

PARTICULATE-INDUCED SEIZURE OF
PISTON-BORE ASSEMBLIES

By

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CHAPTER I

INTRODUCTION

There are two distinct modes of seizure. One is the seizure caused by welding between two sliding surfaces. The other seizure is caused by a third body which enters and wedges between two sliding surfaces. This third body bridges the clearance and prevents sliding motion. This is called particulate-induced seizure. There are two types of this mode of seizure. One type occurs when the third body, called a transfer element, is a result of surface contact wear and is a mixture of the two sliding surface materials. These transfer elements are known to grow in size as they combine together, and they cause seizure when they bridge across the two sliding surfaces. The other type occurs when the third body is composed of material different than that of the sliding surfaces. As the fluid media flows between the sliding surfaces, it transports foreign particulates which induce seizure. The following study examines the nature of this second type of particulate-induced seizure known to occur among piston-bore assemblies.

For years, piston-bore assemblies have been used for various industrial applications, and as the fluid power industry has grown, these applications have become more sophisticated and extensive. However, research scientists have never understood the classical problem of

piston-bore assemblies: seizure of the assembly. Especially with the recent stringent requirements imposed upon the assembly such as high pressure and tight clearance, understanding the mechanism of particulate-induced seizure and the force required to break the seizure has become critical. Although researchers have attempted to analyze the process of particulate-induced seizure, none have offered a successful method to predict the occurrence of seizure nor to assess the force required to break seizure. Researchers attempted to prevent particulate-induced seizure by applying dither to the assembly, but as of yet, this method has not proven successful.

This study therefore examines the nature of the particulate-induced seizure of a piston-bore assembly in order to predict the force required to break seizure and thus avoid catastrophic failures associated with the seizure of a piston-bore assembly. Three theoretical models were first developed. The first model is the silt process model which describes how solid particles silt in the clearance of a piston-bore assembly. The second model is the particulate-induced seizure model developed from the stress relation of three interacting bodies: the piston, the bore, and the particle. The force required to break the seizure of a piston-bore assembly was found from the three body stress relation and the assembly geometry. The third model, the dither model, predicts that when a piston-bore assembly is treated as a filter, the higher the dither frequency, the lower the assembly filtration efficiency.

To verify the integrity of these models, a computer simulation program that combines the first two models is developed. Experiments for

each model are performed, and the results are compared against the computer simulation results.

CHAPTER II

PREVIOUS INVESTIGATIONS

The study of seizure on piston-bore assemblies began in the early 1950's. Sweeney [1] conducted experimental and analytical studies on the phenomenon called "hydraulic lock." He believed that when an axial pressure exists on one surface of a piston, the non-uniform pressure distribution in the clearance of the piston-bore assembly caused the piston to adhere to the bore. Sweeney observed that when the measured leakage flow corresponds to the mathematical leakage flow model with an eccentricity of one, hydraulic lock occurs. This suggests that when the piston sticks to the bore, indicating an eccentricity of one, more frictional force exists to retard the spool movement.

In contrast, Stringer [2] stated that dirt in the oil caused hydraulic lock, and this locking force is ten times as great as those reported by Sweeney.

Mannam [3] summarized the analytical investigation of hydraulic lock. He presented an approximate pressure distribution in the clearance assuming that the hydraulic fluid is incompressible and has constant viscosity. The analytical equation he used to obtain the approximate solution is

$$\frac{\partial}{\partial x} \left(h^3 \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial y} \left(h^3 \frac{\partial P}{\partial y} \right) = 0 \quad (1)$$

where

p = the pressure at point x,y on the surface of the piston

h = radial clearance

x = axial direction

y = circumferential direction

Figure 1 presents possible applications of the equation.

When the land surfaces of the piston and bore are perfectly parallel to each other in the clearance (Fig.1a), there is no lateral force. In addition, a movement will be generated to correct any tilting of the piston axis relative to the bore axis if the tilting occurs (Fig. 1b).

When the land of the piston has a uniform taper in the axial direction, there will be no resultant lateral force, provided that there is no eccentricity. However, if an eccentricity exists, then a clearance forming a taper diverging in the direction of axial flow would have a lateral resultant force proportional to the magnitude of the eccentricity (Fig. 1c). On the other hand, a tapered piston with a converging clearance in the direction of axial flow has the centralizing resultant force to reduce the eccentricity (Fig. 1d).

Mannam also indicated that the grooves in the piston land and stepped land reduce this lateral force; therefore, less hydraulic lock force occurs. Mannam did not give any details about the effect of dirt, although he was aware of its importance.

In 1966, Dransfield et. al. [4] also analytically investigated the hydraulic lock. To simulate the hydraulic lock they developed a mathematical model which includes the eccentricity and elliptic shape of

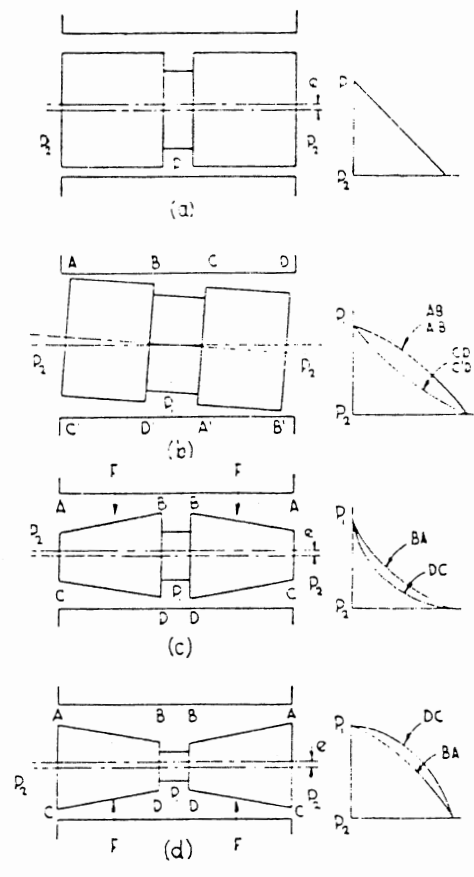


Figure 1. Examples of Piston Pairs [3].

a piston cross section. They found that the elliptic shape increases the locking force.

In 1967, Dransfield [5] published experimental results on the hydraulic lock using the fixture shown in Fig. 2. Dransfield measured two parameters out of this experimental fixture: 1) leakage, and 2) force required to move the yoke. Dransfield and Bruce [6] developed the leakage equation including the pressure effect on the piston-bore geometry and pressure and temperature effect on viscosity. Figure 3 shows the measured results of both leakage and force required to move the yoke. Dransfield found that the hydraulic lock force is a function of the axial pressure, and, as the applied pressure increases, the measured force increases to its maximum peak and decreases to zero. The leakage flow correlates closely with the hydraulic lock force. When the hydraulic force disappears at a certain pressure level, the leakage flow also decreases from an eccentricity one leakage down to an eccentricity near zero.

The existence of a maximum peak and gradual decrease of hydraulic lock force, first found and analyzed by Whiteman [7], is further researched by Dransfield and Bruce. They considered that very high axial pressure, creating the expansion of the clearance, also caused the decrease in the lock force. High axial pressure reduces the diameter; thus, the clearance forms a taper converging in the direction of the axial leakage flow. Consequently, the assymmetric pressure distribution in the clearance acts to reduce the eccentricity.

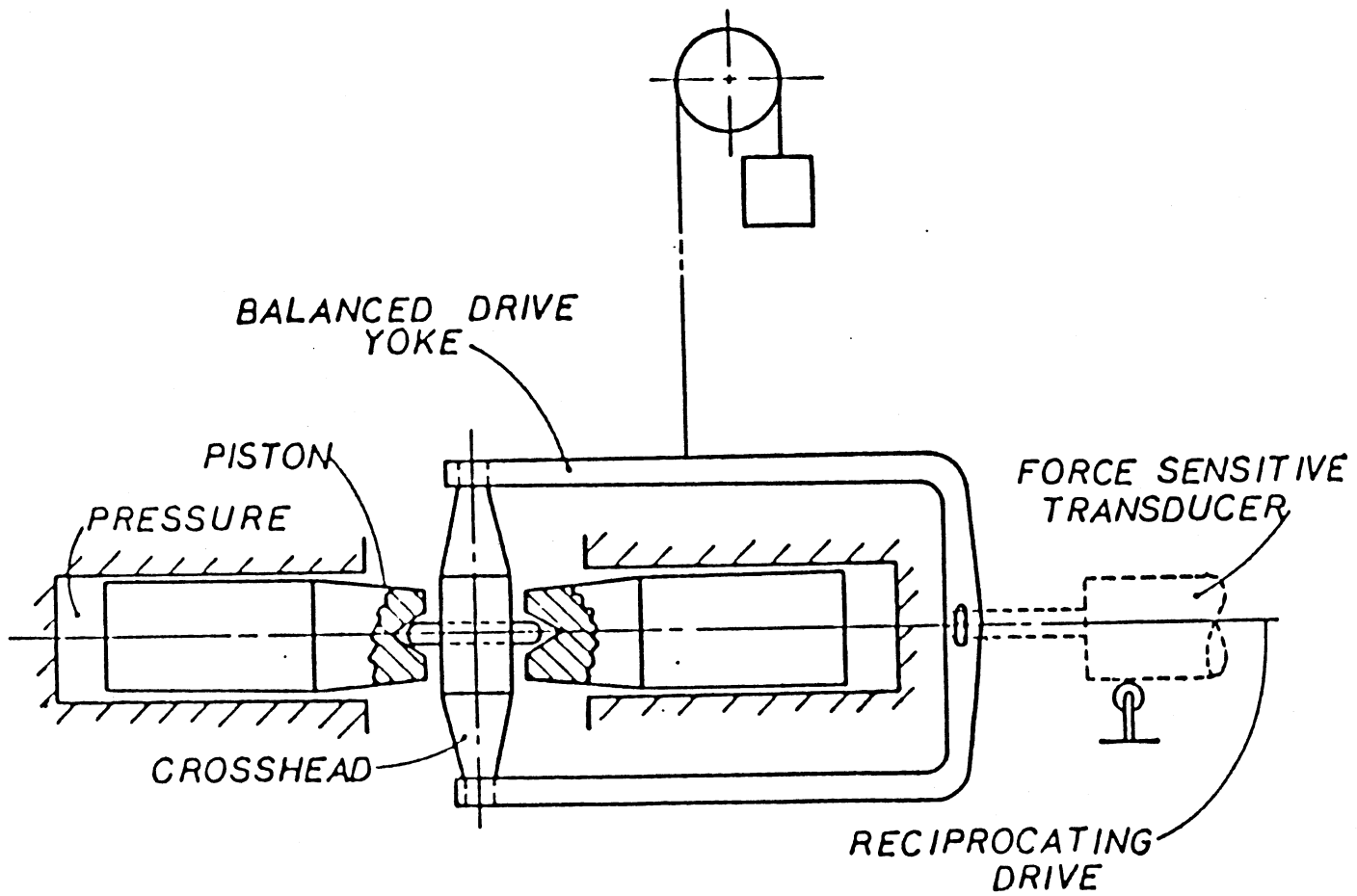


Figure. 2. Experimental Piston-Cylinder Set Up [5].

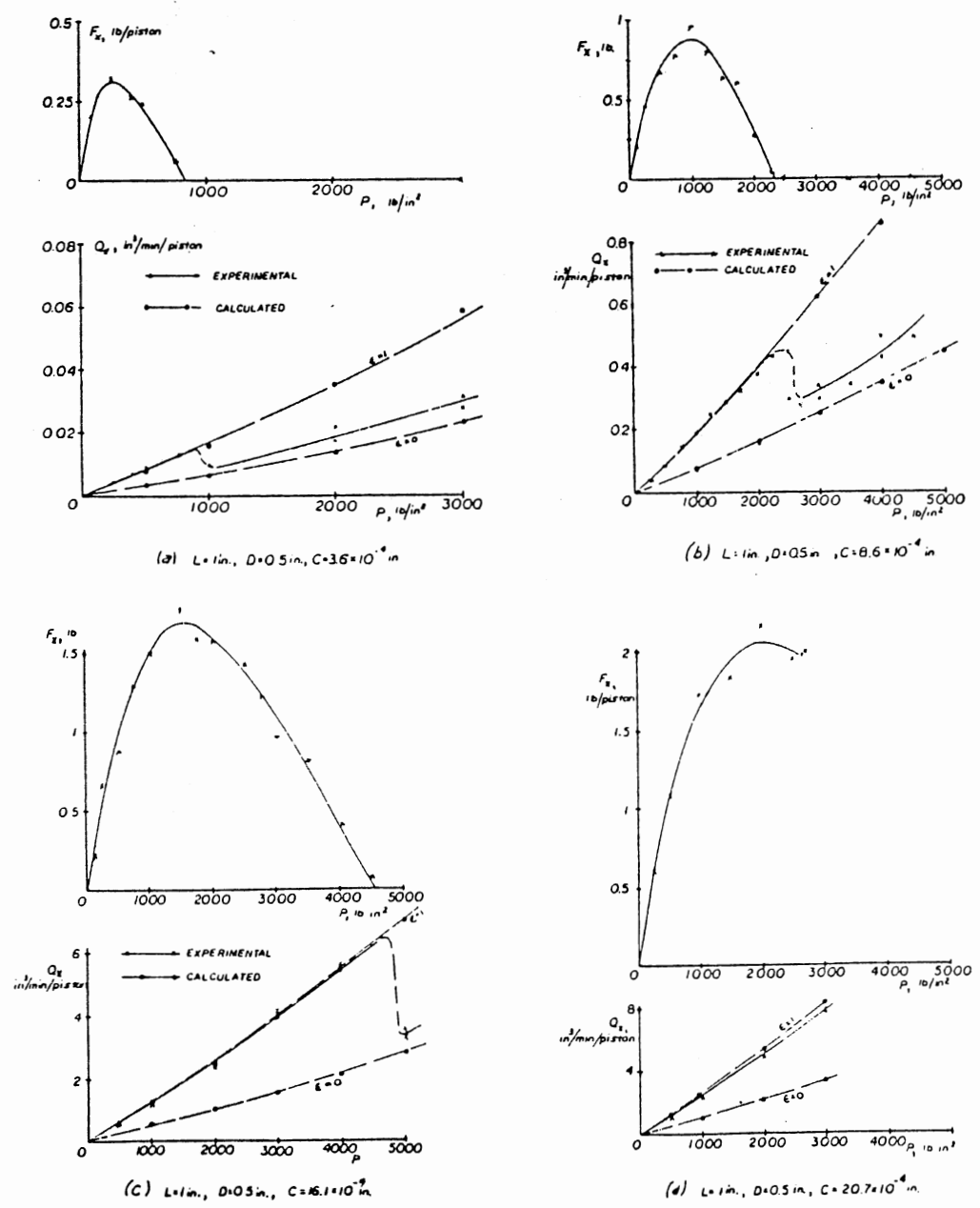


Figure. 3. Break-Out Force (F_x) and Leakage Flow Rate (Q_x) Versus Pressure Characteristics, for Various Diametral Clearances (C) [6].

Dransfield and Bruce revealed other important evidence:

- (1) The larger the clearance, the greater the maximum force required to overcome the seizure.
- (2) The decrease in leakage flow takes place within a 100 to 500 psi range of pressure changes at which the lock force decreases close to zero.

In 1970, Kamijo and others [8] investigated the importance of the curve effect in the spool axis. They pointed out that if the effect of elastic deformation occurred only as Whiteman and Dransfield suggested, then the lock force reduction would occur at a much higher pressure (Fig. 4). When Kamijo and others included the curving effect in the spool axis and calculated the pressure distribution and its resultant force, they found a close agreement with the experimental result shown in Fig. 4 (elastic deformation and inclination of spool).

Kamijo and others, who built the experimental apparatus to measure the pressure distribution in the piston-bore assembly clearance (Fig. 5), were the first to prove experimentally that an asymmetric pressure distribution exists in the clearance (Fig. 6). Figure 6 also shows the variable viscosity pressure curve, which takes into account the pressure and temperature effect on viscosity and shows a better fit to the actual pressure values than the constant viscosity pressure curve.

Using the same apparatus, Kamijo et. al. analyzed the dirt effect on pressure distribution in the clearance. Dirt filtered by a 10-micrometre mesh was injected into hydraulic fluid circulating through the test apparatus. Figure 7 demonstrates the measured result of the pressure

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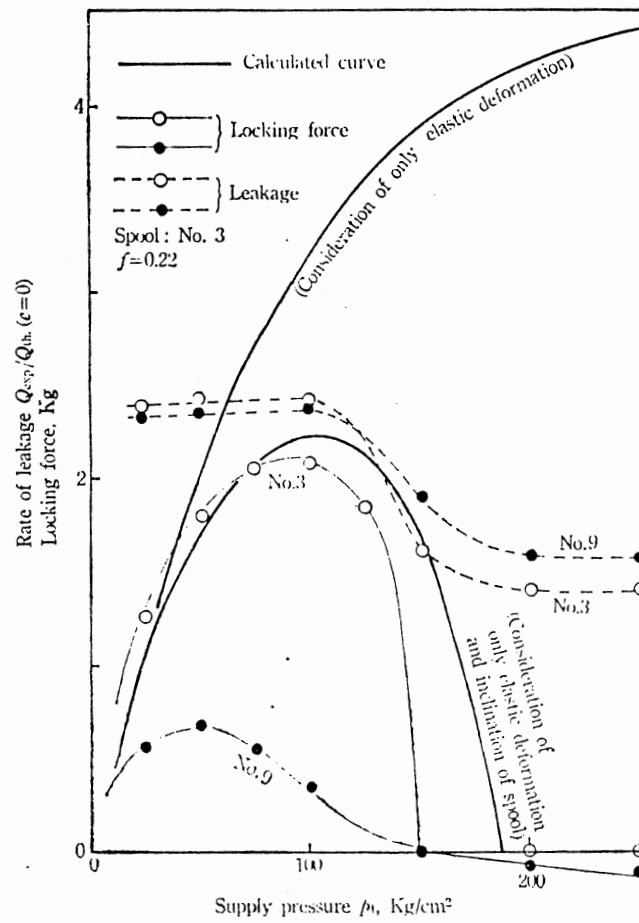


Figure 4. Locking Force and Leakage at Higher Pressure [8].

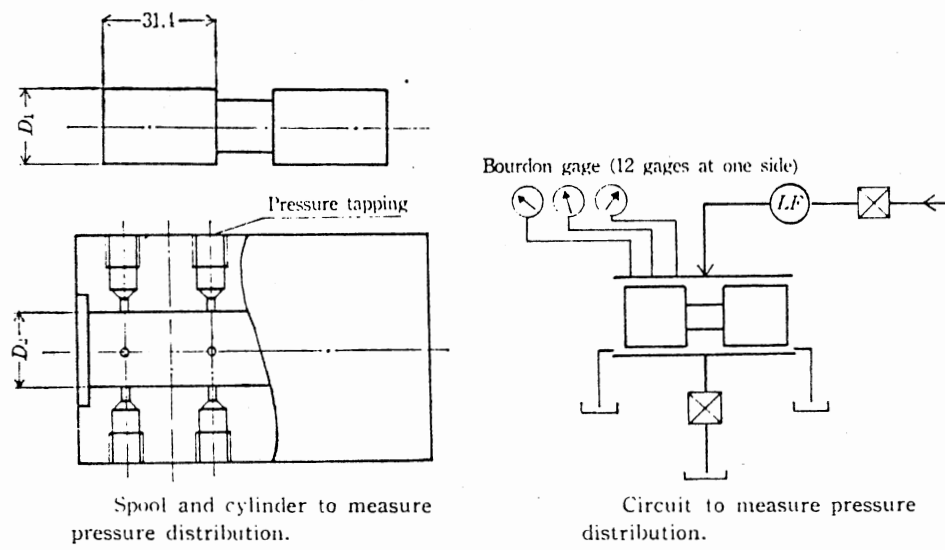


Figure. 5. Pressure Distribution Measurement Apparatus [8].

Hydraulic Lock on Spool Valve (2nd Report)

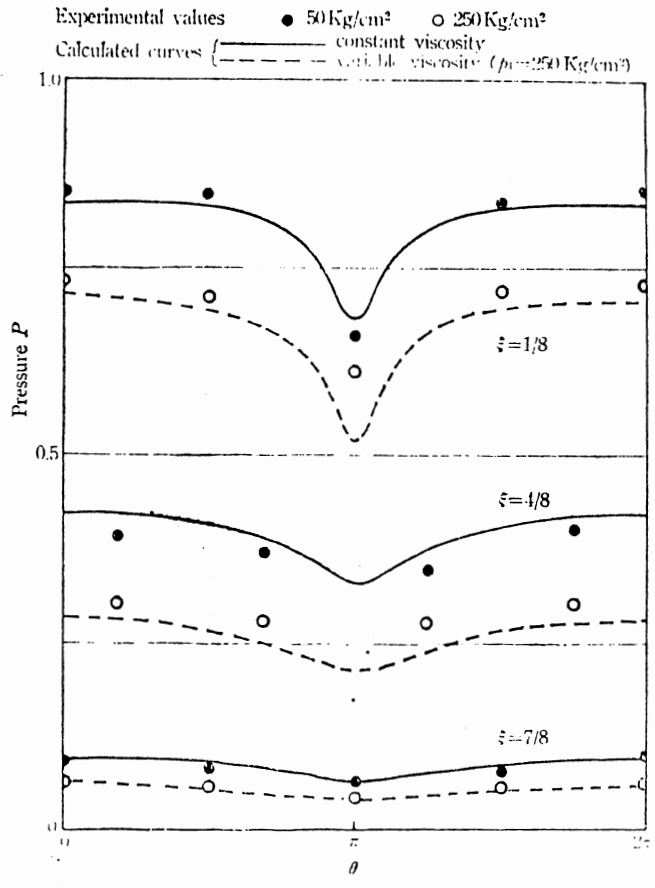


Figure. 6. Pressure Distribution Around Tapered Spool [8].

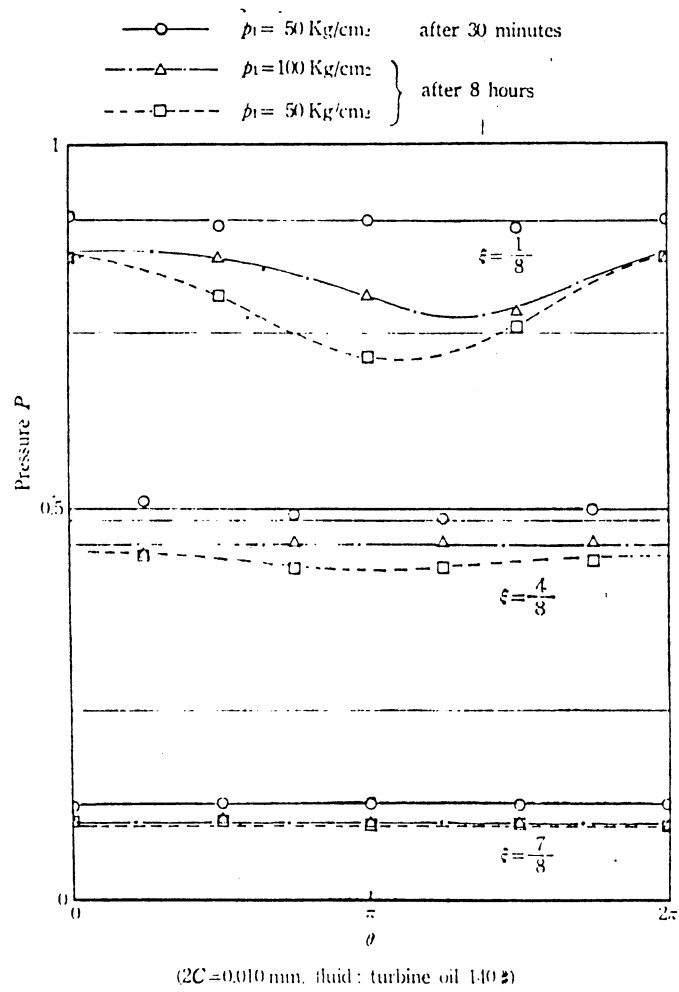


Figure. 7. Influence of Dirts on Pressure Distributions With Parallel Spool [8].

distribution. Kamiyo and others verified in the same report that the hydraulic lock has a very short delay or saturation time. Therefore, the long development time observed in Fig. 7 proves that the dirt causes the non-uniform pressure distribution. In addition, Figure 7 suggests that dirt tends to accumulate in the neighborhood of the inlet. This agrees with the work of Laurenson [9]. He also found that when the clearance was increased to 22 micrometres under the same test conditions as before, no pressure fall took place.

Kamiyo and others continued their experiments to apply dither on the piston of the piston-bore assembly. The dither amplitude was fixed to be 0.05 mm., and the frequency was also set at 20 Hz. Figure 8 shows the dither effect on the clearance pressure distribution. Obviously, the dither is capable of preventing or minimizing the non-uniform pressure distribution in the clearance.

In 1976, Surjatmadja and Fitch [10] published a series of papers on particulate-induced seizure and proposed four modes of particulate-induced seizure. No experimental results were presented.

Iyenger [11] also conducted experiments on particulate-induced seizure in 1976. He observed that the force required to break seizure increases with time until the force reaches a saturation level. He found that ACFTD 0-5 micrometre, lower-cut dust causes the most severe lock on the test valve with a design clearance between 3.8 to 7.6 micrometres.

Inoue [12], in 1980, developed an analytical model to predict the force required to break particulate-induced seizure, and the model incorporates the derivative of a constant filtration model to account

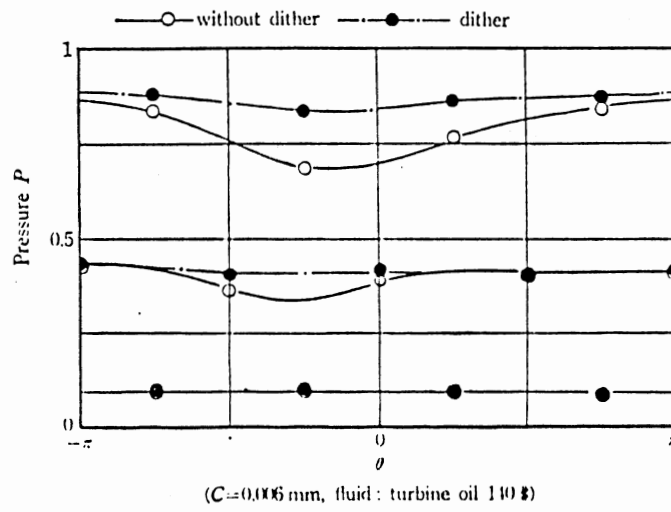


Figure. 8. Effect of Dither on Pressure Distributions With Parallel Spool [8].

for the silt process of particles and the reduction in leakage flow through the clearance. Due to many unknown parameters included in his model, one who plans to use the model must first conduct experiments to identify unknown parameters. He also presented experimental data demonstrating the strong influence of particle size distribution on particulate-induced seizure force, and he found the induced force to be over 50 lbf, which is considerably higher than the force required to break the hydraulic lock.

Nikitin and Chekov [13] reported experimental results on the dither effect to seizure (Fig. 9). However, the report lacks detailed information of piston-bore geometries and test conditions.

Nair [14] surveyed the work performed on the study of dither. He presented the proportional control valve performance data illustrating that dither reduces the effect of particulates in the fluid.

Ito [15] hypothesized that particles close to the clearance size are the major source of particulate-induced seizure. He presented experimental data supporting his postulate.

Sasada and Michina [16] verified with their experiments that wear particles close to the size of the piston-bore clearance caused seizure.

One of the difficulties in analyzing the particulate-induced seizure is the fact that in the past no researcher had a quick and convenient method to analyze the size distribution of the particulate or dirt. As a result, researchers could only roughly regulate the size distribution by filtering particles through a mesh having an approximate size. This approach normally could only provide a coarse control over the upper

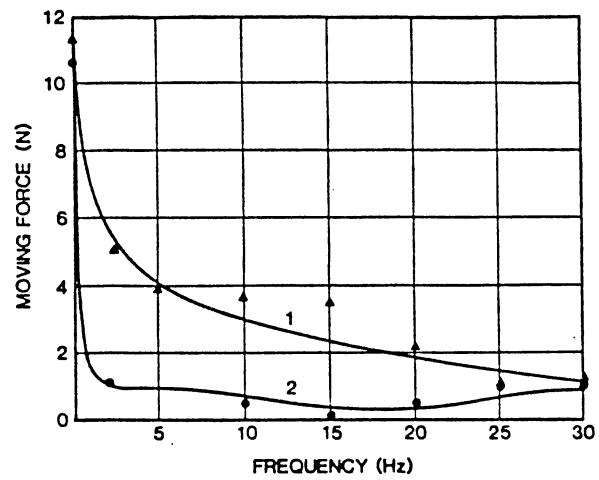


Figure. 9a. Frequency of Oscillations on the Force Necessary for Movement of Plunger of Spool Valve [13].

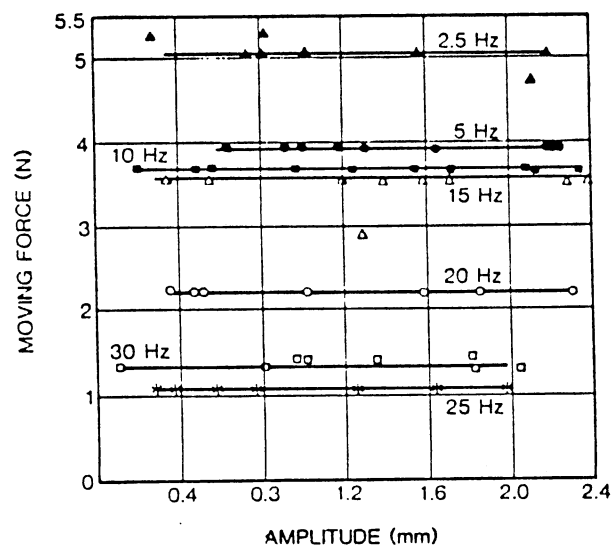


Figure. 9b. Effect of Magnitude of Amplitude and Frequency of Oscillations on the Force Necessary for Movement of Plunger of Spool Valve [13].

limits of particle size.

From the early 1970's to the mid 1970's, Erwin and Bensch [17] established the ACFTD particle size distribution. Cole, and later Bensch and Fitch [18, 19], presented an analytical model to describe particle size distribution, and this model was applied to ACFTD. Though useful particle counting techniques and particle size distribution models are now available, no researcher to date has used this technology to investigate the particulate-induced seizure.

Since particulate-induced seizure occurs only when particles are deposited in the clearance, this silting process can be investigated by treating the piston-bore assembly as a filter.

Fluid Power Research Center (FPRC) has investigated the particle separation mechanisms in a fibrous filter for many years and has identified the following types:

1. Seiving
2. Direct Interception
3. Inertial Impaction
4. Brownian Diffusion
5. Gravity Settling
6. Electrostatic Precipitation
7. Obliteration

The second through the fifth mechanisms are minor mechanisms compared to the others because although they may capture particles, they have very poor retention (dirt holding) capability. In addition, the seventh mechanism becomes significant only at the freezing temperature (0 degrees

Celsius) [26]. Therefore, the sieving and electrostatic precipitation mechanisms are the two known to most effectively capture and retain particles, thus being the main mechanisms of the silt process in piston-bore assemblies. Of these two mechanisms, sieving contributes to the seizure the most because particles large enough to bridge the clearance are suspected of being the major cause of the seizure.

To summarize, there is no analytical model which could estimate the required force to break particulate-induced seizure for a given set of conditions of contaminant size, fluid flow rate, piston-bore design, and pressure drop. Furthermore, the theoretical and experimental studies of the effect of dither on particulate-induced seizure are seriously lacking.

CHAPTER III

DEVELOPMENT OF THEORETICAL MODELS

Silt Process (Silt Beta) Model

To analyze how particles silt in the clearance of a piston-bore assembly, the system must be first described and then analyzed according to known models developed in the current work. The description of the assembly system starts with a list of vital inputs and outputs listed in Fig. 10, and then the relationships of these parameters are investigated.

The relationship between the axial pressure difference and the leakage flow through the clearance is described by:

$$Q(\tau) = \frac{\pi D h^3 (1 + 1.5 (e/h)^2)}{12 \mu L} (P_u - P_d) \quad (2)$$

where

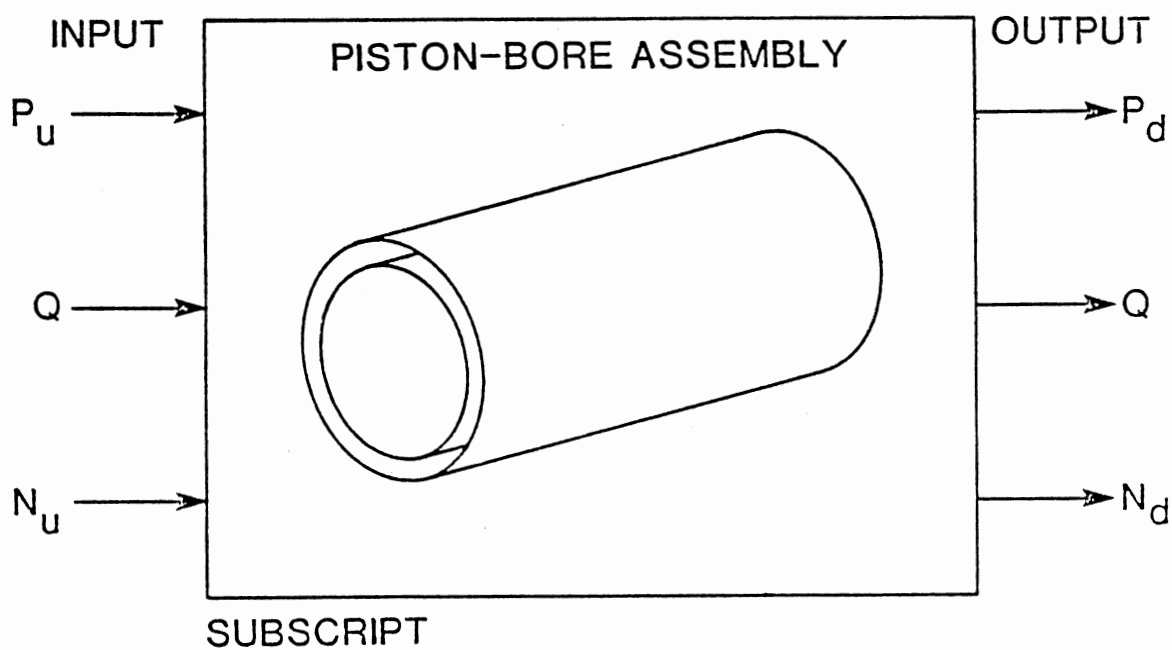
e = eccentricity

h = nominal clearance

P_u = upstream axial pressure

P_d = downstream axial pressure

D = bore diameter



u - UPSTREAM
d - DOWNSTREAM

PARAMETER

P - PRESSURE
Q - LEAKAGE FLOW
N - PARTICLE SIZE DISTRIBUTION

Figure. 10. Input and Output of Piston-Bore Assemblies.

μ = viscosity (including pressure and
temperature effect)

L = piston land length

However, as soon as particulate contaminants enter the clearance of the piston-bore assembly, the leakage flow decreases. Particles silt up in the clearance, causing the effective clearance size h to decrease with time. In order to model the decrease of the leakage flow, the particle size distribution upstream (N_u) and downstream (N_d) from the assembly have to be defined. The difference between the two particle size distributions indicates the process of particle silting per unit volume of leakage through the clearance of the piston-bore assembly. The upstream and downstream particle size distribution are mathematically modeled [17-19], and the difference between the two distributions are represented by the Beta rating system. The ratio of the number of particles for a given size upstream vs. downstream is the Beta value used in the Beta rating system. The larger the value of Beta, the more the particles at the evaluated particle size are retained by the assembly. Therefore, the Beta value evaluated at the nominal clearance size will be referred to as the silt Beta β . The silt Beta value and the number of particles greater than 1 micrometer downstream (NT_d) define a downstream particle size distribution.

Therefore, the volume of particles silted in the clearance can be found by a three step procedure:

Step 1. Find particle size distribution upstream (ND_u) and downstream (ND_d):

$$NDu = NTu e^{(-Bu \ln^2(D))} \quad (3)$$

$$Bd = Bu + \ln(NTd / NTu \beta) / \ln^2(h) \quad (4)$$

$$NDd = NTd e^{(-Bd \ln^2(D))} \quad (5)$$

where

h = nominal clearance size.

Step 2. Find the total volume occupied by each particle size distribution per unit volume of fluid (see references 17 to 19 for detailed derivations):

$$v_u = \frac{\pi NTu}{6 S} \left\{ 1 + 3 \sqrt{\frac{\pi}{Bu}} e^{(9/(4Bu))} \int_{-\infty}^{\frac{3}{\sqrt{2Bu}}} \frac{1}{\sqrt{2\pi}} e^{(-x^2/2)} dx \right\} \quad (6)$$

$$v_d = \frac{\pi NTd}{6 S} \left\{ 1 + 3 \sqrt{\frac{\pi}{Bd}} e^{(9/(4Bd))} \int_{-\infty}^{\frac{3}{\sqrt{2Bd}}} \frac{1}{\sqrt{2\pi}} e^{(-x^2/2)} dx \right\} \quad (7)$$

where

$$x/\sqrt{2} = y - 3/(2\sqrt{B})$$

$$y = Bi \ln D$$

'i' = subscript indicating either 'u' or 'd'.

'u' = upstream

'd' = downstream

Step 3. Compute the total volume of particles retained in the clearance by the difference between upstream and downstream volume.

$$V_t = v_u - v_d \quad (8)$$

In addition, find the frequency (number of particles for a given size) versus size by application of the equation:

$$f(D)_u = 2 NTu Bu \ln(D) / D e^{(-Bu (\ln^2(D)))} \quad (9)$$

The above equation is derived by taking a derivative of Eq. 3 with respect to particle size D . Thus, the frequency versus the size of particles retained in the clearance after a unit volume of leakage flow passes through the clearance is:

$$f(D)_t = f(D)_u - f(D)_d \quad (10)$$

Particles silted and retained in the clearance of the piston-bore assembly affect the leakage flow through the clearance described by Eq.

1. In order to find the reduction of the clearance size, the total volume of particles retained in the clearance within a unit time of Δt is:

$$\Delta S = \int_t^{t+\Delta t} v_t(t) Q(t) dt \quad (11)$$

Therefore, the reduction of clearance in unit time Δt is:

$$\epsilon = \Delta S / (2 \pi L (D - h)) \quad (12)$$

Then the clearance reduces to:

$$h = h - 2 \epsilon \quad (13)$$

The flow chart shown in Fig. 11 summarizes the entire silt process. Notice three different particle retention cases exist. The above steps describe the particle retention (silt Beta) case 1; however, the same

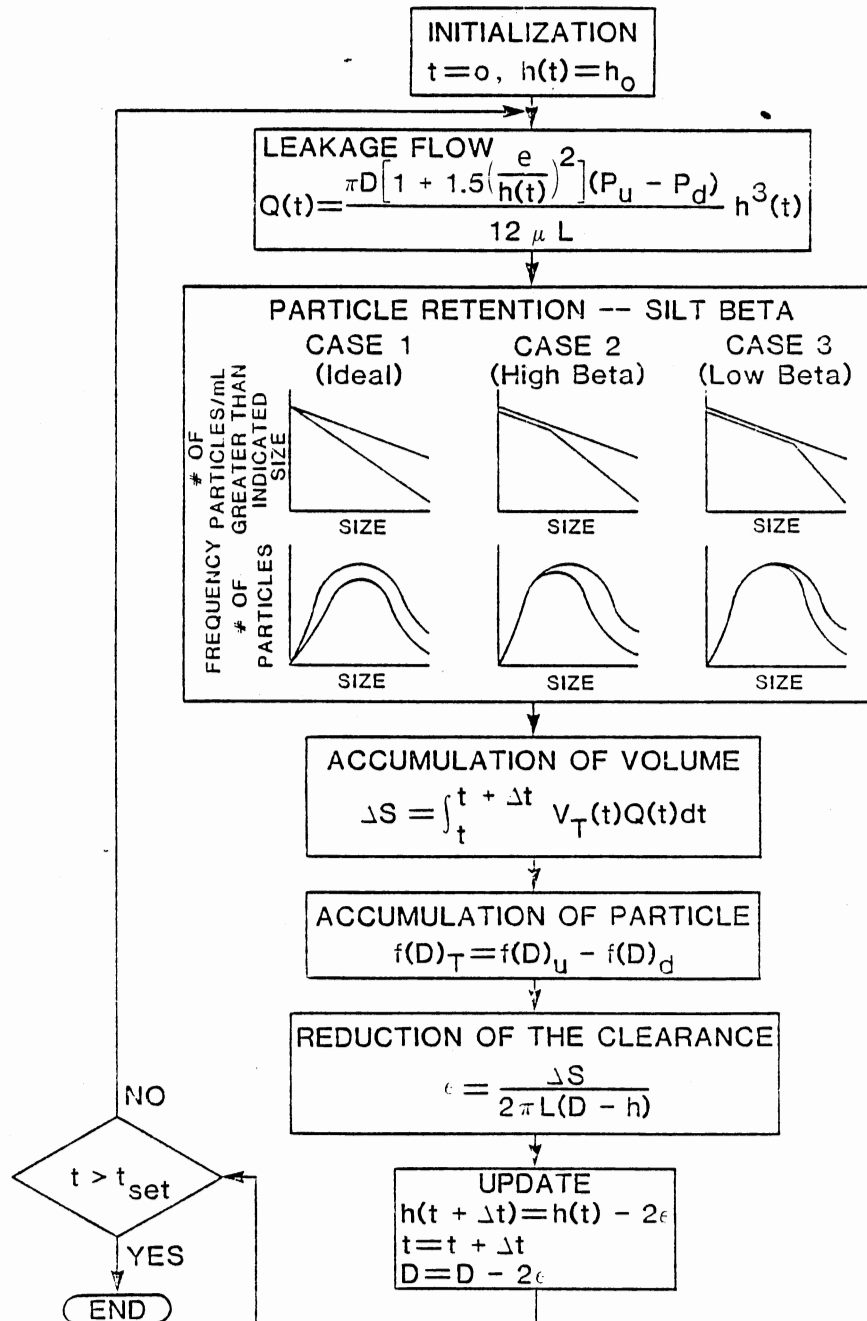


Figure 11. Silt Process Algorithm

approach applies to the linear approximation of cases 2 and 3. By fitting straight lines to the downstream particle size distribution and applying the above steps for each straight line segment, the silt volume V_t can be found. Then, the application of Eq. 11 through 13 enables an estimate to be made of the clearance and leakage reduction.

Particulate-Induced Seizure Model

Ito et. al. [21] obtained successful three body wear model results using the following hypothesis: a particle in the clearance of a piston-bore assembly continues to indent into both constraining surfaces of the piston-bore assembly as long as a sufficient force exists to maintain the surface pressures P_1 & p_1 equal to or above the lower yield strength of the two contacting surface materials (see Fig. 12). This means that when a particle has higher yield strength than the material of a piston-bore assembly, the particle indents into both surfaces of the piston-bore assembly, and when a particle has lower yield strength, the particle deforms.

Thus, the three body wear model was modified to predict the necessary force to break seizure. The criterion is that the contact pressure be equal to the yield strength (Fig. 12). Consequently,

$$P_1 = S_{yc} = FL \cos \theta \cos \gamma / (dc \ 1) \quad (14)$$

Solving for FL gives:

$$FL = S_{yc} \times dc \ 1 / (\cos \theta \cos \gamma) \quad (15)$$

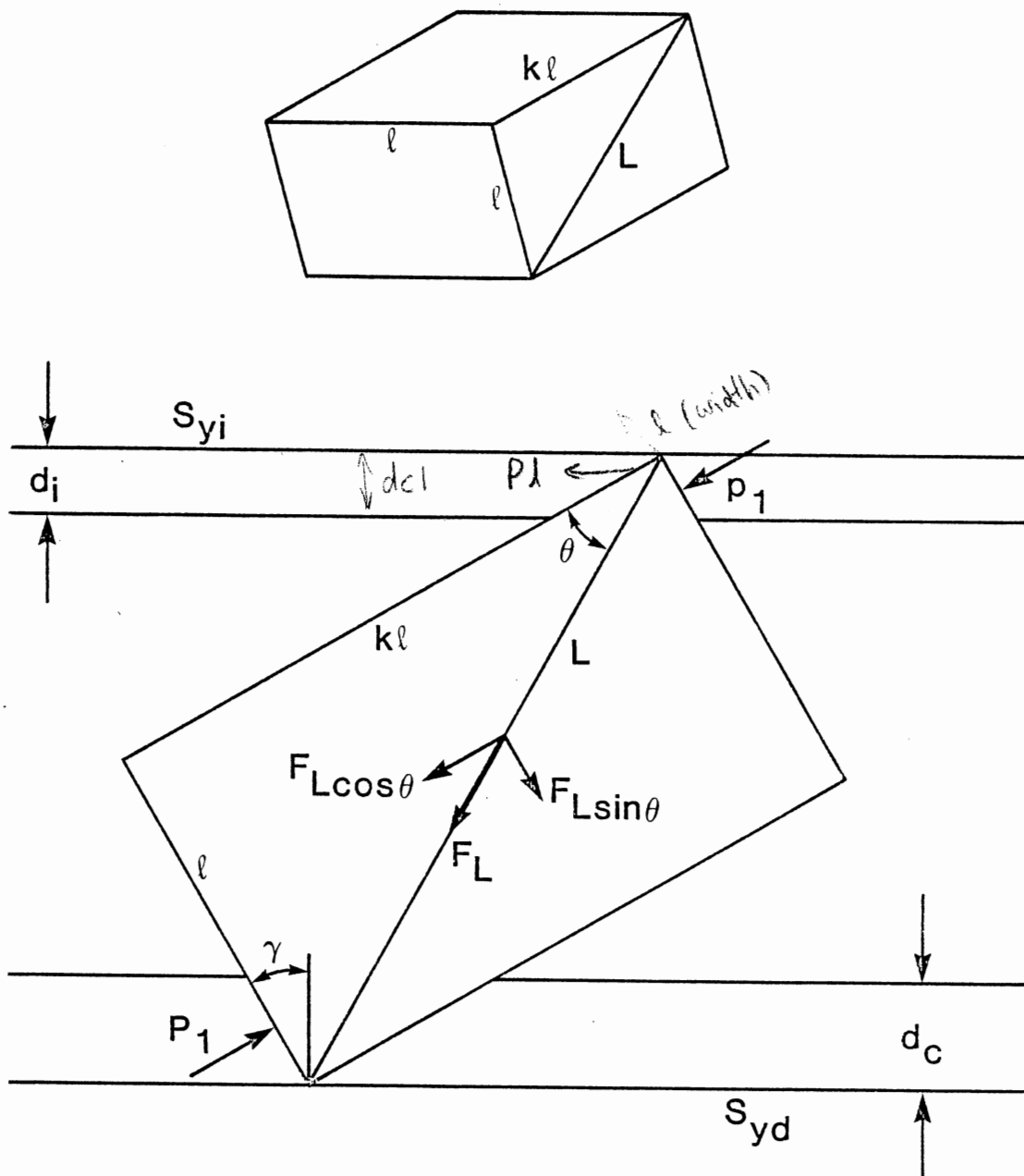


Figure. 12. Three Body Model.

Similarly, the force FL on the other surface is:

$$FL = S_{yi} \frac{d_i l}{\cos \theta \cos \gamma} \quad (16)$$

Area of cross section

Equations 15 and 16 are combined to eliminate FL, and the result is:

$$S_{yc} / S_{yi} = d_i / d_c \quad (17)$$

The above equation reveals an important relationship between the indentation depths and the yield strengths of a piston-bore assembly. Furthermore, the component of force FL that resists the movement of the spool is:

$$F_P = FL \cos(\theta + \gamma) \quad (18)$$

The geometrical relationship between the depth of indentations, particle size, and clearance size is given by:

$$d_i + d_c = L \sin(\theta + \gamma) - H \quad (19)$$

From Eq. 17 and 19, the following equation can be derived:

$$d_c = (L \sin(\theta + \gamma) - H) / (1 + S_{yc} / S_{yi}) \quad (20)$$

Equation 20 replaces dc in Eq. 15, resulting in:

$$FL = \frac{S_{yc} l (L \sin(\theta + \gamma) - H)}{\cos \theta \cos \gamma (1 + S_{yc} / S_{yi})} \quad (21)$$

From the particle geometry,

$$l = L \sin \theta \quad (22)$$

and Eq. 18, 21, and 22 may be combined to solve for FP:

$$FP = \alpha \frac{\{\sin(\theta + \gamma) - H / L\} \sin \theta}{\cos \theta \cos \gamma} \cos(\theta + \gamma) \quad (23)$$

where

$$\alpha = L^2 / (1 / S_{yc} + 1 / S_{yi}) \quad (24)$$

The above equation defines the force needed to achieve the rake angle.

The parameters of the above equation have the following limits. The limits of the rake angle are:

$$0 \leq \gamma \leq \left(\frac{\pi}{2}\right) - \theta \quad (25)$$

The ratio limits of the clearance size H to the size of a particle L is:

$$\sin \theta \leq H / L \leq 1 \quad (26)$$

Moreover, the length-to-width ratio [21] of a particle in nature is limited to:

$$1 \leq k \leq 1.5 \quad (27)$$

In order to closely simulate the conditions at which particulate-induced seizure occurs, the particulate-induced force equation must be applied in light of the piston-bore clearance information and the

probabilistic treatment on the particles' location inside the clearance. To accomplish such a task, the following two subsections develop two mathematical models which are essential for the prediction of the particulate-induced seizure of a given piston-bore assembly. These models are to find:

- (1) the force variation for a given piston-bore clearance condition and particle size.
- (2) the probability that particles contribute to the particulate-induced seizure.

Effect of Clearance Size and Particle Size on Particulate-Induced Seizure Force

If the length-to-width ratio of an ACFTD particle is 1.49 ($k = 1.49$) [20], then the ratio limits of the clearance size to a particle size is:

$$0.5573 \ (\theta = \text{atn}(1/1.49)) \leq H/L \leq 1 \quad (28)$$

And, the limits of the rake angle become:

$$0 \leq \gamma \leq 56.13 \quad (29)$$

Assuming that the value of alpha in Eq. 24 is unity, the effect of the rake angle and the ratio of the clearance H to the particle size L was investigated by developing the simulation program of Eq. 23 and 24. The result of the program is graphically presented in Fig. 13. This figure clearly illustrates how the particulate-induced force varies

H/L	.557	.704	.852	1
FPmax	.1164	.0675	.0263	0
FPavg	.0781	.0363	.0098	0

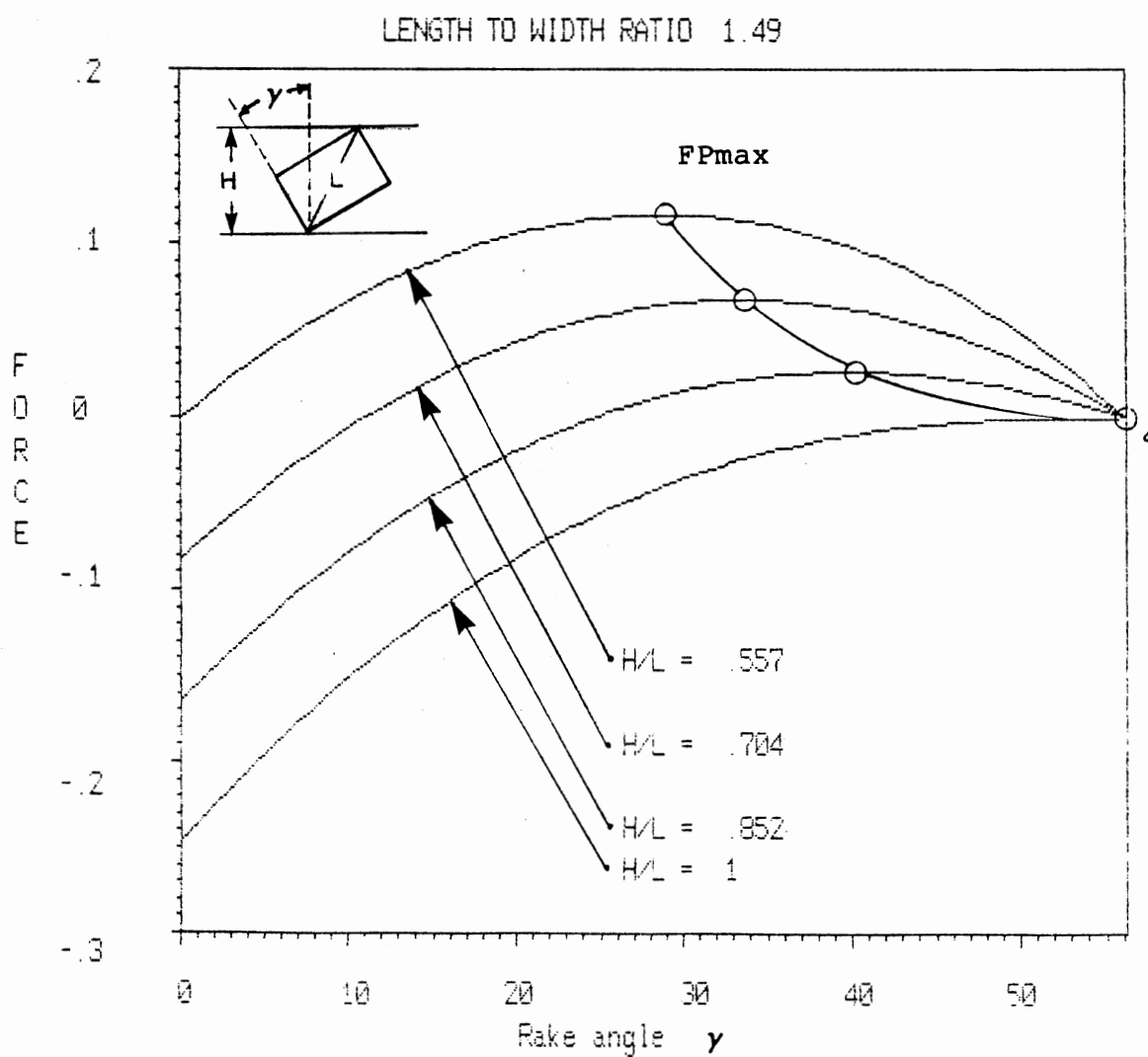


Figure. 13. Seizure Force.

according to a given rake angle: the size ratio of the clearance H to the particle size L . Note that the negative force is meaningless here because in order for a size L particle to touch the surfaces of the clearance and generate the induced force, the particle must rotate by increasing the rake angle and indenting the surfaces. Hence, no matter how much the rake angle increases, no force will be generated when the ratio H/L is one since the particle never indents the surfaces.

On the other hand, when the ratio H/L is less than unity, the particle eventually makes the indentation as the rake angle increases; thus, positive induced force occurs.

If the particle with its length-to-width ratio (k) is 1.49, the minimum of the ratio H/L is approximately 0.557. This occurs because when the ratio H/L becomes smaller than 0.557, the width of the particle becomes bigger than the size of the clearance, and the particle can no longer enter inside the clearance space.

Figure 14 plots the maximum and average force against the ratio H/L . FP_{\max} and FP_{avg} are smooth functions of H/L .

$$FP_{\max} = f(H/L) \quad (30)$$

$$FP_{\text{avg}} = g(H/L) \quad (31)$$

The straight line that connects the four data points shown in Fig. 14 closely approximates the true values between data points. Therefore, the computer simulation results, shown later, use the data derived from the straight line.

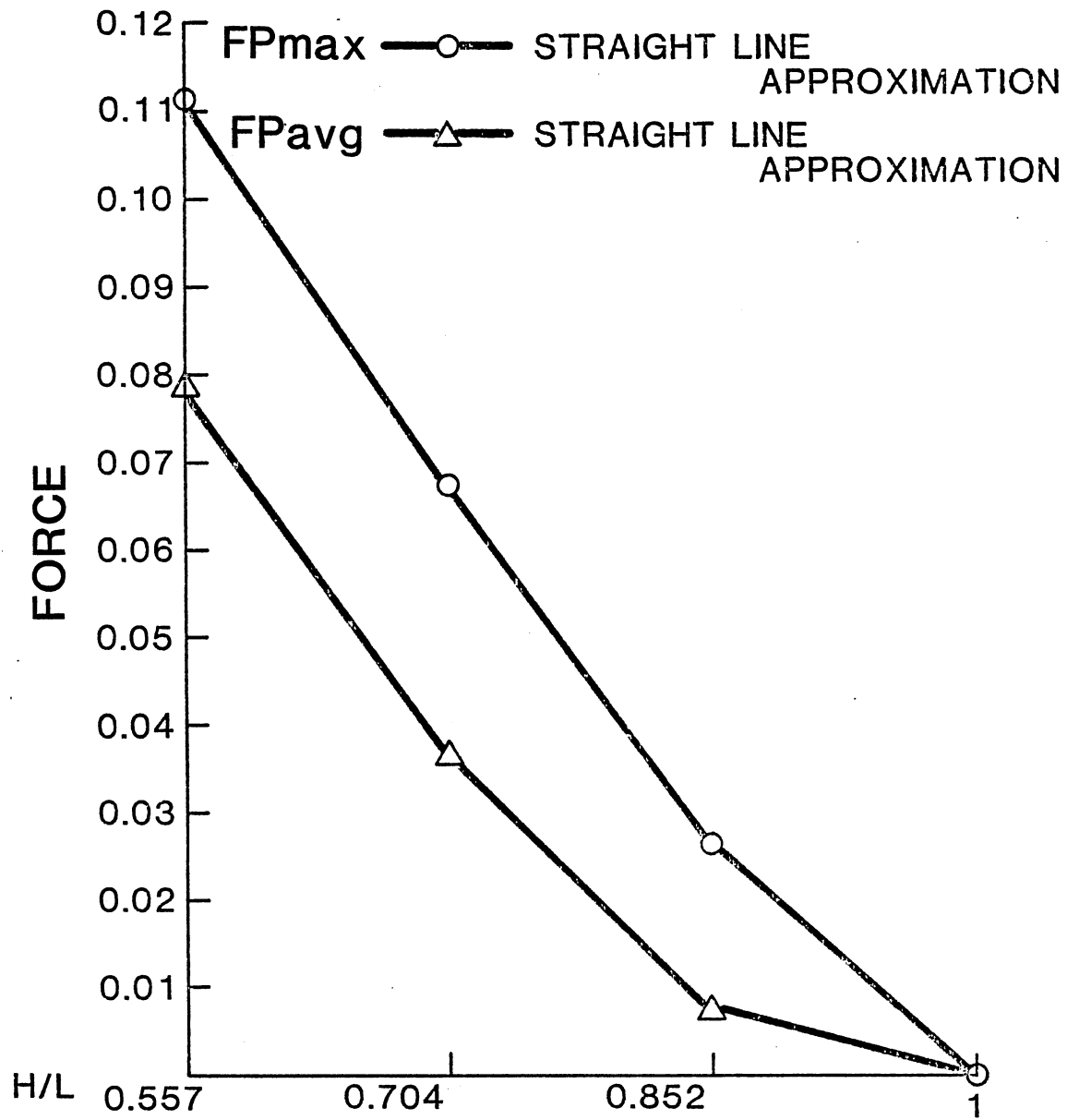


Figure. 14. Seizure Force Versus H/L.

Contribution of Silt Particles to
Particulate-Induced Seizure Force

Assuming that the piston-bore assembly exists with an eccentricity of one (a good assumption according to Dransfield's experiment), the cross sectional area that the size L particle can enter is presented in Fig. 15 and marked with the angle w_1 . In addition, the cross sectional area in which size L particles can contribute to the particulate-induced force is designated by the angle difference between w_1 and w_2 , and the corresponding magnitude for FP_{max} and FP_{avg} is also shown in Fig. 15. Thus, if the clearance is specified as a function of w ,

$$h = h(w) = \sqrt{R^2 + e^2 - 2 R e \cos(w)} - r \quad (32)$$

where

R = radius of the bore

e = eccentricity distance

r = radius of the piston

then, the cross sectional area pointed by w can be described by:

$$\text{Area}(w, 0) = \int_0^w h(w) \, dw \quad (33)$$

And, the area between w_1 and w_2 is:

$$\text{Area}(w_2, w_1) = \text{Area}(w_2, 0) - \text{Area}(w_1, 0) \quad (34)$$

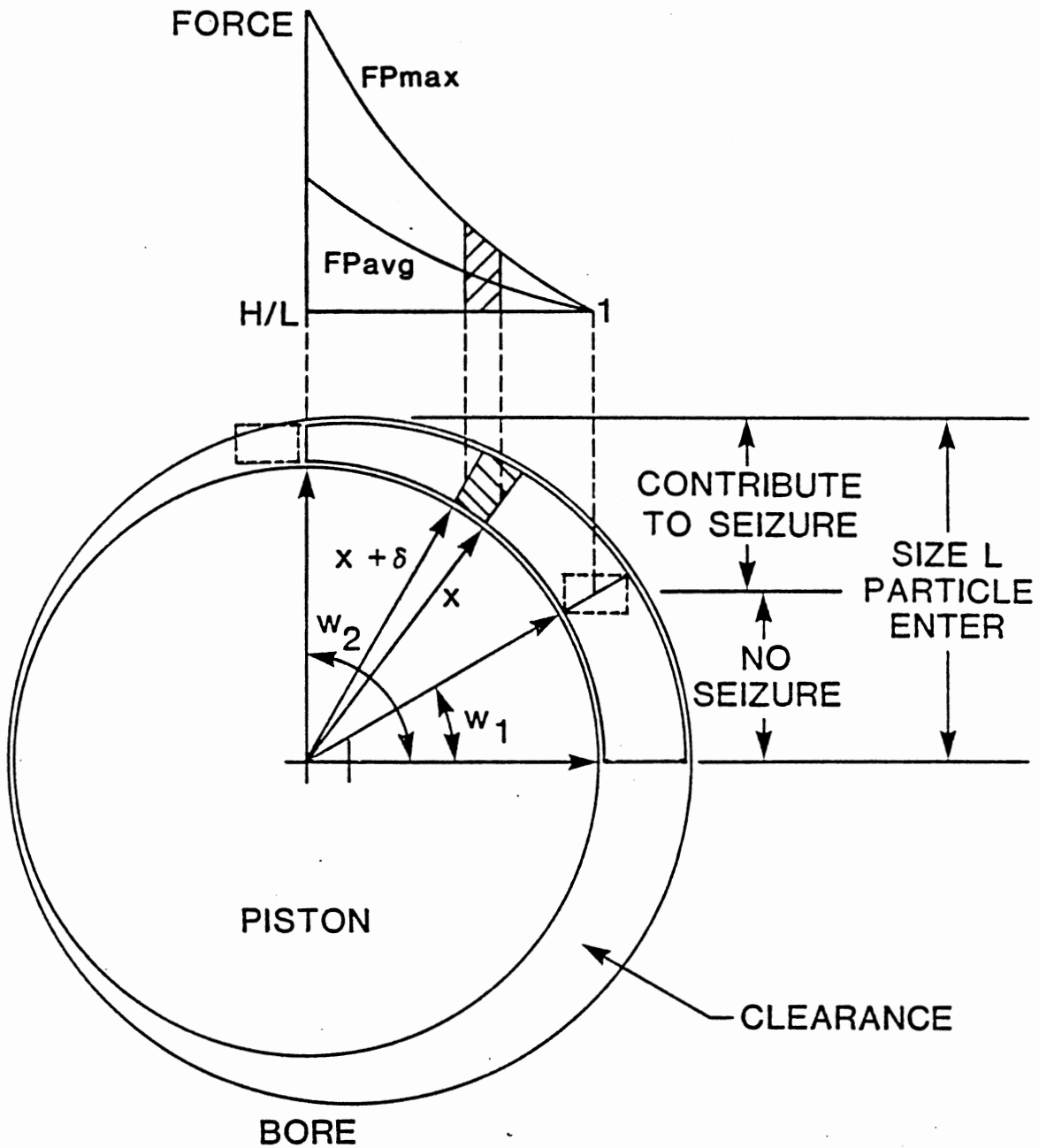


Figure. 15. Contribution of Silt Particles to Particulate-Induced Seizure.

If the total number of size L particles silted in the clearance is $MD(L)$ (see Fig. 10), then particles among $MD(L)$ could resist the spool movement and contribute to the seizure, calculated by:

$$MS(L) = MD(L) \frac{\text{Area}(w_2, w_1)}{\text{Area}(w_2, 0)} \quad (35)$$

Furthermore, the maximum induced force varies depending upon the position of w_x as Fig. 15 shows. The total maximum particulate-induced force due to the silted size L particles is:

$$FI(L) = MS(L) \sum_{x=1}^2 \left\{ \frac{\text{Area}(w_{x+\delta}, w_x)}{\text{Area}(w_2, w_1)} f(h(w_{x+.5\delta})/L) \right\} \quad (36)$$

The maximum total induced force covering the entire size range of silted particles is:

$$FMAX = \sum_{L=1}^{LM} FI(L) \quad (37)$$

where

$$LM = L \sin(\text{atn}(1/k))$$

When the function $g()$ replaces the function $f()$ in Eq. 36 (see Eq. 30 & 31), the result is the average total induced force:

$$FAVG = \sum_{L=1}^{LM} FI(L) \quad (38)$$

Particulate-Induced Seizure Model's Validity Investigation by Computer Simulation

The simulation program (Appendix A) was developed in two parts. The first part simulates the process of particles silting in the clearance of the piston-bore assembly, and the second part simulates the particulate-induced seizure force. Table I shows a typical input for both parts.

The silt process program simulation contains the algorithm presented in Fig. 11 and gives four graphic outputs: clearance vs. time, leakage flow vs. time, silt volume vs. time, and number of particles (frequency) vs. size. Figures 16 through 19 show the example outputs based upon the inputs illustrated in Table I. The clearance and leakage flow reduction agree with the previous investigators' observations and experimental data [1, 2, 5, & 9]. Figure 18 demonstrates that the accumulation of silt per unit leakage flow volume increases as time increases. This indicates that the piston-bore assembly gradually becomes efficient in capturing particles flowing through the clearance of the assembly. Figure 19 is the result of Eq. 10. Notice that although the internal nominal clearance is 25 micrometers, large numbers of particles less than 25 micrometers in size have silted in the clearance. The above result can be attributed to the silt Beta and NTd assumption, and these assumptions have been verified by experiments to be described shortly.

The particulate-induced seizure simulation program has two output values: FMAX and FAVG. One of the four selected parameters (time, gravimetric level, axial pressure, and silt Beta) was varied while the

TABLE I
INPUT PARAMETERS

1 ---	H0 : initial clearance micrometer	25
2 ---	D : inner dia. of the bore inches	.2501969
3 ---	PU : Upstream pressure lbf/in ²	190
4 ---	PD : Down stream pressre lbf/in ²	10
5 ---	L : Silt land length in inches	.25
6 ---	SYP: Yield strength of particle lbf/in ²	58000
7 ---	SYB: Yield Strength of Bore lbf/in ²	10000
8 ---	SYS: Yield Strength of Spool lbf/in ²	30000
9 ---	S : shape factor	1
10---	G : Concentration mg/L	50
11---	BETA : Retention characteristic (Nu/Nd)	2
12---	ECC: (0<= ECC <=1) Eccentricity	1
13---	DT : Time step in sec.	6
14---	TSET : Total length of time. (sec)	60
15---	GLN : Total number of grooves	0
16---	GL : The average length of grooves (in.)	.01

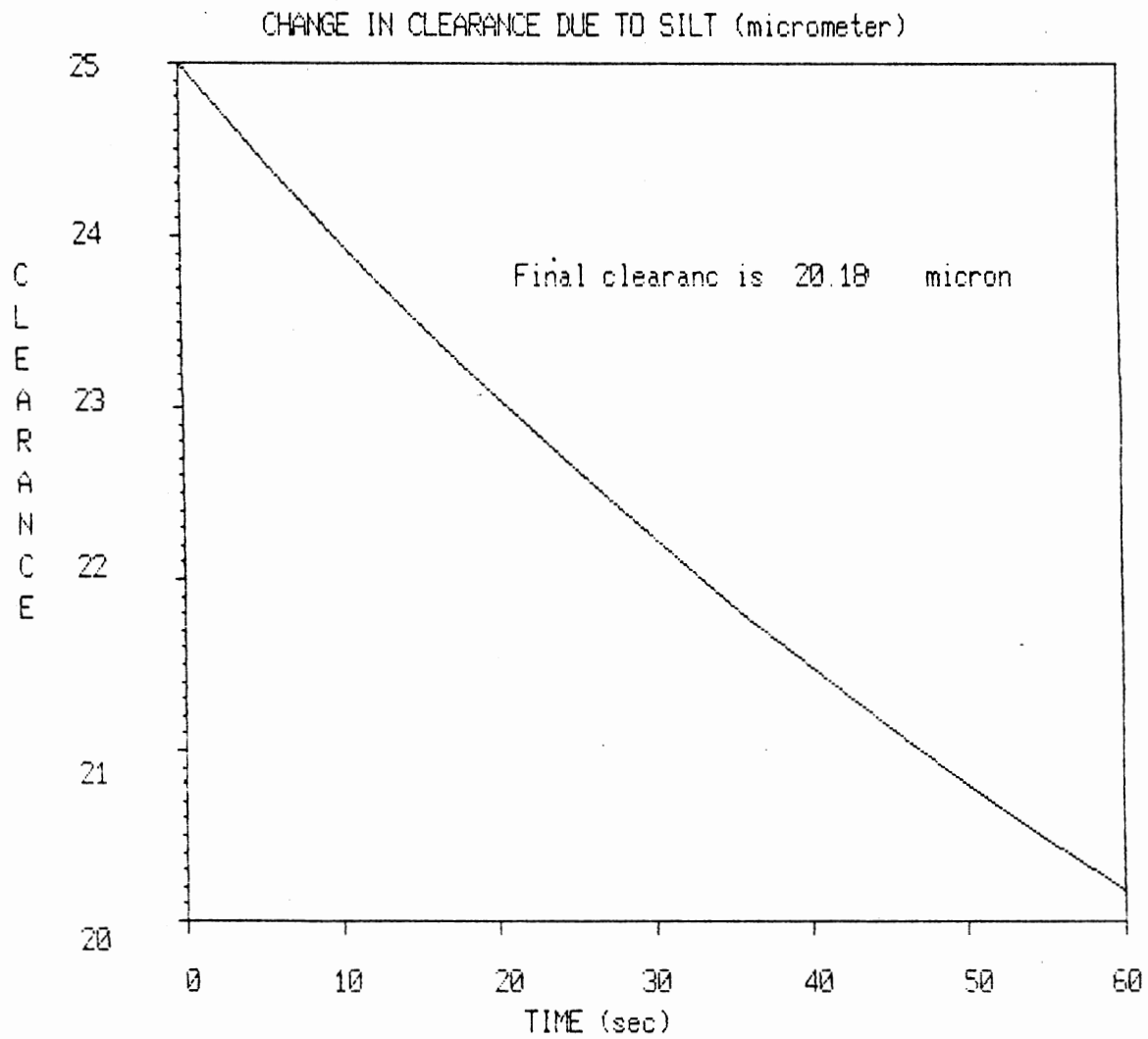


Figure. 16. Change in Clearance Due to Silt.

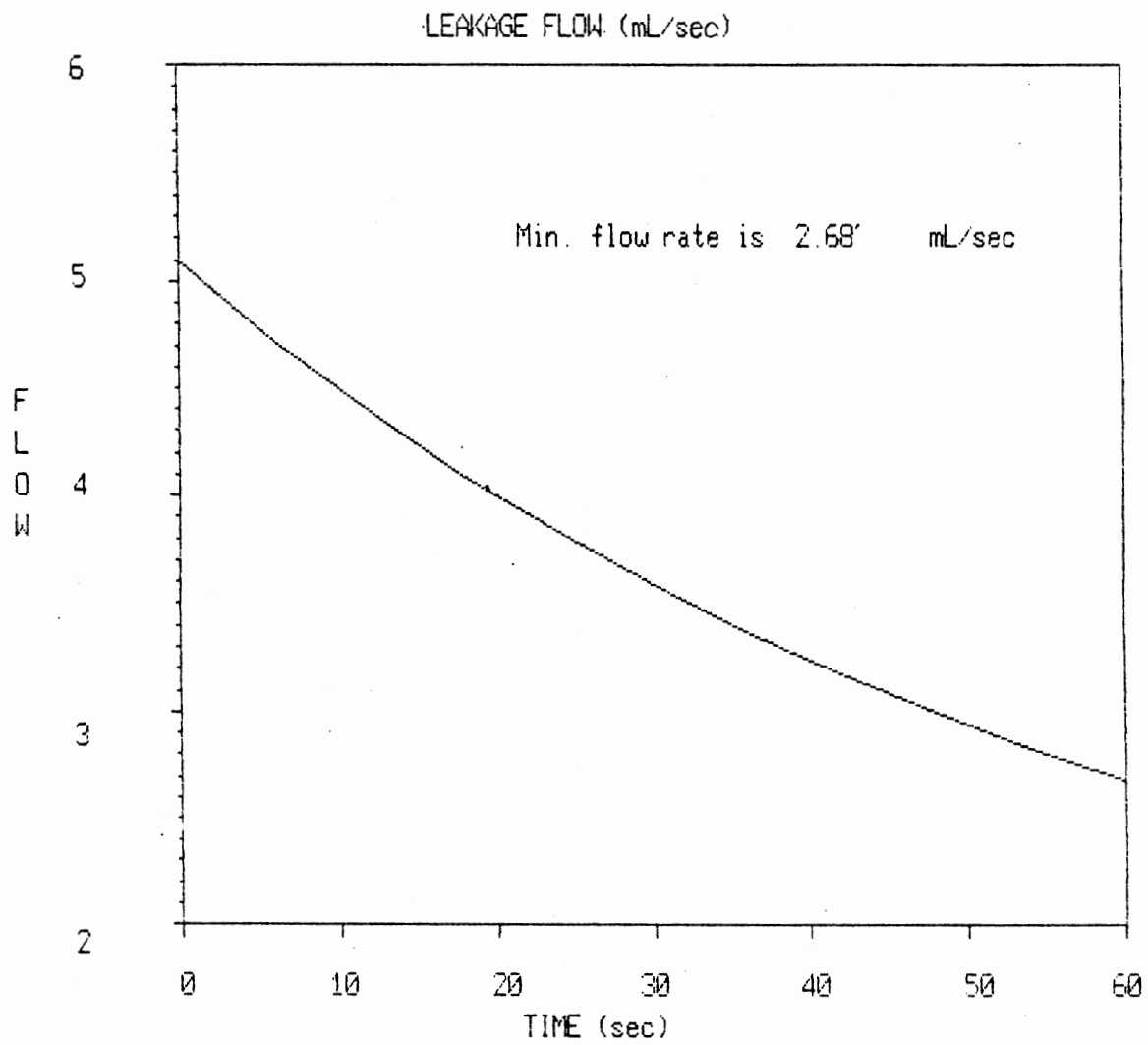


Figure. 17. Leakage Flow.

