENSITIVITY - CONSTANT SPACE VELOCITY GLOBAL MODEL PARAMETERS
(NORMALIZED OBJECTIVE FUNCTION)

LHSV hr ⁻¹	A wt% ¹⁻ⁿ /psi ^m /hr	E Kcal/gmole	m	n	Average Error %	FOBJ
2	1.975 E14	4.309 E4	8.371 E-1	1.005	1.100 E-1	6.000 E-1
3	7.514 E13	4.250 E4	9.039 E-1	1.011	8.535	3.441 E-1
9	3.733 E10	3.313 E4	8.474 E-1	8.468 E-1	1.984	1.870 E-2
12	8.367 E9	3.104 E4	8.118 E-1	7.521 E-1	1.273	7.620 E-3
15	4.009 E9	3.000 E4	7.955 E-1	6.900 E-1	9.509 E-1	4.100 E-3
20	2.248 E9	2.919 E4	7.854 E-1	6.359 E-1	6.810 E-1	2.010 E-3
25	1.707 E9	2.882 E4	7.825 E-1	6.158 E-1	5.322 E-1	1.210 E-3
30	1.454 E9	2.863 E4	7.819 E-1	6.136 E-1	4.373 E-1	8.100 E-4
35	1.306 E9	2.851 E4	7.821 E-1	6.216 E-1	3.715 E-1	5.800 E-4

$$FOBJ = \sum \left(\frac{C_{fit} - C_{dat}}{C_{dat}} \right)^2$$

TABLE XIII

PARAMETER SENSITIVITY - CONSTANT TEMPERATURE GLOBAL MODEL PARAMETERS

T °F	K_t wt% ¹⁻ⁿ /psi ^m /hr	m	n	Average Error %	FOBJ (wt%) ²
450	3.329 E-6	1.332 E-1	1.055 E-1	1.339 E-2	5.559 E-6
475	3.011 E-4	2.026 E-1	6.059	4.613 E-2	5.791 E-5
500	3.722 E-3	2.898 E-1	3.591	1.348 E-1	4.001 E-4
550	2.985 E-2	4.944 E-1	1.484	7.557 E-1	5.118 E-3
600	5.359 E-2	6.810 E-1	9.333 E-1	6.003	9.221 E-3
650	7.077 E-2	8.403 E-1	7.048 E-1	1.048 E14	1.014 E-2
700	1.204 E-1	9.187 E-1	5.222 E-1	3.831 E9	9.689 E-4

$$K_t = A \exp(-E/RT)$$

$$FOBJ = \sum (c_{fit} - c_{dat})^2$$

TABLE XIV

PARAMETER SENSITIVITY - CONSTANT TEMPERATURE GLOBAL MODEL PARAMETERS
(NORMALIZED OBJECTIVE FUNCTION)

T °F	K_t wt% ¹⁻ⁿ /psi ^m /hr	m	n	Average Error %	FOBJ
400	6.293 E-9	4.680 E-2	1.574 E-1	1.847 E-3	6.354 E-8
450	3.334 E-6	1.331 E-1	1.055 E-1	1.339 E-2	5.559 E-6
475	3.022 E-4	2.023 E-1	6.057	4.615 E-2	5.791 E-5
500	3.760 E-3	2.886 E-1	3.588	1.349 E-1	4.003 E-4
550	3.157 E-2	4.863 E-1	1.477	7.476 E-1	5.210 E-3
600	7.623 E-2	6.277 E-1	9.730 E-1	3.858	3.325 E-2

$$K_t = A \exp(-E/RT)$$

$$FOBJ = \sum \left(\frac{C_{fit} - C_{dat}}{C_{dat}} \right)^2$$

TABLE XV

PRE-EXPONENTIAL CONSTANTS AND ACTIVATION ENERGIES CALCULATED FROM THE
ARRHENIUS PLOT OF THE GLOBAL MODEL CONSTANT K_t

T	A	E	A	E
°F	wt% ¹⁻ⁿ /psi ^m /hr	Kcal/gmole	wt% ¹⁻ⁿ /psi ^m /hr	Kcal/gmole
400	9.621 E94	2.317 E5	9.621 E94	2.317 E5
450	2.448 E81	2.009 E5	2.452 E81	2.009 E5
475	2.123 E52	1.327 E5	2.131 E52	1.327 E5
500	6.285 E25	6.889 E4	6.348 E25	6.889 E4
550	2.285 E8	2.538 E4	2.432 E9	2.795 E4
600	2.214 E2	9.745 E3	3.039 E5	1.779 E4
650	2.014 E2	9.745 E3	---	1.779 E4
700	2.431 E2	9.745 E3	---	1.779 E4

$$FOBJ = \sum (C_{fit} - C_{dat})^2$$

$$FOBJ = \sum \left(\frac{C_{fit} - C_{dat}}{C_{dat}} \right)^2$$

$$K_t = A \exp(-E/RT)$$

TABLE XVI

PRE-EXPONENTIAL CONSTANT AND ACTIVATION ENERGY CALCULATED FROM THE
 LINEAR REGRESSION OF LOGARITHMIC PLOT OF THE GLOBAL
 MODEL CONSTANT K_p VERSUS HYDROGEN PRESSURE

Slope = m	7.990	6.975
Standard error	2.123	1.417
Intercept = log A	-9.751	-9.844
Standard error	6.155	4.266
A (wt% ¹⁻ⁿ /psi ^m /hr)	1.722 E-10	1.433 E-10
Coeff. of det.	0.993	0.997
FOBJ	$\sum (C_{\text{fit}} - C_{\text{dat}})^2$	$\sum \left(\frac{C_{\text{fit}} - C_{\text{dat}}}{C_{\text{dat}}} \right)^2$

APPENDIX D

LISTING OF THE MODIFIED MARQUARDT NONLINEAR
DATA FIT PROGRAM


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6      DOUBLE PRECISION P,V,YSIG,H,SCALE,XMAX,XMIN,DELTX,DELMN,      MARO 112
      * ERR,POBJ,FLAMB,FNU,RELP,OSORT,ARG,CRIT,FLDEF,RELMN,      MARO 113
      * RLTL,FACECL,HUGE,RZERO,RUNIT,RTWO,DELN,FMGN,FCUT,      MARO 114
      * STFAC,RTERM,SCALE,SA,PIVOT,EM,SUM,COSIN,SE,SC,NH,      MARO 115
      * FRMIN,SMR,XMH,DENON,FRAC,UPFAC,RLFAC,RSFAC,RMSDV,      MARO 116
      * SOVMX,OMAX1,OMINI,OABS,ARGB      MARO 117
7      DOUBLE PRECISION X,XSAVE,XTEMP,GRAD,FIT,FITSV,      MARO 118
      * XSAV,SIG,RTERM,PHI,PMNEW,PMALP,XLIM      MARO 119
C      THE DIMENSIONS OF THE VECTORS AND MATRICES (AS OPPOSED TO ARRAYS)      MARO 120
C      ARE ...      MARO 121
C      P(NPTS,NACTV) (OR P(1,NACTV) IF KALCP.EQ.-1),      MARO 122
C      FITSV(NPTS) (OR FITSV(1) IF KALCP.EQ.-1),      MARO 123
C      X(NV),XMAX(NV),XMIN(NV),DELMN(NV),ERR(NV,NV+1),      MARO 124
C      XSAVE(NV),HWI,MSKTI(NV),      MARO 125
C      GRAD(NACTV),SCALE(NACTV),      MARO 126
C      Y(NPTS),FIT(NPTS),YSIG(NPTS) (OR YSIG(1) IF LEQU.NE.O),      MARO 127
C      WHERE NACTV IS THE NUMBER OF ACTIVE (UNMASKED) X(J).      MARO 128
C      DIMENSION P(LPDMA,LPDMB)      MARO 129
8      DIMENSION Y(1),YSIG(1),FIT(1),FITSV(1)      MARO 130
9      DIMENSION XSAVE(20),H(20),GRAD(20),MSKT(20),XTEMP(20)      MARO 131
10     DIMENSION XSAVE(20),H(20),GRAD(20),MSKT(20),XTEMP(20)      MARO 132
C      USER COMMON .....      MARO 133
11     COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),      MARO 134
      * ERR(20,21),POBJ,NV,NTRAC,MATX,MSK(20),      MARO 135
      * NPMAX,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERPL,KW      MARO 136
C      MARO COMMON .....      MARO 137
12     COMMON /MLL34/ FLAMB,FNU,RELP,RELMN,METHD,KALCP,KORDP,MAXIT,      MARO 138
      * LEQU,MXSUB,MXUPD      MARO 139
C      SET THE LIBRARY FUNCTIONS FOR DOUBLE PRECISION (DSORT, DABS, DMAX1,      MARO 140
C      DMIN1) OR FOR SINGLE PRECISION (SORT, ABS, AMAX1, AMIN1).      MARO 141
C      OSORT(ARG)=DSORT(ARG)      MARO 142
13     OABS(ARG)=DABS(ARG)      MARO 143
14     OMAX1(ARG,ARGB)=DMAX1(ARG,ARGB)      MARO 144
15     OMIN1(ARG,ARGB)=DMIN1(ARG,ARGB)      MARO 145
16     *****      MARO 146
C      SET FIXED QUANTITIES ....      MARO 147
C      NVMAX IS THE MAXIMUM PERMISSIBLE VALUE OF NV. IT IS ALSO THE      MARO 148
C      DIMENSION OF THE ARRAYS X, XMAX, XMIN, MASK, DELMN,      MARO 149
C      XSAVE, H, MSKT, GRAD, AND SCALE, AND THE FIRST DIMENSION OF ERR.      MARO 150
C      THE SECOND DIMENSION OF ERR IS NVMAX+1.      MARO 151
17     NVMAX=20      MARO 152
C      CRIT ... COSINE OF MARQUARDT-S CRITICAL      MARO 153
C      ANGLE, GAMMA SUB ZERO      MARO 154
18     CRIT=.70711      MARO 155
C      FLDEF ... DEFAULT VALUE FOR FLAMB      MARO 156
19     FLDEF=1.      MARO 157
C      RLTL ... TOLERANCE FOR A WARNING MESSAGE      MARO 158
20     RLTL=1.E-4      MARO 159
C      FACECL ... ACCELERATION FACTOR FOR FCUT      MARO 160
21     FACECL=2.      MARO 161
C      FNULM ... LIMIT ON THE FACTOR BY WHICH      MARO 162
C      (1+FLAMB) MAY CHANGE      MARO 163
22     FNULM=2.      MARO 164
C      HUGE ... A VERY LARGE REAL NUMBER      MARO 165
C      (DEFAULT VALUE FOR XMAX AND XMIN)      MARO 166
23     HUGE=1.E30      MARO 167
24     RZERO=0.      MARO 168
25     RUNIT=1.      MARO 169
26     RTWO=2.      MARO 170
C      NO FLOATING POINT CONSTANTS ARE USED BEYOND THIS POINT.      MARO 171
C      NFLAG=0      MARO 172
27     NOREP=0      MARO 173
28     ITER=0      MARO 174
29     PHI=HUGE      MARO 175
30     SC=HUGE      MARO 176
31     IF(NTRAC.GE.-1) WRITE(KW,10)      MARO 177
32     10 FORMAT(48H1MRO ... BEGIN NONLINEAR LEAST SQUARES SOLUTION)      MARO 178
33     NACTV=99      MARO 179
34     IF(NV.GT.O .AND. NV.LE.NVMAX .AND. NV.LE.LPDMA .AND.      MARO 180
      * NPTS.GE.1 .AND. [KALCP.LT.O .OR. NPTS.LE.LPDMA]) GO TO 20      MARO 181
35     NFLAG=1      MARO 182
36     GO TO 80      MARO 183
37     CHECK SOME INPUT QUANTITIES, AND SET THEM TO DEFAULT VALUES IF      MARO 184
C      DESIRED.      MARO 185
C      NACTV ... NUMBER OF ACTIVE X(J)      MARO 186
38     20 NACTV=0      MARO 187
39     DO 50 JX=1,NV      MARO 188
40     DELN=OABS(DELMN(JX))      MARO 189
41     IF(MASK(JX))10,30,50      MARO 190
42     30 NACTV=NACTV+1      MARO 191
43     IF(DELN.EQ.RZERO) DELN=OABS(RELMN*X(JX))      MARO 192
44     IF(DELN.EQ.RZERO) DELN=RELMN      MARO 193
45     IF(XMAX(JX).GT.XMIN(JX)) GO TO 40      MARO 194
46     XMAX(JX)=HUGE      MARO 195
47     XMIN(JX)=-HUGE      MARO 196
48     X(JX)=OMAX1(XMIN(JX),OMINI(XMAX(JX),X(JX)))      MARO 197
49     DELM(JX)=DELN      MARO 198
C      IF(NACTV.GT.O) GO TO 80      MARO 199
50     KFLAG=2      MARO 200
51     80 CONTINUE      MARO 201
52     WRITE(KW,70)NV,NVMAX,NACTV,NPTS,LPDMA,LPDMB,KALCP      MARO 202
53     70 FORMAT(/29H ILLEGAL INPUT VALUE IN MARO ,4X,5H NV ,13,4X,      MARO 203
      * 5H NVMAX ,13,4X,5H NACTV ,13/10X,7H NPTS ,13,4X,5H LPDMA ,13,      MARO 204
      * 5H LPDMB ,13,4X,5H KALCP ,13)      MARO 205
54     GO TO 1300      MARO 206
55     80 CONTINUE      MARO 207
56     IF(NTRAC.LT.-1) GO TO 160      MARO 208
57     WRITE(KW,90)(MASK(J),J=1,NV)      MARO 209
58     90 FORMAT(/10H MASK ,17,713/(4X,813))      MARO 210
59     WRITE(KW,100)(X(J),J=1,NV)      MARO 211
60     100 FORMAT(/10H X ,13,5/(10X,8E13.5))      MARO 212
61     WRITE(KW,110)(XMAX(J),J=1,NV)      MARO 213
62     110 FORMAT(/10H XMAX ,13,5/(10X,8E13.5))      MARO 214
63     WRITE(KW,120)(XMIN(J),J=1,NV)      MARO 215
64     120 FORMAT(/10H XMIN ,13,5/(10X,8E13.5))      MARO 216

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66 WRITE(KW,130) (DELHM(J),J=1,NV) MARO 232
67 130 FORMAT(/10H DELHM = ,E12.5/(10X,SE13.5)) MARO 233
68 WRITE(KW,140) NV,NPTS,LPDMS,LPDMS,NTRAC,METHOD,KALCP,KORDP, MARO 234
   * NPLAT,NFMAX,MAXIT,MXSUB,CRIT,RELPD,RELHM MARO 235
69 140 FORMAT(/7H NV = ,14,5X,7H NPTS = ,18,5X,8H LPDMS = ,18,5X, MARO 236
   * 8H LPDMS = ,14,5X,8H NTRAC = ,12,5X,8H METHOD = ,13,5X,8H KALCP = , MARO 237
   * 13/8H KORDP = ,12,5X,8H NPLAT = ,12,5X,8H NFMAX = ,17,5X, MARO 238
   * 8H MAXIT = ,15,5X,8H MXSUB = ,14/7H CRIT = ,E12.5,5X,8H RELPD = , MARO 239
   * E12.5,5X,8H RELHM = ,E12.5) MARO 240
70 150 JVAR=0 MARO 241
   C MARO 242
   C SET FMGN. IF NECESSARY, RESET FLAMB AND/OR FACCL. MARO 243
   C MARO 244
71 FMGN=RUNIT MARO 245
72 UPNU=FN0 MARO 246
73 DOWNU=FN0 MARO 247
74 IF (FLAMB.LE.0) FLAMB=FLDEF MARO 248
75 IF (METHOD.EQ.0) FLAMB=RZERO MARO 249
76 IF (METHOD.NE.1) FACCL=RUNIT MARO 250
   C MARO 251
   C COMPUTE THE INITIAL GOODNESS OF FIT OF THE MODEL TO THE DATA. MARO 252
   C CALL FUNC TO CALCULATE THE VECTOR OF FITTED VALUES. MARO 253
   C MARO 254
77 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 255
   C MARO 256
   C NF ... EQUIVALENT NUMBER OF CALLS TO FUNC MARO 257
78 NF=1 MARO 258
79 IF (INTRAC.GE.-1) WRITE(KW,160) PHI,FLAMB MARO 259
80 160 FORMAT(/27H PHI (THE SUM OF SQUARES) = ,E16.8,57X,8H LAMBDA = , MARO 260
   * E12.5//1H ) MARO 261
   C MARO 262
   C * * * * * MARO 263
   C BEGIN THE NEXT ITERATION. MARO 264
   C THIS IS THE ENTRY POINT AFTER A SUCCESSFUL STEP IF THE CONVERGENCE MARO 265
   C CRITERION IS NOT MET. MARO 267
   C MARO 268
81 170 JSUB=0 MARO 269
82 FCUT=RTWO MARO 270
83 ITER=ITER+1 MARO 271
84 IF (INTRAC.GE.1) WRITE(KW,180) ITER,FMGN,FLAMB MARO 272
85 180 FORMAT(/16H BEGIN ITERATION,18,44X,7H FMGN = ,E12.5,15X, MARO 273
   * 8H LAMBDA = ,E12.5) MARO 274
86 IF (INTRAC.GE.2) WRITE(KW,190) MARO 275
87 190 FORMAT(/28H P (THE JACOBIAN MATRIX) ...//1H ) MARO 276
   C MARO 277
   C INITIALIZE FOR THIS ITERATION. MARO 278
88 STFAC=RUNIT MARO 279
89 DO 200 JX=1,NACTV MARO 280
90 GRAD(JX)=RZERO MARO 281
91 DO 200 KX=1,JX MARO 282
92 200 ERR(JX,KX)=RZERO MARO 283
   C MARO 284
   C CALL DERIV (OR CALCO) TO COMPUTE THE JACOBIAN MATRIX. P. MARO 285
   C DERIV IS CALLED NPTS TIMES IF KALCP=1. MARO 286
   C MARO 287
93 SIG=YSIG(1) MARO 288
94 DO 270 JPT=1,NPTS MARO 289
95 KPT=JPT MARO 290
96 IF (KALCP.LT.0) GO TO 210 MARO 291

97 IF (JPT.NE.1) GO TO 230 MARO 292
98 KPT=1 MARO 293
99 IF (KORDP.LE.2) GO TO 220 MARO 294
100 CALL CALCO (JPT,P,LPDMS,LPDMS) MARO 295
101 GO TO 230 MARO 296
102 CALL DERIV (JPT,FUNK,NPTS,FIT,FITSV,P,LPDMS,LPDMS) MARO 297
103 CONTINUE MARO 298
104 IF (INTRAC.GE.3) WRITE(KW,240) JPT, (P(KPT,JX),JX=1,NACTV) MARO 299
105 240 FORMAT(1X,13,2X,SE16.7/(8X,SE16.7)) MARO 300
   C MARO 301
   C COMPUTE OSAY AND GRAD. MARO 302
   C OSAY, WHICH IS STORED IN ONE HALF OF THE ARRAY ERR(=,=), IS PT*P. MARO 303
   C GRAD(=) IS HALF THE GRADIENT OF PHI. MARO 304
   C MARO 305
106 IF (LEOU.EQ.0) SIG=YSIG(JPT) MARO 306
107 RTERM=(FIT(JPT)-P(JPT))/SIG**2 MARO 307
108 DO 250 JX=1,NACTV MARO 308
109 GRAD(JX)=GRAD(JX)+P(KPT,JX)*RTERM MARO 309
110 PTERM=P(KPT,JX)/SIG**2 MARO 310
111 DO 250 KX=1,JX MARO 311
112 250 ERR(JX,KX)=ERR(JX,KX)+P(KPT,KX)*PTERM MARO 312
113 CONTINUE MARO 313
114 270 CONTINUE MARO 314
   C MARO 315
   C RESTORE FIT IF IT WAS DESTROYED IN DERIV. MARO 316
115 IF (KORDP.NE.2) GO TO 280 MARO 316
116 IF (KALCP.NE.0) GO TO 280 MARO 317
117 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 318
118 NF=NF+1 MARO 319
119 280 NF=NF+NACTV MARO 320
120 280 NF=NF+NACTV MARO 321
   C MARO 322
   C COMPUTE THE SCALE FACTORS AND STORE THEM IN DELTX(=). SCALE GRAD. MARO 323
   C MARO 324
121 DO 300 JX=1,NACTV MARO 325
122 SCALJ=OSORT(ERR(JX,JX)) MARO 326
123 IF (SCALJ.EQ.RZERO) SCALJ=RUNIT MARO 327
124 DELTX(JX)=SCALJ MARO 328
125 300 GRAD(JX)=GRAD(JX)/SCALJ MARO 329
126 IF (INTRAC.GE.1) WRITE(KW,310) (GRAD(JX),JX=1,NACTV) MARO 330
127 310 FORMAT(/21H SCALED GRADIENT = ,E16.7/(21X,SE16.7)) MARO 331
   C MARO 332
   C SCALE OSAY. THE DIAGONAL ELEMENTS OF OSAY ARE SCALED TO UNITY. MARO 333
   C MARO 334
128 DO 355 JX=1,NACTV MARO 335
129 DO 350 KX=1,JX MARO 336
130 SA=ERR(JX,KX)/(DELTX(JX)*DELTX(KX)) MARO 337
131 IF (KX.NE.JX) GO TO 320 MARO 338
132 IF (SA.EQ.RZERO) GO TO 330 MARO 339
133 SA=RUNIT MARO 340
134 GO TO 350 MARO 341
135 320 IF (OABS(SA).LT.RUNIT-RTOL) GO TO 380 MARO 342
136 CONTINUE MARO 343
137 IF (INTRAC.GE.-2) WRITE(KW,340) JX,KX,SA,ITER MARO 344
138 340 FORMAT(28H ***** POSSIBLY DANGEROUS VALUE OF MARO 345
   * 18H COEFFICIENT .....EX,8H OSAY(,13,1H,,13,3H) = ,E16.7,8X, MARO 346
   * 10H ITERATION,15) MARO 347
139 350 ERR(JX,KX)=SA MARO 348
140 CONTINUE MARO 349
141 IF (INTRAC.LT.2) GO TO 360 MARO 349
142 WRITE(KW,360) MARO 350

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143 380 FORMAT(/48H OSAY (PT=P, SCALED, WHERE P IS THE JACOBIAN).../1M ) MARO 361
144 DD 370 JX=1,NACTV MARO 362
145 378 WRITE(KW,240)JX,(ERR(JX,KX),KX=1,JX) MARO 363
146 380 DD 380 JX=1,NV MARO 364
147 380 XSAVE(JX)=X(JX) MARO 365
C INITIALIZE MASK AND NACT. MARO 366
148 400 NACT=NACTV MARO 367
149 DD 410 JX=1,NV MARO 368
150 410 MASK(JX)=MASK(JX) MARO 369
C COPY OSAY INTO O AND GRAD INTO H, AND SET THE DIAGONAL ELEMENTS OF O. MARO 361
C THIS IS THE ENTRY POINT FOR SUBITERATIONS IN WHICH FLAME IS MARO 362
C INCREASED OR CONSTRAINTS ARE IMPOSED. MARO 363
151 420 KRANK=O MARO 364
152 JO=O MARO 365
153 JT=O MARO 366
154 DD 430 JX=1,NV MARO 367
155 IF(MASK(JX).NE.O) GO TO 430 MARO 368
156 JO=JO+1 MARO 369
157 IF(MASK(JX).NE.O) GO TO 430 MARO 370
158 JT=JT+1 MARO 371
159 H(JT)=GRAD(JO) MARO 372
160 KO=O MARO 373
161 KT=O MARO 374
162 DD 440 KX=1,JX MARO 375
163 IF(MASK(KX).NE.O) GO TO 440 MARO 376
164 KO=KO+1 MARO 377
165 IF(MASK(KX).NE.O) GO TO 440 MARO 378
166 KT=KT+1 MARO 379
167 SA=ERR(JO,KO) MARO 380
168 IF(KX.NE.JX OR SA.EQ.RZERO) GO TO 430 MARO 381
169 SA=RUNIT+FLAMB MARO 382
170 KRANK=KRANK+1 MARO 383
171 430 ERR(KT,JT+1)=SA MARO 384
172 440 CONTINUE MARO 385
173 450 CONTINUE MARO 386
C SOLVE THE NORMAL EQUATIONS FOR H, THE CORRECTION VECTOR. MARO 387
C MARO 388
174 NSMAL=O MARO 389
175 NMU=NACT-1 MARO 390
176 IF(NMU.EQ.O) GO TO 490 MARO 391
C REDUCE THE SYSTEM TO TRIANGULAR FORM. MARO 392
C UTILIZING THE SYMMETRY OF THE MATRIX. MARO 393
177 DD 460 J=1,NMU MARO 394
178 PIVOT=ERR(J,J+1) MARO 395
179 IF(PIVOT.EQ.RZERO) GO TO 460 MARO 396
180 JPU=J+1 MARO 397
181 DD 470 K=JPU,NACT MARO 398
182 EM=ERR(J,K+1)/PIVOT MARO 399
183 IF(EM.EQ.RZERO) GO TO 470 MARO 400
184 DD 480 L=K,NACT MARO 401
185 ERR(K,L+1)=ERR(K,L+1)-ERR(J,L+1)*EM MARO 402
186 H(K)=H(K)-H(J)*EM MARO 403
187 480 CONTINUE MARO 404
C DO THE BACK SOLUTION. MARO 405
188 490 DD 520 JINV=1,NACT MARO 406
189 J=(NACT+1)-JINV MARO 407
C MARO 408
190 PIVOT=ERR(J,J+1) MARO 411
191 IF(PIVOT.LE.RZERO) NSMAL=NSMAL+1 MARO 412
192 IF(PIVOT.NE.RZERO) GO TO 500 MARO 413
193 H(J)=RZERO MARO 414
194 GO TO 520 MARO 415
195 500 SUM=RZERO MARO 416
196 IF(J.EQ.NACT) GO TO 520 MARO 417
197 JPU=J+1 MARO 418
198 DD 510 K=JPU,NACT MARO 419
199 SUM=SUM+ERR(J,K+1)*H(K) MARO 420
200 H(J)=(H(J)-SUM)/PIVOT MARO 421
201 530 CONTINUE MARO 422
C IF THE COEFFICIENT MATRIX WAS RANK DEFICIENT, PRINT A MESSAGE. MARO 423
C MARO 424
202 MRANK=NACT-NSMAL MARO 425
203 IF(MRANK.EQ.NACT) GO TO 560 MARO 426
204 COSIN=HUGE MARO 427
205 IF(INTRAC.GE -2) WRITE(KW,540)MRANK,NACT,ITER MARO 428
206 540 FORMAT(/41H RANK-DEFICIENT NORMAL EQUATIONS IN MARO ,5X,7H RANK , MARO 429
207 + I4,7X,15H ORDER OF MATRIX ,I4,5X,10H ITERATION,15) MARO 430
208 IF(MRANK.GT.O) GO TO 560 MARO 431
209 KFLAG=-4 MARO 432
210 GO TO 1200 MARO 433
560 IF(METHD.GT.O .AND. MRANK.LT.KRANK) GO TO 880 MARO 434
C UNPACK AND DE-SCALE THE CORRECTION VECTOR H. MARO 435
C COMPUTE THE INNER PRODUCTS SA, SB, AND SC. MARO 436
C MARO 437
211 580 SA=RZERO MARO 438
212 SB=RZERO MARO 439
213 SC=RZERO MARO 440
214 KI=NV MARO 441
215 KO=NACTV MARO 442
216 KY=NACT MARO 443
217 DD 590 JX=1,NV MARO 444
218 H=RZERO MARO 445
219 IF(MASK(KX).NE.O) GO TO 580 MARO 446
220 IF(MASK(KX).NE.O) GO TO 570 MARO 447
221 H=H(KT) MARO 448
222 SA=SA+H*GRAD(KO) MARO 449
223 SB=SB+H*H MARO 450
224 SC=SC+GRAD(KO)**2 MARO 451
225 H=H*FMGN/DELTA(KO) MARO 452
226 KT=KT+1 MARO 453
227 KO=KO+1 MARO 454
228 570 H(KX)=H MARO 455
229 580 KX=KX+1 MARO 456
C ADD THE CORRECTION VECTOR TO THE PARAMETER VECTOR AND MARO 457
C CHECK FOR CONSTRAINT VIOLATIONS. MARO 458
C THIS IS THE ENTRY POINT FOLLOWING A CUTSTEP. MARO 459
C MARO 460
230 600 CONTINUE MARO 461
231 IF(NTRAC.GE 1) WRITE(KW,610)(H(JX),JX=1,NV) MARO 462
232 610 FORMAT(/7X,14H CORRECTION = ,8E16.7/(21X,8E16.7)) MARO 463
233 NACT=NACTV MARO 464
234 FRMIN=RUNIT MARO 465
235 NLOOP=O MARO 466
236 JXLIM=O MARO 467

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237      820 DD 720 JX=1,MV
238          IF(MASK(JX).NE.0) GO TO 720
239          XSAV=XSAVE(JX)
240          XMX=XMX(JX)
241          XMN=XMN(JX)
242          MH=H(JX)
243          IF((XSAV.LT.XMX .OR. MH.LE.RZERO) .AND
244             (XSAV.GT.XMN .OR. MH.GE.RZERO)) GO TO 840
245          MASK(JX)=1
246          NACT=NACT-1
247          X(JX)=XSAV
248          IF(INTRAC.GE.-1) WRITE(KW,830)JX,XSAV,ITER
249          FORMAT(/5H FIX X(,13,4H) = ,E12.5,22H TEMPORARILY. TO AVOID,
250             * 24H VIOLATING A CONSTRAINT.,25X,10H ITERATION,15)
251          GO TO 720
252          840 XLIM=XSAV+MH*FRMIN
253          IF(JX.NE.JXLIM) GO TO 850
254          IF(KBND)880,880,880
255          X(JX)=XLIM
256          IF(XLIM.LE.XMX) GO TO 870
257          X(JX)=XMX
258          JEND=1
259          GO TO 880
260          870 IF(XLIM.GE.XMN) GO TO 720
261          X(JX)=XMN
262          JEND=-1
263          IF(JX.NE.JXLIM) GO TO 710
264          IF(INTRAC.LT.-1) GO TO 720
265          WRITE(KW,700)JX,X(JX),FRMIN,ITER
266          FORMAT(/25H CONSTRAINT VIOLATED BY X(,13,
267             * 20H) VALUE RESET TO ,E15.8,24H USING CUTSTEP FACTOR = ,E12.5,
268             * 3X,5H ITER.,15)
269          GO TO 720
270          710 IF(NLOOP.NE.0) GO TO 720
271          DENOM=XLIM-XSAV
272          IF(DENOM.EQ.RZERO) GO TO 720
273          FRAC=(X(JX)-XSAV)/DENOM
274          IF(FRAC.GE.FRMIN) GO TO 720
275          FRMIN=FRAC
276          JXLIM=JX
277          KEND=JEND
278          CONTINUE
279          720 CONTINUE
280
281          C
282          C IF THE PROPOSED STEP WOULD VIOLATE ANY ALREADY ACTIVE CONSTRAINTS,
283          C FIX THOSE COMPONENTS OF H EQUAL TO ZERO AND RECOMPUTE THE
284          C OTHER COMPONENTS.
285          C
286          IF(NACT.GT.0) GO TO 740
287          KFLAG=3
288          IF(INTRAC.LT.-2) GO TO 1200
289          WRITE(KW,730)
290          730 FORMAT(///47H APPARENT CONSTRAINED OPTIMUM LIES IN A CORNER.)
291          GO TO 1200
292          740 IF(NACT.LT.NACTSV) GO TO 420
293          IF(NLOOP.NE.0) GO TO 780
294          WLOOP=1
295          IF(XLIM.NE.0) GO TO 820
296          750 CONTINUE
297          IF(INTRAC.GE.1) WRITE(KW,760)(X(JX),JX=1,MV)
298          760 FORMAT(/16X,5H X = ,8E15.7/(21X,5E15.7))
299
300          C
301          C CALCULATE THE NEW FITTED VALUES.
302          C
303          CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHNEW)
304          PHNF=1
305          IF(PHNEW-PHI)820,770,790
306
307          C
308          C THE NEW VALUE OF PHI IS EXACTLY EQUAL TO THE OLD VALUE.
309          C CHECK FOR CONVERGENCE UNDER THE NPLAT OPTION.
310          C
311          770 IF(NFLAT.EQ.0) GO TO 830
312          KFLAG=2
313          IF(INTRAC.LT.-1) GO TO 830
314          WRITE(KW,780)
315          780 FORMAT(/145H CONVERGENCE ACHIEVED UNDER THE NPLAT OPTION.)
316          GO TO 830
317
318          C
319          C THE NEW VALUE OF PHI IS GREATER THAN THE OLD VALUE.
320          C
321          790 CONTINUE
322          IF(INTRAC.GE.1) WRITE(KW,800)PHI,PHNEW
323          800 FORMAT(/32X,10H OLD PHI =,E15.8,5X,10H NEW PHI =,E15.8)
324
325          C
326          C CHECK WHETHER JSUB HAS EXCEEDED MXSUB.
327          C
328          JSUB=JSUB+1
329          IF(JSUB.GT.MXSUB) GO TO 810
330          IF(METHD)880,1090,880
331          810 KFLAG=-1
332          IF(INTRAC.GE.-1) WRITE(KW,820)MXSUB
333          820 FORMAT(/43X EXCEEDED MAXIMUM NUMBER OF SUBITERATIONS =,13,
334             * 5H IN MARO.)
335          RESTORE X TO THE BASE POINT.
336          830 DD 840 JX=1,MV
337          840 X(JX)=XSAVE(JX)
338          CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI)
339          GO TO 1200
340
341          C
342          C THE NEW FIT IS WORSE THAN THE OLD FIT. COMPUTE COSIN, THE COSINE
343          C OF THE ANGLE BETWEEN THE SCALED GRADIENT AND THE SCALED CORRECTION
344          C VECTOR.
345          C
346          850 DENOM=SB*EC
347          IF(DENOM.LE.RZERO) GO TO 860
348          COSIN=SA/OSORT(DENOM)
349          IF(COSIN.GT.CRIT) GO TO 880
350
351          C
352          C COSIN IS NOT GREATER THAN CRIT. INCREASE THE VALUE OF LAMBDA.
353          C
354          860 UPFAC=UPNU
355          UPNU=OMIN1(UPNU*RTWO,FNU)
356          IF(METHD.EQ.1) UPFAC=OMIN1(UPFAC,FNULM*RUNIT/PLAMB)
357          FLAMB=FLAMB*UPFAC
358          IF(INTRAC.GE.1) WRITE(KW,870)JSUB,COSIN,FLAMB
359          870 FORMAT(/18H **** SUBITERATION,13,4X,17H INCREASE LAMBDA.,4X,
360             * 13H COS(GAMMA) =,E12.5,25X,5H LAMBDA =,E12.5)
361
362          C
363          C GO BACK AND FORM THE NORMAL EQUATIONS
364          C USING A LARGER VALUE OF LAMBDA.
365          C
366          GO TO 400
367
368          MARO 471
369          MARO 472
370          MARO 473
371          MARO 474
372          MARO 475
373          MARO 476
374          MARO 477
375          MARO 478
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479          MARO 580
480          MARO 581
481          MARO 582
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483          MARO 584
484          MARO 585
485          MARO 586
486          MARO 587
487          MARO 588
488          MARO 589
489          MARO 590