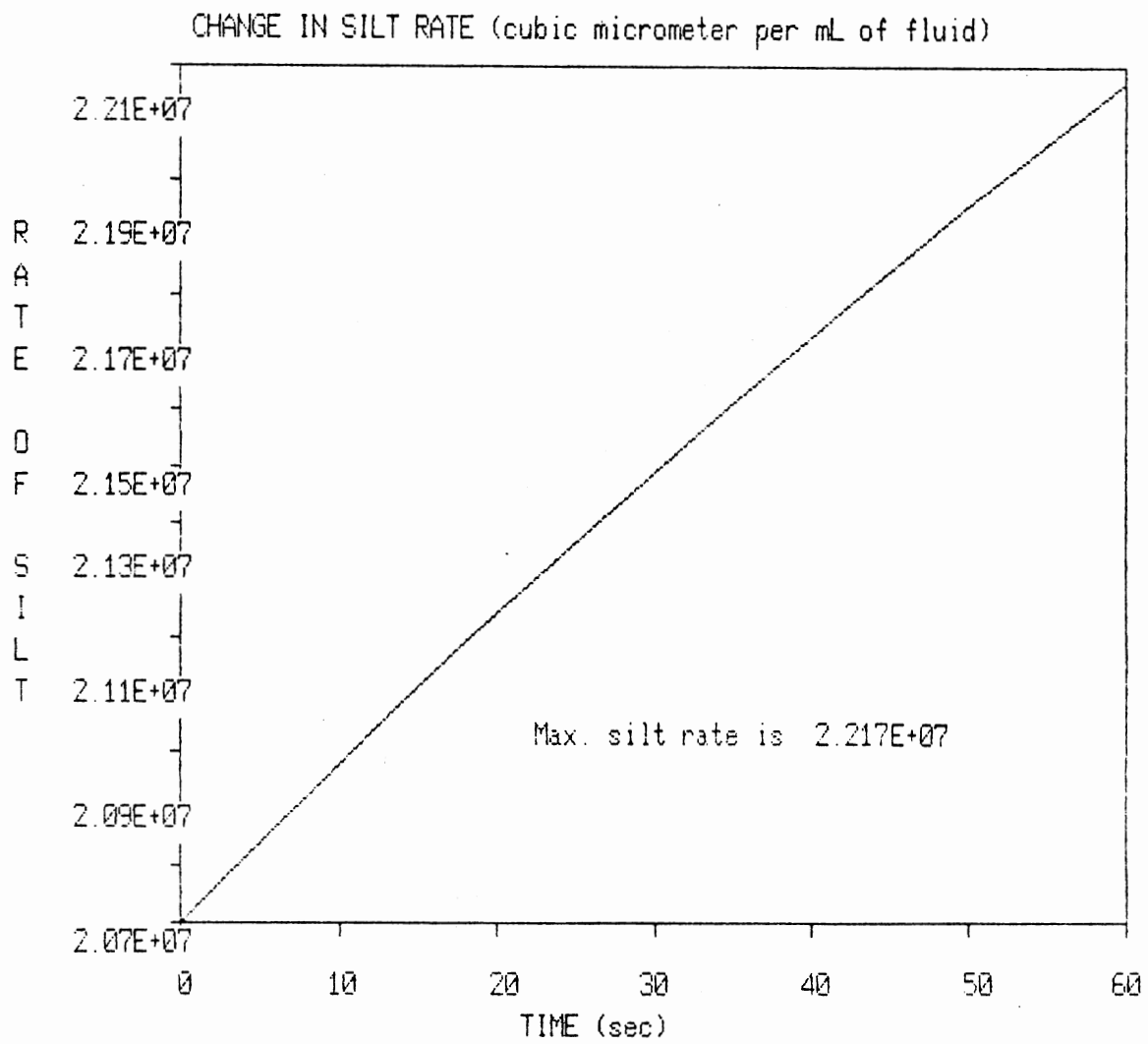


Figure. 18. Change in Silt Rate.

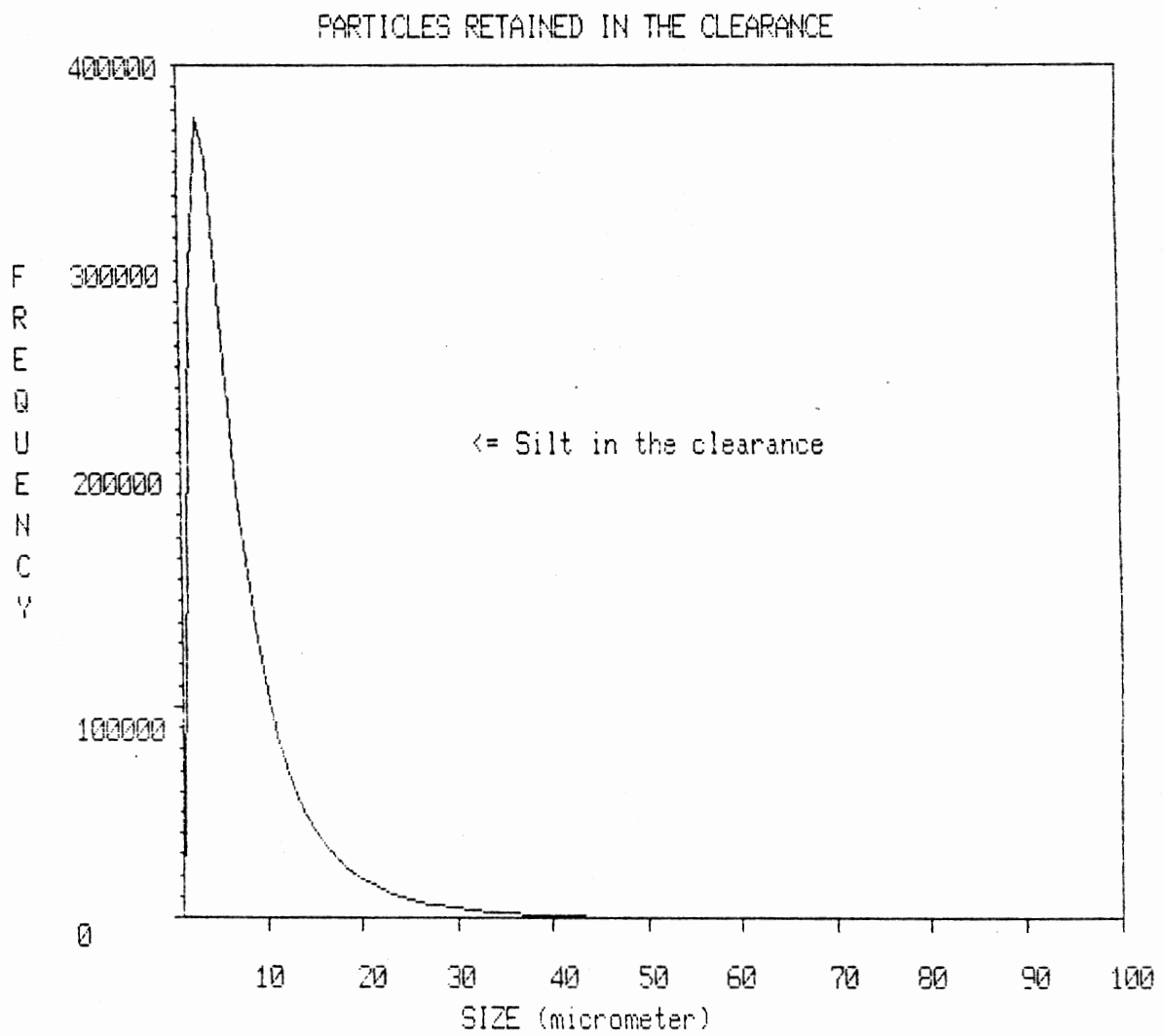


Figure. 19. Particle Retained in the Clearance.

others were held constant to investigate the parametric effect on the seizure force. Figures 20 through 23 exhibit the result. Figures 20 through 22 agree with previous experimental results [1, 3, 4, 7, 8, 11, 12, and 13]. The seizure force FAVG increases as a parameter increases, yet the increasing trend is concave downward indicating the possible terminal saturation level, which has also been observed by previous investigators. Figure 23 of the seizure force vs. silt Beta clearly displays the existence of the saturation level and demonstrates a steep increase in the seizure force at a silt Beta value between 1 and 10. These results show that the simulation programs adequately describe observed key characteristics of the dynamics of seizure observed in the previous experiments by other workers.

Dither Model

Among the parameters shown in Table I, silt Beta β_s is the only parameter that dither can affect. As Figure 23 shows, when the silt Beta value decreases, FAVG decreases accordingly (so does FMAX); therefore, when the dither is applied to the piston-bore assembly, silt Beta must decrease. Kamiyo's experimental results (Fig. 8) support this postulate, as his results clearly show the decrease in dirt damming and piling in the piston-bore clearance when dither is applied to the piston. Hence, the results of dither should appear as a change in the downstream particle size distribution NDd and may be measured by monitoring NDd. In order to estimate NDd, according to Eq. 4 & 5, both silt Beta value and

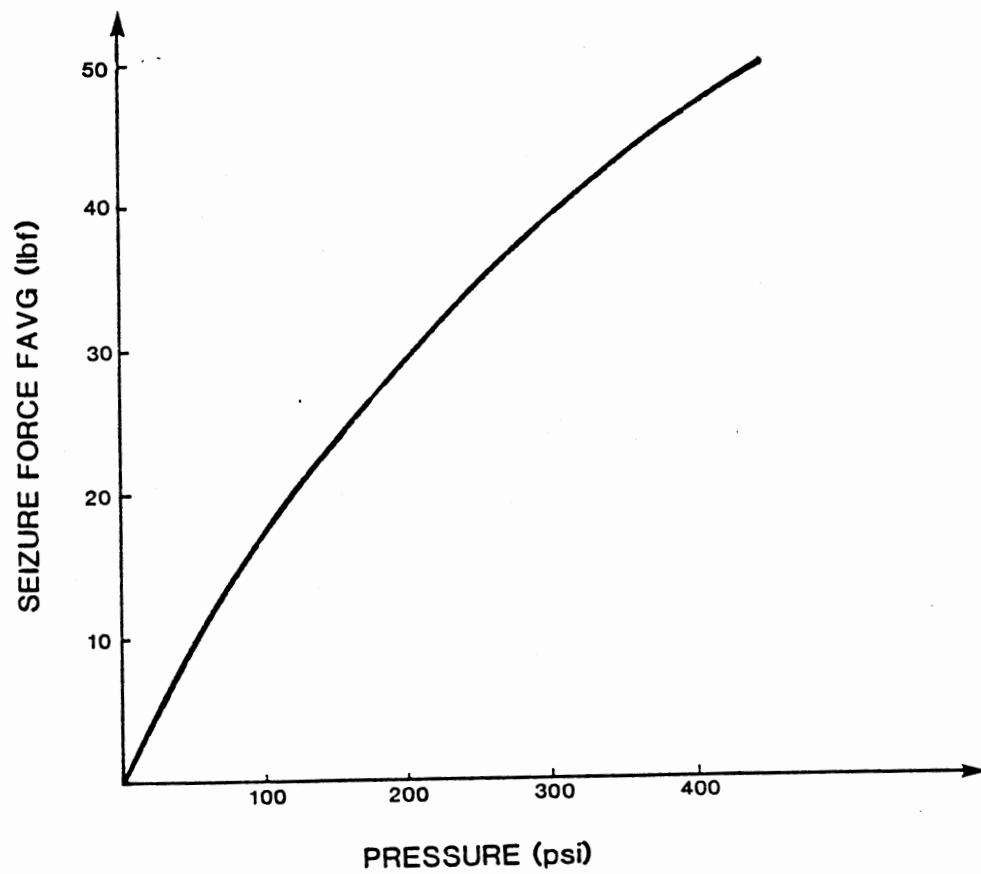


Figure. 20. Seizure Force Versus Pressure.

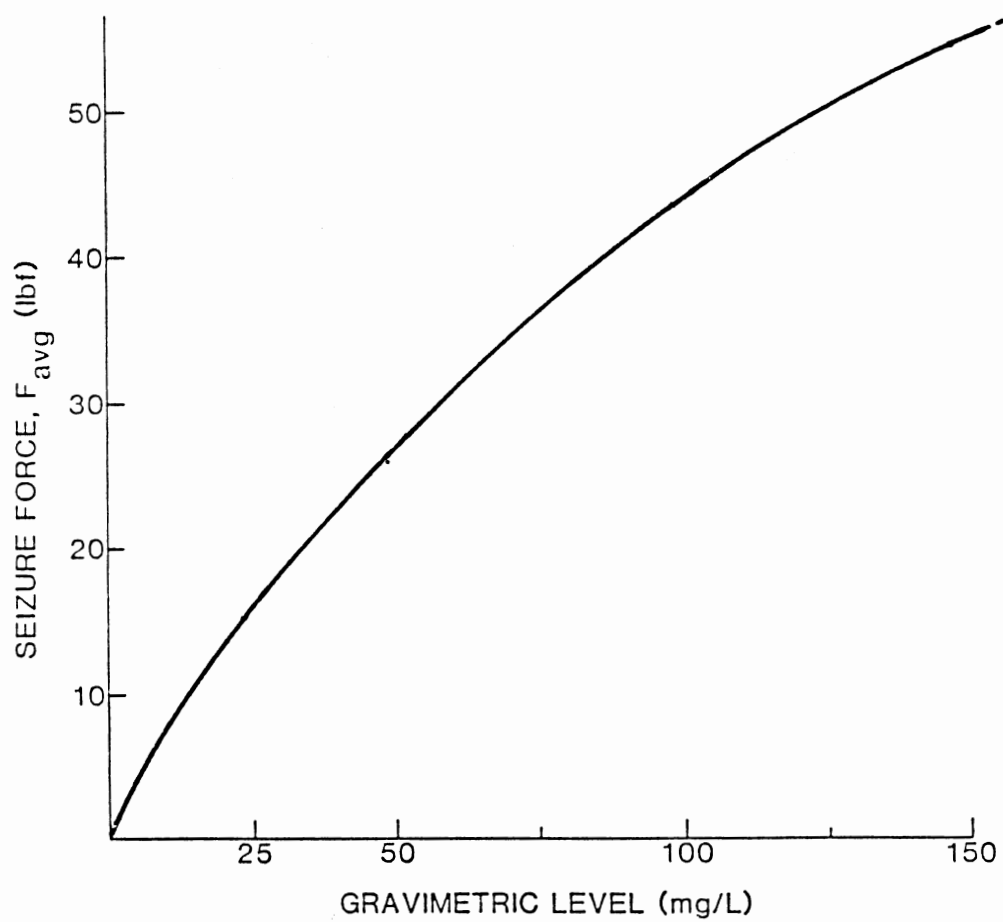


Figure. 21. Seizure Force Versus Gravimetric Level.

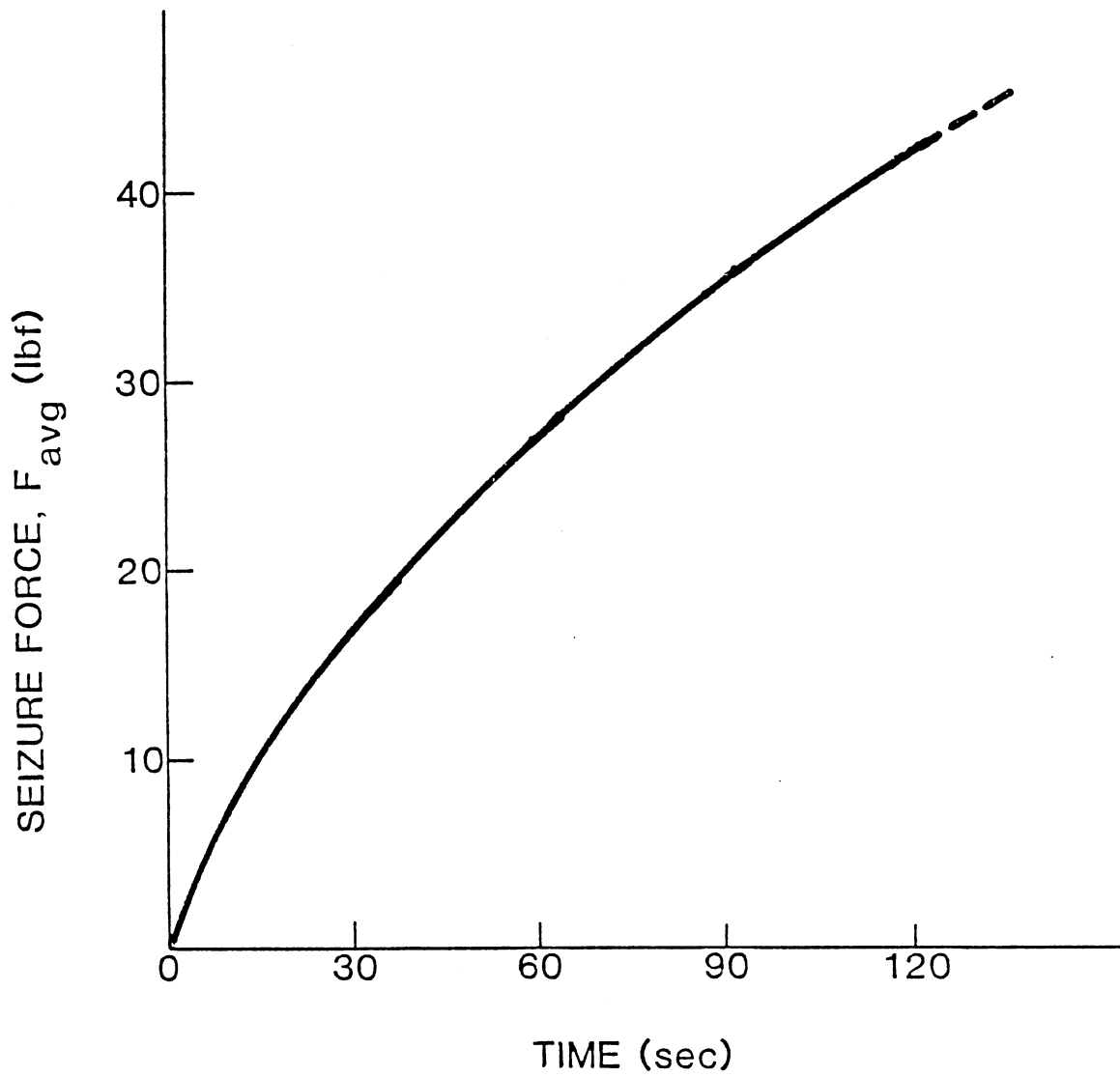


Figure. 22. Seizure Force Versus Time.

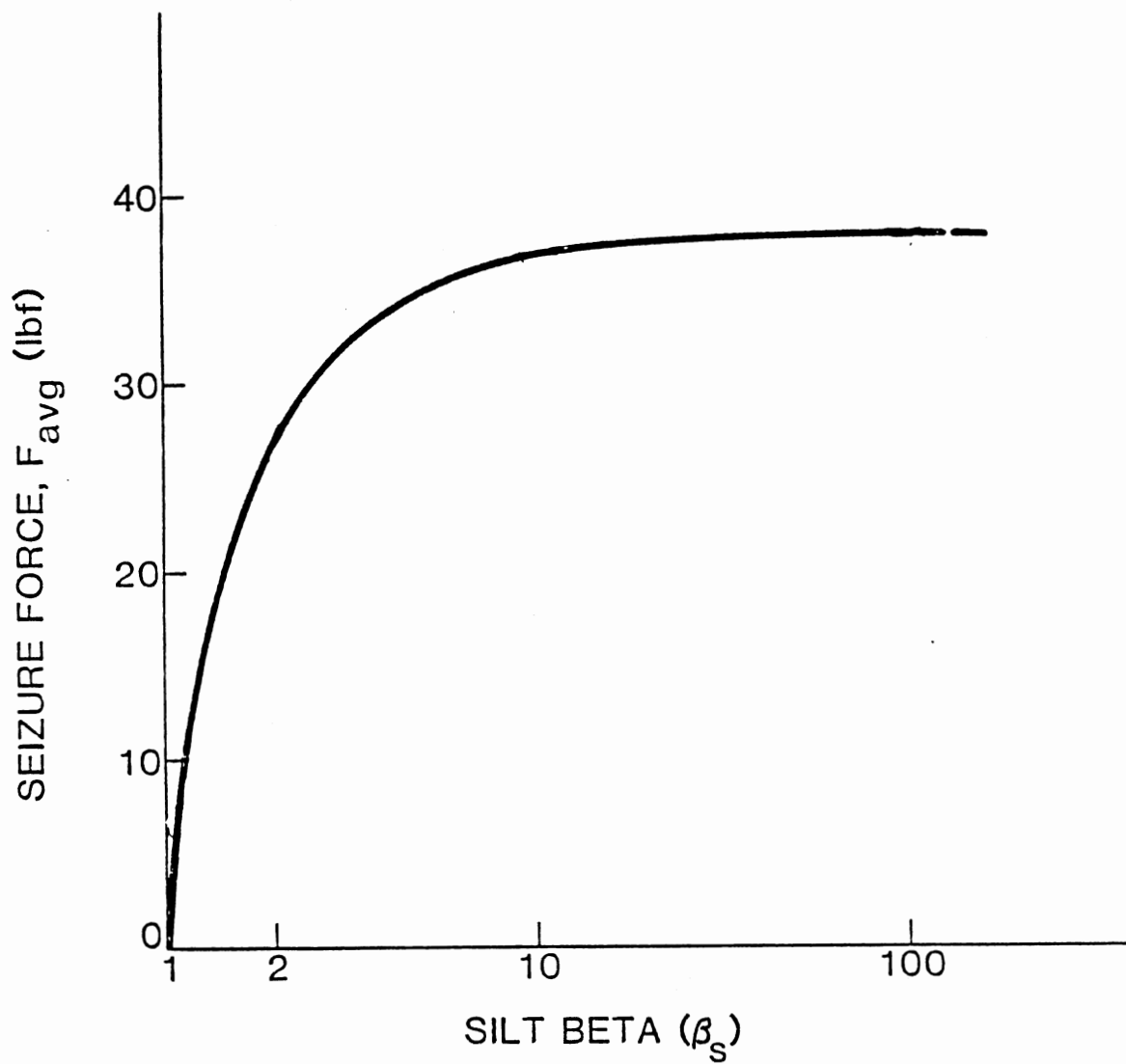


Figure. 23. Seizure Force Versus Silt Beta.

NTd must be measured.

It should be noted that in the presence of dither, various parameters and associated symbols are altered: note that the dither changes NDd to NPDd and its coefficients to β_p and NPTd. The relationship between β and β_p is assumed to be similar to Nikitin's experimental results (Fig.9). The force required to break the seizure decreases as a function of frequency--in a manner similar to exponential decay. Thus, the logarithm of silt Beta ratio also decreases:

$$\frac{\ln(\beta_p)}{\ln(\beta)} = A e^{-Cw} \quad (39)$$

where A and C are constants for the exponential decay function, and w is the frequency of the controlled pulsation.

Solving for β_p gives:

$$\beta_p = \beta A e^{-Cw} \quad (40)$$

For a given value of β_p , the range of NPTd can be determined as follows. From the definition of silt Beta,

$$\beta_p = \frac{NTu e^{(-Bu \ln^2(h))}}{NPTd e^{(-Bd \ln^2(h))}} \quad (41)$$

where h is the nominal clearance at the instance when the silt Beta value

is obtained. Solving for B_d gives:

$$B_d = B_u + \frac{\ln(\beta_p) Ga}{\ln^2(h)} \quad (42)$$

where

$$Ga = NPT_d / NT_u \quad (43)$$

$$0 < Ga < 1 \quad (44)$$

From now on, the NPT_d range is specified by the range of Ga because NT_u is a constant. The range exhibited by Eq. 44 is further narrowed by the non-desorption constraints. When the following inequality is satisfied, fine particle size designated by F (smaller than h) does not desorb from the piston-bore clearance:

$$\frac{2 NT_u B_u \ln(F)}{F} e^{(-B_u \ln^2 F)} > \frac{2 NPT_d B_d \ln(F)}{F} e^{(-B_d \ln^2 F)} \quad (45)$$

Eliminating and organizing terms, the inequality becomes:

$$\ln(B_u / (Ga B_d)) > (B_u - B_d) \ln^2 F \quad (46)$$

However, Eq. 42 is the same as:

$$B_u - B_d = -n \ln(\beta_p Ga) \quad (47)$$

where

$$n = 1 / \ln^2(h) \quad (48)$$

Replacing $B_u - B_d$ in Eq. 46 with Eq. 47, the inequality becomes:

$$B_d < \frac{B_u}{G_a (\beta_p G_a)^{-n} \ln^2 F} \quad (49)$$

The result of dividing both sides of Eq. 49 with B_u and organizing it is:

$$\frac{B_d}{B_u} < \frac{(\beta_p G_a)^n \ln^2 F}{G_a} \quad (50)$$

When the desorption constraint $B_d/B_u > 1$ is satisfied, retained particles with sizes greater than h do not desorb from the piston-bore assembly. As a result, $B_d/B_u > 1$ and the insertion of Eq. 48 into Eq. 42 yields:

$$\frac{B_d}{B_u} = 1 + \frac{n \ln(\beta_p G_a)}{B_u} > 1 \quad (51)$$

Solving Eq. 51 for G_a results in:

$$G_a > 1 / \beta_p \quad (52)$$

Figure 24 illustrates the range of G_a ($= NPT_d/NT_d$) as a function of B_d/B_u , where desorption constraints limit the range of G_a . Therefore, by the experimental determination of silt Beta (see Eq. 39), the range of non-desorption NPT_d can be determined. If the particle counter analysis reveals that the actual NPT_d is outside of the non-desorption range, then the size range of the desorption can be identified.

$N_{Td} = 1751.83$
 $B_u = 4.7138 \times 10^{-1}$
 $h = 25$ micrometres
 $F = 2$ micrometres

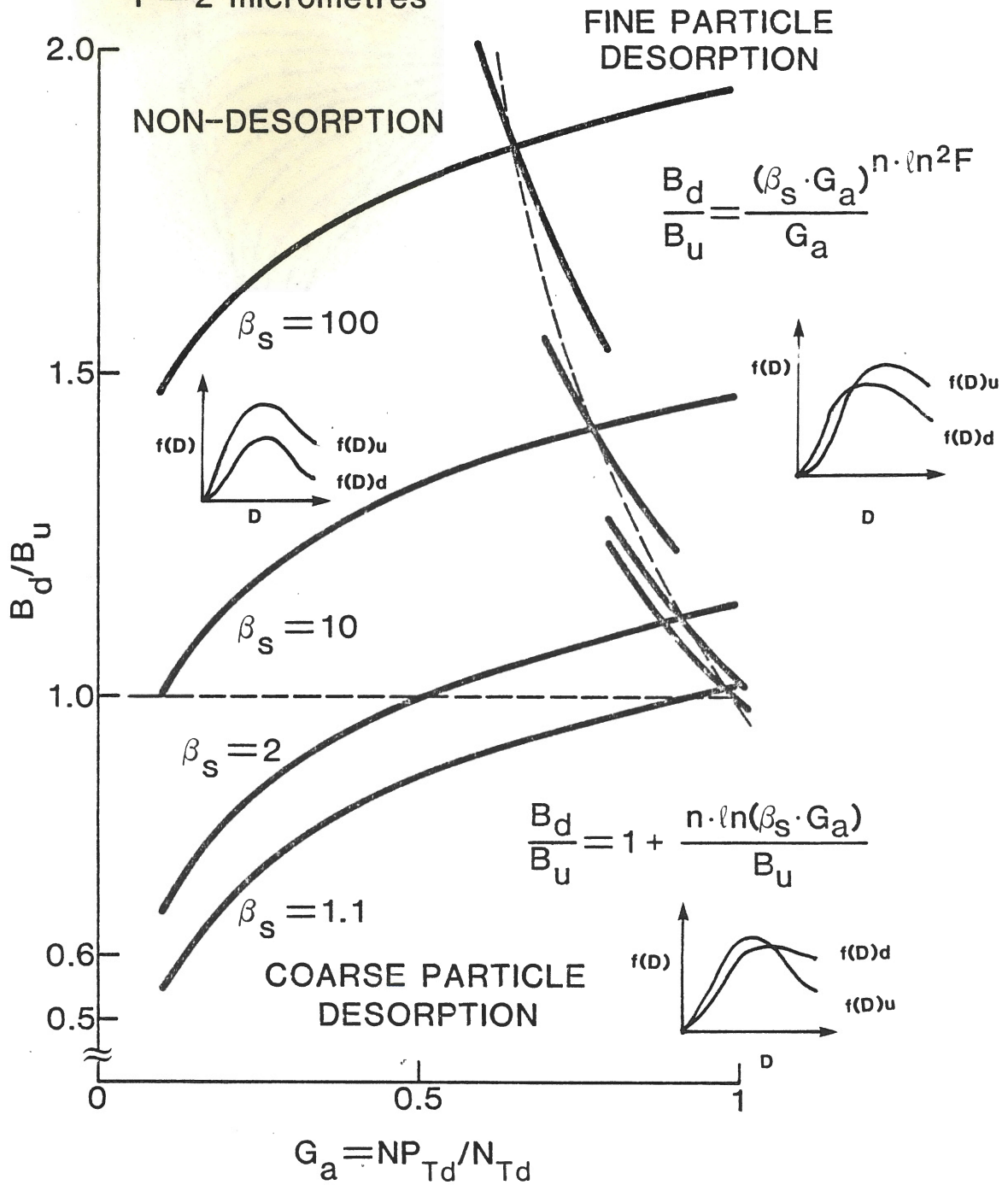


Figure. 24. Desorption.

CHAPTER IV

VERIFICATION OF SILT PROCESS MODEL

Experimental Scheme

As a result of the simulation studies, several experimental objectives ensue. The first is to investigate whether the leakage through a piston-bore assembly follows the theory that is presented in the previous chapter, and the second is to develop from the experimental data an equation describing the silt Beta as a function of particle size.

The leakage equation (Eq. 2) shows that the eccentricity of a piston in the bore greatly influences the leakage. This was confirmed by many researchers in the past. Kamijo and Dransfield [5, 8], in particular, experimentally proved that when the pressure difference across the clearance of a piston-bore assembly is below 1000 psi, then the eccentricity is always close to one.

Besides the eccentricity, the absolute viscosity also affects the outcome of the leakage flow. Since Dexron II contains additives, the effect of this additive over the absolute viscosity is investigated by varying the shear rate of the leakage through the clearance of a piston-bore assembly.

Since no information on the silt Beta values of a given piston-bore

assembly is available, first the method to identify a silt Beta value at each particle size is developed, and then, using this method, the silt Beta values versus the particle size of a given piston-bore assembly is determined. The variation of silt Beta values is investigated for three different clearances with two different piston land lengths (a total of six different cases). These silt Beta values obtained through the experiments are then implemented in the computer simulation program for analyzing the validity of the silt process model.

Development of Experimental Facility

The generic test housing (Fig. 25) and piston and bore test pieces were fabricated. A combination of a piston and bore was installed inside the housing, as shown in Fig. 25. The actuation rod controlled the position of the piston with respect to the bore. When the actuation rod inserted the piston inside the bore, as shown in Fig. 25, the nominal clearance between the piston and bore was established by their diameter difference. A complete set of piston and bores with their dimensions is listed in Table II.

Table II has two measurements. The above measurement was performed optically by STADCO Automatic Co. in Fairborn, Ohio. The lower tabulated value was obtained by the precision measurement device (minimum resolution of 0.254 micrometer) manufactured by Pratt & Whitney.

Pistons No.1 through 9 and bore No. 1 were made out of soft cold rolled steel 12L/4. Pistons No. 10 through 18 and bore No. 2 were made

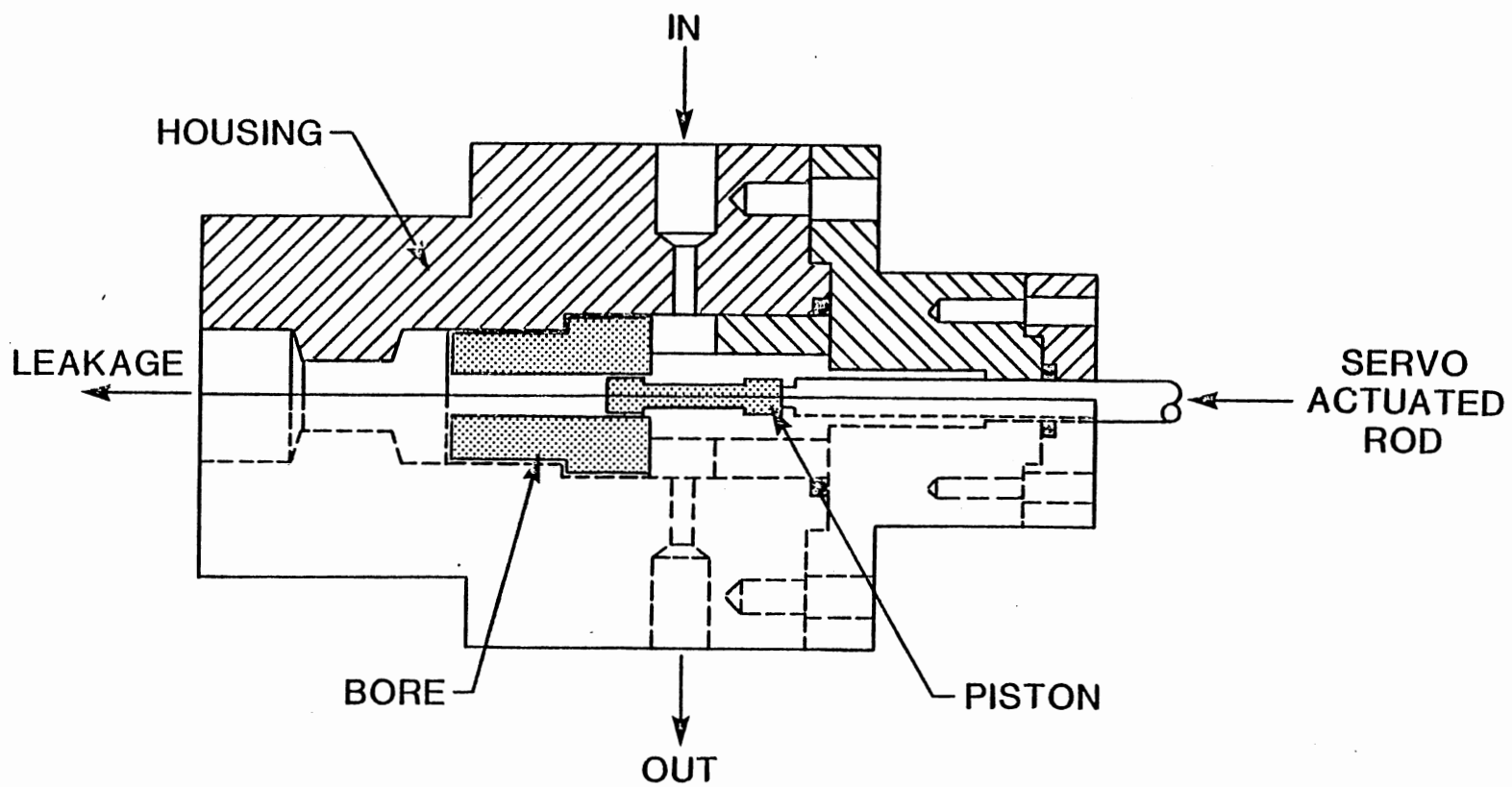
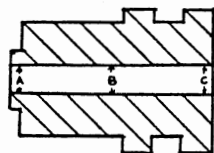


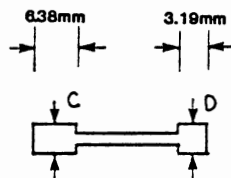
Figure. 25. Piston-Bore Assemblies and Housing.

TABLE II
PISTON-BORE DIMENSION



BORE DIMENSION (mm)

No. Hardness Brinell	A	B	C
1 Hb=120	6.350	6.350	6.350
2 Hb=400	6.351	6.351	6.351
3 Hb=725	6.351	6.351	6.351



PISTON DIMENSION (mm)

No. Hardness Brinell	C	D	No. Hardness Brinell	C	D	No. Hardness Brinell	C	D
1 Hb=120	6.341 6.3375	6.341 6.3381	11 Hb=400	6.339 6.3373	6.341 6.3373	21 Hb=725	6.341 6.3383	6.341 6.3398
2 Hb=120	6.341 6.3406	6.341 6.3428	12 Hb=400	6.339 6.3381	6.339 6.3385	22 Hb=725	6.332 6.3284	6.332 6.3309
3 Hb=120	6.341 6.3373	6.341 6.3423	13 Hb=400	6.330 6.3298	6.330 6.3298	23 Hb=725	6.332 6.3322	6.332 6.3322
4 Hb=120	6.329 6.3296	6.329 6.3296	14 Hb=400	6.330 6.3296	6.330 6.3309	24 Hb=725	6.332 6.3322	6.330 6.3322
5 Hb=120	6.332 6.3322	6.330 6.3309	15 Hb=400	6.329 6.3303	6.330 6.3296	25 Hb=725	6.322 6.3220	6.322 6.3220
6 Hb=120	6.332 6.3296	6.330 6.3322	16 Hb=400	6.320 6.3220	6.320 6.3220	26 Hb=725	6.320 6.3220	6.322 6.3220
7 Hb=120	6.320 6.3220	6.320 6.3220	17 Hb=400	6.319 6.3195	6.319 6.3195	27 Hb=725	----- 6.3474	----- -----
8 Hb=120	6.322 6.3220	6.322 6.3220	18 Hb=400	6.322 6.3220	6.322 6.3220	28 Hb=725	----- 6.3474	----- -----
9 Hb=120	6.322 6.3220	6.320 6.3220	19 Hb=725	6.339 6.3398	6.341 6.3398	29 Hb=725	----- 6.3449	----- -----
10 Hb=400	6.339 6.3398	6.341 6.3373	20 Hb=725	6.341 6.3398	6.341 6.3398	21 Hb=725	----- 6.3449	----- -----

of cold rolled steel 1018, carburized, and have a hardness of 43 to 45 on the Rockwell C scale. Pistons No. 19 through 26 and bore No. 3 were made of A-2 and hardened to achieve a 62 to 64 hardness on the Rockwell C scale.

The test hydraulic circuitry, shown in Fig. 26, was developed and confirmed to control the following parameters:

1. temperature
2. pressure
3. cleanliness through high Beta value filter
4. concentration of the injected particles for the entire test period

The accumulator was oriented vertically to avoid providing any space where the injected particles might settle.

Leakage Flow Test

The leakage flow of a piston-bore assembly under clean fluid is well defined, and many researchers [6, 8] have experimentally proved the integrity of Eq. 2. Dransfield [5] verified the validity of Eq. 2 with Shell Tellus 27 (known as a non-additive industrial mineral hydraulic oil), and Kamijo et al. [8] verified its validity with turbine oil #140. Since Equation 2 was derived from the Poiseuille flow equation, the equation is thus valid for laminar flow and for cases where the constant viscosity and density assumption is applicable.

For this study, Dexron II was chosen as a test fluid because of its

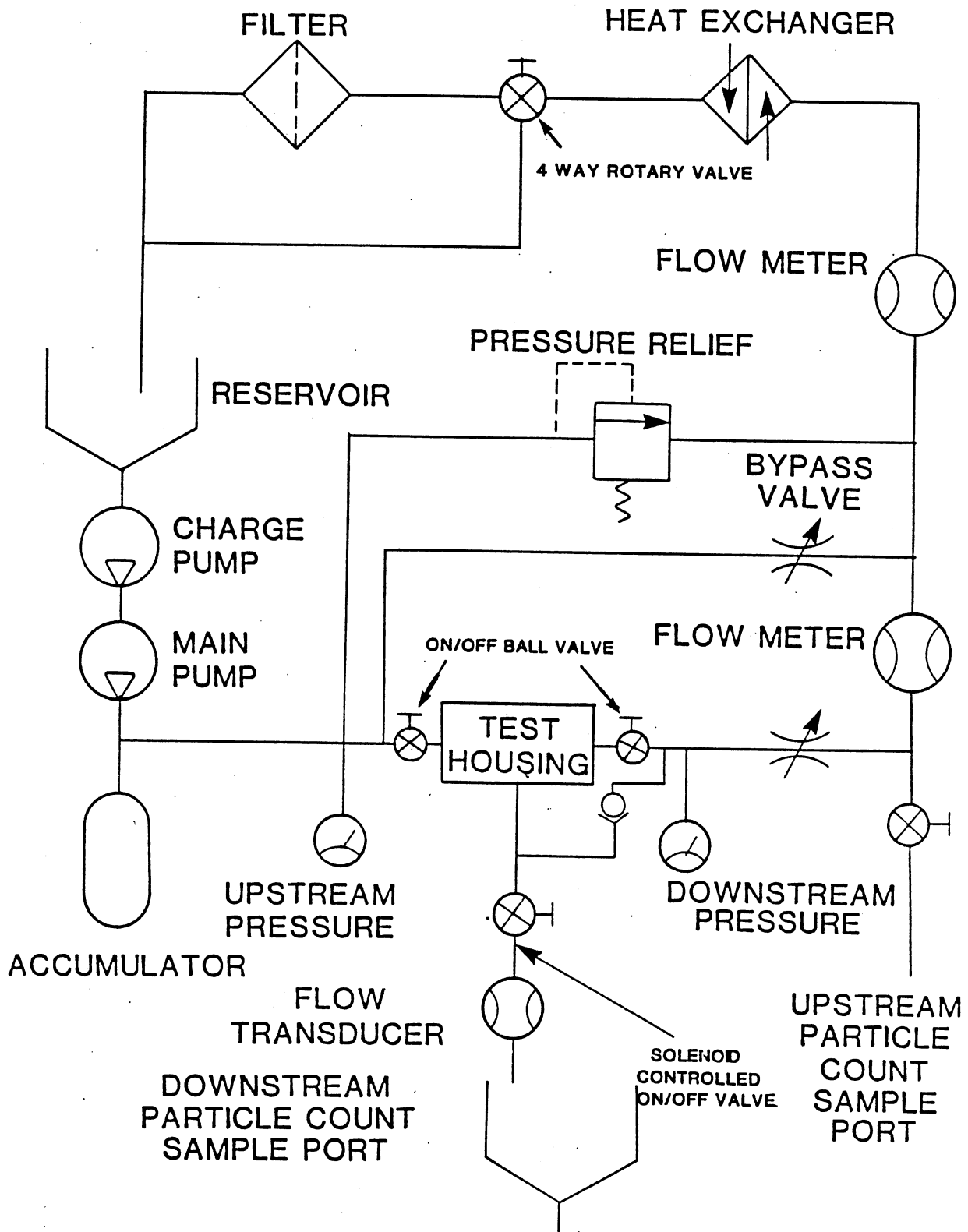


Figure. 26. Hydraulic Circuitry.

wide industrial use; however, it had to be experimentally tested as to whether it follows Eq. 2.

The test housing was installed and connected to the test hydraulic circuitry as shown in Fig. 26. The piston was inserted into the bore as Fig. 25 shows, and pressure was applied such that there was 1000 psi difference between the upstream and downstream of the leakage flow through the piston-bore clearance.

The combinations of the piston-bore assemblies are displayed in Table III. Bore No. 3 and pistons No. 19, 23, and 26 were made out of the same material and have the same hardness; therefore, the temperature effect over the nominal clearance of a given combination of a piston-bore assembly was minimized. Moreover, each piston had the land length of 3.19mm and 6.38mm; thus, the effect of land length over the leakage flow could be investigated. The leakage flow test results of Table III were plotted against the theoretical leakage flow derived from Eq. 2. The values used for the theoretical calculations are

viscosity :	$\mu = 2.32\text{E-}06 \text{ lbf/in}^2$
clearance :	$h = 5, 10 \text{ and } 15 \mu\text{m}$
land length :	$L = 3.19 \text{ and } 6.38 \text{ mm.}$
upstream pressure :	$P_u = 1000 \text{ lbf/in}^2$
downstream pressure :	$P_d = 0 \text{ lbf/in}^2$ (atmospheric pressure)
spool diameter :	$D = 6.320, 6.330 \text{ and } 6.340 \text{ mm.}$
eccentricity :	$e = 0 \text{ and } 1.$

Figures 27 and 28 show that all the experimental results stay within both

TABLE III
LEAKAGE FLOW TEST (DEXRON II CLEAN FLUID)

BORE No.	SPOOL No.	NOMINAL CLEARANCE μm	LAND LENGTH e; eccentricity	
			6.38 mm	3.19 mm
3	19	5	2.73 mL/min $e=1.222(h=5)$ $e=0.764(h=6)$	6.96 mL/min $e=1.184(h=5)$ $e=.963(h=6)$
3	23	10	10.0 mL/min $e=0.568(h=5)$	21.6 mL/min $e=0.634(h=5)$
3	26	15	40.0 mL/min $e=0.711(h=5)$	97.0 mL/min $e=0.868(h=5)$

h = actual clearance size in micrometer.

extremes of eccentricity, except for the results for a nominal clearance of 5 micrometers. A close examination of Table II shows that the bore No. 3 and piston No. 19 combination has a clearance of 6 micrometers, according to the measurement done by the Pratt & Whitney precision measurement device. If the clearance of 6 micrometers were used instead of 5 micrometers in Eq. 2, the estimated eccentricities would change as shown in Table III and would be less than unity.

Dransfield and Sasada's experimental data show that a given piston-bore assembly always presents eccentricities above 0.9 and close to 1 for Newtonian fluids. However, the eccentricity of the experimental data shown in Fig. 27 and 28 are not always above 0.9.

Since Dexron II is known to contain proprietary additives, it may have significant non-Newtonian characteristics. To examine the non-Newtonian characteristics of Dexron II, a copper capillary of 190 inches with 1.4mm inner diameter was used. One end of the capillary was left open to atmospheric pressure, and Dexron II pressured higher than atmospheric pressure was applied to the other end. When the higher pressure was fixed, the pressure drop per unit length became constant. The leakage through the capillary was collected in a graduated cylinder, and the time taken to collect the leakage was measured. The leakage flow rate was calculated by the leakage volume in the graduated cylinder divided by the time needed to collect the volume. The fully developed laminar equation (Eq. 53) was used to find the absolute viscosity:

$$\mu = \pi D^4 (P_u - P_d) / (128 Q L) \quad (53)$$

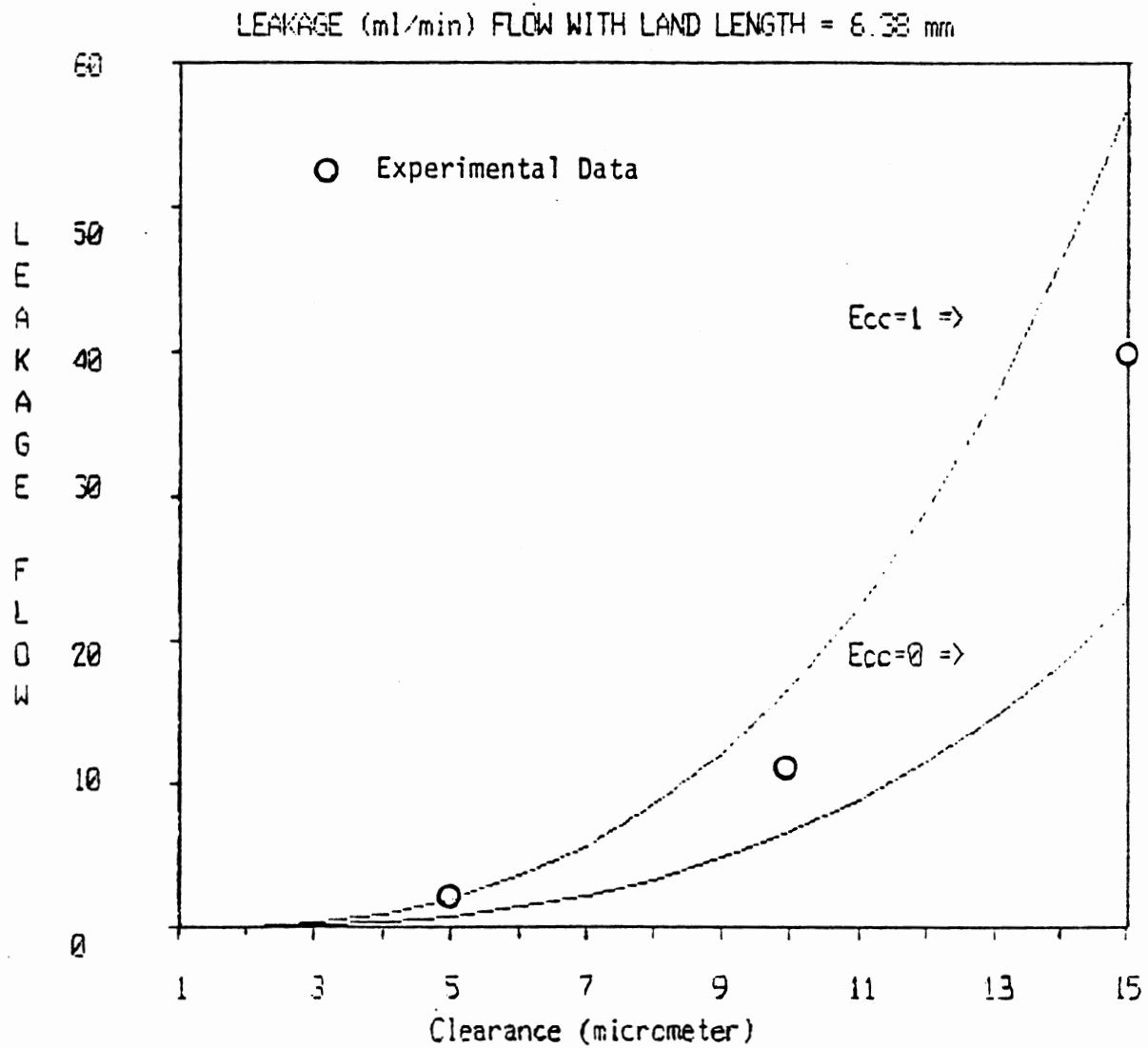


Figure. 27. Leakage Flow of a Piston-Bore Assembly With 6.38mm Land Length.

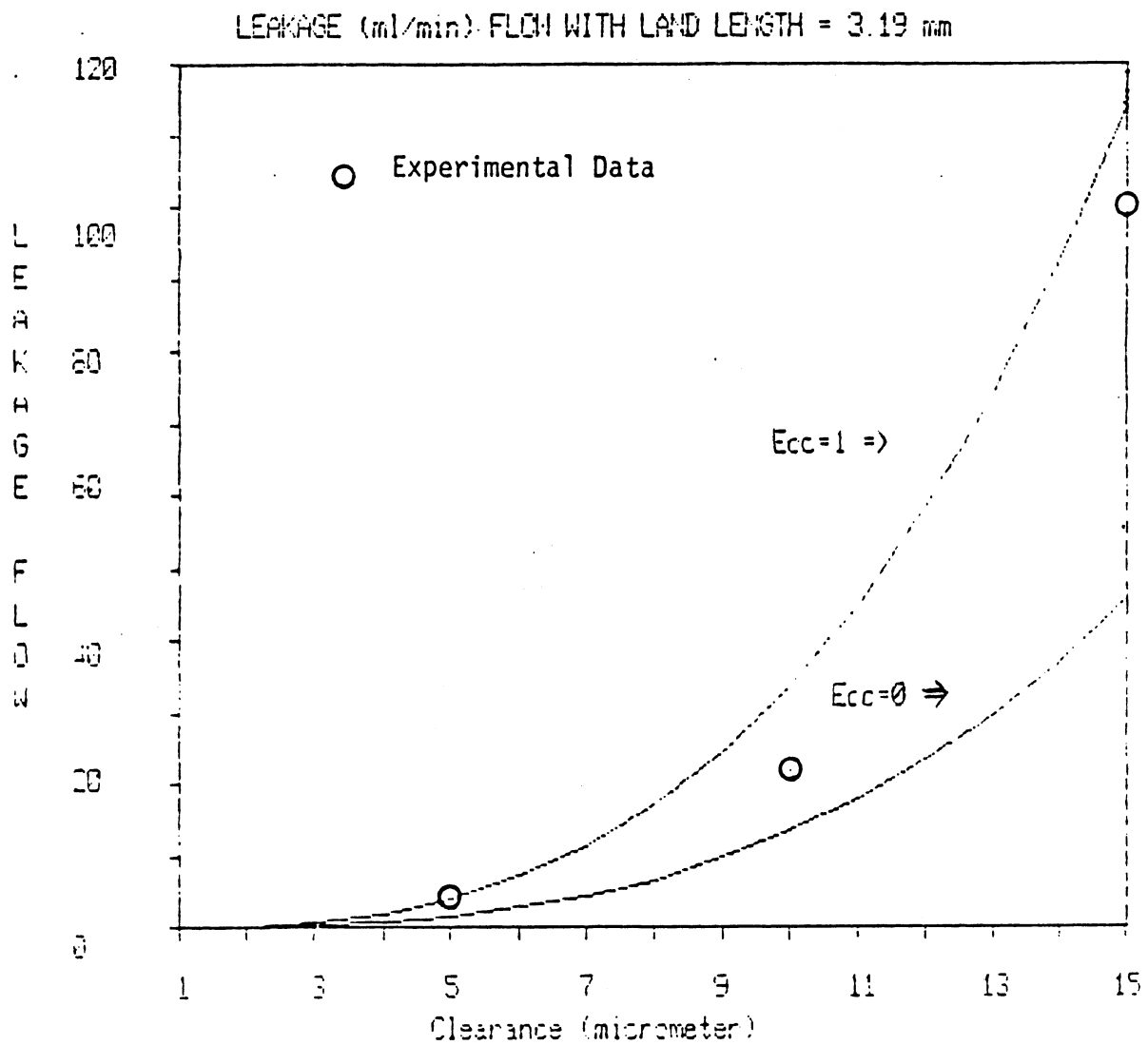


Figure. 28. Leakage Flow of a Piston-Bore Assembly With 3.19mm Land Length.

where

D = inner diameter of capillary

Q = leakage flow rate

P_u = higher pressure (end of capillary)

P_d = lower pressure (end of capillary)

L = length of capillary

In addition, the highest shear rate, which occurs at the wall of a capillary, was also calculated by:

$$\left. \frac{du}{dr} \right|_{r=R} = - \frac{4 \text{ VAVG}}{R} \quad (54)$$

where R is the inner radius of the capillary, and VAVG is calculated by dividing the leakage by the cross sectional area of the capillary.

Figure 29 shows the experimental result of absolute viscosity versus the shear rate at the capillary wall. This figure clearly demonstrates that the absolute viscosity increases as the shear rate increases. Yet, the increase is nonlinear. To correlate this capillary test data with the piston-bore assemblies' test, the shear rate of the leakage flow through the piston-bore assemblies must be known.

An accurate value of the shear rate of the leakage flow through the piston-bore assemblies can not readily be calculated; however, the shear rate was estimated by the following approach. If the piston is assumed to be concentric with the bore, then the average flow velocity could be calculated by:

$$\text{VAVG} = Q / (\pi h (D - h)) \quad (55)$$

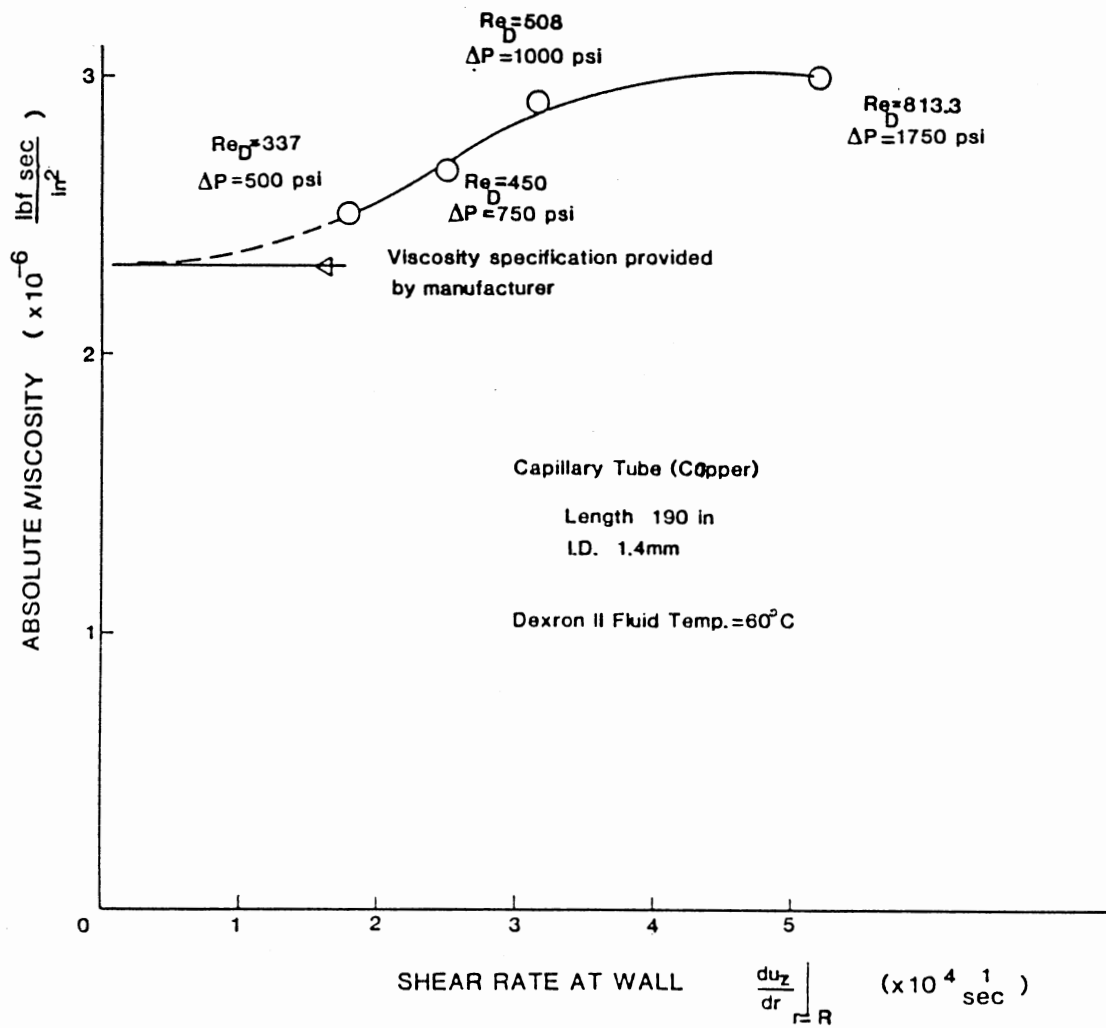


Figure. 29. Absolute Viscosity Versus Shear Rate at the Wall of the Capillary Tube.

where

Q = the leakage flow

h = the clearance size

D = the inner diameter of the bore

The shear rate was then estimated by using the fully developed laminar flow equation for flat plates and is:

$$\left. \frac{du}{dy} \right|_{y=h/2} = - \frac{6 V_{AVG}}{h} \quad (56)$$

where u , h and y are explained in Fig. 30. In reality, the piston is not normally concentric with the bore; therefore, if the actual leakage flow (leakage under eccentric condition with a higher flow rate than concentric condition) is used in Eq. 55 to find the estimated shear rate in Eq. 56, this shear rate becomes approximately the average shear rate of the eccentric condition.

Based upon the data in Table III, the average shear rate was calculated using Eq. 55 and 56 in Table IV. It is evident that the leakage through the clearance of a piston-bore assembly experiences a shear rate 9 to 50 times higher than the shear rate found in the capillary test. However, from the experimental data shown in Fig. 27 and 28, the absolute viscosity does not increase at the same rate as the shear rate. If the absolute viscosity were to increase in proportion to the shear rate, the leakage would have been 1/9 or 1/50 of what actually was measured. Furthermore, it is reasonable to postulate that the increased absolute viscosity due to the high shear rate results in a lower leakage flow in

For the case of $\pi (D-h) \gg h$

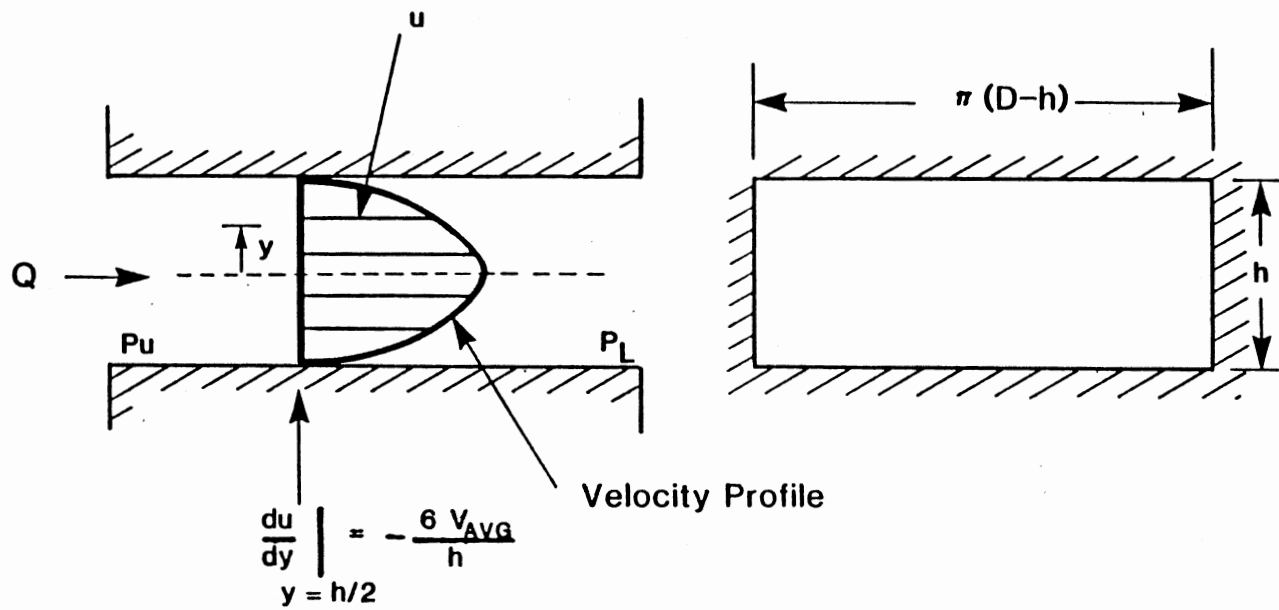


Figure. 30. Laminar Flow Through Flat Plates.

TABLE IV
AVERAGE SHEAR RATE

BORE No.	SPOOL No.	NOMINAL CLEARANCE μm	LAND LENGTH	
			6.38 mm	3.19 mm
3	19	5	452700 1/sec	1154000 1/sec
3	23	10	556200 1/sec	1201000 1/sec
3	26	15	955700 1/sec	2318000 1/sec

the piston-bore assemblies than the leakage flow calculated by the low shear rate absolute viscosity. For these reasons, many of the estimated eccentricities in Table III are below 0.9.

Leakage Flow Test Under Contamination

Though Laurenson [9] indicated in his work that the leakage through the capillary and fine slots seem to decrease exponentially when solid particles silt in the passage, no experimental data is available to support his claim for the case of a piston-bore assembly. In addition, Laurenson used siliconcarbide particles, which are known to have a narrow band size distribution. He did not use ACFTD full distribution, which has a wide band size distribution. This experiment therefore investigates the change in the leakage flow through a piston-bore assembly clearance when the fluid is contaminated with ACFTD full size distribution.

ACFTD full distribution was first injected into the reservoir to achieve a 100 mg/L gravimetric level of the test fluid (Dexron II) circulating through the test hydraulic circuit. Prior to this injection, the filter system was isolated by the valve at the upstream of the filter system. Then, the No. 19 piston was inserted into the No. 3 bore to form the nominal 5 micrometer test clearance between the land of the piston and bore surface. Initially, the test housing was completely isolated from the test circuitry by two ball valves: one at the upstream and the other at the downstream of the test housing. Hence, there was no axial

pressure on the piston-bore assembly. Then, the closed ball valves were opened to introduce 1000 psi axial pressure on the piston-bore assembly. The constant axial pressure was well maintained by controlling the bypass valve.

The leakage flow was collected in a clean bottle for the analysis of Nd: the downstream particle size distribution. When the leakage came out in the form of droplets, these droplets were counted and timed to investigate the silt accumulation in the clearance. Prior to the injection of dust, while the test fluid was clean, the volume of a droplet coming out of the 1/4" tube was determined to be 0.0392 ml/drop and out of the 3/8" tube was 0.0335 ml/drop. The system fluid temperature was always maintained at 60 degrees Celsius plus or minus 2 degrees.

Figure 31 shows the result of the leakage volume in the number of droplets versus time in seconds. The total number of droplets was no more than 17 over a period of 10 minutes for the combination of bore No. 3 and spool No. 19. The leakage flow clearly demonstrated a progressively decreasing trend and deviated further away from the leakage flow with clean fluid as the silting time increased.

If Laurenson's postulate is correct, the leakage can be described by:

$$Q(t) = Q_0 e^{-kt} \quad (57)$$

where

Q_0 = the leakage under clean fluid

k = a constant

t = time

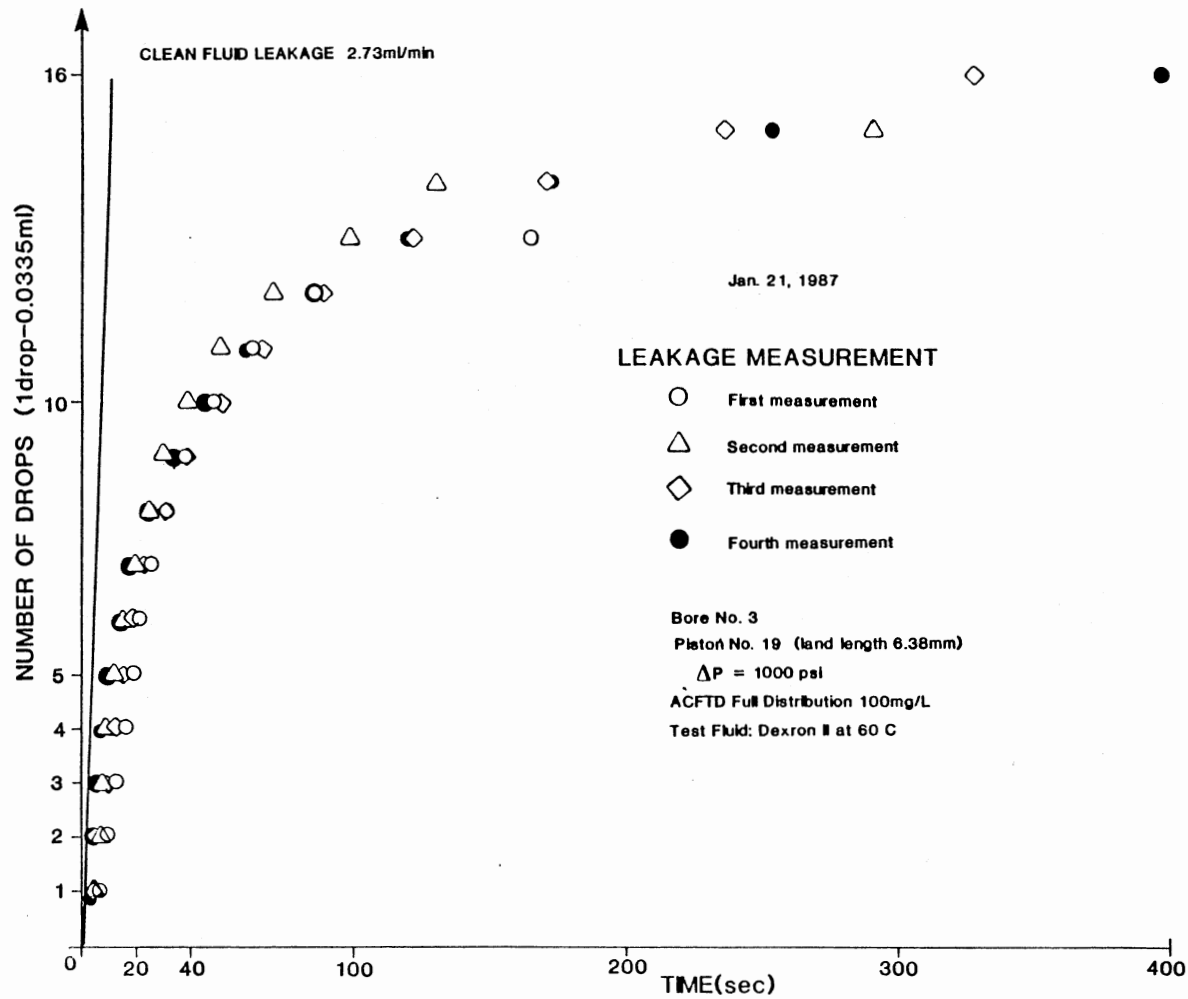


Figure. 31. Piston-Bore Assembly Leakage Volume Under Contamination (100 mg/L).

Equation 57 can be modified as:

$$\ln (Q(t) / Q_0) = -kt \quad (58)$$

Equation 58 shows that the logarithm of $Q(t)$ divided by Q_0 has a linear relationship with time. Figure 32 was derived from Figure 31 to investigate the relationship between the leakage flow and time, as Fig. 25 shows that the leakage passing through the clearance must travel until either the end of the bore piece or the end of the housing to form a droplet. There was a delayed response due to the long passage. The first 20 seconds of Fig. 32 clearly demonstrates the delayed response of the leakage flow rate, which is not conspicuous in Fig. 31. After 20 seconds, the leakage flow rate quickly diverged from the linear relationship. The same leakage test was repeated with 25 mg/L of ACFTD full distribution instead of 100 mg/L.

Figure 33 shows higher leakage volume with a moderately decreasing trend. Since there is a concentration of 25 mg/L of solid particles, it is very logical to have more leakage volume because there are fewer particles to block the passage than when the concentration is 100 mg/L. Figure 34 shows the leakage flow rate analysis. As with Figure 32, there is a delayed response at the beginning, and then later the flow rate deviates from the straight line.

For the first 70% to 80% of the total leakage volume, Laurenson's postulate may correctly predict the reduction of the leakage flow; however, the experimental data of Fig. 32 and 34 clearly show that the

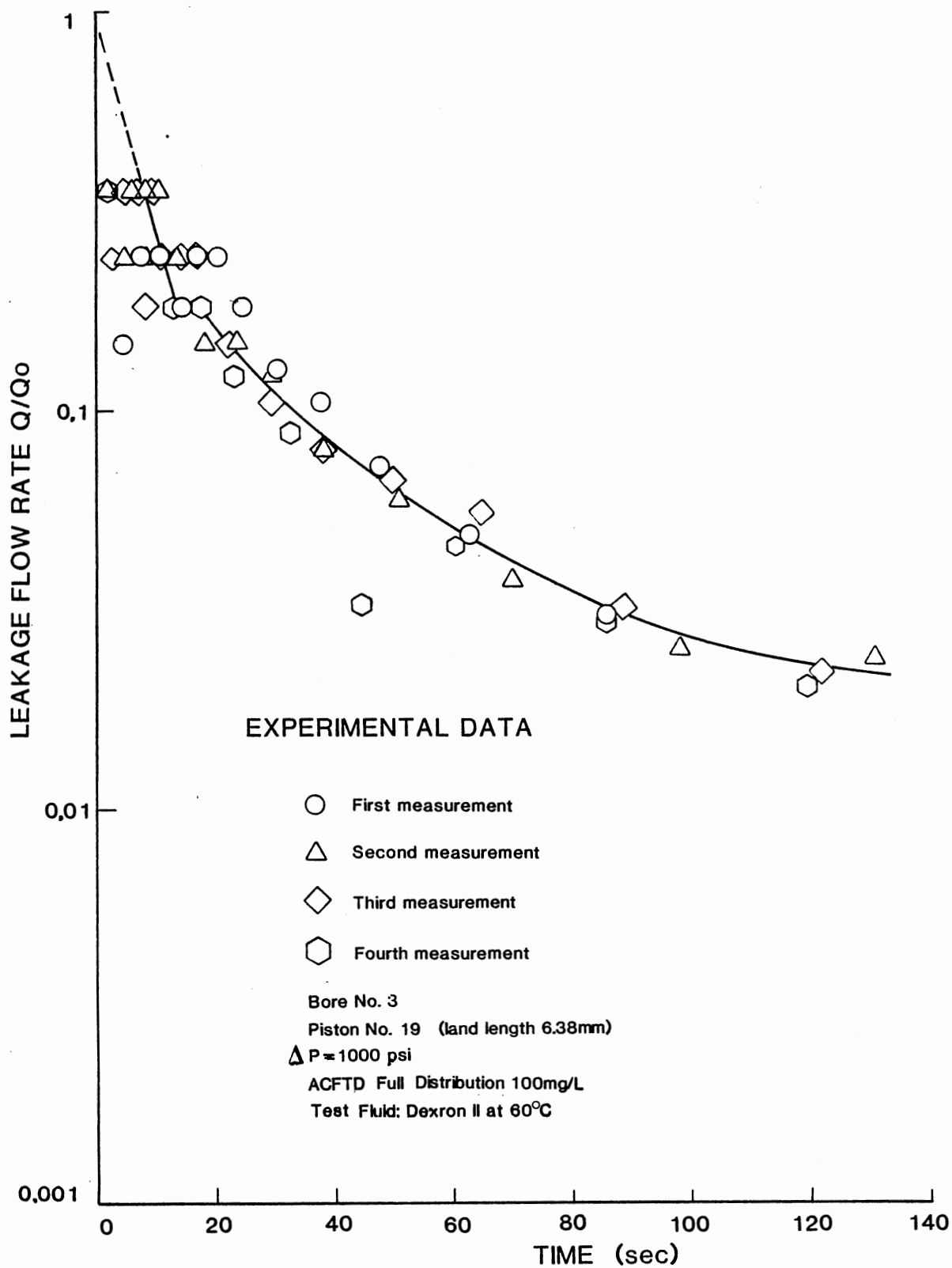


Figure. 32. Piston-Bore Assembly Leakage Flow Rate Under Contamination (100 mg/L).

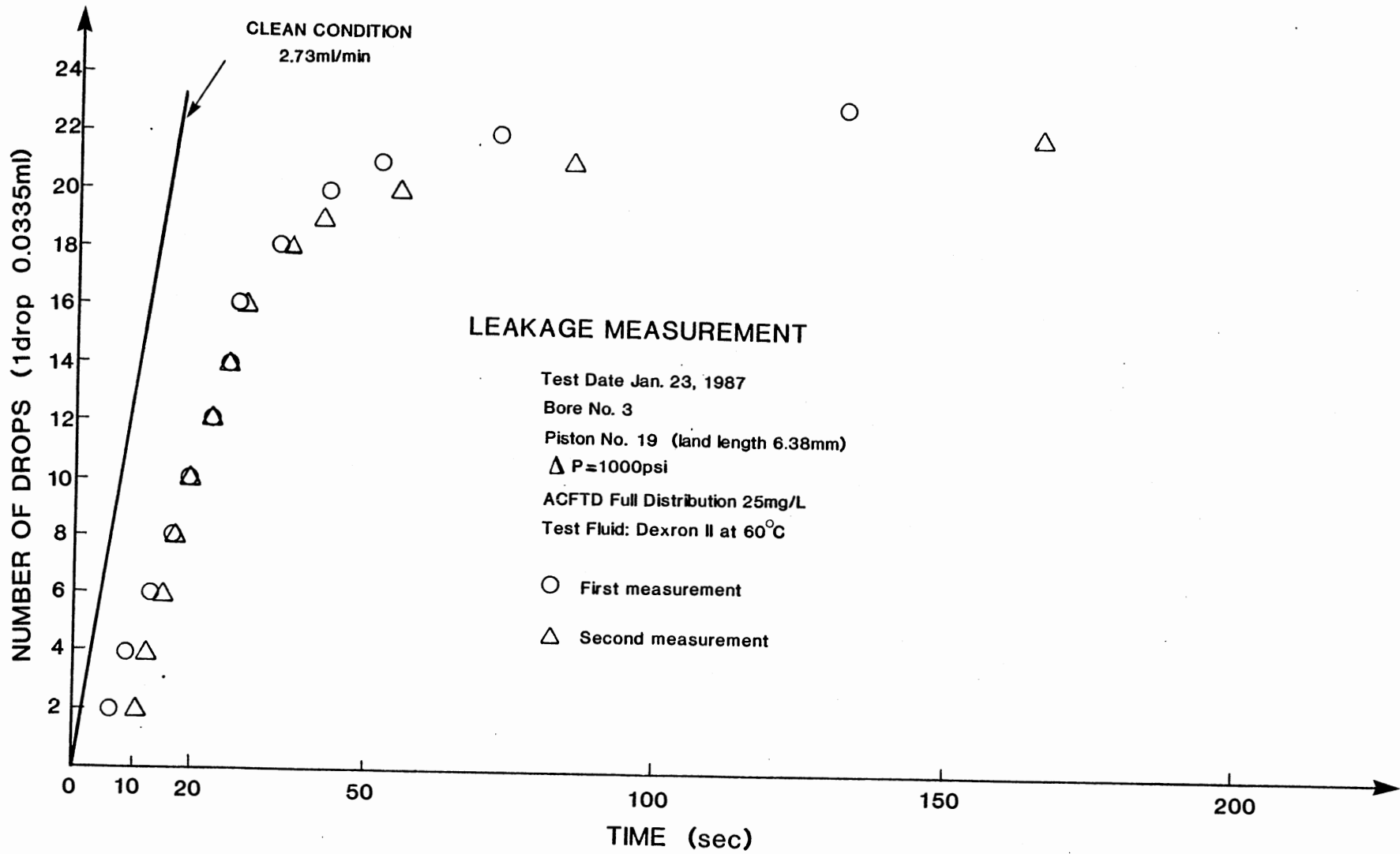


Figure. 33. Piston-Bore Assembly Leakage Volume Under Contamination (25 mg/L).

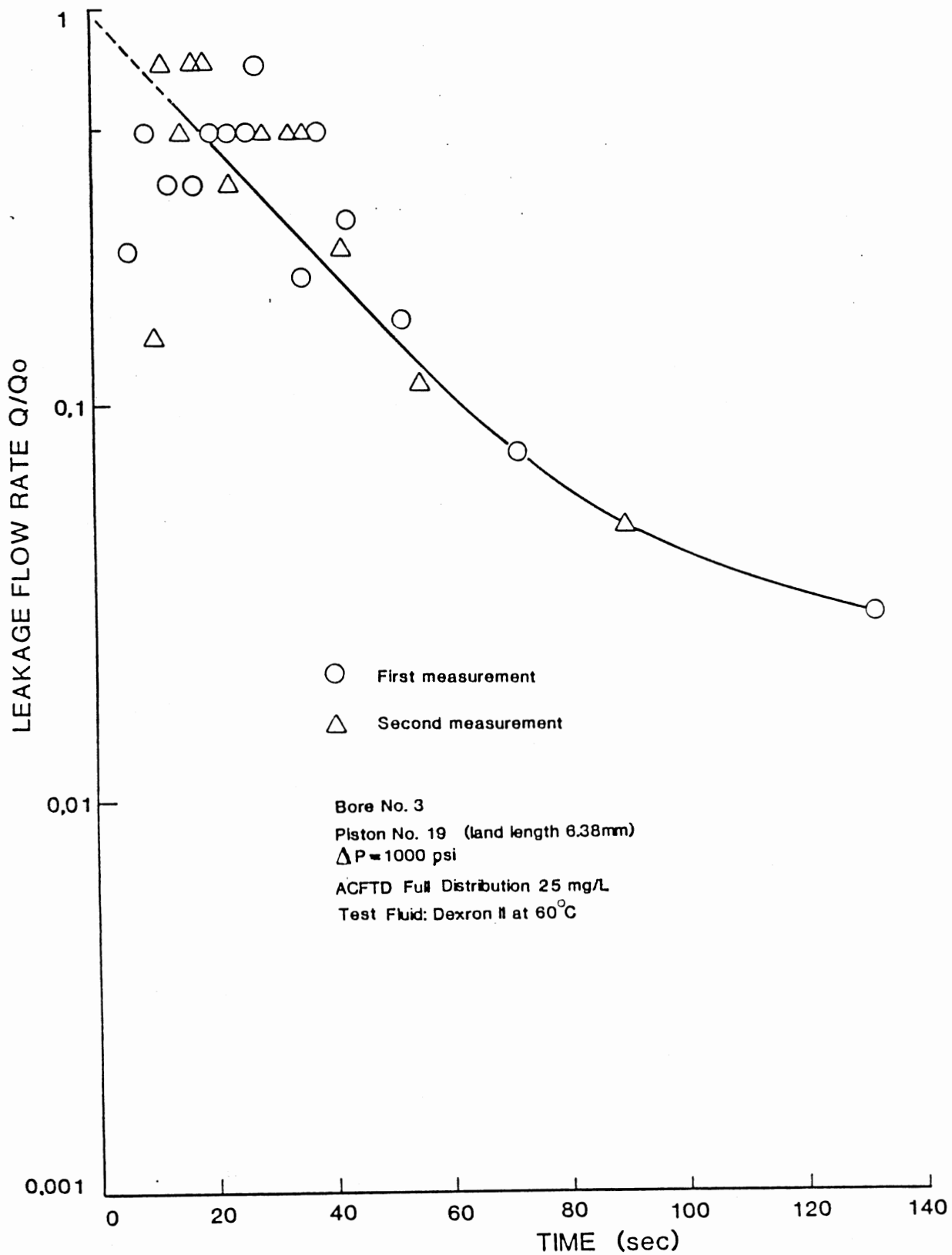


Figure. 34. Piston-Bore Assembly Leakage Flow Rate Under Contamination (25 mg/L).

leakage persists longer than what the initial leakage flow rate projects. The following hypothesis may explain why the leakage flow rate behaves the way Fig. 32 and 34 show. Since Laurenson selected solid particles that have a narrow range of distribution for his experiment, if it is assumed that each particle silted in a piston-bore assembly clearance equally contributes to the reduction of the leakage flow through the clearance, the following differential equation should hold to be true:

$$dQ / dt = -kQ \quad (59)$$

Assuming that particles are uniformly distributed in the fluid, a unit leakage flow rate through the clearance should result in a corresponding decrease in the rate of change in the leakage flow rate per unit time. The solution of Eq. 59 is Eq. 57, and this supports Laurenson's work.

However, when the solid particles have a wide distribution such as ACFTD full distribution, the leakage flow follows Eq. 59 at first, because for a given clearance size, only a particle whose size is close to the clearance can silt. These particles also play a major role in reducing the leakage flow rate at the beginning of the leakage test (see Fig. 35a). Smaller particles silt around the particles whose sizes are close to the clearance size and form a caking condition, as shown in Fig. 35(b). As a result, when the initial particles whose sizes are close to the clearance size no longer have a space to silt, only smaller sized particles can wander through the tortuous path of the cake

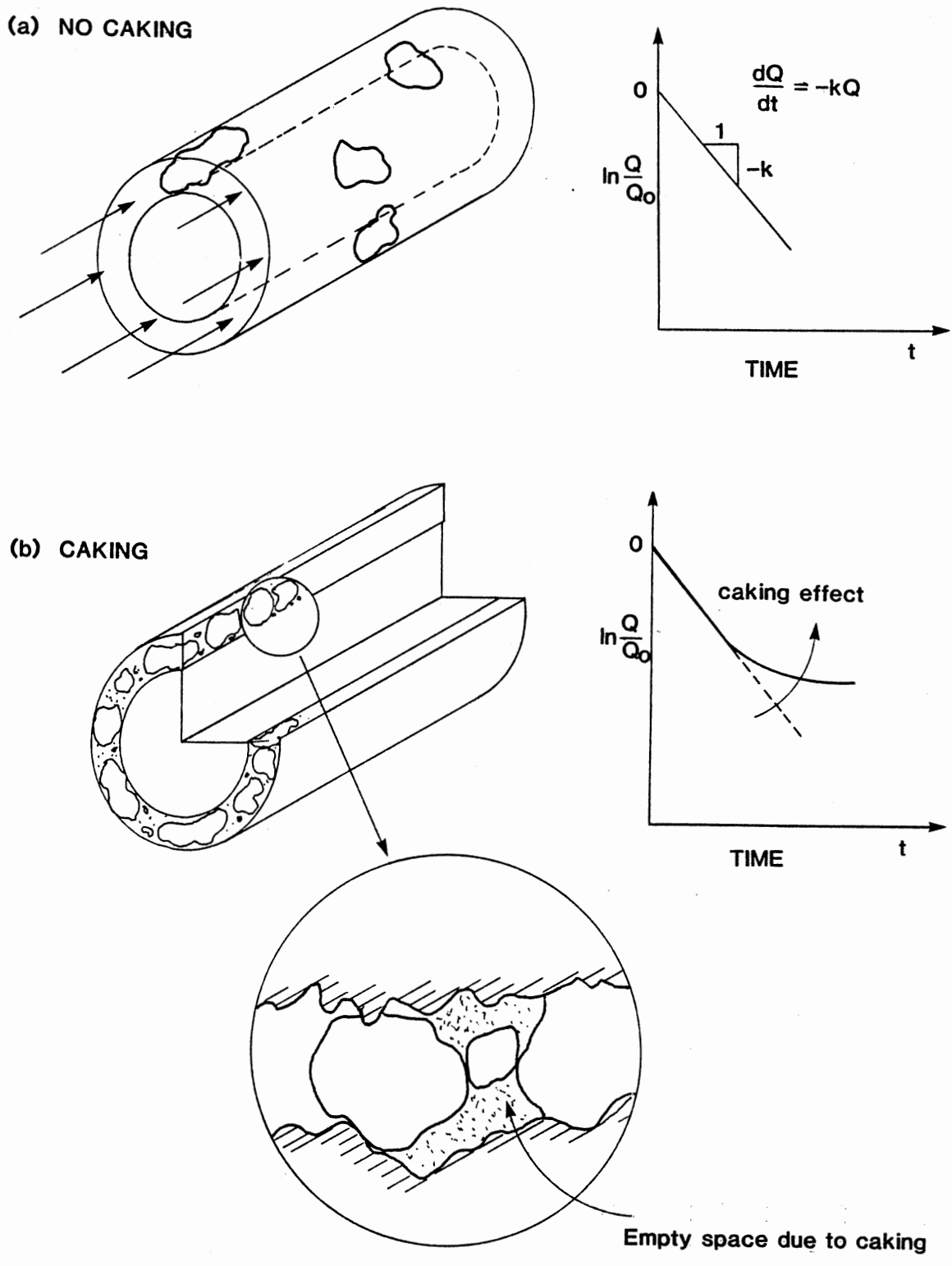


Figure. 35. Cake Formation in the Clearance of the Piston-Bore Assembly.

formation and silt. Hence, Eq. 59 is no longer valid and thus becomes:

$$dQ / dt < -kQ \quad (60)$$

Investigation of Background Count

The leakage flow test of the No. 3 bore and No. 19 piston (with 6.38mm land length) combination gives no more than 17 drops (Fig. 31) when the fluid Dexron II contains 100 mg/L ACFTD full distribution. The total 17 drops or less is not a sufficient sample of fluid to dilute with the super clean fluid and to run through the particle analyzer. Since the minimum necessary sample fluid for particle analysis is about 60 cc, 17 drops only amounts to 0.5695 ml and must be diluted with super clean fluid that is nearly 700 times more in volume to obtain 60 cc. When the sample fluid is diluted 100 times, the particle count of the sample fluid becomes so diluted that it may become impossible to conduct a particle count analysis.

To assess the silt Beta of a piston-bore assembly, the instruments and processes to identify silt Beta had to be qualified (known to be able to achieve the desired task). The leakage flow was collected in a clean bottle. The bottle was cleansed so that when the fluid was added, there was no more than 1.5 particles greater than 10 micrometers per milliliter of super clean fluid. In addition, the super clean fluid itself had a cleanliness level of less than one particle per milliliter greater than

five micrometers. The sample fluid in the clean bottle was later diluted to achieve sufficient fluid volume for the particle analyzer to analyze the particle size distribution.

The most critical process that might destroy the particle size distribution information is this dilution process. Thus, careful attention was paid in order to statistically estimate how much particle size distribution information may have been corrupted through the dilution process. The identified level of corruption due to the dilution process is hereafter called "background count." The expected particle count result of the sampled fluid should be ten times or higher than the background count so that the sample fluid count will not be corrupted by the background.

The minimum sample fluid volume for the particle analyzer is 60 cc. Thus, the total sample fluid volume had to be high enough so that the added super clean fluid would not dilute excessively. Since the minimum concentration that was used in the silt Beta test was 25 mg/L, the nominal particle count of 25 mg/L ACFTD full distribution greater than 5 micrometers was 12917. If this were diluted x times, the diluted count would be:

$$\text{diluted count} = 12917 / x \quad (61)$$

The background count should not exceed 10% of the diluted count; then,

$$\text{background count} < 0.1 (\text{diluted count}) \quad (62)$$

Combining Equations 61 and 62, Eq. 63 results in:

$$x < 1291.7 / \text{background count} \quad (63)$$

So, as soon as the background count is available, the maximum allowable dilution factor x can be found.

Figure 36 shows the process employed to make the sample for the particle analyzer. The leakage volume was first poured into a pipet to measure the volume accurately. It took approximately 10 minutes to transfer most of the fluid in the 15 cc bottle to the pipet. Then, the fluid was poured into a 125 cc clean bottle. Step 3 and 4 were repeated at least twice to transfer particles from the pipet to the 125 cc bottle. To transfer the remaining particles in the 15 cc bottle to the 125 cc bottle, a known super clean fluid measured by a graduated cylinder was poured into the 15 cc bottle. Then, the 15 cc bottle was shaken vigorously with its clean cap on, and the fluid was poured into the 125 cc bottle. These steps, 5, 6, 7, and 8, were repeated at least twice.

After each step was completed, the pipet, graduated cylinder, and rubber glove were immediately flushed with ether to clean off any residual solid particles on their surface.

As Figure 36 shows, steps 1, 4, 6, and 7 may introduce additional particles because the leakage comes in contact with surfaces that may have foreign particles. As a result, due to the intrusion of foreign particles, it was important to know how many particles there would be in the 125 cc sample bottle after the dilution process.

By following all of the steps in Fig. 36 with super clean fluid in the 15 cc sample bottle instead of the sample fluid, the background count in the 125 cc bottle was identified. The results of 54 analyses are plotted in Fig. 37. As Figure 37 shows, the number of particles per

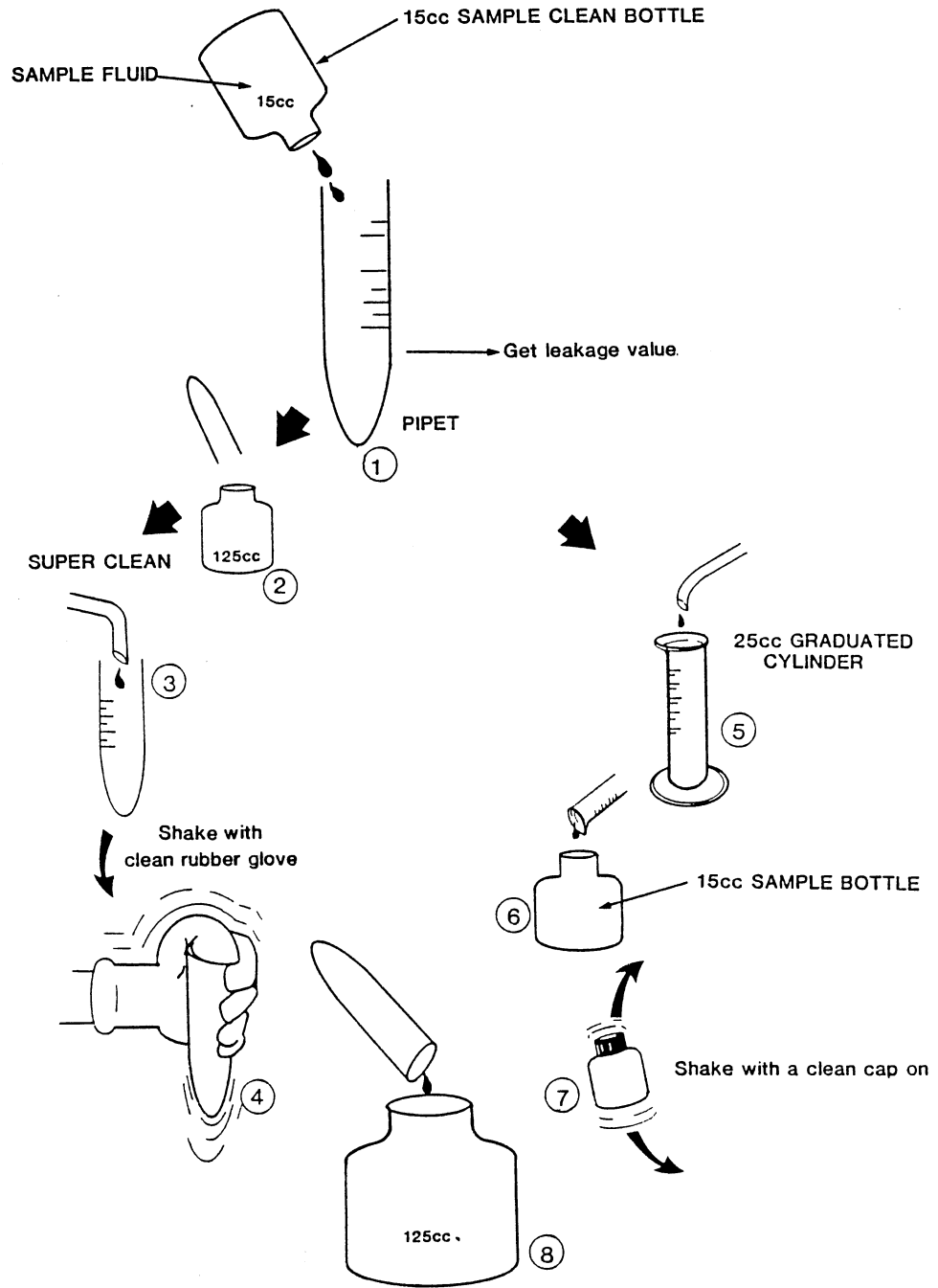


Figure 36. Dilution Process.

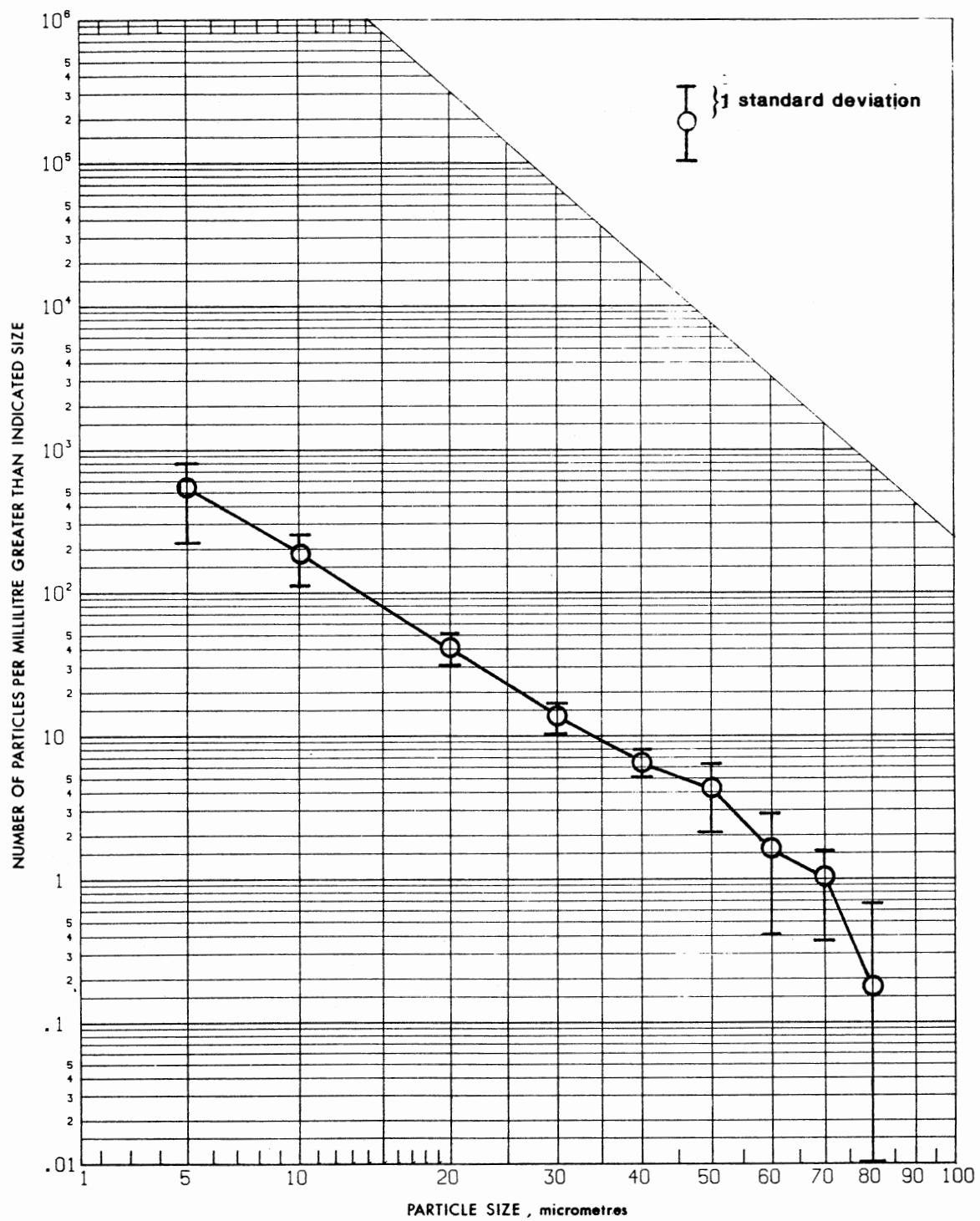


Figure 37. Dilution Process of Background Count (I).

milliliter greater than 5 micrometers is 563. Using Eq 63, the maximum allowable dilution factor is 2.29. Figure 38 shows just how important it is to maintain a high level of cleanliness throughout the dilution process. The data specified by the triangle were obtained when bare fingers were used in step 4 of Fig. 36. The background was tremendously corrupted.

The Hiac-Royco Particle Size Analyzer Model : PC-320 with the Hiac Particle Counting Sensor G3-90-68sp were used to analyze the upstream and downstream particle size distribution (Fig. 39). The counter and sensors were calibrated per ISO standard 4402. The sample bottles were shaken vigorously by a paint shaker for 15 minutes. Then, they were placed in an ultrasonic bath to eliminate the bubbles in the fluid. After that, the bottle cap was taken off and the bottle was placed in a vacuum chamber to further degas the fluid until no significant bubbles remained. Finally, the sample bottle was placed in the chamber shown in Fig. 39 to conduct particle counts. An air pump pressurized the chamber causing the sample fluid to travel up the channel which passes through the particle counting sensor. When the fluid level in the metering tube hit the lower level sensor, the particle counter began counting until the fluid level reached the upper level sensor. By positioning the level sensors so that the volume passing through the particle counter sensor was known, the number of particles were counted in the counter and were then described in a per milliliter basis. From the information obtained from the calibration method mentioned earlier, the counter was set to measure the number of particles at the desired size or greater.

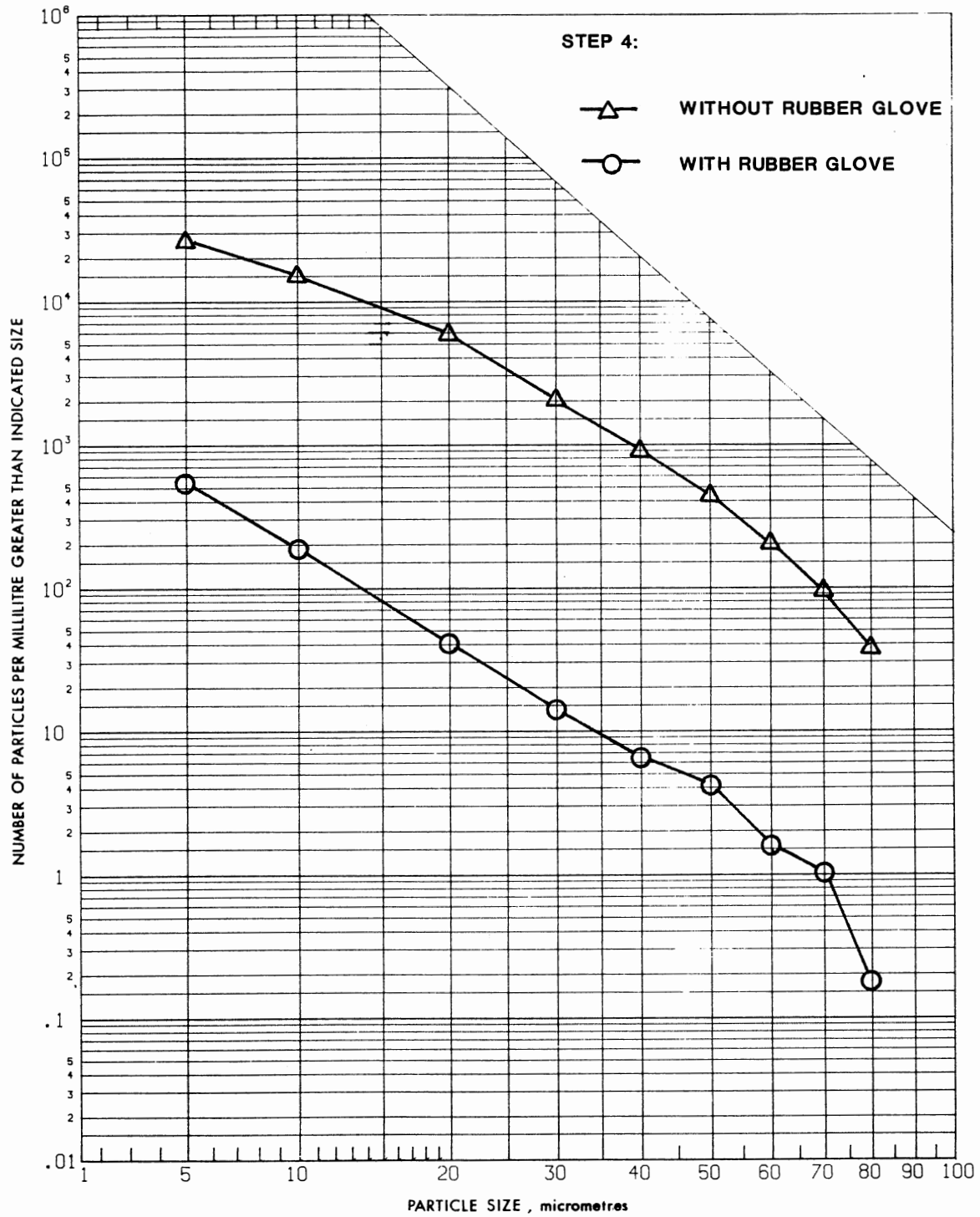


Figure 38. Dilution Process of Background Count (II).

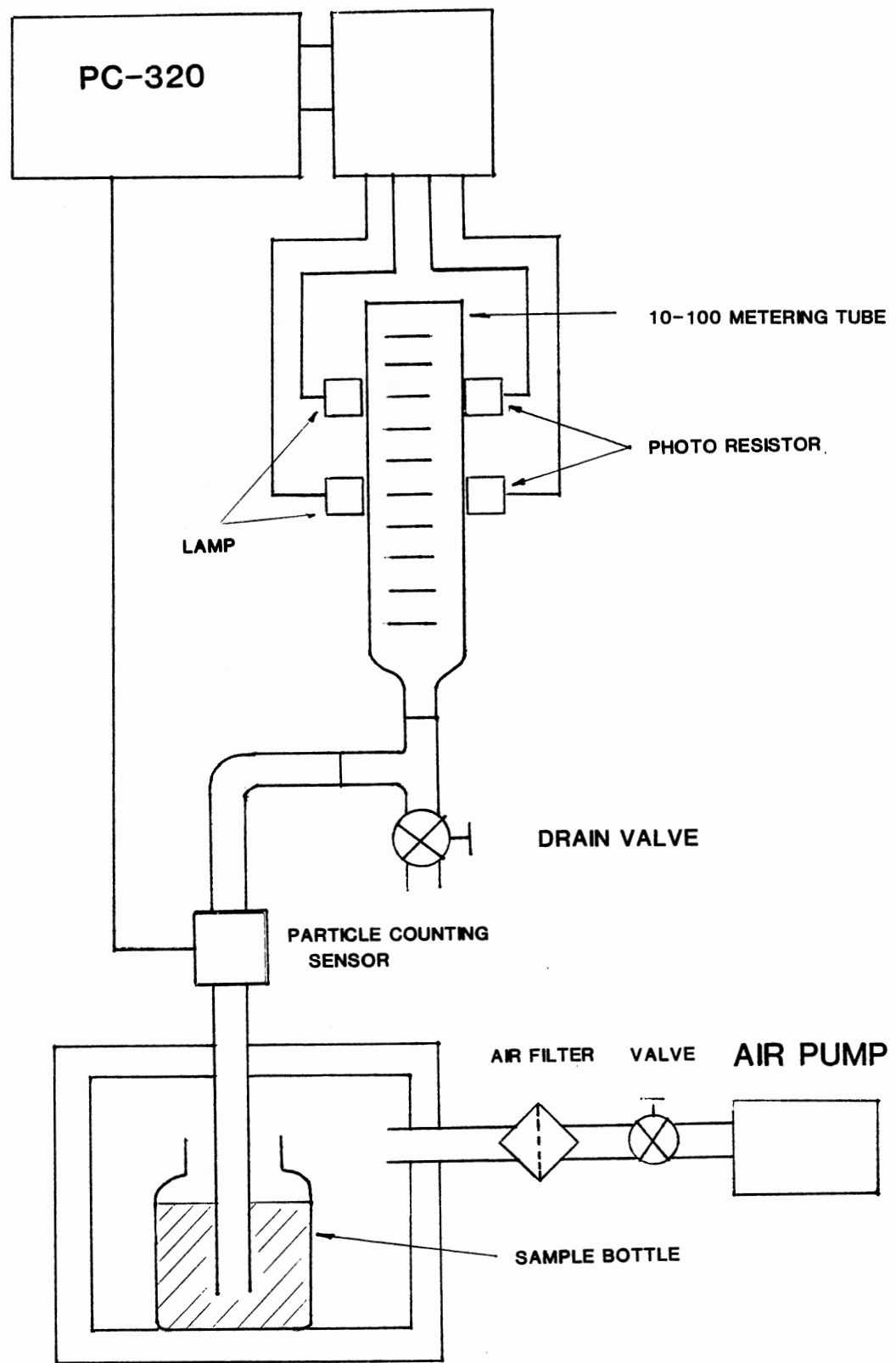


Figure 39. Particle Count Analysis Facility.

Silt Beta Experiment

The leakage was collected in clean bottles while the system pressure was set at 1000 psi. The sample position of the leakage is called "downstream" and the collected leakage itself is the downstream sample (see Fig. 2). The upstream sample was collected from the main test circuitry. In order to collect a sufficient amount of fluid for the particle analysis, the leakage test was repeated several times. Prior to each leakage test, the clearance was first flushed by the test fluid circulating through the hydraulic circuitry. This was done simply by pulling the piston out of the bore. Then, the test housing was isolated from the rest of the test circuitry by closing both of the ball valves located right next to the test housing. After that, the piston was positioned back inside the bore to establish the test clearance, as in Fig. 25.

To flush residual particles in the bore surface and the test housing, the nozzle of a plastic bottle containing ether was inserted as shown in Fig. 40. This process was repeated several times to ensure that the flushing was performed properly.

The downstream and upstream samples were collected as Table V shows. The samples were collected within a 10 minute period, which was sufficient to determine the last drop the system could collect. The detailed results of Test Code 2I are shown in Fig. 41. Test Code 1I contains the upstream sample and 2I contains the downstream sample particle size distribution, as Fig. 41 shows. The difference between the

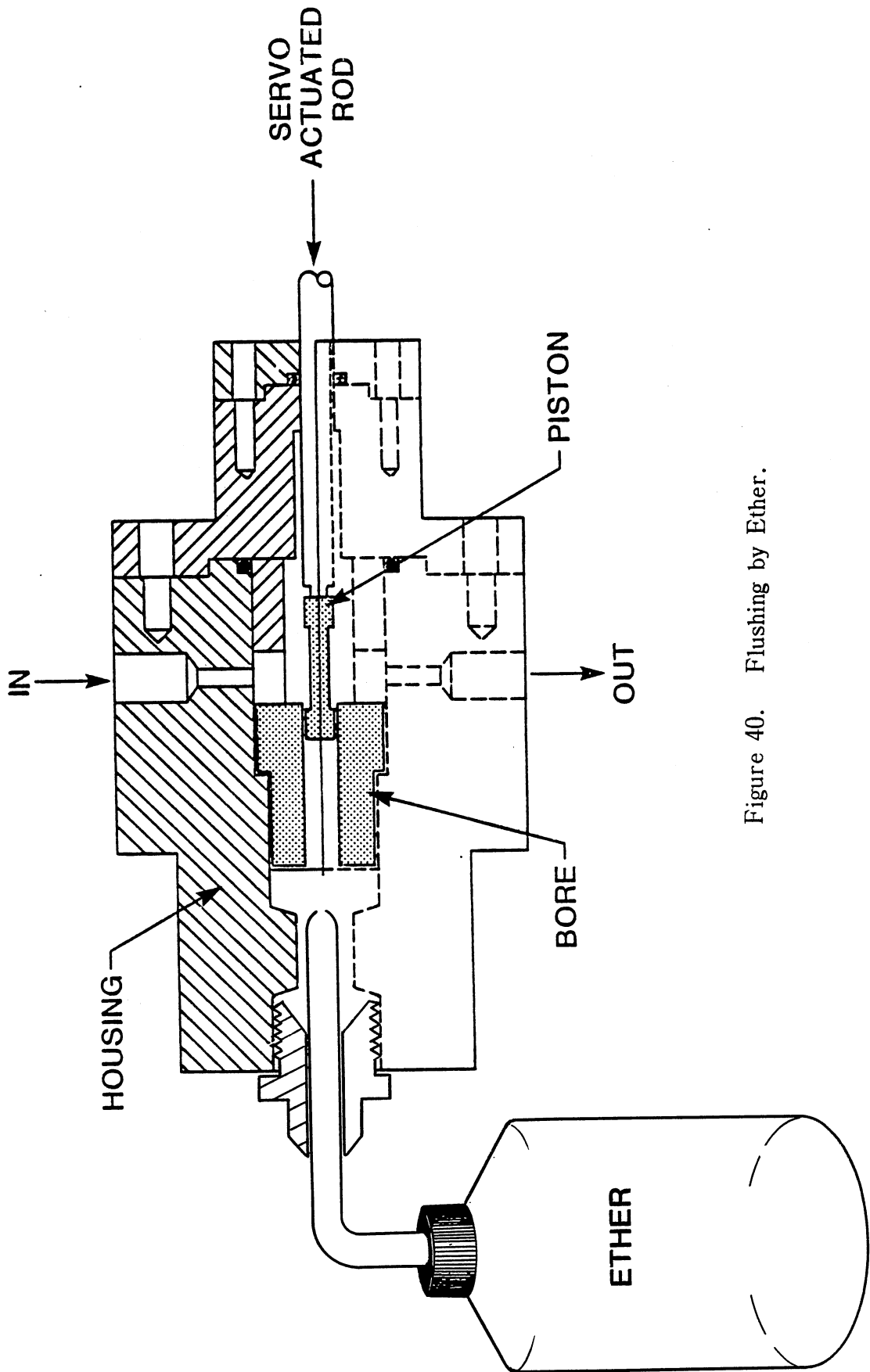


Figure 40. Flushing by Ether.

TABLE V
SILT BETA ASSESSMENT TEST

<TEST CONDITIONS>

BORE NO. 3
 CONTAMINANT: ACFTD FULL DISTRIBUTION
 CONCENTRATION: 25 mg/L
 PRESSURE DIF.: 1000 psi
 TEST FLUID: Dexron II at 60 degrees celsius

NOMINAL CLEARANCE SIZE(m)	SPOOL NO.	LAND LENGTH (mm)	TEST CODE	SAMPLE POSITION
5	19	6.38	1I 2I 3I	UPSTREAM DOWNSTREAM DOWNSTREAM
5	19	3.19	1J 2J 3J	UPSTREAM DOWNSTREAM DOWNSTREAM
10	23	6.38	1K 3K	UPSTREAM DOWNSTREAM
10	23	3.19	1L 3L	UPSTREAM DOWNSTREAM
15	25	6.38	1G 2G	UPSTREAM DOWNSTREAM
15	25	3.19	1H 2H 4H	UPSTREAM DOWNSTREAM DOWNSTREAM

***** 1 & 2H TEST RESULT *****

Bore No.3 - Piston No.19, Land Length (6.39 mm)
5 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	11008.8	7279.271	1.512349
10	3597.918	2878.8	958.8991	3.827451
20	637.1161	487.1	113.8693	4.277713
30	187.6002	132.4	23.8326	5.555416
40	71.72498	48.5	5.8554	9.593702
50	32.244	22.4	2.8888	7.754084
60	16.28372	8.729999	.238326	36.63049
70	8.837601	3.81	.238326	15.9865
80	5.133417	2.09	.01	****

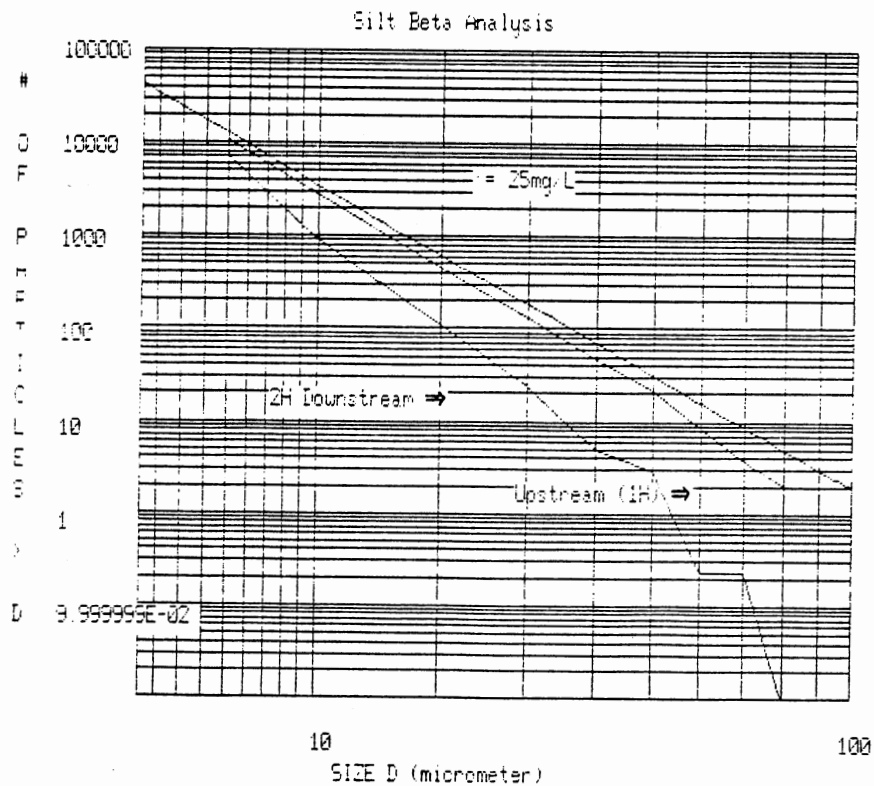


Figure 41. Particle Size Distribution Analysis.

upstream and downstream clearly demonstrates that the piston-bore assembly (bore No. 3 and piston No. 19 with 6.19 mm land) filtered particles as the leakage passed through the clearance of the piston-bore assembly.

The combination of bore No. 3 and piston No. 19 gives the nominal clearance size of 5 micrometers. Therefore, when the piston is fully eccentric with the bore, the largest clearance is 10 micrometers. Since the average length to width ratio of ACFTD full distribution is 1.49/1, it is possible that a particle with a length of 1.49 micrometers and a width of 10 micrometers can enter the clearance, as shown in Fig. 42. Moreover, the length to width ratio 1.49 is the average ratio, and careful microscopic observation of ACFTD shows that the length to width ratio of ACFTD does not exceed 3 to 1. Therefore, there should be no particles greater than 30 micrometers at downstream for the combination of the No. 3 bore and No. 19 piston (having a nominal clearance of 5 micrometers).

Though Figure 41 shows the presence of particles above 30 micrometers at downstream, as the background count of Fig. 37 presents, the downstream counts are corrupted by the background counts. The downstream particle count at 5 micrometers is the most accurate value because the average background count at 5 micrometers only amounts to 7.7% of the downstream count. However, the average background count comes close to 19% of the downstream particle count at 10 micrometers; thus, the downstream count at 10 micrometers is less accurate than the particle count at 5 micrometers. The downstream particle count at larger than 10

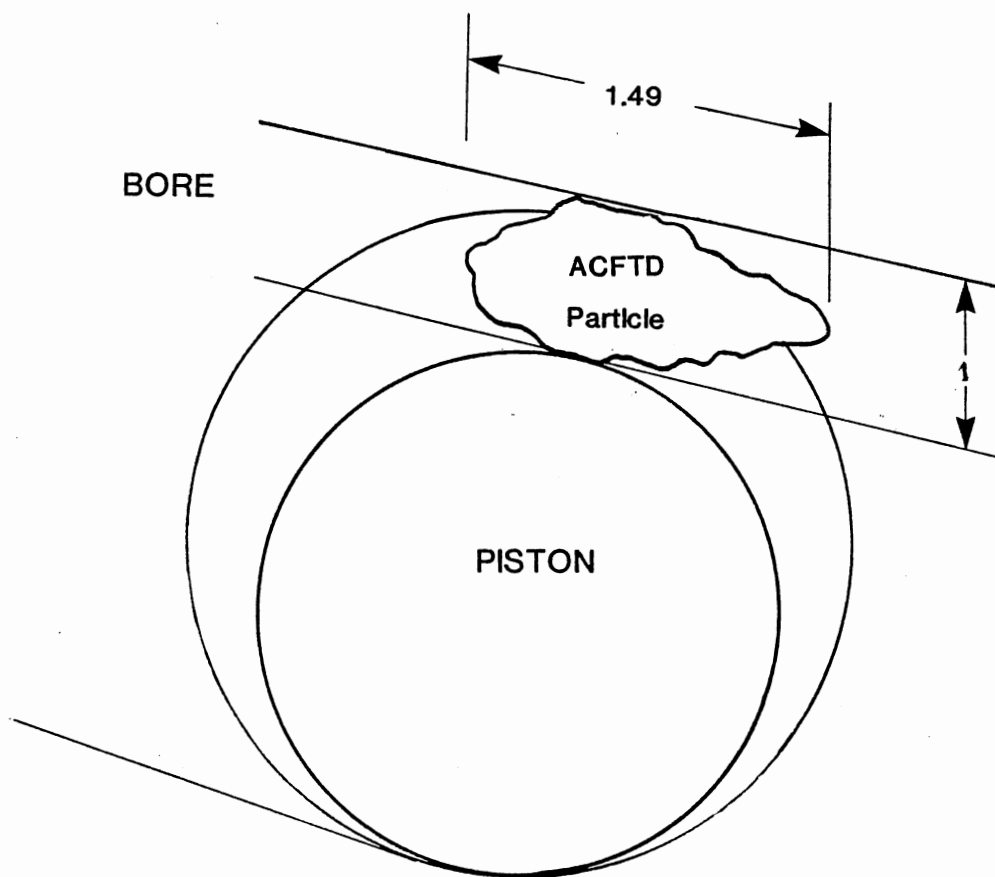


Figure 42. Maximum Entrained Particle Size.

micrometers becomes less accurate as the particle size becomes larger. Therefore, 5 μ m and 10 μ m are the two datapoints with the least error. Based on these datapoints, the following silt Beta model is developed.

Silt Beta Model

Tessman and Fitch [23] presented the filtration Beta of hydraulic filter elements as a function of particle size (Fig. 43). This relation can be closely approximated by:

$$\ln \beta = M + R \ln^2 D \quad (64)$$

where

M & R = constants

β = filtration Beta

D = particle size

Hydraulic filter elements have a certain pore size distribution, and the maximum size at which particles can pass through is not definite, whereas a piston-bore assembly can have the maximum limit because of its known geometrical configuration. Therefore, the upper limit size constraint was added in Eq. 64, and the silt Beta model for a piston-bore assembly became:

$$\ln \beta = M + R \ln^2 D - U \ln (\ln^2 C - \ln^2 D) \quad (65)$$

where

U = constant

C = upper limit size in micrometers

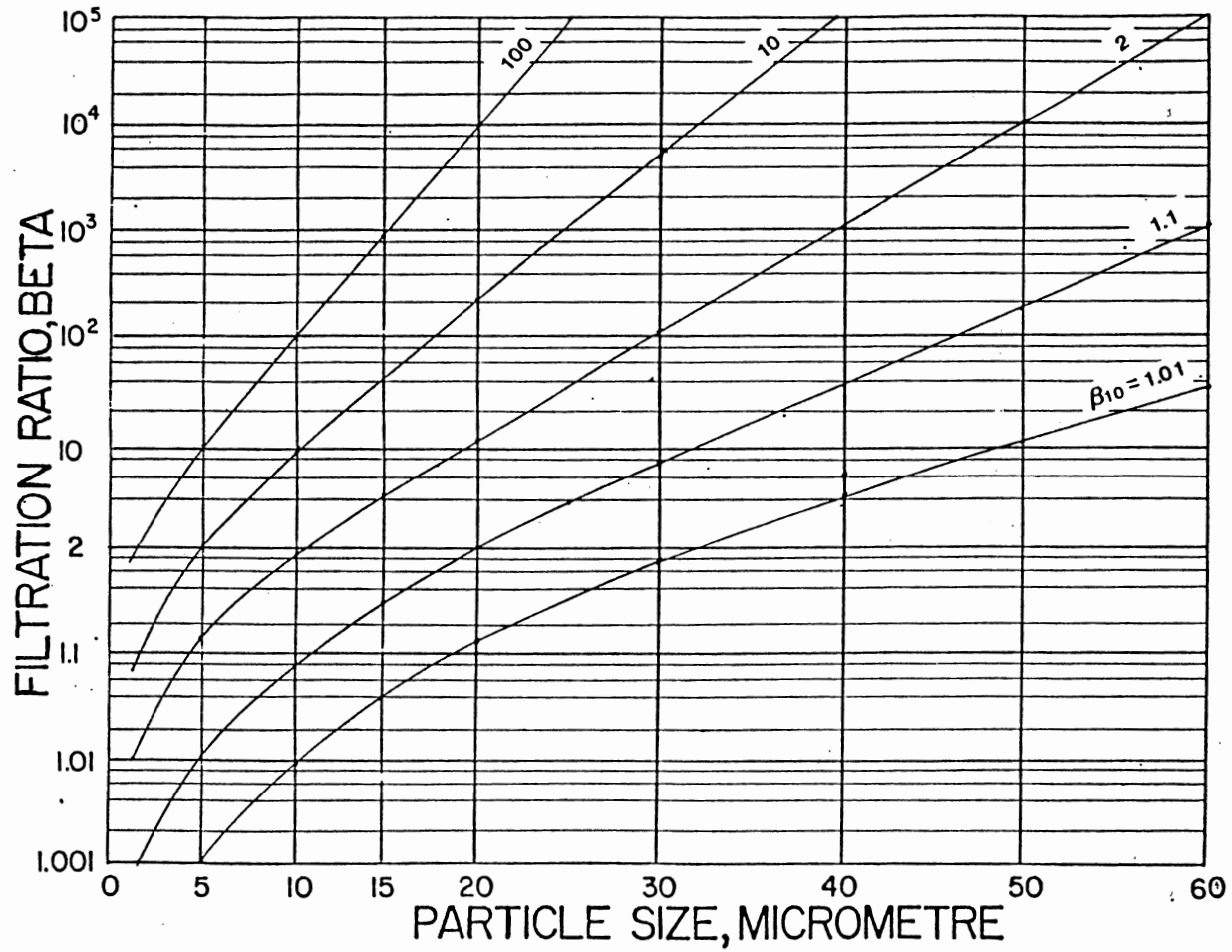


Figure 43. Log Normal Filter Model.

Three experimental data points are needed to determine three constants in Eq. 65. However, as found in previous sections, only the data at 5 micrometers and 10 micrometers can maintain the average error percentage less than 20 percent. As a consequence, further data was taken from the following assumption. If the number of particles filtered per milliliter greater than 5 micrometers is described as:

$$\Delta_5 = Nu_5 - Nd_5 \quad (66)$$

then the particles filtered at greater than 1 micrometer is:

$$\Delta_1 = Nu_1 - Nd_1 \quad (67)$$

and the postulate is:

$$\Delta_1 \geq \Delta_5 \quad (68)$$

This assumption is valid as long as there is no significant desorption of once filtered particles in the clearance. Figure 44 describes why. When the upstream and downstream particle size distribution is described in the graph as frequency versus size, it will be as shown in Fig. 44. What is described by Eq 66 is the area between the upstream and downstream greater than 5 micrometers; the area between the upstream and downstream greater than 1 micrometer is described by Eq 67. As long as there is no desorption of silted particles, the downstream curve will not exceed the upstream, and thus Eq. 68 holds true. Combining Equations 66 through 68,

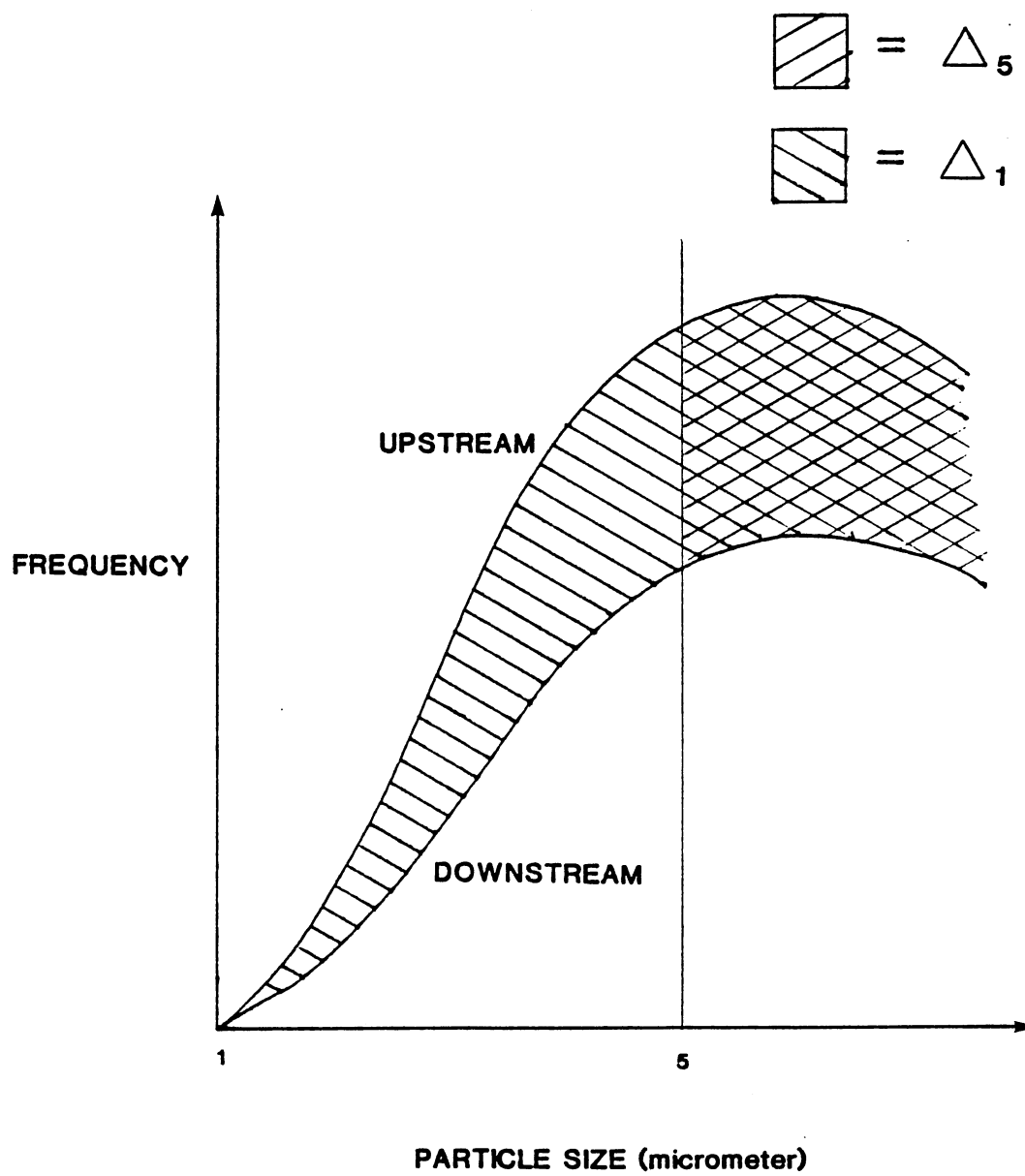


Figure 44. Frequency Versus Particle Size.

Eq. 69 results in:

$$\text{Nu}_1 \left(1 - \frac{\text{Nd}_1}{\text{Nu}_1}\right) \geq \text{Nu}_5 \left(1 - \frac{\text{Nd}_5}{\text{Nu}_5}\right) \quad (69)$$

Using the definition of Beta,

$$\beta = \text{Nd} / \text{Nu} \quad \beta = \frac{\text{Nu}}{\text{Nd}} \quad (70)$$

Equation 69 becomes:

$$\frac{\text{Nu}_1}{\text{Nd}_1} \left(1 - \frac{1}{\beta_1}\right) \geq \left(1 - \frac{1}{\beta_5}\right) \quad (71)$$

Since the upstream is ACFTD full distribution, Nu1 divided by Nu5 is always 1.259, as follows:

$$T = \frac{\text{Nu}_1}{\text{Nu}_5} = e^{\text{Bu} (\ln^2(5) - \ln^2(1))} = 1.259 \quad (72)$$

Solving for β_1 , Eq. 71 becomes:

$$\beta_1 > \frac{1}{1 - (1 - 1/\beta_5)(1/T)} \quad (73)$$

It is also known from Fig. 43 that:

$$\beta_5 > \beta_1 \quad (74)$$

Figure 45 shows the boundary of values that β_1 can take, provided that there is no desorption of silted particles.

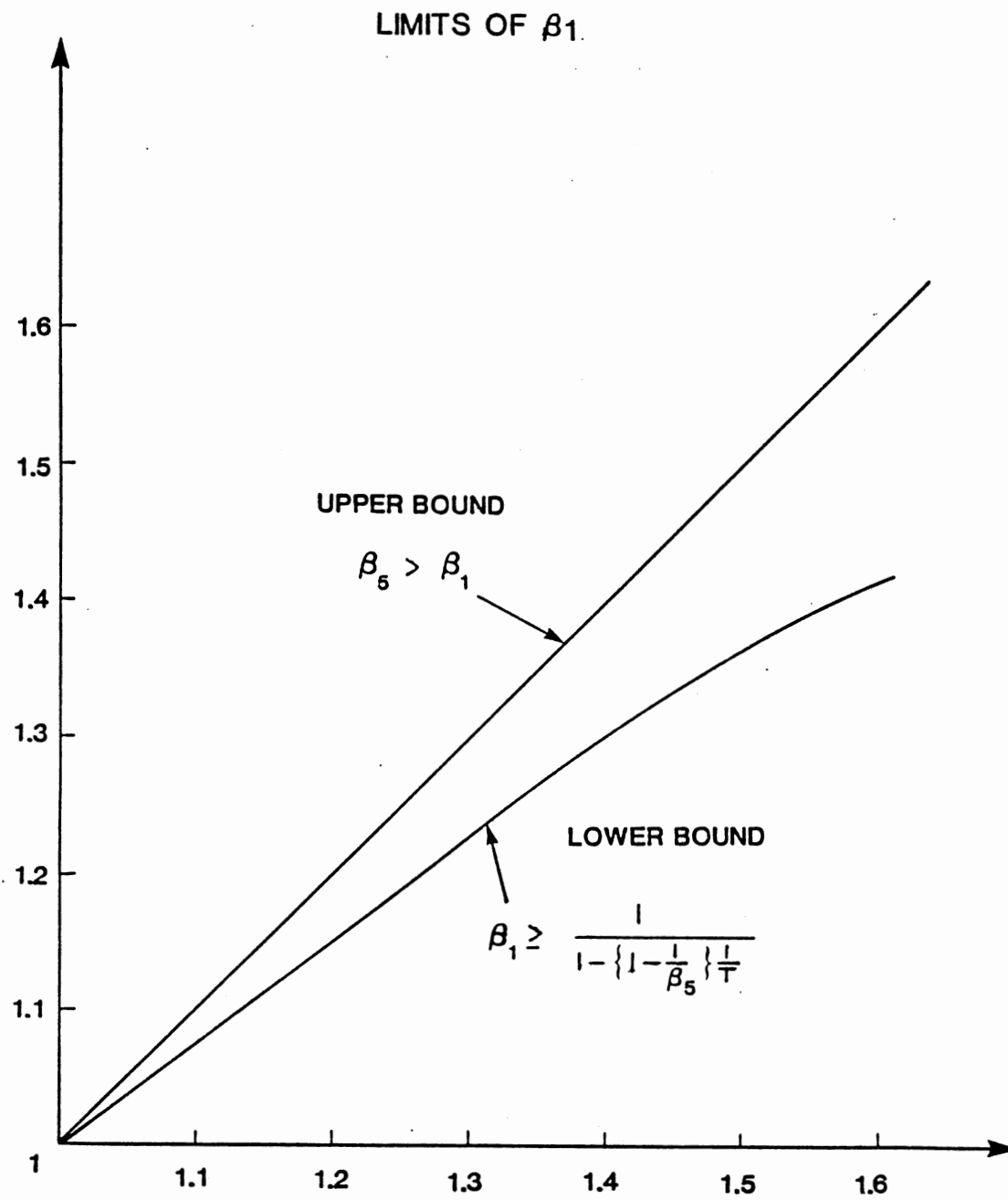


Figure 45. Limits of β_1 .

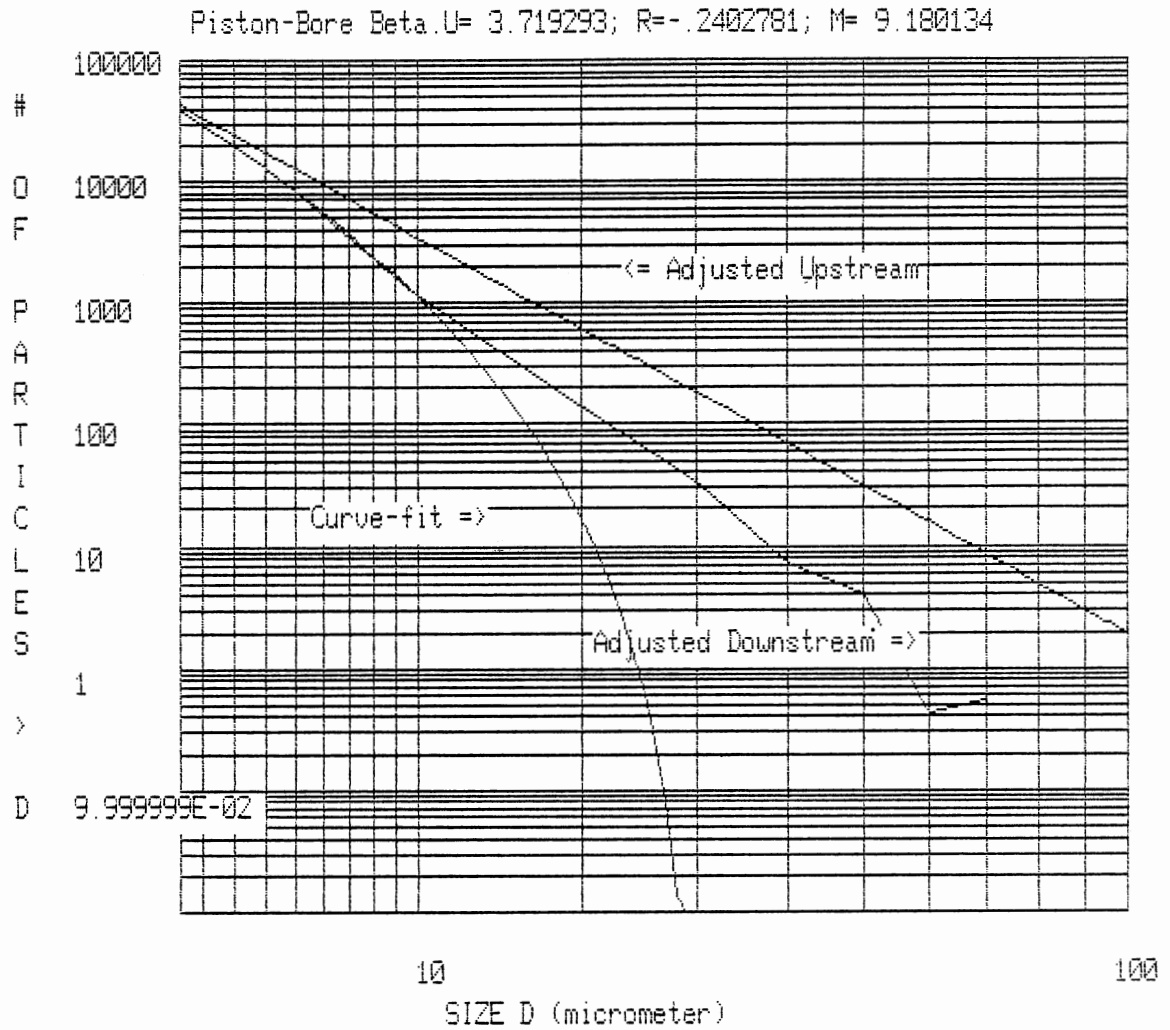
For the third data to find the constants of Eq. 65, Eq. 75 was chosen because this silt Beta value:

$$\beta_1 = \frac{1}{1 - (1 - 1 / \beta_5)(1 / \tau)} \quad (75)$$

is the most conservative value, and the error involved with this choice is a maximum of 11 percent at $\beta_5 = 1.6$, and at the smaller value of β_5 , the error is less. Keeping the same silt Beta value at each particle size shown in Fig. 41, the downstream was redrawn in relation to the theoretical 25 mg/L ACFTD full distribution as the upstream particle size distribution in Fig. 46. Figure 46 demonstrates a good agreement between the silt model curve of the downstream distribution and the experimental data for the 1 to 10 micrometers range; it also demonstrates a diverging deviation after 10 micrometers. As a consequence, this silt model curve satisfies two important conditions:

1. The model fits well between 1 to 10 micrometers where the actual downstream data is the most accurate.
2. The curve satisfies the maximum particle size at which no particle should be found in the downstream.

The silt Beta test data analyses for 3I through 4H shown in Table V are presented in Appendix B. The silt models found from the silt Beta test are plotted in Fig. 47. In the figure, hydraulic filter Beta curves are also superimposed. This figure clearly demonstrates that the smaller the nominal clearance is, the higher the silt Beta is. Moreover, the silt model tends to have better Beta values than the hydraulic filter



Size micron	Upstream	Downstream	Beta
1	43797.5	40067.96	1.09308
5	12917.2	8541.142	1.51235
10	3597.918	1188.432	3.02745
15	1380.819	170.7609	8.08627
20	637.1161	18.3983	34.62907
25	331.3792	.718631	461.1257
30	187.6002	.01	****
35	113.1623	.01	****
40	71.72498	.01	****
45	47.30907	.01	****
50	32.244	.01	****

Figure 46. Silt Beta Model Fit.

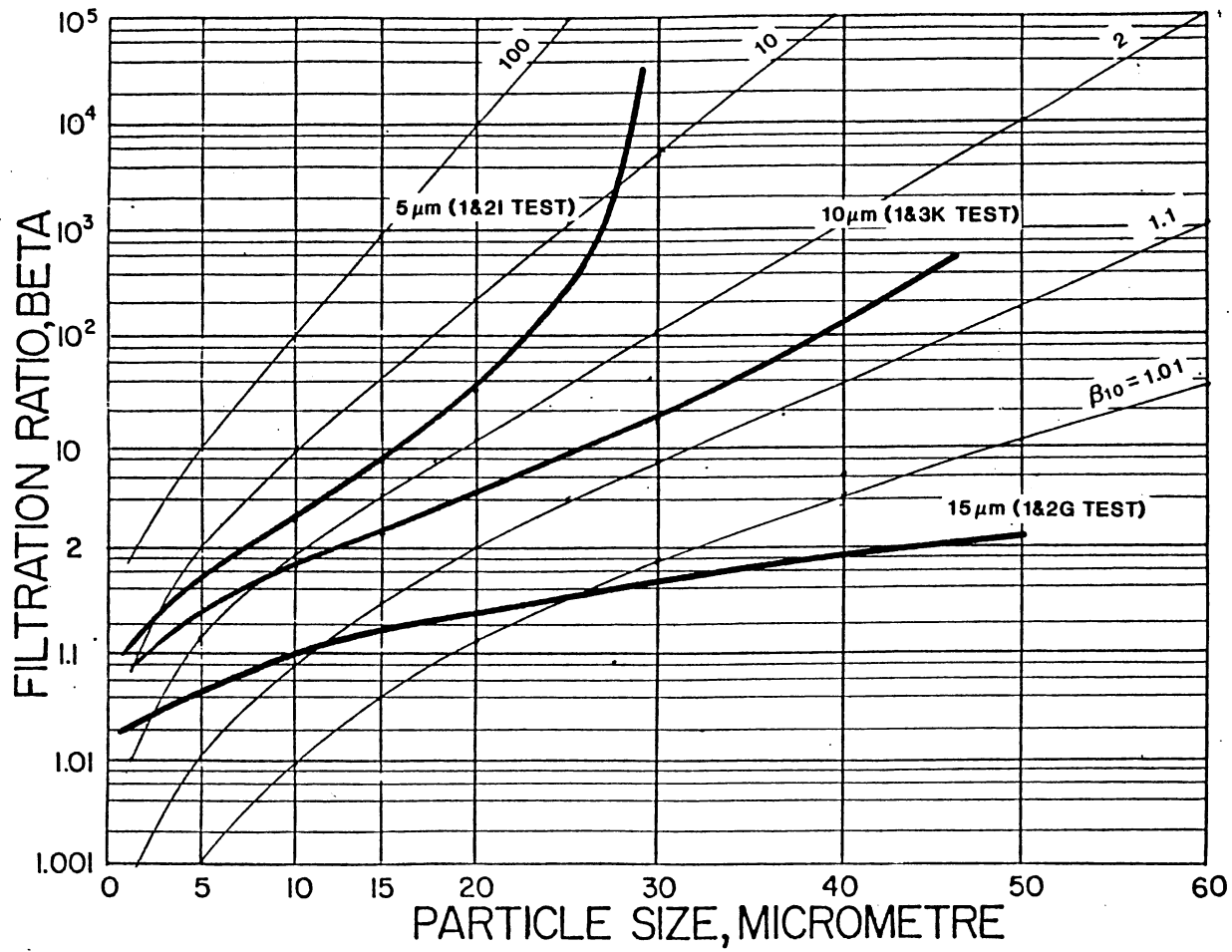


Figure 47. Piston-Bore Assembly Silt Beta (6.38mm Land Length).

Beta at below the 10 micrometers range. Since the silt model is derived from data at 1, 5, and 10 micrometers with their maximum error percentage at 3.3, 7.7, and 19 respectively, data in this range maintains high accuracy, and Beta values of piston-bore assemblies tend to maintain higher values than the hydraulic filter in this range. Furthermore, the Beta values in Fig. 47 were converted into the filter efficiency by the equation:

$$\eta = 1 - 1 / \beta \quad (76)$$

and plotted in Fig. 48. Hydraulic filter elements' filter efficiency [24] lines were also plotted to compare with the filter efficiency of piston-bore assemblies. This figure shows that hydraulic filter elements are straight lines, indicating that:

$$\eta = \int_{-\infty}^{Xe} \frac{1}{\sqrt{2\pi}} e^{-x^2/2} dx \quad (77)$$

and X_e is expressed as:

$$X_e = k_1 \log D + k_2 \quad (78)$$

where

k_1 and k_2 = constants

D = particle size in micrometers

On the other hand, the filtration efficiency is nonlinear, and thus the

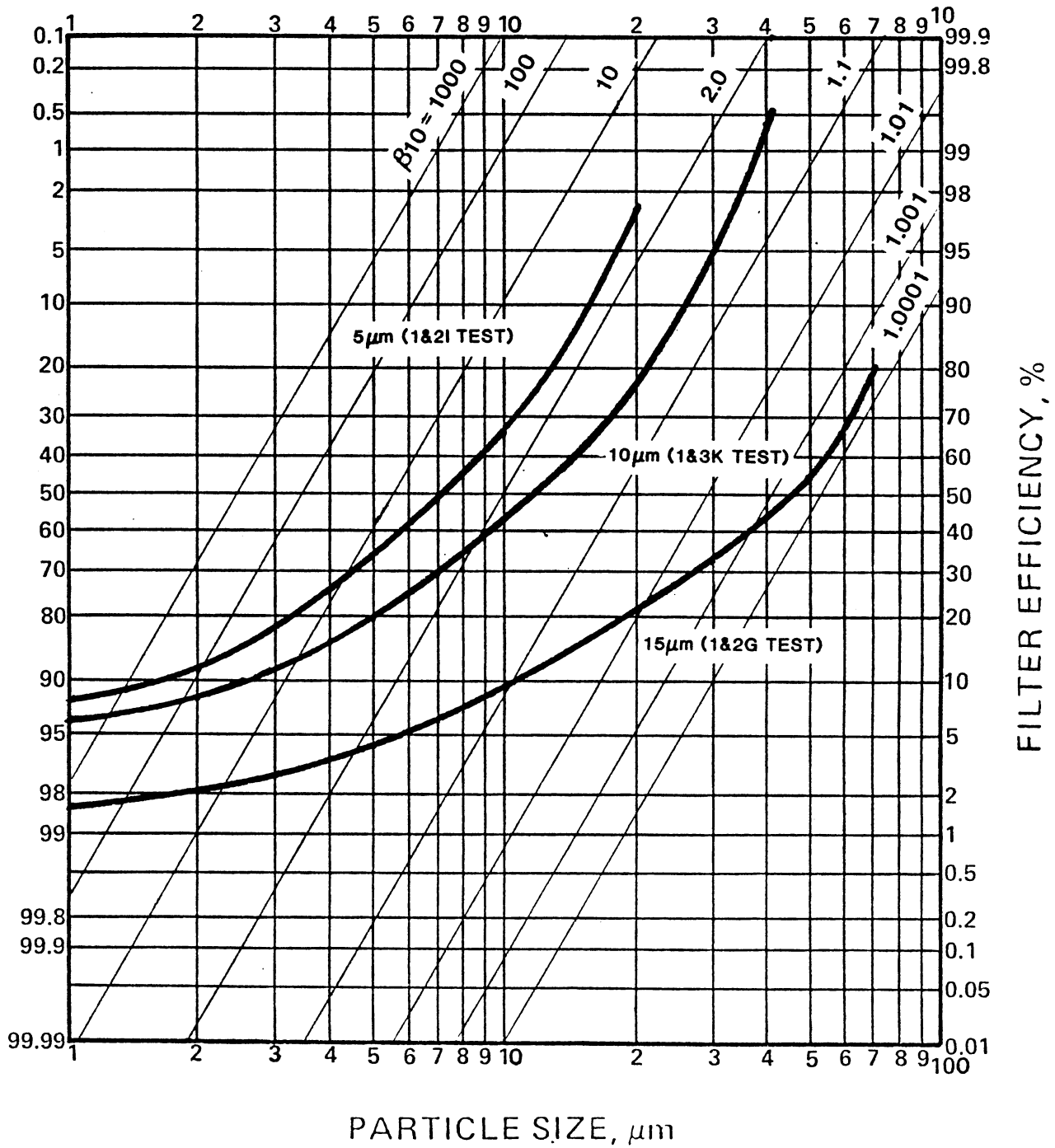


Figure 48. Piston-Bore Assembly Filtration Efficiency (6.38mm Land Length).

equation of X_e for the piston-bore assemblies needs to be changed to express nonlinearity.

The significance of this nonlinearity found among the piston-bore assemblies' filter efficiency is argued in the following. If there are two straight lines in the filter efficiency graph as shown in Fig. 49a, the separation efficiency at each particle size versus the logarithm of particle size displays two corresponding normal distributions (Fig. 49b). When the slope is steep, the separation efficiency shows narrow band normal distribution (the small standard deviation), and when the slope is moderate, the normal distribution has the large standard deviation. However, when the filter efficiency curve is nonlinear, such as Fig. 49c, the resulting separation efficiency is as illustrated in Fig. 49d. This indicates that over a period of time, the filtration efficiency progressively improved, and the assembly became capable of filtering finer particles. Figure 48 shows the progressive improvement by demonstrating the time average of the assembly filtration efficiency. This progressive improvement in filtration efficiency is observed among hydraulic filters and is called "caking."

The cake formation was previously analyzed based upon the leakage experiment, and here is further evidence that supports the presence of caking. As the cake formation builds up in the clearance of a piston-bore assembly, finer particles start silting in the tortuous path of the cake formation. As a result, the mean separation efficiency shifts to a smaller size. The separation efficiency curve of Fig. 48 is shown in Fig. 50 and clearly demonstrates the gradual slope of curves at a smaller

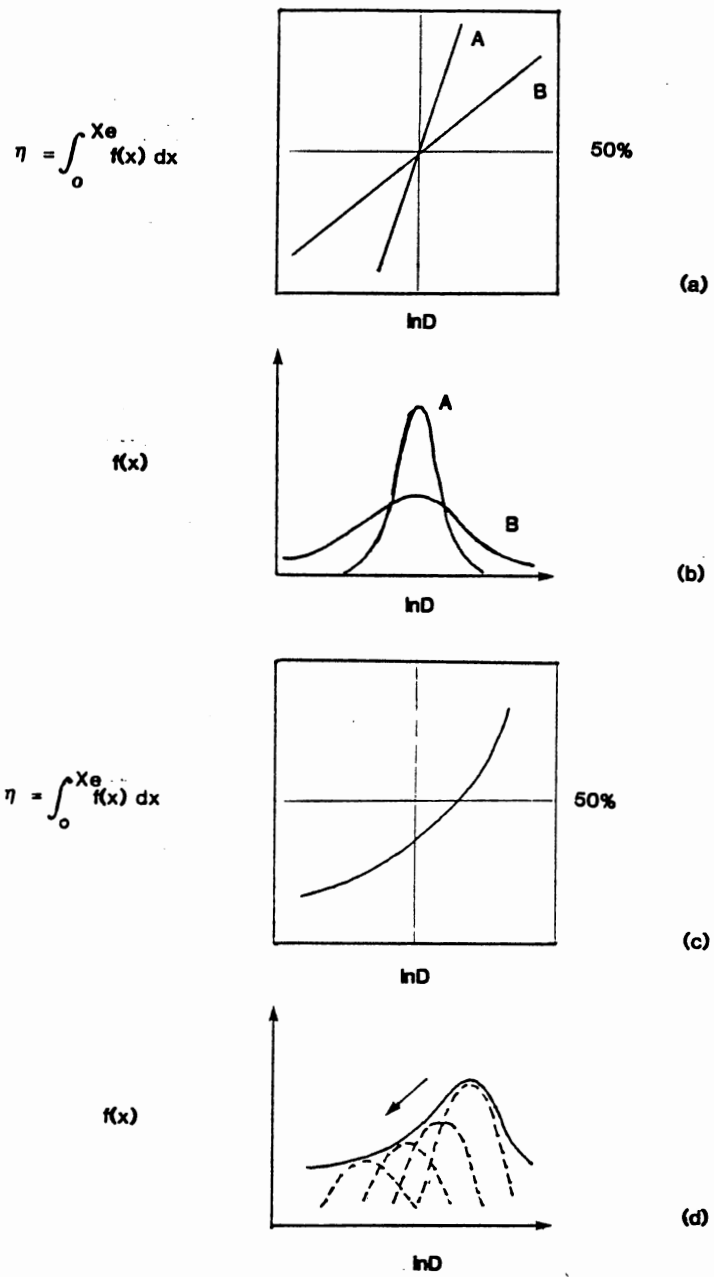


Figure 49. Analysis of Cake Formation.

particle size range than the mean size, and the steep slope of the curve at a larger particle size range than the mean size.

Furthermore, Fig. 48 shows that the particle size at which 50% filter efficiency of a piston-bore assembly locates is slightly bigger than the nominal clearance size of the assembly. For the case of 15 micrometers nominal clearance, the main filtration efficiency occurs at quite a larger size than 15 micrometers. This could be explained by the fact that as the clearance increases, the initial leakage flow and shear rate increase enough to prevent fine particles from silting in the clearance. Therefore, the overall filtration efficiency degrades.

The effect of land length on the assembly filtration efficiency was investigated. Half land length (3.19mm) tests are presented in Fig. 51 and 52. Figure 51 shows the filtration ratio versus particle size, and Fig. 52 shows filter efficiency versus particle size. The comparison between Fig. 48 and 52 exhibits that the assembly with 6.38mm land length has a higher filtration efficiency than the one with 3.19mm land length when both assemblies have the same clearance size.