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C COSIN IS GREATER THAN CRIT. CUT THE MAGNITUDE OF THE STEP. H. MARO 581
C MARO 582
C MARO 583
321 880 STFAC=STFAC/FCUT MARO 584
322 IF(METHD.GE.0) GO TO 880 MARO 585
323 FMGN=FMGN/FCUT MARO 586
324 GO TO 800 MARO 587
325 890 IF(METHD.EQ.1) FLAMB=FLAMB*RTWO MARO 588
326 DO 910 JX=1,NV MARO 589
327 H(JX)=H(JX)-XSAVE(JX)/FCUT MARO 590
328 FCUT=FCUT*FAC1 MARO 591
329 IF(NTRAC.GE.1) WRITE(KW,920)JSUB,COSIN,STFAC MARO 592
330 920 FORMAT(/16H *** SUBITERATION,13.4X,16H TAKE CUT STEPS,.4X, MARO 593
" 13H COS(GAMMA) *.E12.5,5X,17H CUTSTEP FACTOR *.E12.5) MARO 594
C MARO 595
C GO BACK AND TRY A SMALLER CUTSTEP. MARO 596
331 GO TO 800 MARO 597
C MARO 598
C THE VALUE OF PHI HAS DECREASED. TRY A HALF STEP. MARO 599
C MARO 600
C MARO 601
332 930 IF(METHD.EQ.0 .OR. METHD.EQ.2) GO TO 1080 MARO 611
333 DO 940 JX=1,NV MARO 612
334 XTEMP(JX)=X(JX) MARO 613
335 IF(MASK(JX).NE.0) GO TO 840 MARO 614
336 X(JX)+XSAVE(JX)+X(JX)-XSAVE(JX)/RTWO MARO 615
337 X(JX)+OMAX1(XMIN(JX),OMINI(XMAX(JX),X(JX))) MARO 616
338 CONTINUE MARO 617
339 DO 950 JPT=1,NPTS MARO 618
340 FITSV(JPT)=FIT(JPT) MARO 619
341 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHALF) MARO 620
342 NF=NF+1 MARO 621
C MARO 622
C USE QUADRATIC INTERPOLATION. IN ORDER TO TRY TO REFINE THE MARO 623
C POSITION OF THE MINIMUM OF PHI. MARO 624
C MARO 625
343 RLFAC=RUNIT MARO 626
344 DENOM=RTWO*(PHNEW-PHALF)-(PHALF-PHI) MARO 627
345 STFAC=RZERO MARO 628
346 IF(DENOM.LE.RZERO) GO TO 860 MARO 629
347 STFAC=(PHI-PHNEW)/DENOM MARO 630
348 RSPAC=(RUNIT-STFAC)/RTWO MARO 631
C MARO 632
C DO NOT EXTRAPOLATE. MARO 633
349 IF(STFAC.GE.RUNIT) STFAC=RZERO MARO 634
350 DO 870 JX=1,NV MARO 635
351 H(JX)=X(JX) MARO 636
352 X(JX)+X(JX)+XTEMP(JX)-X(JX))*STFAC MARO 637
353 IF(PHALF.GE.PHNEW) GO TO 1010 MARO 638
354 RLFAC=RUNIT/RTWO MARO 639
355 JSUB=JSUB+1 MARO 640
356 DO 880 JX=1,NV MARO 641
357 XTEMP(JX)=H(JX) MARO 642
358 DO 890 JPT=1,NPTS MARO 643
359 FITSV(JPT)=FIT(JPT) MARO 644
360 IF(NTRAC.GE.1) WRITE(KW,1000)PHNEW,PHALF MARO 645
361 1000 FORMAT(/21H HALF STEP SUCCEEDED.,15X,8H PHNEW *.E15.8,18X, MARO 646
" 8H PHALF *.E15.8) MARO 647
362 PHNEW=PHALF MARO 648
363 1010 IF(STFAC.EQ.RZERO) GO TO 1020 MARO 649
364 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 650
C MARO 651
365 NF=NF+1 MARO 652
366 IF(PHI.LT.PHNEW) GO TO 1060 MARO 653
367 DO 1030 JX=1,NV MARO 654
368 X(JX)=XTEMP(JX) MARO 655
369 DO 1040 JPT=1,NPTS MARO 656
370 FIT(JPT)=FITSV(JPT) MARO 657
371 IF(STFAC.EQ.RZERO) GO TO 1080 MARO 658
372 IF(NTRAC.LT.1) GO TO 1080 MARO 659
373 WRITE(KW,1050)RLFAC,PHI MARO 660
374 1050 FORMAT(/25H QUADRATIC INTERPOLATION .22X,8H RSPAC *.E12.8,12X, MARO 661
" 8H PHI *.E15.8) MARO 662
375 GO TO 1080 MARO 663
376 1080 RLFAC=RLFAC MARO 664
377 PHNEW=PHI MARO 665
378 IF(NTRAC.GE.1) WRITE(KW,1070)RLFAC,PHI MARO 666
379 1070 FORMAT(/35H QUADRATIC INTERPOLATION SUCCEEDED.,12X,8H RLFAC *. MARO 667
" .E12.8,12X,8H PHI *.E15.8) MARO 668
380 1090 IF(RLFAC.LE.RZERO) GO TO 1090 MARO 669
381 FLAMB=FLAMB/RLFAC MARO 670
382 IF(METHD.LT.0) FMGN=FMGN/RLFAC MARO 671
C MARO 672
C THE STEP IS ACCEPTED. TEST FOR CONVERGENCE IF NO CONSTRAINT MARO 673
C BECAME ACTIVE DURING THIS ITERATION. MARO 674
C MARO 675
383 1080 CONTINUE MARO 676
384 IF(NTRAC.GE.1) WRITE(KW,1100)ITER,PHNEW MARO 677
385 1100 FORMAT(/16H END ITERATION,15.56X,8H PHI *.E15.8) MARO 678
386 PHI=PHNEW MARO 679
387 IF(XMIN.EQ.0) GO TO 1130 MARO 680
388 DO 1110 JX=1,NV MARO 681
389 IF(MASK(JX).NE.0) GO TO 1110 MARO 682
390 IF(OABS(X(JX)-XSAVE(JX)).GT.DELMN(JX)) GO TO 1130 MARO 683
391 CONTINUE MARO 684
392 EFLAG=1 MARO 685
393 IF(NTRAC.LT.-1) GO TO 1200 MARO 686
394 WRITE(KW,1120) MARO 687
395 1120 FORMAT(/38H CONVERGED WHEN THE STEP BECAME SMALL.) MARO 688
396 GO TO 1200 MARO 689
C MARO 690
C THE ITERATION HAS NOT YET CONVERGED. MARO 691
C MARO 692
397 1130 IF(ITER.LT.MAXIT) GO TO 1180 MARO 693
398 KFLAG=8 MARO 694
399 WRITE(KW,1140)MAXIT MARO 695
400 1140 FORMAT(/46H MAXIMUM NUMBER OF ITERATIONS REACHED IN MARO.,5X, MARO 696
" 8H MAXIT *.15) MARO 697
401 GO TO 1200 MARO 698
C MARO 699
C IF SUBITERATIONS WERE NOT PERFORMED THIS ITERATION. DECREASE LAMBDA. MARO 700
C MARO 701
402 1150 IF(NF.GE.NPMMAX) GO TO 1180 MARO 702
403 IF(JSUB.GT.0) GO TO 1160 MARO 703
404 FMGN=OMINI(FMGN*RTWO,RUNIT) MARO 704
405 SCAL=ORUNIT*FLAMB MARO 705
406 IF(SCAL.GT.RUNIT) FLAMB=FLAMB/ODWNU MARO 706
407 UPNU=ODWNU MARO 707
408 DDWNU=OMINI(DDWNU*RTWO,PNU) MARO 708
409 GO TO 1170 MARO 709
410 1160 IF(METHD.NE.1) GO TO 1170 MARO 708
411 UPNU=PHALF MARO 710

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412      DOWNU=FNULM      MARQ 711
413      1170 CONTINUE      MARQ 712
C      GO BACK AND DO ANOTHER ITERATION.      MARQ 713
414      GO TO 170      MARQ 714
415      1180 KFLAG=-7      MARQ 715
416      WRITE(KW,1190)NPMAX      MARQ 716
417      1190 FORMAT(//23H NF HAS REACHED NPMAX *,17,9H IN MARQ.)      MARQ 717
C      * * * * *      MARQ 718
C      * * * * *      MARQ 719
C      * * * * *      MARQ 720
C      THE ITERATION HAS TERMINATED.      MARQ 721
C      PRINT OUT THE DATA, FITTED VALUES, AND RESIDUALS.      MARQ 722
C      COMPUTE AND PRINT THE STANDARD DEVIATION OF THE DATA FROM THE FIT.      MARQ 723
C      * * * * *      MARQ 724
418      1200 CONTINUE      MARQ 725
419      SC=OSORT(SC)      MARQ 726
420      IF(NTRAC.LT.-1) GO TO 1290      MARQ 727
421      WRITE(KW,1210)ITER,NF,PHI,FMGN,FLAMB,SC      MARQ 728
422      1210 FORMAT(//14X,11H ITERATIONS,7X,5H NF *,15,9X,5H PHI *,E12.5,10X,      MARQ 729
      * 7H FMGN *,E12.5,7X,5H LAMBDA *,E12.5//9X,15H NORM OF SCALED,      MARQ 730
      * 18H GRADIENT VECTOR *,E12.5)      MARQ 731
423      WRITE(KW,760)(X(JK),JK=1,NV)      MARQ 732
424      IF(NTRAC.GE.0) WRITE(KW,1220)      MARQ 733
425      1220 FORMAT(//14X,14H,5X,5H Y(J),14X,7H FIT(J),10X,      MARQ 734
      * 12H Y(J)-FIT(J),7X,5H YSIG(J),11X,13H (Y-FIT)/YSIG(1H)      MARQ 735
426      SIG=YSIG(1)      MARQ 736
427      RMSDV=RZERO      MARQ 737
428      SDVMX=RZERO      MARQ 738
429      DO 1240 JPT=1,NPTS      MARQ 739
430      * IF(LEOU.EQ.0) SIG=YSIG(JPT)      MARQ 740
431      * YV=Y(JPT)      MARQ 741
432      * PTERM=YV-FIT(JPT)      MARQ 742
433      * RTERM=PTERM/SIG      MARQ 743
434      IF(NTRAC.GE.0) WRITE(KW,1230)JPT,YV,FIT(JPT),PTERM,SIG,RTERM      MARQ 744
435      1230 FORMAT(//14X,11X,5X,5H Y,5X,5H FIT,5X,5H SIG,5X,5H RTERM,5X,5H Y,5X,5H FIT,5X,5H SIG,5X,5H RTERM)      MARQ 745
436      RMSDV=RMSDV+RTERM**2      MARQ 746
437      1240 SDVMX=OMAX(1,SDVMX,ABS(RTERM))      MARQ 747
438      DENOM=NPTS-NACTV      MARQ 748
439      WRITE(KW,1250)DENOM      MARQ 749
440      1250 FORMAT(//23H NUMBER OF DEGREES OF FREEDOM *,E12.5)      MARQ 750
441      IF(DENOM.LE.RZERO) GO TO 1270      MARQ 751
442      RMSDV=OSORT(RMSDV/DENOM)      MARQ 752
443      WRITE(KW,1260)RMSDV      MARQ 753
444      1260 FORMAT(//43H R.M.S. SCALED DEVIATION OF DATA FROM FIT *,E12.5)      MARQ 754
445      1270 CONTINUE      MARQ 755
446      WRITE(KW,1280)SDVMX      MARQ 756
447      1280 FORMAT(//27H MAXIMUM SCALED DEVIATION *,E12.5)      MARQ 757
C      * * * * *      MARQ 758
C      CALL FUNC TO SET THE FINAL VALUES.      MARQ 759
C      * * * * *      MARQ 760
448      1290 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI)      MARQ 761
449      FDBJ=PHI      MARQ 762
C      * * * * *      MARQ 763
C      CALL MOERR TO PRINT THE PARAMETER ERRORS AND CORRELATIONS.      MARQ 764
C      A DUMMY ROUTINE MAY BE SUBSTITUTED FOR MOERR IF THESE ARE NOT NEEDED.      MARQ 765
C      * * * * *      MARQ 766
450      IF(MATRX.EQ.0) RETURN      MARQ 767
451      CALL MOERR (NACTV,NPTS)      MARQ 768
C      * * * * *      MARQ 769
452      1300 RETURN      MARQ 770

C      * * * * *      MARQ 771
453      END MARQ.      MARQ 772
C      * * * * *      MARQ 773

454      SUBROUTINE FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI)      FUNC 1
C      * * * * *      FUNC 2
C      UPDATED BY J. CHANDLER, OSU DEPARTMENT OF COMPUTING AND      FUNC 2
C      INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES, MAY 1981      FUNC 2
C      * * * * *      FUNC 2
C      FUNC CALLS FUNK OR POPX TO COMPUTE THE ARRAY OF FITTED VALUES FITH.      FUNC 3
C      * * * * *      FUNC 4
455      DOUBLE PRECISION Y,YSIG,XMAX,XMIN,DELTX,DELMN,ERR,FDBJ,      FUNC 5
      * FLAMB,FNU,RELDF,RELNM      FUNC 6
456      DOUBLE PRECISION X,FIT,F,PHI,SIG      FUNC 7
C      * * * * *      FUNC 8
457      DIMENSION Y(1),YSIG(1),FIT(1)      FUNC 9
C      * * * * *      FUNC 10
458      COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),      FUNC 11
      * ERR(20),FDBJ,NV,NTRAC,MATRX,MAXX(20),      FUNC 12
      * NPMAX,NPLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW      FUNC 13
459      COMMON /NLSA/ FLAMB,FNU,RELDF,RELNM,METHD,KALCP,KORDF,MAXIT,      FUNC 14
      * LEOU,MXSUB,MXUPD      FUNC 15
C      * * * * *      FUNC 16
460      RZERO=0.      FUNC 16
461      IF(KALCP.NE.0) GO TO 10      FUNC 17
C      * * * * *      FUNC 18
462      CALL FUNK (FIT)      FUNC 18
463      GO TO 30      FUNC 19
C      * * * * *      FUNC 20
464      10 DO 20 JPT=1,NPTS      FUNC 22
465      * CALL POPX(JPT,NV,X,F)      FUNC 23
466      * FIT(JPT)=F      FUNC 24
C      * * * * *      FUNC 25
467      30 PHI=RZERO      FUNC 26
468      SIG=YSIG(1)      FUNC 27
469      DO 50 JPT=1,NPTS      FUNC 28
470      * IF(LEOU.EQ.0) SIG=YSIG(JPT)      FUNC 30
C      * * * * *      FUNC 31
C      * * * * *      FUNC 32
471      IF(SIG.GT.RZERO) CHECK FOR AN ILLEGAL VALUE OF SIG.      FUNC 32
472      * WRITE(KW,40)LEOU,JPT,SIG      FUNC 33
473      40 FORMAT(//26H ERROR IN MARQ. .... LEOU = *,11,5X,5H JPT = *,15,5X,      FUNC 34
      * 7H YSIG = *,E12.5,14H IS *.LE. ZERO.)      FUNC 35
474      STOP      FUNC 36
C      * * * * *      FUNC 37
475      50 PHI=PHI+((FIT(JPT)-Y(JPT))/SIG)**2      FUNC 38
C      * * * * *      FUNC 39
476      RETURN      FUNC 40
C      * * * * *      FUNC 41
477      END FUNC.      FUNC 42
C      * * * * *      FUNC 43

478      SUBROUTINE CALCD (JPT,P,LPDMA,LPDMB)      CALCDUM1
C      * * * * *      CALCDUM2
C      UPDATE BY J. CHANDLER, MAY 1981, OSU COMPUTER SCIENCE      CALCDUM2
C      DEPARTMENT--J. HANSON, UCC USER SERVICES      CALCDUM2
C      * * * * *      CALCDUM2
C      THIS IS A DUMMY VERSION OF SUBROUTINE CALCD.      CALCDUM3
C      A NON-DUMMY VERSION OF CALCD MAY BE USED (OPTIONALLY) TO SUPPLY      CALCDUM4
C      TO MARQ ANALYTIC VALUES OF THE ELEMENTS OF THE JACOBIAN MATRIX,      CALCDUM5
C      INSTEAD OF APPROXIMATING THEM BY FINITE DIFFERENCES.      CALCDUM6
C      HOWEVER, MOST USERS PREFER TO USE FINITE DIFFERENCES.      CALCDUM7

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C
478 DOUBLE PRECISION P
480 DIMENSION P(LPOMA,LPDMS)
481 RETURN
482 END
CALCDUM8
CALCDUM8
CALCDU10
CALCDU11
CALCDU12

483 SUBROUTINE DERIV (JPT,FUNK,NPTS,FIT,FITSV,P,LPOMA,LPDMS)
C
C UPDATED BY J. CHANDLER, OSU DEPARTMENT OF COMPUTING AND
C INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES
C
C DERIV 4.1 A.N.S.I. STANDARD FORTRAN MAY 1961
C
C DERIV COMPUTES THE JACOBIAN MATRIX P USING FINITE DIFFERENCES.
C
C P(J,K) IS THE PARTIAL DERIVATIVE OF FIT(J) WITH RESPECT TO X(K).
C IF KORDF.EQ.1, DERIV USES A NONCENTRAL DIFFERENCE FORMULA.
C IF KORDF.EQ.2, DERIV USES A CENTRAL DIFFERENCE FORMULA.
C KORDF.EQ.1 IS ABOUT TWICE AS FAST AS KORDF.EQ.2, BUT LESS ACCURATE.
C
484 DOUBLE PRECISION P,XMAX,XMIN,DELTX,DELMN,ERR,FOBJ,
485 FLAMB,FNU,RELOP,RELMM,RZERO
486 DOUBLE PRECISION X,FIT,FITSV,DEL,TWODDL,XSAVE,FXO,FXI
487 DIMENSION FIT(1),FITSV(1),P(LPOMA,LPDMS)
488 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
489 ERR(20,21),FOBJ,NV,NTRAC,MATRX,MASK(20),
490 NFMAR,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW
491 COMMON /M154/ FLAMB,FNU,RELOP,RELMM,METHD,KALCP,KORDF,MAXIT,
492 LEQU,MXSUB,MXUPD
493 RZERO=0.
494 JVARY=0
C
C SAVE FIT IF KALCP.GE.0
C
491 IF(KALCP.LT.0) GO TO 20
492 DO 10 J=1,NPTS
493 FIT(J)=FIT(J)
C
C LOOP OVER THE ACTIVE PARAMETERS X(JX).
C
494 DO 20 KX=0
495 DO 150 JX=1,NV
496 IF(MASK(JX).NE.0) GO TO 150
497 KX=KX+1
498 DEL=RELOP*X(JX)
499 IF(DEL.EQ.RZERO) DEL=RELOP
500 XSAVE=X(JX)
501 X(JX)=XSAVE+DEL
502 TWODDL=DEL+DEL
503 IF(KALCP)110,30,80
C
C KALCP.EQ.0 COMPUTE P, ONE COLUMN AT A TIME.
C
504 DO 30 J=1,NPTS
505 IF(KORDF.EQ.2) GO TO 80
506 DO 40 JX=1,NPTS
507 P(J,KX)=(FIT(J)-FITSV(J))/DEL
C
C
508 GO TO 140
C
C KALCP.EQ.0 AND KORDF.EQ.2 IN THIS CASE, THE INPUT VALUES OF
C FIT(J) WILL BE DESTROYED.
C
508 DO 50 JX=1,NPTS
509 DO 50 J=1,NPTS
510 FITSV(J)=FIT(J)
511 DO 50 JX=1,NPTS
512 JVARY=JX
513 CALL FUNK (FIT)
514 JVARY=0
515 DO 70 J=1,NPTS
516 P(J,KX)=(FITSV(J)-FIT(J))/TWODDL
517 GO TO 140
C
C KALCP.GT.0 COMPUTE P, ONE ELEMENT AT A TIME.
C
518 DO 80 J=1,NPTS
519 CALL POPX (J,NV,X,FXI)
520 IF(KORDF.EQ.2) GO TO 80
521 P(J,KX)=(FXI-FITSV(J))/DEL
522 GO TO 100
523 DO 90 JX=1,NPTS
524 CALL POPX (J,NV,X,FXO)
525 P(J,KX)=(FXI-FXO)/TWODDL
526 X(JX)=XSAVE+DEL
527 CONTINUE
528 GO TO 140
C
C KALCP.LT.0 COMPUTE ONE ROW OF P, ONE ELEMENT AT A TIME.
C
529 DO 110 J=1,NPTS
530 CALL POPX (JPT,NV,X,FXI)
531 IF(KORDF.EQ.2) GO TO 120
532 P(J,KX)=(FXI-FITSV(J))/DEL
533 GO TO 130
534 DO 120 JX=1,NPTS
535 CALL POPX (JPT,NV,X,FXO)
536 P(J,KX)=(FXI-FXO)/TWODDL
537 FIT(JPT)=FITSV(J)
C
C RESTORE X(JX).
538 DO 140 JX=1,NPTS
539 X(JX)=XSAVE
540 CONTINUE
C
540 IF(KALCP.LT.0) RETURN
541 DO 150 J=1,NPTS
542 FIT(J)=FITSV(J)
C
C RETURN
543 RETURN
544 END DERIV
545
546 SUBROUTINE MOERR (NACTV,NPTS)
C
C UPDATED BY J. CHANDLER, OSU DEPARTMENT OF COMPUTING AND
C INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES
C
C MOERR 3.0 A.N.S.I. STANDARD FORTRAN MAY 1961
C
C MOERR IS CALLED BY MARG TO COMPUTE AND PRINT APPROXIMATE VALUES OF

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C THE PARAMETER ERRORS AND CORRELATIONS. MOERR 6
C MOERR 7
C FOR THE MEANING OF THE -MAXIMUM VARIANCE INFLATION FACTOR- BELOW. MOERR 8
C SEE... D. W. MARQUARDT AND R. D. SNEE. MOERR 9
C RIDGE REGRESSION IN PRACTICE. MOERR 10
C THE AMERICAN STATISTICIAN 28 (1975) 3-20 MOERR 11
C INPUT QUANTITIES..... KW,ERR(*,*),NACTV,DELTX(*),NPTS,NV,NTRAC. MOERR 13
C MASK(*),FOBJ MOERR 14
C OUTPUT QUANTITIES..... ERR(*,*) MOERR 15
C MOERR 16
546 DOUBLE PRECISION N,SCALE,XMAX,XMIN,DELTX,DELMN,ERR,FOBJ, MOERR 18
C OSORT,ARG,RZERO,RUNIT,HUGE,PIVOT,O,VIFMX,ER,TEMP, MOERR 18
C DENOM,SCFAC,RESCL X MOERR 19
C MOERR 20
547 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20), MOERR 21
C ERR(20,21),FOBJ,NV,NTRAC,MATRX,MASK(20), MOERR 22
C NPMAX,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERPL,KW MOERR 23
C MOERR 24
548 OSORT(ARG)+OSORT(ARG) MOERR 25
C MOERR 26
C ..... MOERR 27
C MOERR 28
549 RZERO=0. MOERR 28
550 RUNIT=1. MOERR 30
551 HUGE=1.E30 MOERR 31
C PRINT OSAY. MOERR 32
552 IF(NTRAC.LT.-1) GO TO 40 MOERR 32
553 WRITE(KW,10) MOERR 33
554 10 FORMAT(///16H SUBROUTINE MOERR.//26H OSAY (PT=P, SCALED, WHERE, MOERR 35
C 23H P IS THE JACOBIAN).... MOERR 36
555 DO 30 JX=1,NACTV MOERR 37
556 WRITE(KW,20)JX,(ERR(JX,KV),KV=1,JX) MOERR 38
557 20 FORMAT(/1X,13,2X,6E15.7/(6X,6E15.7)) MOERR 39
558 30 CONTINUE MOERR 40
C MOERR 41
C COMPUTE THE SCALED ERROR MATRIX, WHICH IS THE INVERSE OF OSAY. MOERR 42
C INVERT OSAY USING THE GAUSS-JORDAN METHOD WITHOUT PIVOTING. MOERR 43
C F. L. BAUER AND C. REINSCH, P. 45 IN "LINEAR ALGEBRA" MOERR 44
C BY J. H. WILKINSON AND C. REINSCH (SPRINGER-VERLAG, 1971) MOERR 45
C ERR(*,NV+1) IS USED AS A SCRATCH VECTOR. MOERR 46
C MOERR 47
559 40 NVPLU=NV+1 MOERR 47
560 NSMAL=0 MOERR 48
561 DO 130 LINV=1,NACTV MOERR 50
562 L=(NACTV+1)-LINV MOERR 51
563 PIVOT=ERR(L,1) MOERR 52
564 IF(PIVOT.LE.RZERO) NSMAL=NSMAL+1 MOERR 53
565 IF(NACTV.LT.2) GO TO 90 MOERR 54
566 DO 80 K=2,NACTV MOERR 55
567 O=ERR(K,1) MOERR 56
568 IF(PIVOT.NE.RZERO) GO TO 60 MOERR 57
569 ERR(K,NVPLU)=RZERO MOERR 58
570 GO TO 70 MOERR 59
571 60 IF(K.GT.L) GO TO 60 MOERR 60
572 ERR(K,NVPLU)=O/PIVOT MOERR 61
573 GO TO 70 MOERR 62
574 80 ERR(K,NVPLU)=O/PIVOT MOERR 63
575 70 DO 80 M=2,K MOERR 64
576 ERR(K-1,M-1)=ERR(K,M)+O*ERR(M,NVPLU) MOERR 65
C MOERR 66
577 90 IF(PIVOT.NE.RZERO) GO TO 100 MOERR 66
578 ERR(NACTV,NACTV)=RZERO MOERR 67
579 GO TO 110 MOERR 68
580 100 ERR(NACTV,NACTV)=RUNIT/PIVOT MOERR 68
581 110 IF(NACTV.LT.2) GO TO 130 MOERR 70
582 DO 120 K=2,NACTV MOERR 71
583 ERR(NACTV,K-1)=ERR(K,NVPLU) MOERR 72
584 130 CONTINUE MOERR 73
C MOERR 74
585 NNRANK=NACTV-NSMAL MOERR 74
586 IF(NNRANK.LT.NACTV) WRITE(KW,140)NNRANK,NACTV MOERR 76
587 140 FORMAT(//51H THE SECOND DERIVATIVE MATRIX IS SINGULAR IN MOERR., MOERR 77
C 6X,7H NRANK =,13,7X,8H ORDER =,13//24H THEREFORE ALL PARAMETER, MOERR 78
C 21H ERRORS ARE INFINITE.) MOERR 79
C MOERR 80
C UNPACK THE ERROR MATRIX INTO THE UPPER MOERR 81
C TRIANGLE OF ERR(*,*), DE-SCALING IT. MOERR 82
C MOERR 83
588 JV=0 MOERR 83
589 VIFMX=RZERO MOERR 84
590 DO 180 JX=1,NV MOERR 84
591 IF(MASK(JX).EQ.0) JV=JV+1 MOERR 85
592 KV=0 MOERR 86
593 DO 180 KX=1,JX MOERR 87
594 ER=RZERO MOERR 88
595 IF(MASK(JX).NE.0 .OR. MASK(KX).NE.0) GO TO 160 MOERR 89
596 KV=KV+1 MOERR 91
597 TEMP=RZERO MOERR 92
598 DENOM=DELTX(JV)=DELTX(KV) MOERR 93
599 IF(DENOM.EQ.RZERO) GO TO 160 MOERR 94
600 TEMP=ERR(JV,KV) MOERR 95
601 ER=TEMP/DENOM MOERR 96
602 160 IF(JX.NE.KX) GO TO 180 MOERR 97
603 IF(TEMP.GT.RZERO) GO TO 170 MOERR 98
604 IF(NTRAC.GE.-2) WRITE(KW,180)JX,KX,TEMP MOERR 99
605 180 FORMAT(/8H THE (,13,1X,13,22H) ELEMENT OF OSAY=+1 +,E12.5, MOERR 100
C 6X,45H THEREFORE ALL PARAMETER ERRORS ARE INFINITE.) MOERR 101
606 TEMP=-TEMP MOERR 102
607 170 IF(TEMP.GT.VIFMX) VIFMX=TEMP MOERR 103
608 180 ERR(KX,JX)=ER MOERR 104
609 190 CONTINUE MOERR 105
C MOERR 106
C COMPUTE AND PRINT THE STANDARD ERRORS. MOERR 107
610 NOF=NPTS-NACTV MOERR 107
611 SCFAC=HUGE MOERR 108
612 IF(NOF.LE.0) GO TO 200 MOERR 108
613 SCFAC=NOF MOERR 109
614 SCFAC=OSORT(FOBJ/SCFAC) MOERR 110
615 200 RESCL=NOF+NOF MOERR 111
616 IF(RESCL.GT.RZERO) RESCL=OSORT(RESCL) MOERR 112
617 IF(NTRAC.LT.-1) GO TO 240 MOERR 114
618 WRITE(KW,210)NOF,NOF,RESCL,FOBJ,SCFAC MOERR 115
619 210 FORMAT(///41H NUMBER OF DEGREES OF FREEDOM (N.D.F.) = MOERR 116
C 14H(NPTS-NACTV) +,15//24H EXPECTED VALUE OF PHI = MOERR 117
C 38H N.D.F. PLUS OR MINUS SORT(2*N.D.F.) +,15, MOERR 118
C 18H PLUS OR MINUS,E12.5//22H ACTUAL VALUE OF PHI +,E12.5// MOERR 119
C 26H RESCALING FACTOR = SORT(PHI/N.D.F.) +,E12.5) MOERR 120
620 WRITE(KW,220)VIFMX MOERR 121
621 220 FORMAT(///36H MAXIMUM VARIANCE INFLATION FACTOR +,E12.5/// MOERR 122
C 32H APPROXIMATE STANDARD ERRORS .../68X,8H RESCALED/12X,10H, MOERR 123
C 6X,7HMASK(J),6X,4HX(J),14X,6HERROR,12X,5HERROR) MOERR 124
622 RESCL=HUGE MOERR 125