Evaluation of the Simulation Program for the Silt Process Model

Though silt Beta values are now known (Fig. 47 and 52), these figures show the time average silt Beta over a period of time T . The silt Beta values at the beginning of the silt process (when solid particles are introduced) is slower than at the end of the silt process

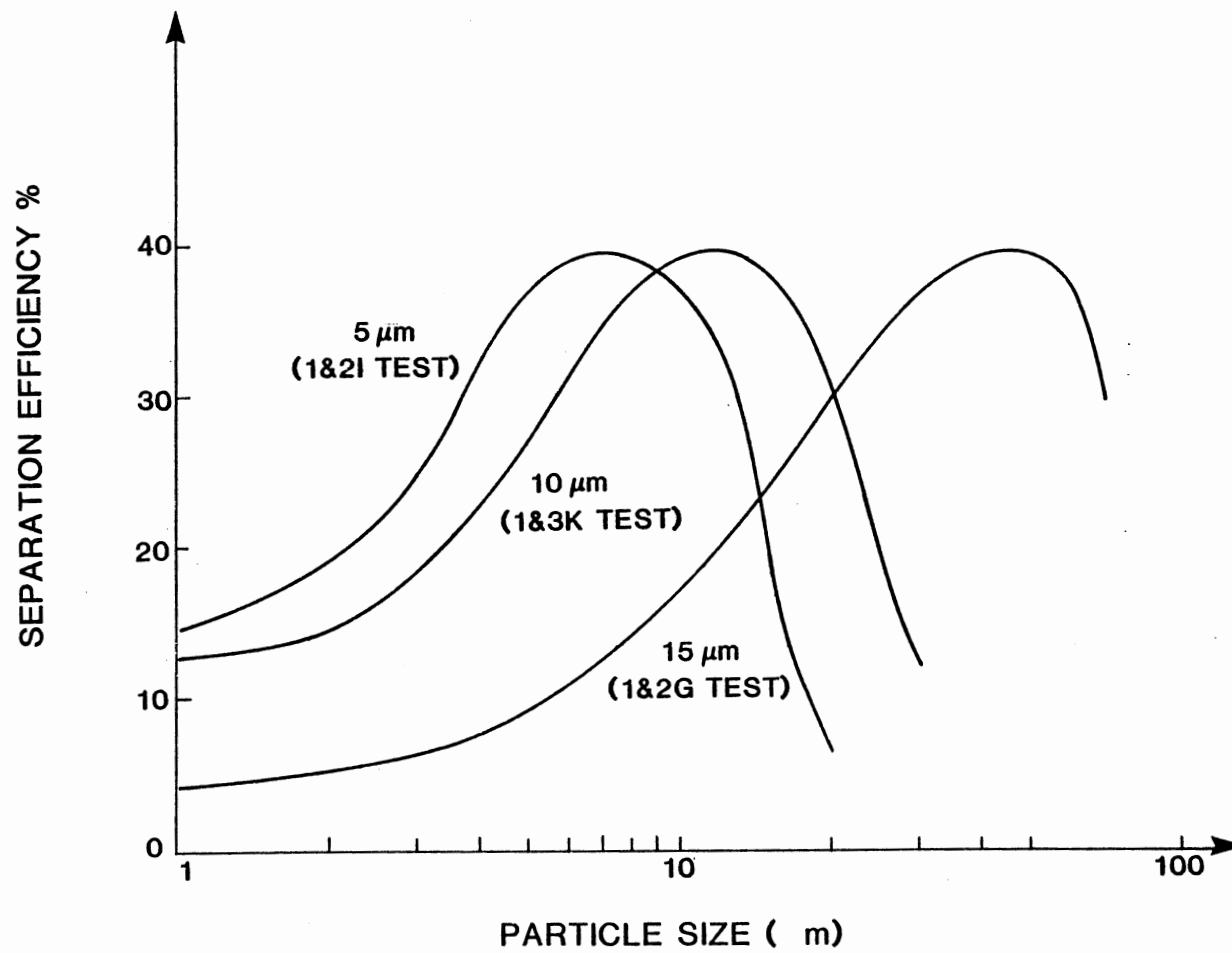


Figure 50. Piston-Bore Assembly Separation Efficiency.

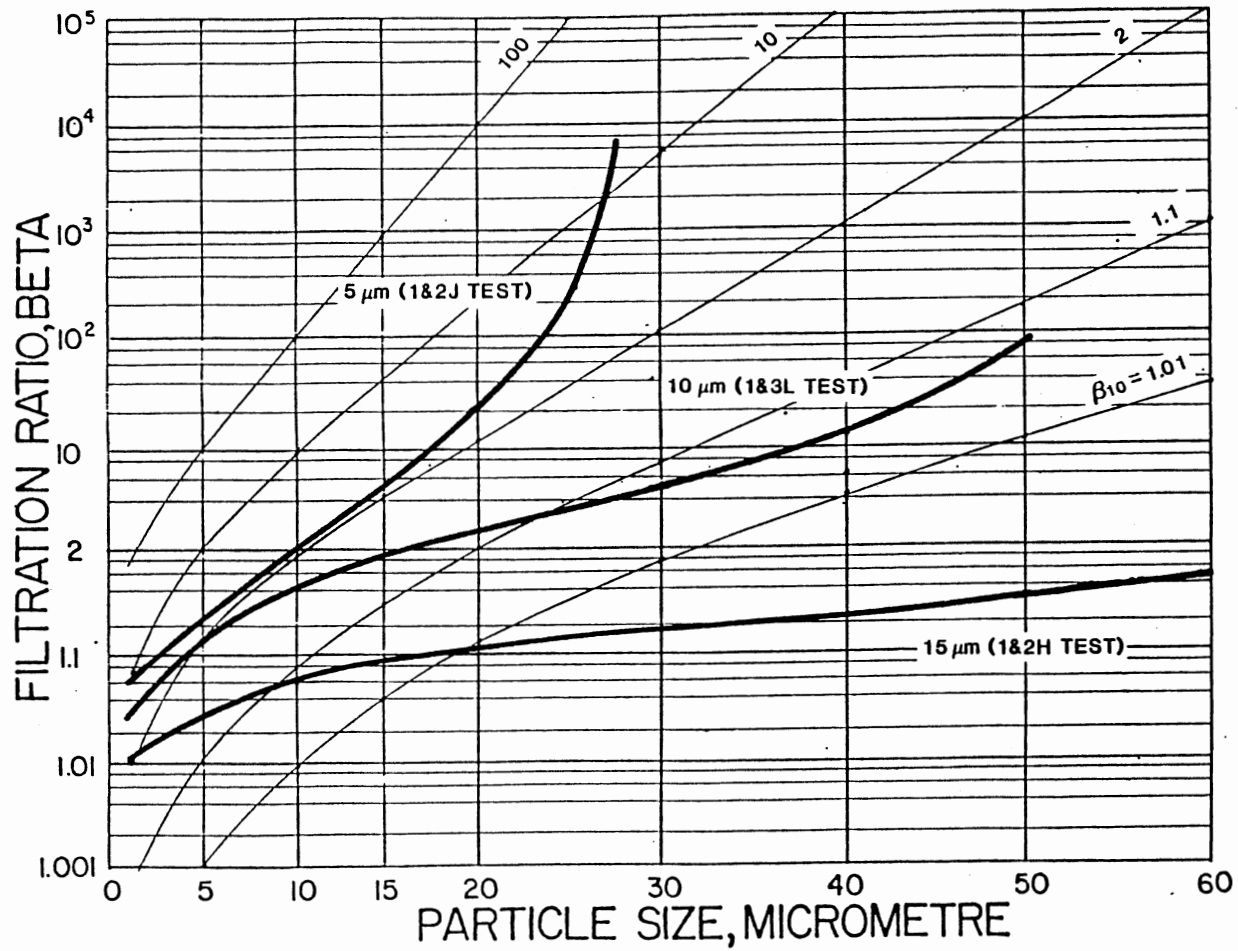


Figure 51. Piston-Bore Assembly Silt Beta (3.19mm Land Length).

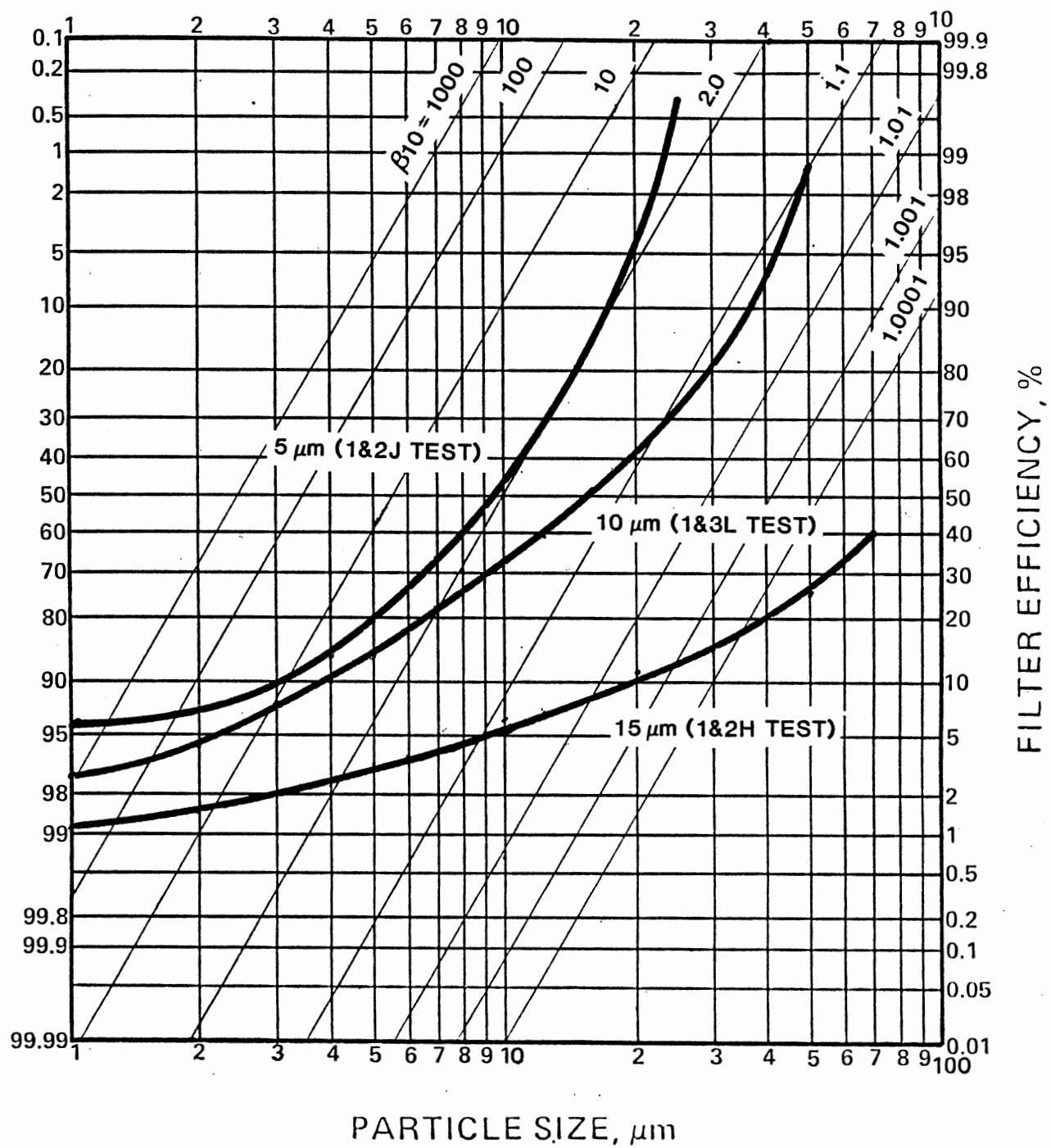


Figure 52. Piston-Bore Assembly Filtration Efficiency (3.19mm Land Length).

(when the leakage diminishes). Thus, the average silt Beta is represented by:

$$\bar{\beta}_s = \left(\int_0^T \beta \, dt \right) / T \quad (79)$$

Equation 79 can also be shown as:

$$\bar{\beta}_s = Nu / \bar{Nd} \quad (80)$$

where the upstream particle size distribution is not a function of time. It is a constant over a test period. Since we know Nu and Nd, the time average of the particle frequency distribution upstream $f(D)_u$ and downstream $f(D)_d$ can be calculated from Eq. 9. Thus, the particle frequency distribution of particles silted in the clearance of a piston-bore assembly is:

$$\overline{f(D)}_t = \overline{f(D)}_u - \overline{f(D)}_d \quad (81)$$

However, the unit associated with each term in Eq. 81 is the number of particles at size D per milliliter of the leakage. Hence, the total leakage volume has to be known to identify the particle frequency distribution after a test of duration T and is defined mathematically by:

$$F(D)_t = \overline{f(D)}_t \int_0^T Q \, dt \quad (82)$$

or

$$F(D)_t = \overline{f(D)}_t \text{Vol} \quad (83)$$

where

$$\text{Vol} = \int_0^T Q \, dt \quad (84)$$

In a similar fashion, Eq. 8 becomes:

$$\overline{v_t} = v_u - \overline{v_d} \quad (85)$$

where

$\overline{v_d}$ = the time average volume of the downstream particle size distribution per unit leakage volume.

$\overline{v_t}$ = the time average volume of the particles in the piston-bore clearance.

Thus, the total silt particle volume is:

$$s = \int_0^T \overline{v_t} Q(t) dt \quad (86)$$

Substituting Eq. 84, this becomes:

$$s = \overline{v_t} vol \quad (87)$$

Both terms on the right side of Eq. 87 can be experimentally measured to identify the silt volume S; however, the way this silt volume blocks the leakage flow through the clearance must be investigated. To do so, the silt models shown in Fig. 47 and Fig. 52 are implemented in the simulation program. For a piston-bore assembly that has a clearance size other than 5, 10, or 15 micrometers, and a land length other than 6.38mm and 3.19mm, the program has also been implemented to linearly interpolate and/or extrapolate (according to the requested range of silt Beta values) from data shown in Fig. 47 and Fig. 52.

The experimental results shown in Fig. 33 are used to investigate the performance of the simulation program. In Figure 53, the experimental results are compared with the simulation results. The curve marked $A = 1$ is the simulation result. The simulation program predicts far more leakage volume than is observed experimentally. This indicates that the silt particles in the clearance are piling up in such a way that the leakage flow through the clearance is reduced more than is predicted by the silt model process. To better define the effectiveness of this leakage flow reduction, Eq. 87 may be modified to have a constant multiplier, A :

$$s = \overline{v}t \text{ Vol } A \quad (88)$$

A was varied, as Fig. 53 shows, to define the effective particle reduction of the leakage flow. When the value of A is 40, the simulated leakage volume approaches the experimental results at short times.

The discrepancy between the silt process model and the experimental data is illustrated in Fig. 54. The silt process model hypothesizes that the reduction of the leakage flow can be calculated by uniformly decreasing the clearance size (thus decreasing the clearance space) according to the volume of particles silted in the clearance (Fig. 54a). However, if the theory is correct, the experimental results should show 40 times more silt volume than what is actually measured. This experimental result indicates that the silt volume does not uniformly spread and decrease the clearance size, but instead, tends to agglomerate

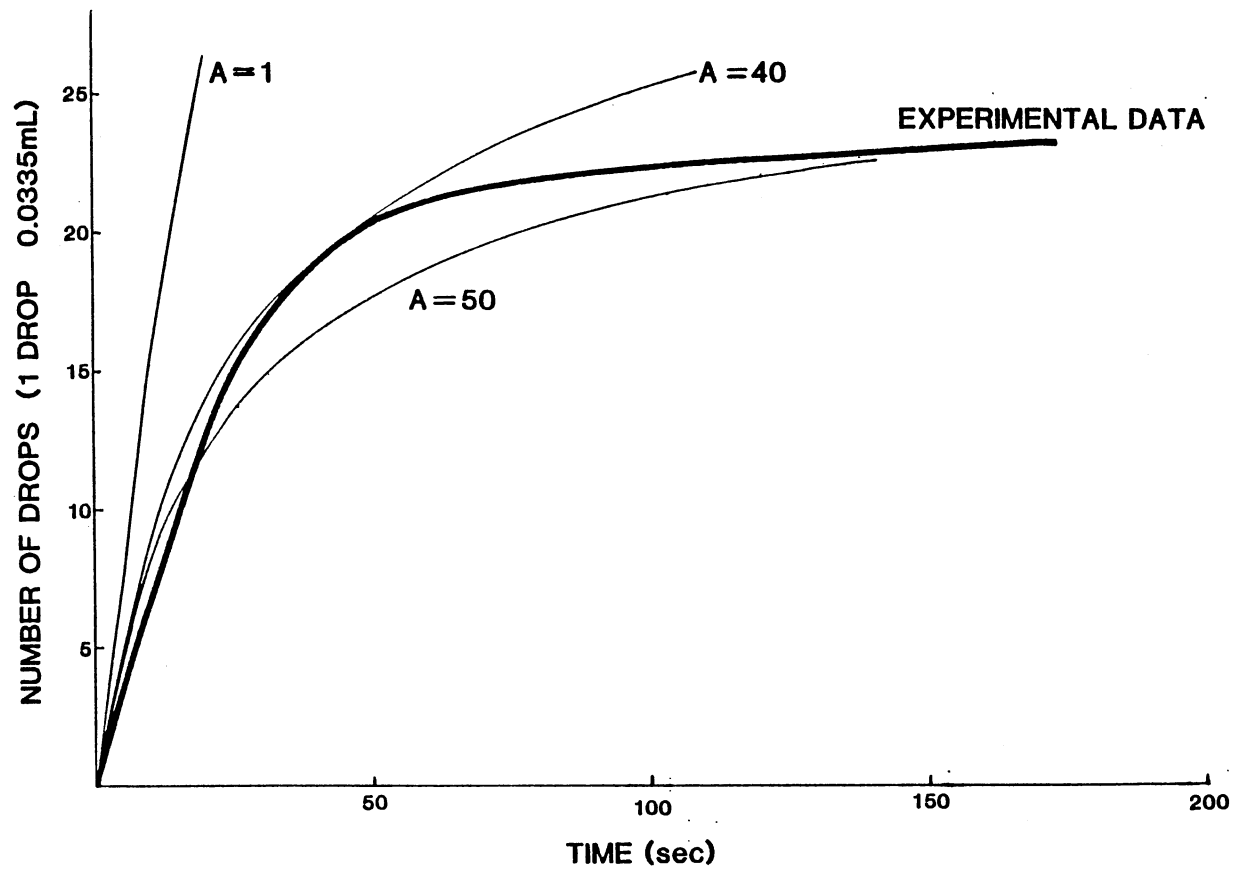


Figure 53. Constant Multiplier Analysis.

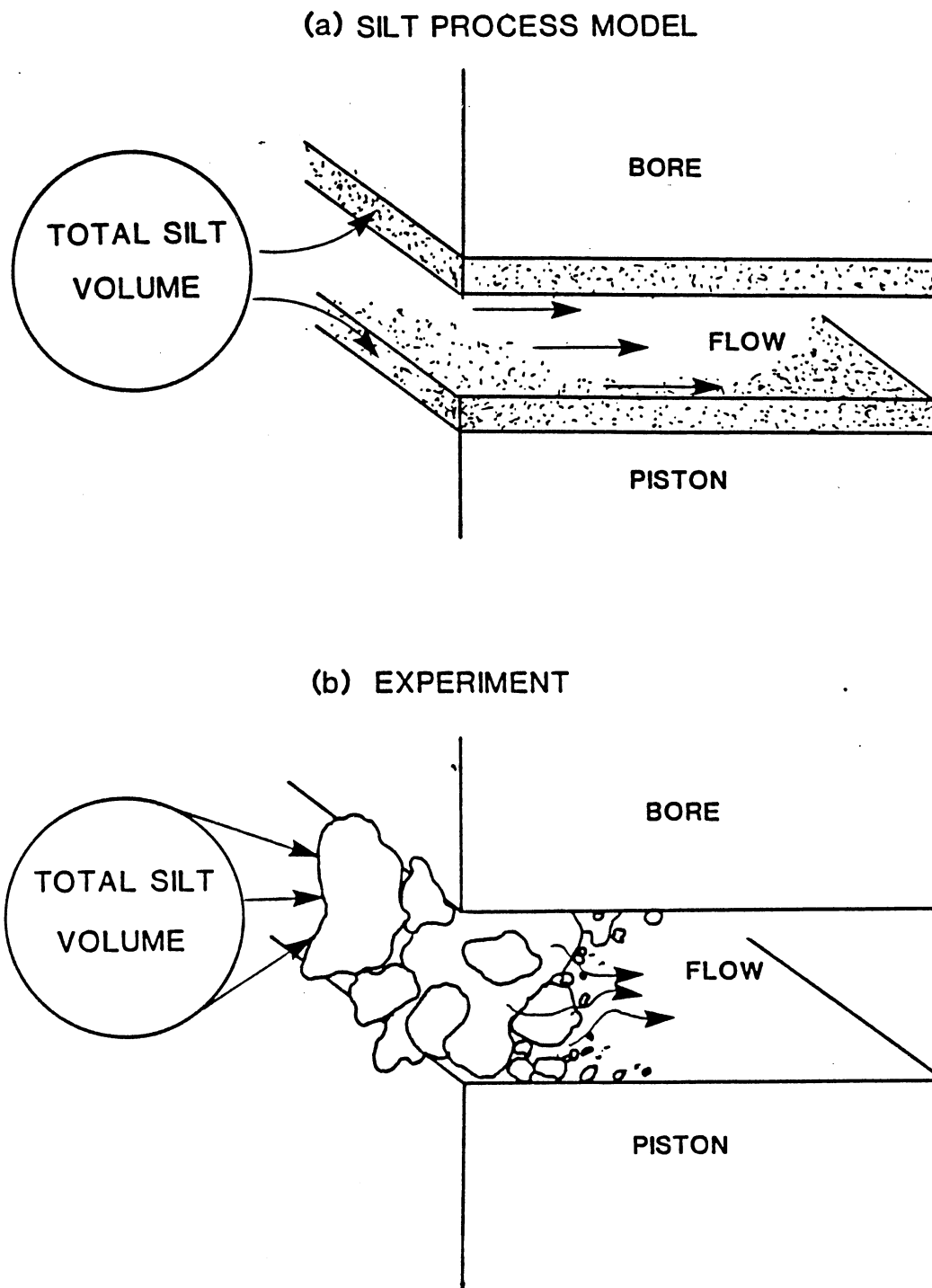


Figure 54. Silt Pattern (Theory and Practice).

somewhere in the clearance and effectively decrease the leakage.

Further analysis was performed to investigate the discrepancy. The rate of silt volume accumulation in the clearance, for the case of Fig. 33, was found to be 1.409×10^7 cubic micrometers per milliliter of the leakage volume passing through the clearance of the piston-bore assembly. From Fig. 33, there are no more than 24 drops for the piston-bore assembly under the specified test condition in the same figure. Therefore, the total leakage volume is no more than 0.804 milliliter (24 drops \times 0.0335 ml/drop). The total silt volume accumulated in the clearance is then calculated by:

$$(1.409 \times 10^7 \mu\text{m}^3/\text{mL of leakage}) \times (0.804 \text{ mL of leakage}) = 1.133 \times 10^7 \mu\text{m}^3 \quad (89)$$

The total space available in the clearance of the piston-bore is calculated by:

$$V_{c1} = \pi L h (D - h) \quad (90)$$

where

$L = 6.38\text{mm}$; land length

$h = 6 \mu\text{m}$; clearance size

$D = 6.351\text{mm}$; inner diameter of the bore

and is 7.63×10^{10} cubic micrometers. Thus, while the silt volume (Eq. 89) found from the experiments only amounts to 1.79 % of the clearance space available, the silt particles block the leakage with a calculated

efficiency corresponding to a summed volume of 60 to 80 percent of the clearance space occupied. Clearly, the model needs refinement. One explanation for this discrepancy is that the silt particles are locally concentrated in the clearance space and effectively increase resistance to the leakage flow through the clearance. Moreover, this packing takes place preferentially at the entrance to the clearance of the piston-bore assembly, as Fig. 54b shows. Results obtained by Kamiyo [8] and Laurenson [9] support this contention.

To reconcile this discrepancy between the theory and the experimental results, the variation of the A value in Eq. 88 was investigated for different geometrical configurations of piston-bore assemblies. If A varies according to some non-dimensional parameters associated with the leakage flow through the clearance, then the use of the constant multiplier A in Eq. 88 is a valid approach for reconciling the discrepancy.

Table VI summarizes the result of finding A values, along with other information, for various assemblies. This table reveals several important facts. For instance, it was found that the larger the clearance, the larger the leakage and the total silt volume in the clearance. Furthermore, among piston-bore assemblies with the same clearance size, those with a land length of 3.19mm have a higher total silt volume in the clearance than those with a land length of 6.38mm. The piston-bore assemblies with a 3.19mm land length are less efficient in filtering particles than the assemblies with a 6.38mm land length (compare Fig. 47 and 51); however, by the end of the filtering process,

TABLE VI
SILT VOLUME ANALYSIS

CLEARANCE SIZE μm	SPOOL NO.	ACFTD CONCEN- TRATION mg/L	PRESSURE DIFFERENCE psi	LAND LENGTH mm	SILT VOL. / LEAKAGE $\mu\text{m}^3/\text{mL}$	AVERAGE LEAKAGE mL	TOTAL SILT VOLUME μm^3	% OF SILT VOLUME PER CLEARANCE SPACE	VALUE OF 'A'
6	19	25	1000	6.38	1.409E07	0.804	1.133E07	1.48	50
5	20	25	1000	3.19	1.354E07	1.325	1.794E07	5.64	11-12
9.5	23	25	1000	6.38	1.236E07	1.918	2.371E07	1.96	39-40
9.5	23	25	1000	3.19	1.075E07	2.43	2.612E07	2.163	17-18
14.5	25	25	1000	6.38	5.939E06	14.1	8.373E07	4.547	14-15
14.5	25	25	1000	3.19	3.583E06	13.49	4.833E07	5.249	14-15

the assemblies with a 3.19mm land length retain more particles in the clearance because these assemblies allow a larger amount of total leakage volume to pass through the clearance.

When the value of A (in logarithmic scale) is plotted against the average shear rate at the wall of the assembly clearance (in logarithmic scale), there seems to be a linear relation between the A values and the shear rates (Fig. 55). The linear regression of A versus shear rate is:

$$A = 2710381 (\text{Shear Rate})^{-0.8547663} \quad (91)$$

The correlation coefficient of the above equation is 0.81. Thus, Equation 91 may be incorporated into the simulation program to account for the discrepancy between the experimental data and the silt process model.

For a given piston-bore assembly, only the pressure across the clearance of the assembly and the fluid viscosity determine the shear rate. At a constant temperature of fluid, it can be assumed that the fluid viscosity does not vary significantly. Since Dexron II is maintained at a constant temperature throughout the experiment, while the leakage flowing through the clearance is laminar flow, the pressure across the clearance becomes the only parameter that determines the shear rate of the assembly. Thus, the higher the pressure, the higher the shear rate. However, the constant multiplier A decreases as the pressure across the clearance increases. At high pressure, there exists a high leakage flow, and the rate of the silt volume accumulation in the

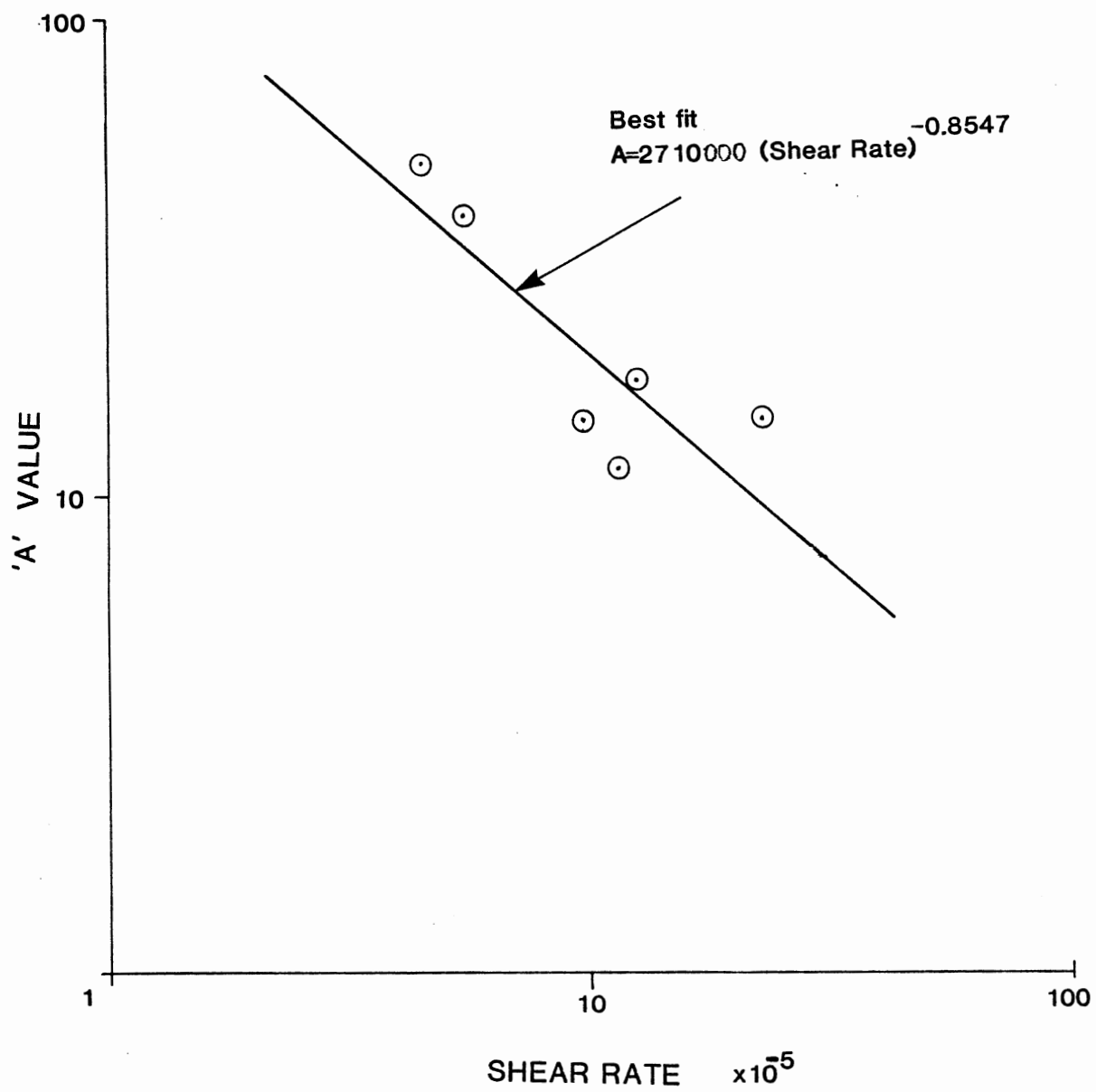


Figure 55. 'A' Value Versus Shear Rate.

clearance is high. This silt volume, however, does not block the leakage as effectively as the silt volume accumulating under a lower shear rate. When the fluid is first introduced into the clearance (at the beginning of the silting process), the average shear rate at the wall of the clearance is high. The leakage flow has the ability to transport particles finer than the clearance size deep into the clearance and even through the clearance. Consequently, silt particles are spreading and their build up is thin, thus causing the A values to decrease.

CHAPTER V
VERIFICATION OF PARTICULATE-INDUCED
SEIZURE MODEL

Experimental Considerations

A review of past research [11, 12, & 25] reveals that the motion of the mechanism to measure the force required to break seizure must be well controlled so that each motion of the mechanism is repeatable and consistent.

For example, in contaminant diagnostic monitor research [25] seizure force has been used as a method to evaluate the contamination level of hydraulic systems (Fig. 56). The monitor used employed a weight system to actuate the tapered piston (the spool in the figure) in the bore housing as shown in Fig. 57. However, this actuation system had the following problems:

1. The correct weight to use for a given test condition was difficult to calculate in advance.
2. No actuator motion control was available.
3. The time allowed for the silt process to take place was imprecise because of a lack of automation.

The lack of an actuator motion control was a particularly serious

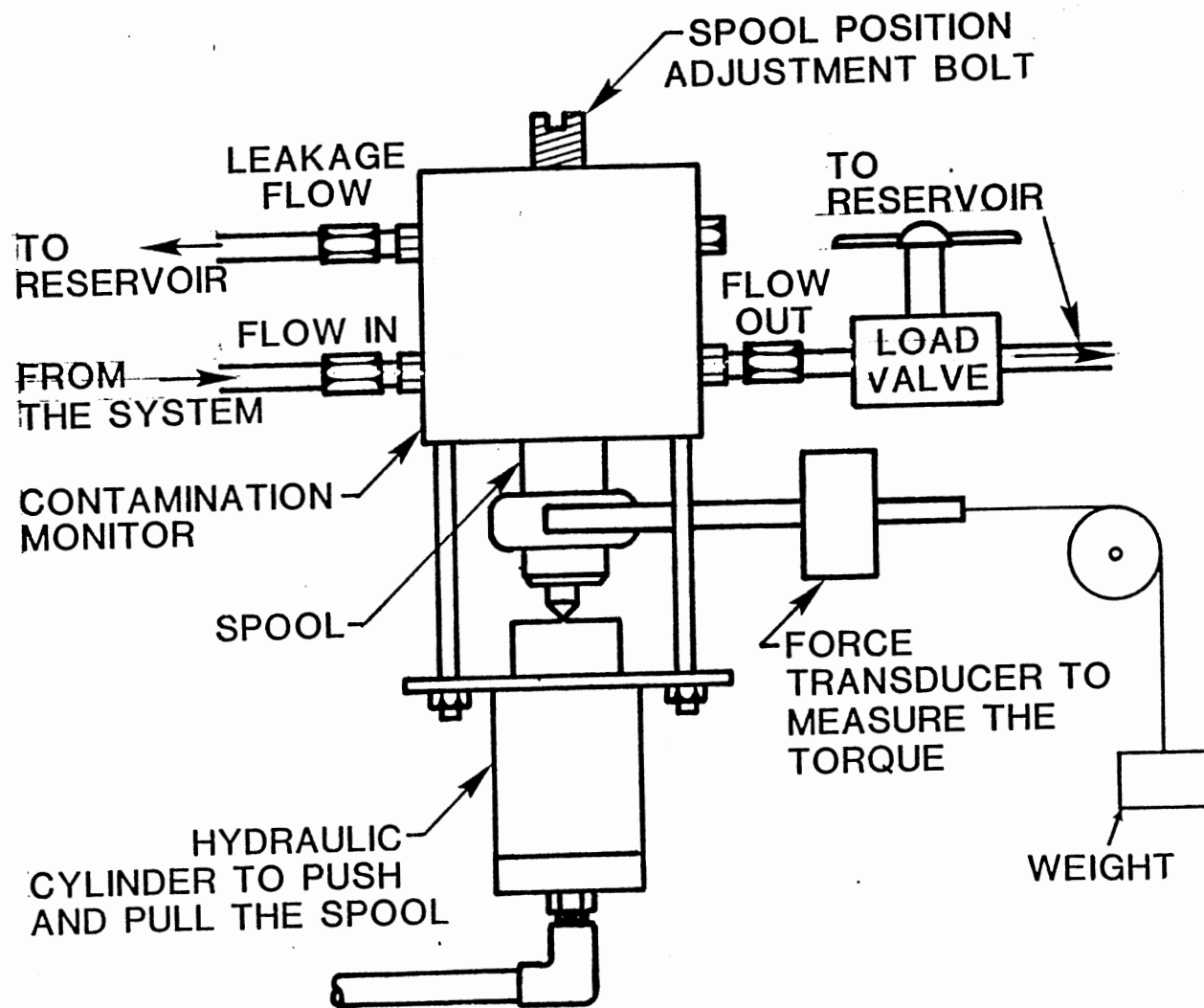


Figure 56. DOE Test Valve and System Set Up.

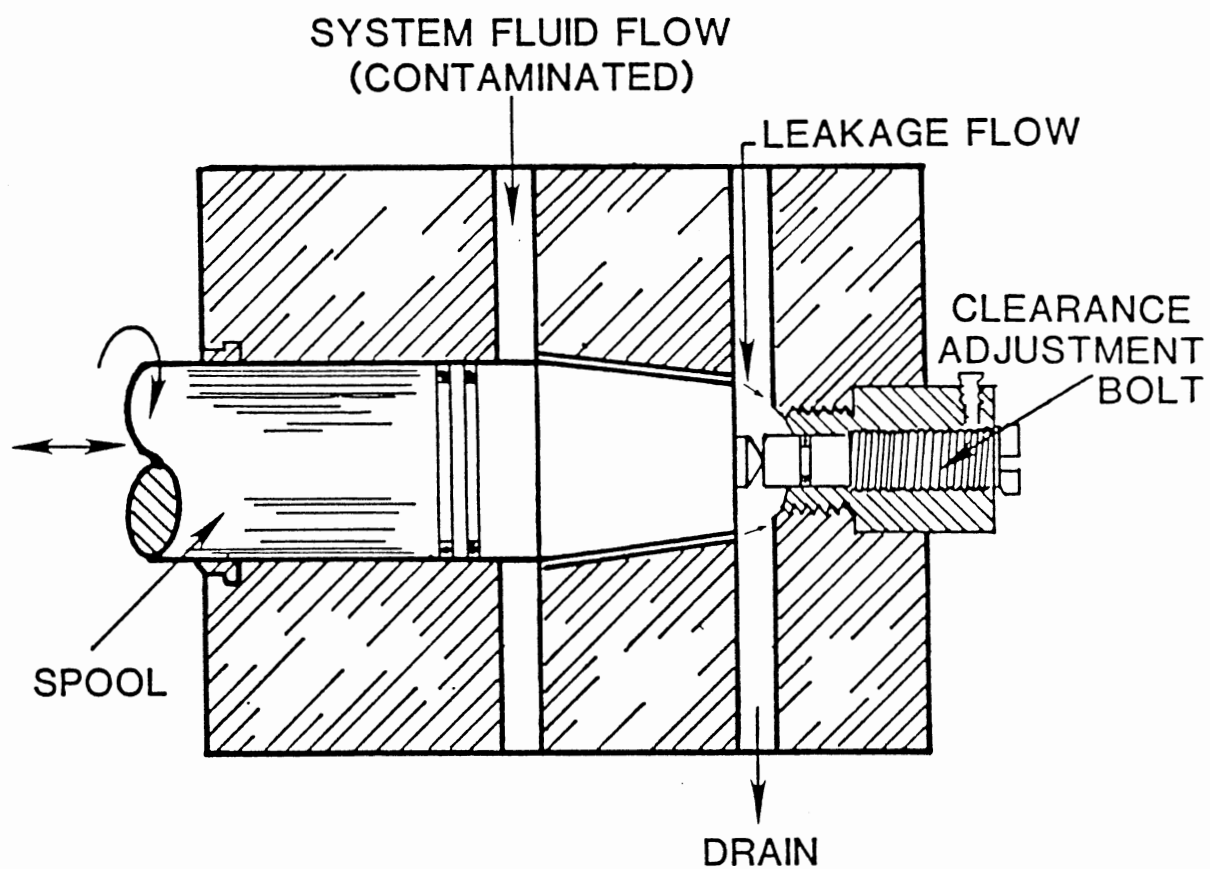


Figure 57. DOE Test Valve.

shortcoming. When the angular velocity of the spool rotation changed, the viscous drag changed. Ideally, the spool rotational motion was maintained constant throughout the test; however, when ACFTD was injected, particles entrained in the clearance impeded the rotational motion of the spool. Sometimes, a given weight could not overcome the seizure force generated by particles, and the spool rotation stopped in the middle of the process. In short, the rotational motion was impeded in an uncontrolled manner.

An improved actuator and motion controller for the actuator is definitely needed to verify the particulate-induced seizure model.

Development of Experimental Facility-Hardware

Mechanical hardware was designed (Fig. 58) and built to achieve this precise motion control. The rotational motion of the rotor at the top of the whole assembly was converted into linear motion through linkages and spheric joints. The force sensor was placed between the two linear bearing systems. The position sensor was attached to the linkage above the force transducer so that the position sensor would not affect the force measurement. A coupling was provided between the linkage and the actuation rod to ease possible misalignments. A hydraulic motor and hydraulic servovalves were chosen to drive the rotor because of their high frequency response and wide range of controllable speed. In addition, this electrohydraulic servo system could generate more power than an electrical motor of equivalent physical size. An additional

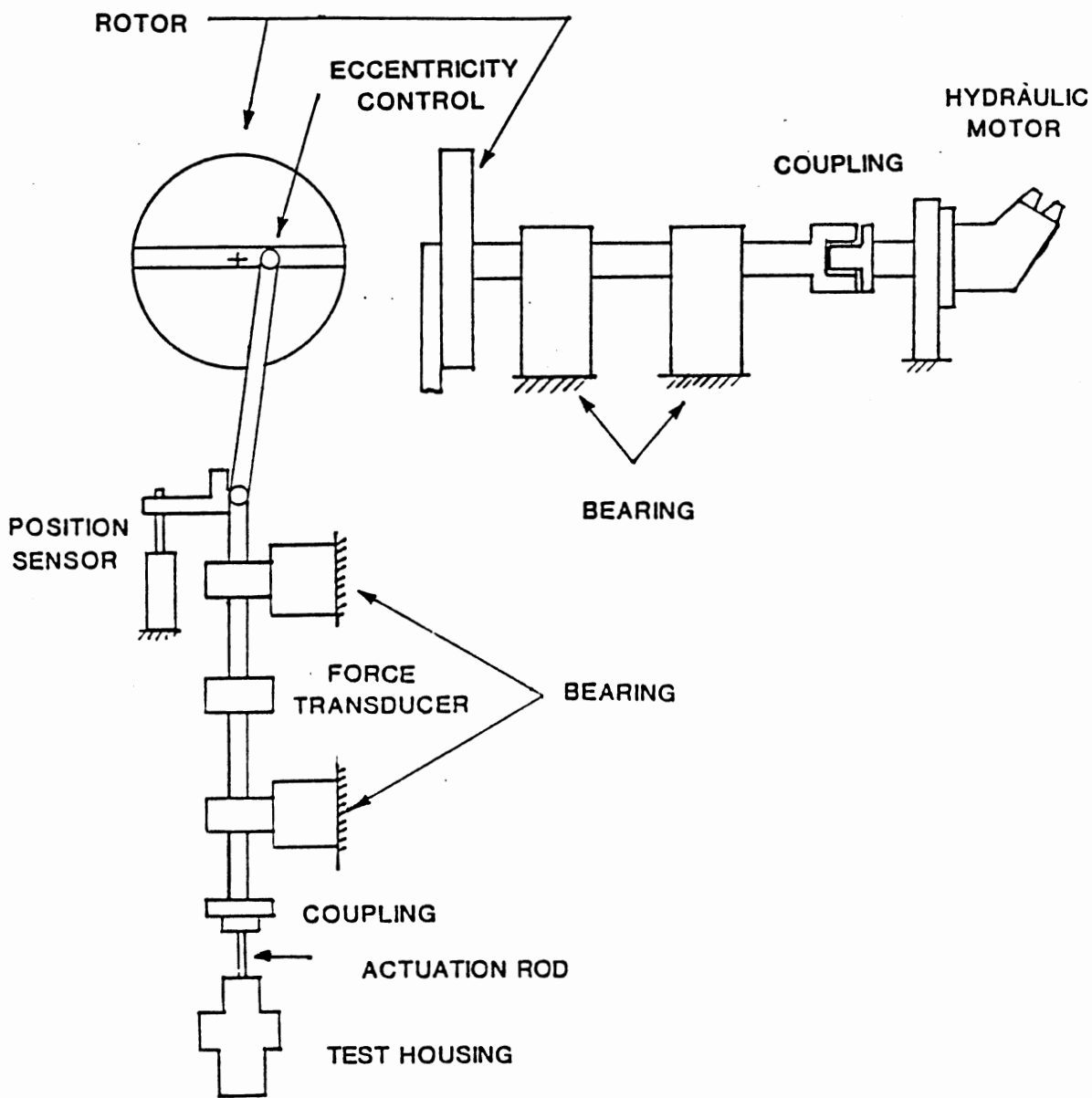


Figure 58. Actuation System.

power unit for this electrohydraulic servo system was built to supply constant pressure to the hydraulic servovalve.

Electronics hardware was either purchased or developed to achieve the desired motion control of the actuation system. A microcomputer system was developed to control the mechanics. This low level system was also designed to communicate with other computer systems (Fig. 59). The machine interface microcomputer consists of six major functions: main processor, communication, memory, on/off input and output, D/A, and A/D. The heart of this device is the control function designed around the Intel 80188 processor. The IEEE 488 card enables the machine interface to transfer information to and from a personal computer (Tandy 2000) at the speed of 500k bytes per second. The combination of a 12 bits D/A (digital to analog converter) and a power operational amplifier drives the hydraulic servovalve. The output of the position sensor from the servovalve was fed directly into a 12 bits A/D (analog to digital converter); however, the output of the force transducer was fed through the signal conditioning units to achieve noise suppressed signal amplification. The schematic diagram of this unit is shown in Fig. 60. The signal conditioning unit was fully equipped with noise rejection capability, a low pass filter, and laser trimmed gain accuracy. The I/O unit and opto-electronic unit turn on and off the 120 volts solenoid valve placed downstream of the test housing.

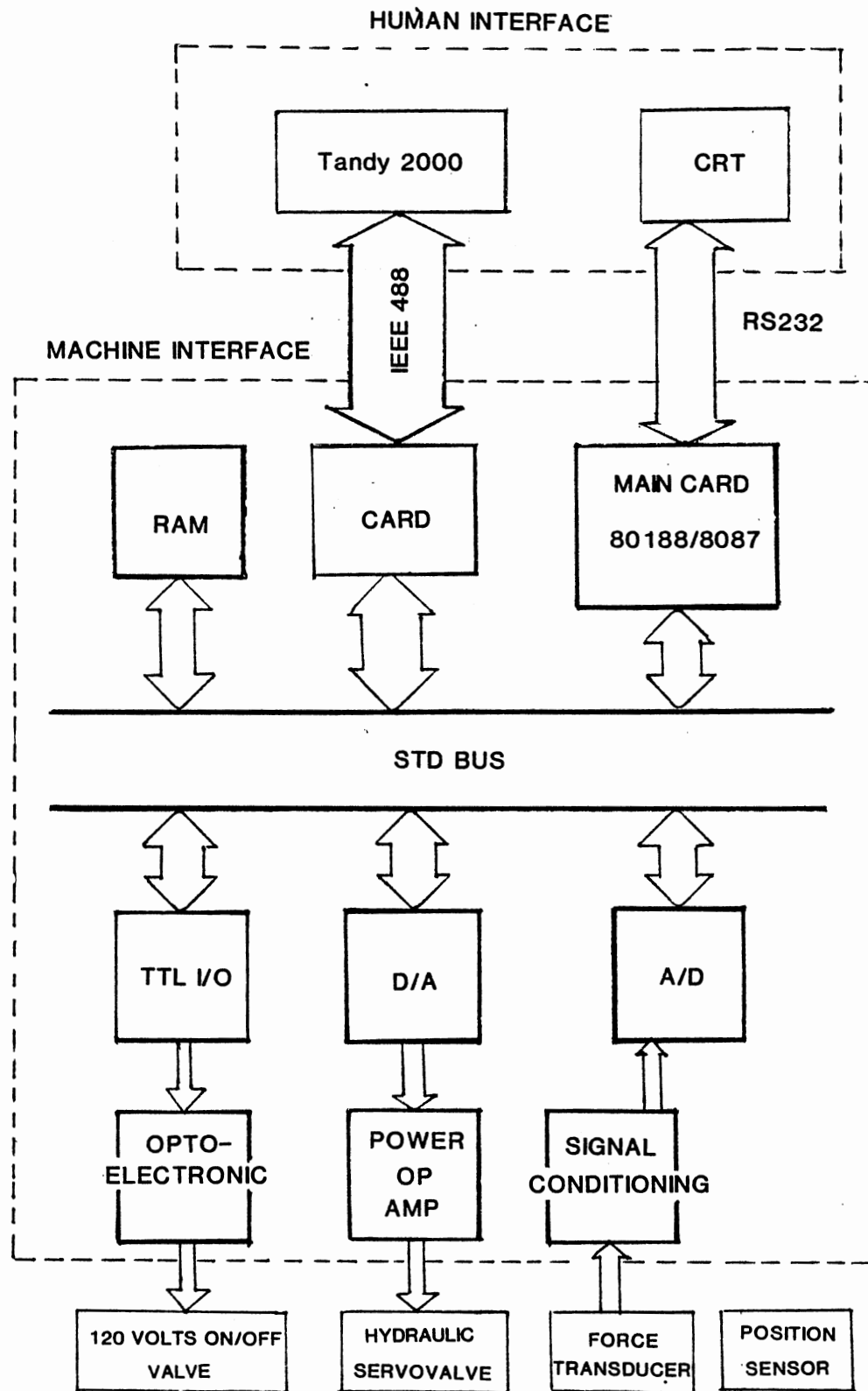


Figure 59. Microcomputer System Hardware.

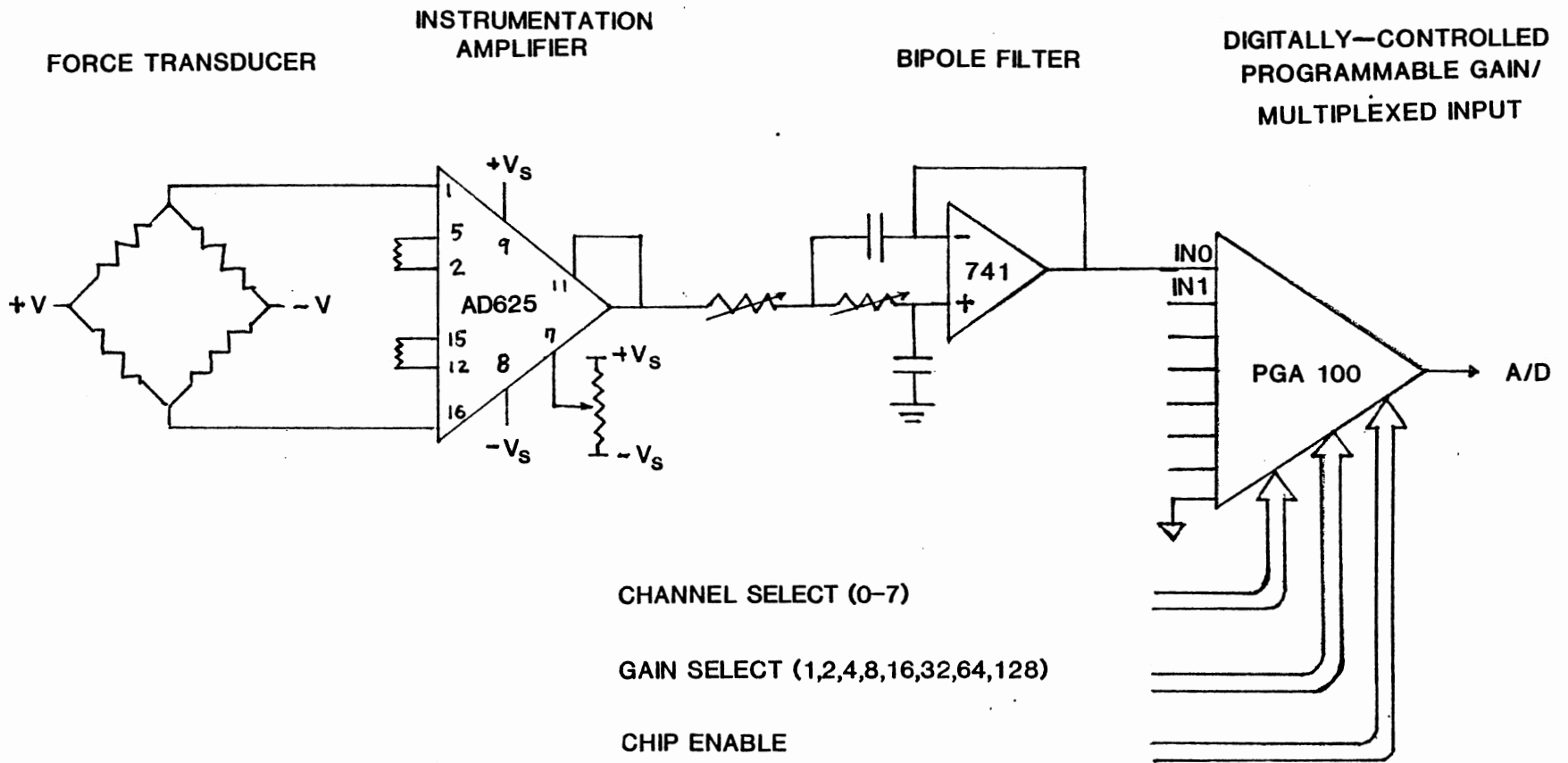


Figure 60. Signal Conditioning Unit.

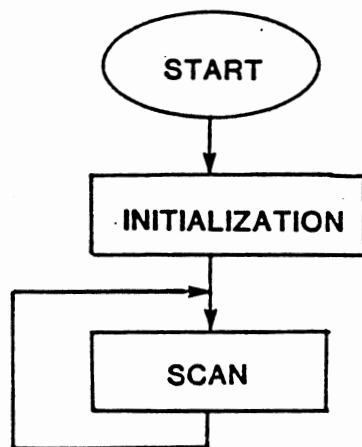
Development of Experimental Facility-Software

The hardware part of the system therefore consisted of a test bed, a low level computer, and a high level computer. Software was written to effect a smooth interface between these independent units. Critical to the success of this software was careful attention to the operational priorities of each unit. The communication between the two computers was initiated only upon request by the master (high level) computer. The details of the low level operation of the test bed were looked after entirely by the slave computer. Because of the need for high speed and precise timing of the various operations, the slave computer was designed and built with a minimal number of allowable interrupts.

The main task of the slave computer is the tight loop of scanning the request from the master computer (Fig. 61). Then, the scanning routine first finds whether the slave computer is to listen to what the master computer talks, or to talk to the master computer. The master must become the talker and the slave the listener when the communication is initiated; then, only when the master computer requests the slave computer to talk, the slave computer talks. The scan routine algorithm shown in Fig. 61 achieves this listener-talker alternation.

When the slave computer listens to the master computer, the master computer gives a series of instructions and information to achieve the desired task. Therefore, these instructions must be decoded (and executed if so required) immediately. While the master and slave computer communicate, both computers are executing their task at a much

MAIN ROUTINE



SCAN

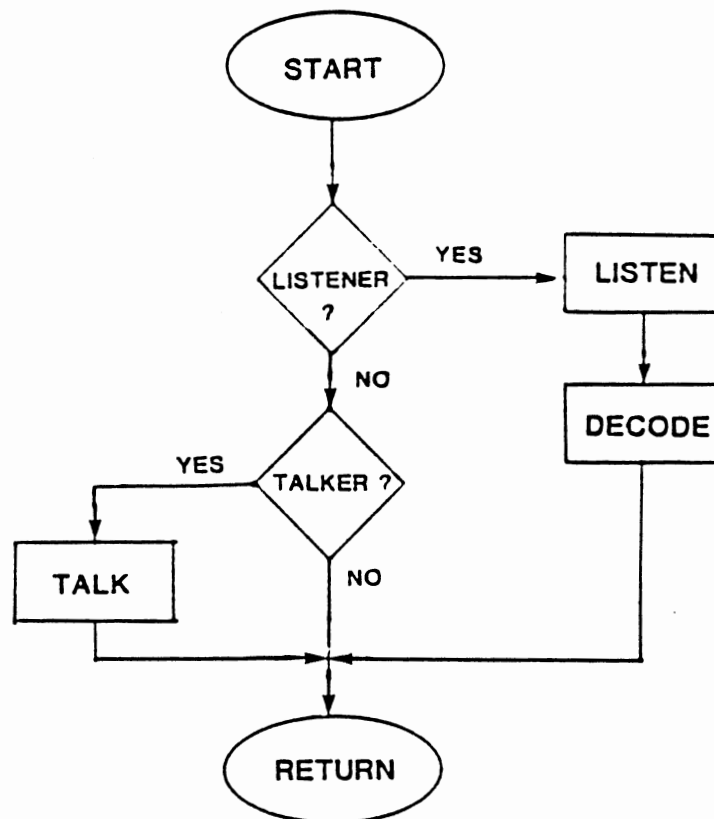


Figure 61. Algorithm of Slave Computer.

reduced speed because the response time of the communication hardware between computers is slow compared to the speed of the computers themselves. To minimize this delay the instruction set was written in as compact a manner as feasible.

Figure 62 illustrates the approach used with the slave computer for this experiment. The first byte received determines the type of operation. As the example in the figure shows, if this byte is 00H (zero-zero in hexadecimal), then the task is A/D conversion. The information of the channel number and the required number of conversion then follows as Fig. 62 shows. This way the master computer can access as many as 256 channels and trigger as many as 65536 A/D conversions by sending a mere four bytes of instructions to the slave computer.

A total of eight levels of task selections were implemented in the slave computer (Fig. 63), and the source code for this software is presented in Appendix C. The software shown in Appendix C was first developed on a Tandy 2000 (the master computer) and subsequently downloaded through an RS 232C serial port to the slave computer. The file downloading program was written in a combination of C language and Assembly. This program used the BIOS (basic input and output service routine) interrupt 14H (fourteen in hexadecimal) to drive the RS 232C of the Tandy 2000 and 16H to control the keyboard buffer. The software for the communications between the Tandy 2000 and the slave computer is presented in Appendix D.

TASK SELECTION SUPPLEMENTALY INFORMATION

--	--	--	--	--

1st byte

2nd

3rd

4th

EXAMPLE OF A/D INSTRUCTIONS

00H A/D con- version	A/D channel number	LOWER BYTE	HIGHER BYTE
----------------------------	--------------------------	---------------	----------------



 TOTAL NUMBER
 OF CONVERSION

Figure 62. String of Instructions.

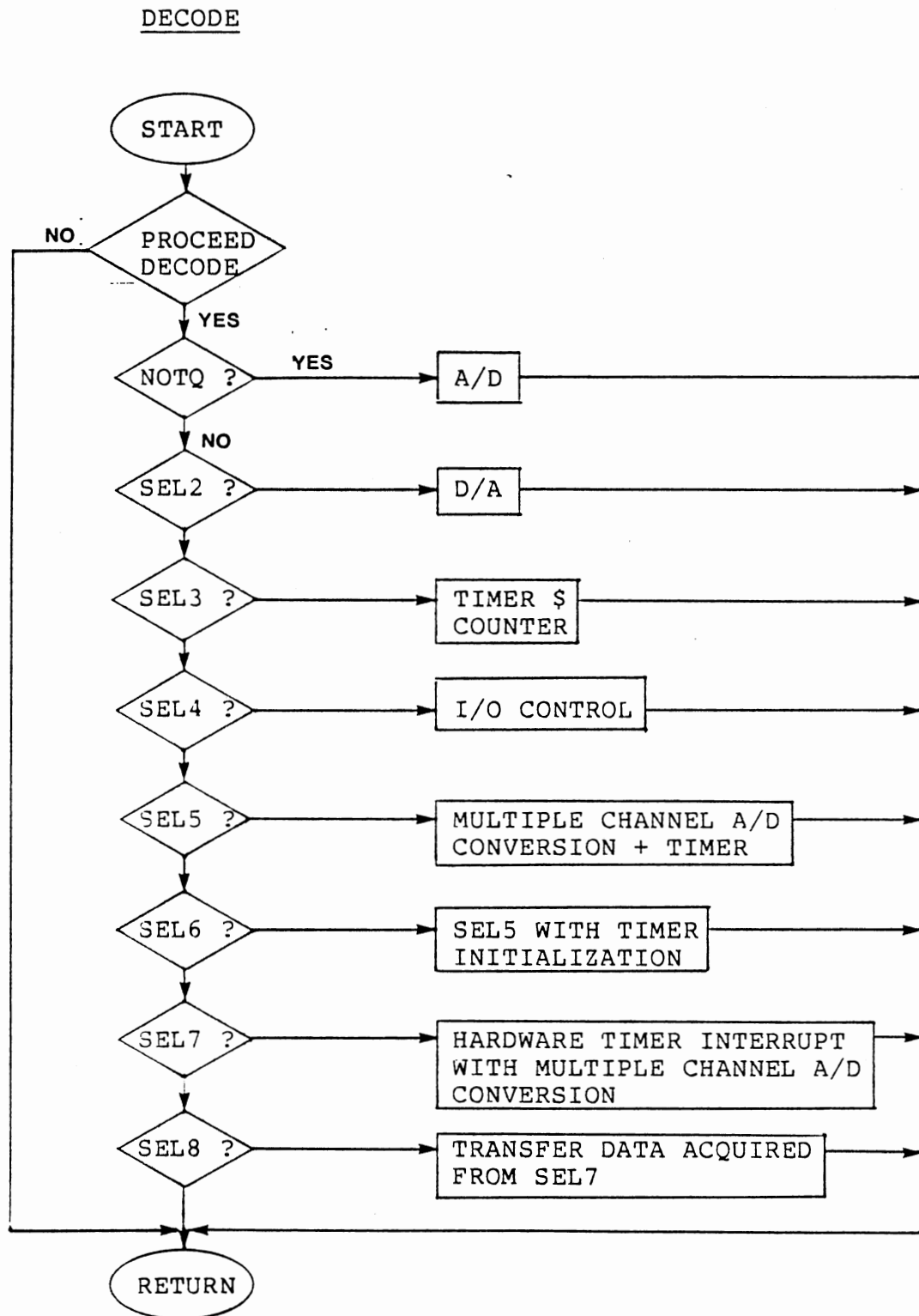


Figure 63. Decoding Routine.

Actuation Mechanism Control

The rotor which controls the position of a piston in the test housing is driven by the hydraulic motor shown in Fig. 64. The speed of the rotor is regulated by the hydraulic servovalve. The orifice of the servovalve opens by an amount proportional to the input current delivered by the power amplifier and D/A. A pressure relief valve maintains a constant supply of pressure to the servovalve constant. A heat exchanger keeps the temperature of the hydraulic fluid constant, and a hydraulic filter cleans the hydraulic fluid as this fluid moves through the hydraulic circuitry.

While the rotor turns, the position of the piston is monitored by a position sensor. When the piston is out of the bore (Fig. 65b), the downstream on/off solenoid valve is closed so that the fluid flushed through the piston-bore assembly can escape through the check valve to the reservoir. When the piston is inside the bore (Fig. 65a), the solenoid valve remains open so that the pressure difference between the upstream and downstream sides of the piston is referenced to atmospheric pressure. Under this condition, the leakage starts upstream and moves downstream through the clearance. These flushing and silting conditions must be well coordinated by the software which controls the actuation mechanism. The force required to pull the piston out of the bore must be measured. This force will be equal to the initial friction when the hydraulic fluid is filtered and clean. However, when the fluid contains solid particles such as ACFTD full distribution, the force required to

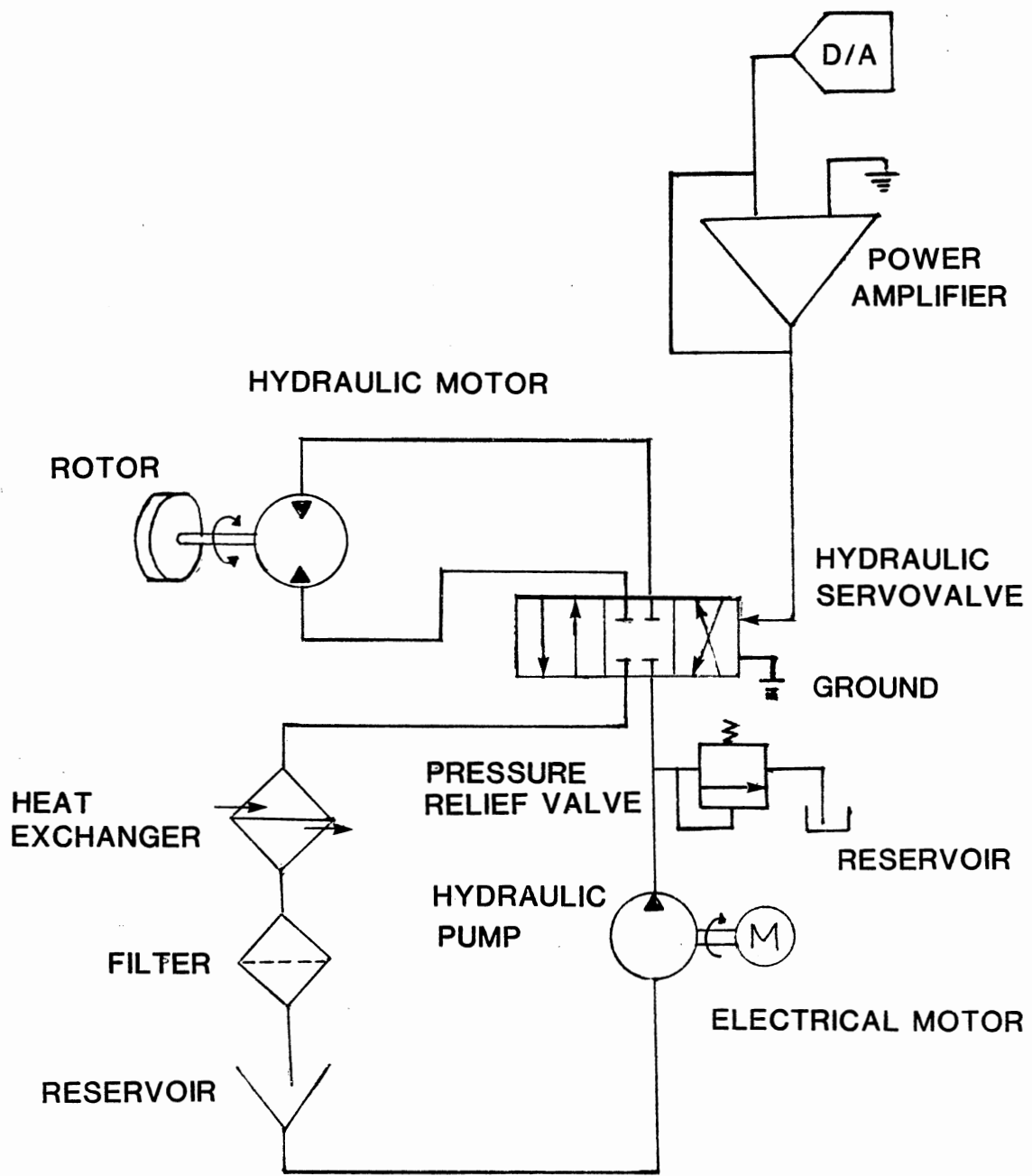


Figure 64. Hydraulic Circuitry of Actuation System.

(a) SILTING POSITION

(b) FLUSHING POSITION

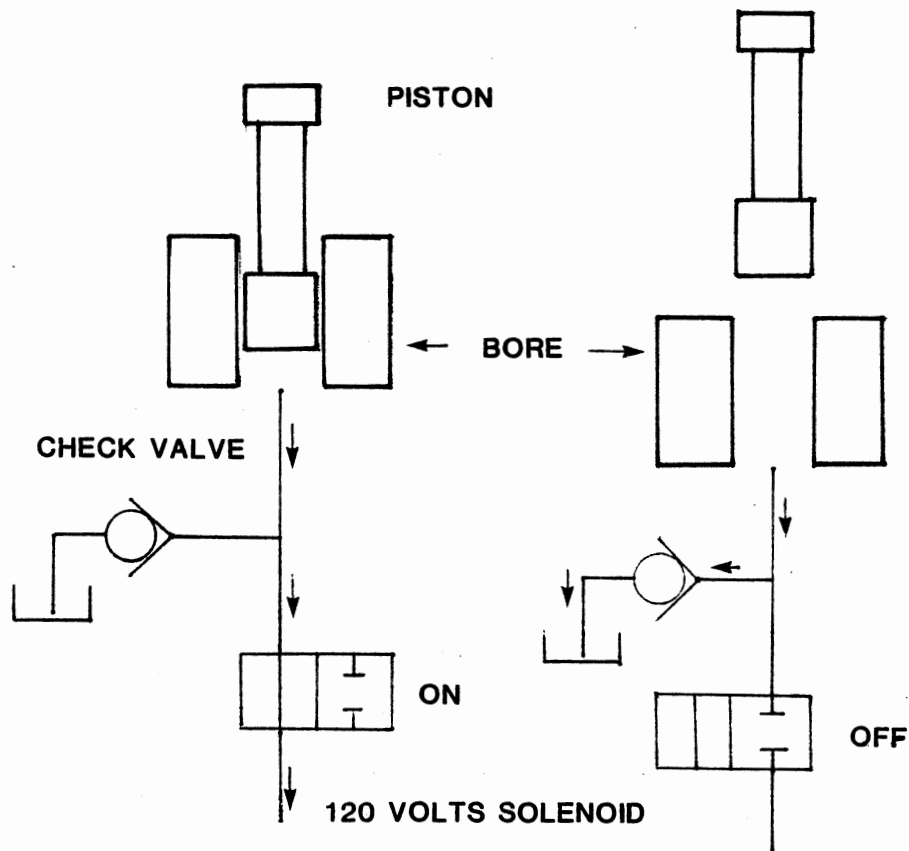
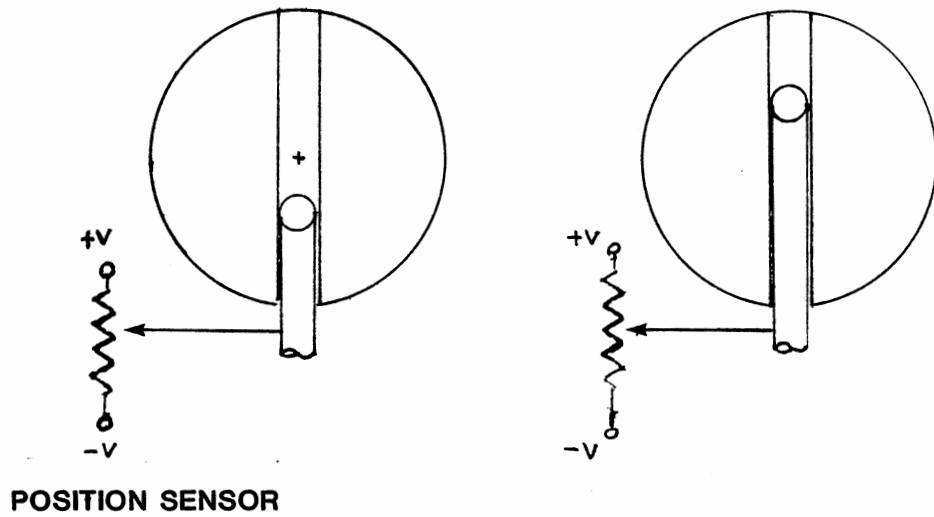


Figure 65. Piston Actuation Mechanism.

pull the piston out of the bore is expected to increase beyond the initial friction. This increase in force is the force required to break seizure. The algorithm used by the master computer is shown in Fig. 66. The main program sends the instructions to close the solenoid valve at the downstream of the test housing. Then, the master sends instructions which cause the rotor to turn so that the maximum and minimum position of the piston are checked. The rotation of the rotor also serves to flush the piston-bore assembly. The position of the piston is monitored throughout this motion by feed back control to the A/D converter which is suitably acknowledged by the master. This feed back control lowers the piston, inserts the piston into the bore, and stops the motion of the piston for the silt process. As soon as the final position of the piston is set, the master computer commands the slave computer to open the solenoid valve and allow the silt process to take place in the clearance of the piston-bore assembly for a pre-defined time (stationary time). The master computer keeps track of this stationary time, and, as soon as the defined stationary time is past, the master computer commands the slave computer to close the solenoid valve and initialize the hardware timer interrupt routine.

The hardware timer interrupt routine, when programmed for a certain period (e.g. 10 milliseconds), sends a signal to the hardware interrupt controller every 10 milliseconds. The hardware interrupt controller then signals the central processing unit (CPU) to stop execution of the present program and switch to the independent interrupt service program. This interrupt service program is executed every 10 milliseconds. The

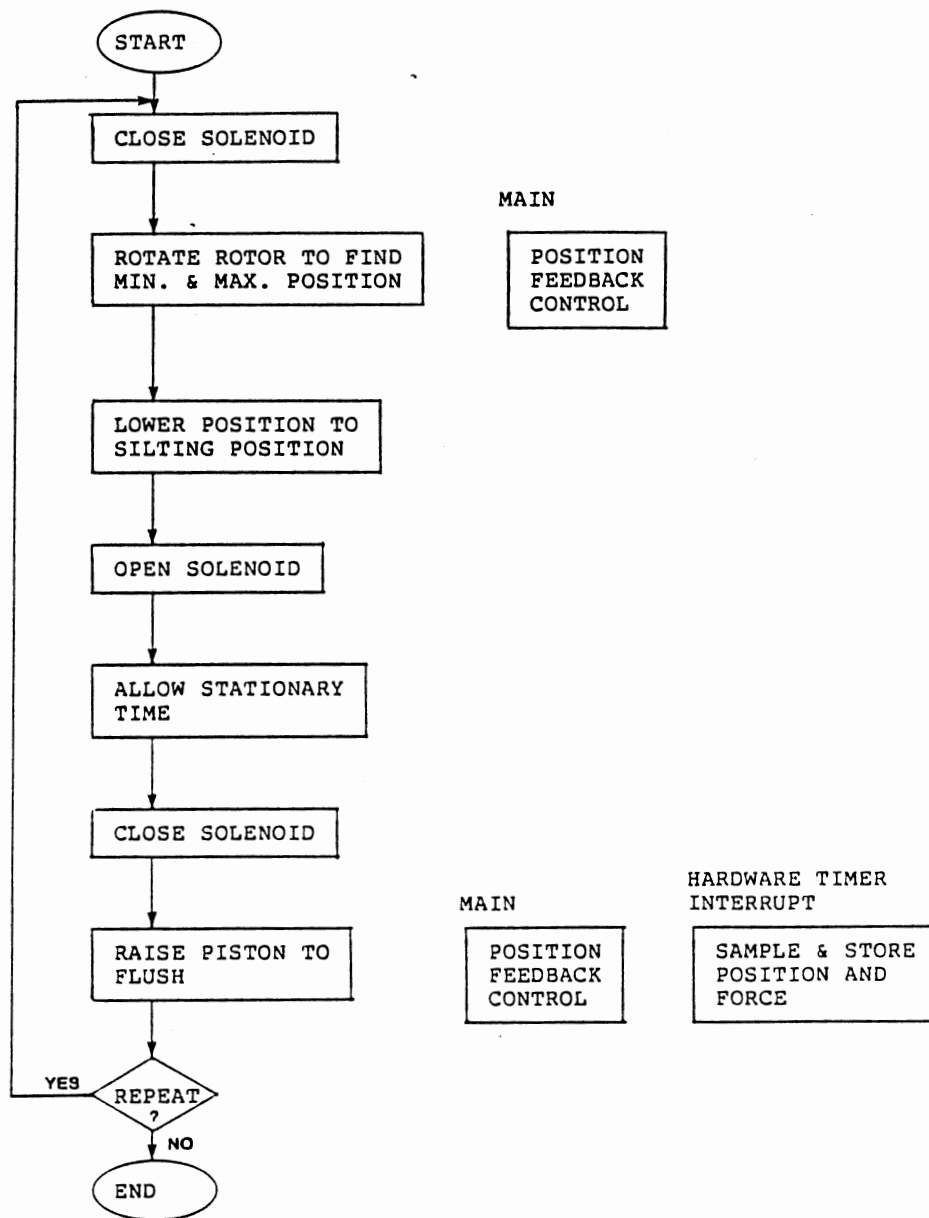


Figure 66. Actuation Algorithm for Main CPU.

duration of this program must not exceed that required by the CPU to execute this program. As soon as the CPU finishes executing the interrupt service program, the CPU returns control to the main program and resumes execution of the main program. This hardware timer interrupt procedure allows the slave computer to execute a time-critical program along with a non-time-critical (main) program. Appendix E contains a listing of the source code for this main program.

It is now apparent that the integration of the hardware and software achieves the following:

1. Precise time control of the piston movement.
2. Precise and accurate motion of a piston.
3. An actuation mechanism control with virtually no human error

Further improvements were made to reduce the initial friction between the actuation rod and the housing by adding a teflon cap seal between the actuation rod and the O ring seal.

A preliminary test run of the actuation mechanism revealed that a guide is needed to smoothly insert a test piston into a bore smoothly. Without a guide, an excessive misalignment between the axis of the piston and the axis of the bore can cause the piston to collide with the bore. A guide cap was therefore designed and built, and a 45 degrees chanfer was machined on the bore surface as shown in Fig. 67. These additions immediately corrected any misalignment problems.

Another problem was noted once testing began. This appeared to be due to flow-induced vibration of the piston. When the piston is outside the bore, the circulating hydraulic fluid hits the side of the piston.