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```

623      DO 270 JX=1,NV
624          SCALJ=RUNIT
625          ER=ERR(JX,JX+1)
626          IF(ER)230,250,240
627      230      ER=-OSORT(-ER)
628          SCALJ=-ER
629          GO TO 250
630      240      ER=OSORT(ER)
631          SCALJ=ER
632      250      IF(NDF.GT.0 .AND. NFRANK.EQ.NACTV) RESCL=SCFAC*ER
633          DELTX(JX)=SCALJ
634          WRITE(KW,260)JX,MASK(JX),X(JX),ER,RESCL
635      260      FORMAT(/10X,13,110,6X,E15.5,4X,E13.5,4X,E13.5)
636      270      CONTINUE
C          COMPUTE AND PRINT THE CORRELATIONS.
637      IF(NV.LT.2) GO TO 340
638          WRITE(KW,280)(K,K+1,NV)
639      280      FORMAT(///45H LOWER TRIANGLE OF THE CORRELATION MATRIX.....//12X,
        * 7H R .....15,7113/(11X,8113))
640          WRITE(KW,290)(MASK(K),K+1,NV)
641      290      FORMAT(/7X,12H MASK(K).....15,7113/(11X,8113))
642          WRITE(KW,300)
643      300      FORMAT(/3X,1HJ,4X,7HMASK(J) )
644          DO 310 KX=1,JX
645          DO 310 KK=1,JX
646      310          ERR(KX,JX+1)/(DELTX(JX)+DELTX(KX))
647          WRITE(KW,320)JX,MASK(JX),(ERR(KX,1),KK=1,JX)
648      320      FORMAT(/1X,13,14,5X,E13.5/(17X,8E13.5))
649      330      CONTINUE
C          RESCALE ERR AND SYMMETRIZE IT.
650      SCFAC=SCFAC+2
651      IF(SCFAC.LT.RUNIT) SCFAC=RUNIT
652          DO 350 JX=1,NV
653          DO 350 KX=1,JX
654          ERR(JX,KX)+ERR(KX,JX+1)*SCFAC
655      350      ERR(KX,JX)=ERR(JX,KX)
C
656      RETURN
C END MOERR.
657      END
658
SUBROUTINE POFX (JPT,NV,X,F)
C
C   UPDATED BY J. CHANDLER, MAY 1981, OSU COMPUTER SCIENCE
C   DEPARTMENT--J. HANSON, UCC USER SERVICES
C
C   THIS IS A DUMMY VERSION OF SUBROUTINE POFX.
C   A NON-DUMMY VERSION OF POFX MAY BE USED (OPTIONALLY) TO SUPPLY
C   TO MARO VALUES OF THE FUNCTION BEING FITTED. INSTEAD OF USING A
C   -FUNR- SUBROUTINE TO DO THIS. THE USE OF POFX REQUIRES
C   SUBSTANTIALLY MORE OVERHEAD TIME DURING EXECUTION, BUT SAVES
C   CONSIDERABLE STORAGE BY NOT REQUIRING THAT THE JACOBIAN MATRIX, P,
C   BE STORED.
C
659      DOUBLE PRECISION X,F
660      DIMENSION X(20)
661      RETURN
662      END
***ERROR*** WRONG NUMBER OF ARGUMENTS IN REFERENCE TO SUBPROGRAM MARO

```

MOERR126
MOERR127
MOERR128
MOERR129
MOERR130
MOERR131
MOERR132
MOERR133
MOERR134
MOERR135
MOERR136
MOERR137
MOERR138
MOERR139
MOERR140
MOERR141
MOERR142
MOERR143
MOERR144
MOERR145
MOERR146
MOERR147
MOERR148
MOERR149
MOERR150
MOERR151
MOERR152
MOERR153
MOERR154
MOERR155
MOERR156
MOERR157
MOERR158
MOERR159
MOERR160
MOERR161
MOERR162
MOERR163
MOERR164
MOERR165
POFXDUM1
POFXDUM2
POFXDUM2
POFXDUM2
POFXDUM2
POFXDUM3
POFXDUM4
POFXDUM5
POFXDUM6
POFXDUM7
POFXDUM8
POFXDUM8
POFXDUM10
POFXDUM11
POFXDUM12
POFXDUM13
POFXDUM14

PROGRAM WAS EXECUTING LINE 1 IN ROUTINE M/PROG WHEN TERMINATION OCCURRED

STATEMENTS EXECUTED: 1
CORE USAGE OBJECT CODE: 37568 BYTES,ARRAY AREA: 5076 BYTES,TOTAL AREA AVAILABLE: 126024 BYTES
DIAGNOSTICS NUMBER OF ERRORS: 1, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 9
COMPILE TIME: 0.32 SEC,EXECUTION TIME: 0.01 SEC, 14.17.10 FRIDAY 22 JUL 82 WATFIV - MAR 1980 V2L0

CSSTOP


```

1  SJOB      ,LIBLIST
2  CALL STEP
3  STOP
4  END

5  SENTRY
6  SUBROUTINE STEPT (FUNK)
7
8  C
9  C   UPDATED MAY 1981 BY J. P. CHANDLER, OSU DEPARTMENT OF COMPUTING
10 C   AND INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES
11 C
12 C   INTERFACE TO MAKE MARO LOOK LIKE STEPT.
13 C
14 C   TO USE THIS ROUTINE, SET THE VALUES OF LPDMA AND LPDMS, AND SET
15 C   THE DIMENSIONS OF THE ARRAYS P, FITSV, FIT, Y, AND YSIG.
16 C   NORMALLY THE DIMENSIONS ARE
17 C   P(LPDMA,LPDMS), FITSV(LPDMA), FIT(LPDMA), Y(LPDMA), YSIG(LPDMA),
18 C   WHERE LPDMA IS .GE. NPTS AND LPDMS IS .GE. NV.
19 C
20 C   COMMON/CDAT/ DOES NOT APPEAR IN ANY ROUTINE OF THE MARO PACKAGE
21 C   OTHER THAN THIS ONE, SO THIS IS THE ONLY ROUTINE THAT MUST BE
22 C   RECOMPILED WHEN THE DIMENSIONS OF THE ARRAYS ARE CHANGED.
23 C
24 C   THE FOLLOWING EXTERNAL STATEMENT IS REQUIRED BY SOME COMPILERS
25 C   (WAITFIV, FOR EXAMPLE) AND FORBIDDEN BY OTHERS (MDDCOMP II).
26 C   EXTERNAL FUNK
27
28 C
29 C   DOUBLE PRECISION FIT,FITSV      ,Y,YSIG,P
30 C
31 C   DIMENSION P(300,20),FITSV(300)
32 C   COMMON /CDAT/ FIT(300),Y(300),YSIG(300),NPTS
33 C
34 C   LPDMA=300
35 C   LPDMS=20
36 C
37 C   CALL MARO (FUNK,Y,YSIG,NPTS,FIT,FITSV,P,LPDMA,LPDMS)
38 C
39 C   RETURN
40 C   END
41
42 SUBROUTINE MARO (FUNK,Y,YSIG,NPTS,FIT,FITSV,P,LPDMA,LPDMS)
43
44 C
45 C   MARO 3.0      A. N. S. I. STANDARD FORTRAN      MAY 1981
46 C   COPYRIGHT (C) 1981 J. P. CHANDLER
47 C
48 C   J. P. CHANDLER AND LEON W. JACKSON,
49 C   DEPARTMENT OF COMPUTING AND INFORMATION SCIENCES
50 C   OKLAHOMA STATE UNIVERSITY, STILLWATER, OKLAHOMA 74074
51 C
52 C   MARO PERFORMS A NONLINEAR LEAST SQUARES FIT OF A USER-SUPPLIED
53 C   FUNCTION TO A GIVEN SET OF DATA, USING MAROQUARDT-S METHOD, OR THE
54 C   GAUSS-NEWTON METHOD, OR A MODIFIED GAUSS-NEWTON METHOD.
55 C
56 C   UPDATE ADDED TO WAITFIV LIBRARY BY J. HANSON, UCC USER SERVICES
57 C
58 C   INPUT QUANTITIES..... FUNK,X(*),XMAX(*),XMIN(*),DELMN(*),NF,NTRAC,
59 C   MASK(I),MATRIX,NFMAX,NFLAT,KW,
60 C   Y(*),YSIG(*),NPTS,LPCOL.
61
62 C
63 C   FLAMB,FNU,RELP,METHD,KALCP,KORDF,
64 C   MAXIT,LEOU,MXSUB
65 C   OUTPUT QUANTITIES.... X(*),POBJ,ERR(*,*) ,KFLAG,FIT(*)
66 C   SCRATCH VECTOR..... DELTX(*)
67 C   UNUSED QUANTITIES (INCLUDED FOR COMPATIBILITY WITH STEPT COMMON)....
68 C   JVARY,NXTRA,NOREP,KERFL
69 C
70 C   FUNK      -- THE NAME OF THE SUBROUTINE CALLED TO OBTAIN
71 C   THE FITTED VALUES IF KALCP=0
72 C   X(JX)     -- THE JX-TH PARAMETER
73 C   XMAX(JX)  -- THE UPPER LIMIT FOR X(JX)
74 C   XMIN(JX)  -- THE LOWER LIMIT FOR X(JX)
75 C   DELMN(JX) -- THE CONVERGENCE TOLERANCE FOR X(JX)
76 C   POBJ      -- RETURNS THE FINAL VALUE OF PHI, THE WEIGHTED
77 C   SUM OF SQUARES (PHI IS BEING MINIMIZED AS A
78 C   FUNCTION OF THE X(JX))
79 C   NV       -- THE NUMBER OF PARAMETERS
80 C   NTRAC    -- USER PRINT CONTROL
81 C   * 3, NO OUTPUT EXCEPT FATAL ERROR MESSAGES
82 C   * 2, NO OUTPUT EXCEPT DIAGNOSTIC MESSAGES
83 C   * 1, STANDARD OUTPUT EXCEPT FINAL FIT VALUES
84 C   * 0, STANDARD OUTPUT
85 C   * 1, ALSO PRINTS RESULTS OF EACH ITERATION
86 C   * 2, ALSO PRINTS THE COEFFICIENT MATRIX, OSAY
87 C   * 3, ALSO PRINTS THE JACOBIAN MATRIX, P
88 C   MATRIX   -- NONZERO IF STATISTICAL ERRORS ARE TO BE COMPUTED
89 C   MASK(JX) -- NONZERO IF X(JX) IS TO BE HELD FIXED
90 C   NFMAX    -- THE MAXIMUM NUMBER OF FUNCTION COMPUTATIONS
91 C   NFLAT    -- NONZERO IF THE SEARCH IS TO TERMINATE WHEN TWO
92 C   ITERATIONS GIVE IDENTICAL VALUES OF PHI
93 C   KW       -- THE LOGICAL UNIT NUMBER OF THE PRINTER
94 C   ERR(JX,KX) -- RETURNS THE ERROR MATRIX
95 C   KFLAG    -- RETURNED .GT. ZERO FOR A NORMAL EXIT,
96 C   RETURNED .LT. ZERO FOR AN ABNORMAL EXIT
97 C
98 C   Y(JPT)   -- THE JPT-TH DATA ORDINATE
99 C   YSIG(JPT) -- THE EXPECTED ERROR IN Y(JPT)
100 C   NPTS     -- THE NUMBER OF DATA OBSERVATIONS
101 C   FIT(JPT) -- THE JPT-TH FITTED VALUE
102 C   FITSV    -- A SCRATCH VECTOR OF NPTS VALUES
103 C   PIJPT,JX -- THE FIRST PARTIAL DERIVATIVE
104 C   OF FIT(JPT) WITH RESPECT TO X(JX)
105 C   LPDMA    -- THE FIRST DIMENSION OF THE ARRAY CONTAINING P
106 C   (LPCOL MUST BE .GE. NPTS IF KALCP IS .GE. ZERO)
107 C   LPDMS    -- THE SECOND DIMENSION OF THE ARRAY CONTAINING P
108 C   (LPDMS MUST BE .GE. NV)
109 C   FLAMB    -- MAROQUARDT-S LAMBDA, THE RELATIVE AMOUNT BY WHICH
110 C   THE DIAGONAL COEFFICIENTS OF THE NORMAL
111 C   EQUATIONS ARE AUGMENTED
112 C   FNU      -- MAROQUARDT-S NU, THE FACTOR BY WHICH FLAMB IS
113 C   CHANGED
114 C   RELP     -- DETERMINES THE MAGNITUDE OF THE DIFFERENCING STEP
115 C   RELMN    -- RELATIVE CONVERGENCE CRITERION USED FOR EACH X(J)
116 C   FOR WHICH DELMN(J) IS ZERO
117 C   METHD    -- DETERMINES THE METHOD USED
118 C   * 1, MODIFIED GAUSS-NEWTON METHOD
119 C   * 0, GAUSS-NEWTON METHOD
120 C   * 1, MODIFIED FORM OF MAROQUARDT-S METHOD
121 C   * 2, MAROQUARDT-S METHOD
122 C   KALCP    -- DETERMINES WHICH ROUTINE IS CALLED TO COMPUTE THE

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C CHECK SOME INPUT QUANTITIES, AND SET THEM TO DEFAULT VALUES IF      MARO 188
C DESIRED.                                                                MARO 189
C                                                                           MARO 190
48 20 NACTV=0                      NACTV ... NUMBER OF ACTIVE (XIJ)      MARO 200
49 DO 50 JX=1,NV                  MARO 201
50   DELN=OABS(DELNM(JX))         MARO 202
51   IF(MASK(JX))$O,30,50         MARO 203
52   NACTV=NACTV+1                MARO 204
53   IF(DELN.EO.RZERO) DELN=OABS(RELMN*(JX)) MARO 205
54   IF(DELN.EO.RZERO) DELN=RELMN MARO 206
55   IF(XMAX(JX).GT.XMIN(JX)) GO TO 40 MARO 207
56   XMAX(JX)=HUGE                MARO 208
57   XMIN(JX)=-HUGE               MARO 209
58   X(JX)=OMAX(XMIN(JX),OMINI(XMAX(JX),X(JX))) MARO 210
59   DELNM(JX)=DELN              MARO 211
C                                                                           MARO 212
80 IF(NACTV.GT.0) GO TO 80        MARO 213
81 KFLAG=-2                       MARO 214
82 CONTINUE                       MARO 215
83 WRITE(KW,70)NV,NVMAX,NACTV,NPTS,LPDMS,KALCP MARO 216
84 70 FORMAT(//28H ILLEGAL INPUT VALUE IN MARO ,4X,5H NV = ,13,4X, MARO 217
   * 8H NVMAX = ,13,4X,8H NACTV = ,13/10X,7H NPTS = ,15,4X,8H LPDMS = , MARO 218
   * 15,4X,8H LPDMS = ,15,4X,8H KALCP = ,13) MARO 220
85 GO TO 1300                    MARO 221
86 CONTINUE                       MARO 222
87 IF(INTRAC.LT.-1) GO TO 150     MARO 223
88 WRITE(KW,90)(MASK(J),J=1,NV)   MARO 224
89 90 FORMAT(/10H MASK = ,17,7/13/(4X,8I13)) MARO 225
90 WRITE(KW,100)(X(J),J=1,NV)     MARO 226
91 100 FORMAT(/10H X = ,8E13.5/(10X,8E13.5)) MARO 227
92 WRITE(KW,110)(XMAX(J),J=1,NV)  MARO 228
93 110 FORMAT(/10H XMAX = ,8E13.5/(10X,8E13.5)) MARO 229
94 WRITE(KW,120)(XMIN(J),J=1,NV)  MARO 230
95 120 FORMAT(/10H XMIN = ,8E13.5/(10X,8E13.5)) MARO 231
96 WRITE(KW,130)(DELNM(J),J=1,NV) MARO 232
97 130 FORMAT(/10H DELNM = ,8E13.5/(10X,8E13.5)) MARO 233
98 WRITE(KW,140)INV,NPTS,LPDMS,LPDMS,NTRAC,METHOD,KALCP,KORDF, MARO 234
   * NPLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT, MARO 235
   * NPLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT,NPFLAT, MARO 236
   * 8H LPDMS = ,14,5X,8H NTRAC = ,12,5X,8H METHOD = ,13,5X,8H KALCP = , MARO 237
   * 13/8H KORDF = ,12,5X,8H NPLAT = ,12,5X,8H NPFLAT = ,17,5X, MARO 238
   * 8H NPFLAT = ,15,5X,8H NPFLAT = ,14/7H CRIT = ,E12.5,5X,8H RELOF = , MARO 239
   * E12.5,5X,8H RELMN = ,E12.5) MARO 240
99 150 JVAR=0                      MARO 241
C                                                                           MARO 242
C SET FMGN. IF NECESSARY, RESET FLAMB AND/OR FACCL. MARO 243
C                                                                           MARO 244
81 FMGN=RUNIT                     MARO 245
82 UPNU=FNNU                       MARO 246
83 DOWNU=FNNU                      MARO 247
84 IF(FLAMB.LE.RZERO) FLAMB=FLDEF  MARO 248
85 IF(METHOD.EO) FLAMB=RZERO     MARO 249
86 IF(METHOD.NE.1) FACCL=RUNIT   MARO 250
C                                                                           MARO 251
C COMPUTE THE INITIAL GOODNESS OF FIT OF THE MODEL TO THE DATA. MARO 252
C CALL FUNC TO CALCULATE THE VECTOR OF FITTED VALUES. MARO 253
C                                                                           MARO 254
87 CALL FUNC (PUNK,Y,YSIG,NPTS,FIT,PHI) MARO 255
C                                                                           MARO 256
C MF ... EQUIVALENT NUMBER OF CALLS TO FUNC MARO 257
C                                                                           MARO 258
88 MF=1                             MARO 258
89 IF(INTRAC.GE.-1) WRITE(KW,160)PHI,FLAMB MARO 259
90 160 FORMAT(/27H PHI (THE SUM OF SQUARES) = ,E15.8,57X,8H LAMBDA = , MARO 260
   * E12.5//1H) MARO 261
C ***** MARO 262
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C ***** MARO 317
91 170 JSUB=0                      MARO 268
92 FCUT=RTWO                       MARO 270
93 ITER=ITER+1                     MARO 271
94 IF(INTRAC.GE.1) WRITE(KW,180)ITER,FMGN,FLAMB MARO 272
95 180 FORMAT(//16H BEGIN ITERATION,15,44X,7H FMGN = ,E12.5,15X, MARO 273
   * 8H LAMBDA = ,E12.5) MARO 274
96 IF(INTRAC.GE.3) WRITE(KW,190)   MARO 275
97 190 FORMAT(/28H P (THE JACOBIAN MATRIX)...../1H) MARO 276
C ***** MARO 277
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C ***** MARO 317
98 STPAC=RUNIT                     MARO 279
99 DO 200 JX=1,NACTV              MARO 280
100 GRAD(JX)=RZERO                MARO 281
101 DO 200 KX=1,JX                 MARO 282
102 ERR(JX,KX)=RZERO              MARO 283
C ***** MARO 284
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C ***** MARO 317
103 SIG=YSIG(1)                   MARO 288
104 DO 270 JPT=1,NPTS             MARO 289
105 KPT=JPT                        MARO 290
106 IF(KALCP.LT.0) GO TO 210       MARO 291
107 IF(JPT.NE.1) GO TO 230         MARO 292
108 KPT=1                          MARO 293
109 IF(KORDF.LE.2) GO TO 220       MARO 294
110 CALL CALCD (JPT,P,LPDMS,LPDMS) MARO 295
111 GO TO 230                     MARO 296
112 CALL DERIV (JPT,FUNK,NPTS,FIT,FITSV,P,LPDMS,LPDMS) MARO 297
113 CONTINUE                       MARO 298
114 IF(INTRAC.GE.3) WRITE(KW,240)JPT,(P(KPT,JX),JX=1,NACTV) MARO 299
115 240 FORMAT(1X,13,2X,8E15.7/(6X,8E15.7)) MARO 300
C ***** MARO 301
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C ***** MARO 313
C ***** MARO 314
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C ***** MARO 316
C ***** MARO 317
118 COMPUTE OSAY AND GRAD. MARO 302
119 OSAY, WHICH IS STORED IN ONE HALF OF THE ARRAY ERR(=,*) IS PT*P. MARO 303
120 GRAD(=) IS HALF THE GRADIENT OF PHI. MARO 304
C ***** MARO 305
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C ***** MARO 316
C ***** MARO 317
118 IF(LEOU.EO.0) SIG=YSIG(JPT)   MARO 305
119 RTERM=(FIT(JPT)-Y(JPT))/SIG**2 MARO 306
120 DO 250 JX=1,NACTV             MARO 307
121 GRAD(JX)=GRAD(JX)+P(KPT,JX)*RTERM MARO 308
122 PTERM=P(KPT,JX)/SIG**2       MARO 309
123 DO 250 KX=1,JX                MARO 310
124 ERR(JX,KX)=ERR(JX,KX)+PIKPT,KX)*PTERM MARO 311
125 CONTINUE                     MARO 312
126 CONTINUE                     MARO 313
127 CONTINUE                     MARO 314
C ***** MARO 315
C ***** MARO 316
C ***** MARO 317
128 IF(KORDF.NE.2) GO TO 280       MARO 315
129 IF(KALCP.NE.0) GO TO 280       MARO 316

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127 CALL FUNC (FUNK,Y,YSIG,NPTS,PIT,PHI) MARO 316
128 NP=NP+1 MARO 318
129 260 NP=NP+NACTY MARO 320
130 290 NP=NP+NACTY MARO 321
C C COMPUTE THE SCALE FACTORS AND STORE THEM IN DELTX(+). SCALE GRAD. MARO 322
C C MARO 323
131 DD 300 JX=1,NACTY MARO 324
132 SCALJ=OSORT(ERR(JX,JX)) MARO 325
133 IF(SCALJ.EQ.RZERO) SCALJ=RUNIT MARO 326
134 DELTX(JX)=SCALJ MARO 327
135 300 GRAD(JX)=GRAD(JX)/SCALJ MARO 328
136 IF(NTRAC.GE.1) WRITE(KW,310)(GRAD(JX),JX=1,NACTY) MARO 330
137 310 FORMAT(/21H SCALED GRADIENT = ,E15.7/(21X,E15.7)) MARO 331
C C SCALE OSAV. THE DIAGONAL ELEMENTS OF OSAV ARE SCALED TO UNITY. MARO 332
C C MARO 333
138 DD 355 JX=1,NACTY MARO 334
139 DO 380 KX=1,JX MARO 335
140 SA=ERR(JX,KX)/(DELTX(JX)*DELTX(KX)) MARO 337
141 IF(KX.NE.JX) GO TO 320 MARO 338
142 IF(SA.EQ.RZERO) GO TO 330 MARO 339
143 SA=RUNIT MARO 340
144 GO TO 360 MARO 341
145 320 IF(ABS(SA).LT.RUNIT-RLTOL) GO TO 360 MARO 342
146 CONTINUE MARO 343
147 IF(NTRAC.GE.-2) WRITE(KW,340)JX,KX,SA,ITER MARO 344
148 340 FORMAT(38H ***** POSSIBLY DANGEROUS VALUE OF , MARO 345
* 16H COEFFICIENT , ,5X,8H OSAV(,13,1H,,13,3H) ,E15.7,5X, MARO 346
* 10H ITERATION,16) MARO 347
149 350 ERR(JX,KX)=SA MARO 348
150 CONTINUE MARO 349
151 IF(NTRAC.LT.2) GO TO 380 MARO 349
152 WRITE(KW,360) MARO 350
153 360 FORMAT(/49H OSAV (PT=P, SCALED, WHERE P IS THE JACOBIAN)...../1H ) MARO 351
154 DD 370 JX=1,NACTY MARO 352
155 370 WRITE(KW,340)JX,(ERR(JX,KX),KX=1,JX) MARO 353
156 DO 390 JX=1,NV MARO 354
157 380 XSAVE(JX)=X(JX) MARO 355
C INITIALIZE MASKT AND NACT. MARO 356
158 400 NACT=NACTY MARO 357
159 DO 410 JX=1,NV MARO 358
160 410 MASKT(JX)=MASK(JX) MARO 359
C C COPY OSAV INTO O AND GRAD INTO H. AND SET THE DIAGONAL ELEMENTS OF O. MARO 360
C C THIS IS THE ENTRY POINT FOR SUBITERATIONS IN WHICH FLAME IS MARO 361
C C INCREASED OR CONSTRAINTS ARE IMPOSED. MARO 362
161 420 KRANK=0 MARO 363
162 JO=0 MARO 364
163 JT=0 MARO 365
164 DD 450 JX=1,NV MARO 366
165 IF(MASK(JX).NE.O) GO TO 450 MARO 367
166 JO=JO+1 MARO 368
167 IF(MASKT(JX).NE.O) GO TO 460 MARO 369
168 JT=JT+1 MARO 370
169 H(JT)=GRAD(JO) MARO 371
170 KO=0 MARO 372
171 KT=0 MARO 373
172 DD 440 KX=1,JX MARO 374
173 IF(MASK(KX).NE.O) GO TO 440 MARO 375
174 KO=KO+1 MARO 376
175 IF(MASKT(KX).NE.O) GO TO 440 MARO 377
176 KT=KT+1 MARO 378
177 SA=ERR(JO,KO) MARO 379
178 IF(KX.NE.JX .OR. SA.EQ.RZERO) GO TO 430 MARO 380
179 SA=RUNIT*FLAME MARO 381
180 KRANK=KRANK+1 MARO 382
181 430 ERR(KT,JT+1)=SA MARO 383
182 440 CONTINUE MARO 384
183 450 CONTINUE MARO 385
C SOLVE THE NORMAL EQUATIONS FOR H. THE CORRECTION VECTOR. MARO 386
C C MARO 387
184 NSMAL=0 MARO 388
185 NMU=NACT-1 MARO 389
186 IF(NMU.EQ.O) GO TO 480 MARO 390
C C REDUCE THE SYSTEM TO TRIANGULAR FORM. MARO 391
C C UTILIZING THE SYMMETRY OF THE MATRIX. MARO 392
187 DD 480 J=1,NMU MARO 393
188 PIVOT=ERR(J,J+1) MARO 394
189 IF(PIVOT.EQ.RZERO) GO TO 480 MARO 395
190 JPU=J+1 MARO 400
191 DO 470 K=JPU,NACT MARO 401
192 EM=ERR(J,K+1)/PIVOT MARO 402
193 IF(EM.EQ.RZERO) GO TO 470 MARO 403
194 DO 460 L=K,NACT MARO 404
195 ERR(K,L+1)=ERR(K,L+1)-ERR(J,L+1)*EM MARO 405
196 460 H(K)=H(K)-H(J)*EM MARO 406
197 470 CONTINUE MARO 407
C DO THE BACK SOLUTION. MARO 408
198 480 DO 530 J=NV+1,NACT MARO 409
199 J=(NACT+1)-J MARO 410
200 PIVOT=ERR(J,J+1) MARO 411
201 IF(PIVOT.LE.RZERO) NSMAL=NSMAL+1 MARO 412
202 IF(PIVOT.NE.RZERO) GO TO 500 MARO 413
203 H(J)=RZERO MARO 414
204 GO TO 530 MARO 415
205 500 SUM=RZERO MARO 416
206 IF(J.EQ.NACT) GO TO 520 MARO 417
207 JPU=J+1 MARO 418
208 DO 510 K=JPU,NACT MARO 419
209 SUM=SUM+ERR(J,K+1)*H(K) MARO 420
210 510 H(J)=(H(J)-SUM)/PIVOT MARO 421
211 520 CONTINUE MARO 422
C C IF THE COEFFICIENT MATRIX WAS RANK DEFICIENT, PRINT A MESSAGE. MARO 423
C C MARO 424
212 MRANK=NACT-NSMAL MARO 425
213 IF(MRANK.EQ.NACT) GO TO 560 MARO 426
214 COSIN=HUGE MARO 427
215 IF(NTRAC.GE.-2) WRITE(KW,540)MRANK,NACT,ITER MARO 428
216 540 FORMAT(/41H RANK-DEFICIENT NORMAL EQUATIONS IN MARO ,5X,7H RANK , MARO 429
* 14,7X,16H ORDER OF MATRIX ,14,5X,10H ITERATION,16) MARO 430
217 IF(MRANK.GT.O) GO TO 550 MARO 431
218 KFLAG=4 MARO 432
219 GO TO 1300 MARO 433
220 550 IF(METHD.GT.O .AND. MRANK.LT.KRANK) GO TO 560 MARO 434
C MARO 435

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C UNPACK AND DE-SCALE THE CORRECTION VECTOR H.
C COMPUTE THE INNER PRODUCTS SA, SB, AND SC.
C
221 580 SA=RZERO
222 SB=RZERO
223 SC=RZERO
224 KX=NV
225 KO=NACTV
226 KT=NACT
227 DO 590 JX=1,NV
228 NH=RZERO
229 IF(MASK(KX).NE.0) GO TO 580
230 IF(MASK(KN).NE.0) GO TO 570
231 NH=H(KT)
232 SA=SA-NH*GRAD(KO)
233 SB=SB-NH*H
234 SC=SC+GRAD(KO)*2
235 NH=NH+FMGN/DELTX(KO)
236 KT=KT-1
237 KO=KO+1
238 WK(K)=NH
239 KX=KX-1
C
C ADD THE CORRECTION VECTOR TO THE PARAMETER VECTOR AND
C CHECK FOR CONSTRAINT VIOLATIONS.
C THIS IS THE ENTRY POINT FOLLOWING A CUTSTEP.
C
240 600 CONTINUE
241 IF(NTRAC.GE.1) WRITE(KW,510)(H(JX),JX=1,NV)
242 510 FORMAT(/7X,14H CORRECTION ' ',E15.7/(21X,E15.7))
243 NACTV=NACT
244 PRMIN=PRMINIT
245 NLOOP=0
246 JXLIM=0
247 620 DO 720 JX=1,NV
248 IF(MASK(JX).NE.0) GO TO 720
249 XSAV=XSAV(JX)
250 XMX=XMAX(JX)
251 XMN=XMIN(JX)
252 NH=H(JX)
253 IF((XSAV.LT.XMX .OR. NH.LE.RZERO) .AND.
* (XSAV.GT.XMN .OR. NH.GE.RZERO)) GO TO 640
254 MASK(JX)=1
255 NACT=NACT-1
256 X(JX)=XSAV
257 IF(NTRAC.GE.-1) WRITE(KW,630)JX,XSAV,ITER
258 630 FORMAT(/5H FIX X(,12,4H) = ,E12.5,22H TEMPORARILY. TO AVOID,
* 24H VIOLATING A CONSTRAINT.,26X,10H ITERATION,16)
259 GO TO 720
260 640 XLIM=XSAV+NH*PRMIN
261 IF(JX.NE.JXLIM) GO TO 650
262 IF(KEND)650,660,680
263 650 X(JX)=XLIM
264 IF(XLIM.LE.XMX) GO TO 670
265 660 X(JX)=XMX
266 JBND=1
267 GO TO 690
268 670 IF(XLIM.GE.XMN) GO TO 720
269 X(JX)=XMN
270 JBND=-1
C
271 690 IF(JX.NE.JXLIM) GO TO 710
272 IF(NTRAC.LT.-1) GO TO 720
273 WRITE(KW,700)JX,X(JX),PRMIN,ITER
274 700 FORMAT(/28H CONSTRAINT VIOLATED BY X(,12,
* 20H) VALUE RESET TO ,E15.8,24H USING CUTSTEP FACTOR = ,E12.5,40H
* ,3X,8H ITER.,16)
275 GO TO 720
276 710 IF(NLOOP.NE.0) GO TO 720
277 DENOM=XLIM-XSAV
278 IF(DENOM.EQ.RZERO) GO TO 720
279 FRAC=(X(JX)-XSAV)/DENOM
280 IF(FRAC.GE.FRMIN) GO TO 720
281 PRMIN=FRAC
282 JXLIM=JX
283 KEND=JBND
284 720 CONTINUE
C
C IF THE PROPOSED STEP WOULD VIOLATE ANY ALREADY ACTIVE CONSTRAINTS,
C FIX THOSE COMPONENTS OF H EQUAL TO ZERO AND RECDMPUTE THE
C OTHER COMPONENTS.
C
285 IF(NACT.GT.0) GO TO 740
286 KFLAG=3
287 IF(NTRAC.LT.-2) GO TO 1200
288 WRITE(KW,730)
289 730 FORMAT(////47H APPARENT CONSTRAINED OPTIMUM LIES IN A CORNER.)
290 GO TO 1200
291 740 IF(NACT.LT.NACTV) GO TO 420
292 IF(NLOOP.NE.0) GO TO 760
293 NLOOP=1
294 IF(JXLIM.NE.0) GO TO 820
295 750 CONTINUE
296 IF(NTRAC.GE.1) WRITE(KW,750)(X(JX),JX=1,NV)
297 750 FORMAT(/15X,8H X = ,E15.7/(21X,E15.7))
C
C CALCULATE THE NEW FITTED VALUES.
C
298 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHNEW)
299 NP=NP+1
300 IF(PHNEW=PH)830,770,780
C
C THE NEW VALUE OF PHI IS EXACTLY EQUAL TO THE OLD VALUE.
C CHECK FOR CONVERGENCE UNDER THE NPLAT OPTION.
C
301 770 IF(NPLAT.EQ.0) GO TO 830
302 KFLAG=2
303 IF(NTRAC.LT.-1) GO TO 830
304 WRITE(KW,780)
305 780 FORMAT(/45H CONVERGENCE ACHIEVED UNDER THE NPLAT OPTION.)
306 GO TO 830
C
C THE NEW VALUE OF PHI IS GREATER THAN THE OLD VALUE.
C
307 790 CONTINUE
308 IF(NTRAC.GE.1) WRITE(KW,800)PHI,PHNEW
309 800 FORMAT(/33X,10H OLD PHI =,E15.8,5X,10H NEW PHI =,E15.8)
C
C CHECK WHETHER JSUB HAS EXCEEDED MXSUB.
C
310 JSUB=JSUB+1

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311 IF(JSUB.GT.MXSUB) GO TO 810 MARO 557
312 IF(METHD180.1090.850 MARO 558
313 KFLAG=1 MARO 559
314 IF(NTRAC.GE.-1) WRITE(KW,820)MXSUB MARO 560
315 FORMAT(/43H EXCEEDED MAXIMUM NUMBER OF SUBITERATIONS *,13, MARO 561
* 8H IN MARO.) MARO 562
C RESTORE X TO THE BASE POINT. MARO 563
316 DO 840 JX=1,NV MARO 564
317 X(JX)=XSAVE(JX) MARO 565
318 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 566
319 GO TO 1200 MARO 567
C C THE NEW FIT IS WORSE THAN THE OLD FIT COMPUTE COSIN, THE COSINE MARO 568
C OF THE ANGLE BETWEEN THE SCALED GRADIENT AND THE SCALED CORRECTION MARO 570
C VECTOR. MARO 571
320 DENOM=SB+SC MARO 572
321 IF(DENOM.LE.RZERO) GO TO 860 MARO 573
322 COSIN=SA/OSORT(DENOM) MARO 574
323 IF(COSIN.GT.CRIT) GO TO 880 MARO 575
C COSIN IS NOT GREATER THAN CRIT. INCREASE THE VALUE OF LAMBDA. MARO 576
324 UPFAC=UPHU MARO 578
325 UPNU=OMINI*(UPNU*RTWD,FNU) MARO 580
326 IF(METHD.EQ.1) UPFAC=OMINI*(UPFAC,FNUM=RUNIT/FLAMB) MARO 581
327 FLAMB=FLAMB*UPFAC MARO 582
328 IF(NTRAC.GE.1) WRITE(KW,870)JSUB,COSIN,FLAMB MARO 584
329 FORMAT(/18H **** SUBITERATION,13,4X,17H INCREASE LAMBDA *,4X, MARO 585
* 13H COS(GAMMA) *,E12.5,28X,8H LAMBDA *,E12.5) MARO 586
C GO BACK AND FORM THE NORMAL EQUATIONS MARO 587
C USING A LARGER VALUE OF LAMBDA. MARO 588
330 GO TO 400 MARO 589
C COSIN IS GREATER THAN CRIT. CUT THE MAGNITUDE OF THE STEP, H. MARO 591
331 STFAC=STFAC/FCUT MARO 592
332 IF(METHD.GE.0) GO TO 890 MARO 593
333 FMGN=FMGN/FCUT MARO 594
334 GO TO 800 MARO 595
335 890 IF(METHD.EQ.1) FLAMB=FLAMB*RTWD MARO 597
336 DO 910 JX=1,NV MARO 598
337 H(JX)=X(JX)-XSAVE(JX))/FCUT MARO 599
338 FCUT=FCUT*FACCL MARO 600
339 IF(NTRAC.GE.1) WRITE(KW,920)JSUB,COSIN,STFAC MARO 601
340 FORMAT(/18H **** SUBITERATION,13,4X,15H TAKE CUT STEPS *,4X, MARO 602
* 13H COS(GAMMA) *,E12.5,5X,17H CUTSTEP FACTOR *,E12.5) MARO 604
C GO BACK AND TRY A SMALLER CUTSTEP. MARO 605
341 GO TO 800 MARO 606
C THE VALUE OF PHI HAS DECREASED. TRY A HALF STEP. MARO 607
342 IF(METHD.EQ.0 OR METHD.EQ.2) GO TO 1090 MARO 608
343 DO 940 JX=1,NV MARO 609
344 XTEMP(JX)=X(JX) MARO 610
345 IF(MASK(JX).NE.0) GO TO 940 MARO 611
346 X(JX)=XSAVE(JX)+X(JX)-XSAVE(JX))/RTWD MARO 612
347 X(JX)=OMAX*(XMIN(JX),OMINI*(XMAX(JX),X(JX))) MARO 613
C MARO 614
C MARO 615
C MARO 616
348 940 CONTINUE MARO 617
349 DO 950 JPT=1,NPTS MARO 618
350 FITSV(JPT)=FIT(JPT) MARO 619
351 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHALF) MARO 620
352 NF=NF+1 MARO 621
C USE QUADRATIC INTERPOLATION, IN ORDER TO TRY TO REFINER THE MARO 622
C POSITION OF THE MINIMUM OF PHI. MARO 623
353 RLFAC=RUNIT MARO 624
354 DENOM=RTWD*((PHNEW-PHALF)-(PHALF-PHI)) MARO 625
355 STFAC=RZERO MARO 626
356 IF(DENOM.LE.RZERO) GO TO 940 MARO 627
357 STFAC=(PHI-PHNEW)/DENOM MARO 628
358 RSPAC=(RUNIT*STFAC)/RTWD MARO 629
C DO NOT EXTRAPOLATE. MARO 630
359 IF(STFAC.GE.RUNIT) STFAC=RZERO MARO 631
360 DO 970 JX=1,NV MARO 632
361 H(JX)=X(JX) MARO 633
362 X(JX)=X(JX)+XTEMP(JX)-X(JX)*STFAC MARO 634
363 IF(PHALF.GE.PHNEW) GO TO 1010 MARO 635
364 RLFAC=RUNIT/RTWD MARO 636
365 JSUB=JSUB+1 MARO 637
366 DO 980 JX=1,NV MARO 638
367 XTEMP(JX)=X(JX) MARO 639
368 DO 990 JPT=1,NPTS MARO 640
369 FITSV(JPT)=FIT(JPT) MARO 641
370 IF(NTRAC.GE.1) WRITE(KW,1000)PHNEW,PHALF MARO 642
371 1000 FORMAT(/21H HALF STEP SUCCEEDED.,15X,8H PHNEW *,E15.8,18X, MARO 643
* 8H PHALF *,E15.8) MARO 644
372 PHNEW=PHALF MARO 645
373 1010 IF(STFAC.EQ.RZERO) GO TO 1020 MARO 646
374 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 647
375 NF=NF+1 MARO 648
376 IF(PHI.LT.PHNEW) GO TO 1080 MARO 649
377 DO 1020 JX=1,NV MARO 650
378 X(JX)=XTEMP(JX) MARO 651
379 DO 1040 JPT=1,NPTS MARO 652
380 FIT(JPT)=FITSV(JPT) MARO 653
381 IF(STFAC.EQ.RZERO) GO TO 1080 MARO 654
382 IF(NTRAC.LT.1) GO TO 1080 MARO 655
383 WRITE(KW,1050)RLFAC,PHI MARO 656
384 1050 FORMAT(/25H QUADRATIC INTERPOLATION SUCCEEDED.,22X,8H RSPAC *,E12.5,12X, MARO 657
* 8H PHI *,E15.8) MARO 658
385 GO TO 1080 MARO 659
386 RLFAC=RSPAC MARO 660
387 PHNEW=PHI MARO 661
388 IF(NTRAC.GE.1) WRITE(KW,1070)RLFAC,PHI MARO 662
389 1070 FORMAT(/35H QUADRATIC INTERPOLATION SUCCEEDED.,12X,8H RLFAC *, MARO 663
* E12.5,12X,8H PHI *,E15.8) MARO 664
390 IF(RLFAC.LE.RZERO) GO TO 1080 MARO 665
391 FLAMB=FLAMB/RLFAC MARO 666
392 IF(METHD.LT.0) FMGN=FMGN*RLFAC MARO 667
C THE STEP IS ACCEPTED. TEST FOR CONVERGENCE IF NO CONSTRAINT MARO 668
C BECAME ACTIVE DURING THIS ITERATION. MARO 670
C 1080 CONTINUE MARO 671
393 IF(NTRAC.GE.1) WRITE(KW,1100)ITER,PHNEW MARO 672
394 MARO 673
MARO 674
MARO 675
MARO 676

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395 1100 FORMAT(/18H END ITERATION.IS,8X,8H PHI ,E15.8) MARO 877
396 PHIPPHNEW MARO 876
397 IF(JX1H.GT.0) GO TO 1130 MARO 875
398 DO 1110 JX1,NV MARO 880
399 IF(MASK(JX).NE.0) GO TO 1110 MARO 881
400 IF(QABS(X(JX)*XSAYE(JX)) .GT.DELMH(JX)) GO TO 1130 MARO 882
401 1110 CONTINUE MARO 883
402 KFLAG=1 MARO 884
403 IF(INTRAC.LT.-1) GO TO 1200 MARO 885
404 WRITE(KW,1120) MARO 886
405 1120 FORMAT(/38H CONVERGED WHEN THE STEP BECAME SMALL.) MARO 887
406 GO TO 1200 MARO 888
C MARO 889
C THE ITERATION HAS NOT YET CONVERGED. MARO 890
C MARO 891
407 1130 IF(ITER.LT.MAXIT) GO TO 1150 MARO 892
408 KFLAG=-8 MARO 893
409 WRITE(KW,1140)MAXIT MARO 894
410 1140 FORMAT(/48H MAXIMUM NUMBER OF ITERATIONS REACHED IN MARO.,8X, MARO 895
411 8H MAXIT ,E15) MARO 896
GO TO 1200 MARO 897
C MARO 898
C IF SUBITERATIONS WERE NOT PERFORMED THIS ITERATION, DECREASE LAMBDA. MARO 899
C MARO 900
412 1150 IF(NF.GE.NPMAX) GO TO 1160 MARO 901
413 IF(JSUB.GT.0) GO TO 1160 MARO 902
414 PMGN=OMINI(FMGN*RTWO,RUNIT) MARO 903
415 SCALJ=RUNIT*FLAMB MARO 904
416 IF(SCALJ.GT.RUNIT) FLAMB=FLAMB/DDWNU MARO 905
417 UPNU=DDWNU MARO 906
418 DDWNU=OMINI(DDWNU*RTWO,PNU) MARO 907
419 GO TO 1170 MARO 908
420 1160 IF(METHD.NE.1) GO TO 1170 MARO 909
421 UPNU=PNULM MARO 910
422 DDWNU=PNULM MARO 911
423 1170 CONTINUE MARO 912
GO BACK AND GO ANOTHER ITERATION. MARO 913
C MARO 914
424 GO TO 170 MARO 915
425 KFLAG=-7 MARO 916
426 WRITE(KW,1180)NPMAX MARO 917
427 1180 FORMAT(/23H NF HAS REACHED NPMAX ,E17,8H IN MARO.) MARO 918
C MARO 919
C ***** MARO 920
C THE ITERATION HAS TERMINATED. MARO 921
C PRINT OUT THE DATA, FITTED VALUES, AND RESIDUALS. MARO 922
C COMPUTE AND PRINT THE STANDARD DEVIATION OF THE DATA FROM THE FIT. MARO 923
C MARO 924
428 1200 CONTINUE MARO 925
429 SC=OSORT(SC) MARO 926
430 IF(INTRAC.LT.-1) GO TO 1290 MARO 927
431 WRITE(KW,1210)ITER,NF,PHI,PMGN,FLAMB,SC MARO 928
432 1210 FORMAT(/1X,14,11H ITERATIONS,7X,8H NF ,E15,8X,8H PHI ,E15.8,10X, MARO 929
433 7H PMGN ,E12.5,7X,8H LAMBDA ,E12.5//8X,18H NORM OF SCALED, MARO 930
434 18H GRADIENT VECTOR ,E12.5) MARO 931
435 WRITE(KW,780)((JX),JX+1,NV) MARO 932
436 IF(INTRAC.GE.0) WRITE(KW,1220) MARO 933
437 1220 FORMAT(/14X,1HJ,8X,8H Y(J),14X,7H FIT(J),10X, MARO 934
438 12H Y(J)-FIT(J),7X,8H YSIG(J),11X,12H (Y-FIT)/YSIG/1H ) MARO 935
439 SIG=YSIG(1) MARO 936

437 RMSDV=RZERO MARO 737
438 SDVM=RZERO MARO 738
439 DO 1240 JPT=1,NPTS MARO 739
440 IF(LEOU.EQ.0) SIG=YSIG(JPT) MARO 740
441 YY=Y(JPT) MARO 741
442 PTERM=YY-FIT(JPT) MARO 742
443 RTERM=PTERM/SIG MARO 743
444 IF(INTRAC.GE.0) WRITE(KW,1230)JPT,YY,FIT(JPT),PTERM,SIG,RTERM MARO 744
445 1230 FORMAT(5X,11O,5X,E15.8,5X,E15.8,5X,E12.5,5X,E12.5,10X,E12.5) MARO 745
446 RMSDV=RMSDV+RTERM**2 MARO 746
447 1240 SDVMX=OMAX1(SDVMX,OABS(RTERM)) MARO 747
448 DENOM=NPTS*WACTV MARO 748
449 WRITE(KW,1250)DENOM MARO 749
450 1250 FORMAT(/32H NUMBER OF DEGREES OF FREEDOM ,E12.5 ) MARO 750
451 IF(DENOM.LE.RZERO) GO TO 1270 MARO 751
452 RMSDV=OSORT(RMSDV/DENOM) MARO 752
453 WRITE(KW,1280)RMSDV MARO 753
454 1260 FORMAT(/43H R.M.S. SCALED DEVIATION OF DATA FROM FIT ,E12.5) MARO 754
455 1270 CONTINUE MARO 755
456 WRITE(KW,1280)SDVMX MARO 756
457 1280 FORMAT(/27H MAXIMUM SCALED DEVIATION ,E12.5) MARO 757
C MARO 758
C CALL FUNC TO SET THE FINAL VALUES. MARO 759
C MARO 760
458 1280 CALL FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) MARO 761
459 POBJ=PHI MARO 762
C MARO 763
C CALL MOERR TO PRINT THE PARAMETER ERRORS AND CORRELATIONS. MARO 764
C A DUMMY ROUTINE MAY BE SUBSTITUTED FOR MOERR IF THESE ARE NOT NEEDED. MARO 765
C MARO 766
460 IF(MATRX.EQ.0) RETURN MARO 767
461 CALL MOERR (NACTV,NPTS) MARO 768
C MARO 769
462 1300 RETURN MARO 770
463 END MARO 771
END MARO 772

464 SUBROUTINE FUNC (FUNK,Y,YSIG,NPTS,FIT,PHI) FUNC 1
C FUNC 2
C UPDATED BY J CHANDLER, OSU DEPARTMENT OF COMPUTING AND FUNC 2
C INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES, MAY 1981 FUNC 2
C FUNC 2
C FUNC CALLS FUNK OR FOPX TO COMPUTE THE ARRAY OF FITTED VALUES FITM. FUNC 3
C FUNC 4
465 DOUBLE PRECISION Y,YSIG,XMAX,XMIN,DELTX,DELMN,ERR,POBJ, FUNC 5
466 FLAMB,FNU,RELD,RELMN FUNC 6
467 DOUBLE PRECISION X,FIT,P,PHI,SIG FUNC 7
C FUNC 8
468 DIMENSION Y(1),YSIG(1),FIT(1) FUNC 9
C FUNC 10
469 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20), FUNC 11
470 ERR(20,21),POBJ,NV,NTRAC,MATRX,MASK(20), FUNC 12
471 NPMAX,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERPL,KW FUNC 13
472 COMMON /NLS6/ FLAMB,FNU,RELD,RELMN,METHD,KALCP,KORDF,MAXIT, FUNC 14
473 LEQU,MXSUB,MKUPD FUNC 15
C FUNC 16
470 RZERO=0 FUNC 17
471 IF(KALCP.NE.0) GO TO 10 FUNC 18
C FUNC 19
472 CALL FUNK (FIT) FUNC 20

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537 100 CONTINUE
538 GO TO 140
C
C KALCP.LT.O COMPUTE ONE ROW OF P, ONE ELEMENT AT A TIME.
C
539 110 FITSV(1)=FIT(JPT)
540 CALL FDFX [JPT,NV,X,FK1]
541 IF(KDRDF.EQ.2) GO TO 130
542 P(1,KX)=(FK1-FITSV(1))/DEL
543 GO TO 130
544 120 X(JX)=XSAVE-DEL
545 CALL FDFX [JPT,NV,X,FK0]
546 P(1,KX)=(FK1-FK0)/TWDDL
547 FIT(JPT)=FITSV(1)
C
548 140 X(JX)=XSAVE RESTORE X[JX].
549 CONTINUE
C
550 IF(KALCP.LT.O) RETURN
551 GO 160 J+1,NPTS
552 160 FIT(J)=FITSV(J)
C
553 RETURN
554 END DERIV.
555 END
C
556 SUBROUTINE MOERR (NACTV,NPTS)
C
C UPDATED BY J. CHANDLER, OSU DEPARTMENT OF COMPUTING AND
C INFORMATION SCIENCES--J. HANSON, UCC USER SERVICES
C
C MOERR 3.0 A.N.S.I. STANDARD FORTRAN MAY 1981
C
C MOERR IS CALLED BY MARO TO COMPUTE AND PRINT APPROXIMATE VALUES OF
C THE PARAMETER ERRORS AND CORRELATIONS
C
C FOR THE MEANING OF THE -MAXIMUM VARIANCE INFLATION FACTOR- BELOW,
C SEE... O. W. MARQUARDT AND R. D. SHEE,
C RIDGE REGRESSION IN PRACTICE,
C THE AMERICAN STATISTICIAN 29 (1975) 3-20
C
C INPUT QUANTITIES..... KW,ERR(*,*),NACTV,DELTX(*),NPTS,NV,NTRAC,
C MASK(*),FOBJ
C OUTPUT QUANTITIES..... ERR(*,*)
C
558 DOUBLE PRECISION H,SCALE,XMAX,XMIN,DELTX,DELMN,ERR,FOBJ,
C OSORT,ARG,RZERO,RUNIT,HUGE,PIVOT,O,VIFMX,ER,TEMP,
C DENOM,SCFAC,RESCL,X
C
557 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
C ERR(20,21),FOBJ,NV,NTRAC,MATRX,MAK(20),
C NPMAX,NPLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW
C
558 OSORT(ARG)=OSORT(ARG)
C
C * * * * *
559 RZERO=0.
560 RUNIT=1.
561 HUGE=1.E30
C
C
C PRINT OSAY.
562 IF(NTRAC.LT.-1) GO TO 40
563 WRITE(KW,10)
564 10 FORMAT(//18H SUBROUTINE MOERR.//26H OSAY (PT+P, SCALED, WHERE,
C * 23H P IS THE JACOBIAN)...)
565 DO 30 JX=1,NACTV
566 WRITE(KW,20)JX,ERR[JX,KX],KX+1,JX]
567 20 FORMAT(1X,13,2X,6E15.7/(6X,6E15.7))
568 30 CONTINUE
C
C COMPUTE THE SCALED ERROR MATRIX, WHICH IS THE INVERSE OF OSAY.
C INVERT OSAY USING THE GAUSS-JORDAN METHOD WITHOUT PIVOTING.
C F. L. BAUER AND C. REINSCH, P. 45 IN "LINEAR ALGEBRA"
C BY J. M. WILKINSON AND C. REINSCH (SPRINGER-VERLAG, 1971)
C ERR(*,NV+1) IS USED AS A SCRATCH VECTOR.
C
569 40 NVPLU=NV+1
570 NSMAL=0
571 DO 130 LINV=1,NACTV
572 L=(NACTV+1)-LINV
573 PIVOT=ERR(L,1)
574 IF(PIVOT.LE.RZERO) NSMAL=NSMAL+1
575 IF(NACTV.LT.2) GO TO 90
576 DO 80 K=2,NACTV
577 O=ERR(K,1)
578 IF(PIVOT.NE.RZERO) GO TO 50
579 ERR(K,NVPLU)=RZERO
580 GO TO 70
581 50 IF(K.GT.L) GO TO 60
582 ERR(K,NVPLU)=O/PIVOT
583 GO TO 70
584 60 ERR(K,NVPLU)=O/PIVOT
585 70 DO 80 M=2,K
586 ERR(K-1,M-1)=ERR(K,M)+O*ERR(M,NVPLU)
587 80 IF(PIVOT.NE.RZERO) GO TO 100
588 ERR(NACTV,NACTV)=RZERO
589 GO TO 110
590 ERR(NACTV,NACTV)=RUNIT/PIVOT
591 110 IF(NACTV.LT.2) GO TO 130
592 DO 120 K=2,NACTV
593 120 ERR(NACTV,K-1)=ERR(K,NVPLU)
594 130 CONTINUE
C
595 NBRANK=NACTV-NSMAL
596 IF(NBRANK.LT.NACTV) WRITE(KW,140)NBRANK,NACTV
597 140 FORMAT(//51H THE SECOND DERIVATIVE MATRIX IS SINGULAR IN MOERR.
C * 8X,7H RANK =,13,7X,8H ORDER =,13//24H THEREFORE ALL PARAMETER,
C * 21H ERRORS ARE INFINITE.)
C
C UNPACK THE ERROR MATRIX INTO THE UPPER
C TRIANGLE OF ERR(*,*). DE-SCALING IT
598 JV=0
599 VIFMX=RZERO
600 DO 180 JX=1,NV
601 IF(MASK[JX].EQ.O) JV=JV+1
602 KV=0
603 DO 180 KX=1,JX
604 ER=RZERO
605 IF(MASK[JX].NE.O .OR. MASK[KX].NE.O) GO TO 180
606 KV=KV+1

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DERIV 79
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807      TEMP=RZERO
808      DENOM=DELTX(JV)*DELTK(KV)
809      IF(DENOM.EQ.RZERO) GO TO 150
810      TEMP=ERR(JV,KV)
811      ER=TEMP/DENOM
812      150 IF(JX.NE.KX) GO TO 180
813      IF(TEMP.GT.RZERO) GO TO 170
814      IF(NTRAC.GE.-2) WRITE(KW,180)JX,KX,TEMP
815      180 FORMAT/6H THE (.12,1N.,13.23H) ELEMENT OF OSAV**1 +.E13.5.
      * 6X,45H THEREFORE ALL PARAMETER ERRORS ARE INFINITE.)
816      TEMP=-TEMP
817      IF(TEMP.GT.VIFMX) VIFMX=TEMP
818      ER=KX,JX+1)*ER
819      190 CONTINUE
C      COMPUTE AND PRINT THE STANDARD ERRORS.
820      NDF=NPTS-NACTV
821      SCFAC=MUCE
822      IF(NDF.LE.0) GO TO 200
823      SCFAC=NDF
824      SCFAC=OSORT(FOBJ/SCFAC)
825      200 RESCL=NDF*NDF
826      IF(RESCL.GT.RZERO) RESCL=OSORT(RESCL)
827      IF(NTRAC.LT.-1) GO TO 240
828      WRITE(KW,210)NDF,NDF,RESCL,FOBJ,SCFAC
829      210 FORMAT(///41H NUMBER OF DEGREES OF FREEDOM (N D.F.) *
      * 14H(NPTS-NACTV) +.15//24H EXPECTED VALUE OF PHI *
      * 38H N.D.F. PLUS OR MINUS SORT(2*N D.F.) +.15.
      * 15H PLUS OR MINUS.E12.5//22H ACTUAL VALUE OF PHI +.E12.5//
      * 38H RESCALING FACTOR * SORT(PHI/N D.F.) * .E12.5)
830      WRITE(KW,220)VIFMX
831      220 FORMAT(///35H MAXIMUM VARIANCE INFLATION FACTOR +.E12.5//
      * 32H APPROXIMATE STANDARD ERRORS .../6&X,9H RESCALED/12X,1HJ.
      * 6X,7HMASK(J),9X,4H(K),14X,5HERROR,12X,5HERROR)
832      RESCL=MUCE
833      DO 270 JX=1,NV
834      SCALJ=RUNIT
835      ER=ERR(JX,JX+1)
836      IF(ER)230,250,240
837      230 ER=-OSORT(-ER)
838      SCALJ=ER
839      GO TO 260
840      ER=OSORT(ER)
841      SCALJ=ER
842      250 IF(NDF.GT.0.AND.NRANK.EQ.NACTV) RESCL=SCFAC*ER
843      DELTX(JX)=SCALJ
844      WRITE(KW,280)JX,Mask(JX),X(JX),ER,RESCL
845      280 FORMAT(/10X,13.110,6X,E18.8,4X,E13.5,4X,E13.5)
846      270 CONTINUE
C      COMPUTE AND PRINT THE CORRELATIONS.
847      IF(NV.LT.2) GO TO 340
848      WRITE(KW,290)(K,K+1,NV)
849      290 FORMAT(///45H LOWER TRIANGLE OF THE CORRELATION MATRIX...../12X,
      * 7H K .....IS.7113/(11X,8113))
850      WRITE(KW,290)Mask(K),K+1,NV)
851      290 FORMAT(/7X,12H MASK(K).....IS.7113/(11X,8113))
852      WRITE(KW,300)
853      300 FORMAT(/3X,1HJ,4X,7HMASK(J) )
854      DO 330 JX=1,NV
855      DO 310 KX=1,JX
856      ERR(KX,1)*ERR(KX,JX+1)/(DELTX(JX)*DELTK(KX))
      MOERR 82
      MOERR 83
      MOERR 84
      MOERR 85
      MOERR 86
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APPENDIX E

LISTING OF GLOBAL MODEL PROGRAM AND DATA

FIT CALCULATION RESULTS

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SJOB
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C *****
C * 2-ND ORDER GLOBAL MODEL *
C * DATA FROM HECK AND STEIN *
C * HYDRODESULFURIZATION *
C * SRC RECYCLE SOLVENT *
C * HDS-SA CATALYST *
C *****
1  IMPLICIT REAL*8 (A-H,O-Z)
2  EXTERNAL EXPFIT
3  DOUBLE PRECISION X, FIT
4  COMMON /CSTEP/ X(20), XMAX(20), XMIN(20), DELTX(20), DELMN(20),
5  *ERR(20, 21), FOBJ, NV, NTRAC, MATRX, MASK(20),
6  *NPFMAX, NPLAT, JVARY, NXTRA, KPLAC, NOREP, KERFL, KW
7  COMMON /MLLS4/ PLAMB, PNU, RELDP, RELMN, METND, KALCP, KORDP,
8  *MAXIT, LEOU, MXSUE, WKUPD
9  COMMON /CDAT/ FIT(300), Y(300), YSIG(300), NPTS
10 COMMON /CSTOR/ T(70), P(70), ALHSV(70), C1(70), X1(70)
11 KR=8
12 KWS=8
13 FL=1.
14 CALL STSET
15 MAXIT=200
16 NV=3
17 XMIN(1)=0.0
18 X(1)=1.0E10
19 X(2)=8.0E04
20 X(3)=1.5
21 NTRAC=0
22 WRITE(KW, 50)
23 50  FORMAT(////'10X, 'TEMPERATURE', 'SX, 'PRESSURE', 'SX, 'LHSV', 'SX, 'IN. CONC
24 *', 'SX, 'FIN. CONC.', //14X, '(R)', 10X, '(PSI)', 10X, '(1/HR)', 10X, '(WT%)
25 *', 10X, '(WT%)')
26 READ(KR, 100)NPTS
27 100  FORMAT(15)
28 DD 1 10 K=1, NPTS
29 READ(KR, 120)T(K), P(K), ALHSV(K), C1(K), Y(K)
30 120  FORMAT(7X, 5F10. 6)
31 T(K)=T(K)+450.
32 WRITE(KW, 125)NPTS, (K, T(K), P(K), ALHSV(K), C1(K), Y(K), K=1, NPTS)
33 125  FORMAT(//1X, 15//1X, 16, 8E16. 6)
34 CALL STEPY (EXPFIT)
35 DEV=0.0
36 PE=0.0
37 SDS=0.0
38 DD 130 L=1, NPTS
39 DEV=DEV+DABS(FIT(L)-Y(L))/NPTS
40 PE=PE+DABS(FIT(L)-Y(L))/NPTS/Y(L)*100.
41 SDS=SDS+(FIT(L)-Y(L))**2
42 WRITE(KW, 135)
43
44
45 135  FORMAT(1M1, ////'SX, '2-ND ORDER GLOBAL MODEL PARAMETERS', //)
46 WRITE(KW, 140)X(1), X(2), X(3)
47 140  FORMAT(//SX, 'A = ', E10. 4, 3X, 'PSI=([-M]/WT%/HR', //SX, 'E = ', E10. 4, 3
48 *X, 'STU/LBMDLE', //SX, 'M = ', E10. 4)
49 WRITE(KW, 150)DEV, PE, FOBJ, SDS
50 150  FORMAT(////'SX, 'MEAN DEVIATION = ', E10. 4, //SX, 'AVG. PERCENT ERROR =
51 *', E10. 4, //SX, 'FOBJ = ', E10. 4, //SX, 'SUM OF SQUARES = ', E10. 4, //)
52 STOP
53 END
54
55 SUBROUTINE EXPFIT (FITM)
56 IMPLICIT REAL*8 (A-H,O-Z)
57 DOUBLE PRECISION X, FIT, OEXP, DEXP, ARG, FITM, FF
58 DIMENSION FITM(1)
59 COMMON /CSTEP/ X(20), XMAX(20), XMIN(20), DELTX(20), DELMN(20),
60 *ERR(20, 21), FOBJ, NV, NTRAC, MATRX, MASK(20),
61 *NPFMAX, NPLAT, JVARY, NXTRA, KPLAC, NOREP, KERFL, KW
62 COMMON /CDAT/ FIT(300), Y(300), YSIG(300), NPTS
63 COMMON /CSTDR/ T(70), P(70), ALHSV(70), C1(70), X1(70)
64 OEXP(ARG)=DEXP(ARG)
65 FOBJ=0.
66 R=1.987
67 DD 200 J=1, NPTS
68 YSIG(J)=1.0
69 FF=1./[X(1)+OEXP(-X(2)/(R+T(J)))+P(J)+X(3)/ALHSV(J)+1./C1(J)]
70 FITM(J)=FF
71 FOBJ=FOBJ+[(FF-Y(J))/YSIG(J)]**2
72 RETURN
73 END
74
75 SENTRY
76
77 TEMPERATURE      PRESSURE      LHSV      IN. CONC.      FIN. CONC.
78 (R)              (PSI)         (1/HR)    (WT%)         (WT%)
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18 0.123800 04 0.280000 04 0.188000 01 0.410000 00 0.200000-01

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.100000 11 0.800000 05 0.150000 01
 XMAX = 0.100000 31 0.100000 31 0.100000 31
 XMIN = 0.000000 00 -0.100000 31 -0.100000 31
 DELMH = 0.100000 03 0.800000-03 0.150000-07

NY = 2 NPTS = 18 LPDMA = 300 LPDMB = 20 NTRAC = 0 METHD = 1 KALEP = 0
 KORDF = 1 NPLAT = 1 NPMAX = 32767 MAXIT = 200 MHSUB = 25
 CRIT = 0.707110 00 RELDF = 0.100000-07 RELMH = 0.100000-07

PHI (THE SUM OF SQUARES) = 0.738860550-02 LAMBDA = 0.100000 01

CONSTRAINT VIOLATED BY X(1). VALUE RESET TO 0.000000000 00 USING CUTSTEP FACTOR = 0.891280-01 ITER. 1
 CONSTRAINT VIOLATED BY X(1). VALUE RESET TO 0.000000000 00 USING CUTSTEP FACTOR = 0.487310 00 ITER. 2

CONVERGED WHEN THE STEP BECAME SMALL.