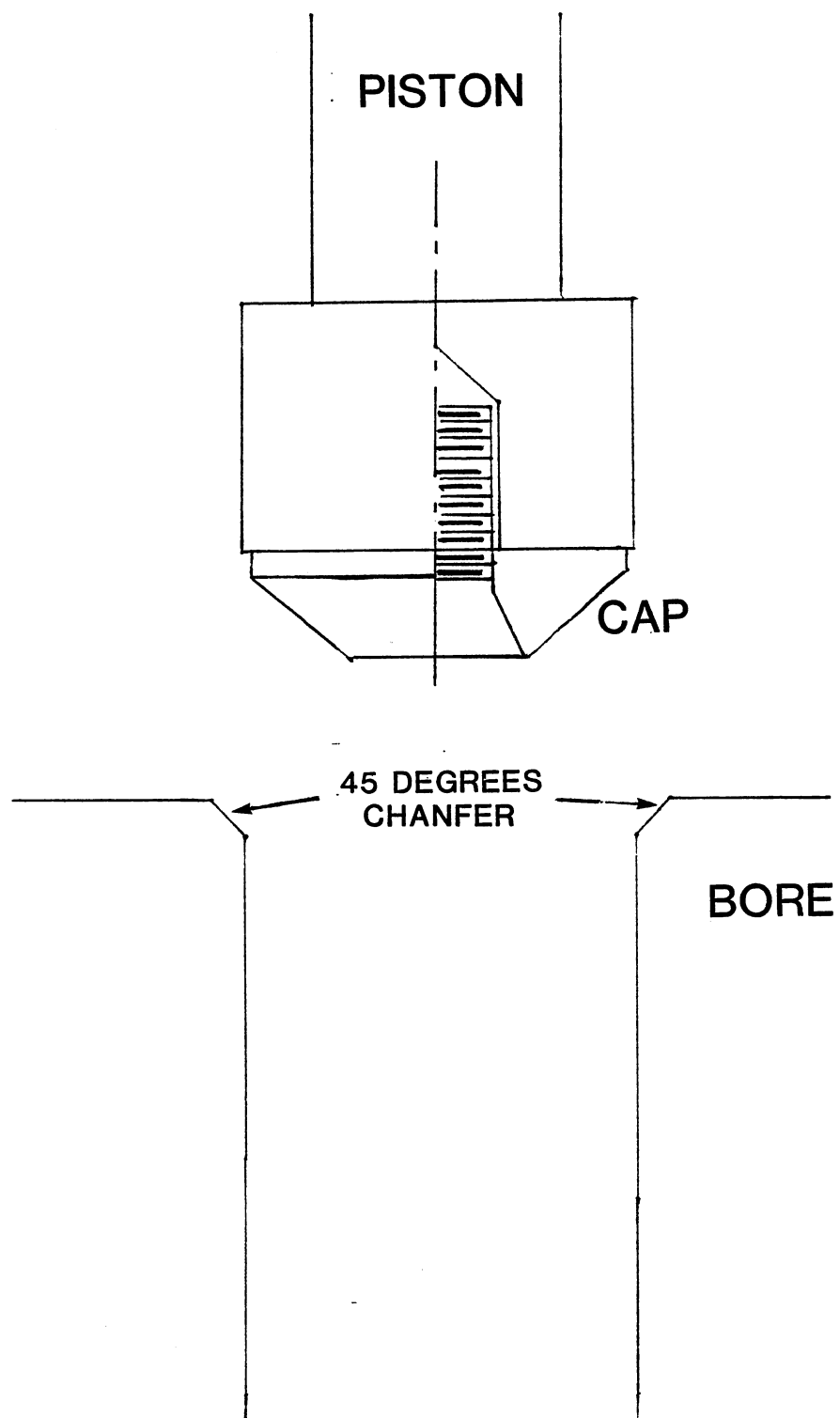


Figure 67. Alignment Improvements.

At 500 psi, this induced vibration is sufficient to unscrew the piston from the actuation rod. An effective remedy to this problem was to use a commercially available threadlocker called "LOCTITE."

Experimental Results and Analysis

The verification tests of the silt process model provide the number of particles, and their size, retained in the clearance of a piston-bore assembly. These particles in the clearance cause a sudden increase in the force which moves the piston from the bore. The experimental facilities are organized to measure this increase in force. To measure the seizure force associated with the presence of silt particles in the clearance of the piston-bore assembly, the initial friction force had to be measured first while the hydraulic fluid (Dexron II for this case) was clean. This initial friction force had to be subtracted from the total seizure force measured after the injection of solid particles. The resultant force was the additional force needed to overcome the seizure caused by the solid particles in the clearance (Fig. 68). From hereafter, this additional force is called the seizure force.

Each piston had two land lengths: 6.38mm and 3.19mm. Thus, a given pair of piston-bore assemblies could be tested for two land lengths. Each pair was tested under three different pressures (100, 200, and 500 psi) and three stationary times (15, 30, and 60 seconds), the stationary time being that allowed for particles to silt in the clearance. For each test condition, at least three measurements were performed. Thus, for

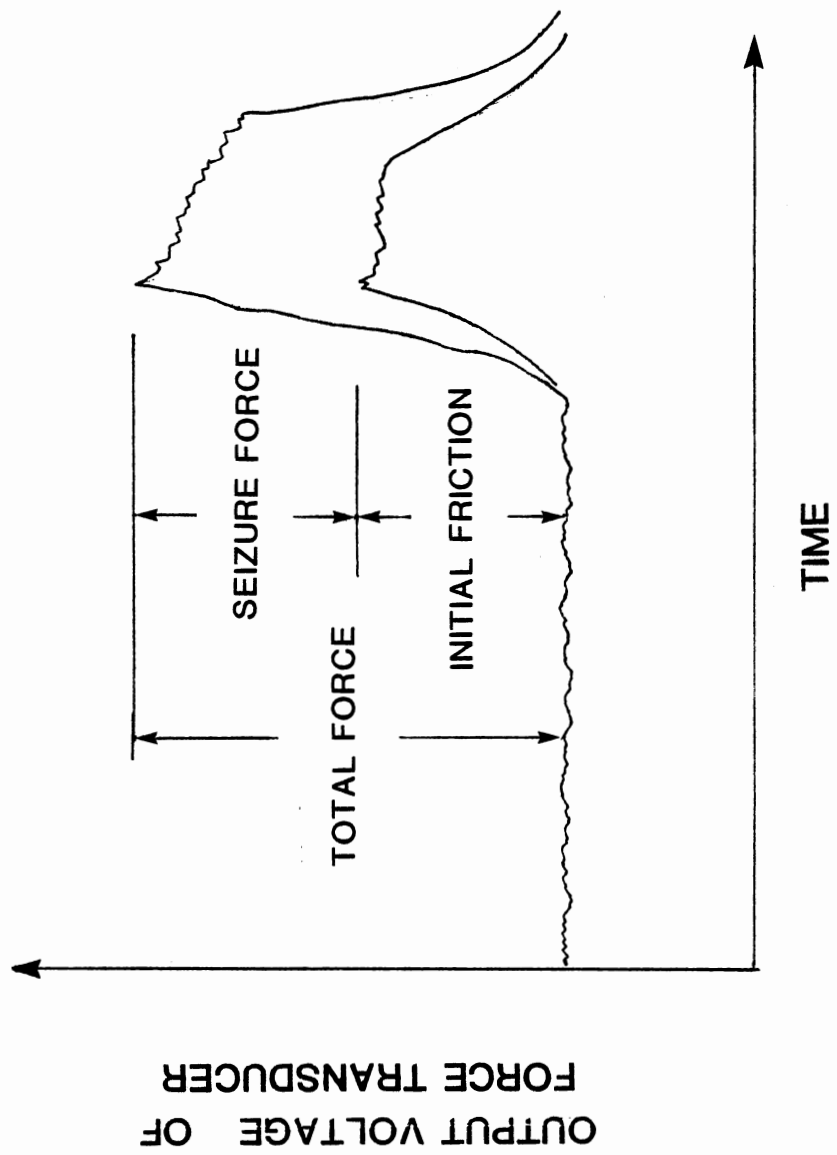


Figure 68. Seizure Force.

each pair of piston-bore assemblies, 54 measurements were made.

ACFTD full distribution was used as the source of solid particles for this particulate-induced seizure test. Enough ACFTD was injected to achieve a solids concentration of 25 mg/L. Since ACFTD full distribution can not be maintained for more than one hour in the hydraulic system used for this experiment [25], and because a set of 54 tests was needed (as explained above), each test could not be permitted to exceed a duration of one minute.

To complete the experimental set, pistons of different hardness were chosen to investigate the effect of hardness on seizure force. The pistons are listed in Table VII. The No. 3 bore with a hardness of 725 Brinell (Rockwell 62-64 on the C scale) was not swapped out for other pistons and remained in the test housing throughout the test. All the experimental results are summarized in the seizure force analysis figures in Appendix F. Three representative seizure force analysis figures were chosen for the following analysis and discussion. The piston-bore assemblies in these representative figures had the same 10 micrometer nominal clearance, and a 6.38mm land length. Only the hardness of the pistons differed. Figure 69 shows the results for the tests of the piston with a hardness of 725 Brinell. The dark lines show the average force predicted by simulation, and the circles, triangles, and rectangles with the dotted lines represent the averaged data points. Since the data points in the figure are the average of three test data, some scattering of the data was expected. Above 200 psi, the experimentally measured seizure forces were consistently less than the simulation results. For

TABLE VII
PISTON SELECTION FOR HARDNESS

BORE NO.	PISTON NO.	NOMINAL CLEARANCE μm	PISTON HARDNESS (Brinell)
3	22	10	725
	25	15	725
	1	5	120
	2	5	120
	5	10	120
	8	15	120
	11	5	400
	14	10	400
	17	15	400

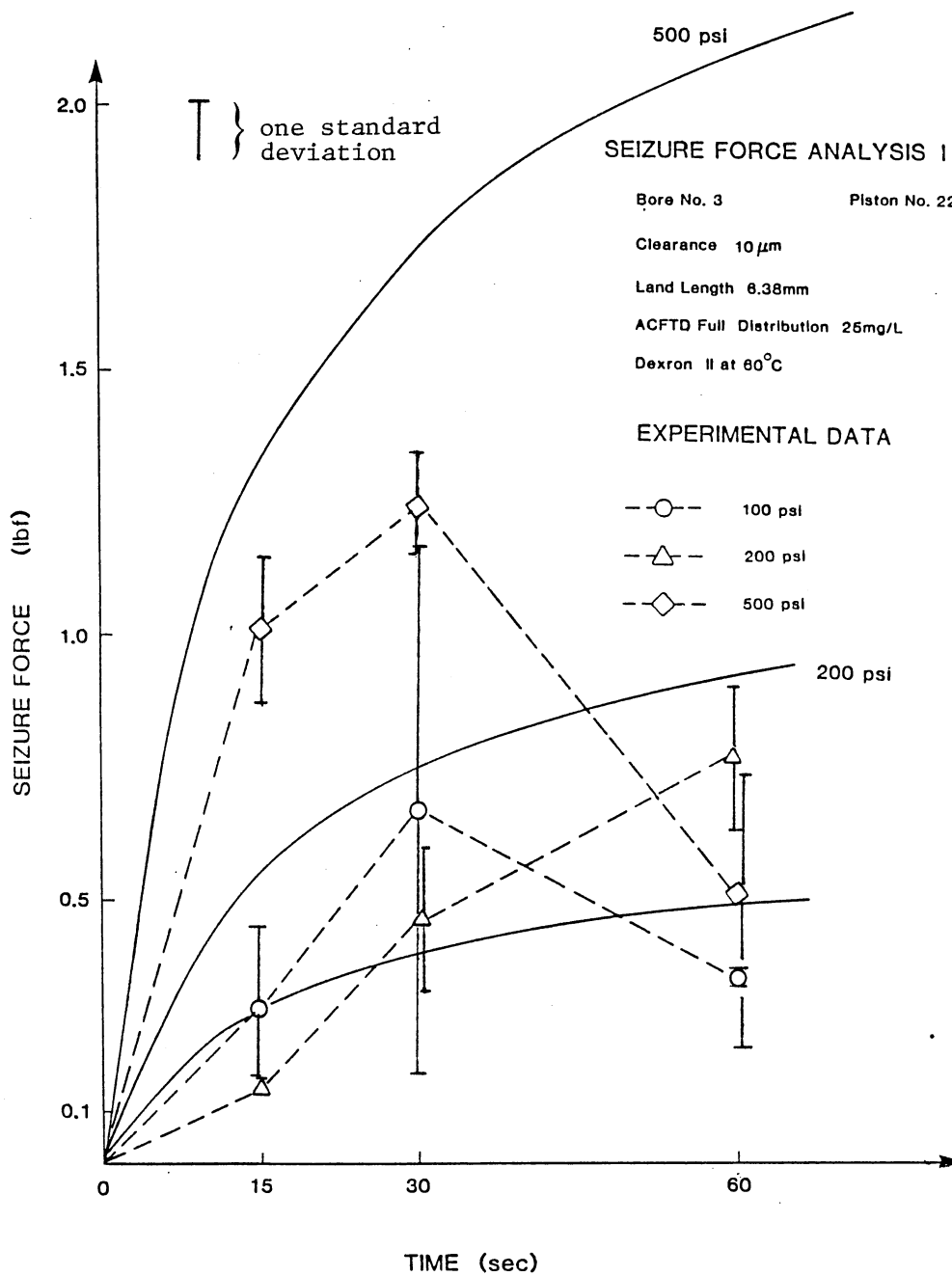


Figure 69. Seizure Force Analysis (I).

the assemblies described by the data in Fig. 69, both the piston and bore were harder than ACFTD, which has an estimated hardness of 500 Brinell. Therefore, the particles were expected to be deformed or crushed under the experimental conditions. It is also possible that Dexron II acted as a lubricant and helped the solid particles to reorient themselves through sliding or cutting the piston and/or bore surfaces. Microscopic observation (Fig. 70) clearly supports that conspicuous cutting action took place on the piston surface at the upstream side where solid particles silted. The controlling stress for seizure force in this case was the yield stress estimated from the hardness of silica (500 in Brinell) through:

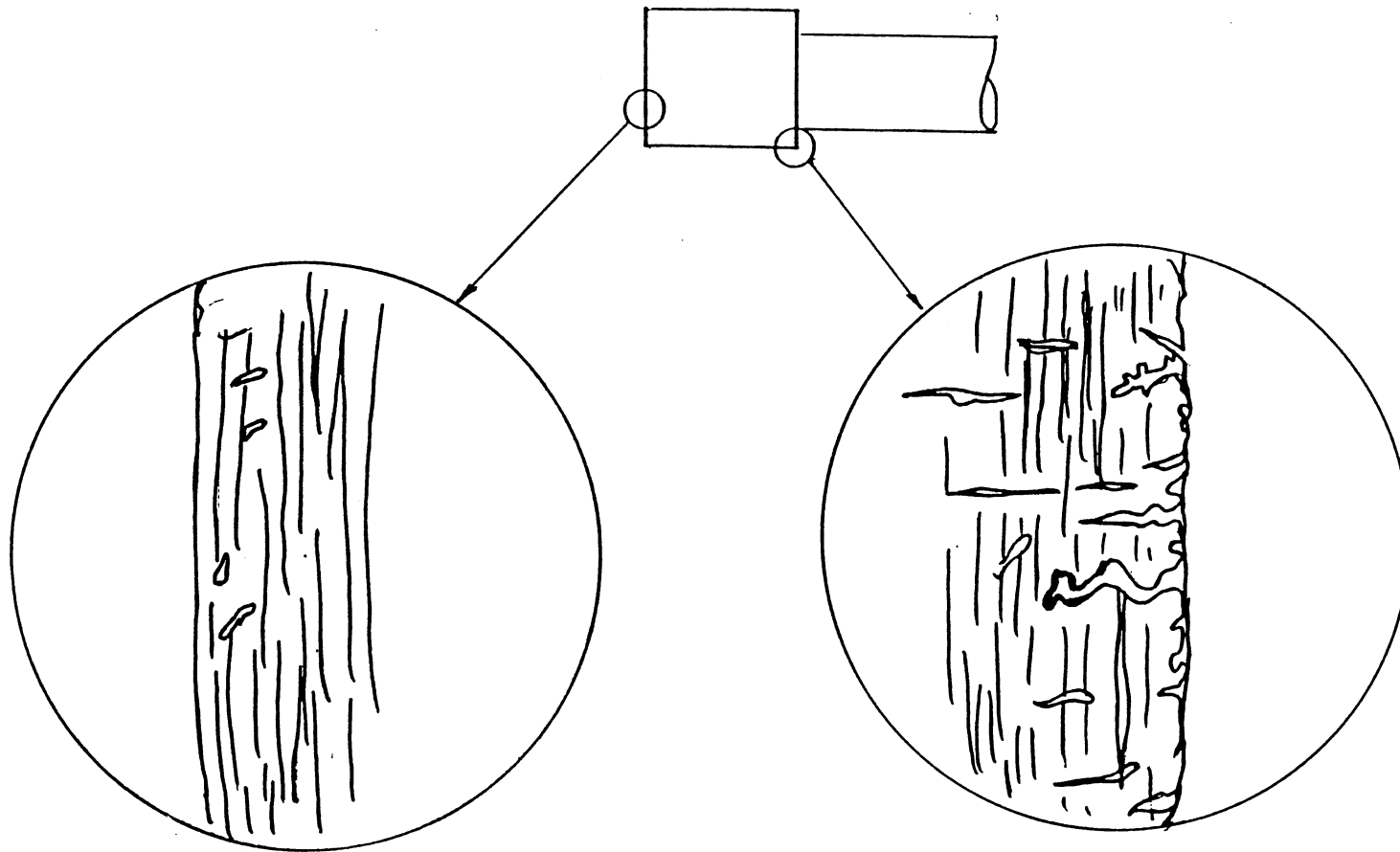
$$\text{Yield Stress} = 500 H_B / 1.8 \quad (92)$$

where

H_B = Brinell hardness.

In contrast to Fig. 69, the experimental data tends to be higher than the simulation results in Fig. 71. For the case in Fig. 71, the piston surface was slightly softer (400 in Brinell) than ACFTD; therefore, particles should have been able to indent into the surface of the piston. If particles only indented, then essentially, the particles should have stayed out of the piston motion, and the seizure force should have decreased. However, more than just indenting action occurred.

Figure 72 is a sketch of the microscopic picture of the upstream side of the surface of the No. 14 piston. In Figure 70, the ground



DOWNSTREAM x400

UPSTREAM x400

Figure 70. Microscopic Observation of Piston Surfaces.

SEIZURE FORCE ANALYSIS II

Bore No. 3

Piston No. 14

Clearance 10 μm

Land Length 6.38mm

ACFTD Full Distribution 25mg/L

Dexron II at 60°C

EXPERIMENTAL DATA

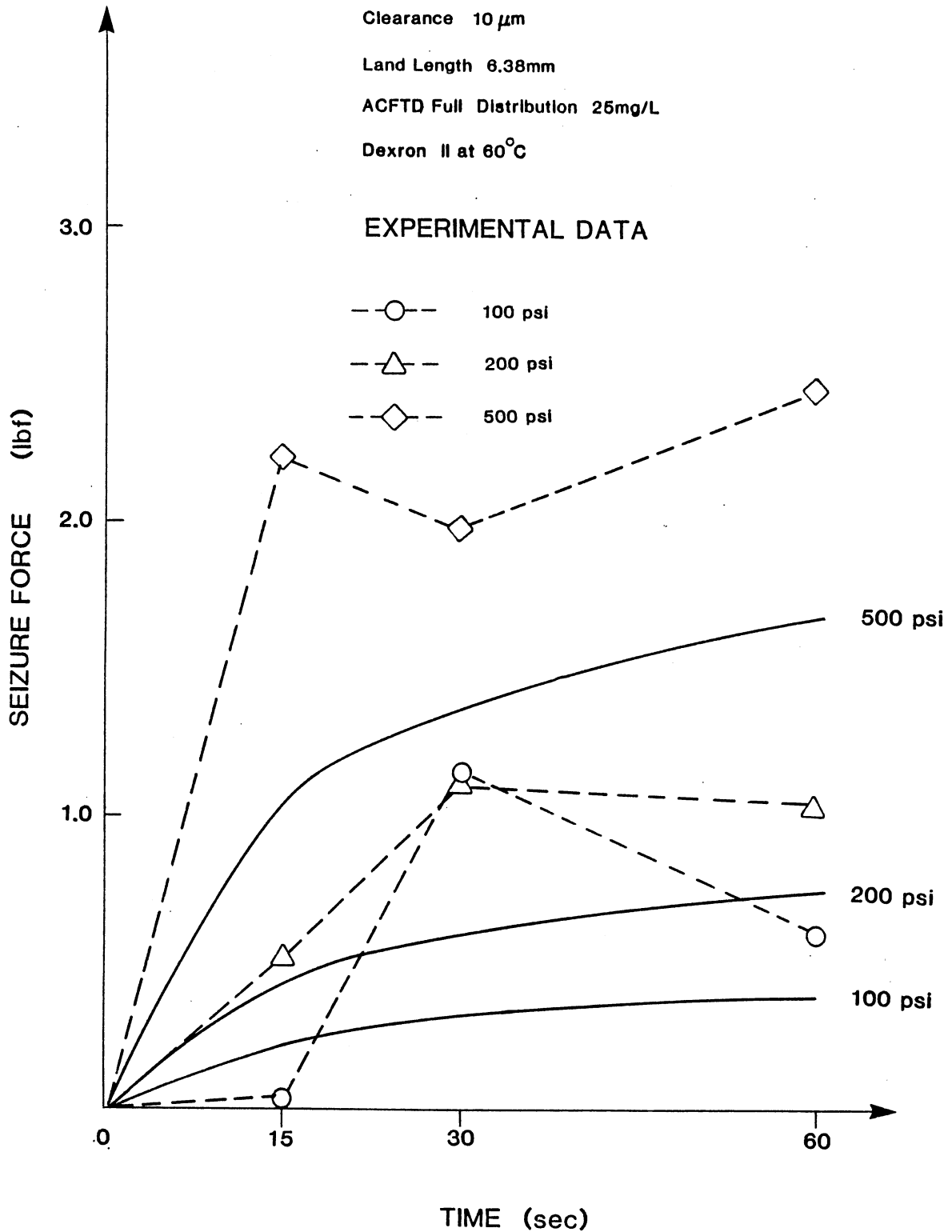


Figure 71. Seizure Force Analysis (II).

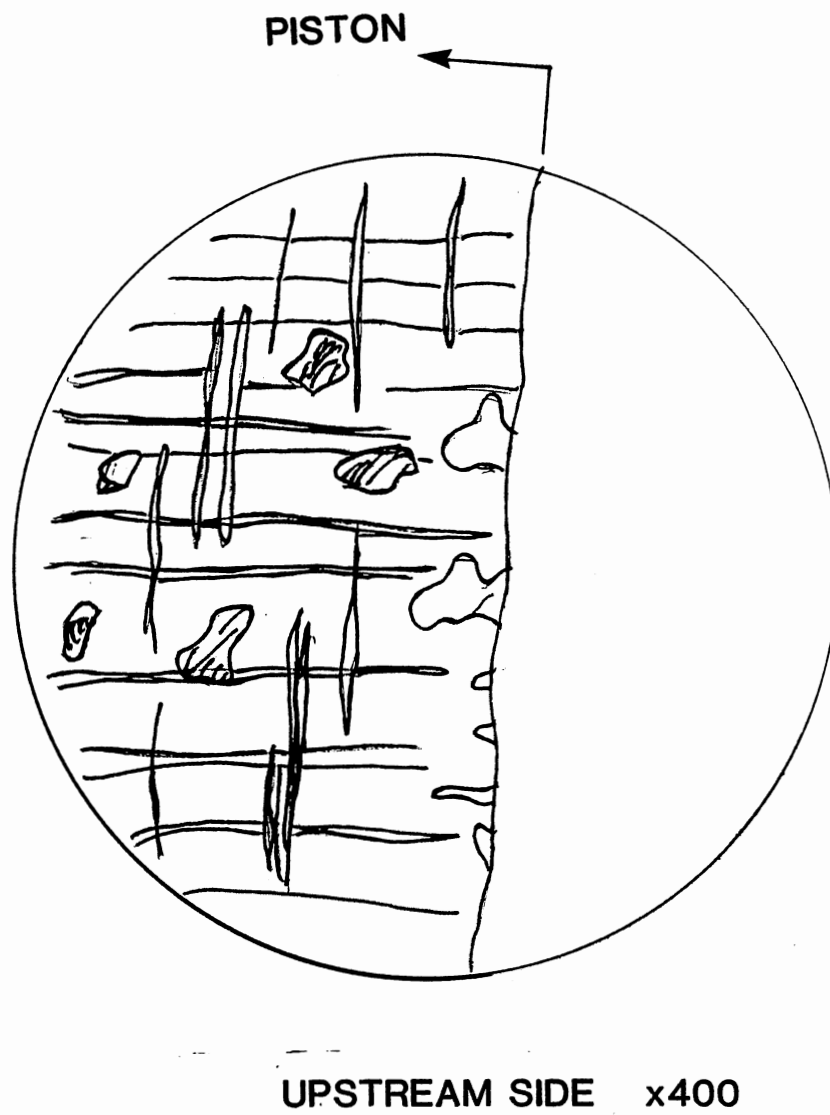


Figure 72. Microscopic Observation of Piston (Rc 43-45).

surface (vertical lines) is obvious; however, in Fig. 72, almost all trace of the grinding action is gone. Instead, there are many lateral lines that must have been created by ACFTD. In addition, there are several noticeable small holes which also must have been created by ACFTD. This means that many ACFTD not only indented into the surface causing the visible small holes, but also performed massive cutting action (shown by the lateral lines). In order for continuous cutting action to take place, there must be sufficient force to plastically deform the piston surface. This may be why the seizure force was higher than what the simulation program predicts. The particulate-induced seizure model predicts seizure force based upon the yield stress, not the ultimate stress, of interacting surfaces. Figure 73 shows the experimental and simulation results for the softest of the three pistons. The experimental data tend to be higher than the simulation data, as Fig. 71 shows. Figure 74 shows the upstream side surface of the piston used for the experiment. The edge of the surface was so destroyed that it no longer retained its original shape. Many small holes and lateral lines were obvious through the microscope.

The results shown in Fig. 71 and Fig. 74 indicate that the simulation result of seizure force will closely model the experimental result if the stress which has a higher value than the yield stress of the softest material among the piston-bore and particle is used.

SEIZURE FORCE ANALYSIS III

Bore No. 3

Piston No. 5

Clearance 9.5 μm

Land Length 6.38mm

ACFTD Full Distribution 25mg/L

Dexron II at 60°C

EXPERIMENTAL DATA

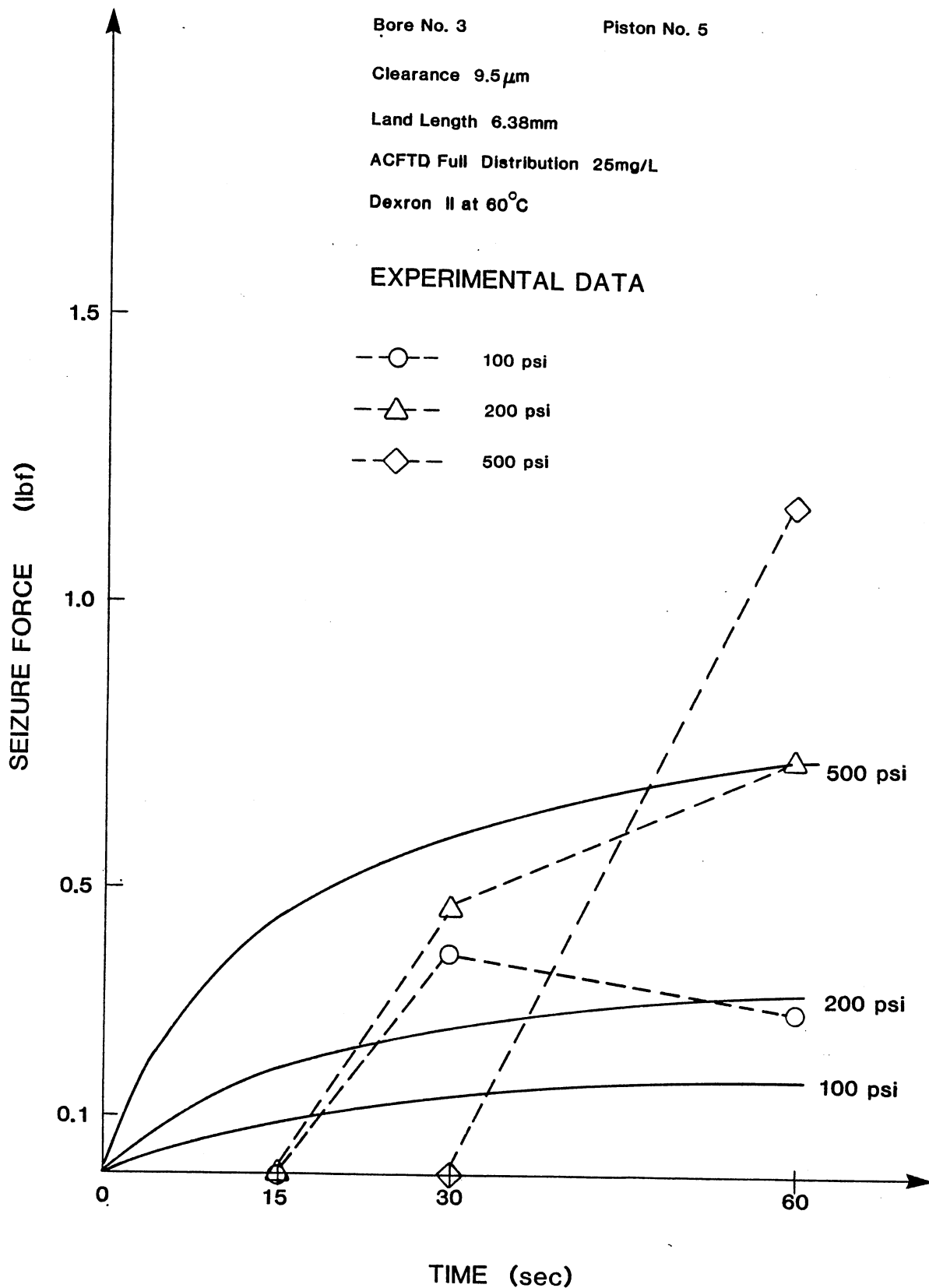
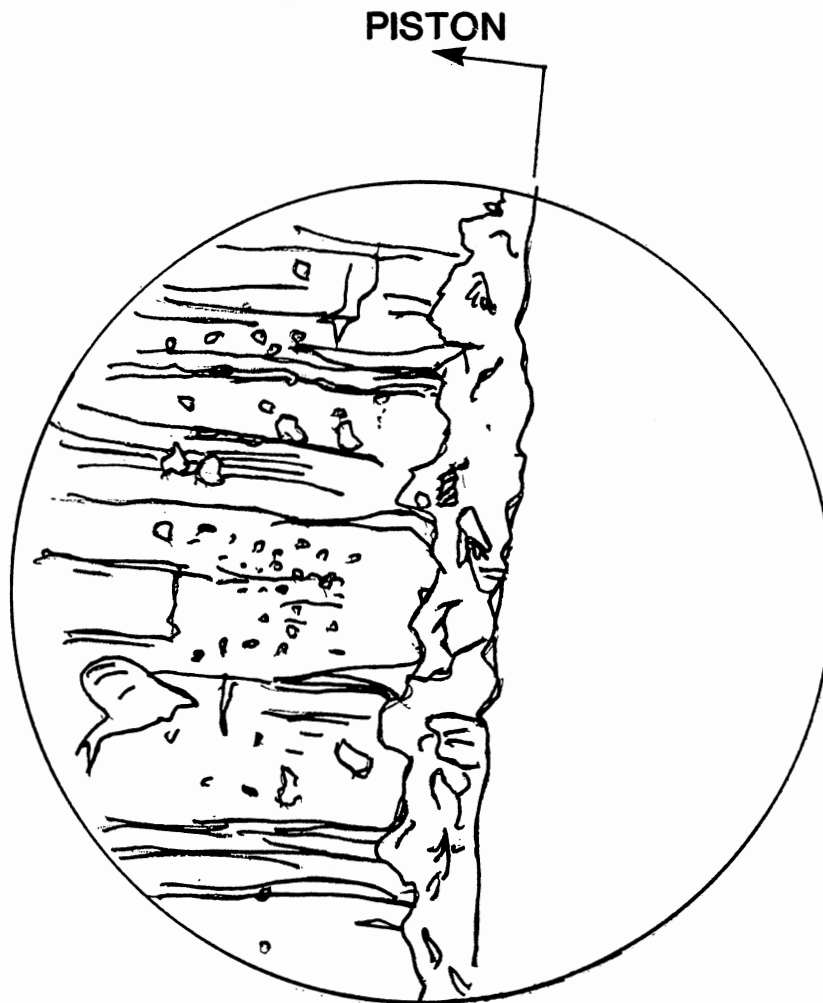


Figure 73. Seizure Force Analysis (III).



UPSTREAM SIDE x400

Figure 74. Microscopic Observation of Piston ($H_B = 120$).

CHAPTER VI

VERIFICATION OF THE DITHER MODEL

Kamijo et. al. observed that dither is capable of preventing non-uniform pressure distribution in the clearance of a piston-bore assembly, and suggested that the solid particles in the clearance are removed by dither [8]. If this is true, then with a given piston-bore assembly and a constant upstream particle size distribution, there should be an increased number of particles at the downstream side of a piston-bore assembly when dither is applied to the piston. This means that silt Beta values of a given piston-bore assembly should decrease when dither is applied. Nikitin's experimental results [13] suggest that the higher the frequency of dither, the more effective is dither in reducing the frictional force required to move the piston of a piston-bore assembly. Kamijo and Nikitin's findings suggest that silt Beta values of a given piston-bore assembly may be a function of dither frequency. The following questions arise:

1. How do silt Beta values of a piston-bore assembly vary as dither is applied to the piston?
2. How does seizure force vary when dither is applied to the piston?

Experimental Facility

The development of the piston actuation mechanism for dither required only a slight modification to the mechanism, shown in Fig. 58. The eccentricity position of the joint between the linkage and rotor was positioned such that the maximum travel of the piston rod was 0.762 millimeter plus or minus 0.08 milliliter. Thus, uni-directional rotation of the rotor caused dither action of the piston with the amplitude of 0.762 millimeter. The frequency of dither could be controlled by varying the input voltage across the servovalves.

For the determination of silt Beta values, the leakage fluid from the tested assembly was collected and analyzed by the method presented in Chapter IV.

Experimental Result and Analysis

The upstream pressure of the piston-bore assemblies was fixed at 1000 psi. The temperature of Dexron II fluid was maintained at 60 degrees Celsius. The No. 6 piston and No. 23 piston (both giving a nominal clearance of 10 micrometers with the No. 3 bore) were chosen for this dither so that the effects of piston hardness could also be studied. The hardness of piston No. 6 was 725 Brinell (harder than ACFTD), while the hardness of piston No. 23 was 120 Brinell (softer than ACFTD).

ACFTD full distribution was chosen as the solid particles source for the dither test. ACFTD was injected from the reservoir to achieve a

concentration of 25 mg/L. When the fluid was filtered and clean, the upstream pressure was raised to 1000 psi, and the downstream pressure was open to atmospheric pressure to create a 1000 psi drop across the clearance of the No. 6 piston with a 6.38mm land length and the No. 3 bore. The rotor was first rotated to record the force variation under low frequency dither. The force was observed to be 2.5 lbf to -0.1 lbf peak to peak (Fig. 75). The positive force means that the force transducer experienced tensile force and the negative force means that the transducer experienced compression. At high frequency dither, the recorded force increased to roughly 3.1 lbf peak to peak (Fig. 76).

The two ball valves in the hydraulic circuitry were closed to isolate lines connected to the test housing. The piston was inserted into the bore, and while the actuation mechanism applied dither motion to the piston, the piston never completely left the bore (Fig. 77). The downstream side of the piston was flushed with ether to remove oil as well as particles, so that the leakage fluid that was collected in the clean bottle for the particle size distribution analysis was not corrupted by unwanted residual particles.

The dither frequency was set at 0.057 Hz, and the two ball valves were opened to introduce contaminated fluid (25 mg/L of ACFTD full distribution). Immediately after the introduction of solid particles to the clearance, both the tension and compression force increased (Fig. 78). The force was about 3.5 lbf to -1.5 lbf peak to peak. As time elapsed, the peak to peak force decreased.

The dither frequency was raised to 1.24 Hz and the same test was

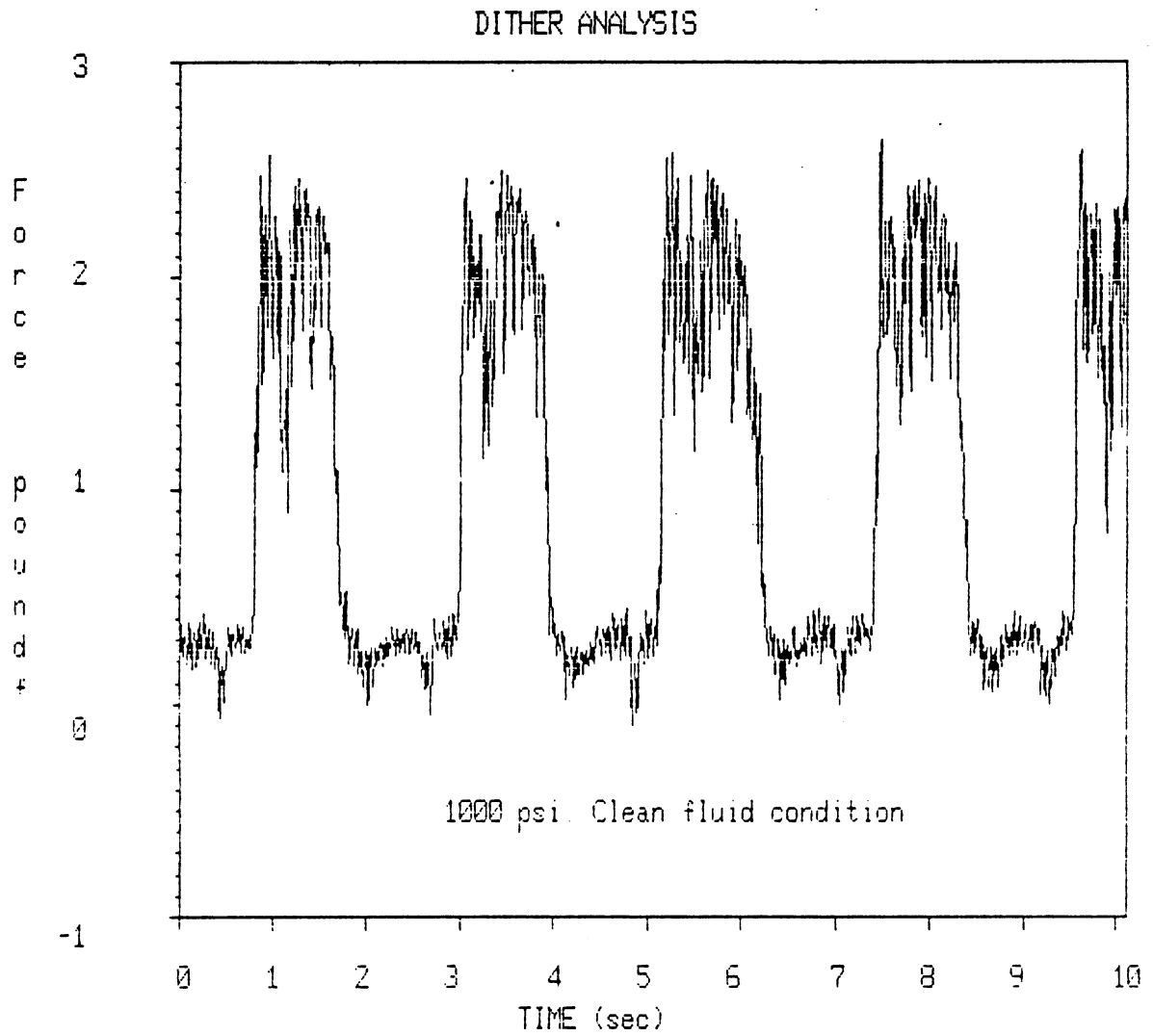


Figure 75. Dither Analysis (I).

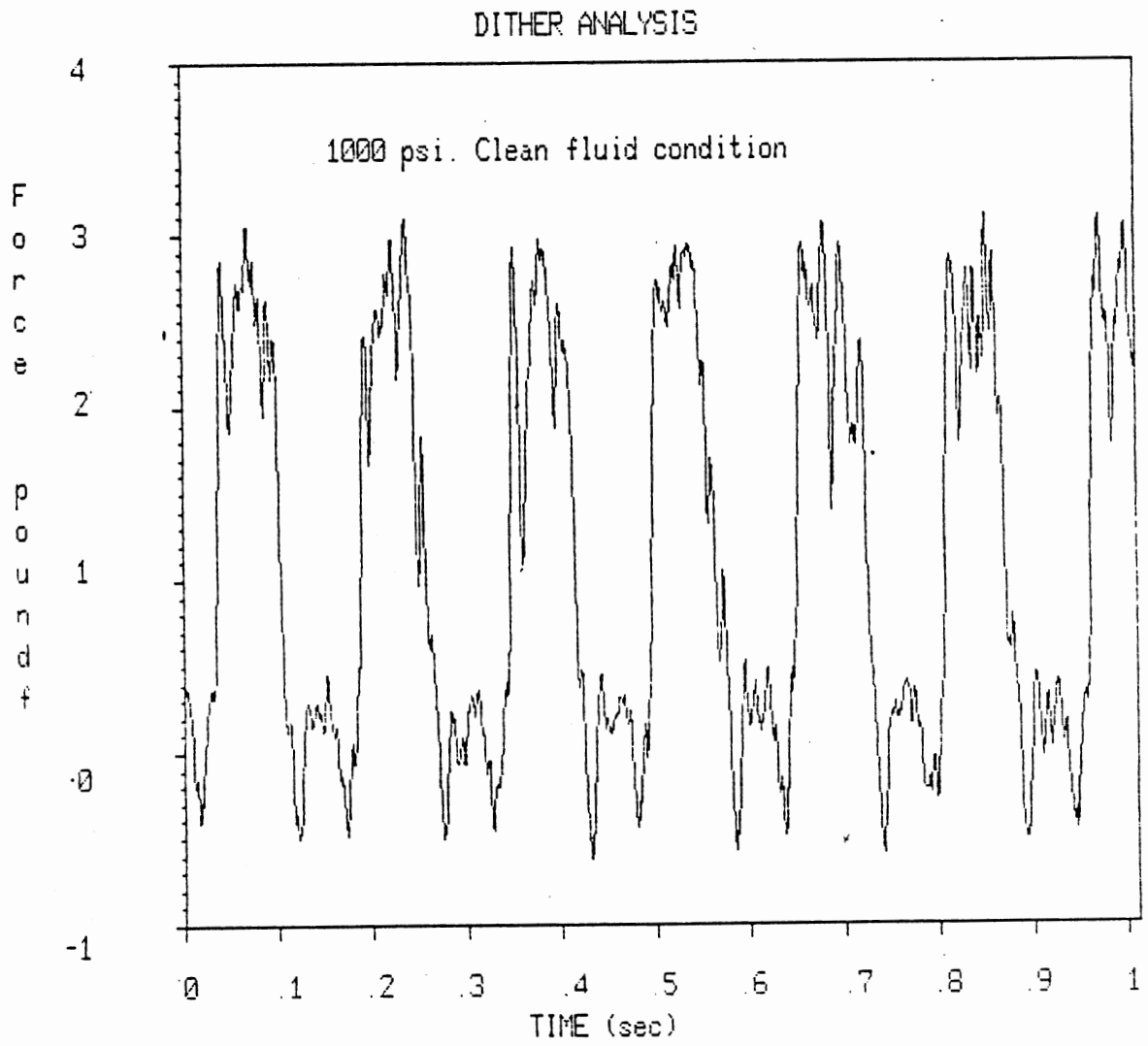


Figure 76. Dither Analysis (II).

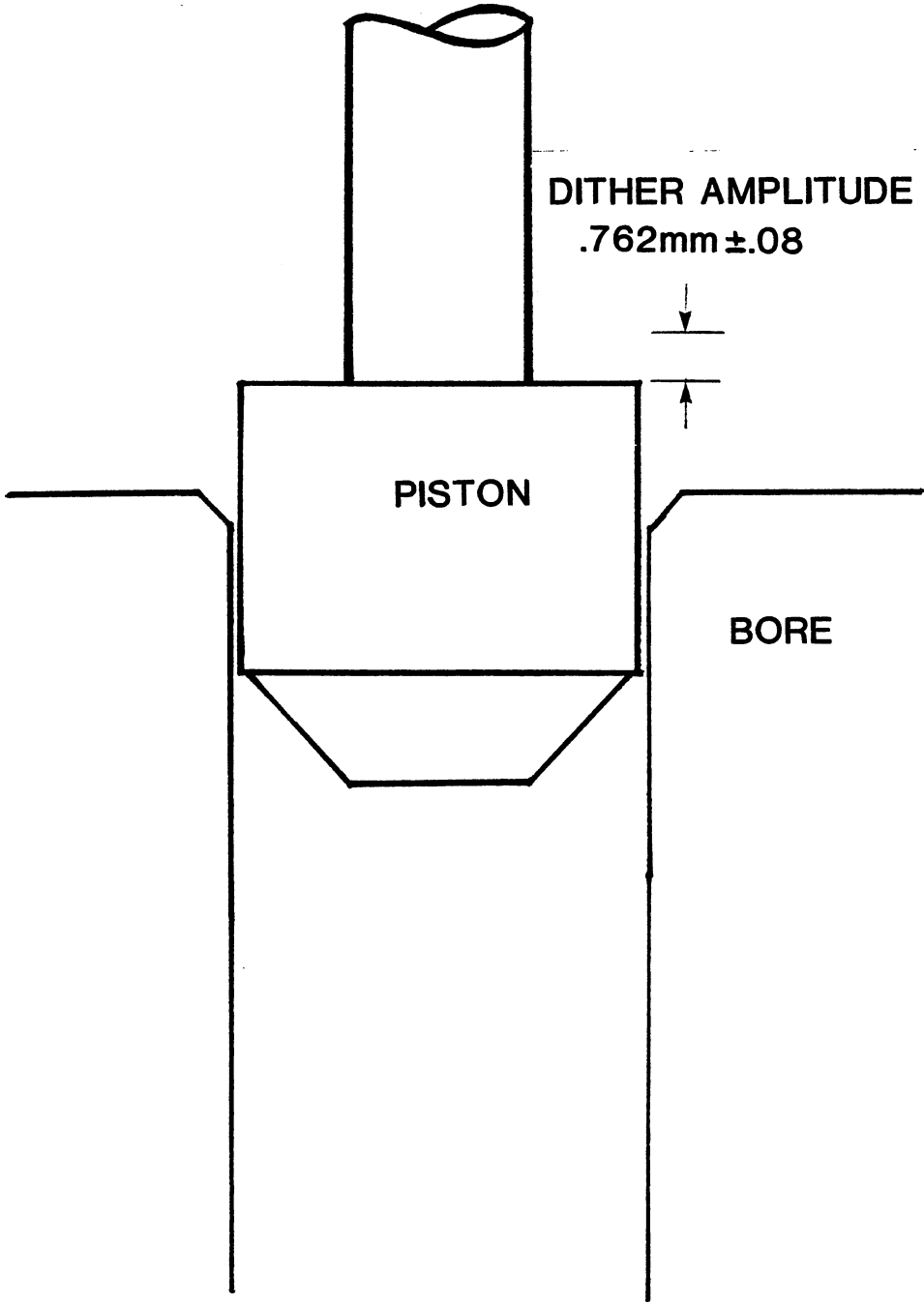


Figure 77. Dither.

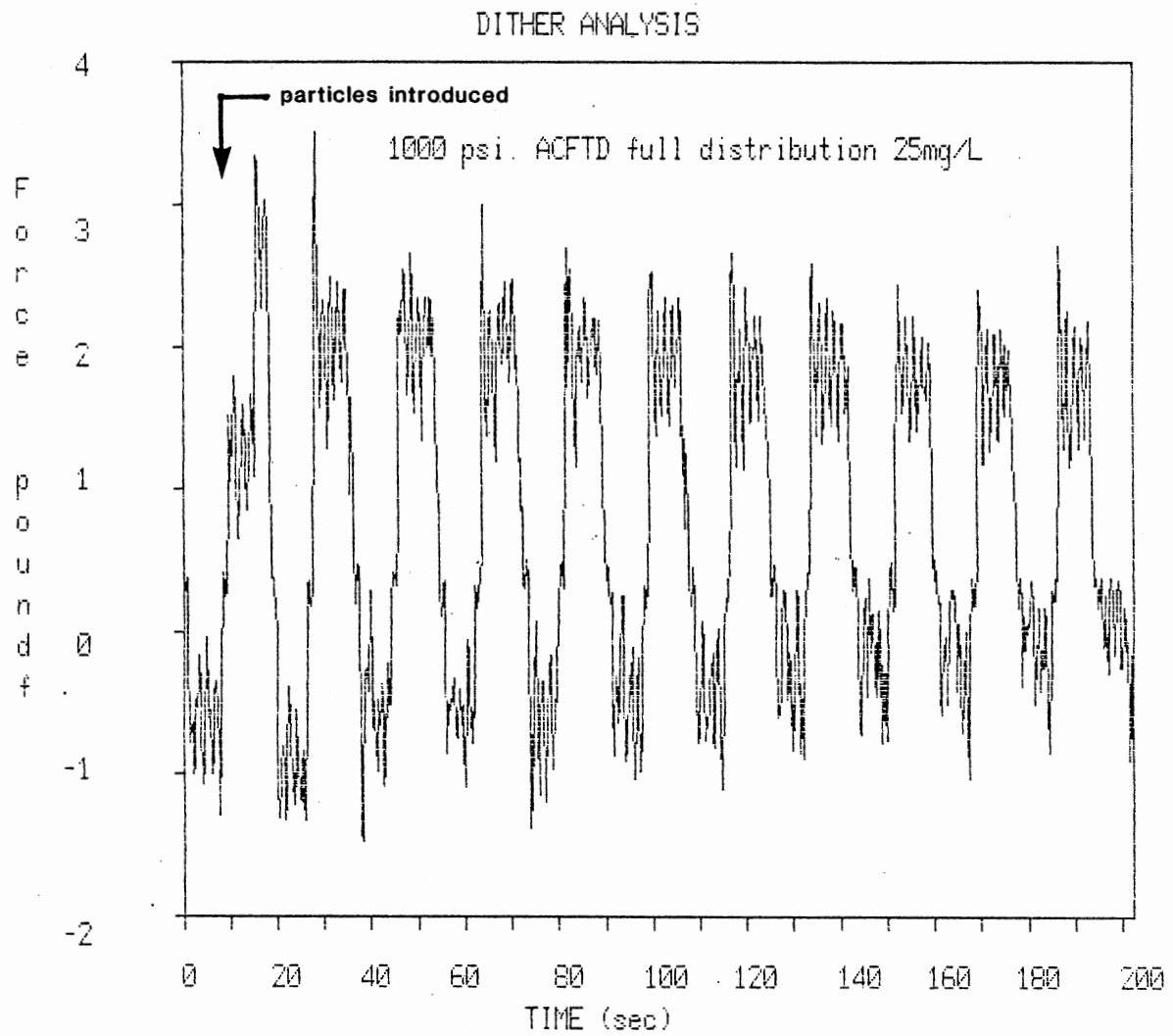


Figure 78. Dither Analysis (III).

repeated (Fig. 79). For approximately the first 20 seconds from the time that the ACFTD was introduced, the peak to peak force was affected and the maximum peak to peak force was increased to 4.5 lbf (3.5 lbf to ~~-0.1~~^{-1.0} lbf). After that, the peak to peak force gradually decreased and remained at 2.5 lbf to -0.5 lbf. The dither frequency was further increased to 7.9 Hz (Fig. 80). The measured force was immediately increased to 3.8 lbf to -1.5 lbf, a difference of 5.3 lbf. The force due to solid particles lasted approximately 25 seconds after, which the force seemed to resume steady oscillation.

The difference between the upper peak and the lower peak force was plotted in Fig. 81. The peak to peak difference in the force under clean fluid showed gradual increase as the dither frequency increased. This is probably caused by the inertia of the bearing rod attached underneath the force transducer. On the other hand, the difference in the force under the contamination decreased at first, and then gradually increased. The difference between the force under clean fluid and contaminated fluid is the force needed to overcome the extra friction caused by particles entrained in the clearance. This extra friction decreased quickly at first as the dither frequency increased to 1.5 Hz, yet it did not show a diminishing trend when the dither frequency was raised above 1.5 Hz.

The downstream particle size distribution was analyzed from the leakage collected in the clean bottles. The silt Beta values were obtained and converted to filter efficiency versus particle size, as shown in Fig. 82. With a dither frequency of 0.057 Hz, the piston-bore assembly actually filtered particles better than the assembly without

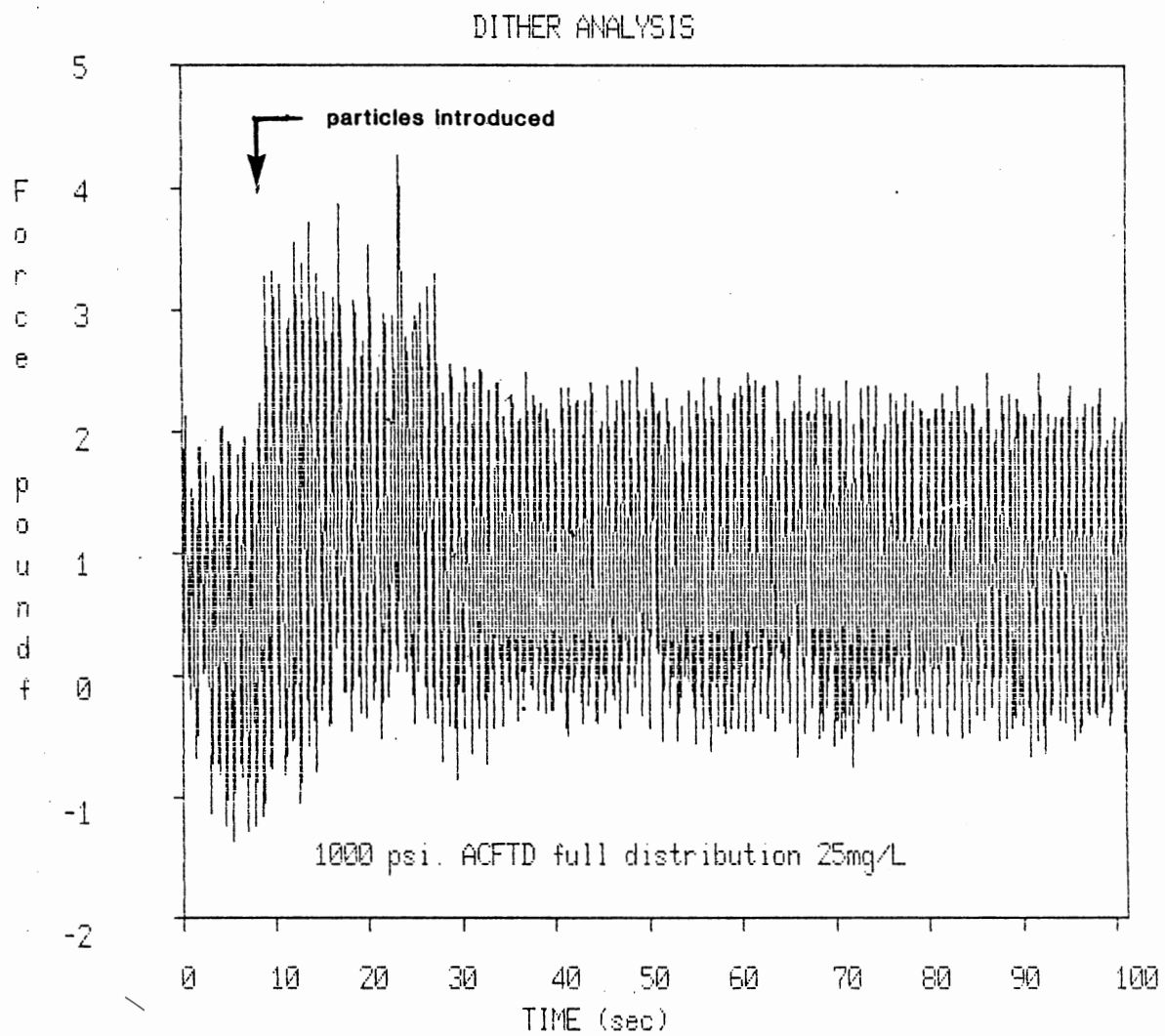


Figure 79. Dither Analysis (IV).

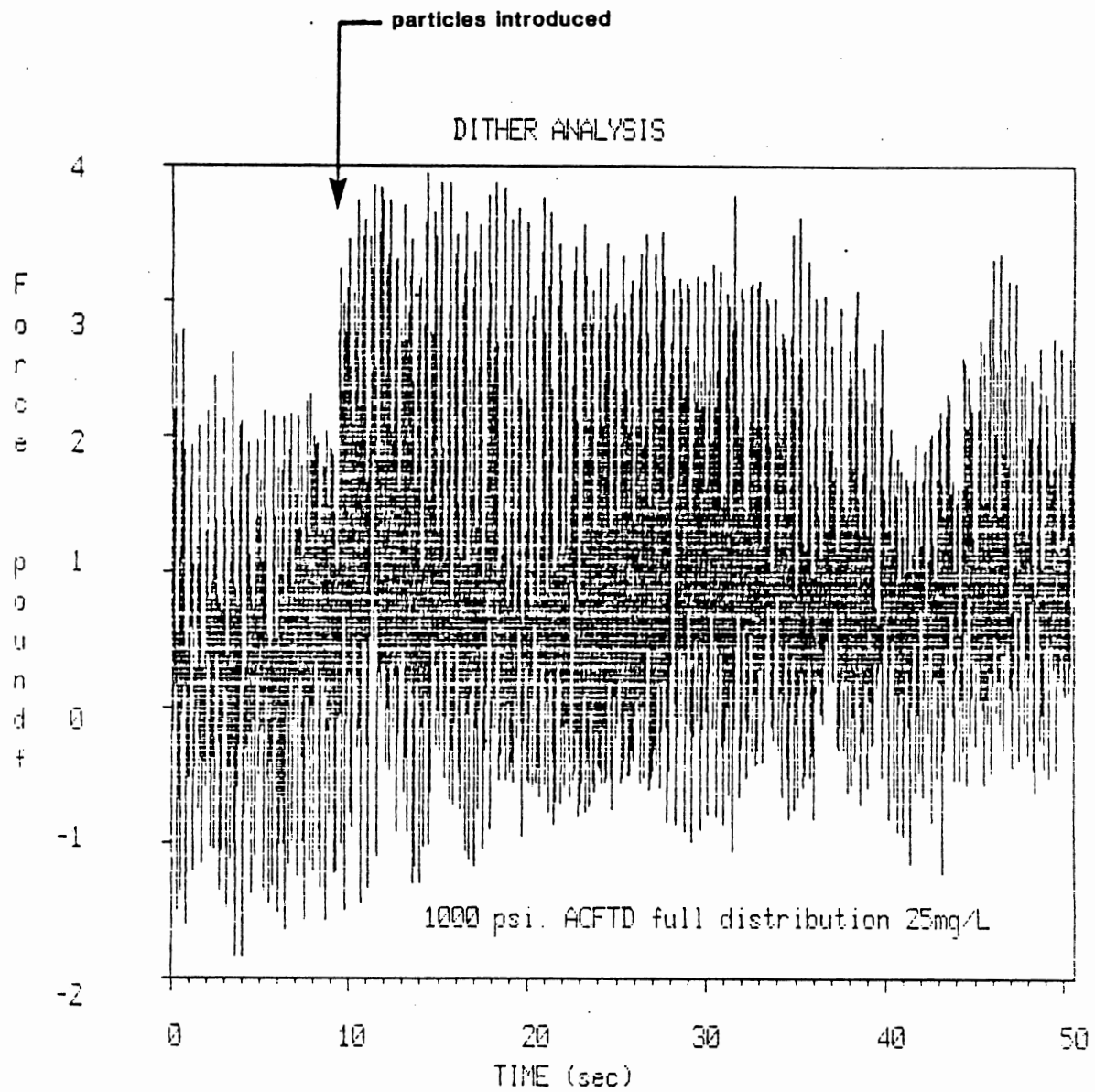


Figure 80. Dither Analysis (V).

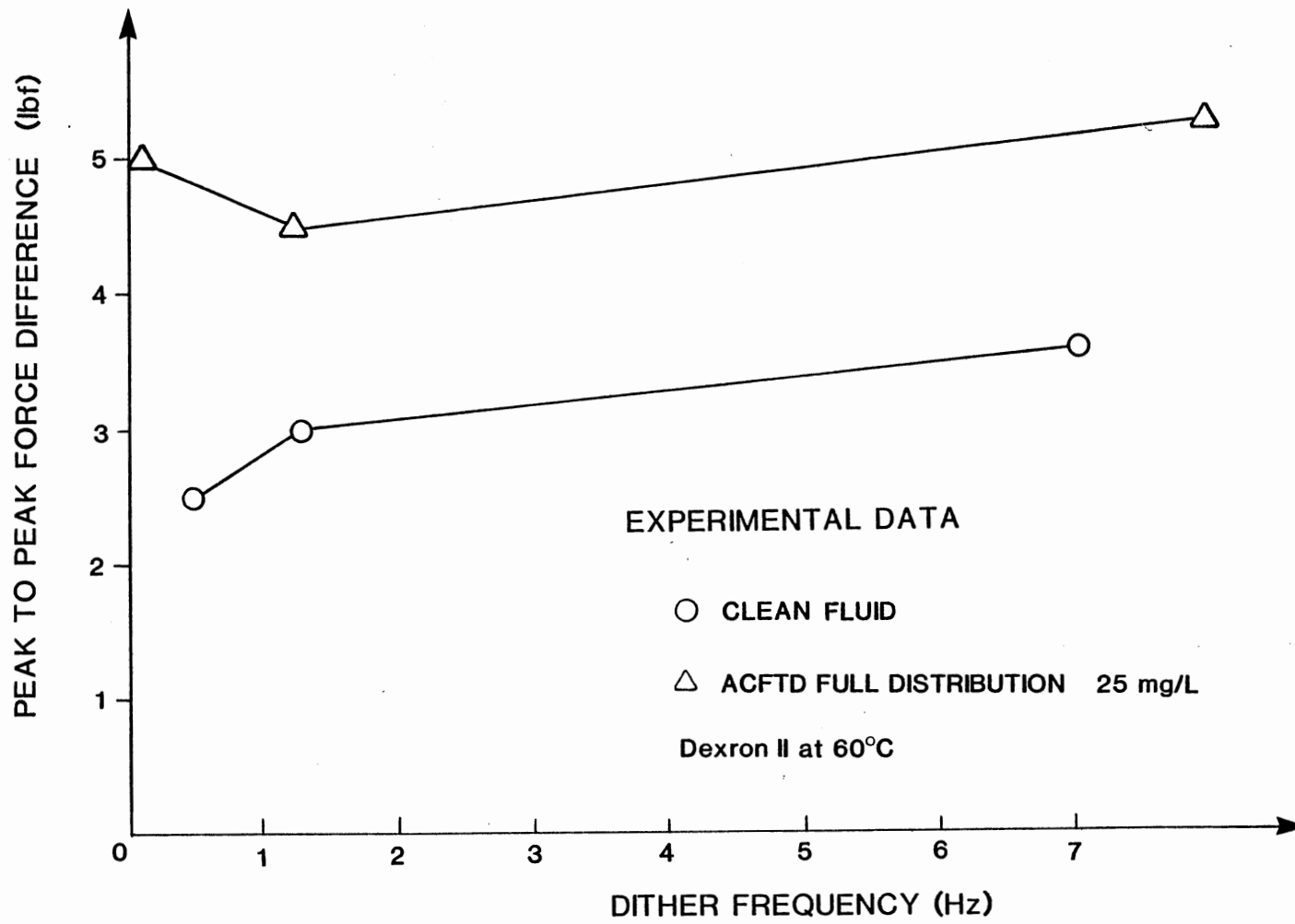


Figure 81. Friction Force Under Dither.

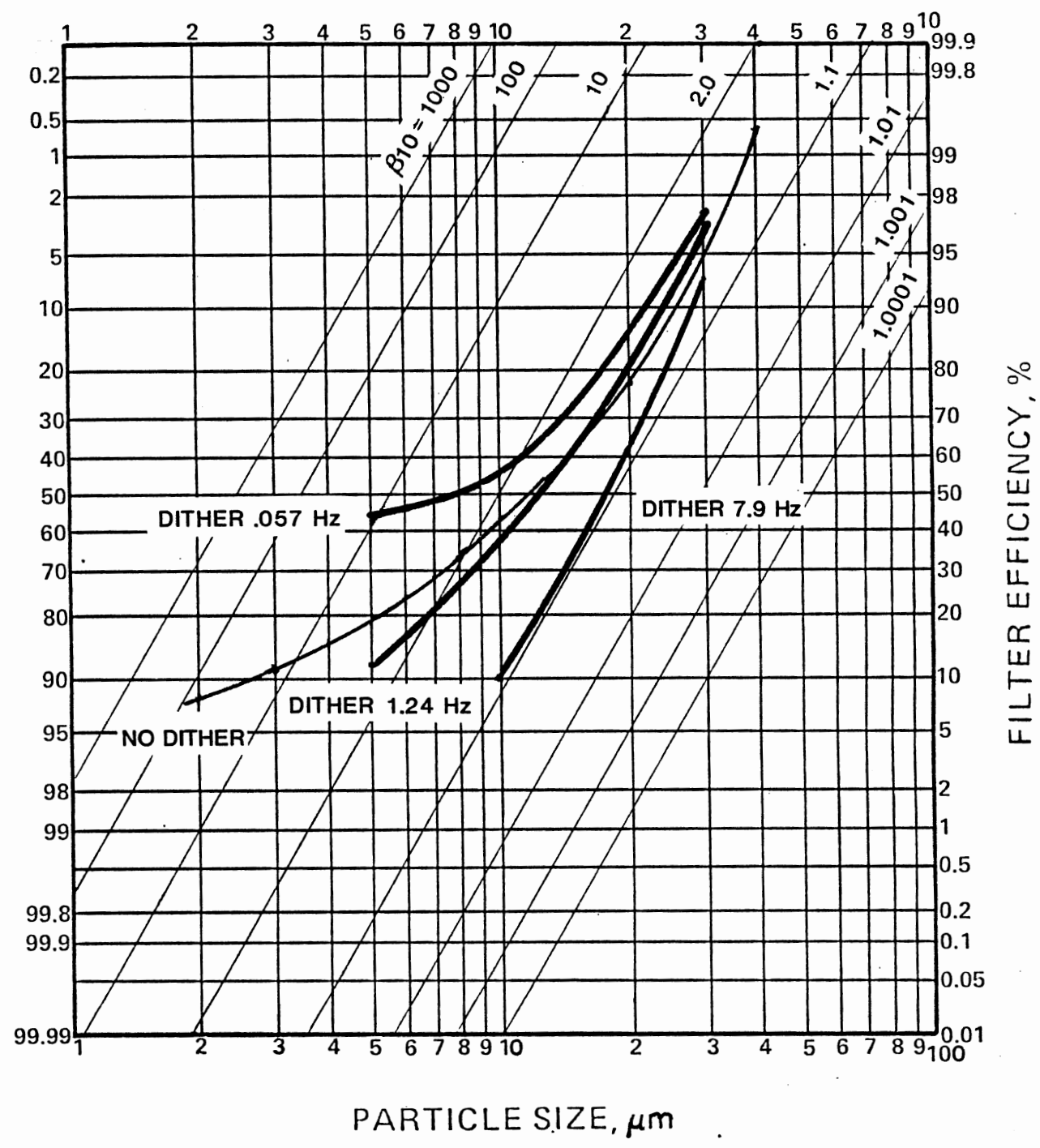


Figure 82. Effect of Dither Frequency on Filtration Efficiency.

dither. This was probably because the slow dither motion disturbed the cake formation to allow more leakage volume than the leakage under no dither. Also, the average cleanliness of the total collected leakage became cleaner than the leakage collected under no dither. Therefore, this leakage passing through the cake formation is a well filtered fluid, and so the time average downstream particle size distribution with dither showed a higher filtration efficiency than for a system without dither. However, as soon as the dither frequency exceeded 1.23 Hz, the dither motion of the piston became abrupt enough to destroy the possibility of initial cake formation or addition to the cake formation. The drastic efficiency degradation at fine particle size clearly demonstrates that there is less caking. At these high frequencies, the piston-bore assembly functioned as a poor filter. Hence, the filtration efficiency decreased as the dither frequency increased. These experimental results agree with the dither model presented in Chapter IV (Eq. 39).

The No. 23 piston was replaced by the No. 6 piston to investigate how hardness would affect the force required to actuate a piston. As Figure 83 shows, as soon as contaminated fluid was introduced into the test housing, the recorded force exhibited a "sticking" effect at the tension side with a higher peak value than for the force exhibited under a clean condition of the same assembly. At higher dither frequency, the force appeared to increase with elapsed time (Fig. 84). The peak to peak value of the force was difficult to assess with this piston-bore assembly because of unstable behavior of the system. This may be attributed to the severe wear taking place on the surface of the piston. After the

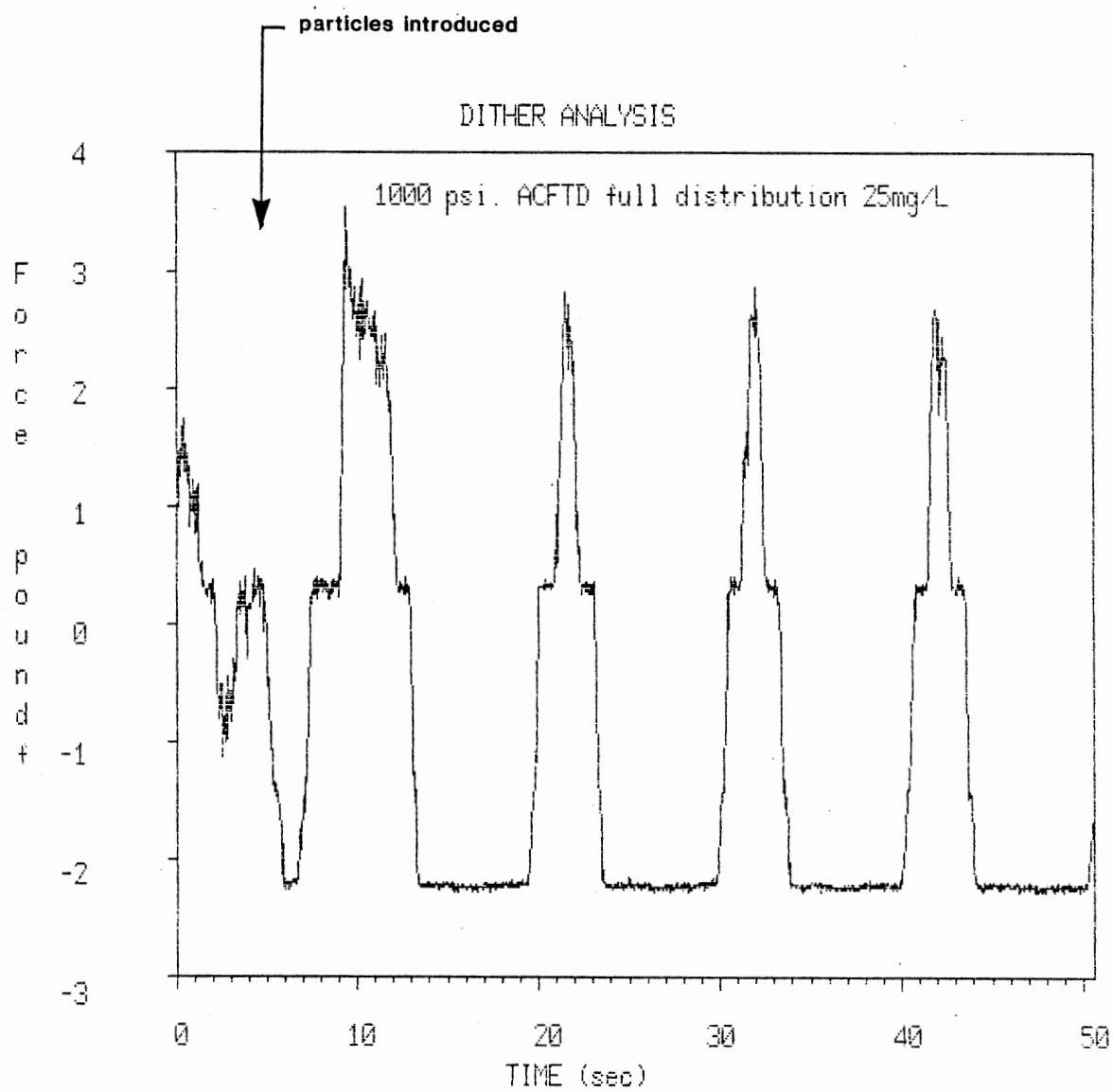


Figure 83. Dither Analysis (VI).

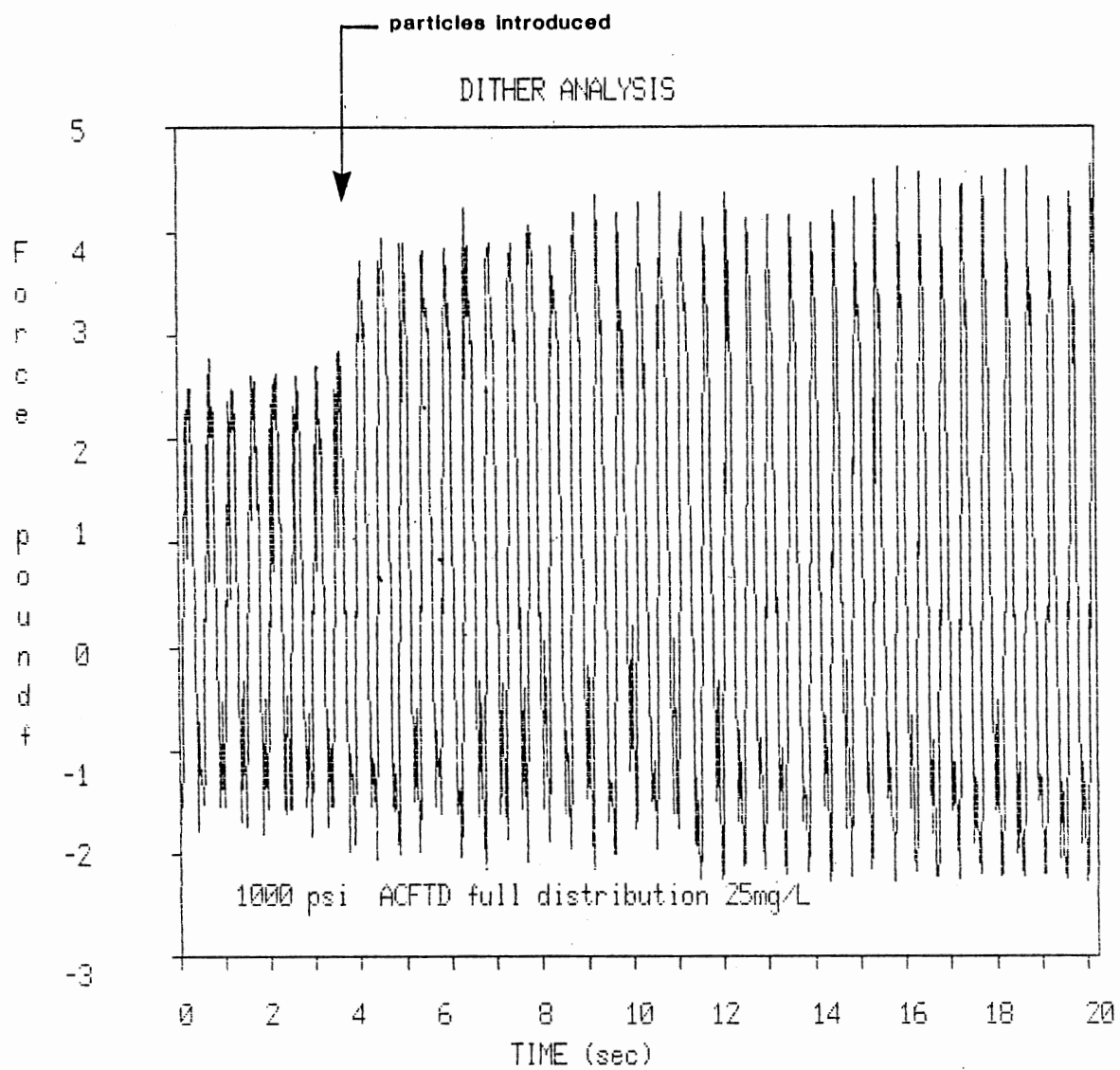


Figure 84. Dither Analysis (VII).

test, a band of wear all the way around the surface of both the No. 23 (Fig. 85) and No. 6 (Fig.86) piston was noted. Microscopic observation revealed that different wear was occurring at the upstream side compared with the downstream side surface of the piston. The difference in wear was vividly illustrated when the piston (No.²³6) is softer than ACFTD particles. There were many lateral lines created by the dither motion on the surface at the upstream side. This may have been caused by large particles indenting on the harder surface of the bore, cutting into the softer surface of the piston. In addition, there were many pits of various sizes that were created by solid particles under the influence of dither.