114 ITERATIONS NF = 831 PHI = 0.878806300-03 FMGN = 0.100000 01 LAMBDA = 0.127140-02

NORM OF SCALED GRADIENT VECTOR = 0.347520-10

X = 0.44640380 03 0.28860980 05 0.13737480 01

J	V(J)	FIT(J)	V(J)-FIT(J)	YSIG(J)	(V-FIT)/YSIG
1	0.1999990E-01	0.1888880E-01	0.113340-02	0.100000 01	0.113340-02
2	0.2999990E-01	0.3577770E-01	-0.578740-02	0.100000 01	-0.578740-02
3	0.3999990E-02	0.1029642E-01	-0.298630-03	0.100000 01	-0.298630-03
4	0.99999970E-02	0.4513545E-02	0.548850-02	0.100000 01	0.548850-02
5	0.1999990E-01	0.8265819E-02	0.107340-01	0.100000 01	0.107340-01
6	0.99999970E-02	0.5358840E-02	0.484010-02	0.100000 01	0.484010-02
7	0.99999970E-02	0.7808538E-02	0.219140-02	0.100000 01	0.219140-02
8	0.99999970E-02	0.1384425E-01	-0.358430-02	0.100000 01	-0.358430-02
9	0.99999970E-02	0.8700050E-02	0.129890-02	0.100000 01	0.129890-02
10	0.2999990E-01	0.2356650E-01	0.633350-02	0.100000 01	0.633350-02
11	0.4999990E-01	0.4753884E-01	0.246110-02	0.100000 01	0.246110-02
12	0.1999990E-01	0.2529559E-01	-0.529560-02	0.100000 01	-0.529560-02
13	0.99999970E-02	0.1785327E-01	-0.785340-02	0.100000 01	-0.785340-02
14	0.1999990E-01	0.1022708E-01	0.877290-02	0.100000 01	0.877290-02
15	0.99999970E-02	0.6802689E-02	0.419740-02	0.100000 01	0.419740-02
16	0.99999970E-02	0.3971473E-02	0.285250-04	0.100000 01	0.285250-04
17	0.1999990E-01	0.2832838E-01	-0.832840-02	0.100000 01	-0.832840-02
18	0.1999990E-01	0.1171434E-01	0.828570-02	0.100000 01	0.828570-02

NUMBER OF DEGREES OF FREEDOM = 0.18000D 02
 R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.82124D-02
 MAXIMUM SCALED DEVIATION = 0.10734D-01

SUBROUTINE MOERR.

QRAY (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.1000000D 01
2  -0.888168D 00  0.1000000D 01
3  0.888310D 00 -0.888188D 00  0.1000000D 01

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 18
 EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 18 PLUS OR MINUS 0.84772D-01
 ACTUAL VALUE OF PHI = 0.87891D-03
 RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.82124D-02

MAXIMUM VARIANCE INFLATION FACTOR = 0.16159D 04

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.44840348D 03	0.23162D 06	0.14383D 04
2	0	0.28880863D 05	0.86143D 06	0.58727D 04
3	0	0.13737458D 01	0.36188D 02	0.22461D 00

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K ....  1      2      3
MASK(K)....  0      0      0
J  MASK(J)
1  0      0.10000D 01
2  0      0.86741D 00  0.10000D 01
3  0      -0.88773D 00 -0.18088D 00  0.10000D 01

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3-ND ORDER GLOBAL MODEL PARAMETERS

A = 0.4484D 03 PSI = (-M)/WTS/HR
 E = 0.2888D 05 BTU/LBMOLE
 M = 0.1374D 01

MEAN DEVIATION = 0.4782D-02
 AVG. PERCENT ERROR = 0.3048D 02
 F0BJ = 0.8789D-03
 SUM OF SQUARES = 0.8789D-03

STATEMENTS EXECUTED= 198907

CORE USAGE OBJECT CODE= 43378 BYTES, ARRAY AREA= 66486 BYTES, TOTAL AREA AVAILABLE= 174080 BYTES

DIAGNOSTICS NUMBER OF ERRORS= 0, NUMBER OF WARNINGS= 0, NUMBER OF EXTENSIONS= 10

COMPILE TIME= 0.28 SEC, EXECUTION TIME= 2.63 SEC, 11.21.33 SATURDAY 23 JUL 83 WATFV - MAR 1980 V2L0

CSSTDP

APPENDIX F

LISTING OF DIBENZOTHIOPHENE PROCESS

MODEL PROGRAM AND DATA FIT

CALCULATION RESULTS

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SJOB
*****
DIBENZOTHIOPHENE HDS MODEL
2-TYPE SITE INTRINSIC RATE EXPRESSION (BRODDERICK)
ISOHERMAL FIT
DATA FROM ESPINO
*****

GLOSSARY
A(J)=SIMPLIFICATION TERM FOR INTEGRATED RATE EQUATION
AM2=PRE-EXPONENTIAL CONSTANT FOR HYDROGEN EQUILIBRIUM CONSTANT
(1/WTL)
ALNSV(J)=LIQUID HOURLY SPACE VELOCITY FOR DATA POINT J (1/HR)
ALNSV1(J)=J-TH VALUE IN LIQUID HOURLY SPACE VELOCITY GROUP
(1/HR)
AP=PRE-EXPONENTIAL CONSTANT FOR PRODUCT EQUILIBRIUM CONSTANT
(1/WTL)
AR=PRE-EXPONENTIAL CONSTANT FOR REACTANT EQUILIBRIUM CONSTANT
(1/WTL)
ARX=PRE-EXPONENTIAL CONSTANT FOR REACTION RATE CONSTANT
(GRAM/GRAM CAT/HR)
B(J)=SIMPLIFICATION TERM FOR INTEGRATED RATE EQUATION (1/WTL)
C(J)=CALCULATED OUTLET CONCENTRATION IN CONVERGENCE LOOP(WTL)
CG1=A=ASSUMED OUTLET CONCENTRATION IN CONVERGENCE LOOP (WTL)
CR(J,K)=CONVERGED VALUE FOR OUTLET CONCENTRATION FOR DATA
POINT J, GROUP K (WTL)
CP1=WEIGHT PERCENT PRODUCT INTRODUCED IN FEED (WTL)
CRAD=CATALYST PARTICLE RADIUS (CM)
CR22=OUTLET CONCENTRATION FOR DATA POINT 22 (WTL)
CR1=INLET CONCENTRATION (WTL)
CSTOR=STORAGE VARIABLE FOR OUTLET CONCENTRATION IN EFF FACTOR
LOOP (WTL)
C1(J)=INLET CONCENTRATION (WTL)
DAB(J)=FREE LIQUID DIFFUSIVITY OF A IN SOLVENT B (50 CM/SEC)
DEFF(J)=EFFECTIVE DIFFUSIVITY OF A IN SOLVENT B (50 CM/SEC)
DEL=INCREMENTAL CHANGE IN ASSUMED OUTLET CONCENTRATION (WTL)
DEN=DENSITY OF LIQUID AT TREF (GRAM/CC)
DENS(J)=DENSITY OF LIQUID AT DATA POINT J (GRAM/CC)
D1-DS=CONSTANTS USED IN LIQUID DENSITY CALCULATION
E=EFFECTIVENESS FACTOR
E1(J)=EFFECTIVENESS FACTOR FOR DATA POINT J
E2(J)=HYDROGEN HEAT OF ADSORPTION (CAL/GMOLE)
EP1(J)=PRODUCT HEAT OF ADSORPTION (CAL/GMOLE)
ER(J)=REACTANT HEAT OF ADSORPTION (CAL/GMOLE)
ERX(J)=REACTION ACTIVATION ENERGY (CAL/GMOLE)
FFF=FUNCTION TO BE FITTED
FITM(J)=FITTED VALUE FOR J-TH DATA POINT
FL=INITIAL VALUE OF FLAMB, THE RELATIVE AMOUNT BY WHICH THE
DIAGONAL COEFFICIENTS ARE AUGMENTED
FOBJ=RETURNS THE FINAL VALUE OF PHI, THE WEIGHTED SUM OF
SQUARES

H=CONSTANT USED IN EFFECTIVENESS FACTOR CALCULATION
K1=CONSTANT USED IN DIFFUSIVITY CALCULATION
KH2(J)=HYDROGEN ADSORPTION EQUILIBRIUM CONSTANT (1/WTL)
KH2REF=HYDROGEN ADSORPTION EQUILIBRIUM CONSTANT AT REFERENCE
TEMPERATURE (1/PSI)
KNTP=COUNTER FOR PRESSURE GROUP IN DATA SET GENERATOR
KNTT=COUNTER FOR TEMPERATURE GROUP IN DATA SET GENERATOR
KOB=OBSERVED REACTION RATE CONSTANT (1/HR)
KOUNT=COUNTER IN OUTLET CONCENTRATION CONVERGENCE LOOP
KOWNT=COUNTER IN EFFECTIVENESS FACTOR CALCULATION
KP(J)=PRODUCT ADSORPTION EQUILIBRIUM CONSTANT (1/WTL)
KR=LOGICAL UNIT NUMBER FOR THE READER
KRE(J)=REACTANT ADSORPTION EQUILIBRIUM CONSTANT (1/WTL)
KRK(J)=REACTION EQUILIBRIUM CONSTANT (GRAM/GRAM CAT/HR)
KW=LOGICAL UNIT NUMBER OF THE PRINTER
LL=MEMBER NUMBER FOR LIQUID HOURLY SPACE VELOCITY GROUP
LP=MEMBER NUMBER FOR PRESSURE GROUP
LT=MEMBER NUMBER FOR TEMPERATURE GROUP
M=NUMBER OF DIFFERENT SETS OF ADSORPTION EQUILIBRIUM TERMS
MNBK(J)=NONZERO IF K1(J) IS TO BE HELD CONSTANT
MATRX=NONZERO IF STATISTICAL ERRORS ARE TO BE CALCULATED
MAX=MAXIMUM ITERATIONS IN OUTLET CONCENTRATION LOOP
MAXE=MAXIMUM NO. OF ITERATIONS IN THE EFF. FACTOR CALCULATION
MAXIT=MAXIMUM ITERATIONS IN MARQUARDT DATA FIT
METH=DETERMINES CONVERGENCE METHOD USED IN DATA FIT
MN=NO. OF COMBINATIONS OF M AND N
MWB=MOLECULAR WEIGHT OF SOLVENT LIQUID (G/GMOLE)
MWN2=MOLECULAR WEIGHT OF HYDROGEN (G/GMOLE)
MWP=MOLECULAR WEIGHT OF REACTION PRODUCT (G/GMOLE)
MWR=MOLECULAR WEIGHT OF REACTANT (G/GMOLE)
MWS=MOLECULAR WEIGHT OF ELEMENTAL SULFUR (G/GMOLE)
N=NUMBER OF DIFFERENT SETS OF VALUES FOR ACTIVATION ENERGY
AND HEATS OF ADSORPTION
NL=NUMBER OF MEMBERS IN LIQUID HOURLY SPACE VELOCITY GROUP
NML=LOGICAL UNIT NUMBER IN OUTLET CONCENTRATION STORAGE ARRAY
NP=NUMBER OF MEMBERS IN PRESSURE GROUP
NPTS=NUMBER OF POINTS IN THE DATA SET
NT=NUMBER OF MEMBERS IN TEMPERATURE GROUP
NTEMP=NUMBER OF TEMPERATURES AT WHICH A UNIQUE FIT IS TO BE
MADE
NTRAC=USER PRINT CONTROL
NV=NUMBER OF PARAMETERS IN FUNCTION TO BE FIT
P(J)=PRESSURE FOR DATA POINT J (PSI)
P1(J)=J-TH VALUE IN PRESSURE GROUP (PSI)
PC=CRITICAL PRESSURE OF SOLVENT (ATM)
PRAD=AVERAGE CATALYST PORE RADIUS (ANGSTROMS)
Q=CONSTANT USED IN VISCOSITY CALCULATION
R=IDEAL GAS CONSTANT (CAL/GMOLE/K)
R=IDEAL GAS CONSTANT
RP(J)=RATIO OF KP(J) : KH2REF AT THE REFERENCE TEMPERATURE
RK(J)=RATIO OF KR(J) : KH2REF AT THE REFERENCE TEMPERATURE
S(J)=SOLUBILITY OF HYDROGEN IN SOLVENT (WTL)
S1=CONSTANT USED IN SOLUBILITY CALCULATION
S2=CONSTANT USED IN SOLUBILITY CALCULATION
S12=SIZE OF REACTANT MOLECULE (ANGSTROMS)
T1(J)=TEMPERATURE FOR DATA POINT J (K)
T1(J)=J-TH VALUE IN TEMPERATURE GROUP (K)
TC=CRITICAL TEMPERATURE OF SOLVENT (K)
TEMP(J)=J-TH OF NT DIFFERENT TEMPERATURES IN THE DATA SET (F)
TERM(J)=SIMPLIFICATION TERM FOR INTEGRATED RATE EQUATION

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211 DEL=DEL/10.
212 CG1=CG2
213 CF1=CF2
214 GO TO 240
215 262 CG1=CG2
216 CF1=CF2
217 GO TO 240
218 265 DEL=DEL/10
219 270 CG3=CG2*DEL
220 CG4=CG2*DEL
221 IF (CG3.LE.0.0) CG3=0.000001
222 IF (CG4.LE.0.0) CG4=0.000001
223 CF2=CR1*(CF1+CR1)*DLOG(CR1/CG3)/([KROKP(L)*E-1.]-WT*S(L)*E=100.*
  *KRX(L)*KM2(L)*KROKP(L)/ALHSV(L)/VR/DENS(L)/[1.+KM2(L)*S(L)]/
  *([KROKP(L)*E-1.]
224 CF4=CR1*(CF1+CR1)*DLOG(CR1/CG4)/([KROKP(L)*E-1.]-WT*S(L)*E=100.*
  *KRX(L)*KM2(L)*KROKP(L)/ALHSV(L)/VR/DENS(L)/[1.+KM2(L)*S(L)]/
  *([KROKP(L)*E-1.]
225 IF (DABS(CG2-CF3).LT.DABS(CG2-CF4)) GO TO 275
226 DEL=DEL
227 275 CG1=CG2
228 CG2=CG1*DEL
229 IF (CG2.LE.0.0) CG2=0.000001
230 KOUNT=KOUNT+1
231 CF1=CR1*(CF1+CR1)*DLOG(CR1/CG1)/([KROKP(L)*E-1.]-WT*S(L)*E=100.*
  *KRX(L)*KM2(L)*KROKP(L)/ALHSV(L)/VR/DENS(L)/[1.+KM2(L)*S(L)]/
  *([KROKP(L)*E-1.]
232 CF2=CR1*(CF1+CR1)*DLOG(CR1/CG2)/([KROKP(L)*E-1.]-WT*S(L)*E=100.*
  *KRX(L)*KM2(L)*KROKP(L)/ALHSV(L)/VR/DENS(L)/[1.+KM2(L)*S(L)]/
  *([KROKP(L)*E-1.]
233 IF (L.LT.5) GO TO 278
234 IF (L.LT.4) GO TO 278
235 TERM1=DLOG(CR1/CG2)*A(L)/B(L)/2.
236 TERM2=(CR1**2-CG2**2)*B(L)/A(L)/4.
237 TERM3=CR1
238 TERM4=KRX(L)*KM2(L)*KRE(L)*WT*S(L)*E=100./ALHSV(L)/VR/DENS(L)/[1.+
  *KM2(L)*S(L)]/2./A(L)/B(L)
239 TERMS=TERM1+TERM2+TERM3+TERM4
240 278 IF (KOUNT.GE.MAX) GO TO 285
241 IF ((CG1-CF1)/(CG2-CF2).LT.0.0) GO TO 280
242 GO TO 270
243 280 DEL=DEL/10.
244 IF (DABS(DEL/CG2).LT.0.00001) GO TO 285
245 IF (DABS(DEL).LE.0.000001) GO TO 285
246 GO TO 270
C
C
C
C
C
C
C
C
C
247 285 TR=TK(L)/TC
248 IF (TR.LT.0.98) GO TO 288
249 WRITE(KW,267)TR
250 287 FORMAT(////10X,'THE REDUCED TEMPERATURE ',F8.1,3X,'IS ABOVE THE
  *ACCEPTABLE MAXIMUM IN THE VISCOSITY CALCULATION.////)
251 288 @*TC=(1./S.)/MWB*0.5/PC*(2./3.)
C
C
C
C
C
C
C
C
C
252 V01=0.018174-.02135*TR+.0075*TR*TR
253 V02=.042582-.07574*TR+.0340*TR*TR
254 VIS(L)=(V01+W*V02)/O
255 K1=[1.+[3.*VB/VA)]*(2./3.)*KNUM
256 DAB(L)=K*TK(L)/VIS(L)/VA*(1./3.)
257 DEFF(L)=VR*DAB(L)/TOR*(1.-S12/PRAD)*4.
258 KOB=DLOG(CR1/CG2)*ALHSV(L)
259 H=CRAD*(KOB/DEFF(L)/3600.)*0.5
260 E1(L)=3./H/H*([DEXP(H)+DEXP(-H)]/[DEXP(H)-DEXP(-H)]-1.)
261 IF (INPUT.NE.1) GO TO 70
262 IF (DABS(CG2-CSTORE)/CG2.LT.0.000002) GO TO 290
263 CSTORE=CG2
264 E=E1(L)
265 GO TO 235
266 290 IF (KOWNT.LE.MAXE) GO TO 295
267 WRITE(KW,237)KOWNT,L,J,K
268 237 FORMAT(//5X,'THE MAXIMUM NO. OF ',I4,1X,'ITERATIONS HAS BEEN REA
  *CHED IN THE EFFECTIVENESS FACTOR CALCULATION',/5X,'FOR DATA POINT'
  *,I3,1X,'IN E-SET NO.',I3,1X,'AND K-RATIO NO.',I3,/)
269 285 IF (KOUNT.LE.MAX) GO TO 299
270 WRITE(KW,280)KOUNT,L,J,K
271 280 FORMAT(//5X,'THE MAXIMUM NO. OF ',I4,1X,'ITERATIONS HAS BEEN REA
  *CHED IN THE OUTLET CONCENTRATION CALCULATION',/5X,'FOR DATA POINT'
  *,I3,1X,'IN E-SET NO.',I3,1X,'AND K-RATIO NO.',I3,/)
272 289 NM=(J-1)*M*K
273 CR(NM,L)=CG2
274 IF (L.LT.NPTS) GO TO 230
C
C
C
C
C
C
C
C
C
275 WRITE(KW,*)KRX(1),KM2(1),KRE(1),KP(1)
276 WRITE(KW,310)ERX(J)/1000.,EN2(J)/1000.,EP(J)/1000.,ER(J)/1000.,RP(
  *K),RRIK1, KM2REP*DEXP(-S1/625.-S2)/DEN/MW2
277 310 //5X,'THIS PROGRAM GENERATES A SET OF OUTLET REACT
  *ANT CONCENTRATIONS GIVEN TEMPERATURE, PRESSURE, //5X,'LHSV, AND I
  *LET REACTANT CONCENTRATIONS GIVEN AN INTEGRATED RATE EQUATION AND
  * ITS RATE CONSTANTS. //5X,'IT THEN FITS A KINETIC MODEL EQUATION
  * TO THIS SET OF HYPOTHETICALLY GENERATED DATA.'
  * REACTION A
  * CTIVATION ENERGY =',F8.2,1X,'KCAL/GMOLE',/5X,'HYDROGEN HEAT OF AD
  *SORPTION =',F8.2,1X,'KCAL/GMOLE',/5X,'PRODUCT HEAT OF ADSORPTION
  * =',F8.2,1X,'KCAL/GMOLE',/5X,'REACTANT HEAT OF ADSORPTION =',F8.2,
  * 1X,'KCAL/GMOLE',/5X,'ADSORPTION RATE CONSTANT RATIO K-H2 (1/MOLE
  * X H2) : K-PRODUCT (1/MOLE*H2) =',F8.1,1X,'/38X,'K-H2 (1/MOLE*
  * H2) : K-REACTANT (1/MOLE*H2) =',F8.1,1X,'/5X,'FOR A REFERENCE
  * VALUE FOR K-H2 =',F8.2,1X,'/PSI AT 628K. //5X,'WTL IS THE W
  *EIGHT PERCENT OF ELEMENTAL SULFUR IN THE BULK FLUID.////)
278 311 IF (INPUT.EQ.1) GO TO 314
279 WRITE(KW,312)
280 312 FORMAT(//5X,'THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL
  * TO A SET OF EXPERIMENTAL DST NDS DATA. //5X,'WTL IS THE WEIGHT
  * PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.////)
281 314 WRITE(KW,315)CRAD*20.,PRAD*2.,VP,TOR
282 315 FORMAT(//5X,'CATALYST PROPERTIES ARE ://5X,'PARTICLE DIAMETER *

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THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL TO A SET OF EXPERIMENTAL DBT HDS DATA.

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.800
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (SQ CM/SEC)	EFF FACTOR	IN. CONC (WT%)	FIN. CONC. (WT%)
1	545.0	250.0	1.00	0.335150-01	0.378580-06	0.897300 00	0.243000 01	0.147000 01
2	545.0	250.0	3.00	0.335150-01	0.378580-06	0.896780 00	0.243000 01	0.188000 01
3	545.0	250.0	8.00	0.335150-01	0.378580-06	0.896650 00	0.243000 01	0.219000 01
4	545.0	250.0	8.00	0.335150-01	0.378580-06	0.896600 00	0.243000 01	0.226000 01
5	545.0	350.0	1.00	0.488210-01	0.378580-06	0.896860 00	0.243000 01	0.138000 01
6	545.0	350.0	3.00	0.488210-01	0.378580-06	0.896210 00	0.243000 01	0.192000 01
7	545.0	350.0	8.00	0.488210-01	0.378580-06	0.895910 00	0.243000 01	0.214000 01
8	545.0	350.0	8.00	0.488210-01	0.378580-06	0.895850 00	0.243000 01	0.223000 01
9	545.0	450.0	1.00	0.603270-01	0.378580-06	0.896550 00	0.243000 01	0.128000 01
10	545.0	450.0	3.00	0.603270-01	0.378580-06	0.895790 00	0.243000 01	0.187000 01
11	545.0	450.0	8.00	0.603270-01	0.378580-06	0.895450 00	0.243000 01	0.211000 01
12	545.0	450.0	8.00	0.603270-01	0.378580-06	0.895210 00	0.243000 01	0.220000 01

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.000000 00 0.000000 00 0.000000 00
 IMAX = 0.100000 31 0.100000 21 0.100000 31
 XMIN = -0.100000 31 -0.100000 31 -0.100000 31
 DELMN = 0.100000-07 0.100000-07 0.100000-07

NY = 3 NPTS = 12 LPDMA = 300 LPDMS = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDP = 1 NPLAT = 1 NPMAX = 1000 MAXIT = 80 MXSUB = 25
 CRIT = 0.707110 00 RELDF = 0.100000-07 RELMN = 0.100000-07

PHI (THE SUM OF SQUARES) = 0.383371100 00 LAMBDA = 0.100000 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT.... OSAY(2, 2) = 0.00000000 00 ITERATION 1
 RANK-DEFICIENT NORMAL EQUATIONS IN MARQ. RANK = 2 ORDER OF MATRIX = 3 ITERATION 1

CONVERGED WHEN THE STEP BECAME SMALL.

15 ITERATIONS NF = 92 PHI = 0.24032180-03 FMGN = 0.100000 01 LAMBDA = 0.270680 02
 NORM OF SCALED GRADIENT VECTOR = 0.272820-09
 X = 0.63201680 00 0.18825460 02 0.34851680 00

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.12722780E 01	0.12871741D 01	0.810480-02	0.100000 01	0.810480-02
2	0.11022000E 01	0.10981818D 01	0.400930-02	0.100000 01	0.400930-02
3	0.10528950E 01	0.10518847D 01	0.498920-02	0.100000 01	-0.498920-02
4	0.10367010E 01	0.10377476D 01	-0.104640-02	0.100000 01	-0.104640-02
5	0.12181180E 01	0.13207825D 01	-0.246340-02	0.100000 01	-0.246340-02
6	0.11224020E 01	0.11185011D 01	0.290110-02	0.100000 01	0.290110-02
7	0.10648880E 01	0.10630365D 01	0.185150-02	0.100000 01	0.185150-02
8	0.10438890E 01	0.10493286D 01	-0.577050-02	0.100000 01	-0.577050-02
9	0.13545240E 01	0.13871775D 01	-0.285100-02	0.100000 01	-0.285100-02
10	0.11368870E 01	0.11346072D 01	0.218010-02	0.100000 01	0.218010-02
11	0.10722610E 01	0.10741638D 01	-0.190200-02	0.100000 01	-0.190200-02
12	0.10505390E 01	0.10438682D 01	0.697380-02	0.100000 01	0.697380-02

NUMBER OF DEGREES OF FREEDOM = 0.800000 01
 R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.516720-02
 MAXIMUM SCALED DEVIATION = 0.898920-02

SUBROUTINE MOERR.

QSAV (PT*P, SCALED, WHERE P IS THE JACOBIAN)....

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1   0.1000000D 01
2  -0.8921821D 00  0.1000000D 01
3  -0.9756327D 00  0.8832032D 00  0.1000000D 01

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 9

EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 9 PLUS OR MINUS 0.42428D 01

ACTUAL VALUE OF PHI = 0.24031D-03

RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.51873D-02

MAXIMUM VARIANCE INFLATION FACTOR = 0.99406D 02

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.83201852D 00	0.30871D 01	0.15852D-01
2	0	0.18926464D 02	0.19008D 03	0.98224D 00
3	0	0.34881684D 00	0.13414D 01	0.89316D-02

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K .... 1      2      3
MASK(K).... 0      0      0
J  MASK(J)
1   0      0.10000D 01
2   0      0.88940D 00  0.10000D 01
3   0      0.59508D 00  0.17837D 00  0.10000D 01

```

INTRINSIC MODEL PARAMETERS

FITTED BY $y = [1/x] \ln(1/(1-x))$

X(1) = K(KN)(KR/KP) = 0.8320D 00

X(2) = KN = 0.1883D 02 1/WT%

X(3) = KR/KP = 0.3488D 00

K = 0.8043D-01 WT%/HR

MEAN DEVIATION = 0.01413

AVERAGE PERCENT ERROR = 0.71387

STATEMENTS EXECUTED= 32402

CORE USAGE OBJECT CODE= 61868 BYTES,ARRAY AREA= 89868 BYTES,TOTAL AREA AVAILABLE= 174060 BYTES

DIAGNOSTICS NUMBER OF ERRORS= 0, NUMBER OF WARNINGS= 0, NUMBER OF EXTENSIONS= 18

COMPILE TIME= 0.45 SEC,EXECUTION TIME= 0.38 SEC, 17.35.28 SUNDAY 24 JUL 83 WATFIV - MAR 1980 V2L0

CSSTOP

THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL TO A SET OF EXPERIMENTAL DBT HOS DATA.

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.500
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (SQ CM/SEC)	EFF FACTOR	IN. CONC. (WT%)	FIN. CONC. (WT%)
1	572.0	250.0	1.00	0.34658D-01	0.42408D-06	0.89530D 00	0.24300D 01	0.81000D 00
2	572.0	250.0	3.00	0.34658D-01	0.42408D-06	0.89521D 00	0.24300D 01	0.17400D 01
3	572.0	250.0	5.00	0.34658D-01	0.42408D-06	0.89526D 00	0.24300D 01	0.20800D 01
4	572.0	250.0	8.00	0.34658D-01	0.42408D-06	0.89513D 00	0.24300D 01	0.21700D 01
5	572.0	350.0	1.00	0.48622D-01	0.42408D-06	0.98413D 00	0.24300D 01	0.71000D 00
6	572.0	350.0	3.00	0.48622D-01	0.42408D-06	0.98402D 00	0.24300D 01	0.18000D 01
7	572.0	350.0	5.00	0.48622D-01	0.42408D-06	0.98399D 00	0.24300D 01	0.18700D 01
8	572.0	350.0	8.00	0.48622D-01	0.42408D-06	0.98383D 00	0.24300D 01	0.21100D 01
9	572.0	450.0	12.00	0.62386D-01	0.42408D-06	0.98404D 00	0.24300D 01	0.21800D 01
10	572.0	450.0	1.00	0.62386D-01	0.42408D-06	0.98317D 00	0.24300D 01	0.58000D 00
11	572.0	450.0	3.00	0.62386D-01	0.42408D-06	0.98316D 00	0.24300D 01	0.15000D 01
12	572.0	450.0	5.00	0.62386D-01	0.42408D-06	0.98296D 00	0.24300D 01	0.19000D 01
13	572.0	450.0	8.00	0.62386D-01	0.42408D-06	0.98291D 00	0.24300D 01	0.20600D 01
14	572.0	450.0	12.00	0.62386D-01	0.42408D-06	0.98300D 00	0.24300D 01	0.21500D 01

MARG... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.00000D 00 0.00000D 00 0.00000D 00
 XMAX = 0.10000D 31 0.10000D 31 0.10000D 31
 XMIN = -0.10000D 31 -0.10000D 31 -0.10000D 31
 DELMN = 0.10000D-07 0.10000D-07 0.10000D-07

NV = 3 NPTS = 14 LPDMA = 300 LPDMS = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDP = 1 NPLAT = 1 NPMAX = 1000 MAXIT = 50 MXSUB = 25
 CRIT = 0.70711D 00 RELDF = 0.10000D-07 RELMN = 0.10000D-07

PHI (THE SUM OF SQUARES) = 0.18644402D 01 LAMBDA = 0.10000D 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT... OSAV(2, 2) = 0.000000D 00 ITERATION 1
 RANK-DEFICIENT NORMAL EQUATIONS IN MARG. RANK = 2 ORDER OF MATRIX = 3 ITERATION 1

CONVERGENCE ACHIEVED UNDER THE NPLAT OPTION.

19 ITERATIONS NF = 116 PHI = 0.78687323D-03 FMCH = 0.10000D 01 LAMBDA = 0.88881D 02
 NORM OF SCALED GRADIENT VECTOR = 0.25328D-08
 X = 0.1680122D 01 0.1136383D 02 0.9354837D 00

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	[Y-FIT]/YSIG
1	0.1570230E 01	0.15711830D 01	-0.96254D-03	0.10000D 01	-0.96254D-03
2	0.11752810E 01	0.11720244D 01	0.42571D-02	0.10000D 01	0.42571D-02
3	0.10848840E 01	0.10875028D 01	-0.12638D-01	0.10000D 01	-0.12638D-01
4	0.10578480E 01	0.10447512D 01	0.12887D-01	0.10000D 01	0.12887D-01
5	0.17322700E 01	0.17380388D 01	0.22118D-02	0.10000D 01	0.22118D-02
6	0.12234630E 01	0.12222051D 01	0.12884D-02	0.10000D 01	0.12884D-02
7	0.11088960E 01	0.11094897D 01	-0.90388D-03	0.10000D 01	-0.90388D-03
8	0.10722810E 01	0.10681901D 01	0.60717D-02	0.10000D 01	0.60717D-02
9	0.10528950E 01	0.10681974D 01	-0.13302D-01	0.10000D 01	-0.13302D-01
10	0.18817830E 01	0.18792528D 01	0.24108D-02	0.10000D 01	0.24108D-02
11	0.12605320E 01	0.12700431D 01	-0.95108D-02	0.10000D 01	-0.95108D-02
12	0.11260570E 01	0.11223726D 01	0.50649D-02	0.10000D 01	0.50649D-02
13	0.10848840E 01	0.10755860D 01	0.92765D-02	0.10000D 01	0.92765D-02
14	0.10824690E 01	0.10888255D 01	-0.61855D-02	0.10000D 01	-0.61855D-02

NUMBER OF DEGREES OF FREEDOM = 0.11000D 02

R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.84677D-02

MAXIMUM SCALED DEVIATION = 0.13302D-01

SUBROUTINE MOERR.

OSAY (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.1000000 01
2  -0.3684334D 00  0.1000000 01
3  -0.8758311D 00  0.8608114D 00  0.1000000 01

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 11

EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 11 PLUS OR MINUS 0.46804D 01

ACTUAL VALUE OF PHI = 0.78687D-03

RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.84678D-02

MAXIMUM VARIANCE INFLATION FACTOR = 0.78275D 02

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.16601215D 01	0.32462D 01	0.27456D-01
2	0	0.11353632D 02	0.46318D 02	0.40867D 00
3	0	0.93846271D 00	0.12442D 01	0.10523D-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K .... 1      2      3
MASK(K).... 0      0      0
J  MASK(J)
1  0      0.10000D 01
2  0      0.85855D 00  0.10000D 01
3  0      0.62831D 00  0.14861D 00  0.10000D 01

```

INTRINSIC MODEL PARAMETERS

FITTED BY $Y = (1/X) \ln(1/(1-X))$

$X(1) = K(KH)(KR/KP) = 0.1660D 01$

$X(2) = KH = 0.1135D 02 \quad 1/WT\%$

$X(3) = KR/KP = 0.9385D 00$

$K = 0.1583D 00 \quad WT\%/HR$

MEAN DEVIATION = 0.02182

AVERAGE PERCENT ERROR = 1.09811

STATEMENTS EXECUTED: 40145

CODE USAGE OBJECT CODE= 61666 BYTES,ARRAY AREA= 88656 BYTES,TOTAL AREA AVAILABLE= 174080 BYTES

DIAGNOSTICS NUMBER OF ERRORS= 0, NUMBER OF WARNINGS= 0, NUMBER OF EXTENSIONS= 18

COMPILE TIME: 0.46 SEC,EXECUTION TIME: 0.47 SEC, 17.38.47 SUNDAY 24 JUL 83 WATPIV - MAR 1980 V2L0

CSSTOP

THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL TO A SET OF EXPERIMENTAL DBT HDS DATA.

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.800
 TORTUOSITY FACTOR = 2.80

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	N2 SOLUBILITY (WT%)	EFF DIFF (50 CM/SEC)	EFF FACTOR	IN. CONC. (WT%)	FIN. CONC. (WT%)
1	590.0	250.0	1.00	0.35408D-01	0.45808D-08	0.99147D 00	0.24300D 01	0.28000D 00
2	590.0	250.0	3.00	0.35408D-01	0.45808D-08	0.99223D 00	0.24300D 01	0.13500D 01
3	590.0	250.0	5.00	0.35408D-01	0.45808D-08	0.99250D 00	0.24300D 01	0.18300D 01
4	590.0	250.0	8.00	0.35408D-01	0.45808D-08	0.99288D 00	0.24300D 01	0.20200D 01
5	590.0	250.0	12.00	0.35408D-01	0.45808D-08	0.99253D 00	0.24300D 01	0.21100D 01
6	590.0	250.0	15.00	0.35408D-01	0.45808D-08	0.99242D 00	0.24300D 01	0.21800D 01
7	590.0	350.0	1.00	0.48572D-01	0.45808D-08	0.98882D 00	0.24300D 01	0.19000D 00
8	590.0	350.0	3.00	0.48572D-01	0.45808D-08	0.98991D 00	0.24300D 01	0.11300D 01
9	590.0	350.0	6.00	0.48572D-01	0.45808D-08	0.99027D 00	0.24300D 01	0.18800D 01
10	590.0	350.0	8.00	0.48572D-01	0.45808D-08	0.99047D 00	0.24300D 01	0.18100D 01
11	590.0	350.0	12.00	0.48572D-01	0.45808D-08	0.99051D 00	0.24300D 01	0.20200D 01
12	590.0	350.0	15.00	0.48572D-01	0.45808D-08	0.99089D 00	0.24300D 01	0.21100D 01
13	590.0	450.0	3.00	0.83738D-01	0.45808D-08	0.98793D 00	0.24300D 01	0.87000D 00
14	590.0	450.0	6.00	0.83738D-01	0.45808D-08	0.98881D 00	0.24300D 01	0.15700D 01
15	590.0	450.0	8.00	0.83738D-01	0.45808D-08	0.98888D 00	0.24300D 01	0.18200D 01
16	590.0	450.0	12.00	0.83738D-01	0.45808D-08	0.98888D 00	0.24300D 01	0.18800D 01
17	590.0	450.0	15.00	0.83738D-01	0.45808D-08	0.98881D 00	0.24300D 01	0.20800D 01

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.00000D 00 0.00000D 00 0.00000D 00
 XMAX = 0.10000D 31 0.10000D 31 0.10000D 31
 XMIN = -0.10000D 31 -0.10000D 31 -0.10000D 31
 DELMH = 0.10000D-07 0.10000D-07 0.10000D-07

NV = 3 NPTS = 17 LPDMA = 300 LPDMB = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDF = 1 NPLAT = 1 NPMAX = 1000 MAXIT = 80 MXSUB = 26
 CRIT = 0.70711D 00 RELDF = 0.10000D-07 RELMH = 0.10000D-07

PHI (THE SUM OF SQUARES) = 0.54860081D 01 LAMBDA = 0.10000D 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT..... OSAV(2, 2) = 0.0000000D 00 ITERATION 1
 RANK-DEFICIENT NORMAL EQUATIONS IN MARQ. RANK = 2 ORDER OF MATRIX = -3 ITERATION 1

CONVERGENCE ACHIEVED UNDER THE NPLAT OPTION.

14 ITERATIONS NF = 80 PHI = 0.21158386D-02 FMEN = 0.10000D 01 LAMBDA = 0.10106D-03
 NORM OF SCALED GRADIENT VECTOR = 0.11088D-08
 X = 0.3582173D 01 0.8178806D 01 0.1398840D 01

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.22837700E 01	0.22815308D 01	0.22392D-02	0.10000D 01	0.22392D-02
2	0.13228190E 01	0.13142754D 01	0.82438D-02	0.10000D 01	0.82438D-02
3	0.11484790E 01	0.11442887D 01	0.41907D-02	0.10000D 01	0.41907D-02
4	0.10852400E 01	0.11089738D 01	-0.11733D-01	0.10000D 01	-0.11733D-01
5	0.10722810E 01	0.10488248D 01	0.23837D-01	0.10000D 01	0.23837D-01
6	0.10852840E 01	0.10830894D 01	-0.27828D-01	0.10000D 01	-0.27828D-01
7	0.27848000E 01	0.27872271D 01	-0.24270D-02	0.10000D 01	-0.24270D-02
8	0.14312200E 01	0.14275880D 01	0.38341D-02	0.10000D 01	0.38341D-02
9	0.11988750E 01	0.11882758D 01	0.98988D-02	0.10000D 01	0.98988D-02
10	0.11282200E 01	0.11258358D 01	-0.71835D-03	0.10000D 01	-0.71835D-03
11	0.10826210E 01	0.10882024D 01	0.44184D-02	0.10000D 01	0.44184D-02
12	0.10722810E 01	0.10882178D 01	-0.18956D-01	0.10000D 01	-0.18956D-01
13	0.16284870E 01	0.16308008D 01	-0.24138D-02	0.10000D 01	-0.24138D-02
14	0.12242370E 01	0.12421878D 01	-0.78301D-02	0.10000D 01	-0.78301D-02
15	0.1514790E 01	0.1448440D 01	0.88358D-02	0.10000D 01	0.88358D-02
16	0.11113200E 01	0.11040808D 01	0.72397D-02	0.10000D 01	0.72397D-02
17	0.10874320E 01	0.10884880D 01	-0.10283D-02	0.10000D 01	-0.10283D-02

NUMBER OF DEGREES OF FREEDOM = 0.14000D 02

R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.12294D-01
 MAXIMUM SCALED DEVIATION = 0.27626D-01

SUBROUTINE MOERR.

OSAY (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.100000D 01
2  -0.887188D 00  0.100000D 01
3  -0.988630D 00  0.887144D 00  0.100000D 01

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 14
 EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 14 PLUS OR MINUS 0.62616D 01
 ACTUAL VALUE OF PHI = 0.21189D-02
 RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.12294D-01

MAXIMUM VARIANCE INFLATION FACTOR = 0.48698D 02

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.36821734D 01	0.34006D 01	0.41805D-01
2	0	0.81766058D 01	0.24638D 02	0.30537D 00
3	0	0.12868401D 01	0.88266D 00	0.11837D-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K .... 1      2      3
      MASK(K).... 0      0      0
J      MASK(J)
1      0      0.10000D 01
2      0      0.82852D 00  0.10000D 01
3      0      0.43806D 00 -0.11886D 00  0.10000D 01

```

INTRINSIC MODEL PARAMETERS

FITTED BY $Y = (1/X) \ln(1/(1-X))$
 $X(1) = K(KN)(KR/KP) = 0.3682D 01$
 $X(2) = KN = 0.8177D 01$ 1/WT%
 $X(3) = KR/KP = 0.1287D 01$
 $K = 0.2138D 00$ WT%/HR

MEAN DEVIATION = 0.02857
 AVERAGE PERCENT ERROR = 1.50215

STATEMENTS EXECUTED: 32475

CORE USAGE OBJECT CODE: 81656 BYTES, ARRAY AREA: 68556 BYTES, TOTAL AREA AVAILABLE: 174060 BYTES

DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 16

COMPILE TIME: 0.46 SEC, EXECUTION TIME: 0.41 SEC, 17.43.26 SUNDAY 24 JUL 63 WATFIV - MAR 1960 V2LO

CBSTOP

THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL TO A SET OF EXPERIMENTAL DBY NOS DATA.

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.500
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (SQ CM/SEC)	EFF FACTOR	IN. CONC. (WT%)	FIN. CONC. (WT%)
1	817.0	250.0	3.00	0.38515D-01	0.51574D-06	0.98488D 00	0.24300D 01	0.80000D 00
2	817.0	250.0	6.00	0.38515D-01	0.51574D-06	0.98580D 00	0.24300D 01	0.13200D 01
3	817.0	250.0	9.00	0.38515D-01	0.51574D-06	0.98627D 00	0.24300D 01	0.16400D 01
4	817.0	250.0	12.00	0.38515D-01	0.51574D-06	0.98628D 00	0.24300D 01	0.18100D 01
5	817.0	250.0	15.00	0.38515D-01	0.51574D-06	0.98658D 00	0.24300D 01	0.19300D 01
6	817.0	350.0	3.00	0.51121D-01	0.51574D-06	0.97821D 00	0.24300D 01	0.40000D 00
7	817.0	350.0	6.00	0.51121D-01	0.51574D-06	0.98104D 00	0.24300D 01	0.10700D 01
8	817.0	350.0	9.00	0.51121D-01	0.51574D-06	0.98180D 00	0.24300D 01	0.14300D 01
9	817.0	350.0	12.00	0.51121D-01	0.51574D-06	0.98208D 00	0.24300D 01	0.16800D 01
10	817.0	350.0	15.00	0.51121D-01	0.51574D-06	0.98231D 00	0.24300D 01	0.17800D 01
11	817.0	450.0	3.00	0.65727D-01	0.51574D-06	0.97484D 00	0.24300D 01	0.27000D 00
12	817.0	450.0	6.00	0.65727D-01	0.51574D-06	0.97688D 00	0.24300D 01	0.88000D 00
13	817.0	450.0	9.00	0.65727D-01	0.51574D-06	0.97782D 00	0.24300D 01	0.12700D 01
14	817.0	450.0	12.00	0.65727D-01	0.51574D-06	0.97810D 00	0.24300D 01	0.15100D 01
15	817.0	450.0	15.00	0.65727D-01	0.51574D-06	0.97841D 00	0.24300D 01	0.16700D 01

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.00000D 00 0.00000D 00 0.00000D 00
 XMAX = 0.10000D 31 0.10000D 31 0.10000D 31
 XMIN = -0.10000D 31 -0.10000D 31 -0.10000D 31
 BELMN = 0.10000D-07 0.10000D-07 0.10000D-07

NV = 3 NPTS = 15 LPDHA = 300 LPDHB = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KBRDF = 1 NPLAT = 1 NPMAX = 1000 MAXIT = 50 MXSUB = 25
 CRIT = 0.70711D 00 RELDF = 0.10000D-07 RELMN = 0.10000D-07

PHI (THE SUM OF SQUARES) = 0.52831752D 01 LAMBDA = 0.10000D 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT.... QSAV(2, 2) = 0.0000000D 00 ITERATION 1
 RANK-DEFICIENT NORMAL EQUATIONS IN MARQ. RANK = 2 ORDER OF MATRIX = 3 ITERATION 1

CONVERGED WHEN THE STEP BECAME SMALL.

15 ITERATIONS NP = 63 PHI = 0.17811584D-02 FMCN = 0.10000D 01 LAMBDA = 0.61752D-08
 NORM OF SCALED GRADIENT VECTOR = 0.28515D-09
 X = 0.7075803D 01 0.5416278D 01 0.1635184D 01

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.17884220E 01	0.18028783D 01	-0.13454D-01	0.10000D 01	-0.13454D-01
2	0.13358720E 01	0.13338818D 01	0.19910D-02	0.10000D 01	0.19910D-02
3	0.12094470E 01	0.12171841D 01	-0.77182D-02	0.10000D 01	-0.77182D-02
4	0.11648010E 01	0.11403773D 01	0.14125D-01	0.10000D 01	0.14125D-01
5	0.11192040E 01	0.11271803D 01	-0.75762D-02	0.10000D 01	-0.75762D-02
6	0.21588880E 01	0.21321586D 01	0.27527D-01	0.10000D 01	0.27527D-01
7	0.14555810E 01	0.14844877D 01	0.10741D-02	0.10000D 01	0.10741D-02
8	0.12884260E 01	0.12807299D 01	0.78985D-02	0.10000D 01	0.78985D-02
9	0.12060140E 01	0.12120785D 01	-0.59820D-02	0.10000D 01	-0.59820D-02
10	0.11895120E 01	0.11891224D 01	0.85103D-02	0.10000D 01	0.85103D-02
11	0.24718770E 01	0.24887723D 01	-0.16895D-01	0.10000D 01	-0.16895D-01
12	0.15823830E 01	0.15846487D 01	0.77471D-02	0.10000D 01	0.77471D-02
13	0.13582790E 01	0.13874277D 01	0.18519D-02	0.10000D 01	0.18519D-02
14	0.12566830E 01	0.12589638D 01	0.11952D-03	0.10000D 01	0.11952D-03
15	0.11982290E 01	0.12011081D 01	-0.18789D-02	0.10000D 01	-0.18789D-02

NUMBER OF DEGREES OF FREEDOM = 0.12000D 02
 R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.12143D-01

MAXIMUM SCALED DEVIATION = 0.27527D-01

SUBROUTINE MOERR.

QSAY (PT*P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.100000D 01
2  -0.9541785D 00  0.100000D 01
3  -0.9810201D 00  0.9532284D 00  0.100000D 01

```

NUMBER OF DEGREES OF FREEDOM [N.D.F.] = (NPTS-NACTY) = 12

EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 12 PLUS OR MINUS 0.48880D 01

ACTUAL VALUE OF PHI = 0.17512D-02

RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.12183D-01

MAXIMUM VARIANCE INFLATION FACTOR = 0.85450D 02

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERRDR	RESCALED ERRDR
1	0	0.70758028D 01	0.85148D 01	0.10374D 00
2	0	0.54152757D 01	0.18873D 02	0.22893D 00
3	0	0.15351535D 01	0.14444D 01	0.17586D-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K ..... 1      2      3
MASK(K).... 0      0      0
J  MASK(J)
1  0      0.10000D 01
2  0      0.83150D 00  0.10000D 01
3  0      0.78487D 00  0.33807D 00  0.10000D 01

```

INTRINSIC MODEL PARAMETERS

FITTED BY $Y = \{1/X\}LH\{1/(1-X)\}$

X(1) = K(KH)[KR/KP] = 0.7075D 01

X(2) = KH = 0.5415D 01 1/WT%

X(3) = KR/KP = 0.1535D 01

K = 0.8511D 00 WT%/HR

MEAN DEVIATION = 0.01450

AVERAGE PERCENT ERROR = 1.27822

STATEMENTS EXECUTED: 28256

CORE USAGE OBJECT CODE: 51856 BYTES, ARRAY AREA: 58856 BYTES, TOTAL AREA AVAILABLE: 174080 BYTES

DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 18

COMPILE TIME: 0.45 SEC, EXECUTION TIME: 0.35 SEC, 17.30.22 SUNDAY 26 JUL 83 WATPIV - MAR 1980 V2LO

CSSTOP

THIS PROGRAM FITS AN INTRINSIC KINETIC RATE MODEL TO A SET OF EXPERIMENTAL DBT NDS DATA.

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.500
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (SQ CM/SEC)	EFF FACTOR	IN. CONC. (WT%)	FIN. CONC. (WT%)
1	552.0	250.0	8.00	0.383100-01	0.833770-06	0.974840 00	0.243000 01	0.830000 00
2	552.0	250.0	8.00	0.383100-01	0.833770-06	0.977250 00	0.243000 01	0.108000 01
3	552.0	250.0	12.00	0.383100-01	0.833770-06	0.978260 00	0.243000 01	0.138000 01
4	552.0	250.0	15.00	0.383100-01	0.833770-06	0.978930 00	0.243000 01	0.155000 01
5	552.0	350.0	8.00	0.528350-01	0.833770-06	0.983420 00	0.243000 01	0.330000 00
6	552.0	350.0	8.00	0.528350-01	0.833770-06	0.975000 00	0.243000 01	0.750000 00
7	552.0	350.0	12.00	0.528350-01	0.833770-06	0.988330 00	0.243000 01	0.108000 01
8	552.0	350.0	15.00	0.528350-01	0.833770-06	0.970680 00	0.243000 01	0.128000 01
9	552.0	450.0	8.00	0.588580-01	0.833770-06	0.982050 00	0.243000 01	0.170000 00
10	552.0	450.0	8.00	0.588580-01	0.833770-06	0.957970 00	0.243000 01	0.520000 00
11	552.0	450.0	12.00	0.588580-01	0.833770-06	0.980780 00	0.243000 01	0.830000 00
12	552.0	450.0	15.00	0.588580-01	0.833770-06	0.982460 00	0.243000 01	0.107000 01

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0
 X = 0.000000 00 0.000000 00 0.000000 00
 XMAX = 0.100000 31 0.100000 31 0.100000 31
 XMIN = -0.100000 31 -0.100000 31 -0.100000 31
 DELMN = 0.100000-07 0.100000-07 0.100000-07

NV = 3 NPTS = 12 LPDMA = 300 LPDME = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KBRDF = 1 NPLAT = 1 NPMAX = 1000 MAXIT = 50 MXSUB = 25
 CRIT = 0.707110 00 RELDF = 0.100000-07 RELMN = 0.100000-07

PHI (THE SUM OF SQUARES) = 0.888860530 01 LAMBDA = 0.100000 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT... OSAY(2, 2) = 0.00000000 00 ITERATION 1
 RANK-DEFICIENT NORMAL EQUATIONS IN MARQ. RANK = 2 ORDER OF MATRIX = 3 ITERATION 1

CONVERGED WHEN THE STEP BECAME SMALL.

17 ITERATIONS NF = 88 PHI = 0.800435540-03 PMGN = 0.100000 01 LAMBDA = 0.858550-01

NORM OF SCALED GRADIENT VECTOR = 0.800770-10

X = 0.18803470 02 0.28058380 01 0.24355820 01

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.18224010E 01	0.182139040 01	0.101070-02	0.100000 01	0.101070-02
2	0.14596730E 01	0.145748830 01	-0.779250-02	0.100000 01	-0.779250-02
3	0.13161190E 01	0.131478600 01	-0.235510-02	0.100000 01	-0.235510-02
4	0.12418090E 01	0.124136380 01	-0.244860-03	0.100000 01	-0.244860-03
5	0.23102870E 01	0.231064460 01	-0.346590-03	0.100000 01	-0.346590-03
6	0.17003820E 01	0.170409120 01	-0.370890-02	0.100000 01	-0.370890-02
7	0.14715190E 01	0.148922830 01	-0.122810-01	0.100000 01	-0.122810-01
8	0.13498200E 01	0.135087000 01	-0.104880-02	0.100000 01	-0.104880-02
9	0.28889240E 01	0.288273010 01	0.719420-02	0.100000 01	0.719420-02
10	0.18815790E 01	0.187781410 01	-0.152350-01	0.100000 01	-0.152350-01
11	0.18314720E 01	0.183304850 01	-0.157890-02	0.100000 01	-0.157890-02
12	0.14688510E 01	0.146888640 01	0.859550-02	0.100000 01	0.859550-02

NUMBER OF DEGREES OF FREEDOM = 0.800000 01

R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.818760-02

MAXIMUM SCALED DEVIATION = 0.182350-01

SUBROUTINE MOERR.

OSAV (PT*P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.1000000 01
2  -0.88074330 00  0.1000000 01
3  -0.88814780 00  0.88484280 00  0.1000000 01

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 8

EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 8 PLUS OR MINUS 0.424280 01

ACTUAL VALUE OF PHI = 0.800440-03

RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.818780-02

MAXIMUM VARIANCE INFLATION FACTOR = 0.148480 03

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.188034710 02	0.181050 02	0.188080 00
2	0	0.280883810 01	0.114720 02	0.837070-01
3	0	0.243888200 01	0.238700 01	0.188780-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

```

      K .... 1      2      3
MASK(K).... 0      0      0
J  MASK(J)
1  0      0.100000 01
2  0      0.830700 00  0.100000 01
3  0      0.808070 00  0.831700 00  0.100000 01

```

INTRINSIC MODEL PARAMETERS

FITTED BY $Y = [1/X] \ln[1/(1-X)]$

X(1) = K(KH)[KR/KP] = 0.18800 02

X(2) = KH = 0.28080 01 1/WT%

X(3) = KR/KP = 0.24380 01

K = 0.28480 01 WT%/HR

MEAN DEVIATION = 0.00828

AVERAGE PERCENT ERROR = 0.74808

STATEMENTS EXECUTED: 27888

CORE USAGE OBJECT CODE: 81856 BYTES, ARRAY AREA: 88856 BYTES, TOTAL AREA AVAILABLE: 174080 BYTES

DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 18

COMPILE TIME: 0.46 SEC, EXECUTION TIME: 0.33 SEC, 17.46.53 SUNDAY 24 JUL 83 WATFIV - MAR 1980 Y2L0

CSSTOP

APPENDIX G

LISTING OF PARAMETER SENSITIVITY PROGRAM
AND SAMPLE DATA FIT CALCULATION RESULTS


```

SJOB
C
C
C *****
C *
C * PARAMETER SENSITIVITY CALCULATIONS
C *
C * DATA GENERATED FROM INTRINSIC DIBENZOTHIOPHENE HDS MODEL
C *
C * FIT TO N-TH ORDER GLOBAL MODEL
C *
C * OPERATING CONDITIONS FROM ESPINO
C *****
C
C
1  IMPLICIT REAL*8 (A-H,O-Z)
2  INTEGER Z2
3  REAL*8 KRX,KH2,KP,KRE,KH2REF,K1,H,KOB,KNUM
4  REAL*8 KRDKP
5  DIMENSION KRX(27),KH2(27),KROKP(27),C2(27)
6  EXTERNAL EXFIT
7  DOUBLE PRECISION X,FIT
8  COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
9  *ERR(20,21),FDBJ,NV,NTRAC,MATRX,MASK(20),
10 *NPMAX,NFLAT,JVARY,EXTRA,KFLAG,NOREP,KERFL,KW
11 *COMMON /NLS4/ FLAME,FNU,RELD,RELMN,METHD,KALCP,KORDP,
12 *MAXIT,LEQU,MXSUE,MXUPD
13 *COMMON /CDAT/ FIT(300),Y(300),YSIG(300),NPTS
14 *COMMON /CSTOR/ T(27),P(27),ALHSV(27),C1(27),TERM(27),T1(10),P1(10)
15 *ALHSV(10),E1(27),DAB(27),DEFF(27),S(27),VIS(27),TEMP(10),
16 *DENS(27),TK(27),C2C(27),C2D(27),DEV,DEV1,DEV2,CP1,WT,VR,ORDER,
17 *Z,CMTN,HI,NDAT
18 *OEXP(ARG)=DEXP(ARG)
19 CALL STSET
C
C
C *****
C *
C * HAROUARDT VARIABLES
C *
C *****
C
14  FL=1.
15  KR=6
16  KW=6
17  MATRX=1
18  NPMAX=4000
19  MAXIT=400
20  METHD=1
21  NTRAC=0
22  NV=4
23  XMIN(1)=0.0
24  XMIN(2)=0.0
25  XMIN(3)=0.0
26  XMAX(4)=0.9999
27  X(4)=0.5
28  MASK(3)=1
29  X(3)=0.0
C
30  X(2)=3.0D+04
31  X(1)=1.0D+10
32  X1=X(1)
33  X2=X(2)
34  X3=X(3)
35  X4=X(4)
C
C *****
C *
C * MODEL CONSTANTS AND VARIABLES
C *
C *****
C
36  AH2=1.1848D-07
37  ARDP=1.3178D+07
38  ARX=6.1278D+13
39  CP=0.0
40  CRAD=0.0106
41  CRZ=0.5
42  CR1=2.43
43  EH2=20934.7
44  ERDP=18971.8
45  ERX=38408.7
46  EOLD=0.5
47  MWS=132.206
48  MWN2=2.015
49  MWP=24.08
50  MWN=184.27
51  MWS=132.064
C
52  NL=1
53  NL=5
54  NP=5
55  NP=1
56  NT=1
57  NT=5
58  NPTS=NT*NP*NL
59  ORDER=0.0
60  PC=34.7
61  PRAD=14.0
62  R=1.8872
63  S1=718.0
64  S2=12.24
65  S12=10.0
66  TC=718.0
67  TOR=2.5
68  TREF=625.0
69  TREF1=283.0
70  VA=162.0
71  VB=147.0
72  VBREF=135.67
73  VF=0.5
74  VR=15.0
75  W=0.303
76  WT=6.0
77  Z2=1
C
C *****

```

```

C      *
C      * DATA MAY BE GENERATED IN TWO MANNERS:
C      * 1 SUPPLY ALL PRE-EXPONENTIAL AND EXPONENTIAL CONSTANTS
C      * 2 SUPPLY EXPONENTIAL CONSTANTS AND RATIOS OF EQUILIBRIUM
C      *   CONSTANTS AT A SPECIFIED REFERENCE TEMPERATURE
C      *
C      *-----*
78      HI=1
79      KNUM=17.E0-8
80      IF (VA/VB.GE.2.5) KNUM=8.2D-8
81      IF (VA/VB.LE.1.0) KNUM=25.2D-8
C
C      *-----*
C      * READ TEMPERATURES, PRESSURES, LHSVS
C      *
C      *-----*
82      DO 110 K=1,NT
83      READ(KR,100)T1(K)
84      100  FORMAT(7X,F10.5)
85      T1(K)=T1(K)+480.
86      110  CONTINUE
87      DO 130 K=1,NP
88      READ(KR,120)P1(K)
89      120  FORMAT(7X,F10.5)
90      130  CONTINUE
91      DO 150 K=1,NL
92      READ(KR,140)ALHSV1(K)
93      140  FORMAT(7X,F10.5)
94      150  CONTINUE
C
C      *-----*
C      * COMBINE TEMP, PRESS, LHSV TO FORM DATA SET
C      *
C      *-----*
95      LT=1
96      LP=1
97      LL=1
98      KNTP=0
99      KNTP=0
100     DD 210 L=1,NPTS
101     KNTP=KNTP+1
102     KNTP=KNTP+1
103     T(L)=T1(LT)
104     P(L)=P1(LP)
105     ALHSV(L)=ALHSV1(LL)
106     IF (KNTP.NE.NP) GO TO 180
107     KNTP=0
108     LT=LT+1
109     180  IF (LP.NE.NP) GO TO 180
110     IF (KNTP.EQ.NL) LP=0
C
111     180  IF (KNTP.NE.NL) GO TO 200
112     KNTP=0
113     LP=LP+1
114     200  IF (LL.EQ.NL) LL=0
115     LL=LL+1
116     210  CONTINUE
C
C      *-----*
C      * START EQUILIBRIUM CONSTANT CALCULATIONS
C      *
C      * PRE-EXPONENTIAL CONSTANTS
C      * ARX-REACTION
C      * AN2-HYDROGEN
C      * AP -PRODUCT
C      * AR -REACTANT
C      *
C      * EQUILIBRIUM CONSTANTS
C      *
C      * KRX-REACTION
C      * KH2-HYDROGEN ADSORPTION
C      * KP -PRODUCT ADSORPTION
C      * KR -REACTANT ADSORPTION
C      *
C      *-----*
117     DD 220 L=1,NPTS
118     TK(L)=T(L)/1.8
119     S(L)=DEXP[-S1/TK(L)-S2]*P(L)=100.
120     TR=TK(L)/TC
121     D1=.33583-.33853*TR+.51841*(TR**2)-2.02512*(TR**3)+1.11422*(TR**4)
122     D2=.29807-.09045*TR-.04842*TR*TR
123     TR=TREFL/TC
124     D3=.33583-.33853*TR+.51841*(TR**2)-2.02512*(TR**3)+1.11422*(TR**4)
125     D4=.29807-.09045*TR-.04842*TR*TR
126     DS=D1*(1.-W*02)/D3/(1.-W*04)
127     DENS(L)=MWB/DS/VBREF
128     KH2(L)=AN2*DEXP[EH2/R/TK(L)]
129     KRX(L)=ARX*DEXP[-ERX/R/TK(L)]
130     220  KRDKP(L)=ARDP*DEXP[ERDP/R/TK(L)]
C
C      *-----*
C      * CALCULATE OUTLET CONCENTRATION CR=FCN(CR)
C      *
C      * CC1=4*ESTIMATED VALUES (0<CC<CR1)
C      * CF1=4*CALCULATED VALUES CF=FCN(CG)
C      *
C      * CC IS ADJUSTED BY DECREASING INCREMENTS UNTIL THE
C      * INCREMENT IS LESS THAN 0.001 OF THE VALUE OF CC
C      *
C      *-----*
131     L=0

```



```

283      YSIG(J)=Y(J)
284      YSIG(J)=1
285      C2D(J)=C2D(K)
286      IF (ORDER.EQ.1.0) GO TO 500
287      TERM(J)=(C1(K)**[1.-X(4)]-X(1))*OEXP(-X(2)/R/TK(K))*P(K)**X(3)
      **([1.-X(4)]/ALMSV(K))
288      IF (TERM(J).LT.0.0) TERM(J)=0.0
289      FF=TERM(J)**[1./[1.-X(4)]]
290      GO TO 501
291      500 FF=C1(K)/OEXP[X(1)*OEXP(-X(2)/R/TK(K))*P(K)**X(3)/ALMSV(K)]
292      501 FITM(J)=FF
293      C2C(J)=FF
294      504 FDSJ=FDSJ+([FF-Y(J)]/YSIG(J))**2
295      340 CONTINUE
296      RETURN
297      END

```

SENTRY

THIS PROGRAM GENERATES A SET OF OUTLET REACTANT CONCENTRATIONS GIVEN TEMPERATURE, PRESSURE, LHSV, AND INLET REACTANT CONCENTRATIONS GIVEN AN INTEGRATED RATE EQUATION AND ITS RATE CONSTANTS. IT THEN FITS AN N-TH ORDER GLOBAL MODEL EQUATION TO THIS SET OF HYPOTHETICALLY GENERATED DATA.

FOR THIS CASE :

REACTION ACTIVATION ENERGY =0.384087D 02 KCAL/GMOLE
 HYDROGEN HEAT OF ADSORPTION =0.208247D 02 KCAL/GMOLE
 REACTANT-PRODUCT HEAT OF ADSORPTION DIFFERENCE *****

WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :

PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.500
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (% CM/SEC)	EFF FACTOR	IN CONC. (WT%)	FIN. CONC. (WT%)
1	450.0	1000.0	1.00	0.11726D 00	0.25843D -08	0.99974D 00	0.24300D 01	0.23499D 01
2	450.0	1000.0	3.00	0.11726D 00	0.25843D -08	0.99971D 00	0.24300D 01	0.24001D 01
3	450.0	1000.0	5.00	0.11726D 00	0.25843D -08	0.99970D 00	0.24300D 01	0.24146D 01
4	450.0	1000.0	9.00	0.11726D 00	0.25843D -08	0.99970D 00	0.24300D 01	0.24196D 01
5	450.0	1000.0	12.00	0.11726D 00	0.25843D -08	0.99869D 00	0.24300D 01	0.24221D 01
6	500.0	1000.0	1.00	0.12624D 00	0.31546D -06	0.99886D 00	0.24300D 01	0.19820D 01
7	500.0	1000.0	3.00	0.12624D 00	0.31546D -06	0.99845D 00	0.24300D 01	0.22436D 01
8	500.0	1000.0	5.00	0.12624D 00	0.31546D -06	0.99836D 00	0.24300D 01	0.23296D 01
9	500.0	1000.0	9.00	0.12624D 00	0.31546D -06	0.99833D 00	0.24300D 01	0.23610D 01
10	500.0	1000.0	12.00	0.12624D 00	0.31546D -06	0.99831D 00	0.24300D 01	0.23776D 01
11	550.0	1000.0	1.00	0.13481D 00	0.38662D -06	0.99452D 00	0.24300D 01	0.85408D 00
12	550.0	1000.0	3.00	0.13481D 00	0.38662D -06	0.99389D 00	0.24300D 01	0.16258D 01
13	550.0	1000.0	5.00	0.13481D 00	0.38662D -06	0.99331D 00	0.24300D 01	0.19632D 01
14	550.0	1000.0	9.00	0.13481D 00	0.38662D -06	0.99314D 00	0.24300D 01	0.21005D 01
15	550.0	1000.0	12.00	0.13481D 00	0.38662D -06	0.99305D 00	0.24300D 01	0.21752D 01
16	600.0	1000.0	1.00	0.14328D 00	0.47845D -06	0.97517D 00	0.24300D 01	0.58247D -02
17	600.0	1000.0	3.00	0.14328D 00	0.47845D -06	0.97622D 00	0.24300D 01	0.35515D 00
18	600.0	1000.0	5.00	0.14328D 00	0.47845D -06	0.97694D 00	0.24300D 01	0.85767D 00
19	600.0	1000.0	9.00	0.14328D 00	0.47845D -06	0.97727D 00	0.24300D 01	0.13182D 01
20	600.0	1000.0	12.00	0.14328D 00	0.47845D -06	0.97746D 00	0.24300D 01	0.15419D 01
21	650.0	1000.0	1.00	0.18136D 00	0.59920D -06	0.90097D 00	0.24300D 01	0.50448D -14

22	850.0	1000.0	3.00	0.15135D 00	0.59920D-06	0.90679D 00	0.24300D 01	0.88378D-04
23	850.0	1000.0	8.00	0.15135D 00	0.59920D-06	0.91587D 00	0.24300D 01	0.22702D-01
24	850.0	1000.0	9.00	0.15135D 00	0.59920D-06	0.92404D 00	0.24300D 01	0.15128D 00
25	850.0	1000.0	12.00	0.15135D 00	0.59920D-06	0.93010D 00	0.24300D 01	0.36413D 00

MARQ.... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 1 0
 X = 0.10000D 11 0.30000D 0E 0.00000D 00 0.50000D 00
 XMAX = 0.10000D 31 0.10000D 31 0.10000D 31 0.99990D 00
 XMIN = 0.00000D 00 0.00000D 00 0.00000D 00 -0.10000D 31
 DELMN = 0.10000D 03 0.30000D-03 0.00000D 00 0.50000D-08

NY = 4 NPTS = 24 LPDMA = 300 LPDME = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDP = 1 NPLAT = 1 NPMAX = 4000 MAXIT = 400 MXSUB = 25
 CRIT = 0.70711D 00 RELDF = 0.10000D-07 RELMN = 0.10000D-07

PHI (THE SUM OF SQUARES) = 0.37228198D 02 LAMBDA = 0.10000D 01

***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT.... OSAY(2, 1) = 0.1000000D 01 ITERATION 1
 ***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT.... OSAY(3, 1) = 0.1000000D 01 ITERATION 1
 ***** POSSIBLY DANGEROUS VALUE OF COEFFICIENT.... OSAY(3, 2) = 0.1000000D 01 ITERATION 1
 CONSTRAINT VIOLATED BY X(4). VALUE RESET TO 0.9999998D 00 USING CUTSTEP FACTOR = 0.17873D 00 ITER. 2
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 3
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 4
 CONSTRAINT VIOLATED BY X(4). VALUE RESET TO 0.9999998D 00 USING CUTSTEP FACTOR = 0.64196D 00 ITER. 27
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 28
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 28
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 29
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 30
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 30
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 31
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 32
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 33
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 34
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 35
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 36
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 37
 FIX X(4) = 0.99990D 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 38

```

FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 38
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 40
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 41
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 42
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 43
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 44
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 45
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 46
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 47
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 47
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 48
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 49
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 50
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 51
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 52
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 53
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 53
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 53
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 53
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 54
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 54
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 54
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 55
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 56
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 56
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 56
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 56
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 57
FIX X( 4) = 0.999900 00 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT.      ITERATION 58
    
```

CONVERGED WHEN THE STEP BECAME SMALL.