In contrast to the upstream side surface, the downstream side was less worn, and vertical lines caused by initial fabrication grinding were conspicuous, indicating minimal wear taking place. The observation of wear conditions at the upstream side indicates that larger particles which can bridge the clearance were stuck at the entrance region of the clearance and were causing severe wear. The silt process predicted the locally concentrated silt at the clearance entrance, and this upstream side wear on the piston surface clearly confirms the accuracy of that prediction. Furthermore, the wear shows that these large particles continued to stay at the entrance region and do not move downstream. This further indicates that particles which bridge the clearance at the entrance region significantly contribute to the seizure and provide extra surfaces for finer particles to silt and block the leakage path through the clearance.

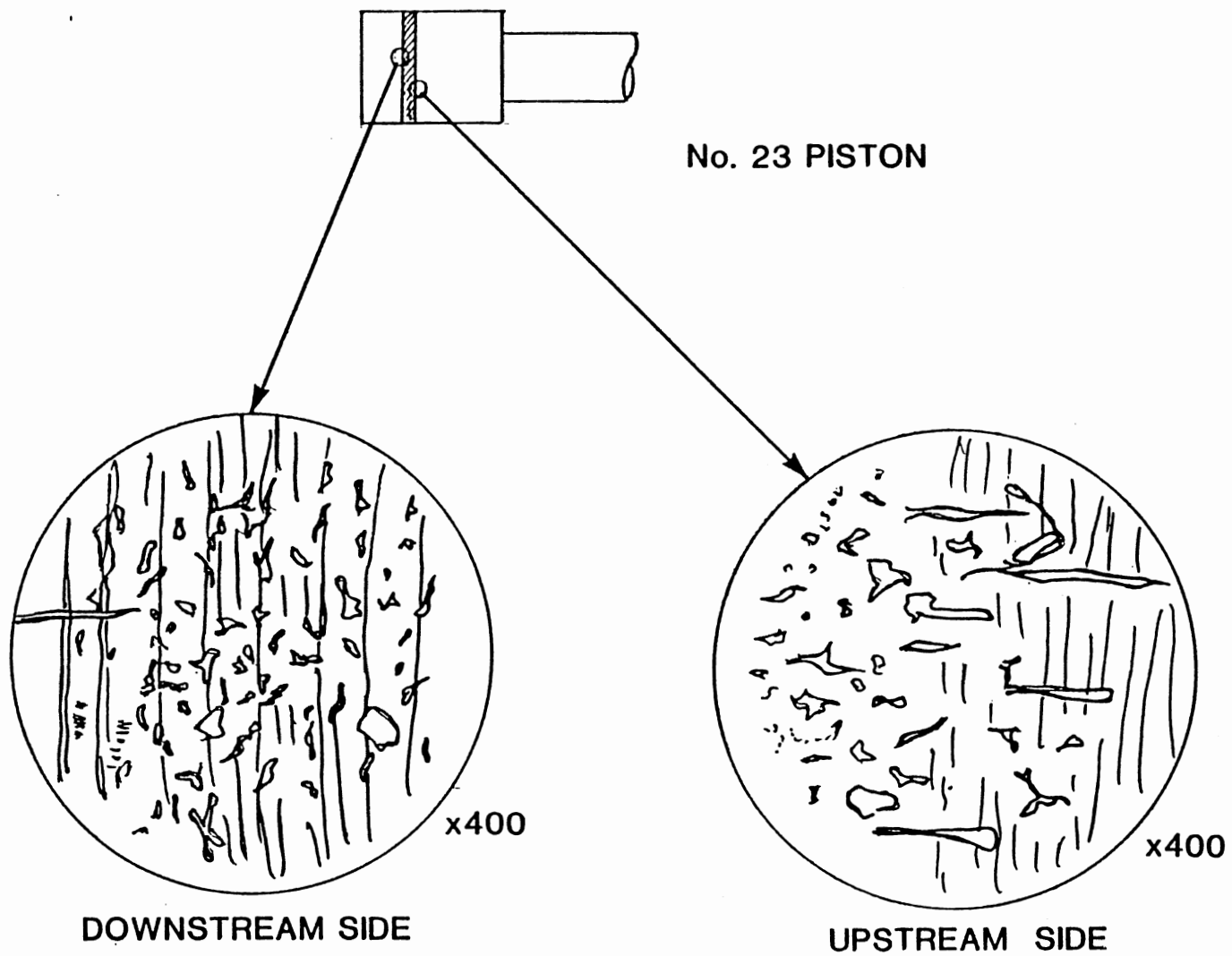


Figure 85. Microscopic Observation of Wear Caused by Dither (I).

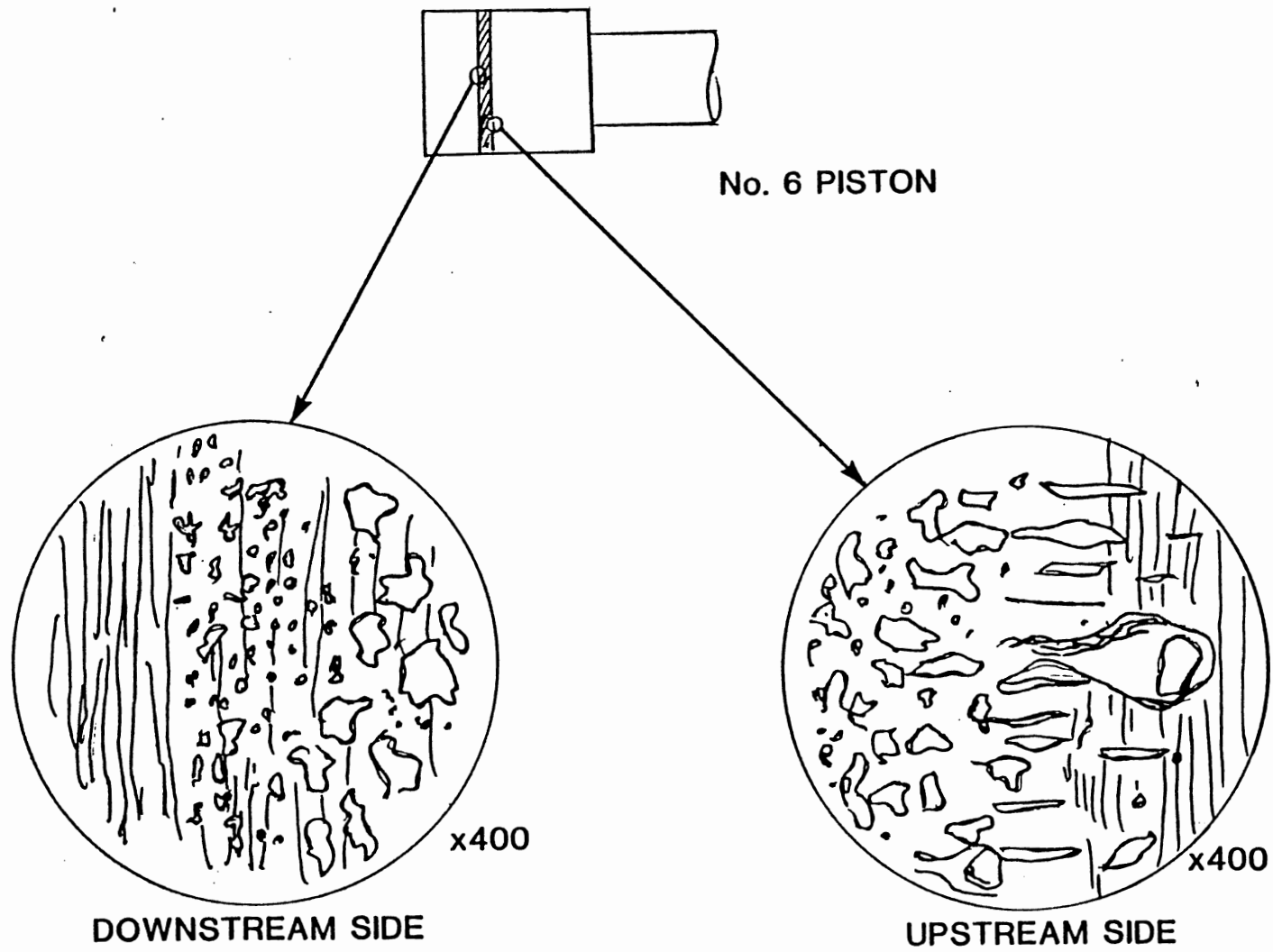


Figure 86. Microscopic Observation of Wear Caused by Dither (II).

When the piston material is softer than the particles, the serious wear on the surface of the piston discourages the application of dither. Furthermore, high frequency dither application, shown in Fig. 84, demonstrates the unpredictable and continuous uncontrollable increase in peak to peak friction force. This type of unpredictable force increase may cause catastrophic failures of the piston-bore assembly.

When the assembly materials were harder than the particles, however, very little wear was observed on the surface of the piston. The measured peak to peak force increase was stable and predictable, as presented in Fig. 81.

CHAPTER VII

SUMMARY AND CONCLUSIONS

The application of piston-bore assemblies varies from such mundane equipment as earth moving machines to as far reaching as robotics and space vehicles, and the sophistication of the assemblies has developed from the simple muscle of heavy equipment to the delicate pressure and flow control elements. Within the last decade, the control methods of these assemblies have achieved such a sophistication that they can now imitate the intricate muscle movements of living creatures. However, even with such advanced technology, particulate-induced seizure of the piston-bore assembly has hardly been understood. This lack of understanding has led to catastrophic failures and accidents in industry. Design engineers, in the past, have had no means of understanding seizure. Thus, the only solution to seizure they have had has solely been through the experience of engineers and through trial and error methods. The understanding of seizure, however, can alleviate possible catastrophic failures by allowing design engineers to predict the occurrence and magnitude of the force required to break seizure. This dissertation provides the essential tools that engineers need for predicting the force required to break seizure and thus maintain normal operation of piston-bore assemblies.

The verification tests of the three theoretical models developed in this dissertation uncovered important evidence as to the mechanisms that cause particulate-induced seizure. To analyze how particles in the clearance cause seizure, the silt process had to be understood so that the number and size of particles in the clearance prior to seizure could be known. Thus, the silt process model laid the foundation of this study.

The experimental results of the silt process model revealed that the smaller clearance of a piston-bore assembly sieves finer particles, and the long land length increases the retention (dirt holding) capability by reducing the average shear rate at the wall of the clearance. The effect of shear rate was clearly demonstrated by the leakage measurement. While the initial shear rate is low, particles smaller than the clearance size are loosely captured in the assembly clearance and effectively reduce the leakage; however, at the high initial shear rate, these particles are either flushed away or moved aside from the leakage path until the leakage reduces and approaches the low shear rate.

The verification test of the particulate-induced seizure model confirmed the integrity of the silt process model and established the means for predicting the force required to break seizure. It was found that the particles must bridge across the clearance in order to contribute to the seizure force. Furthermore, the controlling stress of the force required to break seizure is the ultimate stress of the softest material of the three interacting bodies.

After establishing the method for predicting the magnitude of the seizure force, the dither model was developed to investigate the effect of dither on the filtration efficiency of the assembly. This experiment confirmed that the higher the dither frequency, the lower the filtration efficiency. This result indicates that the vibrational effect caused by dither enhanced the dislodgement of fine particles smaller than the clearance. When the particles are softer than the assembly, the application of dither to reduce the seizure force is appropriate; however, when the particles are harder than the assembly material, the application of dither may increase the seizure force due to wear which takes place on the assembly surface.

To the author's knowledge, this dissertation has demonstrated for the first time that the occurrence and magnitude of seizure force can be predicted. The combination of the silt process model and the particulate-induced seizure model gives design engineers the capability to develop piston-bore assemblies which are seizure-free. It is firmly believed that this study advances the understanding of seizure and encourages extensive application of these models in the area of fluid power engineering.

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APPENDIX A

SEIZURE MODEL SIMULATION PROGRAM

```

100 '*****
120 '
140 '   THIS PROGRAM VERIFIES THE INTEGRITY OF THE THREE PROPOSED
160 '   MODEL.  THE DETAIL IS EXPLAINED AFTER SUBROUTINES ( LINE# 10700-).
180 '
200 '           PROGRAMMED BY TOKUNOSUKE ITO
220 '
240 '*****
260 '
280   CLS
300   CLEAR: CLEAR 1000
320   DIM CTABLE(180)
340   DIM HL(3),FM(3),FA(3),BFM(3),BFA(3),ANGLE(3),CAREA(3)
360   IBM = 0
380   IF IBM = 1 THEN GOSUB 860 ELSE GOSUB 480
400   GOTO 1140
420 '
440 '----- TANDY 2000 ---
460 '
480   KEY 11,"EDIT "
500   KEY 12,"AUTO "
520   LPRINT CHR$(27);CHR$(14):'           CONDENSED CHARACTER
540   DIMC = 0:'           To avoid the duplicate dif.
560   WIDTH LPRINT 117:'           SET PRINTER, 117chars/line
580   YOFFS = 350
600   SCS = 4
620   AY = 330:'           MAX. WIDTH OF YAXIS
640   YKON = (22-2)/(8-330)
660   YOFF = 2
680   YSET = 180
700   KB1 = 28
720   KB2 = 29
740   KB3 = 30
760   KB4 = 31
780   RETURN
800 '
820 '----- IBM HIGH RES. SETTING ---
840 '
860 '
880   YOFFS = 180
900   SCS = 2
920   AY = 170
940   YKON = (2-23)/(170-0)
960   YOFF = 0
980   YSET = 85
1000  KB1 = 54:'           AT KEY CODE
1020  KB2 = 52
1040  KB3 = 56
1060  KB4 = 50
1080 '
1100  RETURN
1120 '
1140  GOTO 19040:'JUMP TO MAIN ROUTINE
1160 '
1180 '***** HIGH RESOLUTION GRAPHICS *****
1200 '
1220  SCREEN (SCS):'           HIGHEST RESOLUTION
1240  KEY OFF:'ELIMINATE FUNCTION KEY DISPLAY
1260  RETURN
1280 '

```

```

1300 '***** END OF HIGH RESOLUTION (TURN_ON)*****
1320 '
1340 '
1360 '
1380 LINE (XD1,YD1)-(XD2,YD2),K AND &HFOF
1400 =====
1420 '
1440 SUBROUTINE
1460 '
1480 -----
1500 '
1520 XD1=X1+90:YD1=YOFFS-Y1
1540 XD2=X2+90:YD2=YOFFS-Y2
1560 LINE (XD1,YD1)-(XD2,YD2),CLR
1580 RETURN
1600 '
1620 '
1640 '**** BOX DRAWING *****
1660 '
1680 CLR=1:' COLOR CODE
1700 X1=0:Y1=0
1720 X2=510:Y2=0:GOSUB 1500
1740 X1=510:Y1=AY:GOSUB 1500
1760 X2=0:Y2=AY:GOSUB 1500
1780 X1=0:Y1=0:GOSUB 1500
1800 RETURN
1820 '
1840 '*****
1860 '
1880 '***** MAX. & MIN. *****8
1900 '
1920 '##### X-AXIS FIRST #####
1940 '
1960 IF I=SS(J) THEN K=S(I):PX=X(I,K):XMAX=PX:XMIN=PX
1980 FOR K=S(I) TO Z(I)
2000 PX=X(I,K)
2020 IF XMIN > PX THEN XMIN = PX
2040 IF XMAX < PX THEN XMAX = PX
2060 NEXT K
2080 '
2100 '----- Y-AXIS -----
2120 '
2140 IF I=SS(J) THEN K=S(I):PY=Y(I,K):YMAX=PY:YMIN=PY
2160 FOR K=S(I) TO Z(I)
2180 PY=Y(I,K)
2200 IF YMIN > PY THEN YMIN=PY
2220 IF YMAX < PY THEN YMAX = PY
2240 PRINT"YMAX ";YMAX,"YMIN ";YMIN
2260 '
2280 NEXT K
2300 '
2320 RETURN
2340 '
2360 '***** END OF MAX. & MIN. *****
2380 '
2400 '***** TITLE & AXIES LABEL CONTROL ****
2420 '
2440 '
2460 T$="TEST GRAPHING"
2480 XL$="TIME (sec)"

```



```

2500 ' YL$="OUTPUT PARAMETER"
2520 '
2540 IF LEN(T$(J))>80 THEN T$(J)=LEFT$(T$(J),80)
2560 IF LEN(XL$(J))>80 THEN XL$(J)=LEFT$(XL$(J),80)
2580 IF LEN(YL$(J))>24 THEN YL$(J)=LEFT$(YL$(J),24)
2600 N=INT((80-LEN(XL$(J)))/2):' MAINTAIN THE ORDER FOR IBM
2620 LOCATE 25,N:PRINT XL$(J)
2640 N=INT((80-LEN(T$(J)))/2)
2660 LOCATE 1,N:PRINT T$(J)
2680 M=0
2700 NM=INT((24-LEN(YL$(J)))/2)
2720 FOR N=NM TO LEN(YL$(J))+NM
2740 M=M+1
2760 LOCATE N,1:PRINT MID$(YL$(J),M,1)
2780 NEXT N
2800 RETURN
2820 '
2840 '***** END OF TITLES *****
2860 SDELTA=INT((BASE + DELTA * F)*10^(POWER+4))/(10^(POWER+4))
2880 '***** TIC MARK FOR X-AXIS *****
2900 '
2920 ' XMAX=3.2:XMIN=-1.6
2940 CLR=1
2960 AX=510:' WIDTH OF GRAPHICS
2980 POWER=0:' POWER INCREMENT TO FIND THE SPACE BETWEEN XMAX,XMIN
3000 IF XMAX >= 0 THEN SIGNMAX=1 ELSE SIGNMAX=-1
3020 IF XMIN >= 0 THEN SIGNMIN=1 ELSE SIGNMIN=1:'**** NOTE INT(-1.1)=-2
3040 LX=INT(XMAX*10^POWER + .5*SIGNMAX)
3060 SX=INT(XMIN*10^POWER + .5*SIGNMIN)
3080 DE=LX-SX
3100 ' PRINT"DE ";DE,"LX ";LX,"SX ";SX,"POWER ";POWER
3120 IF DE < 2 THEN POWER=POWER + 1:GOTO 3040
3140 IF DE > 20 THEN POWER=POWER - 1:GOTO 3040
3160 IF XMAX < LX*10^(-POWER) THEN LX=LX-1
3180 IF XMIN > SX*10^(-POWER) THEN SX=SX+1
3200 DE=LX-SX:'PRINT "DE ";DE;"POWER ";POWER;"SX ";SX
3220 DELTA = 10^(-POWER)
3240 BASE=SX*DELTA
3260 FOR F=0 TO DE
3280 SDELTA=INT((BASE + DELTA * F)*10^(POWER+4)+.5)/(10^(POWER+4))
3300 '***** GOOD ALGORITHM *****
3320 '
3340 S$=STR$(SDELTA)
3360 CK$=RIGHT$(S$,4)
3380 IF LEFT$(CK$,1) <> "E" THEN SDELTA=VAL(LEFT$(S$,5)):GOTO 3460
3400 EX=VAL(RIGHT$(CK$,2))
3420 IF MID$(CK$,2,1)="+" THEN SDELTA=VAL(LEFT$(S$,5))*10^EX
3440 IF MID$(CK$,2,1)="-" THEN SDELTA=VAL(LEFT$(S$,5))*10^(-EX)
3460 '
3480 X1=INT(AX/(XMAX-XMIN)*(SDELTA - XMIN))
3500 X2=X1:SMALL1=X1
3520 Y1=0:Y2=-5
3540 'PRINT X1,X2,Y1,Y2
3560 GOSUB 1500
3580 IF DE <=10 THEN 3640
3600 JUDGE= INT(F/2)
3620 IF F <> JUDGE*2 THEN 3800
3640 LOCATE 24,INT(X1/8)+11:PRINT ;SDELTA;:' LABELING
3660 IF F < 1 OR DE > 5 THEN 3800:' FINER RESOLUTION

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3680          DIFF=SMALL1-SMALL0
3700          FOR N=1 TO 9
3720              X1=SMALL0 + INT(DIFF/10*N+.5):X2=X1
3740              Y1=0:Y2=-2
3760              GOSUB 1500
3780          NEXT N
3800          SMALL0=SMALL1
3820      NEXT F
3840 '
3860      IF DE > 5 THEN GOTO 4340
3880 '==== UPPER END TIC MARK CONTROL =====
3900 '
3920      NUM=0
3940      NUM=NUM+1
3960      X1=SMALL1 + INT(DIFF/10*NUM+.5)
3980 ' PRINT"X1 ";X1;" SMALL1 ";SMALL1;" SMALL ";SMALL;" NUM ";NUM
4000      IF X1 >= AX THEN 4160
4020      X2=X1
4040      Y1=0:Y2=-2
4060      GOSUB 1500
4080      GOTO 3940
4100 '
4120 '==== LOWER END TIC MARK CONTROL =====
4140 '
4160      SMALL0=INT(AX/(XMAX-XMIN)*(BASE-XMIN))
4180      NUM=0
4200      NUM=NUM+1
4220      X1=SMALL0-INT(DIFF/10*NUM+.5)
4240      IF X1 =< 0 THEN GOTO 4340
4260      X2=X1
4280      Y1=0:Y2=-2:'          REDUNDANT
4300      GOSUB 1500
4320      GOTO 4200
4340      RETURN
4360 '
4380 '***** END OF X-AXIS TIC MARK *****
4400 '
4420 '***** TIC MARK FOR Y AXIS *****
4440 '
4460 '      YMAX=2.25:YMIN=-1.1:'          DUMMY VALUES
4480      CLR=1
4500      POWER=0:'          INITIALIZATION OF POWER
4520      '
4540 '
4560      LY=INT(YMAX*10^POWER + .5)
4580      SY=INT(YMIN*10^POWER)
4600      DE=LY-SY
4620      IF DE < 2 THEN POWER = POWER + 1:GOTO 4560
4640      IF DE > 20 THEN POWER = POWER - 1:GOTO 4560
4660      IF YMAX > LY*10^(-POWER) THEN LY=LY+1
4680      IF YMIN < SY*10^(-POWER) THEN SY=SY-1:'          THIS WILL BE RARE
4700      DE=LY-SY
4720      DELTA=10^(-POWER):'          THIS IS EQUIVALENT TO 1 UNIT IN GRAPH
4740      BASE=SY*DELTA:'          THIS IS THE BOTTOM VALUE OF Y-AXIS
4760      YDMAX=LY*10^(-POWER):YDMIN=SY*10^(-POWER):'          Y HAS BOUNDARY LARGER TH
AN YMAX,YMIN
4780      FOR F=0 TO DE
4800          SDELTA=INT((BASE + DELTA * F)*(10^(POWER+4))+.5)/(10^(POWER+4)):
'          INCREMENT EACH UNIT FROM BOTTOM

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4820         Y1=INT(AY/(YDMAX-YDMIN)*(SDELTA-YDMIN))
4840         Y2=Y1:SMALL1=Y1
4860         X1=0:X2=-5
4880         GOSUB 1500:'           DRAW LINE
4900         IF DE <= 10 THEN 4960:'       IF INCREMENT IS WITHIN 10,WRITE N
UMBER DIRECTLY
4920         JUDGE=INT(F/2):'           THIS IS TO WRITE EVERY OTHER TIC
MARK #
4940         IF F <> JUDGE*2 THEN 5140
4960         POSI= 23+INT(YKON*(Y1-YOFF))
4980         LOCATE POSI,4:PRINT SDELTA
5000         ' PRINT "F ";F;" POSI ";POSI;" Y1 ";Y1
5020         IF F < 1 OR DE > 5 THEN 5140
5040         DIFF=SMALL1-SMALL0
5060         FOR N=1 TO 9
5080             Y1=SMALL0 + INT(DIFF/10*N +.5):Y2=Y1:X2=-2
5100             GOSUB 1500:'**** NOTE   SPEC OF X2,X1 IGNORED
5120         NEXT N
5140         SMALL0=SMALL1
5160 '
5180 '
5200 '
5220         NEXT F
5240         YMAX=YDMAX:'           NEW YMAX VALUE
5260         YMIN=YDMIN:'           NEW YMIN VALUE FOR THE GRAPHICS PURPOSE
5280 '
5300         RETURN
5320 '
5340 '***** END OF Y-AXIS TIC MARK *****
5360 '
5380 '***** DRAWING ROUTINE *****
5400 '
5420         K=S(I)
5440         X1=INT(AX/(XMAX-XMIN)*(X(I,K)-XMIN))
5460         Y1=INT(AY/(YMAX-YMIN)*(Y(I,K)-YMIN))
5480 '
5500         FOR K=S(I)+1 TO Z(I)
5520             X2=INT(AX/(XMAX-XMIN)*(X(I,K)-XMIN))
5540             Y2=INT(AY/(YMAX-YMIN)*(Y(I,K)-YMIN))
5560 '
5580             IF I <> INT(I/2)*2 THEN CLR=1:GOTO 4500
5600             CLR=(-1)^K:CLR=(ABS(CLR)+CLR)/2
5620             CLR=1
5640             GOSUB 1500
5660             X1=X2:Y1=Y2
5680         NEXT K
5700         GOSUB 5820:'           LINE LABLING
5720         RETURN
5740 '
5760 '***** END OF DRAWING *****
5780 '
5800 '***** LINE LABEL POSITIONING *****
5820 '
5840         XSET=255
5860         A$=INKEY$:IF A$="" THEN GOSUB 6140:GOTO 5860
5880         DIS=ASC(A$)
5900         IF DIS=KB1 THEN XSET=XSET+10
5920         IF DIS=KB2 THEN XSET=XSET-10
5940         IF DIS=KB3 THEN YSET=YSET+10
5960         IF DIS=KB4 THEN YSET=YSET-10

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```

5980     IF DIS < > 32 THEN 5860
6000     POSI=23+INT(YKON*(YSET-YOFF))
6020     LOCATE POSI,INT(XSET/8)+11:PRINT NA$(J,I)
6040     RETURN
6060 '
6080 '***** END OF LINE LABEL *****
6100 '
6120 '***** FLASHING POINT *****
6140 '
6160     INDICATOR=0:'           0= DOT ON, 1= DOT OFF
6180     XFLASH=XSET + 90
6200     YFLASH=YOFFS - YSET
6220     IF POINT(XFLASH,YFLASH)=1 THEN INDICATOR=1
6240     PSET(XFLASH,YFLASH)
6260     FOR N=0 TO 10:NEXT N
6280     PRESET(XFLASH,YFLASH),0
6300     FOR N=0 TO 10: NEXT N
6320     IF INDICATOR=1 THEN PSET(XFLASH,YFLASH)
6340     RETURN
6360 '
6380 '***** END OF FLASHIBG *****
6400 '
6420 '***** DOTTING THE DATA POINT *****
6440 '
6460     FOR L=1 TO LIMIT
6480         XC = INT(AX/(XMAX - XMIN) * (XX(L) - XMIN)) + 90
6500         YC = YOFFS - INT(AY/(YMAX - YMIN) * (YY(L) - YMIN))
6520         CIRCLE(XC,YC),2
6540     NEXT L
6560     RETURN
6580 '
6600 '***** END OF DATA MARK *****
6620 '
6640 '***** GRAPHICS STARTS *****
6660 '
6680     FOR J=JS TO JEND
6700         FOR I=SS(J) TO ZZ(J)
6720             GOSUB 1940:'           MAX. & MIN.
6740         NEXT I
6760 '
6780 '
6800         GOSUB 1200:'           TURN-ON HIGH RESOLUTION SCREEN
6820         GOSUB 2440:'           TITLE OF THE GRAPH
6840         GOSUB 1660:'           SET-UP BOX
6860         GOSUB 2900:'           TIC MARK ON X-AXIS
6880         GOSUB 4440:'           TIC MARK OF Y-AXIS
6900 '
6920         FOR I = SS(J) TO ZZ(J)
6940             IF SAMPLE(0)=1 THEN GOSUB 6440
6960             GOSUB 5400:'           DRAWING ROUTINE
6980         NEXT I
7000         IF IBM = 0 THEN LPRINT CHR$(27) CHR$(19)
7020         A$=INKEY$:IF A$="" THEN 7020 ELSE A$=""
7040         IF IBM = 0 THEN LPRINT CHR$(27) CHR$(20)
7060         SCREEN(0):KEY ON
7080     NEXT J
7100 '
7120     RETURN
7140 '
7160 '***** END OF GRAPHICS *****

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7180 '
7200 '
7220 '
7240 '***** GRAPHICS CONTROL *****
7260 '
7280 ' ARRAY OF X(W,XX),Y(W,XX)
7300 '     W = MAX. DATA SET - 1
7320 '     XX = MAX. DATA POINTS - 1
7340 '
7360 ' I,J,K - CONTROL
7380 ' *** NOTE ****
7400 '     I,J,K ARE USED TO CONTROL DATA SET & POINTS
7420 '     DO NOT CHANGE IN THE MIDDLE OF GRAPHICS ROUTINE
7440 '
7460 '     J CONTROLS NUMBER OF PICTURES TO BE DRAWN
7480 '     I CONTROLS NUMBER OF DATA SETS TO BE DRAWN IN ONE GRAPH
7500 '     K CONTROLS DATA POINTS IN A DATA SET
7520 '
7540 '     FOR J=0 TO JEND
7560 '         FOR I=SS(J) TO ZZ(J)
7580 '             FOR K=S(I) TO Z(I)
7600 '                 X(I,K)
7620 '                 Y(I,K)
7640 '             NEXT K
7660 '         NEXT I
7680 '     NEXT J
7700 '
7720 '
7740 '
7760 ' -----
7780 ' ----- Print Out Routine -----
7800 ' -----
7820 ' PRINT "SIZE & NUMBER OF PARTICLES"
7840 ' C$(0)=" micron      ":C$(1) = " particles"
7860 '
7880 '
7900 ' FOR I= 1 TO XX+1 STEP 2
7920 '     LPRINT I;C$(0);Y(3,I);C$(1),I+1;C$(0);Y(3,I+1);C$(1)
7940 ' NEXT I
7960 ' RETURN
7980 '
8000 ' -----
8020 '
8040 '
8060 ' CLS: CL=15
8080 ' C$(1)="Graphics output selection"
8100 ' C$(2)="1 - Force only      "
8120 ' C$(3)="2 - Leakage only"
8140 ' C$(4)="3 - Clearance only"
8160 ' C$(5)="4 - Frequency vs. Size only"
8180 ' C$(6)="5 - Silt rate only"
8200 ' C$(7)="6 - Print Out of Freq. vs. Size"
8220 ' C$(8)="7 - All"
8240 '
8260 ' FOR RW=3 TO 10
8280 '     LOCATE RW,CL:PRINT C$(RW-2)
8300 ' NEXT RW
8320 '
8340 ' A$=INKEY$:IF A$="" THEN 8340
8360 ' A=VAL(A$):A$=""

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```

8380 IF A=1 THEN JS=4:JEND=4:GOTO 8540
8400 IF A = 2 THEN JS=0:JEND =0:GOTO 8540
8420 IF A = 3 THEN JS=2:JEND=2:GOTO 8540
8440 IF A =4 THEN JS=3:JEND=3:GOTO 8540
8460 IF A = 5 THEN JS=1:JEND=1:GOTO 8540
8480 IF A = 6 THEN GOSUB 7820:GOTO 8040
8500 IF A <> 7 THEN CLS:GOTO 8260
8520 JS=0
8540 SS(0)=0:ZZ(0)=0:' I-CONTROL
8560 S(0)=0:Z(0)=XX1:'SAMPLE(0)=1:' K-CONTROL
8580 SS(1) = 1:ZZ(1) = 1
8600 S(1)=0:Z(1)=XX1
8620 SS(2) = 2:ZZ(2) = 2
8640 S(2)=0:Z(2) = XX1
8660 SS(3) = 3:ZZ(3) = 3
8680 S(3)=0:Z(3)=XX
8700 SS(4) = 4:ZZ(4) = 4
8720 S(4)=0:Z(4)=XX
8740 '
8760 RETURN
8780 '
8800 '-----
8820 '
8840 '
8860 W=4:' W=X;X+1 IS NUMBER OF DATA SET YOU HAVE
8880 XLMT=300:' XX=?;XX-1 IS NUMBER OF ELEMENTS
8900 JEND=4:' JEND=#;#+1 DRAWINGS
8920 DIM X(W,XLMT),Y(W,XLMT):'T(XX)
8940 '
8960 '
8980 '----- AXIS LABELS -----
9000 '
9020 XL$(0)="TIME (sec)"
9040 YL$(0)="FLOW"
9060 T$(0)="LEAKAGE FLOW (mL/sce)"
9080 XL$(1)="TIME (sec)"
9100 YL$(1)="RATE OF SILT"
9120 T$(1)="CHANGE IN SILT RATE (cubic micrometer per mL of fluid)"
9140 XL$(2)="TIME (sec)"
9160 YL$(2)="CLEARANCE"
9180 T$(2)="CHANGE IN CLEARANCE DUE TO SILT (micrometer)"
9200 XL$(3)="SIZE (micrometer)"
9220 YL$(3)="FREQUENCY"
9240 T$(3)="PARTICLES RETAINED IN THE CLEARANCE"
9260 XL$(4)="FORCE (lbf)"
9280 YL$(4)="PROBABILITY"
9300 T$(4)="PROBABILITY OF FORCE REQUIRED TO BREAK SEIZURE"
9320 NA$(0,0)="Min. flow rate is "+STR$(Y(0,XX1))+ " mL/sec"
9340 NA$(1,1)="Max. silt rate is "+STR$(Y(1,XX1))
9360 NA$(2,2)="Final clearanc is "+STR$(Y(2,XX1))+ " micron"
9380 NA$(3,3)="<= Silt in the clearance"
9400 NA$(4,4)=" Max Force is "+STR$(FORCE)+" lbf"
9420 '
9440 '
9460 RETURN
9480 '
9500 '***** END OF GRAPHICS CONTROL *****
9520 '
9540 '***** MAIN PROGRAM SUBROUTINES *****
9560 '

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9580 ' ----- PRE-CALCULATION OF AREA UNDER STANDARD NORMAL CURVE --
9600 '
9620 '   DIM NORMAL(401)
9640 '   GOTO 9780
9660 '
9680 ' ----- FUNCTION TO BE INTEGRATED -----
9700 '
9720 '   F = CONST * EXP(-X*X/2)
9740 '   RETURN
9760 '
9780 '
9800 '   PI = 3.1415927#
9820 '   FX = .5           : '       AT X=0 ,FX=0.5
9840 '   NORMAL(0) = FX
9860 '   H = .01
9880 '   CONST = 1/SQR(2*PI)
9900 '
9920 '   CLS:LOCATE 12,5:PRINT "wait a minute"
9940 '   FOR J=0 TO 4 STEP H
9960 '       P = J * 100
9980 '       X = J
10000 '       GOSUB 9700
10020 '       K1 = H*F
10040 '       X=J+H/2
10060 '       GOSUB 9700
10080 '       K2 = H*F
10100 '       K3 = K2
10120 '       X = J + H
10140 '       GOSUB 9700
10160 '       K4 = H * F
10180 '       FX = FX + (K1 + 2*K2 + 2*K3 +K4)/6
10200 '       NORMAL(P+1) = FX
10220 '       PRINT P,NORMAL(P)
10240 '   NEXT J
10260 '
10280 '   RETURN
10300 '
10320 ' -----
10340 '
10360 ' ----- reassignment of Variables -----
10380 '
10400 '   H0 = R(1):D=R(2):PU=R(3):PD=R(4):L=R(5):SYP=R(6):SYB=R(7):SYS=R(8)
10420 '   S=R(9):G=R(10):BETA=R(11):ECC=R(12):DT=R(13):TSET=R(14)
10440 '   GLN=R(15):GL=R(16)
10460 '   RETURN
10480 '
10500 ' -----
10520 '
10540 ' ----- PRINT STATEMENTS -----
10560 '
10580 '   LOCATE RW,CL:PRINT B$;VR
10600 '   RETURN
10620 '
10640 ' -----
10660 '
10680 '
10700 ' ----- INITIALIZATION & ASSIGNMENT OF PARAMETER -----
10720 '
10740 '   The required inputs
10760 '

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10780 '      HO      ;      initial clearance
10800 '      D      ;      inner dia. of the bore (in.)
10820 '      MU      ;      absolute viscosity (lbf * sec^2 / in. )
10840 '      PU      ;      upstream pressure (psi)
10860 '      PD      ;      downstream pressure (psi)
10880 '      L      ;      silt land length (in)
10900 '      SYP     ;      Yield Strength of Particle (lbf/in^2)
10920 '      SYB     ;      Yield Strength of Bore (lbf/in^2)
10940 '      SYS     ;      Yield Strength of Spool (lbf/in^2)
10960 '
10980 ' ***** PARTICLE SIZE DISTRIBUTION INFORMATION *****
11000 '
11020 ' <Upstream>
11040 '      NTU     ;      number of particle greater than 1 micrometer in
11060 '                  1 mg/L of ACFTD
11080 '      BU     ;      slope of particle size distribution in log - lo
11100 '                  g
11120 '      G      ;      normal
11140 '                  gravimetric level (mg/L)
11160 ' <Downstream>
11180 '      NTD     ;      number of particle greater than 1 micrometer in
11200 '                  1 mg/L of ACFTD
11220 '      BD     ;      slope of particle size distribution in log - lo
11240 '                  g
11260 '                  normal
11280 ' -----
11300 '
11320 ' ----- initialization -----
11340 '
11360 '      HO = 25      :' micrometer
11380 '      D  = 6.355/25.4 :' inches
11400 '      MU = 2.889E-06 :' lbf*sec/in^2 (Dexron II at 80 C => 20 centistokes)
11420 '
11440 '      PU = 190     :' lbf/in^2
11460 '      PD = 10      :' lbf/in^2
11480 '      L  = .25     :' rough estimate
11500 '      SYP = 58000! :' yield strength of particle
11520 '      SYB = 10000  :' yield strength of bore
11540 '      SYS = 30000  :' yield strength of spool
11560 '      MI = .0001/2.54 :' converts micrometer to inch
11580 '      S  = 1       :' shape factor
11600 '      G  = 50      :' mg/L
11620 '      BETA = 2     :' (Nu/Nd)
11640 '      ECC = 1     :' (0<= ECC <=1) Eccentricity
11660 '      T  = 0      :' (sec)
11680 '      DT = 6      :' (time step)
11700 '      I  = 0      :' counter
11720 '      TSET = 60   :' sec;
11740 '      CIML = 2.54^3 :' cubic inches to milli-liter
11760 '      GLN = 0     :' number of grooves
11780 '      GL  = .01   :' average length of grooves (inches)
11800 '      HS = 400   :' hardness of spool (Brinell)
11820 ' -----
11840 '
11860 '

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11880 | ----- ASSIGNMENTS -----
11900 |
11920 |   DIM R(17)
11940 |   R(1) = H0:R(2)=D:R(3)=PU:R(4)=PD:R(5)=L:R(6)=SYP
11960 |   R(7)=SYB:R(8)=SYS:R(9)=S:R(10)=G:R(11)=BETA:R(12)=ECC
11980 |   R(13)=DT:R(14)=TSET:R(15)=GLN:R(16)=GL
12000 |
12020 | -----
12040 |
12060 |
12080 |
12100 |
12120 |   DIM C$(20)
12140 |
12160 |   CLS
12180 |   LOCATE 2,25:PRINT"MENU"
12200 |   C$(1)="1 --- H0 : initial clearance micrometer      "
12220 |   C$(2)="2 --- D  : inner dia. of the bore inches      "
12240 |   C$(3)="3 --- PU : Upstream pressure lbf/in^2         "
12260 |   C$(4)="4 --- PD : Down stream pressre lbf/in^2      "
12280 |   C$(5)="5 --- L  : Silt land length in inches         "
12300 |   C$(6)="6 --- SYP: Yield strength of particle lbf/in^2 "
12320 |   C$(7)="7 --- SYB: Yield Strength of Bore lbf/in^2    "
12340 |   C$(8)="8 --- SYS: Yield Strength of Spool lbf/in^2  "
12360 |   C$(9)="9 --- S  : shape factor                      "
12380 |   C$(10)="10--- G  : Concentration mg/L                "
12400 |   C$(11)="11--- BETA : Retention characteristic (Nu/Nd) "
12420 |   C$(12)="12--- ECC: (0<= ECC <=1) Eccentricity       "
12440 |   C$(13)="13--- DT : Time step in sec.                 "
12460 |   C$(14)="14--- TSET : Total length of time. (sec)     "
12480 |   C$(15)="15--- GLN : Total number of grooves          "
12500 |   C$(16)="16--- GL : The average length of grooves (in.) "
12520 |   CL=10
12540 |   FOR RW=4 TO 19
12560 |       B$=C$(RW-3):VR=R(RW-3)
12580 |       GOSUB 10560
12600 |   NEXT RW
12620 |
12640 |   PRINT" **** Do you want change the value (Y/N)"
12660 |   A$=INKEY$:IF A$="" THEN 12660
12680 |   IF A$="n" OR A$="N" THEN A$="":GOTO 12780
12700 |   INPUT" ---- type in the number of the parameter you want to change";CHOI
12720 |   CE
12740 |   INPUT" ---- type in the new value";R(CHOICE)
12760 |   GOSUB 10380:GOTO 12140
12780 |   RETURN
12800 |
12820 |
12840 |   ----- CALCULATION OF THE VOLUME OF A GIVEN PARTICLE SIZE
12860 |   ----- DISTRIBUTION
12880 |
12900 |   <INPUT>          NT & B
12920 |   <OUTPUT>         V
12940 |   <Variable>      UPL ---- Upper Limit
12960 |                   NOA ---- Area Under Normal Distribution
12980 |
13000 |   UPL = 3/SQR(2*B)
13020 |   UPL = INT(UPL * 100 + .5)
13040 |   IF UPL > 400 THEN NOA = 1 ELSE NOA = NORMAL(UPL)

```

```

13060 '
13080   V = PI*NT*(1+3*SQR(PI/B)*EXP(9/4/B)*NOA)/6/S
13100   RETURN
13120 '
13140 '-----
13160 '
13180 ' ***** TABLE OF PROBABILITY FOR CLEARANCE AREA *****
13200 '
13220   F = SQR(RAD^2 + EXE^2 - 2*RAD*EXE*COS(TH)) - RADS      (32)
13240   RETURN
13260 '
13280 '-----
13300 '
13320 '----- INITIALIZATION -----
13340 '
13360   DIM CTABLE(180)
13380   CLS:PRINT"MAKING A TABLE. IT WILL SOON BE OVER !"
13400   IM = 2.54 * 10000:'      INCHES TO MICRON
13420   RAD = D*IM/2
13440   RADS = .5*(D*IM - 2*H0)
13460   EXE = H0 * ECC
13480   H = PI/180
13500 '
13520 '
13540   FOR J=0 TO 180
13560       LOCATE 1,60:PRINT J
13580       THETA = J*H
13600       TH = THETA
13620       GOSUB 13200
13640       K1 = H*F
13660       TH = THETA + H/2
13680       GOSUB 13200
13700       K2 = H*F
13720       K3 = K2
13740       TH = THETA + H
13760       GOSUB 13200
13780       K4 = H * F
13800       FX = FX + (K1+2*K2+2*K3+K4)/6
13820       CTABLE(J) = FX
13840       PRINT J,THETA,CTABLE(J)
13860   NEXT J
13880 '
13900   MAXAREA = CTABLE(180)
13920 '
13940   RETURN
13960 '
13980 '*****
14000 '
14020 '----- BINARY SEARCH -----
14040 '
14060   FR = (BETA*GM)^(KCON*KON1)/GM-KCON*LOG(BETA*GM)/BU -1
14080   RETURN
14100 '
14120 '-----
14140 '
14160 '
14180 '----- PRELIMINARY CALCULATIONS ----
14200 '
14220 '
14240   NTU = 1751.9      :' particles/ 1 mg/L of ACFTD

```

```

14260 NTU = NTU * G
14280 BU = (LOG(NTU) - LOG(2.869*G))/(LOG(40))^2: ' 2.869 particles- 40 micr
on / mg/L of ACFTD
14300 DP = PU - PD      : '      pressure difference
14320 HT = H0          : '      (HT is variable)
14340 L = L - GLN * GL : '      reduction of effective silt land
14360 ' ----- BINARY SEARCH
14380 LGAM = 1/BETA
14400 D = 2
14420 KON1 = (LOG(D))^2
14440 EPSILON = .000001
14460 GL = LGAM
14480 GU = .999
14500 '
14520 ' -----
14540 '
14560 '
14580 ' ----- CALCULATION OF THE LEAKAGE FLOW
14600 '
14620 Q = (PI*D*(1+1.5*ECC)*DP)/(12*MU*L)*((HT*MI)^3)
14640 Q = Q * CIML      : ' converts to milli-liter
14660 '
14680 ' ----- UPSTREAM VOLUME -----
14700 '
14720 NT = NTU
14740 B = BU
14760 GOSUB 12980
14780 VU = V
14800 '
14820 ' ----- DOWNSTREAM VOLUME -----
14840 '
14860 '          Calculate number of particles at the size HT with
14880 '          particle capture (retention) efficiency BETA
14900 '
14920 ' ----- BINARY SEARCH FINDS THE APPROPRIATE NTD,BD,GAMMA
14940 '
14950 GU = .999:GL = 1/BETA
14960 KCON = 1/(LOG(HT))^2
14980 XO = KCON * KON1
15000 '
15020 GM = GU
15040 GOSUB 14040
15050 ' LOCATE 9,10:PRINT"UP  ";GU,"DOWN ";GL,"ERROR ";FR
15060 ' IF FR>0 THEN GU = (1+GU)/2:GOTO 15020
15080 '
15100 GM = (GL+GU)/2
15120 GOSUB 14040
15140 ' IF ABS(FR) < EPSILON THEN 15240
15160 ' IF FR > 0 THEN GL=GM
15180 ' IF FR < 0 THEN GU = GM
15190 ' LOCATE 10,10:PRINT"UP  ";GU,"DOWN ";GL,"ERROR ";FR
15200 ' GOTO 15100
15220 '
15240 UGAM = GM
15260 GAMMA = LGAM+.9*(UGAM-LGAM)
15270 LOCATE 10,10:PRINT"FINAL GAMMA  ";GAMMA
15280 NTD = GAMMA * NTU
15300 BD = BU + LOG(GAMMA * BETA)*KCON
15320 '
15340 NT = NTD

```

```

15360 B = BD
15380 GOSUB 12980
15400 VD = V
15420 '
15440 ' ----- REMAINED VOLUME
15460 '
15480 VT = VU-VD      :' Cubic micrometer retained / ml of fluid passed clear
ance
15500 '
15520 ' ----- TOTAL SILTED VOLUME
15540 '
15560 SILT = VT * Q * DT * MI^3
15580 '
15600 ' ----- SILT HEIGHT
15620 '
15640 EPSI = (SILT/(2*PI*L*(D-HT*MI)))/MI
15660 '
15680 GOTO 12300
15700 ' ----- FREQUENCY VS SIZE
15720 '
15740 IF FIRST =1 THEN GOTO 15840
15760 FIRST =1
15780 FOR IP = 1 TO 100
15800     X(3,IP-1) = IP
15820 NEXT IP
15840 '
15860 FOR IP = 1 TO 100
15880     FUD = 2*NTU*BU*LOG(IP)/IP*EXP(-BU*(LOG(IP))^2)
15900     FDD = 2*NTD*BD*LOG(IP)/IP*EXP(-BD*(LOG(IP))^2)
15920     TMP = FUD - FDD
15940     IF TMP <0 THEN TMP = 0
15960     Y(3,IP-1) = TMP*Q*DT + Y(3,IP-1)
15980     LOCATE 2,5:PRINT I,IP
16000 NEXT IP
16020 '
16040 ' ----- STORE THE VALUES
16060 '
16080 X(0,I) = T
16100 X(1,I) = X(0,I)
16120 X(2,I) = X(1,I)
16140 '
16160 Y(0,I) = Q      :' (ml/sec)
16180 Y(1,I) = VT    :' (cubic micrometers / ml of fluid)
16200 Y(2,I) = HT
16220 ' PRINT Q;" ML/SEC ",VT;" MICRON^3/ML",HT;" MICRON",EPSI" SILT micron"
16240 ' STOP
16260 '
16280 ' ---- INCREMENT STEP
16300 '
16320 I = I +1
16340 D = D-2*EPSI*MI
16360 HT = HT - 2*EPSI
16380 T = T+DT
16400 '
16420 IF HT < 1 THEN 17220
16440 IF T<= TSET THEN 14600
16460 '
16480 ' ***** FORCE CALCULATION *****
16500 '
16520 GOTO 17220 :' SKIP SUBROUTINE

```

```

16540 ' ----- STEP TO CALCULATE FORCE -----
16560 '
16580 XINT = (RAD*RAD + EXE*EXE - (SIZEX + RADS)^2)/(2*RAD*EXE)
16600 IF XINT = 1 THEN THAI = 0:RETURN
16620 IF XINT = -1 THEN THAI = PI:RETURN
16640 THAI = -ATN(XINT/SQR(-XINT*XINT+1)) + PI/2
16660 RETURN
16680 '
16700 FOR I = SEL TO 3
16720     SIZEX = HL(I) * P
16740     GOSUB 16560
16760     ANGLE(I) = THAI
16780 NEXT I
16800 '
16820 SLP = (TMP-HL(SEL-1))/(HL(SEL)-HL(SEL-1))
16840 BFM(SEL-1)=(FM(SEL)-FM(SEL-1))*SLP + FM(SEL-1)
16860 BFM(SEL-1) = (BFM(SEL-1)+FM(SEL))/2
16880 BFA(SEL-1)=(FA(SEL)-FA(SEL-1))*SLP + FA(SEL-1)
16900 BFA(SEL-1) = (BFA(SEL-1)+FA(SEL))/2
16920 '
16940 RETURN
16960 '
16980 ' -----
17000 '
17020 TMP = PCK/P:ANGLE(0)=PI
17040 IF (TMP > HL(1)) AND (TMP < HL(0)) THEN SEL=1:GOSUB 16700:RETURN
17060 IF TMP>=HL(2) AND TMP<HL(1) THEN SEL=2:ANGLE(1)=PI:GOSUB 16700:RETURN
17080 IF TMP>HL(3) AND TMP<HL(2) THEN SEL=3:ANGLE(2)=PI:ANGLE(1)=PI:GOSUB 167
00:RETURN
17100 IF TMP = HL(3) THEN ANGLE(3) = PI:ANGLE(2)=PI:ANGLE(1)=PI
17120 RETURN
17140 '
17160 ' -----
17180 '
17200 ' ----- Initialization -----
17220 '
17240 DIM HL(3),FM(3),FA(3),BFM(3),BFA(3),ANGLE(3),CAREA(3)
17260 TH = ATN(1/1.49)
17280 '
17300 HL(0) = 1           : '      H/L ratio
17320 HL(1) = .8524232
17340 HL(2) = .7048464
17360 HL(3) = .557269
17380 '
17400 FM(3) = .1116427
17420 FM(2) = 6.756162E-02
17440 FM(1) = 2.633637E-02
17460 FM(0) = 0
17480 '
17500 FA(3) = 7.819522E-02
17520 FA(2) = .0363837
17540 FA(1) = 9.836434E-03
17560 FA(0) = 0
17580 '
17600 IF SYP> SYB THEN SYC=SYB ELSE SYC=SYP
17620 IF SYP> SYS THEN SYI=SYS ELSE SYI=SYP
17640 '
17660 ' -----
17680 '
17700 '

```

```

18840      Y(4,I)=EXP(-(X(4,I)-FORCEA)^2/2/SIGMA^2)/SIGMA/SQR(PI*2)
18860 NEXT I
18880 '
18900 '
18920      LPRINT "TOTAL MAX. FORCE = ";FORCE,"TOTAL AVG. FORCE = ";FORCEA
18940 RETURN
18960 '
18980 '-----
19000 '
19020 ***** MAIN PROGRAM CONTROL *****
19040 '
19060      GOSUB 9600:'      TABLE OF AREA UNDER NORMAL CURVE
19080      GOSUB 11340:'   PARAMETER INITIALIZATION & REASSIGNMENTS
19100 '
19120      FIRSTRUN = FIRSTRUN + 1
19140      XXI = INT(TSET/DT + .5):XX=99
19160      IF XXI<=300 THEN 19260
19180      PRINT" ***** TOO MANY ITERATIONS *****"
19200      PRINT" INCREASE TIME STEP OR DECREASE LENGTH OF TIME"
19220      PRINT" PRESS ANY BAR "
19240      A$ = INKEY$:IF A$="" THEN 19240:GOTO 260
19260 '
19280      GOSUB 13340:'   TABLE OF AREA UNDER CLEARANCE
19300      CLS
19320      LOCATE 5,10:PRINT" TOTAL NUMBER OF SILT PROCESS ITERATION ";(XX
1+1)*(XX+1)
19340 '
19360      IF FIRSTRUN >=2 THEN 19400
19380      GOSUB 8840:'    ARRAY SPACE ALLOCATION
19400      GOSUB 14240:'  MEAT
19420      GOSUB 8040:'   SET GRAPHICS PARAMETER
19440      GOSUB 9320:'   GET MAX FORCE
19460      GOSUB 6660:'   JUMP TO GRAPHICS CONTROL
19480      JEND =4:'      Recovery from J - Control of graphics
19500 '
19520 '
19540      LOCATE 5,10:PRINT " FORCE REQUIRED TO BREAK SEIZURE IS ";FORCE,"lbf"
19560      PRINT
19580      PRINT"          A --- Back to the graphics"
19600      PRINT"          B --- Try other parameters"
19620      PRINT"          Q --- QUIT"
19640      PRINT"
19660      PRINT"          Please select your choice (A or B)"
19680      A$=INKEY$:IF A$="" THEN 19680
19700      IF A$="a" OR A$="A" THEN GOTO 19420
19720      IF A$="b" OR A$="B" THEN GOTO 19820
19740      IF A$="q" OR A$="Q" THEN END
19760      CLS:GOTO 19560
19780 '
19800 '----clean up --
19820 '
19840      I=0:T =0
19860      FOR IP= 1 TO 100
19880          Y(3,IP-1)=0
19900      NEXT IP
19920 '
19940      GOSUB 12160:GOTO 19100
19960 '
19980 PRINT "ERROR CODE ";ERR,"OCCUR AT THE LINE";ERL

```

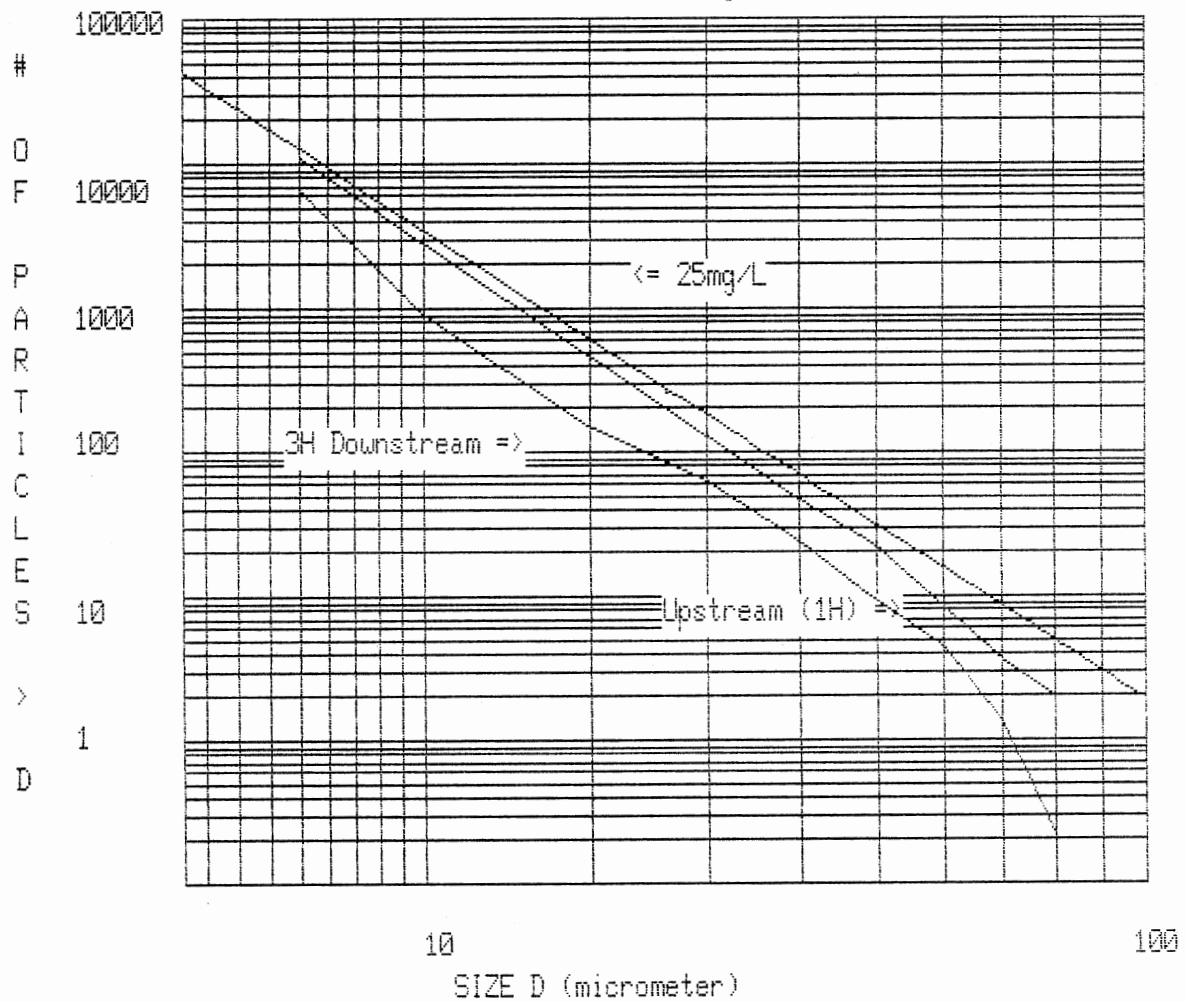
APPENDIX B
SILT BETA ANALYSIS

***** 1 & 3H TEST RESULT *****

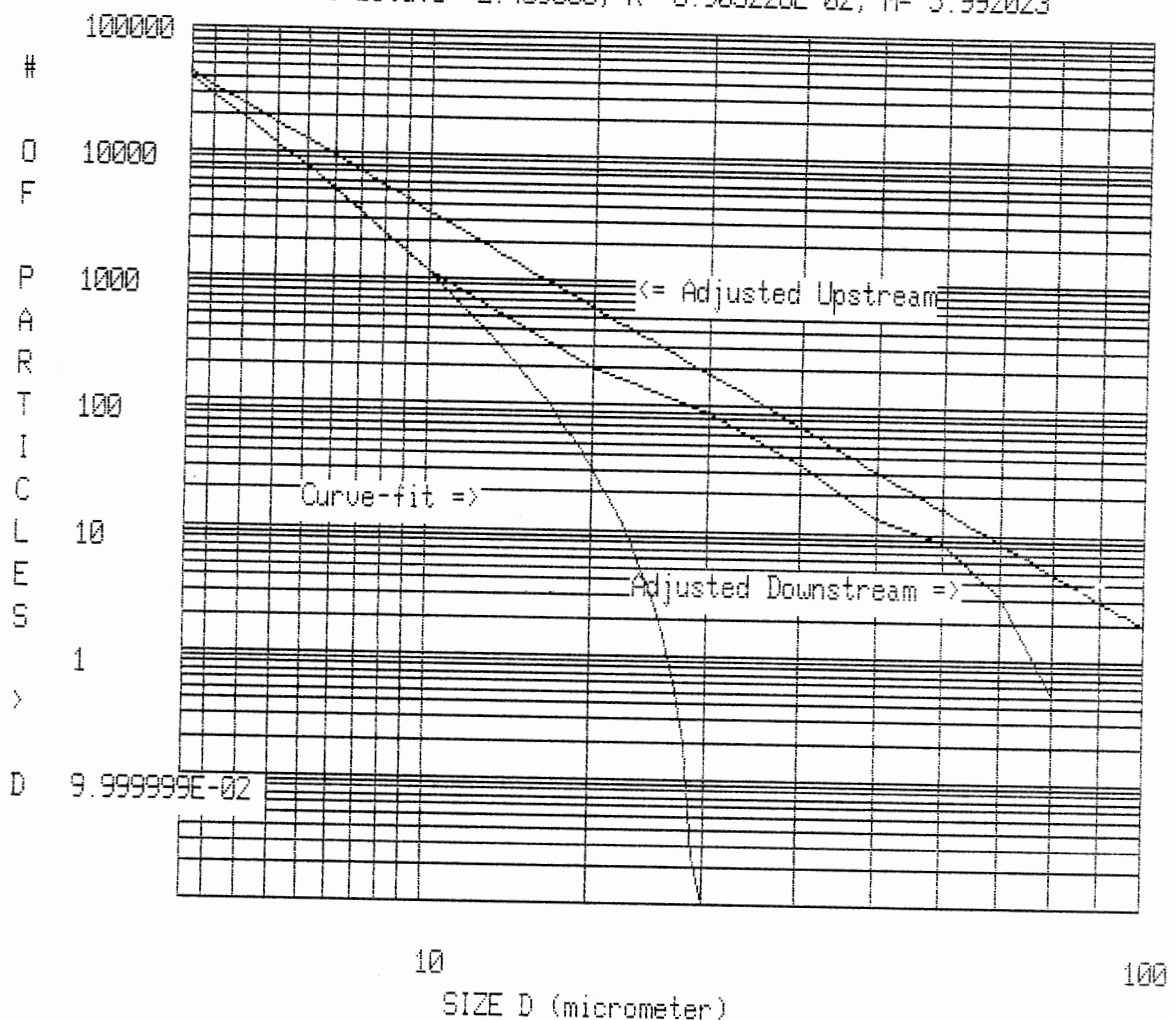
Bore No.3 - Piston No.19, Land Length (6.38 mm)
 5 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	11008.8	6781.337	1.623397
10	3597.918	2878.8	944.0335	3.049468
20	637.1161	487.1	154.7208	3.148252
30	187.6002	132.4	63.5448	2.083569
40	71.72498	48.5	24.36	1.990969
50	32.244	22.4	9.514321	2.354346
60	16.20372	8.729999	4.64232	1.880525
70	8.837601	3.81	1.392	2.737069
80	5.133417	2.09	.231768	9.017638

Downstream Beta Analysis



Piston-Bore Beta.U= 2.409883; R=-8.903226E-02; M= 5.992023



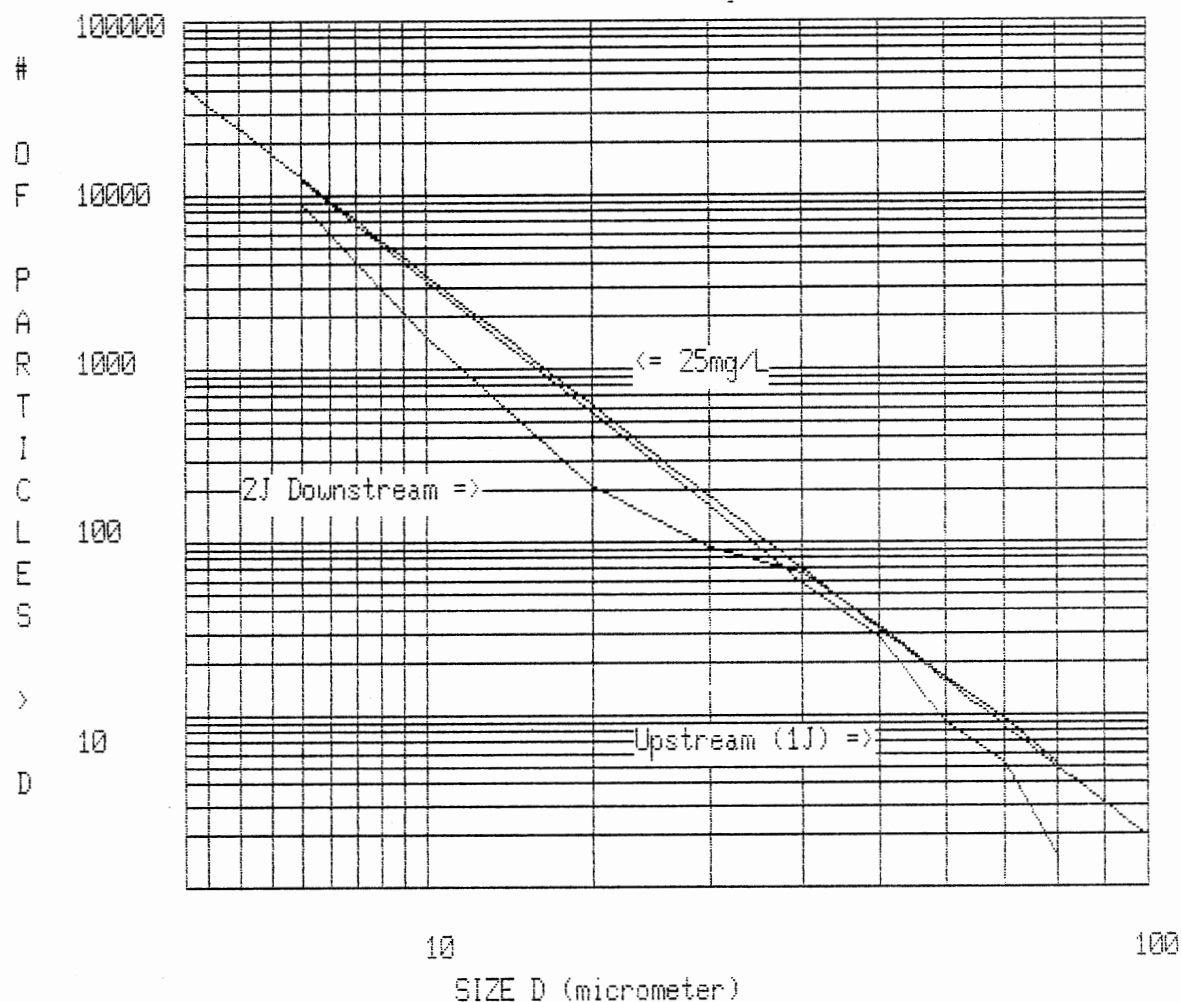
Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	39570.05	1.106835
5	12917.2	7956.898	1.623396
10	3597.918	1179.851	3.049467
15	1380.819	209.2399	6.599215
20	637.1161	33.72313	18.89256
25	331.3792	2.987863	110.9084
30	187.6002	.01	****
35	113.1623	.01	****
40	71.72498	.01	****
45	47.30807	.01	****
50	32.244	.01	****
55	22.59059	.01	****
60	16.20372	.01	****
65	11.86098	.01	****
70	8.837601	.01	****
75	6.688775	.01	****
80	5.133417	.01	****
85	3.989182	.01	****
90	3.135055	.01	****
95	2.489046	.01	****

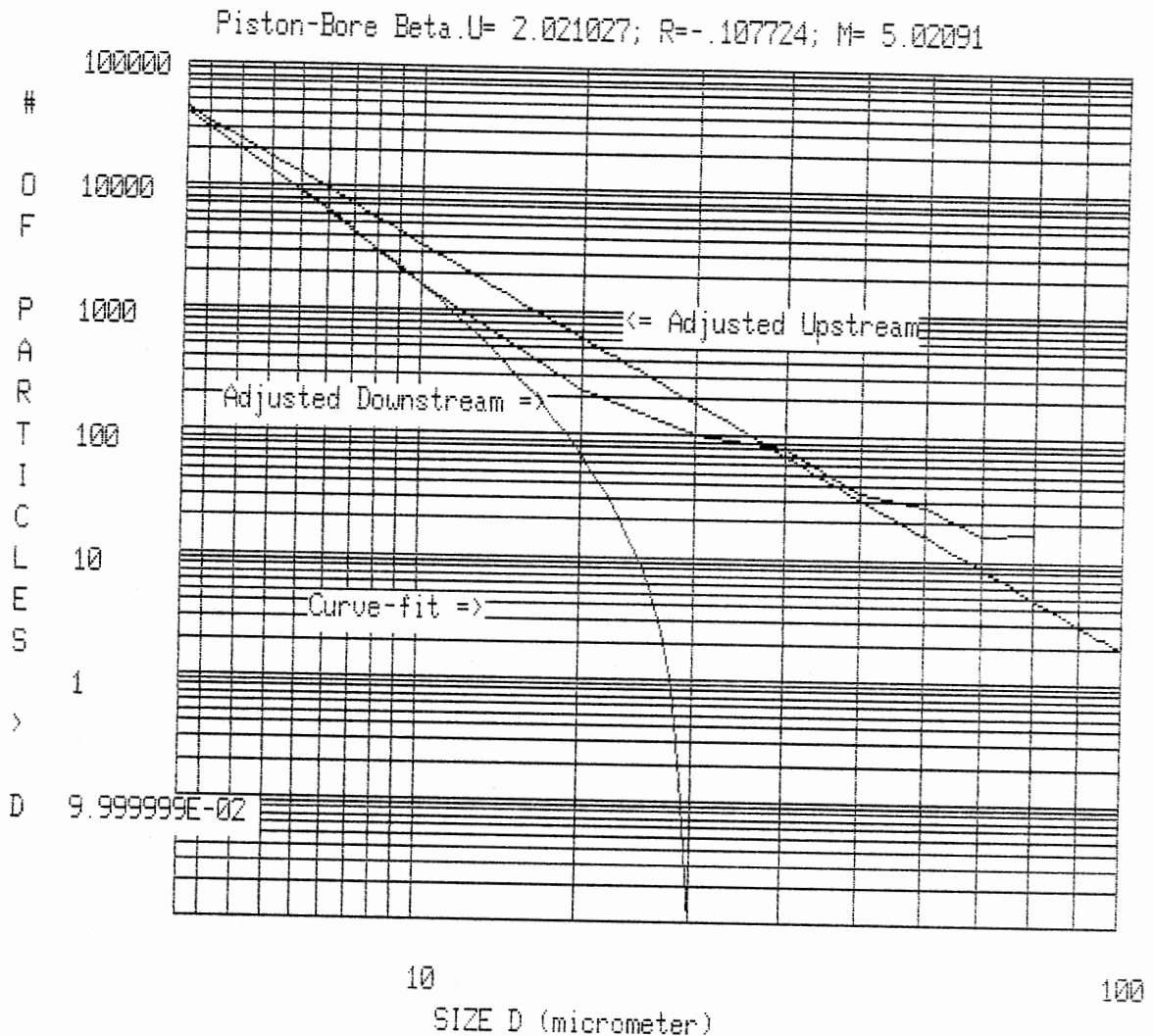
***** 1 & 2J TEST RESULT *****

Bore No.3 - Piston No.19, Land Length (3.19 mm)
5 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	12543.7	9140.876	1.372265
10	3597.918	3353.2	1575.188	2.128762
20	637.1161	592.4	221.7397	2.671601
30	187.6002	166.5	94.34101	1.764874
40	71.72498	59.1	66.729	.8856719
50	32.244	28.9	32.7509	.8824184
60	16.20372	9.25	16.3371	.5661959
70	8.837601	5.42	9.971	.5435765
80	5.133417	1.58	5.369001	.294282

Downstream Beta Analysis





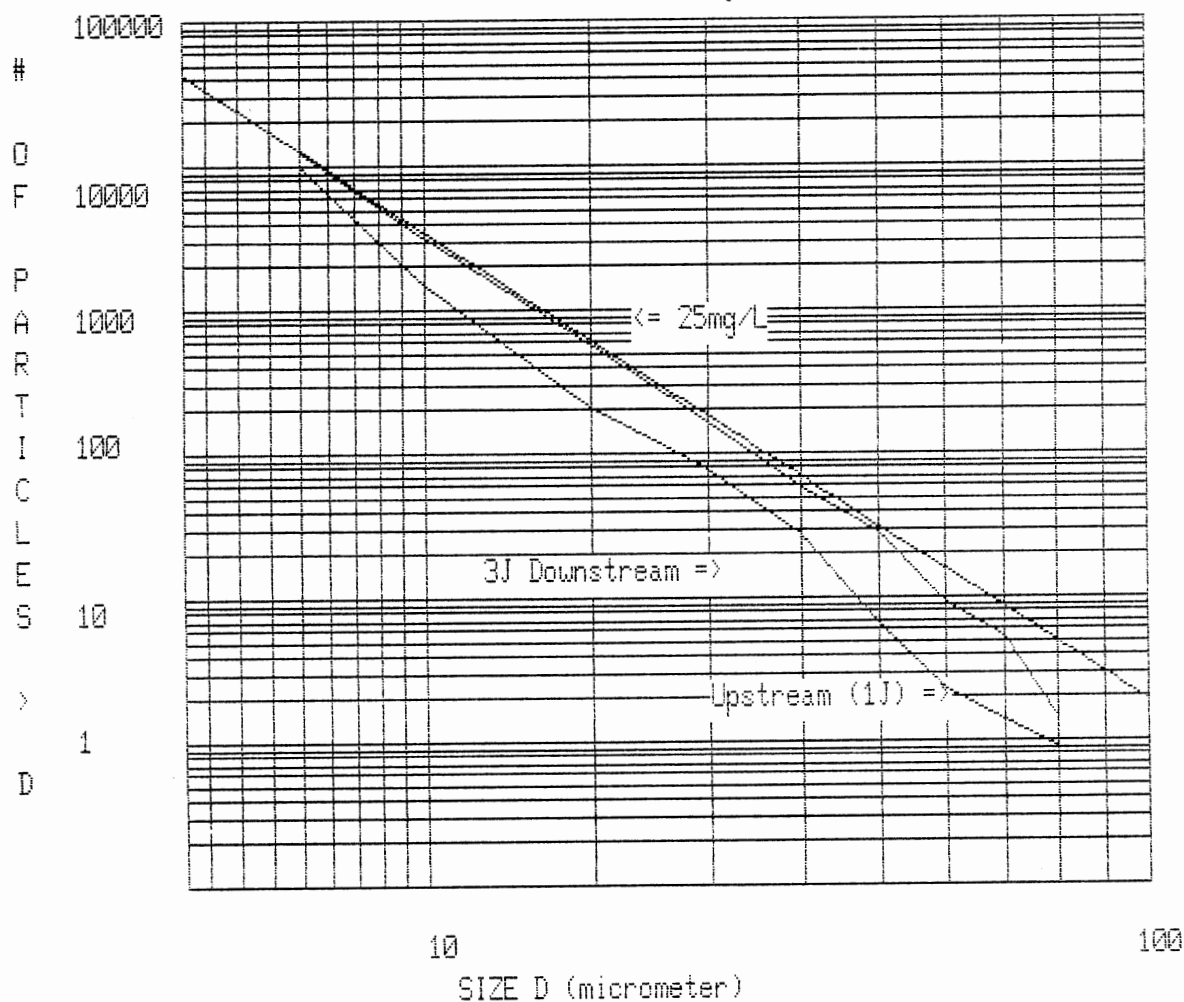
Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	40394.7	1.084239
5	12917.2	9413.055	1.372264
10	3597.918	1690.146	2.128761
15	1380.819	363.0846	3.803023
20	637.1161	73.20782	8.702842
25	331.3792	9.035084	36.67693
30	187.6002	.01	****
35	113.1623	.01	****
40	71.72498	.01	****
45	47.30807	.01	****
50	32.244	.01	****
55	22.59059	.01	****
60	16.20372	.01	****
65	11.86098	.01	****
70	8.837601	.01	****
75	6.688775	.01	****