```

58 ITERATIONS      NF = 340      PHI = 0.44888544D-01      FMGN = 0.100000 01      LAMBDA = 0.12633D 05
NORM OF SCALED GRADIENT VECTOR = 0.98916D-05
X = 0.7442868D 14 0.3543814D 05 0.0000000D 00 0.9999000D 00
    
```

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.23499340E 01	0.23448887D 01	0.50648D-02	0.10000D 01	0.50648D-02
2	0.24001210E 01	0.24012855D 01	-0.11638D-02	0.10000D 01	-0.11638D-02
3	0.24145390E 01	0.24156002D 01	-0.10609D-02	0.10000D 01	-0.10609D-02
4	0.24195680E 01	0.24203908D 01	-0.42460D-03	0.10000D 01	-0.42460D-03
5	0.24221250E 01	0.24227886D 01	-0.66376D-03	0.10000D 01	-0.66376D-03
6	0.19819750E 01	0.19824892D 01	-0.39486D-01	0.10000D 01	-0.39486D-01
7	0.22438280E 01	0.22552251D 01	-0.11801D-01	0.10000D 01	-0.11801D-01
8	0.22284580E 01	0.22409844D 01	-0.11526D-01	0.10000D 01	-0.11526D-01
9	0.23810350E 01	0.23702881D 01	-0.52527D-02	0.10000D 01	-0.52527D-02
10	0.23774880E 01	0.23850772D 01	-0.75804D-02	0.10000D 01	-0.75804D-02
11	0.85408040E 00	0.75252228D 00	0.10156D 00	0.10000D 01	0.10156D 00
12	0.18258390E 01	0.18440588D 01	-0.18219D-01	0.10000D 01	-0.18219D-01
13	0.19231810E 01	0.19278929D 01	-0.35608D-01	0.10000D 01	-0.35608D-01
14	0.21004860E 01	0.21332613D 01	-0.32795D-01	0.10000D 01	-0.32795D-01
15	0.21752200E 01	0.22038635D 01	-0.28643D-01	0.10000D 01	-0.28643D-01
16	0.58348680E-02	0.12750103D-01	-0.89154D-02	0.10000D 01	-0.89154D-02
17	0.35514670E 00	0.42238498D 00	-0.67238D-01	0.10000D 01	-0.67238D-01
18	0.95786890E 00	0.10131806D 01	-0.55484D-01	0.10000D 01	-0.55484D-01
19	0.13182420E 01	0.13561940D 01	-0.37952D-01	0.10000D 01	-0.37952D-01
20	0.15419260E 01	0.15690773D 01	-0.27151D-01	0.10000D 01	-0.27151D-01
21	0.86378480E-04	0.28753210D-08	0.56374D-04	0.10000D 01	0.56374D-04
22	0.22702300E-01	0.25822900D-02	0.20120D-01	0.10000D 01	0.20120D-01
23	0.15127890E 00	0.79281122D-01	0.72018D-01	0.10000D 01	0.72018D-01
24	0.36412790E 00	0.24810307D 00	0.11602D 00	0.10000D 01	0.11602D 00

```

NUMBER OF DEGREES OF FREEDOM = 0.21000D 02
R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.46130D-01
MAXIMUM SCALED DEVIATION = 0.11802D 00
    
```

SUBROUTINE MOERR.

OSAV (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

```

1 0.1000000D 01
2 -0.9893942D 00 0.1000000D 01
3 0.7810400D 00 -0.7732414D 00 0.1000000D 01
    
```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTE-NACTV) = 21
 EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 21 PLUS OR MINUS 0.64807D 01
 ACTUAL VALUE OF PHI = 0.44687D-01
 RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.46129D-01

MAXIMUM VARIANCE INFLATION FACTOR = 0.12046D 04

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.74429691D 14	0.11860D 16	0.64710D 14
2	0	0.35436138D 05	0.18733D 05	0.88414D 03
3	1	0.00000000D 00	0.00000D 00	0.00000D 00
4	0	0.8988998D 00	0.18465D 01	0.75860D-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

K	1	2	3	4
MASK(K).....	0	0	1	0
J	MASK(J)			
1	0	0.10000D 01		
2	0	0.89897D 00	0.10000D 01	
3	1	0.00000D 00	0.00000D 00	0.00000D 00
4	0	0.63167D 00	0.86088D 00	0.00000D 00

N-TH ORDER GLOBAL MODEL PARAMETERS

AP**M = 0.7443D 14 WT%=[(1-N)/NR
 E = 0.3544D 05 CAL/GMOLE
 N = 0.8989D 00

MEAN DEVIATION = 0.2950D-01
 AVG. PERCENT ERROR = 0.1824D 02
 FOSJ = 0.4468D-01
 SUM OF SQUARES = 0.4468D-01

MARQ... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 1 0
 X = 0.100000 11 0.300000 05 0.000000 00 0.150000 01
 XMAX = 0.100000 31 0.100000 31 0.100000 31 0.100000 31
 XMIN = 0.000000 00 0.000000 00 0.000000 00 0.100010 01
 DELMN = 0.100000 03 0.300000-03 0.000000 00 0.500000-08
 NV = 4 NPTS = 24 LPDMA = 300 LPDMB = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDF = 1 NPLAT = 1 NPMAX = 4000 MAXIT = 400 MXSUB = 25
 CRIT = 0.707110 00 RELDF = 0.100000-07 RELMN = 0.100000-07
 PHI (THE SUM OF SQUARES) = 0.321027020 02 LAMBDA = 0.100000 01

CONSTRAINT VIOLATED BY X(4). VALUE RESET TO 0.100010010 01 USING CUTSTEP FACTOR = 0.718640 00 ITER. 3
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 4
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 5
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 6
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 7
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 8
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 9
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 10
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 10
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 11
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 12
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 12
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 13
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 14
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 14
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 15
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 16
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 17
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 18
 FIX X(4) = 0.100010 01 TEMPORARILY, TO AVOID VIOLATING A CONSTRAINT. ITERATION 19

CONVERGENCE ACHIEVED UNDER THE NPLAT OPTION.
 58 ITERATIONS NP = 334 PHI = 0.281071320-01 FMEN = 0.100000 01 LAMBDA = 0.103850 03
 NORM OF SCALED GRADIENT VECTOR = 0.530810-08
 X = 0.22405870 15 0.36802010 05 0.00000000 00 0.12100680 01

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.23489340E 01	0.22507170D 01	-0.78245D-03	0.100000 01	-0.78245D-03
2	0.24001210E 01	0.24022180D 01	-0.30963D-02	0.100000 01	-0.30963D-02
3	0.24145390E 01	0.24185843D 01	-0.20248D-02	0.100000 01	-0.20248D-02
4	0.24195880E 01	0.24210328D 01	-0.14668D-02	0.100000 01	-0.14668D-02
5	0.24221250E 01	0.24222710D 01	-0.11452D-02	0.100000 01	-0.11452D-02
6	0.19819750E 01	0.19516882D 01	0.30287D-01	0.100000 01	0.30287D-01
7	0.22436280E 01	0.22562377D 01	-0.12809D-01	0.100000 01	-0.12809D-01
8	0.23294580E 01	0.23411693D 01	-0.11711D-01	0.100000 01	-0.11711D-01
9	0.23510350E 01	0.23703382D 01	-0.92008D-02	0.100000 01	-0.93008D-02
10	0.23778950E 01	0.23850844D 01	-0.75877D-02	0.100000 01	-0.75877D-02
11	0.85408040E 00	0.79893305D 00	0.54147D-01	0.100000 01	0.54147D-01
12	0.15258390E 01	0.15290574D 01	-0.32185D-02	0.100000 01	-0.32185D-02
13	0.19831610E 01	0.19812913D 01	-0.18130D-01	0.100000 01	-0.18130D-01
14	0.21004660E 01	0.21187542D 01	-0.18287D-01	0.100000 01	-0.18287D-01
15	0.21752200E 01	0.21918060D 01	-0.16586D-01	0.100000 01	-0.16586D-01
16	0.58346680E-02	0.51488285D-01	-0.45654D-01	0.100000 01	-0.45654D-01
17	0.35514670E 00	0.46441180D 00	-0.10927D 00	0.100000 01	-0.10927D 00
18	0.85766890E 00	0.88896263D 00	-0.31296D-01	0.100000 01	-0.31296D-01
19	0.13182420E 01	0.13101141D 01	0.81280D-02	0.100000 01	0.81280D-02
20	0.15819280E 01	0.15177153D 01	0.24211D-01	0.100000 01	0.24211D-01
21	0.86378480E-04	0.42946730D-03	-0.38311D-03	0.100000 01	-0.38311D-03
22	0.22702300E-01	0.20963057D-01	0.17392D-02	0.100000 01	0.17392D-02
23	0.15127890E 00	0.12763088D 00	0.23648D-01	0.100000 01	0.23648D-01
24	0.36412790E 00	0.28267781D 00	0.81450D-01	0.100000 01	0.81450D-01

NUMBER OF DEGREES OF FREEDOM = 0.210000 02
 R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.385860-01
 MAXIMUM SCALED DEVIATION = 0.108270 00

SUBROUTINE MOERR
 OSAV (PT+P, SCALED, WHERE P IS THE JACOBIAN).....
 1 0.10000000 01

```

2  -0.88938380 00 0.10000000 01
3  0.75228150 00 -0.76844320 00 0.10000000 01

```

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 21
EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 21 PLUS OR MINUS 0.848070 01
ACTUAL VALUE OF PHI = 0.281070-01
RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.365860-01

```

MAXIMUM VARIANCE INFLATION FACTOR = 0.122080 04

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.224089730 15	0.383330 16	0.140240 15
2	0	0.368020100 05	0.200830 05	0.736110 03
3	1	0.000000000 00	0.000000 00	0.000000 00
4	0	0.121006800 01	0.170280 01	0.622870-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

K	1	2	3	4
MASK(K)....	0	0	1	0
J	MASK(J)			
1	0.	0.100000 01		
2	0	0.889010 00	0.100000 01	
3	1	0.000000 00	0.000000 00	0.000000 00
4	0	0.841320 00	0.589410 00	0.000000 00 0.100000 01

N-TH ORDER GLOBAL MODEL PARAMETERS

```

AP==M = 0.22410 15  WT%=[(1-N)/NR
E = 0.36800 05  CAL/GMDLE
N = 0.12100 01

```

```

MEAN DEVIATION = 0.21510-01
AVG. PERCENT ERROR = 0.58340 02
FOBJ = 0.28110-01
SUM OF SQUARES = 0.28110-01

```

STATEMENTS EXECUTED: 563816

CORE USAGE OBJECT CODE: 57688 BYTES, ARRAY AREA: 86884 BYTES, TOTAL AREA AVAILABLE: 174080 BYTES

DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 16

CDMPLE TIME: 0.41 SEC, EXECUTION TIME: 6.75 SEC, 23.32.31 MONDAY 25 JUL 83 WATFIV - MAR 1980 V2L0

CSSTOP

APPENDIX H

DIBENZOTHIOPHENE HYDRODESULFURIZATION PROCESS

MODEL FIT TO NON-ISOTHERMAL DATA


```

78      VF=0.5
79      VR=15.0
80      W=0.303
81      WT=6.0
82      ZZ=1
83
C
C *****
C *
C * INPUT=1 IF DATA IS TO BE HYPOTHETICALLY GENERATED
C * INPUT=2 IF DATA IS TO BE SUPPLIED
C *
C * DATA MAY BE GENERATED IN TWO MANNERS:
C * 1 SUPPLY ALL PRE-EXPONENTIAL AND EXPONENTIAL CONSTANTS
C * 2 SUPPLY EXPONENTIAL CONSTANTS AND RATIOS OF EQUILIBRIUM
C *   CONSTANTS AT A SPECIFIED REFERENCE TEMPERATURE
C *****
C
84      KNUM=17.5D-8
85      IF (VA/VB.GE.2.5) KNUM=8.2D-8
86      IF (VA/VB.LE.1.0) KNUM=25.2D-8
87
C
87      READ(KR,10)NPTS
88      FORMAT(15)
89      DD 30 K=1,NPTS
90      READ(KR,20)T(K),P(K),ALHSV(K),C1(K),Y(K)
91      20  FORMAT(7X,F10.5)
92      C2(K)=Y(K)
93      30  T(K)+T(K)+480.
94      IF (MI.EQ.0) GO TO 555
C
C *****
C *
C * READ TEMPERATURES, PRESSURES, LHSVS
C *
C *****
C
95      DD 110 K=1,NT
96      READ(KR,100)T1(K)
97      FORMAT(7X,F10.5)
98      T1(K)+T1(K)+480.
99      CONTINUE
100     DD 130 K=1,NP
101     READ(KR,120)P1(K)
102     FORMAT(7X,F10.5)
103     CONTINUE
104     DD 150 K=1,NL
105     READ(KR,140)ALHSV1(K)
106     FORMAT(7X,F10.5)
107     CONTINUE
C
C *****
C *
C * COMBINE TEMP, PRESS, LHSV TO FORM DATA SET
C *
C *****
C
C
108     LT=1
109     LP=1
110     LL=1
111     KNTP=0
112     KNTP=0
113     DD 210 L=1,NPTS
114     KNTP=KNTP+1
115     KNTP=KNTP+1
116     T(L)=T1(LT)
117     P(L)=P1(LP)
118     ALHSV(L)=ALHSV1(LL)
119     IF (KNTP.NE.NP) GO TO 180
120     KNTP=0
121     LT=LT+1
122     180 IF (LP.NE.NP) GO TO 190
123     IF (KNTP.EQ.NL) LP=0
124     190 IF (KNTP.NE.NL) GO TO 200
125     KNTP=0
126     LP=LP+1
127     200 IF (LL.EQ.NL) LL=0
128     LL=LL+1
129     210 CONTINUE
C
C *****
C *
C * START EQUILIBRIUM CONSTANT CALCULATIONS
C *
C * PRE-EXPONENTIAL CONSTANTS
C * ARX-REACTION
C * AH2-HYDROGEN
C * AP -PRODUCT
C * AR -REACTANT
C *
C * EQUILIBRIUM CONSTANTS
C * KRX-REACTION
C * KH2-HYDROGEN ADSORPTION
C * KP -PRODUCT ADSORPTION
C * KR -REACTANT ADSORPTION
C *****
C
130     555 DD 220 L=1,NPTS
131     TK(L)=T(L)/11.5
132     S(L)=DEXP(-S1/TK(L)-S2)*P(L)=100
133     TR=TK(L)/TC
134     D1=.3359D-.3359*TR+.51941*(TR**2)-2.02512*(TR**3)+1.11422*(TR**4)
135     D2=.28807-.09045*TR-.04842*TR*TR
136     TR=REFL/TC
137     D3=.3359D-.3359*TR+.51941*(TR**2)-2.02512*(TR**3)+1.11422*(TR**4)
138     D4=.28807-.09045*TR-.04842*TR*TR
139     D6=D1*(1.-W*D2)/D3/(1.-W*D4)
140     DENSL)=MWS/D5/VREF
141     KH2(L)=AH2*DEXP(-EH2/R/TK(L))
142     KRX(L)=ARX*DEXP(-ERX/R/TK(L))

```



```

C *****
C
278 SUBROUTINE EXFIT (FITM)
279 IMPLICIT REAL*8 (A-H,O-Z)
280 REAL*8 KRXN,KHYD,KRCT,KPRD
281 REAL*8 K2,K3,K4
282 DOUBLE PRECISION X,FIT,DEXP,DEXP,ARG,FITM,FF
283 DIMENSION FITM(300)
284 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
*ERR(20,21),FDBJ,NV,NTRAC,MATRX,MASK(20),
*RFMAX,NFLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW
285 COMMON /CDAT/ FIT(300),Y(300),YSIG(300),NPTS
286 COMMON /CSTOR/ T(70),P(70),ALHSV(70),C(70),TERM(70),T1(10),P1(10)
*ALHSV1(10),E1(70),DAB(70),DEFF(70),S(70),VIS(70),TEMP(10),
*DENSI(70),DEV,CP1,WT,VR,MI,TK(70), DEV1,DEV2,C2C(70),C2D(70),
*ORDER,2,CMIN,NDAT
287 OEXP(ARG)=DEXP(ARG)
288 K=0
289 R=1.8872
290 FDBJ=0.
291 DO 380 J=1,NPTS
292 480 K=K+1
293 IF (K.GT.NDAT) GO TO 380
294 IF (C2D(K).LT.CMIN) GO TO 480
295 Y(J)=0.0
296 Y(J)=C2D(K)
297 YSIG(J)=Y(J)
298 YSIG(J)=1.
299 K2=X(1)*DEXP(X(2)/R/TK(J))
300 K3=X(3)*DEXP(-X(4)/R/TK(J))
301 K4=X(5)*DEXP(X(6)/R/TK(J))
302 FF=C1(J)*(CP1+C1(J))/(K4+E1(J)-1.)+DLOG(C1(J)/C2D(J))-K2*K3*K4*WT
*100.*S(J)+E1(J)/ALHSV(J)/VR/DENSI(J)/(1.+K2*S(J))/(K4+E1(J)-1.)
303 501 FITM(J)=FF
304 C2C(J)=FF
305 504 FDBJ=FDBJ+[(FF-Y(J))/YSIG(J)]**2
306 380 CONTINUE
307 RETURN
308 END

```

SENTRY

THIS PROGRAM SHOWS THE ABILITY OF THE DIBENZOTHIOPHENE HDS MODEL TO FIT NON-ISOTHERMAL DATA. THE VALUES OF THE MODEL PARAMETERS ARE FIXED AT THOSE VALUES OBTAINED FROM LINEAR FITS TO THE ARRHENIUS PLOTS OF K,KH, AND KR/KP. THESE ARRHENIUS PLOTS WERE DETERMINED BY THE ISOTHERMAL CALCULATION OF THE THREE KINETIC PARAMETERS. WT% IS THE WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK FLUID.

CATALYST PROPERTIES ARE :
 PARTICLE DIAMETER = 0.21 (MM)
 AVERAGE PORE DIAMETER = 28.0 (ANGSTROMS)
 VOID FRACTION = 0.500
 TORTUOSITY FACTOR = 2.50

RUN	TEMP (F)	PRESS (PSI)	LHSV (1/HR)	H2 SOLUBILITY (WT%)	EFF DIFF (SO CM/SEC)	EFF FACTOR	IN. CONC. (WT%)	FIN. CONC. (WT%)
1	845.0	250.0	1.00	0.33515D-01	0.37868D-06	0.89750D 00	0.24300D 01	0.14700D 01
2	845.0	250.0	3.00	0.33515D-01	0.37868D-06	0.89678D 00	0.24300D 01	0.18800D 01
3	845.0	250.0	8.00	0.33515D-01	0.37868D-06	0.89665D 00	0.24300D 01	0.21900D 01
4	845.0	250.0	8.00	0.33515D-01	0.37868D-06	0.89650D 00	0.24300D 01	0.22500D 01
5	845.0	350.0	1.00	0.48821D-01	0.37868D-06	0.89668D 00	0.24300D 01	0.13500D 01
6	845.0	350.0	3.00	0.48821D-01	0.37868D-06	0.89621D 00	0.24300D 01	0.19200D 01
7	845.0	350.0	8.00	0.48821D-01	0.37868D-06	0.89591D 00	0.24300D 01	0.21400D 01
8	845.0	450.0	1.00	0.60327D-01	0.37868D-06	0.89586D 00	0.24300D 01	0.22300D 01
9	845.0	450.0	3.00	0.60327D-01	0.37868D-06	0.89565D 00	0.24300D 01	0.12800D 01
10	845.0	450.0	8.00	0.60327D-01	0.37868D-06	0.89579D 00	0.24300D 01	0.18700D 01
11	845.0	450.0	8.00	0.60327D-01	0.37868D-06	0.89545D 00	0.24300D 01	0.21100D 01
12	845.0	450.0	8.00	0.60327D-01	0.37868D-06	0.89521D 00	0.24300D 01	0.22000D 01
13	872.0	250.0	1.00	0.34658D-01	0.42406D-06	0.89530D 00	0.24300D 01	0.91000D 00
14	872.0	250.0	3.00	0.34658D-01	0.42406D-06	0.89521D 00	0.24300D 01	0.17400D 01
15	872.0	250.0	8.00	0.34658D-01	0.42406D-06	0.89525D 00	0.24300D 01	0.20500D 01
16	872.0	250.0	8.00	0.34658D-01	0.42406D-06	0.89513D 00	0.24300D 01	0.21700D 01
17	872.0	350.0	1.00	0.48822D-01	0.42406D-06	0.89402D 00	0.24300D 01	0.16000D 01
18	872.0	350.0	3.00	0.48822D-01	0.42406D-06	0.89389D 00	0.24300D 01	0.19700D 01
19	872.0	350.0	8.00	0.48822D-01	0.42406D-06	0.89393D 00	0.24300D 01	0.21100D 01
20	872.0	350.0	12.00	0.48822D-01	0.42406D-06	0.89404D 00	0.24300D 01	0.21800D 01
21	872.0	450.0	1.00	0.62386D-01	0.42406D-06	0.89317D 00	0.24300D 01	0.58000D 00
22	872.0	450.0	3.00	0.62386D-01	0.42406D-06	0.89310D 00	0.24300D 01	0.18000D 01
23	872.0	450.0	8.00	0.62386D-01	0.42406D-06	0.89296D 00	0.24300D 01	0.19000D 01
24	872.0	450.0	8.00	0.62386D-01	0.42406D-06	0.89291D 00	0.24300D 01	0.20600D 01
25	872.0	450.0	12.00	0.62386D-01	0.42406D-06	0.89300D 00	0.24300D 01	0.21500D 01
26	890.0	250.0	1.00	0.35409D-01	0.45808D-06	0.89147D 00	0.24300D 01	0.35000D 00
27	890.0	250.0	3.00	0.35409D-01	0.45808D-06	0.89223D 00	0.24300D 01	0.13500D 01
28	890.0	250.0	8.00	0.35409D-01	0.45808D-06	0.89250D 00	0.24300D 01	0.18300D 01

30	590.0	250.0	8.00	0.35408D-01	0.45808D-08	0.99268D 00	0.24300D 01	0.20200D 01
31	590.0	280.0	12.00	0.35409D-01	0.45808D-08	0.99253D 00	0.24300D 01	0.21100D 01
32	590.0	250.0	15.00	0.35409D-01	0.45808D-08	0.99282D 00	0.24300D 01	0.21800D 01
33	590.0	350.0	1.00	0.48572D-01	0.45808D-08	0.98882D 00	0.24300D 01	0.19000D 00
34	590.0	350.0	3.00	0.48572D-01	0.45808D-08	0.98911D 00	0.24300D 01	0.11300D 01
35	590.0	350.0	6.00	0.48572D-01	0.45808D-08	0.99027D 00	0.24300D 01	0.16400D 01
36	590.0	350.0	8.00	0.48572D-01	0.45808D-08	0.99047D 00	0.24300D 01	0.19100D 01
37	590.0	350.0	12.00	0.48572D-01	0.45808D-08	0.99051D 00	0.24300D 01	0.20300D 01
38	590.0	350.0	15.00	0.48572D-01	0.45808D-08	0.99069D 00	0.24300D 01	0.21100D 01
39	590.0	450.0	3.00	0.63736D-01	0.45808D-08	0.98783D 00	0.24300D 01	0.87000D 00
40	590.0	450.0	6.00	0.63736D-01	0.45808D-08	0.98851D 00	0.24300D 01	0.15700D 01
41	590.0	450.0	9.00	0.63736D-01	0.45808D-08	0.98859D 00	0.24300D 01	0.18200D 01
42	590.0	450.0	12.00	0.63736D-01	0.45808D-08	0.98869D 00	0.24300D 01	0.19600D 01
43	590.0	450.0	15.00	0.63736D-01	0.45808D-08	0.98881D 00	0.24300D 01	0.20500D 01
44	617.0	250.0	3.00	0.36515D-01	0.51574D-08	0.98665D 00	0.24300D 01	0.64000D 00
45	617.0	250.0	6.00	0.36515D-01	0.51574D-08	0.98680D 00	0.24300D 01	0.13200D 01
46	617.0	250.0	9.00	0.36515D-01	0.51574D-08	0.98627D 00	0.24300D 01	0.16400D 01
47	617.0	250.0	12.00	0.36515D-01	0.51574D-08	0.98628D 00	0.24300D 01	0.18100D 01
48	617.0	250.0	15.00	0.36515D-01	0.51574D-08	0.98658D 00	0.24300D 01	0.19300D 01
49	617.0	350.0	3.00	0.51121D-01	0.51574D-08	0.97921D 00	0.24300D 01	0.40900D 00
50	617.0	350.0	6.00	0.51121D-01	0.51574D-08	0.98104D 00	0.24300D 01	0.10700D 01
51	617.0	350.0	9.00	0.51121D-01	0.51574D-08	0.98160D 00	0.24300D 01	0.14300D 01
52	617.0	350.0	12.00	0.51121D-01	0.51574D-08	0.98208D 00	0.24300D 01	0.16500D 01
53	617.0	350.0	15.00	0.51121D-01	0.51574D-08	0.98231D 00	0.24300D 01	0.17800D 01
54	617.0	450.0	3.00	0.65727D-01	0.51574D-08	0.97484D 00	0.24300D 01	0.27000D 00
55	617.0	450.0	6.00	0.65727D-01	0.51574D-08	0.97668D 00	0.24300D 01	0.84000D 00
56	617.0	450.0	9.00	0.65727D-01	0.51574D-08	0.97762D 00	0.24300D 01	0.12700D 01
57	617.0	450.0	12.00	0.65727D-01	0.51574D-08	0.97810D 00	0.24300D 01	0.15100D 01
58	617.0	450.0	15.00	0.65727D-01	0.51574D-08	0.97841D 00	0.24300D 01	0.16700D 01
59	622.0	250.0	6.00	0.38310D-01	0.63377D-08	0.97484D 00	0.24300D 01	0.63000D 00
60	622.0	250.0	9.00	0.38310D-01	0.63377D-08	0.97668D 00	0.24300D 01	0.10400D 01
61	622.0	250.0	12.00	0.38310D-01	0.63377D-08	0.97826D 00	0.24300D 01	0.13600D 01
62	622.0	250.0	15.00	0.38310D-01	0.63377D-08	0.97893D 00	0.24300D 01	0.15500D 01
63	622.0	350.0	6.00	0.53635D-01	0.63377D-08	0.96342D 00	0.24300D 01	0.33000D 00
64	622.0	350.0	9.00	0.53635D-01	0.63377D-08	0.96750D 00	0.24300D 01	0.75000D 00
65	622.0	350.0	12.00	0.53635D-01	0.63377D-08	0.96832D 00	0.24300D 01	0.10400D 01
66	622.0	350.0	15.00	0.53635D-01	0.63377D-08	0.97064D 00	0.24300D 01	0.12900D 01
67	622.0	450.0	6.00	0.68959D-01	0.63377D-08	0.95208D 00	0.24300D 01	0.17000D 00
68	622.0	450.0	9.00	0.68959D-01	0.63377D-08	0.95797D 00	0.24300D 01	0.52000D 00
69	622.0	450.0	12.00	0.68959D-01	0.63377D-08	0.96078D 00	0.24300D 01	0.83000D 00
70	622.0	450.0	15.00	0.68959D-01	0.63377D-08	0.96248D 00	0.24300D 01	0.10700D 01

MARQ... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 1 1 0 1 1 1
X = 0.11848D-06 0.20935D 05 0.81278D 14 0.38409D 05 0.13178D 08 -0.18972D 05
XMAX = 0.10000D 31 0.10000D 31 0.82000D 14 0.10000D 31 0.10000D 31 0.10000D 31
XMIN = -0.10000D 31 -0.10000D 31 0.81000D 14 -0.10000D 31 -0.10000D 31 -0.10000D 31
DELMN = 0.00000D 00 0.00000D 00 0.81278D 08 0.00000D 00 0.00000D 00 0.00000D 00

NY = 6 NPTS = 70 LPDMA = 300 LPDME = 20 NTRAC = 0 METHD = 1 KALCP = 0
KORDP = 1 NPLAT = 1 NPMAX = 5000 MAXIT = 1 MXSUB = 25
CRIT = 0.70711D 00 RELDF = 0.10000D-07 RELMN = 0.10000D-07

PHI (THE SUM OF SQUARES) = 0.23728658D 04 LAMBDA = 0.10000D 01

CONSTRAINT VIOLATED BY X(3). VALUE RESET TO 0.82000000D 14 USING CUTSTEP FACTOR = 0.15055D 00 ITER. 1

MAXIMUM NUMBER OF ITERATIONS REACHED IN MARQ. MAXIT = 1
1 ITERATIONS NF = 4 PHI = 0.20389130D 04 FMGN = 0.10000D 01 LAMBDA = 0.10000D 01
NORM OF SCALED GRADIENT VECTOR = 0.42888D 02

X = 0.1184800D-06 0.2093470D 05 0.8200000D 14 0.3840870D 05 0.1317800D 08 -0.1897180D 05

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.1489999E 01	0.1554968D 01	-0.64969D-01	0.10000D 01	-0.64969D-01
2	0.1989999E 01	0.1983851D 01	0.60382D-02	0.10000D 01	0.60382D-02
3	0.2189999E 01	0.2187232D 01	0.27074D-02	0.10000D 01	0.27074D-02
4	0.2259999E 01	0.2252875D 01	0.71242D-02	0.10000D 01	0.71242D-02
5	0.1359999E 01	0.1509850D 01	-0.14989D 00	0.10000D 01	-0.14989D 00
6	0.1919999E 01	0.1921624D 01	-0.18256D-02	0.10000D 01	-0.18256D-02
7	0.2139999E 01	0.2131230D 01	0.87092D-02	0.10000D 01	0.87092D-02
8	0.2229999E 01	0.2225281D 01	0.47185D-02	0.10000D 01	0.47185D-02
9	0.1279999E 01	0.1469977D 01	-0.18998D 00	0.10000D 01	-0.18998D 00
10	0.1869999E 01	0.1878761D 01	-0.87620D-02	0.10000D 01	-0.87620D-02
11	0.2109999E 01	0.2105448D 01	0.45611D-02	0.10000D 01	0.45611D-02
12	0.2189999E 01	0.2186295D 01	0.11704D-01	0.10000D 01	0.11704D-01
13	0.9099999E 00	0.1882088D 01	-0.85921D 00	0.10000D 01	-0.85921D 00
14	0.1739999E 01	0.2173299D 01	-0.43328D 00	0.10000D 01	-0.43328D 00
15	0.2059999E 01	0.2320845D 01	-0.26065D 00	0.10000D 01	-0.26065D 00
16	0.2189999E 01	0.2325124D 01	-0.15513D 00	0.10000D 01	-0.15513D 00
17	0.7099999E 00	0.1789878D 01	-0.10599D 01	0.10000D 01	-0.10599D 01
18	0.1589999E 01	0.2128230D 01	-0.52823D 00	0.10000D 01	-0.52823D 00
19	0.1969999E 01	0.2269494D 01	-0.29949D 00	0.10000D 01	-0.29949D 00
20	0.2109999E 01	0.2309234D 01	-0.19833D 00	0.10000D 01	-0.19833D 00

21	0.2188880E 01	0.2388833E 01	-0.18883D 00	0.10000D 01	-0.18883D 00
22	0.8798880E 00	0.1888188D 01	-0.11042D 01	0.10000D 01	-0.11042D 01
23	0.1800000E 01	0.2131384D 01	-0.83138D 00	0.10000D 01	-0.83138D 00
24	0.1888880E 01	0.2230034D 01	-0.33003D 00	0.10000D 01	-0.33003D 00
25	0.2058880E 01	0.2284512D 01	-0.22451D 00	0.10000D 01	-0.22451D 00
26	0.2148880E 01	0.2236255D 01	-0.18827D 00	0.10000D 01	-0.18827D 00
27	0.3488880E 00	0.2082530D 02	-0.20575D 02	0.10000D 01	-0.20575D 02
28	0.1348880E 01	0.1288347D 01	0.51852D -01	0.10000D 01	0.51852D -01
29	0.1828880E 01	0.8257781D 00	0.11842D 01	0.10000D 01	0.11842D 01
30	0.2018880E 01	0.7381804D 00	0.12818D 01	0.10000D 01	0.12818D 01
31	0.2108880E 01	0.1484378D 01	0.84582D 00	0.10000D 01	0.84582D 00
32	0.2178880E 01	0.1150142D 01	0.10288D 01	0.10000D 01	0.10288D 01
33	0.1888880E 00	0.3883332D 02	-0.38843D 02	0.10000D 01	-0.38843D 02
34	0.1128880E 01	0.2538500D 01	-0.14085D 01	0.10000D 01	-0.14085D 01
35	0.1878880E 01	0.8251911D 00	0.10548D 01	0.10000D 01	0.10548D 01
36	0.1808880E 01	0.5352804D 00	0.13747D 01	0.10000D 01	0.13747D 01
37	0.2028880E 01	0.8128884D 00	0.11181D 01	0.10000D 01	0.11181D 01
38	0.2108880E 01	0.8748662D 00	0.12353D 01	0.10000D 01	0.12353D 01
39	0.8888880E 00	0.4287224D 01	-0.33272D 01	0.10000D 01	-0.33272D 01
40	0.1868880E 01	-0.2415373D 01	0.18042D 01	0.10000D 01	0.18042D 01
41	0.1818880E 01	0.4732288D 00	0.13488D 01	0.10000D 01	0.13488D 01
42	0.1888880E 01	0.8887718D 00	0.12832D 01	0.10000D 01	0.12832D 01
43	0.2048880E 01	0.7725828D 00	0.12774D 01	0.10000D 01	0.12774D 01
44	0.8588880E 00	0.1547648D 01	-0.88785D 00	0.10000D 01	-0.88785D 00
45	0.1318880E 01	0.1788804D 01	-0.47580D 00	0.10000D 01	-0.47580D 00
46	0.1838880E 01	0.1844018D 01	-0.30402D 00	0.10000D 01	-0.30402D 00
47	0.1808880E 01	0.2083878D 01	-0.25388D 00	0.10000D 01	-0.25388D 00
48	0.1828880E 01	0.2112750D 01	-0.18278D 00	0.10000D 01	-0.18278D 00
49	0.3888880E 00	0.1724087D 01	-0.13241D 01	0.10000D 01	-0.13241D 01
50	0.1088880E 01	0.1881350D 01	-0.81814D 00	0.10000D 01	-0.81814D 00
51	0.1428880E 01	0.1857091D 01	-0.42709D 00	0.10000D 01	-0.42709D 00
52	0.1848880E 01	0.18807184D 01	-0.30072D 00	0.10000D 01	-0.30072D 00
53	0.1788880E 01	0.2027721D 01	-0.23772D 00	0.10000D 01	-0.23772D 00
54	0.2888880E 00	0.16898078D 01	-0.13888D 01	0.10000D 01	-0.13888D 01
55	0.8788880E 00	0.1844333D 01	-0.78433D 00	0.10000D 01	-0.78433D 00
56	0.1288880E 01	0.1770710D 01	-0.80071D 00	0.10000D 01	-0.80071D 00
57	0.1808880E 01	0.18838384D 01	-0.37384D 00	0.10000D 01	-0.37384D 00
58	0.1848880E 01	0.1884828D 01	-0.28848D 00	0.10000D 01	-0.28848D 00
59	0.8288880E 00	0.2708861D 00	0.35830D 00	0.10000D 01	0.35830D 00
60	0.1078880E 01	0.8738205D 00	0.20608D 00	0.10000D 01	0.20608D 00
61	0.1288880E 01	0.1228751D 01	0.13325D 00	0.10000D 01	0.13325D 00
62	0.1548880E 01	0.1488323D 01	0.10188D 00	0.10000D 01	0.10188D 00
63	0.3288880E 00	-0.2488178D 00	0.57888D 00	0.10000D 01	0.57888D 00
64	0.7800000E 00	0.4387448D 00	0.31428D 00	0.10000D 01	0.31428D 00
65	0.1088880E 01	0.8852181D 00	0.18478D 00	0.10000D 01	0.18478D 00
66	0.1288880E 01	0.1127888D 01	0.18203D 00	0.10000D 01	0.18203D 00
67	0.1888880E 00	-0.8383504D 00	0.80835D 00	0.10000D 01	0.80835D 00
68	0.5188880E 00	0.8881285D -01	0.48304D 00	0.10000D 01	0.48304D 00
69	0.8288880E 00	0.5488888D 00	0.28341D 00	0.10000D 01	0.28341D 00
70	0.1088880E 01	0.8708833D 00	0.18831D 00	0.10000D 01	0.18831D 00

NUMBER OF DEGREES OF FREEDOM = 0.89000D 02
R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.54388D 01
MAXIMUM SCALED DEVIATION = 0.38843D 02

SUBROUTINE MOERR.

OSAY (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

1 0.1000000D 01

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTY) = 88

EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 88 PLUS OR MINUS 0.11747D 02

ACTUAL VALUE OF PHI = 0.20388D 04

RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.54388D 01

MAXIMUM VARIANCE INFLATION FACTOR = 0.10000D 01

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	1	0.1184800D -08	0.00000D 00	0.00000D 00
2	1	0.2083488D 05	0.00000D 00	0.00000D 00
3	0	0.8200000D 14	0.17718D 12	0.88288D 12
4	1	0.3840888D 05	0.00000D 00	0.00000D 00
5	1	0.1317800D 08	0.00000D 00	0.00000D 00
6	1	-0.1887180D 05	0.00000D 00	0.00000D 00

LOWER TRIANGLE OF THE CORRELATION MATRIX....

K	1	2	3	4	5	6
MASK(K)	1	1	0	1	1	1
J	MASK(J)					
1	1	0.00000D 00				
2	1	0.00000D 00	0.00000D 00			
3	0	0.00000D 00	0.00000D 00	0.10000D 01		
4	1	0.00000D 00	0.00000D 00	0.00000D 00	0.00000D 00	
5	1	0.00000D 00	0.00000D 00	0.00000D 00	0.00000D 00	0.00000D 00
6	1	0.00000D 00	0.00000D 00	0.00000D 00	0.00000D 00	0.00000D 00

DIBENZOTHIOPHENE HDS PROCESS MODEL FIT TO NON-ISOTHERMAL DATA.

THE KINETIC PARAMETERS WERE FIXED AT THE FOLLOWING VALUES:

K A = 0.8200D 14 1/WT% E = 0.3841D 05 CAL/GMOLE
K AH = 0.1185D-06 1/WT% EH = 0.2083D 05 CAL/GMOLE
KR/KP AR/AP = 0.1316D 08 ER-EP = -0.1887D 05 CAL/GMOLE

THE RESULTING FIT:

MEAN DEVIATION = 0.140825D 01
AVERAGE PERCENT ERROR = 0.442053D 03
FDBJ = 0.203881D 04
SUM OF SQUARES = 0.203881D 04

STATEMENTS EXECUTED: 11718

CORE USAGE OBJECT CODE: 58472 BYTES, ARRAY AREA: 73176 BYTES, TOTAL AREA AVAILABLE: 174080 BYTES
DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 12
COMPILE TIME: 0.41 SEC, EXECUTION TIME: 0.24 SEC, 0.38.45 TUESDAY 26 JUL 83 WATFIV - MAR 1980 V2L0

CSSTOP

APPENDIX I

N-TH ORDER GLOBAL MODEL FIT TO NON-ISOTHERMAL
DIBENZOTHIOPHENE HYDRODESULFURIZATION DATA

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SJOB
C
C *****
C * N-TH ORDER GLOBAL MODEL *
C * ESPINO DATA *
C * DIBENZOTHIOPHENE HDS *
C * NON-ISOTHERMAL FIT *
C *****
C
1  IMPLICIT REAL*8 (A-N,O-Z)
2  EXTERNAL EXFIT
3  DOUBLE PRECISION X,FIT
4  COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
5  *ERR(20,21),FOBJ,NV,NTRAC,MATRX,MASK(20),
6  *NFMAX,NPLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW
7  COMMON /NLS4/ FLAME,FNU,RELOF,RELMN,METHD,KALCP,KORDF,
8  *MAXIT,LEOU,MXSUE,MXUPD
9  COMMON /CDAT/ FIT(300),Y(300),YSIG(300),NPTS
10 COMMON /CSTDR/ T(70),P(70),ALHSV(70),C(70),X(70)
11 KR=5
12 KW=8
13 FL=1.
14 CALL STSET
15 MAXIT=200
16 NV=4
17 XMIN(1)=0.1D8
18 XMAX(4)=0.9999
19 X(1)=0.1888D10
20 X(2)=0.8327D8
21 X(3)=0.8794
22 X(4)=1.5
23 NTRAC=0
24 WRITE(KW,40)
25 40  FORMAT(1H1,////SX,'WT% IS WEIGHT PERCENT DIBENZOTHIOPHENE IN THE
26 *BULK LIQUID')
27 WRITE(KW,50)
28 50  FORMAT(////10X,'TEMPERATURE',SX,'PRESSURE',SX,'LHSV',SX,'IN. CONC
29 *',SX,'FIN. CDNC.',//14X,'[R]',10X,'[PSI]',10X,'[1/HR]',10X,'[WT%]'
30 *,10X,'[WTL]')
31 READ(KR,100)NPTS
32 100  FORMAT(1S)
33 DO 110 K=1,NPTS
34 READ(KR,120)T(K),P(K),ALHSV(K),C(1)(K),Y(K)
35 120  FORMAT(7X,5F10.5)
36 T(K)=T(K)+480.
37 WRITE(KW,125)NPTS,(K,T(K),P(K),ALHSV(K),C(1)(K),Y(K),K=1,NPTS)
38 125  FORMAT(//1X,15//1X,15,SE15.5)
39 CALL STEPT (EXFIT)
40 DEV=0.0
41 PE=0.0
42 SOS=0.0
43 DO 130 L=1,NPTS
44 DEV=DEV+DABS(FIT(L)-Y(L))/NPTS
45 PE=PE+DABS(FIT(L)-Y(L))/NPTS/Y(L)=100.
46 SOS=SOS+(FIT(L)-Y(L))**2
47
48
49 WRITE(KW,135)
50 135  FORMAT(1H1,////SX,'N-TH ORDER GLOBAL MODEL PARAMETERS')
51 WRITE(KW,140)X(1),X(2),X(3),X(4)
52 140  FORMAT(//SX,'A = ',E10.4,SX,'WT%=(1-N)/PSI**M/HR',//SX,'E = ',
53 *E10.4,SX,'RTU/LBMOLE',//SX,'M = ',E10.4,//SX,'N = ',E10.4)
54 WRITE(KW,150)DEV,PE,FOBJ,SOS
55 150  FORMAT(//SX,'MEAN DEVIATION = ',E10.4,//SX,'AVG. PERCENT ERROR =
56 *',E10.4,//SX,'FOBJ = ',E10.4,//SX,'SUM OF SQUARES = ',E10.4,////)
57 STOP
58 END
59
60 SUBROUTINE EXFIT (FITM)
61 IMPLICIT REAL*8 (A-N,O-Z)
62 DOUBLE PRECISION X,FIT,DEXP,DEXP,ARG,FITM,FF
63 DIMENSION FITM(1)
64 COMMON /CSTEP/ X(20),XMAX(20),XMIN(20),DELTX(20),DELMN(20),
65 *ERR(20,21),FOBJ,NV,NTRAC,MATRX,MASK(20),
66 *NFMAX,NPLAT,JVARY,NXTRA,KFLAG,NOREP,KERFL,KW
67 COMMON /CDAT/ FIT(300),Y(300),YSIG(300),NPTS
68 COMMON /CSTDR/ T(70),P(70),ALHSV(70),C(70),X(70)
69 DEXP(ARG)=DEXP(ARG)
70 FOBJ=0.
71 R=1.847
72 DO 200 J=1,NPTS
73 YSIG(J)=1.0
74 YSIG(J)=Y(J)
75 TERM=(C(1)(J)**(1.-X(4))-X(1))*DEXP(-X(2)/R/T(J))*P(J)**X(3)**(1.-X(4))
76 IF (TERM.LT.0.0) TERM=0.0
77 FF=TERM**1./1.-X(4)
78 FITM(J)=FF
79 FOBJ=FOBJ+((FF-Y(J))/YSIG(J))**2
80 RETURN
81 END
SENTRY

```

WT% IS WEIGHT PERCENT DIBENZOTHIOPHENE IN THE BULK LIQUID

	TEMPERATURE (R)	PRESSURE (PSI)	LHSV (1/HR)	IN. CONC. (WT%)	FIN. CONC. (WT%)
70					
1	0.100500 04	0.250000 03	0.100000 01	0.243000 01	0.147000 01
2	0.100500 04	0.250000 03	0.200000 01	0.243000 01	0.198000 01
3	0.100500 04	0.250000 03	0.300000 01	0.243000 01	0.218000 01
4	0.100500 04	0.250000 03	0.400000 01	0.243000 01	0.225000 01
5	0.100500 04	0.350000 03	0.100000 01	0.243000 01	0.138000 01
6	0.100500 04	0.350000 03	0.200000 01	0.243000 01	0.192000 01
7	0.100500 04	0.350000 03	0.300000 01	0.243000 01	0.214000 01
8	0.100500 04	0.350000 03	0.400000 01	0.243000 01	0.223000 01
9	0.100500 04	0.450000 03	0.100000 01	0.243000 01	0.128000 01
10	0.100500 04	0.450000 03	0.200000 01	0.243000 01	0.187000 01
11	0.100500 04	0.450000 03	0.300000 01	0.243000 01	0.211000 01
12	0.100500 04	0.450000 03	0.400000 01	0.243000 01	0.220000 01
13	0.103200 04	0.250000 03	0.100000 01	0.243000 01	0.110000 00
14	0.103200 04	0.250000 03	0.200000 01	0.243000 01	0.174000 01
15	0.103200 04	0.250000 03	0.300000 01	0.243000 01	0.208000 01
16	0.103200 04	0.250000 03	0.400000 01	0.243000 01	0.217000 01
17	0.103200 04	0.350000 03	0.100000 01	0.243000 01	0.110000 00
18	0.103200 04	0.350000 03	0.200000 01	0.243000 01	0.160000 01
19	0.103200 04	0.350000 03	0.300000 01	0.243000 01	0.187000 01
20	0.103200 04	0.350000 03	0.400000 01	0.243000 01	0.211000 01
21	0.103200 04	0.450000 03	0.100000 01	0.243000 01	0.118000 01
22	0.103200 04	0.450000 03	0.200000 01	0.243000 01	0.150000 00
23	0.103200 04	0.450000 03	0.300000 01	0.243000 01	0.180000 01
24	0.103200 04	0.450000 03	0.400000 01	0.243000 01	0.190000 01
25	0.103200 04	0.450000 03	0.500000 01	0.243000 01	0.206000 01
26	0.103200 04	0.450000 03	0.120000 02	0.243000 01	0.218000 01
27	0.105000 04	0.250000 03	0.100000 01	0.243000 01	0.130000 00
28	0.105000 04	0.250000 03	0.200000 01	0.243000 01	0.138000 01
29	0.105000 04	0.250000 03	0.300000 01	0.243000 01	0.163000 01
30	0.105000 04	0.250000 03	0.400000 01	0.243000 01	0.202000 01
31	0.105000 04	0.250000 03	0.120000 02	0.243000 01	0.211000 01
32	0.105000 04	0.250000 03	0.150000 02	0.243000 01	0.216000 01
33	0.105000 04	0.350000 03	0.100000 01	0.243000 01	0.190000 00
34	0.105000 04	0.350000 03	0.200000 01	0.243000 01	0.113000 01
35	0.105000 04	0.350000 03	0.300000 01	0.243000 01	0.188000 01
36	0.105000 04	0.350000 03	0.400000 01	0.243000 01	0.181000 01
37	0.105000 04	0.450000 03	0.120000 02	0.243000 01	0.203000 01
38	0.105000 04	0.450000 03	0.150000 02	0.243000 01	0.211000 01
39	0.105000 04	0.450000 03	0.200000 01	0.243000 01	0.170000 00
40	0.105000 04	0.450000 03	0.300000 01	0.243000 01	0.182000 01
41	0.105000 04	0.450000 03	0.400000 01	0.243000 01	0.186000 01
42	0.105000 04	0.450000 03	0.120000 02	0.243000 01	0.186000 01
43	0.105000 04	0.450000 03	0.150000 02	0.243000 01	0.205000 01
44	0.107700 04	0.250000 03	0.200000 01	0.243000 01	0.180000 00
45	0.107700 04	0.250000 03	0.300000 01	0.243000 01	0.132000 01
46	0.107700 04	0.250000 03	0.400000 01	0.243000 01	0.184000 01
47	0.107700 04	0.250000 03	0.120000 02	0.243000 01	0.181000 01
48	0.107700 04	0.250000 03	0.150000 02	0.243000 01	0.193000 01
49	0.107700 04	0.350000 03	0.200000 01	0.243000 01	0.400000 00
50	0.107700 04	0.350000 03	0.300000 01	0.243000 01	0.107000 01
51	0.107700 04	0.350000 03	0.400000 01	0.243000 01	0.143000 01
52	0.107700 04	0.350000 03	0.120000 02	0.243000 01	0.185000 01
53	0.107700 04	0.350000 03	0.150000 02	0.243000 01	0.178000 01
54	0.107700 04	0.450000 03	0.200000 01	0.243000 01	0.270000 00
55	0.107700 04	0.450000 03	0.300000 01	0.243000 01	0.280000 00
56	0.107700 04	0.450000 03	0.400000 01	0.243000 01	0.127000 01
57	0.107700 04	0.450000 03	0.120000 02	0.243000 01	0.181000 01
58	0.107700 04	0.450000 03	0.150000 02	0.243000 01	0.187000 01
59	0.112200 04	0.250000 03	0.300000 01	0.243000 01	0.130000 00
60	0.112200 04	0.250000 03	0.400000 01	0.243000 01	0.108000 01
61	0.112200 04	0.250000 03	0.120000 02	0.243000 01	0.138000 01
62	0.112200 04	0.250000 03	0.150000 02	0.243000 01	0.188000 01
63	0.112200 04	0.350000 03	0.200000 01	0.243000 01	0.178000 01
64	0.112200 04	0.350000 03	0.300000 01	0.243000 01	0.270000 00
65	0.112200 04	0.350000 03	0.400000 01	0.243000 01	0.108000 01
66	0.112200 04	0.350000 03	0.120000 02	0.243000 01	0.128000 01
67	0.112200 04	0.450000 03	0.200000 01	0.243000 01	0.170000 00
68	0.112200 04	0.450000 03	0.300000 01	0.243000 01	0.182000 00
69	0.112200 04	0.450000 03	0.400000 01	0.243000 01	0.183000 00
70	0.112200 04	0.450000 03	0.120000 02	0.243000 01	0.107000 01

MARCO... BEGIN NONLINEAR LEAST SQUARES SOLUTION

MASK = 0 0 0 0
 X = 0.188800 10 0.522700 05 0.478400 00 0.888800 00
 XMAX = 0.100000 31 0.100000 31 0.100000 31 0.888800 00
 XMIN = 0.100000 08 -0.100000 31 -0.100000 31 -0.100000 31
 DELMH = 0.188800 02 0.522700-03 0.478400-08 0.180000-07

NV = 4 NPTS = 70 LPOMA = 300 LPOMB = 20 NTRAC = 0 METHD = 1 KALCP = 0
 KORDF = 1 NPLAT = 1 NFMAX = 32767 MAXIT = 200 MXSUB = 25
 CRIT = 0.70711D 00 RELDF = 0.100000-07 RELMH = 0.100000-07

PHI (THE SUM OF SQUARES) = 0.1055888D 01 LAMBDA = 0.100000 01

CONVERGED WHEN THE STEP BECAME SMALL.

10 ITERATIONS NF = 52 PHI = 0.80808264D 00 FMCN = 0.100000 01 LAMBDA = 0.10833D-08

NORM OF SCALED GRADIENT VECTOR = 0.18975D-07

X = 0.1878723D 10 0.5271368D 05 0.8188646D 00 0.4383858D 00

J	Y(J)	FIT(J)	Y(J)-FIT(J)	YSIG(J)	(Y-FIT)/YSIG
1	0.14888880E 01	0.14188817D 01	0.50318D-01	0.14700D 01	0.342300-01
2	0.18888880E 01	0.20420817D 01	-0.52082D-01	0.18800D 01	-0.28172D-01
3	0.21888880E 01	0.22288888D 01	-0.39000D-01	0.21800D 01	-0.17808D-01
4	0.22888880E 01	0.22843848D 01	-0.34389D-01	0.22800D 01	-0.15218D-01
5	0.12888880E 01	0.11844888D 01	0.17553D 00	0.12800D 01	0.13800D 00
6	0.18188880E 01	0.18303048D 01	-0.10305D-01	0.18200D 01	-0.52874D-02
7	0.21388880E 01	0.21881520D 01	-0.28153D-01	0.21400D 01	-0.13155D-01
8	0.22288880E 01	0.22828780D 01	-0.22878D-01	0.22300D 01	-0.10188D-01
9	0.12788880E 01	0.88227381D 00	0.28773D 00	0.12800D 01	0.22478D 00
10	0.18888880E 01	0.18288978D 01	0.41002D-01	0.18700D 01	0.21828D-01
11	0.21088880E 01	0.21118881D 01	-0.18954D-02	0.21100D 01	-0.80352D-03
12	0.21988880E 01	0.22136718D 01	-0.12872D-01	0.22000D 01	-0.52148D-02
13	0.80888880E 00	0.78888383D 00	0.12032D 00	0.81000D 00	0.13222D 00
14	0.17388880E 01	0.17088772D 01	0.31123D-01	0.17400D 01	0.17847D-01
15	0.20588880E 01	0.20428885D 01	-0.17010D-01	0.20800D 01	-0.82871D-02
16	0.21888880E 01	0.21858030D 01	-0.41838D-02	0.21700D 01	-0.18328D-02
17	0.70888880E 00	0.52881258D 00	0.18348D 00	0.71000D 00	0.25843D 00
18	0.15888880E 01	0.15213887D 01	0.78811D-01	0.16000D 01	0.48132D-01
19	0.19888880E 01	0.18214662D 01	0.38853D-01	0.19700D 01	0.18870D-01
20	0.21088880E 01	0.20871088D 01	0.22884D-01	0.21100D 01	0.10880D 00
21	0.21888880E 01	0.21887408D 01	-0.21218D-01	0.21800D 01	-0.98888D-02
22	0.87888880E 00	0.34881381D 00	0.23108D 00	0.88000D 00	0.38842D 00
23	0.18008000E 01	0.13888658D 01	0.14032D 00	0.18000D 01	0.32858D-01
24	0.18888880E 01	0.18203381D 01	0.88880D-01	0.18000D 01	0.38883D-01
25	0.20588880E 01	0.20148416D 01	0.45388D-01	0.20800D 01	0.22018D-01
26	0.21488880E 01	0.21124811D 01	0.27848D-01	0.21500D 01	0.17484D-01
27	0.34888880E 00	0.34230884D 00	-0.22307D-01	0.35000D 00	-0.82308D-01
28	0.13488880E 01	0.13833724D 01	-0.43373D-01	0.13500D 01	-0.32128D-01
29	0.18288880E 01	0.18518272D 01	-0.21827D-01	0.18300D 01	-0.11827D-01
30	0.20188880E 01	0.20301383D 01	-0.10137D-01	0.20200D 01	-0.50182D-02
31	0.21088880E 01	0.21248317D 01	-0.14532D-01	0.21100D 01	-0.68872D-02
32	0.21788880E 01	0.21829044D 01	-0.28081D-02	0.21800D 01	-0.13244D-02
33	0.18888880E 00	0.18450128D 00	0.54887D-02	0.18000D 00	0.28841D-01
34	0.11288880E 01	0.11547848D 01	-0.24785D-01	0.11300D 01	-0.21807D-01
35	0.18788880E 01	0.18843084D 01	-0.14308D-01	0.18800D 01	-0.88173D-02
36	0.18088880E 01	0.18153007D 01	-0.83008D-02	0.18100D 01	-0.27783D-02
37	0.20288880E 01	0.20348180D 01	-0.45182D-02	0.20300D 01	-0.22287D-02
38	0.21088880E 01	0.21088778D 01	0.10218D-02	0.21100D 01	0.48424D-03
39	0.88888880E 00	0.88087081D 00	0.81282D-02	0.87000D 00	0.94118D-02
40	0.18888880E 01	0.18888288D 01	0.14871D-01	0.18700D 01	0.82485D-02
41	0.18188880E 01	0.18113874D 01	0.85121D-02	0.18200D 01	0.47318D-02
42	0.18888880E 01	0.18820810D 01	0.78380D-02	0.18800D 01	0.40800D-02
43	0.20488880E 01	0.20407818D 01	0.82374D-02	0.20500D 01	0.40818D-02
44	0.88888880E 00	0.81280088D 00	-0.15380D 00	0.88000D 00	-0.22273D 00
45	0.12188880E 01	0.14411034D 01	-0.12110D 00	0.13200D 01	-0.91748D-01
46	0.18388880E 01	0.17238387D 01	-0.33837D-01	0.18400D 01	-0.51181D-01
47	0.18088880E 01	0.18418713D 01	-0.71872D-01	0.18100D 01	-0.38708D-01
48	0.18288880E 01	0.18823024D 01	-0.52304D-01	0.18300D 01	-0.27101D-01
49	0.38888880E 00	0.54808824D 00	-0.14908D 00	0.40000D 00	-0.37272D 00
50	0.10888880E 01	0.12087842D 01	-0.13878D 00	0.10700D 01	-0.12871D 00
51	0.14288880E 01	0.15284177D 01	-0.10842D 00	0.14300D 01	-0.78818D-01
52	0.18488880E 01	0.17311441D 01	-0.81144D-01	0.18500D 01	-0.48178D-01
53	0.17888880E 01	0.18554888D 01	-0.88488D-01	0.17800D 01	-0.38873D-01
54	0.28888880E 00	0.38889470D 00	-0.88888D-01	0.27000D 00	-0.38854D 00
55	0.87888880E 00	0.70181022D 00	-0.13810D 00	0.88000D 00	-0.18883D 00
56	0.12888880E 01	0.13788888D 01	-0.10888D 00	0.12700D 01	-0.88803D-01
57	0.15088880E 01	0.15878810D 01	-0.87882D-01	0.15100D 01	-0.57888D-01
58	0.18888880E 01	0.17414340D 01	-0.71438D-01	0.18700D 01	-0.42778D-01
59	0.82888880E 00	0.53188388D 00	0.88418D-01	0.83000D 00	0.18822D 00
60	0.10788880E 01	0.82131787D 00	0.18888D 00	0.10800D 01	0.14883D 00
61	0.12888880E 01	0.11917284D 01	0.18888D 00	0.13800D 01	0.13272D 00
62	0.15488880E 01	0.13838847D 01	0.18821D 00	0.15500D 01	0.10730D 00
63	0.32888880E 00	0.28918844D 00	0.30803D-01	0.33000D 00	0.82343D-01
64	0.78000000E 00	0.88348875D 00	0.88814D-01	0.75000D 00	0.12888D 00
65	0.10588880E 01	0.93282848D 00	0.12717D 00	0.10800D 01	0.11897D 00
66	0.12888880E 01	0.11838884D 01	0.14814D 00	0.12900D 01	0.11288D 00
67	0.18888880E 00	0.18408881D 00	0.89403D-02	0.17000D 00	0.34843D-01
68	0.81888880E 00	0.48281883D 00	0.87181D-01	0.82000D 00	0.10888D 00
69	0.82888880E 00	0.73234388D 00	0.87888D-01	0.83000D 00	0.11788D 00
70	0.10888880E 01	0.84838878D 00	0.12080D 00	0.10700D 01	0.11271D 00

NUMBER OF DEGREES OF FREEDOM = 0.88000D 02
 R.M.S. SCALED DEVIATION OF DATA FROM FIT = 0.11730D 00
 MAXIMUM SCALED DEVIATION = 0.38842D 00

SUBROUTINE MOZRR.
 OSAY (PT=P, SCALED, WHERE P IS THE JACOBIAN)....

```

1  0.1000000 01
2  -0.8884828D 00  0.1000000 01
3  0.8883237D 00 -0.8885110D 00  0.1000000 01
4  0.1418108D 00 -0.1478237D 00  0.1313248D 00  0.1000000 01
    
```

```

NUMBER OF DEGREES OF FREEDOM (N.D.F.) = (NPTS-NACTV) = 88
EXPECTED VALUE OF PHI = N.D.F. PLUS OR MINUS SORT(2*N.D.F.) = 88 PLUS OR MINUS 0.11488D 02
ACTUAL VALUE OF PHI = 0.80808D 00
RESCALING FACTOR = SORT(PHI/N.D.F.) = 0.11730D 00
    
```

MAXIMUM VARIANCE INFLATION FACTOR = 0.23402D 04

APPROXIMATE STANDARD ERRORS....

J	MASK(J)	X(J)	ERROR	RESCALED ERROR
1	0	0.18787228D 10	0.10817D 11	0.12483D 10
2	0	0.82713488D 06	0.82388D 04	0.88816D 03
3	0	0.81886484D 00	0.87851D 00	0.87823D-01
4	0	0.82838576D 00	0.38472D 00	0.48300D-01

LOWER TRIANGLE OF THE CORRELATION MATRIX....

K	1	2	3	4
MASK(K)....	0	0	0	0
J	MASK(J)			
1	0	0.10000D 01		
2	0	0.80881D 00	0.10000D 01	
3	0	-0.78038D 00	-0.21887D 00	0.10000D 01
4	0	-0.87718D-01	0.12738D 00	0.2E103D 00 0.10000D 01

N-TH ORDER GLOBAL MODEL PARAMETERS

```

A = 0.1877D 10  WTZ=((1-N)/PSI)*M/HR
E = 0.8271D 06  STU/LB/MLE
M = 0.8187D 00
N = 0.8284D 00
    
```

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MEAN DEVIATION = 0.8908D-01
AVE. PERCENT ERROR = 0.7188D 01
F88J = 0.8081D 00
SUM OF SQUARES = 0.8087D 00
    
```

STATEMENTS EXECUTED: 73778

CORE USAGE OBJECT CODE: 43618 BYTES, ARRAY AREA: 85448 BYTES, TOTAL AREA AVAILABLE: 128024 BYTES

DIAGNOSTICS NUMBER OF ERRORS: 0, NUMBER OF WARNINGS: 0, NUMBER OF EXTENSIONS: 10

COMPILE TIME: 0.28 SEC, EXECUTION TIME: 1.34 SEC, 15.08.88 TUESDAY 28 JUL 83 WATFIV - MAR 1980 Y2L0

CSSTOP

2

VITA

Thomas Mason Pendergast

Candidate for the Degree of

Master of Science

Thesis: MATHEMATICAL MODELING OF COAL LIQUID HYDROTREATMENT KINETICS

Major Field: Chemical Engineering

Biographical:

Personal Data: Born in Terre Haute, Indiana, November 25, 1958,
the son of Mr. and Mrs. James H. Pendergast.

Education: Graduated from Terre Haute North Vigo High School,
Terre Haute, Indiana, in June, 1977; received Bachelor of
Science degree in Chemical Engineering from Rose-Hulman
Institute of Technology in 1981; completed requirements
for the Master of Science degree at Oklahoma State Univer-
sity in December, 1983.

Professional Experience: Summer Engineer, DOW Chemical U.S.A.,
1981; graduate teaching assistant, School of Chemical
Engineering, Oklahoma State University, 1981; graduate
research assistant, School of Chemical Engineering, Okla-
homa State University, 1982-83.