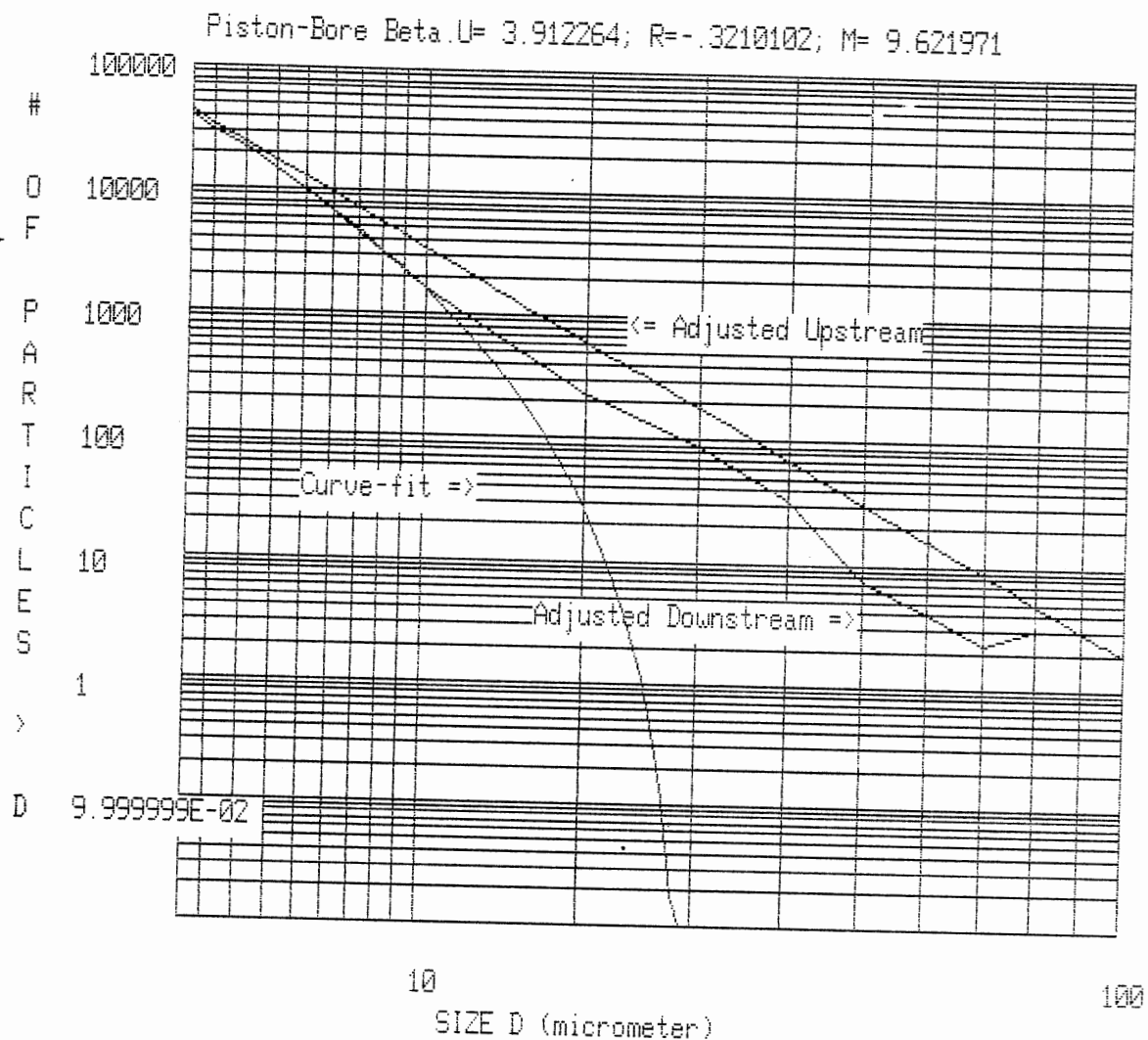
***** 1 & 3J TEST RESULT *****

Bore No.3 - Piston No.19, Land Length (3.19 mm)
5 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	12543.7	10028.01	1.250866
10	3597.918	3353.2	1554.45	2.157162
20	637.1161	592.4	219.2859	2.701496
30	187.6002	166.5	78.30091	2.126412
40	71.72498	59.1	27.474	2.151125
50	32.244	28.9	6.7239	4.298101
60	16.20372	9.25	2.3859	3.876944
70	8.837601	5.42	1.446	3.748271
80	5.133417	1.58	.9398999	1.68103

Downstream Beta Analysis





Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	41281.78	1.06094
5	12917.2	10326.6	1.250867
10	3597.918	1667.893	2.157164
15	1380.819	261.6242	5.277871
20	637.1161	29.2375	21.79106
25	331.3792	1.097602	301.9119
30	187.6002	.01	****
35	113.1623	.01	****
40	71.72498	.01	****
45	47.30807	.01	****
50	32.244	.01	****
55	22.59059	.01	****
60	15.20372	.01	****
65	11.86098	.01	****
70	8.837601	.01	****
75	6.688775	.01	****

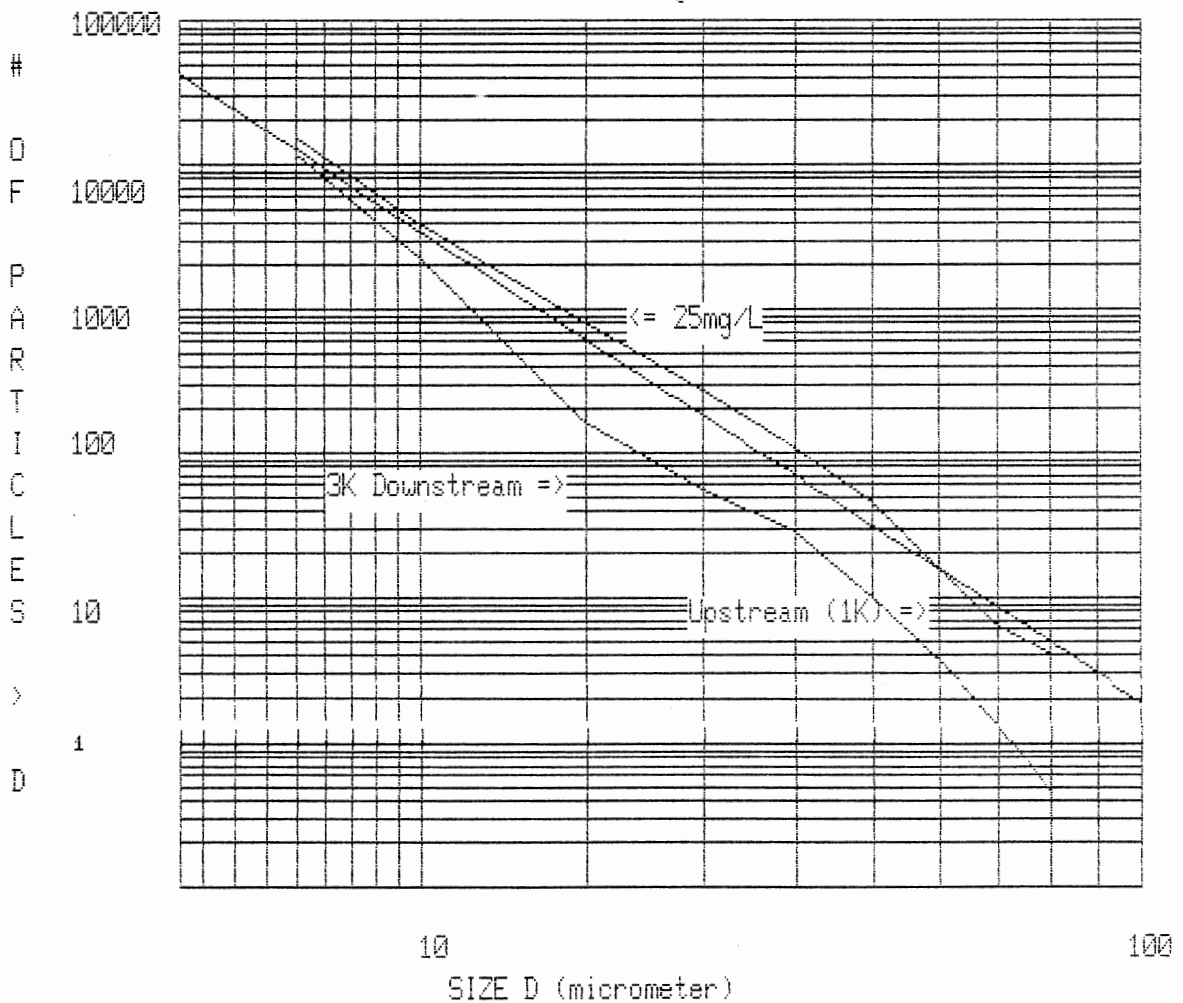
***** 1 & 3K TEST RESULT *****

Bore No.3 - Piston No.23, Land Length (6.38 mm)

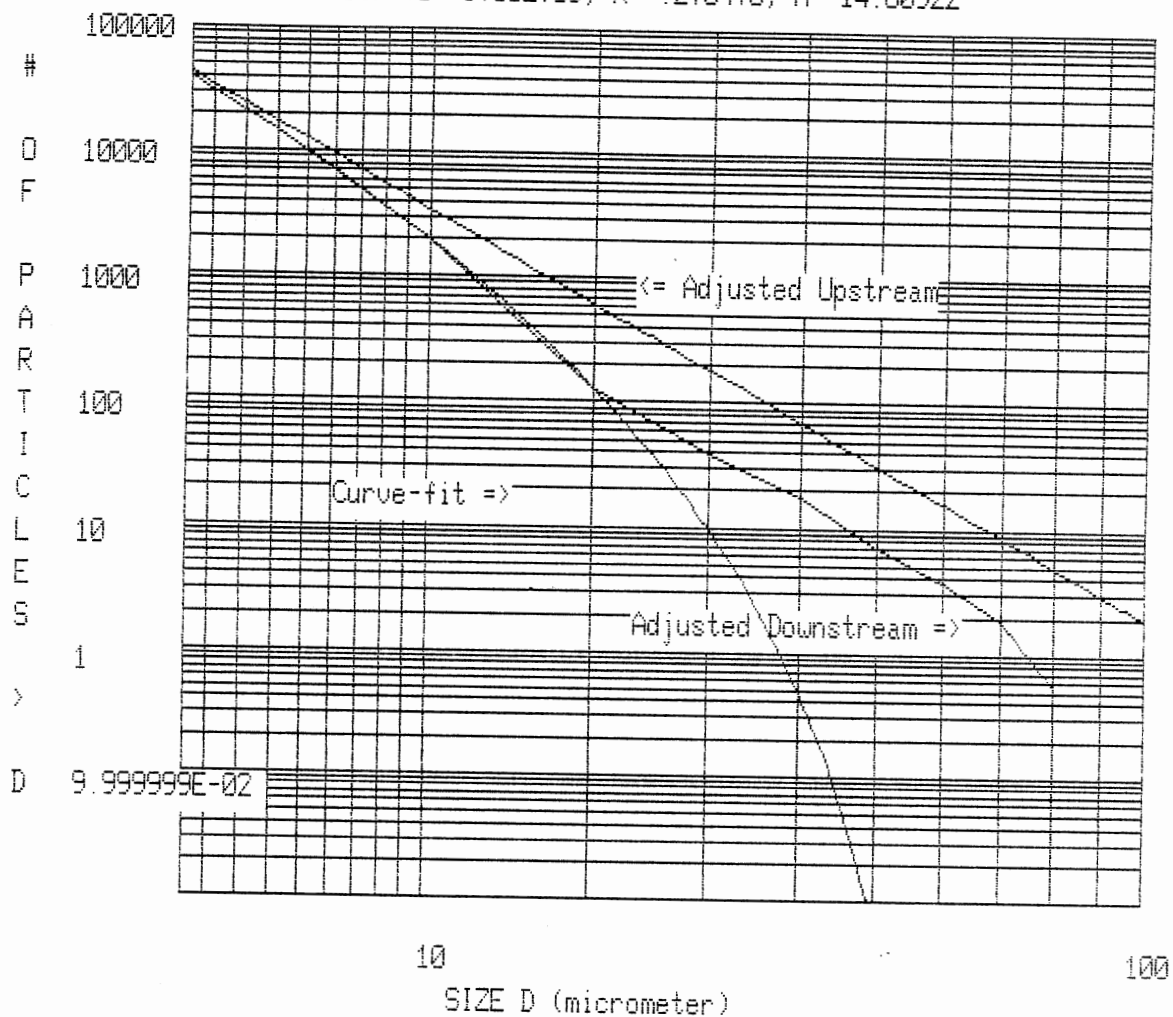
10 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	15258	12251.87	1.245361
10	3597.918	4096.6	2327.531	1.760063
20	637.1161	822.6	170.343	4.82908
30	187.6002	274.8	56.54967	4.859445
40	71.72498	112.9	28.5307	3.957141
50	32.244	46.1	10.0243	4.598825
60	16.20372	16.19	3.7153	4.357656
70	8.837601	6.38	1.402	4.550642
80	5.133417	4.17	.4907	8.498064

Silt Beta Analysis



Silt Beta .U= 5.162785; R=-.278478; M= 14.60922



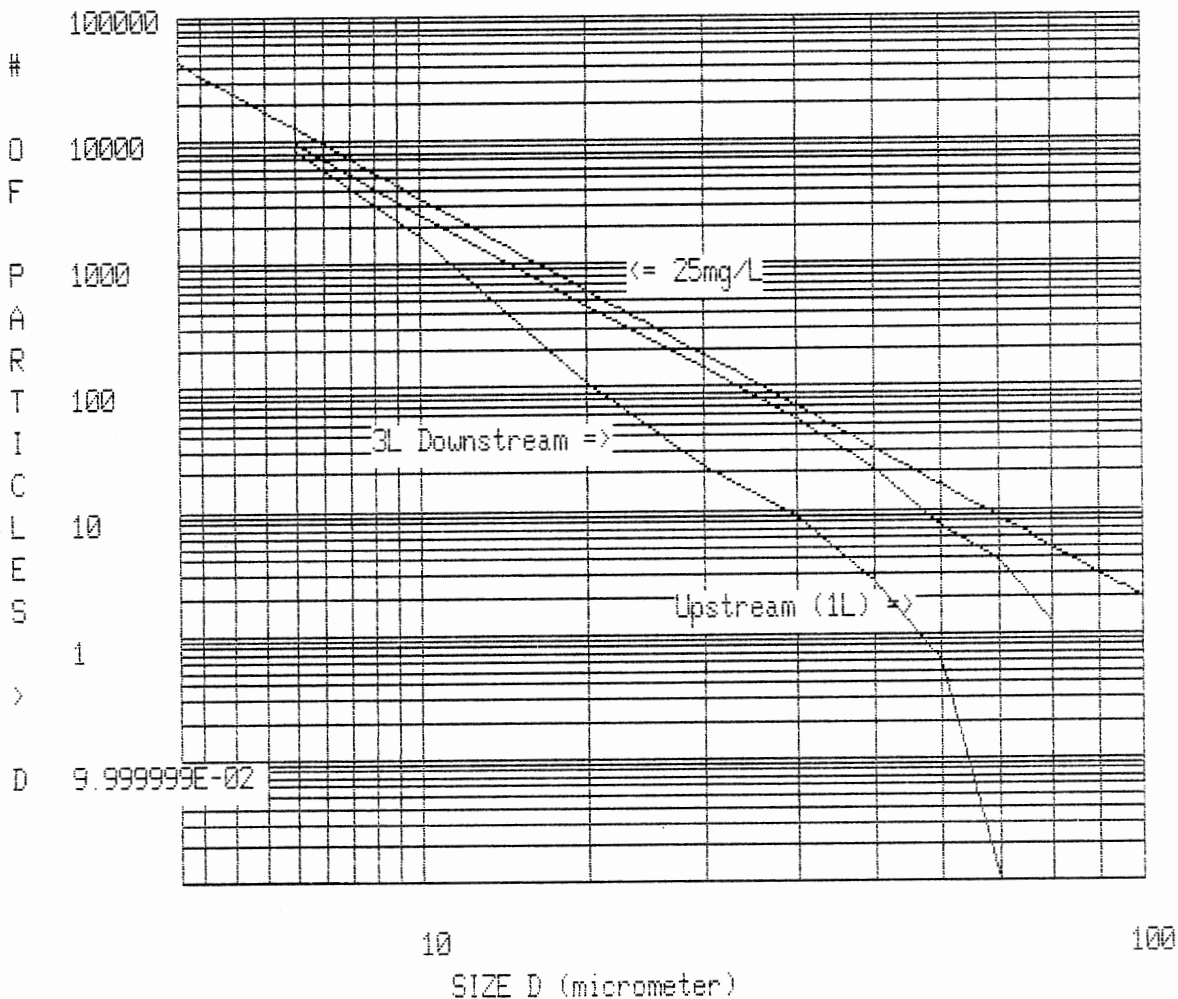
Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	40791.38	1.073695
5	12917.2	10372.26	1.245361
10	3597.918	2044.198	1.760063
15	1380.819	501.8064	2.751696
20	637.1161	135.4207	4.704718
25	331.3792	37.36605	8.868457
30	187.6002	9.965322	18.8253
35	113.1623	2.421582	46.73074
40	71.72498	.4946596	144.9987
45	47.30807	7.398339E-02	639.4418
50	32.244	.01	****
55	22.59059	.01	****
60	16.20372	.01	****
65	11.86098	.01	****
70	8.837601	.01	****
75	6.688775	.01	****

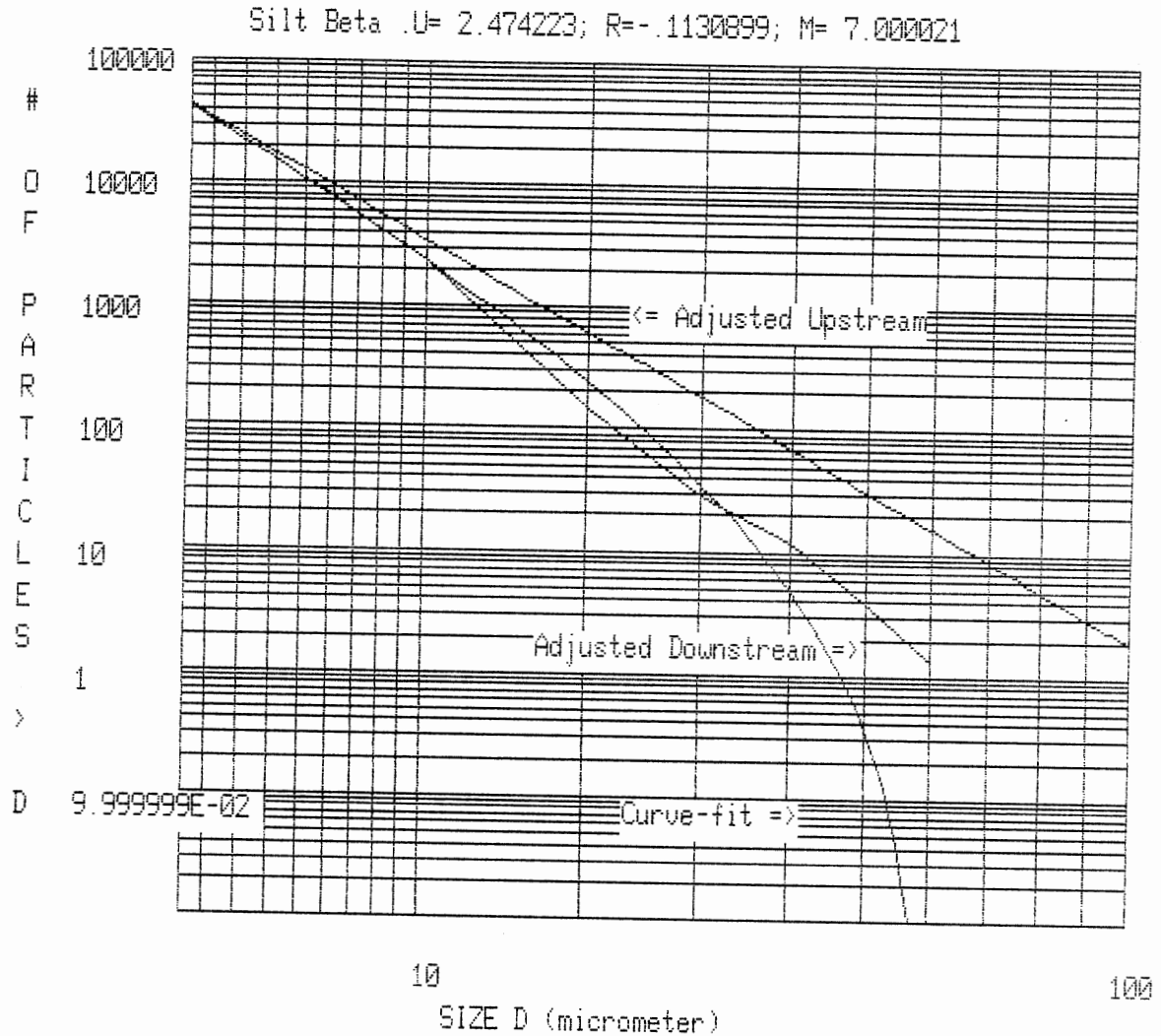
***** 1 & 3L TEST RESULT *****

Bore No.3 - Piston No.23, Land Length (3.19 mm)
 10 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	9735.5	8324.379	1.169517
10	3597.918	2587.7	1773.875	1.458784
20	637.1161	469.7	114.9471	4.086228
30	187.6002	150.2	23.0141	6.526434
40	71.72498	54.4	9.255	5.877904
50	32.244	21.6	2.67161	8.085013
60	16.20372	7.43	.617	12.04214
70	8.837601	3.94	.01	****
80	5.133417	1.31	.01	****

Silt Beta Analysis





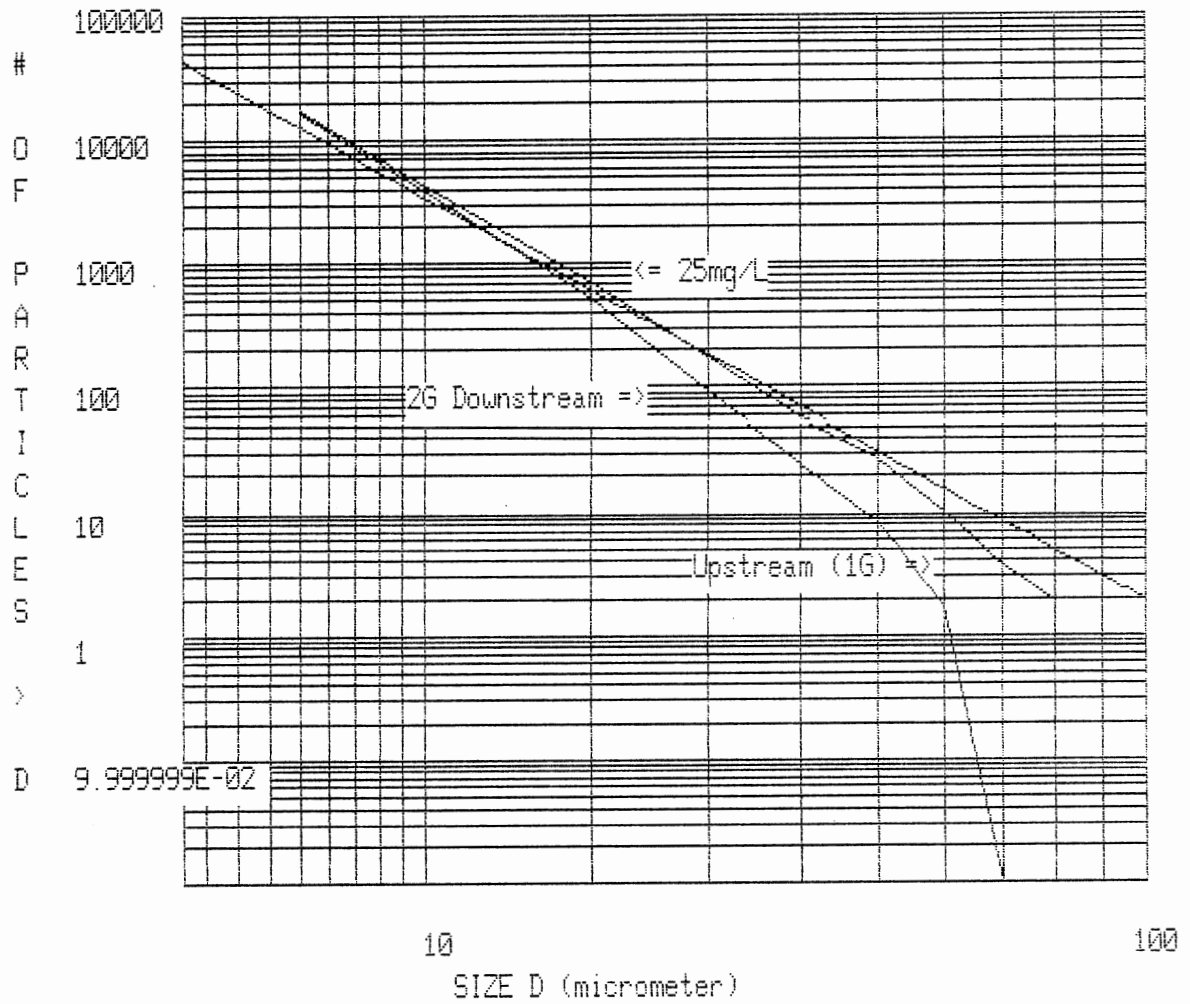
Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	42386.36	1.033292
5	12917.2	11044.9	1.169517
10	3597.918	2466.381	1.458785
15	1380.819	733.105	1.883521
20	637.1161	252.989	2.518355
25	331.3792	94.40591	3.510153
30	187.6002	36.35544	5.160169
35	113.1623	13.87771	8.154248
40	71.72498	5.012532	14.30913
45	47.30807	1.594671	29.66635
50	32.244	.384953	83.76088
55	22.59059	4.365352E-02	517.4977
60	16.20372	.01	****
65	11.86098	.01	****
70	8.837601	.01	****
75	6.688775	.01	****

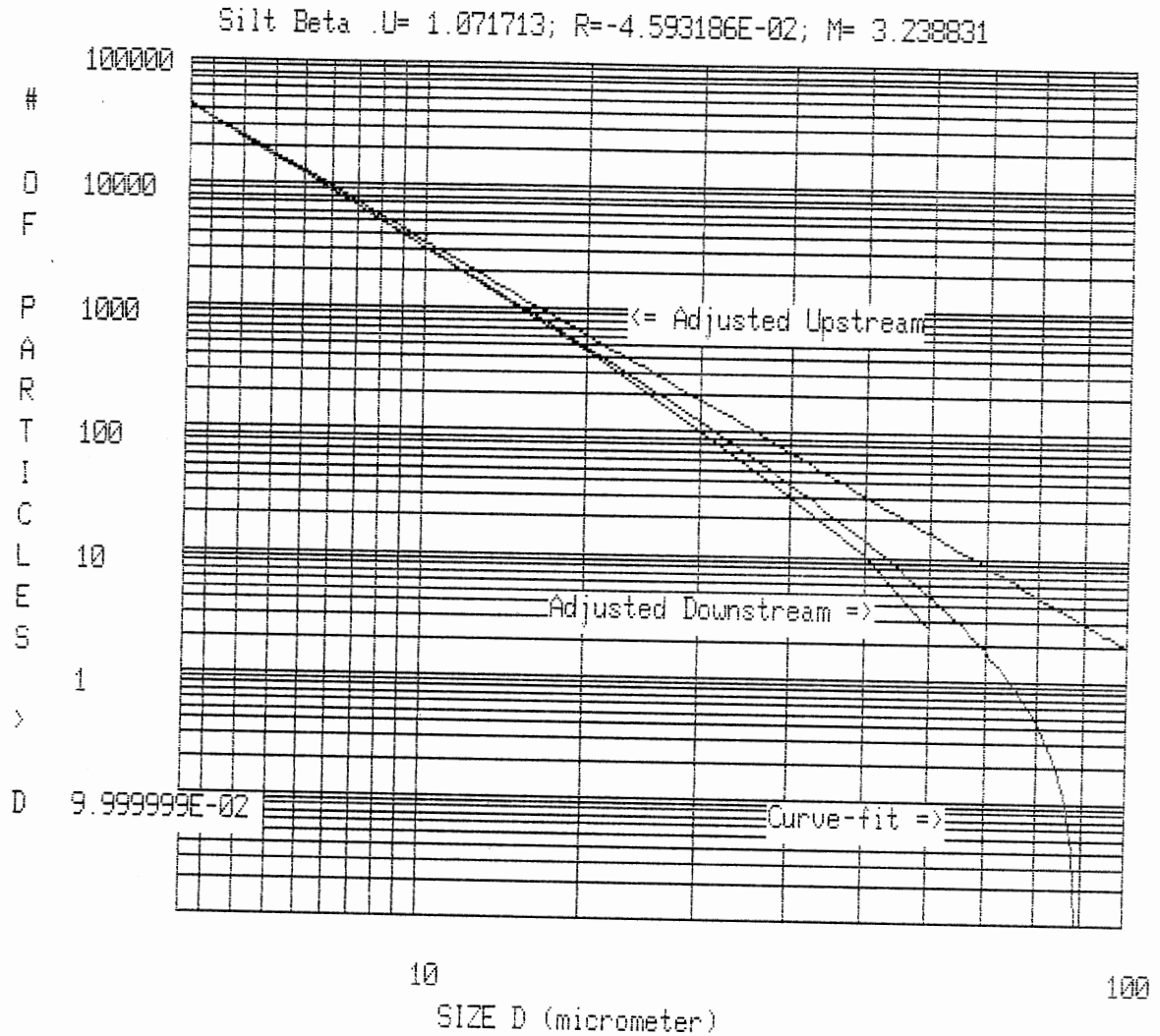
***** 1 & 2G TEST RESULT *****

Bore No.3 - Piston No.25, Land Length (6.38 mm)
 15 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	17444	16652.75	1.047515
10	3597.918	4446.5	4018.49	1.10651
20	637.1161	730.5	540.44	1.351677
30	187.6002	175.1	95.58	1.831973
40	71.72498	59.2	25.075	2.360917
50	32.244	27.7	8.850001	3.129943
60	16.20372	10.74	1.77	6.067796
70	8.837601	3.8	.01	****
80	5.133417	2.01	.01	****

Silt Beta Analysis





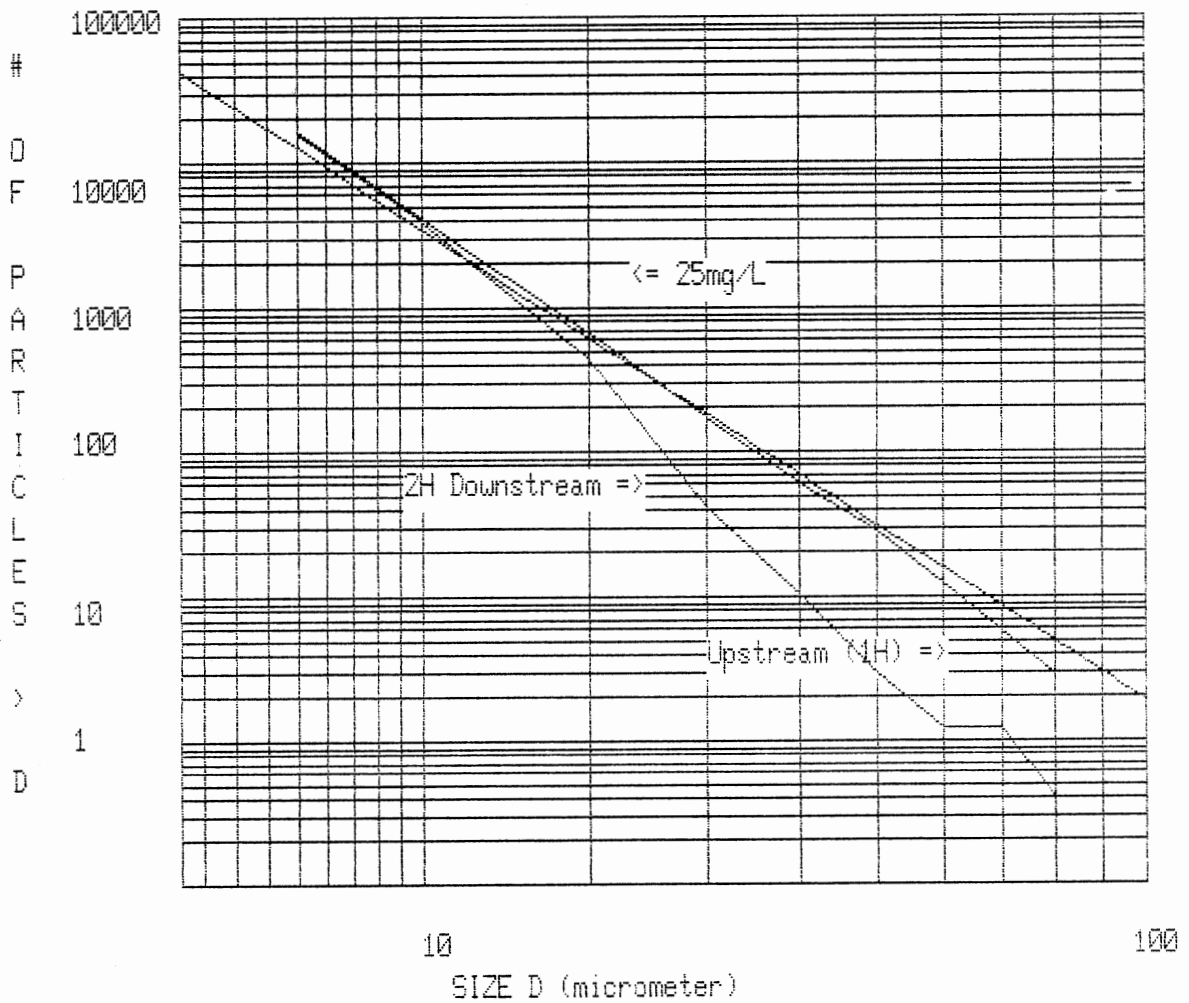
Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	43006.26	1.018398
5	12917.2	12331.28	1.047515
10	3597.918	3251.59	1.10651
15	1380.819	1170.609	1.179573
20	637.1161	503.1112	1.266353
25	331.3792	242.0985	1.368778
30	187.6002	125.8875	1.490221
35	113.1623	69.18451	1.635659
40	71.72498	39.57649	1.812313
45	47.30807	23.29494	2.03083
50	32.244	13.9738	2.307461
55	22.59059	8.466728	2.668161
60	16.20372	5.132644	3.156993
65	11.86098	3.076723	3.85507
70	8.837601	1.792868	4.929309
75	6.688775	.9858079	6.78507

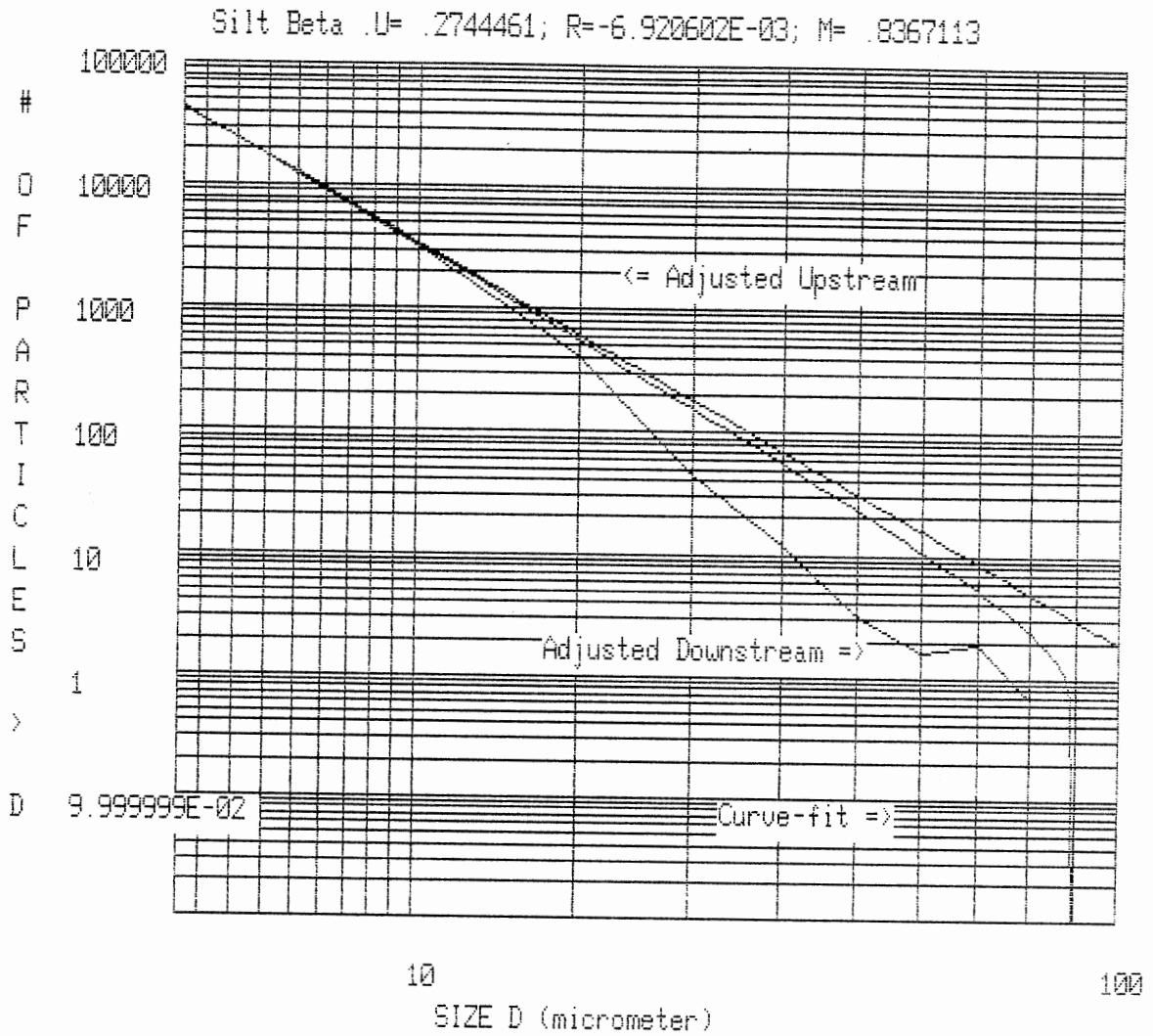
***** 1 & 2H TEST RESULT *****

Bore No.3 - Piston No.25, Land Length (3.19 mm)
 15 micrometers nominal clearance

Size	Distribution of 25 mg/L	Upstream	Downstream	BETA
5	12917.2	16690	16168.66	1.032244
10	3597.918	4291.4	4045.958	1.060664
20	637.1161	700.6	469.2	1.49318
30	187.6002	177	42.96751	4.119393
40	71.72498	62.7	10.62075	5.903538
50	32.244	28.8	2.97075	9.694522
60	16.20372	12.77	1.275	10.01569
70	8.837601	5.97	1.275	4.682353
80	5.133417	3.05	.42075	7.24896

Silt Beta Analysis





Size micron	Adjusted Upstream	Fitted Downstream	Beta
1	43797.5	43276.16	1.012047
5	12917.2	12513.71	1.032244
10	3597.918	3392.139	1.060664
15	1380.819	1268.165	1.088832
20	637.1161	570.0494	1.117651
25	331.3792	288.7042	1.147816
30	187.6002	158.9898	1.179951
35	113.1623	93.15933	1.214718
40	71.72498	57.24731	1.252897
45	47.30807	36.51764	1.295486
50	32.244	23.99406	1.343832
55	22.59059	16.13773	1.399862
60	16.20372	11.04937	1.466484
65	11.86098	7.660099	1.548411
70	8.837601	5.343157	1.654004
75	6.688775	3.715622	1.800177

APPENDIX C

SLAVE COMPUTER PROGRAM

```

;
;
MADDR EQU 180H ;STARTING ADDRESS OF 8256 MUART

MODE equ 186H
P1 equ 188H ;Port1 control
P2IO equ 192H ;Port2 IO register
T2 equ 196H
T3 equ 198H
T4 equ 19aH
T5 equ 19cH

BREAK EQU 018H ;IMMEDIALTY BREAK FROM ROUTINE--CTRL X.
XON EQU 011H ;TRANSMIT ON CHARACTER
XOFF EQU 013H ;TRANSMIT OFF CHARACTER
HOLD EQU 016H ;HOLD LOOP IDENTIFIER-- CTRL V.
MUXCV EQU 0fffbh ;A/D channel address
ADCHI EQU 0fffdh ;A/D high byte data
ADCLO EQU 0fffch ;A/D low byte data
DABASE EQU 0ff00h ;D/A base address
TALK equ 0aah
C8256 equ 0ddH ;2-4 & 3-5 counters, port2 = output
P1IN equ 00H ;port1 is input
HBYTE EQU 0ffH ;write higher byte cause HBYTE * 256 + 255 to be
;stored

;
;<timer address>
;

TMR0 equ 0ff50H ;timer0 register
MAXA0 equ 0ff52H ;maximum count A, timer0
MAXB0 equ 0ff54H ;maximum count B, timer0
MTMR0 equ 0ff56H ;timer0 mode control

TMR1 equ 0ff58H ;timer1 register
MAXA1 equ 0ff5aH ;maximum count A, timer1
MAXB1 equ 0ff5cH ;maximum count B, timer1
MTMR1 equ 0ff5eH ;timer1 mode control

TMR2 equ 0ff60H ;timer2 register
MAXA2 equ 0ff62H ;maximum count A, timer2
MTMR2 equ 0ff66H ;timer2 mode control

Counter equ 0c00dH ;external event counter
Timer equ 0c009H ;timer1 controlled by timer2
Prescale equ 0c001H ;trig timer2 as a prescaler
scale equ 250 ;NOTE this is in decimal.
;250 * 8e-7 gives 200 microseconds

ATD_Int equ 111000000001001B ; e009h scaled by timer2, int. e
T10msec equ 50 ;200 usec * 50 = 10 msec
T500msec equ 2500 ;200 usec * 2500 = 500 msec
T1sec equ 5000 ;200 usec * 5000 = 1 sec

max equ 0ffffH ;maximum count
clr equ 0000H ;clear count. this gives 65536 max.
example equ 50000 ;decimal

;
;
; IEEE-488 names

```

```

;
auxcmd      equ      03h

reset       equ      80h
rstclr      equ      00h

init55      equ      02h
adr_8255    equ      0ch
addr        equ      04h
int0        equ      00h
int1        equ      01h
adstat      equ      02h

hdfa        equ      83h
hdaclr      equ      03h

eoimk       equ      08h
bim         equ      20h
bom         equ      10h
din         equ      07h
rhdf        equ      02h
etx         equ      03h

dout        equ      07h
feoi        equ      08h

MA          equ      04h
LADS        equ      04h
TADS        equ      02h
ZERO        equ      30h ;ASCII 0
ONE         equ      31h ;ASCII 1
Last        equ      02h

;<decoding INSTRUCTION SET>

Do_ATD      equ      00h ;Single shot A/D
SingDTA     equ      01h ;Single shot D/A
SelecATD    equ      0ah ;selective ATD
ISelecATD   equ      0bh ;selective ATD with resetting of timer
Int_ATD     equ      0ch ;start interrupt ATD
Trans       equ      0dh ;transfer data from ATDstore to databuf

Freq        equ      010h ;counter-(timer0) & timer-(timer1)
IO          equ      012h ;io control on 8255 (IEEE488 card)

;<array>

Quit        equ      0ffh ;Quit decoding

;<distalk>
Quitalk     equ      0ffh ;quit talking

ZEROV       equ      0800H ;offset binary equivalent 0 volt

;<Slective ATD>
ten         equ      10
uno         equ      1

```



```
;<interrupt >
```

```
int8ip      equ      8h  
timer_int_ctrl  equ    0ff32h  
eoi_register equ    0ff22h  
non_spec   equ    8000h
```

```

public count, array, distalk, databuf, ATDstore, MAXCOUNT, POINTER
public saveINT8cs, saveINT8ip, memset, memPoint
;
dataseg segment
        count          dw          ?          ;note count stores word number info.
                                                ;NOT bytes
        MAXCOUNT      dw          ?
        POINTER         dw          ?
        saveINT8cs     dw          ?
        saveINT8ip     dw          ?
        databuf        dw          800 dup(?)
        ATDstore       dw          800 dup(?)
        memPoint       dw          ?
        memset         db          ?
        distalk        db          ?
        array          db          3 dup(?)
dataseg ends
;

include b:name.lst

;
codeseg segment
;

public crlf, conv, bout, CHROUT

extrn IntrptATD:near, ISATD:near, SATD:near, IOl:near, CF:near, DTA:near
extrn DTAS:near, ATDS:near, ATD:near, data_trans:near
;
ASSUME CS:codeseg,DS:dataseg
;
;
;

; ***** Segment Assignment *****
;

        mov          ax,dataseg          ;Stack grows downward; therefore,
        mov          ss,ax              ;the address can be ss=ds
        mov          es,ax              ;es is data buffer segment
        mov          ds,ax

; *****
; *****
;
; Listener & Talker routines
;
; Programmed by Ito, Tokunosuke
; *****
;
        call        IRS232

```

```

                call    initlt           ;initialize 9914 as listener
                call    initmr           ;initialize timer
                call    initDTA
                call    initmem         ;initialize memory
st2:            call    scan            ;scan to determine talker or listener
                jmp     st2

;
;
; -----
;
; initmem ---- initialize memory
;                memset = 00h
;
; Entry & Exit condition ---- none
;
; -----
;
initmem        proc            near
                push         ax
                push         di

                mov         di,offset memset
                mov         al,00h
                mov         [di],al

                pop          di
                pop          ax
                ret
initmem        endp

;
;
; -----
;
; initDTA --- initialize DTA to 0 voltage
;                this is necessary so that external devices will not be accidental
;                driven
;
; Entry & Exit condition ---- none
;
; -----
;
initDTA:       push         ax
                push         dx

                mov         ax,ZEROV           ;set 0 volt
                mov         dx,0              ;channel zero
                call        DTA
                mov         dx,1              ;channel 1
                call        DTA
                mov         dx,2              ;channel 2
                call        DTA
                mov         dx,3              ;channel 3
                call        DTA

                pop          dx
                pop          ax
                ret

;
;
;

```

```

;
; -----
;   initmr ---- initialize timer routine
;
;   Entry & Exit condition ---- none
;
; -----
;
initmr:      push    ax
             push    dx
             mov     dx,MAXA0      ;timer0 maxA count = ffffH
             mov     ax,max
             out     dx,ax
             mov     dx,MTMR0      ;initialize tmr0 as counter
             mov     ax,Timer
             out     dx,ax
             mov     dx,MAXA2      ;initialize timer2 with scaled
             mov     ax,scale      ;value
             out     dx,ax
             mov     dx,MTMR2      ;initialize timer2 as prescaler
             mov     ax,Prescale
             out     dx,ax
             mov     dx,MAXA1      ;set maxA count of timer1
             mov     ax,example
             out     dx,ax
;           mov     dx,MAXB1
;           out     dx,ax
             mov     dx,MTMR1      ;initialize tmr1 as event timer
             mov     ax,Timer
             out     dx,ax
             mov     dx,MODE      ;initialize 8256
             mov     al,CS256      ;2-4 & 3-5 counter, port2 outpu
             out     dx,al
             mov     dx,P1        ;initialize port1
             mov     al,PIIN
             out     dx,al
             mov     dx,T4        ;set initial value
             mov     al,HBYTE      ;ffffH
             out     dx,al
             mov     dx,T5
             out     dx,al
             mov     dx,P2IO      ;initialize port2 register
             mov     al,HBYTE      ;set all bits high
             out     dx,al
             mov     ax,clr
             mov     dx,TMR1      ;reset timer
             out     dx,ax
             mov     dx,TMR2      ;reset prescaler

```

```

        out      dx,ax
        pop      dx
        pop      ax
        ret
;
;
;-----
;
;  scan  --- scan address status and trigger
;         listener or talker routine
;
;         Entry condition ----- none
;
;         Exit condition ----- none
;
;-----
;
scan:    push     dx           ;save registers to make
        push     si
        push     cx
        push     ax           ;independent routine

        mov     dx,adstat    ;get address of address status register
        in      al,dx        ;get content

        test    al,LADS      ;listener ?
        jz     next         ;no.

        mov     al,'L'
        call    CHROUT

        call    listen      ;listener primary address start
        call    decode      ;decode what has been received
        jmp     return      ;return

next:    test    al,TADS
        jz     return      ;nop

        mov     al,'T'
        call    CHROUT
        call    inittalker  ;talker !

;*b
        mov     al,'*'
        call    CHROUT
;*e

return:  pop     ax
        pop     cx
        pop     si
        pop     dx
        ret
;
;
;
```

```

; -----
;
; relax --- delay loop
;
;   Entry & EXIT condition --- none
;
; -----
;
relax:      push    cx
            mov     cx,0fffh
bushed:    nop
            loop   bushed
            pop    cx
            ret

; -----
;
;
;
; -----
;
; decode ----- decoding the instructions
;
;   Entry conditions ----- databuf has input data
;
;   Exit condition ----- databuf has the result
;
; -----
;
decode:     push    si
            push    ax
            push    es
;
            mov    ax,ds
            mov    es,ax      ;es = ds
;
            mov    si,offset array
            mov    al,es:[si] ;get instruction
            cmp    al,Quit    ;quit decoding ? Quit=0ffh
            jnz    notq       ;get out this routine promptly
            mov    al,00h     ;clean 1st byte of array
            mov    es:[si],al
            jmp    lsel

notq:      mov    si,offset databuf
            mov    al,es:[si]
            cmp    al,Do_ATD  ;is this ATDS
            jnz    sel2       ;no. Go to 2nd choice
            inc    si         ;make si points the next byte
            call   ATDS       ;NOTE si,ax must be preserved
            jmp    lsel

sel2:     cmp    al,SingDTA    ;is this DTAS
            jnz    sel3       ;no. jump
            inc    si         ;point to next byte
            call   DTAS
            jmp    lsel

sel3:     cmp    al,Freq      ;timer & counter ?
            jnz    sel4       ;if not jump
            mov    al,'F'

```

```

                call    CHROUT
                call    CF
                jmp     lsel          ;any more info.
sel4:           cmp     al,IO          ;IO control ?
                jnz    sel5
                inc    si             ;point to the next byte
                call   IO1
                jmp     lsel
sel5:           cmp     al,SelecATD
                jnz    sel6
                call   SATD          ;call selective ATD
                jmp     lsel
sel6:           cmp     al,ISelecATD  ;initialize timer
                jnz    sel7
                call   ISATD
                jmp     lsel
sel7:           cmp     al,Int_ATD
                jnz    sel8
                inc    si             ;si points to no. of ATD conversion
                call   IntrptATD
                jmp     lsel
sel8:           cmp     al,Trans
                jnz    lsel
                inc    si
                call   data_trans
                jmp     lsel
lsel:           pop     es
                pop     ax
                pop     si
                ret
;
; -----
;
; bout    --- binary output
;
;         Entry condition --- ax contains a word to be outputted
;
;         Exit condition ---- none
;
; -----
;
bout:           push    cx
                push    ax           ;save register
                mov     cl,16        ;one word rotation
trya:           rol     ax,1         ;left rotate
                jc     pl           ;jump if carry
                push    ax
                mov     al,ZERO      ;no jump, send 0
                call   CHROUT
                pop     ax
                jmp     p2          ;jump to loop
pl:            push    ax
                mov     al,ONE       ;send 1

```

```

                call    CHROUT
                pop     ax
p2:             loop    trya
                pop     ax
                pop     cx
                ret
;
;-----
;
; rdchr --- read character
;
;     Entry condition ----- none
;
;     Exit condition ----- none
;
;-----
rdchr:          call    CHRIN
                call    CHROUT
                ret
;
;-----
;
; listen - listener routines
;
;     Entry condition ----- none
;
;-----
listen:         push    ax
                push    dx
                push    si

                mov     dx,auxcmd
                mov     al,hdfa
                out     dx,al

                lea    si, databuf

ls1:           mov     dx,adstat           ;check for talker
                in     al,dx
                test    al,TADS           ;talker ?
                jnz    get_out           ;yes! get out listener routine

                mov     dx,int0           ;BI or EOI ?
                in     al,dx
                and    al,eoimk+bim
                jz     ls1               ;not BI or EOI

                call   recvlt           ;yes! call recvlt

                lea    si,distalk
                mov     al,00h
                mov     es:[si],al
                ;enable talk

                jmp    ls2

```



```

get_out:    lea     si,array
            mov     al,0ffh           ;telling decode to quit
            mov     es:[si],al

ls2:       mov     dx,auxcmd
            mov     al,hdaclr
            out     dx,al

            pop     si
            pop     dx
            pop     ax
            ret

;
;
; -----
;
;   inittalker --- talker routines
;
;   Entry condition ---- none
;
; -----
;
;
;
inittalker: push    si
            push    ax

            mov     si,offset memset
            mov     al,[si]           ;byte transfer
            cmp     al,00h
            jnz     atl1

            mov     si,offset databuf ;get pointer to outut buffer
            jmp     resetmem

atl1:      mov     si,offset memPoint ;get starting address
            mov     ax,[si]
            mov     si,offset ATDstore ;the beginning of ATDstore
            add     si,ax             ;add offset

resetmem:  call    sendlt              ;send them to gpib
            mov     si,offset memset
            mov     al,00h
            mov     [si],al

;*b
            mov     al,'E'
            call    CHROUT

;*e

            pop     ax
            pop     si
            ret

;
;
; -----
;
;   initlt ---- initialize 9914   seems to work for both talker & listener
;
;   Entry condition ----- none
;
;

```

```

;      Exit condition ----- none
;
; -----
;
initlt:      push      ax                ;save working register
             push      dx
             mov       dx,auxcmd        ;point to auxcmd (03h) register
             mov       al,reset        ;reset (80h)
             out       dx,al
             mov       al,rstclr       ;rstclr (00h)
             out       dx,al

;
             mov       al,init55       ;initialize 8255 init55 (02h)
             mov       dx,adr_8255+03h ;load control register addr
             out       dx,al

             mov       dx,adr_8255+1   ;get switch address
             in        al,dx           ;get switch settings

             and       al,01fh         ;protect 5 lowest bits
             mov       dx,addr         ;point to addr register of
             out       dx,al          ;addr (04h)
             xor       al,al          ;clean up al
             mov       dx,int0
             out       dx,al
             mov       dx,int1
             out       dx,al          ;mask out all interrupt

             pop       dx
             pop       ax             ;recover registers
             ret

;
; -----
;
;      string ----- outputting the string of data
;
;      Entry condition ----- si contains the effective address
;
;      Exit condition ----- si destroyed
;
; -----
;
string:      push      ax
checkl:      mov       al,cs:[si]      ;get a byte
             cmp       al,'$'         ;is it yhe end of text
             je        fnprint        ;yes jump
             call      CHROUT         ;output it to screen
             inc       si
             jmp       checkl
fnprint:     pop       ax
             ret

;
; -----
;
;      recvlt ----- receive data
;
;      data is received until EOI is sent with

```

```

;          last byte ETX is added as last byte to
;          indicate end of buffer
;
;          Entry condition ----- si points to data buffer
;                               al contains the status of into
;
;          Exit condition ----- si only have been destroyed
;
;-----
;
recvlt:   push    ax
          push    cx
          push    dx                ;save ax & dx
          push    si
          push    di
          jmp     rcv                ;jump into state acquisition

recvlt1:  mov     dx,int0
          in      al,dx              ;into (00h) contains status

rcv:      and     al,eoimk+bim        ;EOI or BI ?
          jz     rcvlt1              ;wait until EOI or BI is set
          push   ax                  ;save status byte
          and   al,eoimk             ;test for EOI
          jnz   rcvlt2              ;jump if EOI
          pop    ax                  ;restore status

          mov    dx,din              ;now we know that status has B
          in    al,dx                ;get data byte din (07h)
          mov   es:[si],al          ;save

          mov    dx,auxcmd
          mov    al,rhdf              ;rhdf-release RFD holdoff
          out   dx,al                ;rhdf (02h)
          inc   si
          jmp   rcvlt1              ;get more

recvlt2:  pop     ax                  ;restore status byte
;
recvlt2a: and     al,bim                ;byte in ?
          jnz   rcvlt5              ;if so jump. bim (20h)
          mov   dx,int0
          in    al,dx
          jmp   rcvlt2a             ;different from original !!!

recvlt5:  mov     dx,din
          in     al,dx
          mov   es:[si],al          ;store away

          inc   si                  ;this is to leave ETX in da
          mov   al,etx              ;buffer. ETX (03h)
          mov   es:[si],al

recvlt3:  mov     dx,auxcmd
          mov    al,rhdf              ;release Holdoff
          out   dx,al

;        mov    dx,auxcmd
;        mov    al,hdaclr            ;clear Hold-off
;        out   dx,al                ;to 9914

```

```

        pop        di
        pop        si
        pop        dx
        pop        cx
        pop        ax
        ret
;
;
;-----
;
; sendlt --- send data to IEEE488
;
;   Entry condition ---- es = ds
;                       si contains the address of data buffer
;
;   Exit condition ---- si destroyed
;-----
;
sendlt:
        push       ax
        push       cx
        push       dx
        push       di
        push       es

        mov        ax,ds
        mov        es,ax                ;es = ds

        mov        di,offset distalk   ;check previous process
        mov        al,es:[di]
        cmp        al,Quitalk
        jz         disable

        mov        di,offset count     ;get numbet of words to transf
        mov        cx,es:[di]
        mov        ax,cx
        add        cx,ax                ;get no. of bytes from words
                                        ;cx = content of count * 2

; *b
        push       cx
        push       si
        call       crlf
        mov        al,'N'
        call       CHROUT
        mov        ax,cx
        call       conv
        pop        si
        pop        cx

; *e
sendlt1: mov        al,es:[si]           ;si already pionts to the t
                                        ;of memory set by memset
                                        ;if not send out.

        mov        dx,dout
        out        dx,al

;       call       bout                ;check

sendwait: mov       dx,int0

```

```

                in      al,dx      ;get status
                and     al,bom     ;check byte out mask bom (10h)
                jz      sendwait   ;if B0 set then jump to repeat

                cmp     cx,Last    ;is this one before the last byte
                jnz     sendlt2

                mov     dx,auxcmd   ;send EOI
                mov     al,feoi
                out     dx,al

sendlt2:        inc     si
                loop   sendlt1    ;

                mov     di,offset distalk ;mark that talk process is finishe
                mov     al,Quitalk
                mov     es:[di],al

disable:       pop     es
                pop     di
                pop     dx
                pop     cx
                pop     ax
                ret
;

```

```

;
; -----
; crlf  subroutine  - sends CR & LF  to consol
;
;      Entry condition ----- none
;
;      Exit condition ----- destroies none
;
; -----
;
crlf:         push    ax           ;save ax register
                mov     al,0ah     ;line feed
                call   CHROUT      ;out to consol
                mov     al,0dh     ;carriage return
                call   CHROUT      ;send it to consol
                pop     ax         ;restore the register
                ret              ;back to main routine
;
; -----
; conv  subroutine
;

```

```

;           Entry condition ----- ax has binary number
;
;           Exit condition -----
;
; -----
conv:      push    ds           ;save registers
          push    di
          push    dx
          push    cx           ;
          push    bx
          push    ax           ;ax is stored temporarily
          mov     ax,dataseg    ;get dataseg in place
          mov     ds,ax
          lea    di,array      ;get pointer to array
          mov     al,0         ;clean up of the array
          mov     cx,3         ;0-2, 3 bytes
cleanup:   mov     [di],al     ;cleanup loop
          inc    di           ;next byte
          loop   cleanup

          pop     dx           ;get dx(16 bit binary) back formally in ax
          lea    di,array      ;get pointer to array again
getbcd:    mov     ax,dx
          mov     dx,0         ;cleanup upper byte
          mov     cx,10        ;divisor of 10
          div    cx           ;(dx:ax)/cx => ax=quotient,dx=remainder
          mov     bl,al        ;ax=remainder, dx=quotient
          xchg   ax,dx        ;bl has the remainder (al & bl are less than 1)
          mov     ax,dx        ;ax=dx=quotient
          mov     dx,0         ;cleanup upper byte
          mov     cx,10        ;divisor of 10
          div    cx           ;(dx:ax)/cx => ax=quotient, dx=remainder
          xchg   ax,dx        ;dx=quotient, ax=remainder
          mov     cl,4         ;rotate left 4 bits
          rol    al,cl
          and    al,0f0h      ;clean up the last 4 bits
          or     al,bl        ;combine and the result is in al
          mov     [di],al     ;store away
          inc    di
          cmp    dx,0         ;if dx(quotient)=0, finish.
          jnz   getbcd        ;still remaining to convert

;
;   output ASCII converted from BCD
;
          dec    di           ;point to the last byte stored
          mov    dh,0         ;test against zero
          mov    bl,0         ;if bl=0, leading 0. if bl=1, non leading 0
cont:      mov    al,[di]     ;get packed BCD byte
          dec    di           ;and point to next
          mov    dl,al        ;save it in dl
          mov    cl,4         ;rotate left 4 times
          rol    al,cl
          and    al,0fh      ;first BCD
          or     dh,al        ;dh=0
          jz    bcd1         ;if leading zero, skip!
          bl    bl           ;from now on zero will be sent as number
          add    al,30h      ;add 48D(30h) to make ASCII
          call   CHROUT      ;send it
          mov    al,dl        ;dl has the original packed BCD

```



```

MOV     AL,02H
OUT     DX,AL           ;SET 8086 MODE
;
MOV     AL,034h        ;9600 baud rate
MOV     DX,MADDR+2H
OUT     DX,AL           ;SET BAUD RATE
;
MOV     AL,0C0H
MOV     DX,MADDR+4H
OUT     DX,AL           ;ENABLE RECEIVER
AND     AL,81H
MOV     DX,MADDR+4H
OUT     DX,AL           ;RESET MUART
POPF
POP     SI
POP     DX
POP     AX
RET
;
;
msg1    db             'Ad sta  $'
msg2    db             'int0 status is  $'
msg3    db             'Enetered Talker State... $'
msg4    db             'Ready to receive data...(Listener) $'
msg5    db             'End detected in int0  $'
msg6    db             'GPIB status ... $'
msg7    db             'int1 status is  $'
;
;
codeseg ends
;
;
      END

```



```

        mov     si,offset memset           ;memory set for ATDstore
        mov     al,01h
        mov     [si],al

        mov     bx,offset count           ;get no. of words to be
        mov     cx,[bx]                   ;transferred
        mov     bx,offset ATDstore        ;base address
        mov     di,offset memPoint       ;offset
        add     bx,[di]                   ;start address = base + offse

show:   mov     ax,[bx]
        call   conv
        call   crlf
        inc   bx
        inc   bx
        loop  show

        pop   di
        pop   si
        pop   es
        pop   dx
        pop   cx
        pop   bx
        pop   ax
        ret

data_trans   endp
;
;
; -----
; IntrptATD  ----- tap timer interrupt routine
;
;   Entry condition ---- si points the next word (count)
;
;   Exit ----- none
;
; -----
;
IntrptATD:  push   ax
            push   bx
            push   dx
            push   es
            push   si

            mov   ax,ds           ;set ax = ds
            mov   es,ax          ;es = ds

;*b
            xor   ax,ax
            mov   al,'R'         ;interrupt tap enter
            call  CHROUT
            call  crlf

;*e
            pop   si             ;recover si

```

```

push    si
mov     ax,es:[si]      ;si points the count
                        ;es=ds

mov     si,offset MAXCOUNT ;store count in MAXCOUNT

mov     es:[si],ax      ;es = ds

xor     ax,ax           ;clean up ax
mov     si,offset POINTER ;clean up pointer
mov     es:[si],ax

cli                               ;disable interrupt

xor     ax,ax           ;ax = 00h
mov     es,ax          ;es = 00h

mov     si,4*int8ip      ;instruction pointer of type 8 int

mov     ax,es:[si]
mov     bx,offset saveINT8ip ;save old instruction pointer
mov     [bx],ax

inc     si
inc     si               ; a word apart for code segment

mov     ax,es:[si]      ;save codesegement
mov     bx,offset saveINT8cs
mov     [bx],ax

mov     si,4*int8ip
mov     es:[si],offset timer_int ;es = 0000h
inc     si
inc     si
mov     es:[si],cs      ;patching pointers complete

mov     dx,MAXA0        ;set 10 msec interrupt
mov     ax,T10msec
out     dx,ax

mov     dx,MTMR0        ;enable timer interrupt
mov     ax,ATD_Int
out     dx,ax

mov     dx,timer_int_ctrl ;unmask interrupt
mov     ax,clr          ;highest priority
out     dx,ax

mov     dx,TMR0         ;clean up timer0 & timer2
out     dx,ax          ;ax = 0000h from the previous code
mov     dx,TMR2
out     dx,ax

sti                               ;enable processors interrupt

pop     si
pop     es
pop     dx

```

```

                pop     bx
                pop     ax
                ret
;
;
;-----
; timer_int ---- timer interrupt
;
;     Entry & Exit condition ---- none
;
;-----
timer_int      proc     near
                push    ax
                push    bx
                push    cx
                push    dx
                push    es
                push    si
                push    di

                mov     ax,ds           ;ax = ds
                mov     es,ax          ;es = ds

                mov     bx,offset POINTER ;get present pointer
                mov     ax,[bx]
                inc     ax             ;increment by 1
                mov     [bx],ax       ;store it back right away !

                mov     si,offset MAXCOUNT ;compare POINTER with MAXCOUNT
                mov     bx,es:[si]      ;get MAXCOUNT          es=ds
                cmp     ax,bx
                jg      finito         ;if pointer is greater than MAX
                                        ;then go to finish routine
                dec     ax             ;decrement to start from 0

                mov     cx,2           ;multiply ax with 4 by 2 shift
                shl     ax,cl
                mov     si,offset ATDstore
                add     si,ax          ;si + ax(pointer) gives the beg
                                        ;of the storage

                mov     ax,2           ;2nd channel (position)
                call    ATD
                mov     es:[si],ax     ;store     es=ds

                xor     ax,ax          ;clean ax to get 0 channel (for
                add     si,2           ;increment pointer by a word
                call    ATD
                mov     es:[si],ax     ;es=ds

out_of_int:    mov     dx,eoi_register ;non-iRMX 86 non specific
                mov     ax,non_spec   ;end of interrupt
                out     dx,ax

                jmp     end_int

```

```

finito:      cli                                ;clear interrupt
;*b
             mov     al,'E'
             call    CHROUT
             call    crlf
;*e

             xor     ax,ax                       ;ax = 0000h
             mov     es,ax                       ;es = 0000h

             mov     bx,offset saveINT8ip       ;repatch the old info.
             mov     ax,[bx]                   ;get saved ip info.
             mov     si,4*int8ip               ;get the address of int8
             mov     es:[si],ax                ;repatch ip es=0000h

             mov     bx,offset saveINT8cs       ;get address where cs saved
             mov     ax,[bx]                   ;transfer contyent to ax
             inc     si
             inc     si                         ;get address of int8cs
             mov     es:[si],ax                ;es = 0000h

             mov     dx,MTMR0                   ;disable timer interrupt
             mov     ax,Timer
             out     dx,ax

             sti                                ;repatch ended. enable interrup

             jmp     out_of_int

end_int:     pop     di
             pop     si
             pop     es
             pop     dx
             pop     cx
             pop     bx
             pop     ax

             iret

timer_int    endp

;
;
; -----
; ISATD ----- SATD with timer initialization
;
;   Entry & Exit  condition ----- none
;
; -----
;
ISATD:       push    ax
             push    dx
             mov     dx,TMR0                   ;reset timer0
             mov     ax,clr
             out     dx,ax
             mov     dx,TMR2

```

```

        out      dx,ax
        call    SATD
        pop     dx
        pop     ax
        ret

;
;-----
; SATD ---- selective ATD
;
; Entry & Exit condition ---- none
;
;-----
;
SATD:   push     ax
        push     bx
        push     cx
        push     dx
        push     si

        lea     si,count
        mov     es:[si],3           ;3 words transfer

        lea     si,databuf
        mov     ax,clr              ;load pointer to databuf
        mov     es:[si],ax         ;clean up buffer
        add     si,2                ;3 words
        mov     es:[si],ax        ; 1-position
        add     si,2                ; 2-force
        mov     es:[si],ax        ; 3-timer1 prescaled by timer2
        mov     ax,clr              ;reset timer1 & timer2(prescale
        mov     dx,TMR1
        out     dx,ax

        mov     cx,ten              ;# of data sets
        mov     bx,uno              ;counter for 200 usec

again:  lea     si,databuf
        xor     ah,ah
        mov     al,2                ;channel # of position
        call    ATD
        add     es:[si],ax         ;store in databuf
        xor     ax,ax               ;next is 0 channel=force
        add     si,2                ;advance pointer
        call    ATD                ;get force
        add     es:[si],ax
        mov     dx,TMR1            ;200 microsecond wait
        in     ax,dx               ;get timer1 count
again1: cmp     ax,bx
        jl     again1              ;wait until 200 usec
        inc    bx                   ;increment for next
        loop   again

        lea     si,databuf
        mov     cx,2
        mov     bx,ten

```



```

again2:    xor     dx,dx
           mov     ax,es:[si]
           div     bx
           mov     es:[si],ax
           add     si,2
           loop    again2

           mov     dx,TMR0                ;timer 1 count
           in      ax,dx
           mov     es:[si],ax

           pop     si
           pop     dx
           pop     cx
           pop     bx
           pop     ax
           ret

;
;-----
;
; IO1 ---- Industrial IO control
;
;   Entry condition ----- si points to a byte data
;
;   Exit condition ----- none
;
;-----
;
IO1:       push    ax
           push    dx
           mov     al,es:[si]
           mov     dx,P2IO
           out     dx,al
           pop     dx
           pop     ax
           ret

;
;-----
;
; CF ---- Timer0 is counter & timer1 is timer prescaled by
;         timer2 at 200 microseconds.
;
;   Entry conditon ----- none
;
;   Exit condition ----- databuf contains data as follows
;
;         low byte counter: high byte counter: low byte timer : high byte timer
;
;-----
;
CF:        push    ax
           push    bx
           push    dx
           push    si

           lea    si,databuf

           mov     dx,T4
           in      al,dx

```

```

mov     ah,al
mov     dx,T2
in      al,dx

mov     bx,ax
mov     ax,max
sub     ax,bx

mov     es:[si],ax
call   bout
call   crlf
add     si,2
mov     dx,TMR1
in      ax,dx
mov     es:[si],ax
call   bout
call   crlf
call   crlf

lea     si,count
mov     ax,0002h           ;2 words (means 4 bytes in send1
mov     es:[si],ax

mov     ax,clr           ;clean up routine
mov     dx,TMR1         ;reset timer1
out     dx,ax
mov     dx,TMR2         ;reset timer2
out     dx,ax

mov     dx,T4
mov     al,HBYTE
out     dx,al

pop     si
pop     dx
pop     bx
pop     ax
ret

;

; -----
; DTAS ---- single shot ATD
; Entry condition ----- si points to the channel data
; Exit condition ----- si destroyed
; -----
;
DTAS:   push     ax
        push     dx
        mov     dl,es:[si]           ;get channel number
        xor     dh,dh
        inc     si

```

```

        mov     ax,es:[si]           ;get D/A output value
        call   DTA
        pop    dx
        pop    ax
        ret

;
;-----
;
; DTA ---- D/A conversion routine
;
; Entry condition ----- ax = data
;                        dx = channel no. (0-3)
;
; Exit condition ----- ax,dx destroyed
;-----
;
DTA:    push    bx
        push    es

        push    ax
        mov     ax,0000h
        mov     es,ax
        pop     ax

        mov     bx,DATABASE
        add     bx,dx
        add     bx,dx
        mov     es:[bx],ax

        pop     es
        pop     bx
        ret

;
;-----
;
; ATDS ---- ATD  routine
;
; Entry condition ----- si points to data buffer that contains
;                        the channel number
;
; Exit condition ----- databuffer contains ATD result
;-----
;
ATDS:   push    ax
        push    cx
        push    dx
        push    di

        mov     dl,es:[si]         ;get channel number
        inc     si
        mov     cx,es:[si]        ;get number of conversion to take pl
        lea     di,count          ;note it is 2 bytes (word)
        mov     es:[di],cx       ;store away this count

        lea     si,databuf        ;now points the top of the storage

```

```

continue:    mov     al,dl           ;get channel number
             xor     ah,ah         ;clean higher byte
             call    ATD           ;get ATD result
             mov     es:[si],ax    ;store
             add     si,2          ;increment to avoid a word just save
             loop   continue

             pop     di
             pop     dx
             pop     cx
             pop     ax
             ret

;
;-----
;
;   ATD   subroutine
;
;   Entry condition ----- ax contains channel number
;
;   Exit condition ----- ax contains A/D conversion result
;-----
;
ATD:
             push    si
             push    es
             push    ax           ;save ax temporarily
             xor     ax,ax        ;set es = 0000h
             mov     es,ax
             pop     ax           ;get channel no. back
             mov     si,MUXCV     ;send channel no.
             cli
             mov     es:[si],ax
repeat:      mov     si,ADCHI     ;check busy bit
             mov     al,es:[si]
             rol     al,1         ;Busy ?
             jc     repeat
             mov     si,ADCLO     ;get a Word
             mov     ax,es:[si]
             sti

             pop     es
             pop     si
             ret

;
;
codeseq ends
;
;
END

```

APPENDIX D

FILE DOWNLOADING PROGRAM

(INTEL HEX FORMAT)

```

#include      "stdio.h"

#define      NZ      16384      /* 15 th bits */
#define      Baud      224      /* 9600 */
#define      Sb      4      /* 2 stop bits */
#define      Wd      3      /* b bits word length */
#define      Comst      768      /* communication status check */
#define      Reciv      512      /* receive character */
#define      Transm      256      /* transmit character */
#define      Kb_scan      256      /* non-destructive keyboard scan */
#define      Kb_get      0      /* read keyboard buffer */
#define      DR      256      /* rs232 dsr */
#define      Flush      1024      /* ah = 4 */
#define      XONF      768      /* xon/xoff */
#define      CW      23      /* Cntl W */
#define      CNTR      18      /* Cntl R */
#define      CC      03      /* Cntl C */
#define      TR      24576      /* Transmitter register empty */
#define      DATASIZE      15      /* ARRAY SIZE */
#define      FILESIZE      10      /* file name size */
#define      ARBI      15      /* temporary character storage */
#define      CR      13      /* Carriage return */
#define      LF      10      /* Line feed */
#define      H_wipe      255      /* Wipe out higher byte */
#define      ESC      27      /* Escape code */
#define      SUB      26      /* Subtract */

main()
{
    char k,file_name[FILESIZE], mem_loc[DATASIZE], temp[ARBI];
    int a,b,c,d,i,Skip;

    Skip = 0;
    a = Baud;          /* a1 = 11100111, 111 = 9600 baud */
    a = a + Sb;        /* 1 (2^2) = 2 stop bits */
    a = a + Wd;        /* 11 = 8 bits word length */
    d = XONF;          /* dx = 0000011000000000, Xon/Xoff terminal & host */

    a = serial(a,d);   /* reset the serial communication */

    a = Flush;         /* Flush the serial communication */
    a = serial(a,d);

    while(1)
    {
        recicom(&a);
        putchar(a);

        a = Kb_scan;   /* ah =1 */
        KBscan(&a,&b,&d); /* non-destructive keyboard scan */

        if (d == 0)    /* found typed character */
        {
            if (a == CNTR) /* download Intel hex coded prog. */
            {
                printf("\nEnter filename to download:");
                scanf("%s",file_name);
            }
        }
    }
}

```

```

mem_loc[0] = 'R';
mem_loc[1] = ' ';
printf("\nEnter address to send to <seg:offset>:");
scanf("%s",temp);
for(i=0; temp[i] != '\0'; ++i) /* IMPORTANT */
                               /* scanf() places '\0'=0 at the
                               end of the string */
{
    mem_loc[i+2] = temp[i];
}

mem_loc[i+2] = 13;
mem_loc[i+3] = '\0';
printf("down loading information is  %s\n",mem_loc);

sends(mem_loc);

printf("\n\n FILE DOWN LOADING STARTS \n\n");

sendf(file_name);

printf("\n File down-loading complete\n");

a = SUB; /* SUB & ESC sequence terminate downloading */
sendc(a,0);
a = ESC;
sendc(a,0);

Skip = 1; /* Skip the return code check */
}
if (a == CW)
{
    printf("Enter filename to upload:");
    scanf("%s",file_name);
}
if (a == CC) break;

if (Skip == 1)
{
    Skip = 0;
}
else if (Skip == 0)
{
    sendc(a,1);
}
}
}

sends(array)
char array[DATASIZE];
{
    int a,b,i;

    for(i=0; array[i] != '\0'; ++i)

```

```

    {
        b = array[i];
        sendc(b,1); /* printf("%d data of array to be sent is %d",i,b);*/
    }
}

recicom(x)
int *x;
{
    int a,b;

    a = serial(Comst,b);
    if((a & DR) == DR) /* yes ready */
    {
        a = serial(Reciv,b);
        *x = a;
    }
}

sendc(a,echo)
int a,echo;
{
    int b;
    while(1)
    {

        /* printf("\n character to be sent is %d",a);*/

        b = serial(Comst,b);

        /* printf("\n sendc status is %d",b); */

        if ((b & DR) == DR)
        {
            printf("\n found data while tring to transmit %d ",a);
            recicom(&b);
            putchar(b);
        }

        if ((b & TR) != TR) printf("\n Transmitter crowded\n");

        if ((b & TR) == TR)
        {
            b = Transm + a;
            b = serial(b,b);

            if (echo == 1)
            {
                recicom(&b);
                printf("\n OUTLOOP CHECK FOR RETURN %d ",(b & H_wipe));*/
                while (b != a)
                {
                    if ((b == CR) || (b == LF) || (b == '<'))
                    {
                        putchar(b);
                        break;
                    }
                }
                recicom(&b);
                printf("\n INLOOP CHECK FOR RETURN %d ",(b & H_wipe));*/
            }
        }
    }
}

```



```
        }                /* while(b != a) */
    }                /* if (echo == 1) */
    break;          /* get out 'while(1)' loop */
}                /* if ((b & TR) ==TR) */
)                /* while(1) */
)                /* sendc() */

sendf(name)
char name[FILESIZE];
{
    int a,b;
    char c;
    FILE *fp, *fopen();

    fp = fopen(name, "r");

    while((c = getc(fp)) != EOF)
    {
/*      printf("\n down loading information %d %c ",c,c);*/
        sendc((int)c,0);
    }
}
```

```

;
;
;      This program provide basic bios call technic
;
codeseg segment
      assume      cs:codeseg
      public      serial_,KBscan_

serial_ proc      near
      push      bp
      mov       bp,sp
      mov       ax,[bp+4]      ;get first argument
      mov       dx,[bp+6]      ;get second
      int       14h           ;call bios interrupt for RS232

      mov       sp,bp
      pop      bp
      ret

serial_ endp

KBscan_ proc      near           ;non-destructive keyboard scan
      push      bp
      mov       bp,sp
      mov       bx,[bp+4]
      mov       ax,[bx]
      int       16h           ;call non-destructive keyboard
      mov       cx,ax         ;make a copy
      lahf
      and       ax,04000h     ;mask off except 15th bit
      mov       bx,[bp+8]     ;get third argument address
      mov       [bx],ax      ;transfer ax anded result
      cmp       ax,04000h     ;if no character
      jz        back         ;return

      mov       ax,cx         ;copy back
      xor       ch,ch         ;clean up higher byte
      mov       bx,[bp+4]     ;first argument address
      mov       [bx],cx      ;ASCII values of a character
      xor       al,al         ;clean up lower bytes
      mov       bx,[bp+6]     ;second argument address
      mov       [bx],ax      ;keyboard scan code

      mov       ah,03h       ;flush keyboard buffer
      int       16h
back:  mov       sp,bp
      pop      bp
      ret

KBscan_ endp

codeseg ends
end

```

APPENDIX E

MASTER COMPUTER PROGRAM

```

100 CLEAR ,61184! ' BASIC Declarations
110 IBINIT1 = 61184!
120 IBINIT2 = IBINIT1 + 3 ' Lines 1 through 6 MUST be included in your p
130 BLOAD "bib.m",IBINIT1
140 CALL IBINIT1(IBFIND,IBTRG,IBCLR,IBPCT,IBSIC,IBLOC,IBPPC,IBBNA,IBONL,IB
150 CALL IBINIT2(IBGTS,IBCAC,IBWAIT,IBPOKE,IBWRT,IBWRTA,IBCMD,IBCMDA,IBRD,
160 REM Optionally include the following declarations in your program.
170 REM They provide appropriate mnemonics by which
180 REM to reference commonly used values. Some mnemonics (GET%, ERR%,
190 REM END%, ATN%) are preceded by "B" in order to distinguish them from
200 REM BASIC keywords.
210 REM
220 REM GPIB Commands
230 UNL% = &H3F ' GPIB unlisten command
240 UNT% = &H5F ' GPIB untalk command
250 GTL% = &H1 ' GPIB go to local
260 SDC% = &H4 ' GPIB selected device clear
270 PPC% = &H5 ' GPIB parallel poll configure
280 BGET% = &H8 ' GPIB group execute trigger
290 TCT% = &H9 ' GPIB take control
300 LLO% = &H11 ' GPIB local lock out
310 DCL% = &H14 ' GPIB device clear
320 PPU% = &H15 ' GPIB ppoll unconfigure
330 SPE% = &H18 ' GPIB serial poll enable
340 SPD% = &H19 ' GPIB serial poll disable
350 PPE% = &H60 ' GPIB parallel poll enable
360 PPD% = &H70 ' GPIB parallel poll disable
370 REM
380 REM GPIB status bit vector
390 REM global variable IBSTA% and wait mask
400 BERR% = &H8000 ' Error detected
410 TIMO% = &H4000 ' Timeout
420 BEND% = &H2000 ' EOI or EOS detected
430 SRQI% = &H1000 ' SRQ detected by CIC
440 RQS% = &H800 ' Device needs service
450 CMPL% = &H100 ' I/O completed
460 LOK% = &H80 ' Local lockout state
470 REM% = &H40 ' Remote state
480 CIC% = &H20 ' Controller-In-Charge
490 BATN% = &H10 ' Attention asserted
500 TACS% = &H8 ' Talker active
510 LACS% = &H4 ' Listener active
520 DTAS% = &H2 ' Device trigger state
530 DCAS% = &H1 ' Device clear state
540 REM
550 REM Error messages returned in global variable IBERR%
560 EDVR% = 0 ' DOS error
570 ECIC% = 1 ' Function requires board to be CIC
580 ENOL% = 2 ' Write function detected no Listeners
590 EADR% = 3 ' Interface board not addressed correctly
600 EARG% = 4 ' Invalid argument to function call
610 ESAC% = 5 ' Function requires board to be SAC
620 EABO% = 6 ' I/O operation aborted
630 ENEB% = 7 ' Non-existent interface board
640 EOIP% = 10 ' I/O operation started before previous operation compl
650 ECAP% = 11 ' No capability for operation
660 EFSO% = 12 ' File system operation error
670 EBUS% = 14 ' Command error during device call
680 ESTB% = 15 ' Serial poll status byte lost
690 ESRQ% = 16 ' SRQ remains asserted

```

```

700 REM
710 REM EOS mode bits
720 BIN% = &H1000 ' Eight bit compare
730 XEOS% = &H800 ' Send EOI with EOS byte
740 REOS% = &H400 ' Terminate read on EOS
750 REM
760 REM Timeout values and meanings
770 TNONE% = 0 ' Infinite timeout (disabled)
780 T10US% = 1 ' Timeout of 10 us (ideal)
790 T30US% = 2 ' Timeout of 30 us (ideal)
800 T100US% = 3 ' Timeout of 100 us (ideal)
810 T300US% = 4 ' Timeout of 300 us (ideal)
820 T1MS% = 5 ' Timeout of 1 ms (ideal)
830 T3MS% = 6 ' Timeout of 3 ms (ideal)
840 T10MS% = 7 ' Timeout of 10 ms (ideal)
850 T30MS% = 8 ' Timeout of 30 ms (ideal)
860 T100MS% = 9 ' Timeout of 100 ms (ideal)
870 T300MS% = 10 ' Timeout of 300 ms (ideal)
880 T1S% = 11 ' Timeout of 1 s (ideal)
890 T3S% = 12 ' Timeout of 3 s (ideal)
900 T10S% = 13 ' Timeout of 10 s (ideal)
910 T30S% = 14 ' Timeout of 30 s (ideal)
920 T100S% = 15 ' Timeout of 100 s (ideal)
930 T300S% = 16 ' Timeout of 300 s (ideal)
940 T1000S% = 17 ' Timeout of 1000 s (maximum)
950 REM
960 REM Miscellaneous
970 S% = &H8 ' Parallel Poll sense bit
980 LF% = &HA ' Line feed character
990 REM
1000 REM Application program variables passed to
1010 REM GPIB functions
1020 REM
1030 CMD$ = SPACE$(10) ' command buffer
1040 RDS$ = SPACE$(255) ' read data buffer
1050 WRT$ = SPACE$(255) ' write data buffer
1060 BNAME$ = SPACE$(7) ' board name buffer
1070 BDNAME$ = SPACE$(7) ' board or device name buffer
1080 FLNAME$ = SPACE$(50) ' file name buffer
1090 '
1100 '
1110 ' *****
1120 '
1130 REM *****
1140 REM CLOCK.BAS REV. C.1
1150 REM NATIONAL INSTRUMENTS SOFTWARE FOR GPIB-PC2000
1160 REM TIME OF DAY CLOCK (NATIONAL SEMICONDUCTOR MM58167A)
1170 REM (c) Copyright 1985, National Instruments
1180 REM All rights reserved
1190 REM *****
1200 REM
1210 REM GOSUB 10200 ... GETALARM
1220 REM GOSUB 10300 ... SETALARM
1230 REM GOSUB 10400 ... GETCLOCK
1240 REM GOSUB 10500 ... SETCLOCK
1250 REM GOSUB 10600 ... SETFREQ
1260 REM GOSUB 10800 ... OUTCLK
1270 REM
1280 REM *****
1290 REM SUBROUTINE: INITIALIZE PROGRAM VARIABLES

```

```

1300 REM *****
1310 REM
1320 REM REGISTER ADDRESSES
1330 CL.TM.MSEC% = 0
1340 CL.TM.SEC% = 2
1350 CL.TM.MIN% = 3
1360 CL.TM.HR% = 4
1370 CL.TM.DAY% = 5
1380 CL.TM.DATE% = 6
1390 CL.TM.MO% = 7
1400 CL.ALRM.MSEC% = 8
1410 CL.ALRM.CDSEC% = 9
1420 CL.ALRM.SEC% = 10
1430 CL.ALRM.MIN% = 11
1440 CL.ALRM.HR% = 12
1450 CL.ALRM.DAY% = 13
1460 CL.ALRM.DATE% = 14
1470 CL.ALRM.MO% = 15
1480 CL.ISR% = 16
1490 CL.IMR% = 17
1500 CL.CRST% = 18
1510 CL.ARST% = 19
1520 CL.OVFL% = 20
1530 CL.GO% = 21
1540 CL.IE% = 22
1550 DIM TM%(8) ' ARRAY FOR PASSING TIME PARAMETERS TO/FROM SUBROUTINES
1560 MSEC% = 0 ' TEN THOUSANDTHS OF SECONDS
1570 CDSEC% = 1 ' HUNDREDTHS AND TENTHS OF SECONDS
1580 SEC% = 2 ' SECONDS
1590 MIN% = 3 ' MINUTES
1600 HR% = 4 ' HOURS
1610 DAY% = 5 ' DAY OF THE WEEK
1620 DATE% = 6 ' DAY OF THE MONTH
1630 MO% = 7 ' MONTH
1640 YR% = 8 ' YEAR
1650 REM REGISTER ADDRESSES
1660 ISR% = 0 ' INTERRUPT STATUS REGISTER
1670 IMR% = 1 ' INTERRUPT MASK (CONTROL) REGISTER
1680 CRST% = 2 ' COUNTER RESET
1690 ARST% = 3 ' ALARM RESET (RAM)
1700 OVFL% = 4 ' OVERFLOW (STATUS) BIT
1710 GO% = 5 ' GO COMMAND - USED FOR PRECISE STARTING OF CLOCK
1720 IE% = 6 ' INTERRUPT ENABLE (STANDBY INTERRUPT)
1730 REM CLOCK CONTROL REGISTERS
1740 CCR% = &H81E ' CLOCK CONTROL REGISTER
1750 CDR% = &H81C ' CLOCK DATA REGISTER
1760 IE% = &H20 ' INTERRUPT ENABLE (master and separate bits) (5&6)
1770 RESULT% = 0
1780 REM ***** ASSEMBLY LANGUAGE ROUTINES STORED AS DATA *****
1790 DIM ASM%(66)
1800 DATA &H5590, &Hec8b, &H5e8b, &Hba06, &H0000, &H68e8, &H8800, &Hba07
1810 DATA &H0001, &H60e8, &H8800, &H0247, &H02ba, &He800, &H0057, &H4788
1820 DATA &Hba04, &H0003, &H4ee8, &H8800, &H0647, &H04ba, &He800, &H0045
1830 DATA &H4788, &Hba08, &H0005, &H3ce8, &H8800, &H0a47, &H06ba, &He800
1840 DATA &H0033, &H4788, &Hba0c, &H0007, &H2ae8, &H8800, &H0e47, &H14ba
1850 DATA &He800, &H0021, &Hc084, &Haf75, &He58b, &Hca5d, &H0002, &H5590
1860 DATA &Hec8b, &H5e8b, &H8b08, &He817, &H000b, &H5e8b, &H8806, &H8b07
1870 DATA &H5de5, &H04ca, &H8a00, &Hbac2, &H081e, &Hbaee, &H081c, &Hc3ec
1880 DATA &Hcbfa, &Hcbfb
1890 FOR I = 0 TO 65

```

```

1900 READ ASM%(I)
1910 NEXT I
1920 '
1930     BDNAME$ = "DEV1"
1940     CALL    IBFIND(BDNAME$,DEV1%)
1950     BDNAME$ = "GPIB0"
1960     CALL    IBFIND(BDNAME$,GPIB0%)
1970     '
1980     CALL    IBCLR(GPIB0%)
1990     '
2000     IF DEV1% < 0 THEN PRINT"ERROR WITH DEV1  ":STOP
2010     GOTO 5760
2020     '
2030     '
2040     *****
2050     '
2060     '
2070     REM
2080     REM *****
2090     REM SUBROUTINE:  GETALARM
2100     REM     RETURN THE ALARM SETTING IN TM.
2110     REM *****
2120     LOCKOUT = VARPTR(ASM%(64))
2130     CALL LOCKOUT           ' LOCK OUT INTERRUPTS
2140     A% = CL.ALRM.SEC%
2150     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(SEC%))
2160     A% = CL.ALRM.MIN%
2170     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(MIN%))
2180     A% = CL.ALRM.HR%
2190     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(HR%))
2200     A% = CL.ALRM.DAY%
2210     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(DAY%))
2220     A% = CL.ALRM.DATE%
2230     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(DATE%))
2240     A% = CL.ALRM.MO%
2250     INCLK = VARPTR(ASM%(47)) : CALL INCLK(A%,TM%(MO%))
2260     TM%(MSEC%) = 0
2270     TM%(CDSEC%) = 0
2280     TM%(YR%) = 0
2290     UNLOCK = VARPTR(ASM%(65))
2300     CALL UNLOCK           ' RESTORE INTERRUPTS
2310     RETURN
2320     REM
2330     REM *****
2340     REM SUBROUTINE:  SETALARM
2350     REM     SET THE ALARM TIME AS INDICATED BY TM.
2360     REM     NOTE: THE USER MUST SET UP INTERRUPT 23 BEFORE
2370     REM     CALLING THIS FUNCTION
2380     REM *****
2390     LOCKOUT = VARPTR(ASM%(64))
2400     CALL LOCKOUT           ' LOCK OUT INTERRUPTS
2410     IF (TM%(YR%) <> 0) THEN GOTO 2470
2420     IESTATE% = 0
2430     A% = CL.IMR%
2440     D% = 0
2450     GOSUB 3690             ' OUTCLK
2460     GOTO 2690
2470     A% = CL.ALRM.SEC%
2480     D% = TM%(SEC%)
2490     GOSUB 3690             ' OUTCLK

```

```

2500 A% = CL.ALRM.MIN%
2510 D% = TM% (MIN%)
2520 GOSUB 3690 ' OUTCLK
2530 A% = CL.ALRM.HR%
2540 D% = TM% (HR%)
2550 GOSUB 3690 ' OUTCLK
2560 A% = CL.ALRM.DAY%
2570 D% = &HCC
2580 GOSUB 3690 ' OUTCLK
2590 A% = CL.ALRM.DATE%
2600 D% = TM% (DATE%)
2610 GOSUB 3690 ' OUTCLK
2620 A% = CL.ALRM.MO%
2630 D% = TM% (MO%)
2640 GOSUB 3690 ' OUTCLK
2650 IESTATE% = IE%
2660 A% = CL.IMR%
2670 D% = 1
2680 GOSUB 3690 ' OUTCLK
2690 UNLOCK = VARPTR(ASM%(65))
2700 CALL UNLOCK ' RESTORE INTERRUPTS
2710 RETURN
2720 REM
2730 REM *****
2740 REM SUBROUTINE: GETCLOCK
2750 REM PUT THE CURRENT DAY, DATE AND TIME IN TM.
2760 REM *****
2770 LOCKOUT = VARPTR(ASM%(64))
2780 CALL LOCKOUT ' LOCK OUT INTERRUPTS
2790 INCLOCK = VARPTR(ASM%(0))
2800 CALL INCLOCK(TM%(0))
2810 A% = CL.ALRM.CDSEC% OR IESTATE%
2820 INCLK = VARPTR(ASM%(47))
2830 CALL INCLK(A%, RESULT%)
2840 RESULT% = RESULT% AND &H33
2850 PRINT "result & h33", HEX$(RESULT%)
2860 TM%(YR%) = ((RESULT% \ 4) OR RESULT%) AND &HF
2870 A% = CL.ALRM.MSEC
2880 INCLK = VARPTR(ASM%(47))
2890 CALL INCLK(A%, RESULT%)
2900 IF ((TM%(MO%) > 6) OR NOT (RESULT% AND &H20)) THEN GOTO 2950
2910 TM%(YR%) = TM%(YR%) + 1
2920 D% = ((TM%(YR%) * 4) OR TM%(YR%)) OR &HCC
2930 A% = CL.ALRM.CDSEC%
2940 GOSUB 3690 ' OUTCLK
2950 A% = CL.ALRM.MSEC%
2960 IF TM%(MO%) <= 6 THEN GOTO 2990
2970 D% = &HE0
2980 GOTO 3000
2990 D% = &HCO
3000 GOSUB 3690 ' OUTCLK
3010 UNLOCK = VARPTR(ASM%(65))
3020 CALL UNLOCK ' RESTORE INTERRUPTS
3030 RETURN
3040 REM
3050 REM *****
3060 REM SUBROUTINE: SETCLOCK
3070 REM SET THE CLOCK TO THE TIME INDICATED BY TM.
3080 REM *****
3090 LOCKOUT = VARPTR(ASM%(64))

```



```

3100 CALL LOCKOUT          ' LOCK OUT INTERRUPTS
3110 A% = CL.CRST%
3120 D% = &HFF
3130 GOSUB 3690          ' OUTCLK
3140 A% = CL.TM.MSEC%
3150 D% = 0
3160 GOSUB 3690          ' OUTCLK
3170 A% = CL.TM.CDSEC%
3180 D% = 0
3190 GOSUB 3690          ' OUTCLK
3200 A% = CL.TM.SEC%
3210 D% = TM% (SEC%)
3220 GOSUB 3690          ' OUTCLK
3230 A% = CL.TM.MIN%
3240 D% = TM% (MIN%)
3250 GOSUB 3690          ' OUTCLK
3260 A% = CL.TM.HR%
3270 D% = TM% (HR%)
3280 GOSUB 3690          ' OUTCLK
3290 A% = CL.TM.DAY%
3300 D% = TM% (DAY%)
3310 GOSUB 3690          ' OUTCLK
3320 A% = CL.TM.DATE%
3330 D% = TM% (DATE%)
3340 GOSUB 3690          ' OUTCLK
3350 A% = CL.TM.MO%
3360 D% = TM% (MO%)
3370 GOSUB 3690          ' OUTCLK
3380 A% = CL.ALRM.CDSEC%
3390 D% = ((TM%(YR%) * 4) OR TM%(YR%)) OR &HCC
3400 GOSUB 3690          ' OUTCLK
3410 A% = CL.ALRM.MSEC%
3420 IF (TM% (MO%) <= 6) THEN GOTO 3450
3430 D% = &HE0
3440 GOTO 3460
3450 D% = &HCO
3460 GOSUB 3690          ' OUTCLK
3470 UNLOCK = VARPTR(ASM%(65))
3480 CALL UNLOCK          ' RESTORE INTERRUPTS
3490 RETURN
3500 REM
3510 REM *****
3520 REM SUBROUTINE:  SETFREQ
3530 REM   SET THE PERIODIC INTERRUPT FREQUENCY
3540 REM   ACCORDING TO THE BITS IN N.
3550 REM *****
3560 LOCKOUT = VARPTR(ASM%(64))
3570 CALL LOCKOUT          ' LOCK OUT INTERRUPTS
3580 A% = CL.IMR%
3590 IF N% = 0 THEN GOTO 3620          ' SET/CLEAR IE ON NEXT IN/OUT CALL
3600 IESTATE% = 0
3610 GOTO 3630
3620 IESTATE% = IE%
3630 D% = N%
3640 GOSUB 3690          ' OUTCLK
3650 UNLOCK = VARPTR(ASM%(65))
3660 CALL UNLOCK          ' RESTORE INTERRUPTS
3670 RETURN
3680 REM
3690 REM =====

```

```

3700 REM SUBROUTINE: OUTCLK
3710 REM WRITE DATA IN D% TO CLOCK REGISTER A%.
3720 REM =====
3730 REM
3740 OUT CCR%, A% OR IESTATE%
3750 OUT CDR%, D%
3760 RETURN
3770 ' *****
3780 '
3790 ' *****
3800 '
3810 ' INTEGER READ ROUTINE
3820 '
3830 ' WRT$ CONTAINS THE NECESSARY COMMAND & DATA
3840 ' MASK% CONTAINS PROCESS CHECK
3850 ' CALL IBWRT(DEV1%,WRT$)
3860 ' CALL IBWAIT(DEV1%,MASK%)
3870 ' RETURN
3880 '
3890 ' *****
3900 '
3910 ' *****
3920 '
3930 ' INTEGER READ ROUTINE
3940 '
3950 ' RD% IS AN ARRAY
3960 ' CNT% = # OF BYTES TO BE READ
3970 '
3980 ' CALL IBRDI(DEV1%,RD%(M%),CNT%)
3990 ' CALL IBWAIT(DEV1%,MASK%)
4000 ' RETURN
4010 '
4020 ' *****
4030 '
4040 ' *** STRICT 2 BYTES ONLY *****
4050 '
4060 ' CALL IBRDI(DEV1%,RD%(0),CN%)
4070 ' CALL IBWAIT(DEV1%,MASK%)
4080 ' RETURN
4090 '
4100 ' *****
4110 '
4120 ' *****
4130 '
4140 ' ASCII READ ROUTINE
4150 '
4160 ' RD$ IS AN 255 BYTES CHARACTER STORAGE
4170 '
4180 ' CALL IBRD(DEV1%,RD$)
4190 ' CALL IBWAIT(DEV1%,MASK%)
4200 ' RETURN
4210 '
4220 ' *****
4230 '
4240 ' ***** CONTROL OUTPUT *****
4250 '
4260 ' HIGH% = INT(SERVO%/FULL%)
4270 ' LOW% = SERVO% - HIGH%*FULL%
4280 ' WRT$=CHR$(1)+CHR$(1)+CHR$(LOW%)+CHR$(HIGH%)
4290 ' GOSUB 3850:RETURN

```

```

4300 '
4310 ' *****
4320 '
4330 ' ***** COMPLETE STOP *****
4340 '
4350     SERVO% = MIDDLE%
4360     GOSUB 4250:PRINT" SERVO STOP "
4370 '
4380 '
4390     PASS% = 0
4400 '
4410 '
4420     WRT$ = ATD2$
4430     GOSUB 3850:GOSUB 4050
4440     DOLD% = RD%(0)
4450     FOR L% = 1 TO 10
4460         WRT$ = ATD2$
4470         GOSUB 3850:GOSUB 4050
4480         PRINT" CURRENT P";RD%(0)
4490         DNEW% = RD%(0)
4500         DIF%(L%) = ABS(DOLD%-DNEW%)
4510         IF DIF%(L%) >= 4 THEN PASS% = 1
4520         DIF%(L%)=0
4530         DOLD% = DNEW%
4540     NEXT L%
4550 '
4560     IF PASS% > 0 THEN PRINT" NOT PASS ":GOTO 4390
4570 '
4580     PRINT"COMPLETE STOP !!! "
4590     RETURN
4600 '
4610 ' *****
4620 '
4630 ' ***** POSITION CONTROL *****
4640 '
4650     PRINT"ENTER POSITION CONTROL"
4660     GOSUB 4340      :' COMPLETE STOP
4670 '
4680     WRT$ = ATD11$:M% = UP%           :' FIRST 3 BYTES CAN NOT BE USED
4690     GOSUB 3850:GOSUB 3970
4700     PRINT" TAKE A LOOK ";RD%(M%),RD%(M%+1),RD%(M%+2)
4710     STOP
4720     M% = M% + UP%
4730 '
4740 '
4750     SERVO%= NULL% + INC% * DIR%     :' INITIAL INPUT
4760     GOSUB 4250
4770 '
4780     WRT$ = ATD10$                   :' GET NEW POSITION
4790     GOSUB 3850:GOSUB 3970
4800     DNEW% = RD%(M%)
4810     PRINT"TARGET ";SETL%,"CURRENT ";RD%(M%),"SERVO ";SERVO%
4820 '
4830     M% = M% + UP%
4840 '
4850 '
4860     IF ABS(DNEW% - DOLD%) <= 50 THEN SERVO% = SERVO% + DIR%:GOSUB 4250:GOT
4870     PRINT"MOVING"
4880 '
4890     WRT$ = ATD10$

```

```

4900 GOSUB 3850:GOSUB 3970
4910 M% = M% + UP%
4920 PRINT"SET TARGET ";SETL%,"CURRENT ";RD%(M%),"SERVO ";SERVO%
4930 '
4940 IF ABS(SETL% - RD%(M%-UP%)) >= LIMITP% THEN 4890
4950 M% = M% + UP%
4960 '
4970 GOSUB 4340:'COMPLETE STOP
4980 '
4990 FOR I%=0 TO M%-UP%:PRINT I%,RD%(I%),RD%(I%+1),RD%(I%+2):NEXT I%
5000 STOP
5010 '
5020 '
5030 RETURN
5040 '
5050 *****
5060 '
5070 ***** MIN & MAX POSITION *****
5080 '
5090 PRINT"ENTER MIN & MAX ROUTINE"
5100 SERVO% = NULL% + INC%
5110 GOSUB 4250
5120 '
5130 WRT$ = ATD2$
5140 GOSUB 3850:GOSUB 4050
5150 DNEW% = RD%(0)
5160 IF ABS(DNEW% - DOLD%) <= LIMIT% THEN SERVO% = SERVO% + 1:GOTO 5110
5170 PRINT"MOVING"
5180 '
5190 CK% = 0:CK1% = 0:UD% = 0:NO%=0
5200 WRT$ = ATD2$
5210 GOSUB 3850:GOSUB 4050
5220 '
5230 MAX% = RD%(0)
5240 MINI% = RD%(0)
5250 PRINT"MIN ";MINI%,"MAX ";MAX%
5260 '
5270 WRT$ = ATD2$
5280 GOSUB 3850:GOSUB 4050
5290 IF RD%(0) > MAX% THEN MAX% = RD%(0):CK% = 1
5300 IF RD%(0) < MINI% THEN MINI% = RD%(0):CK% = -1
5310 IF CK% <> CK1% THEN CK1% = CK%:UD% = UD% + 1
5320 NO% = NO% + 1
5330 PRINT"MIN ";MINI%,"MAX ";MAX%,"CK ";CK%,"CK1 ";CK1%,"UD ";UD%,"NO ";NO%
5340 IF (UD% >= 3) OR (NO% > 150) THEN RETURN
5350 '
5360 GOTO 5270
5370 '
5380 *****
5390 '
5400 ***** STATIONARY TIME *****
5410 '
5420 SETTIME% = 10
5430 CLS
5440 HOUR%=0:INCMIN%=0
5450 GOSUB 2730
5460 INITMIN% = VAL(HEX$(TM%(MIN%)))
5470 INITSEC% = VAL(HEX$(TM%(SEC%)))
5480 INITSEC% = INITSEC% + SETTIME%
5490 IF INITSEC% > 60 THEN INCMIN% =INT(INITSEC% / 60)

```

```

5500  INITMIN% = INITMIN% + INCMIN%
5510  INITSEC% = INITSEC% - 60 * INCMIN%
5520  IF INITMIN% > 59 THEN HOUR% =INT(INITMIN% / 60)
5530  INITMIN% = INITMIN% - HOUR% * 60
5540  '
5550  GOSUB 2730
5560  '
5570  INTERMIN% = VAL(HEX$(TM%(MIN%)))
5580  INTERSEC% = VAL(HEX$(TM%(SEC%)))
5590  '
5600  TESTMIN% = INITMIN% - INTERMIN% + HOUR% * 60
5610  TESTSEC% = INITSEC% - INTERSEC%
5620  '
5630  IF TESTMIN% < 0 THEN TESTMIN% = TESTMIN% + 60
5640  IF TESTSEC% < 0 THEN TESTSEC% = TESTSEC% + 60:TESTMIN%=TESTMIN%-1
5650  '
5660  '
5670  LOCATE 5,10:PRINT TESTMIN% * 60 + TESTSEC%;" sec "
5680  IF INITMIN% =INTERMIN% AND INTERSEC%=INITSEC% THEN RETURN
5690  '
5700  GOTO 5550
5710  '
5720  '
5730  *****
5740  '
5750  ***** MAIN ROUTIN *****
5760  '
5770  CNT% = 6:CN% = 2
5780  MASK% = &H100
5790  DIM RD$(1000),DIF$(10)
5800  SETL% = 1560:' MIDDLE POSITION
5810  TOP% = 2000
5820  BOTTOM% = 1200
5830  FULL% = 256
5840  LIMIT% = 10
5850  LIMITP% = 15
5860  NULL% = 2048
5870  '
5880  INTERRUPT% = 0
5890  MIDDLE%=2048
5900  GOUP%=2100
5910  GODOWN%=1950
5920  INC% = 50
5930  UP% = 3
5940  '
5950  ATD0$ = CHR$(0)+CHR$(0)+CHR$(1)+CHR$(0)
5960  ATD2$ = CHR$(0)+CHR$(2)+CHR$(1)+CHR$(0)
5970  DTAS$ = CHR$(1)+CHR$(1)+CHR$(LOW%)+CHR$(HIGH%)
5980  FC$ = CHR$(16)
5990  IOFF$ = CHR$(18)+CHR$(31):' 31-OFF, 30-ON
6000  ION$ = CHR$(18)+CHR$(30)
6010  ATD10$ = CHR$(10)
6020  ATD11$ = CHR$(11)
6030  '
6040  ATD12$=CHR$(12)+CHR$(144)+CHR$(1)
6050  ADBASE$=CHR$(13)+CHR$(100)+CHR$(0)
6060  ATD13$(0)=ADBASE$+CHR$(0)+CHR$(0)
6070  ATD13$(1)=ADBASE$+CHR$(100)+CHR$(0)
6080  ATD13$(2)=ADBASE$+CHR$(200)+CHR$(0)
6090  ATD13$(3)=ADBASE$+CHR$(44)+CHR$(1)

```

```

6100 '
6110 '
6120 WRT$ = IOFF$
6130 GOSUB 3850:PRINT "CLOSE L-VALVE"
6140 '
6150 GOSUB 4340 : 'COMPLETE STOP
6160 '
6170 INPUT"WHAT PRESSURE (PSI)";PRESSURE
6180 INPUT"STATIONARITY TIME (SEC)";SETTIME%
6190 '
6200 GOSUB 5080 : ' MIN MAX POSITION SEARCH
6210 '
6220 PRINT"FINAL MAX IS ";MAX%,"FINAL MIN IS ";MINI%,"NO ";NO%
6230 '
6240 IF MAX%-MIN% <300 THEN 6190:' REPEAT
6250 '
6260 '
6270 GOSUB 4340 : ' COMPLETE STOP
6280 '
6290 WRT$ = ATD2$
6300 GOSUB 3850:GOSUB 4050
6310 IF ABS(MAX% - RD%(0)) <= LIMIT% THEN PRINT"ALREADY AT THE TOP":GOTO 637
6320 '
6330 PRINT"NOW POSITION CONTROL FOR TOP POSITION "
6340 SETL% = MAX%:DIR% = 1
6350 GOSUB 4640:PRINT"SPOOL AT THE TOP"
6360 '
6370 SETL% = MINI%:DIR% = -1 : ' SET SPOOL AT THE BOTTOM
6380 GOSUB 4640:PRINT"SPOOL AT THE BOTTOM"
6390 '
6400 WRT$ = ION$
6410 GOSUB 3850:PRINT"LEAKAGE-VALVE OPEN"
6420 '
6430 GOSUB 5410 : ' TIMER
6440 '
6450 WRT$ = IOFF$
6460 GOSUB 3850:PRINT"LEAKAGE VALVE CLOSED"
6470 '
6480 WRT$=ATD12$ : 'TAP INTERRUPT
6490 GOSUB 3850
6500 '
6510 '
6520 SETL% = MAX%:DIR%=1
6530 GOSUB 4640
6540 PRINT"SPOOL AT THE TOP"
6550 '
6560 '
6570 CNT%=400
6580 FOR J=0 TO 3
6590 WRT$=ATD13$(J)
6600 GOSUB 3850
6610 M%=J*200
6620 GOSUB 3970
6630 NEXT J
6640 '
6650 CNT%=6
6660 '
6670 '
6680 GOSUB 2730
6690 FILENAME$="B:"+"A"+HEX$(TM%(DATE%))+HEX$(TM%(HR%))+HEX$(TM%(MIN%))+".S"

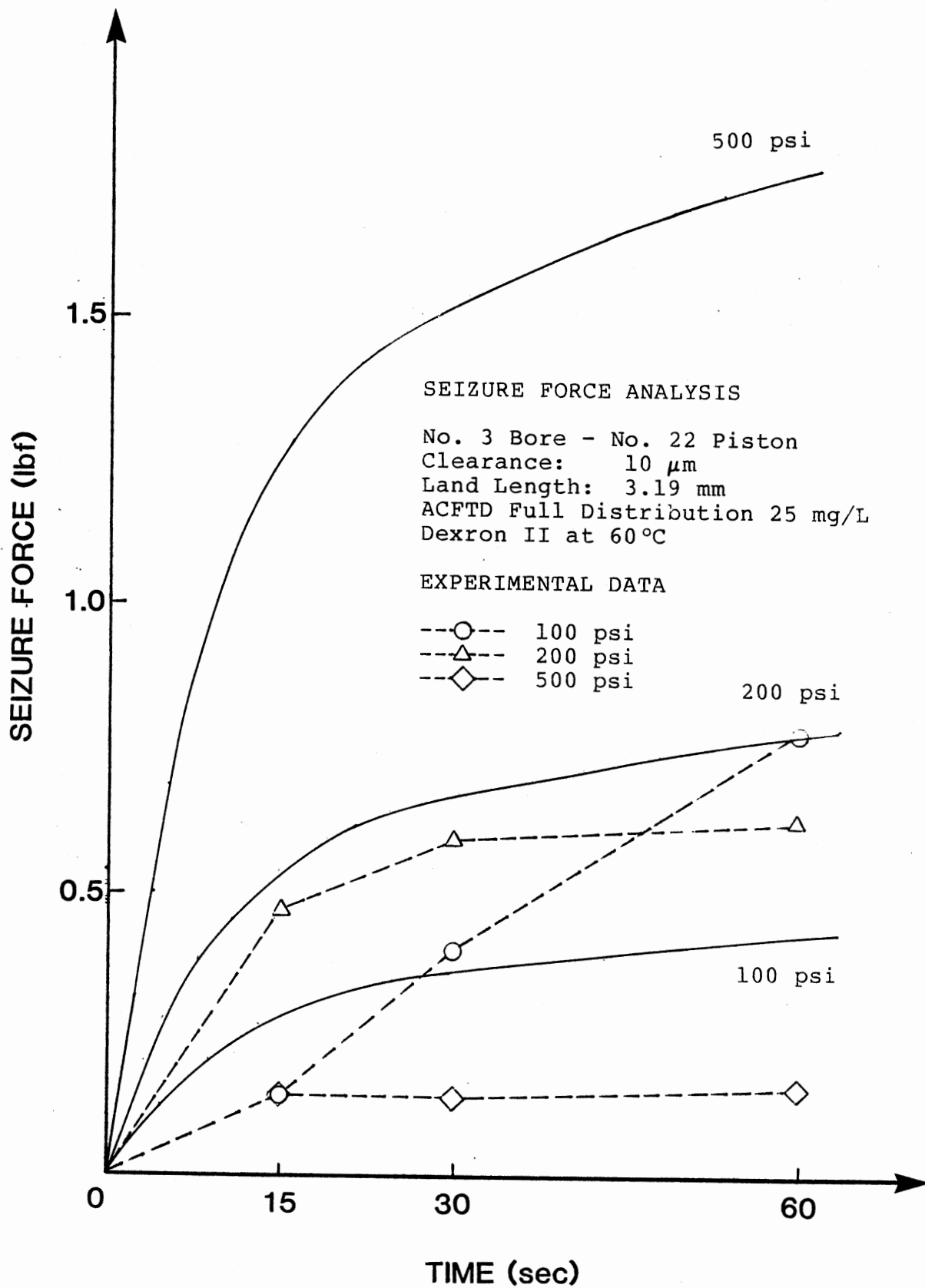
```

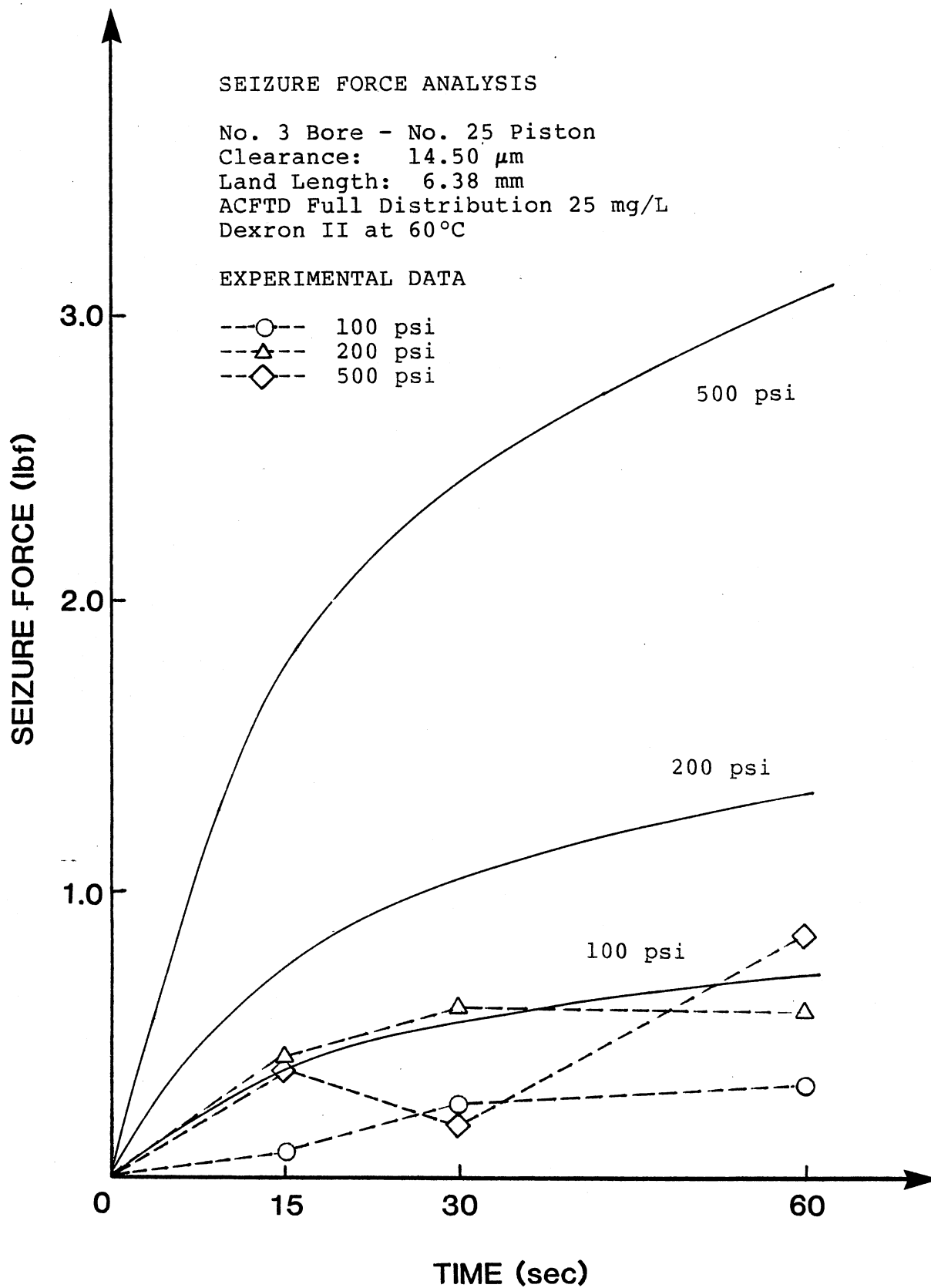
```
6700 PRINT"FILE IS ";FILENAME$
6710 '
6720 OPEN "R",1,FILENAME$,4
6730 FIELD 1,2 AS P$,2 AS F$
6740 '
6750 FOR I% = 0 TO 799 STEP 2
6760     LSET P$=MKI$(RD%(I%))
6770     LSET F$=MKI$(RD%(I%+1))
6780     PUT 1,INT((I%+1)/2)+1
6790 NEXT I%
6800 '
6810 CLOSE 1
6820 '
6830 PRINT"DATA STORED UNDER FILENAME ";FILENAME$
6840 LPRINT"FILENAME ";FILENAME$,"PRESSURE ";PRESSURE;" PSI","TIME ";SETTIM
6850 INPUT"WOULD YOU LIKE TO SEE THE GRAPH OF THIS RESULT ";A$
6860 IF A$ = "Y" OR A$ = "y" THEN RUN"B:GRAPH.BAS"
6870 IF A$ ="N" OR A$ = "n" THEN 6170
6880 GOTO 6850
6890 '
6900 ' GOTO 5960
6910 '
6920 '

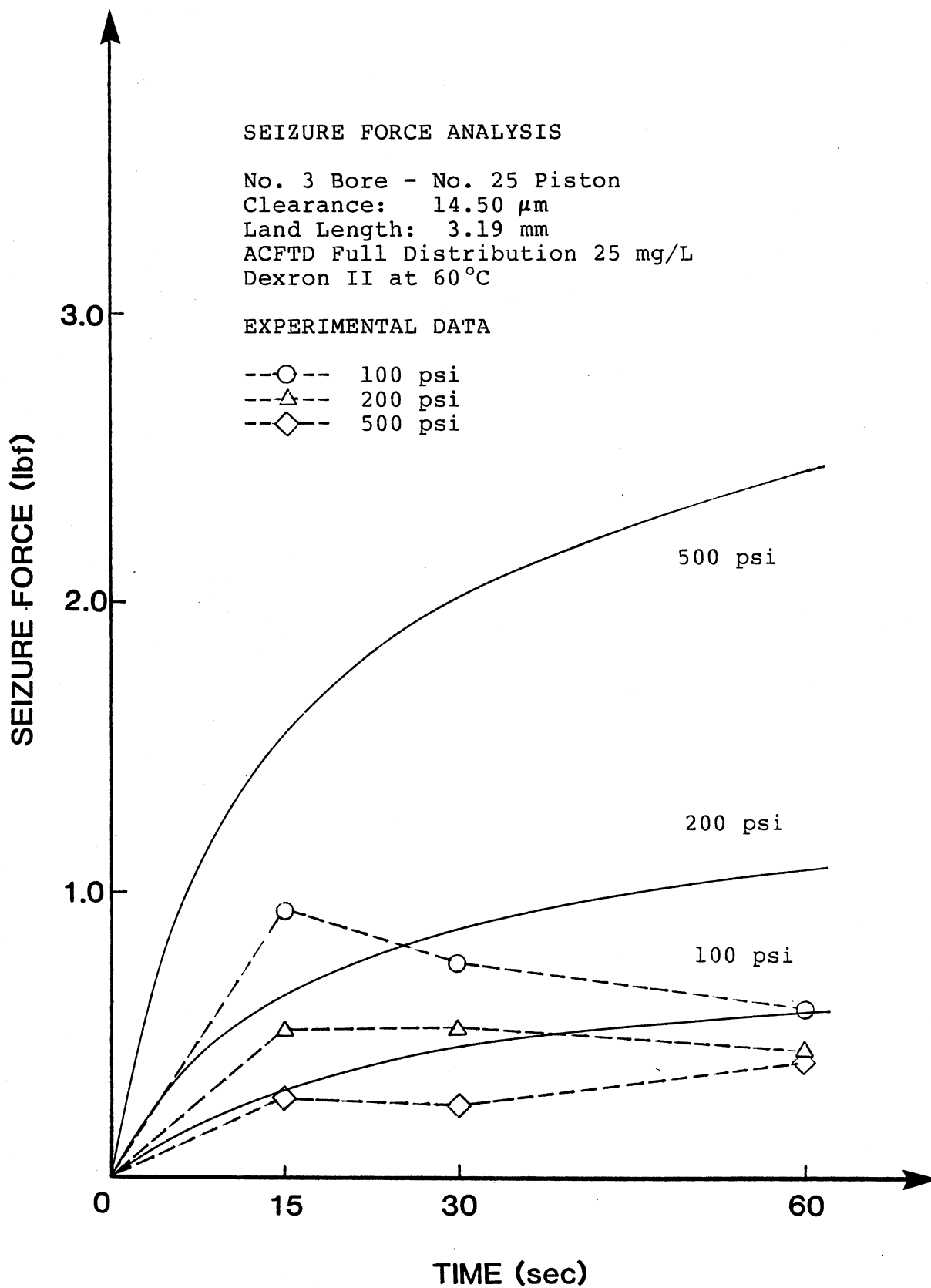
```

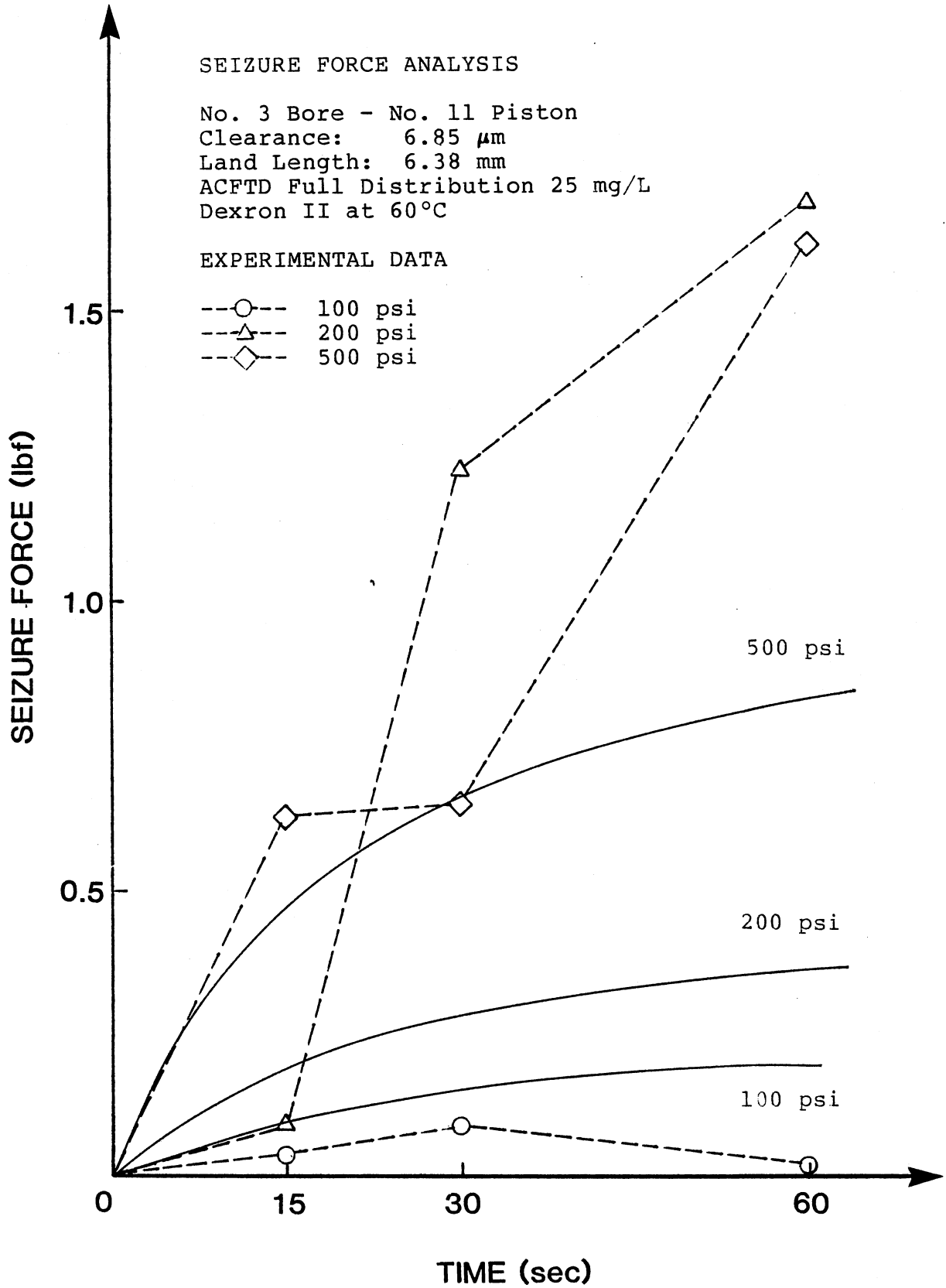
APPENDIX F

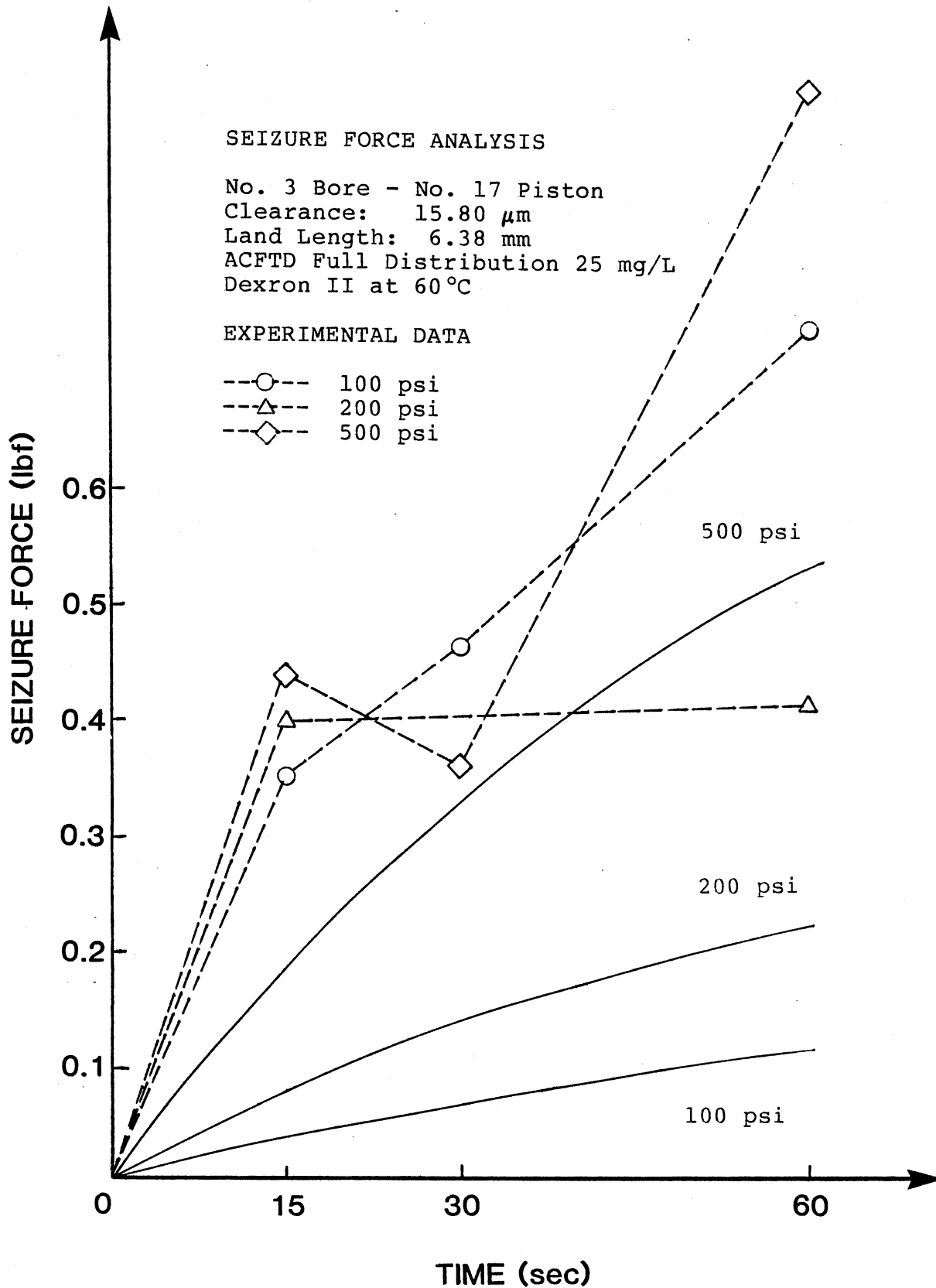
SEIZURE FORCE ANALYSIS

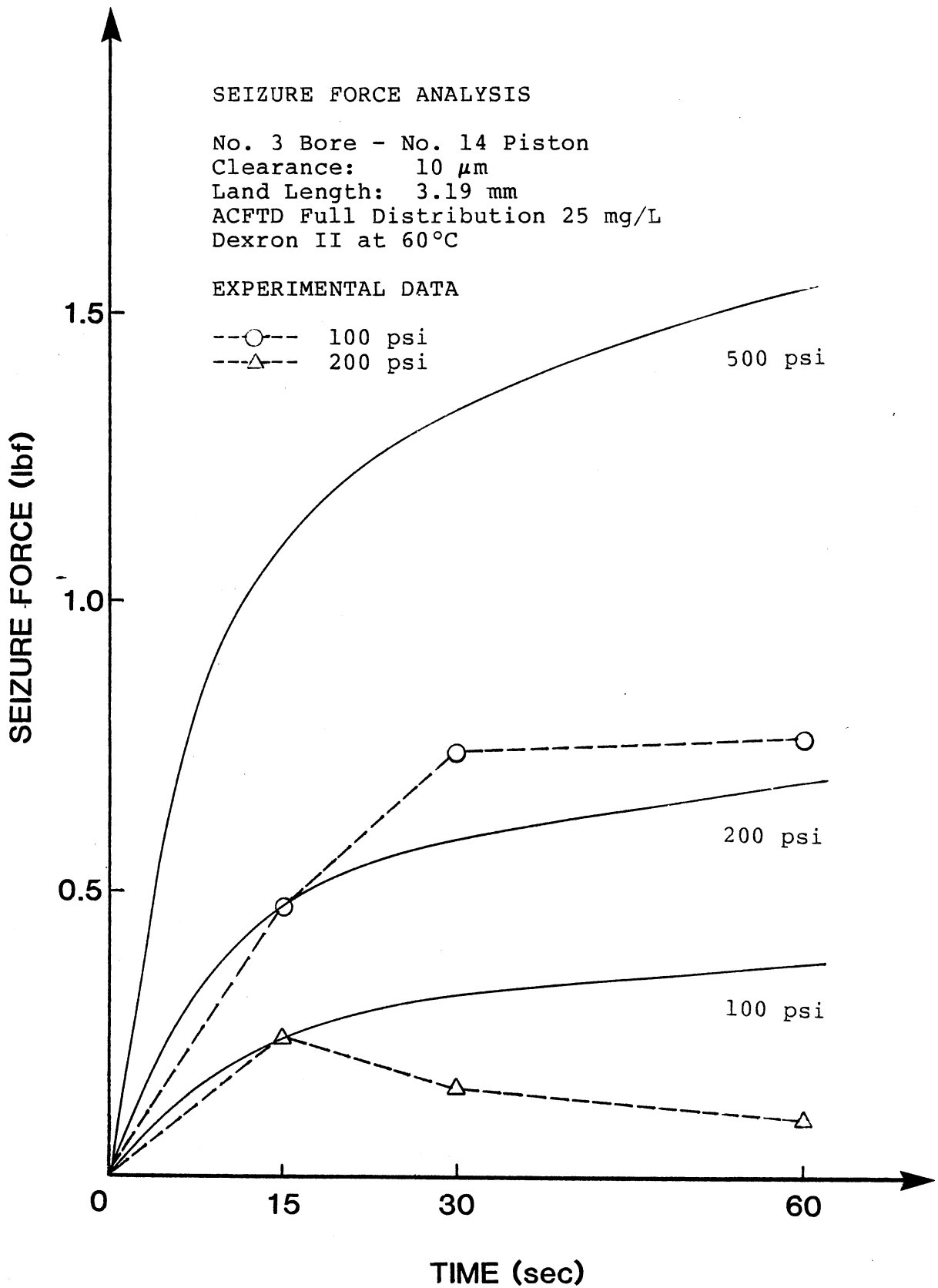


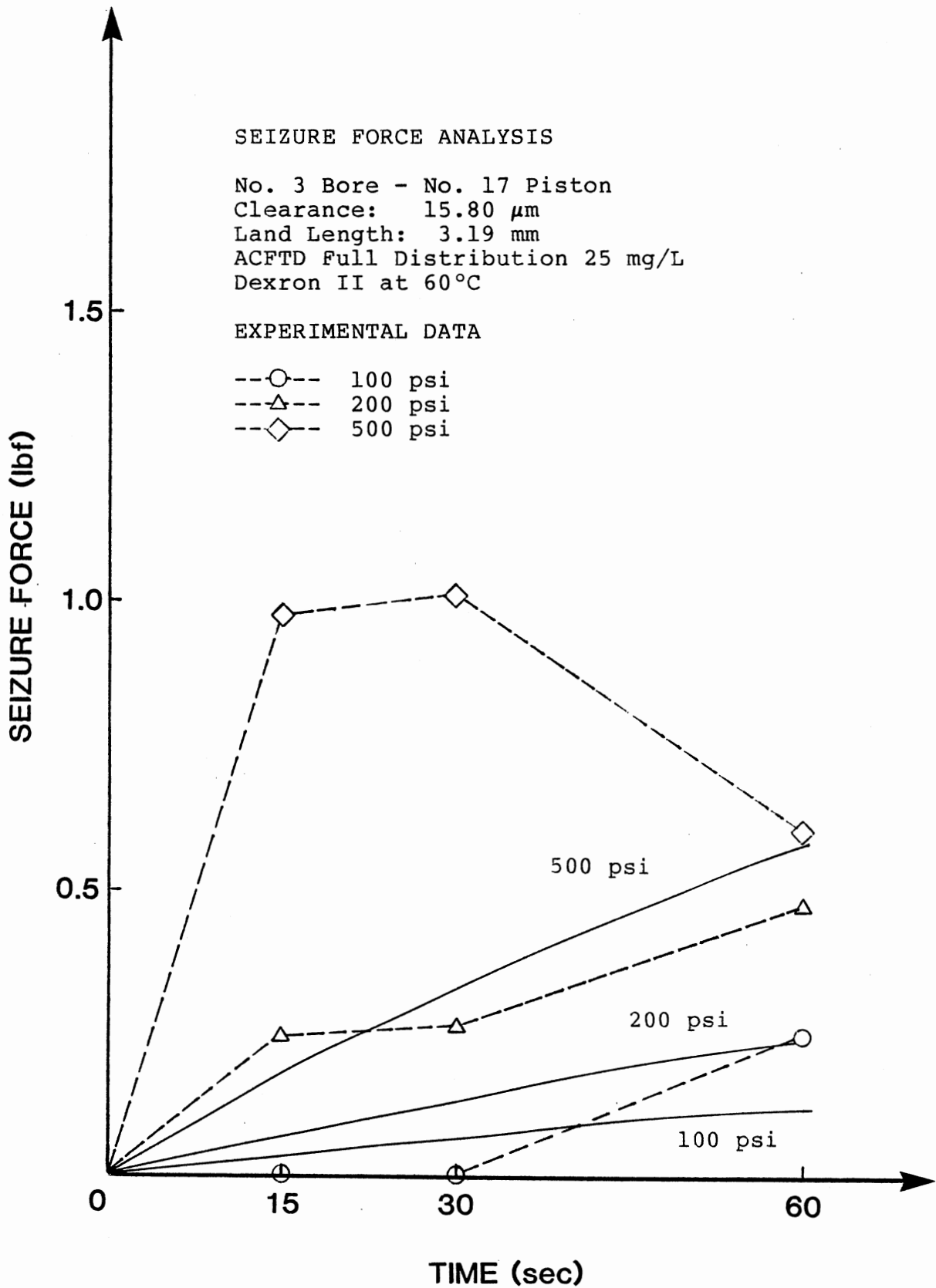


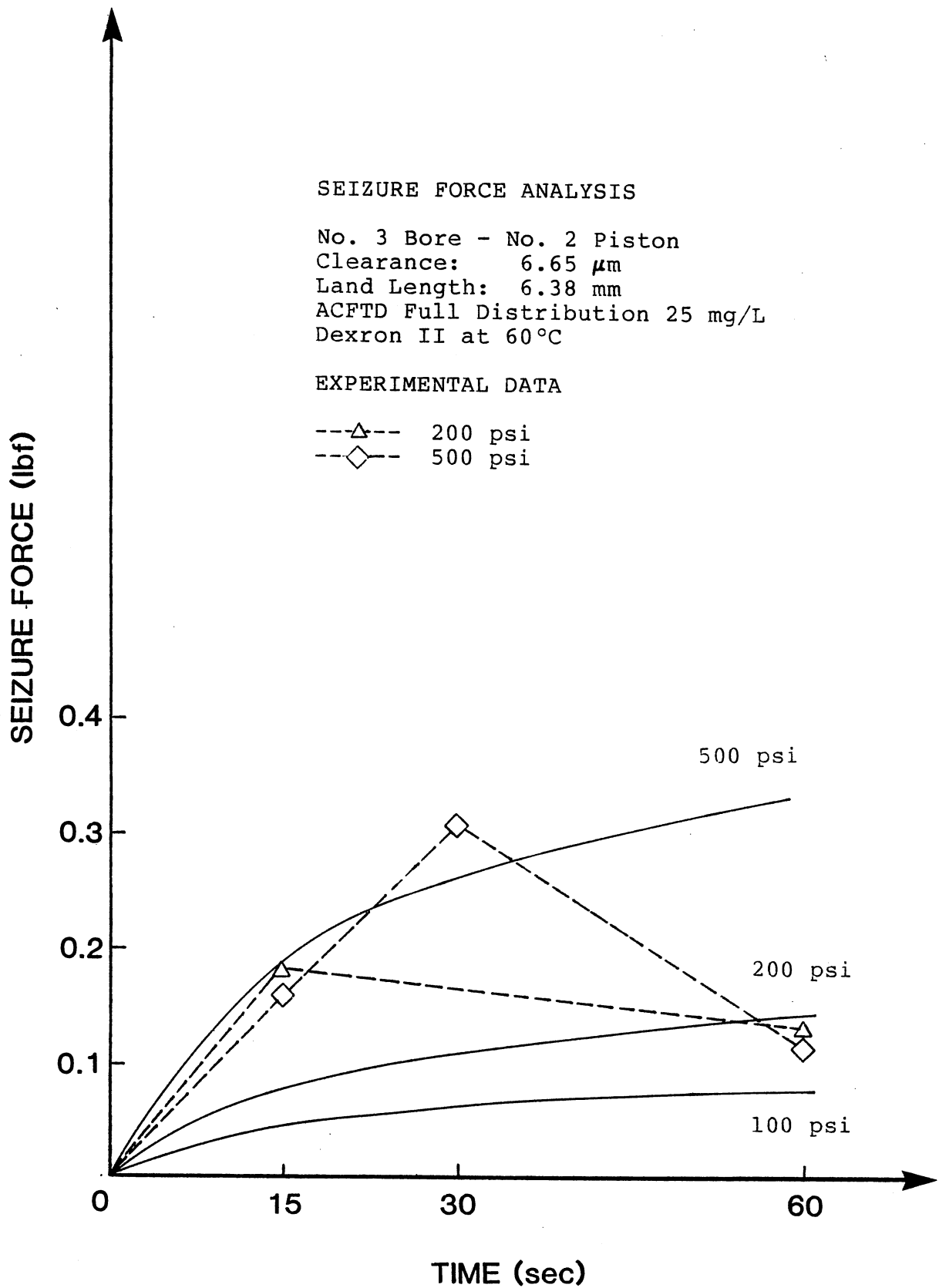


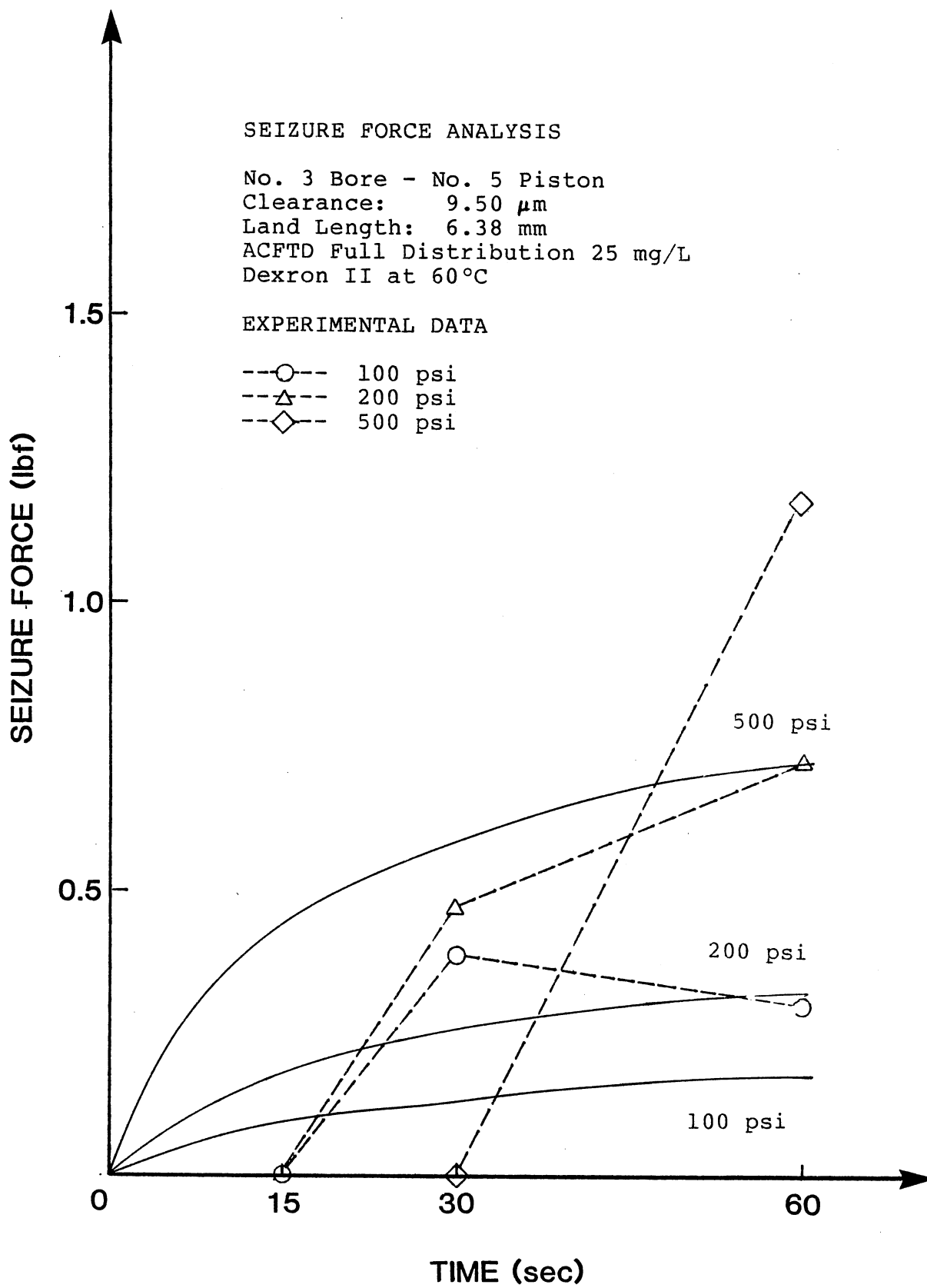


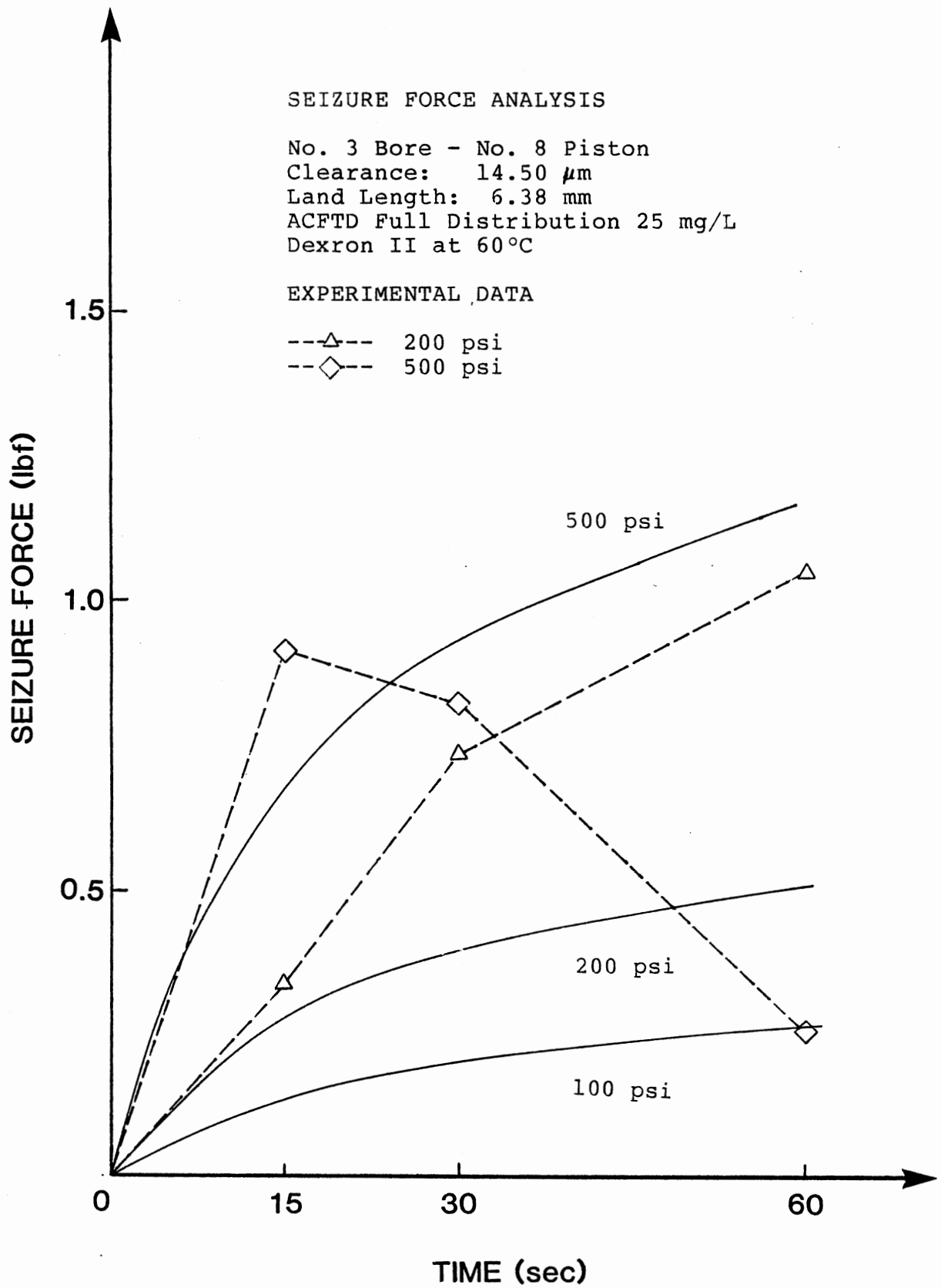


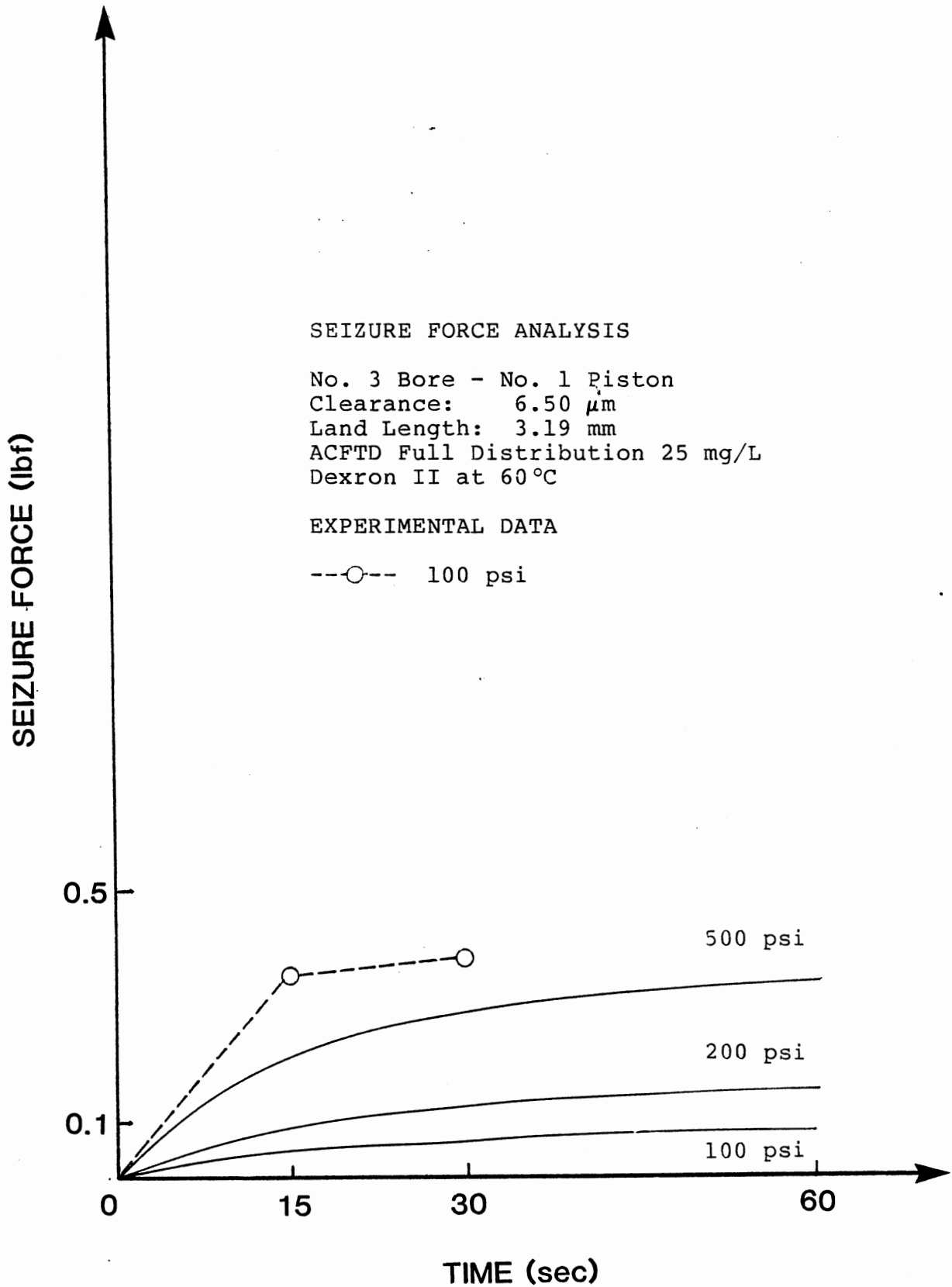


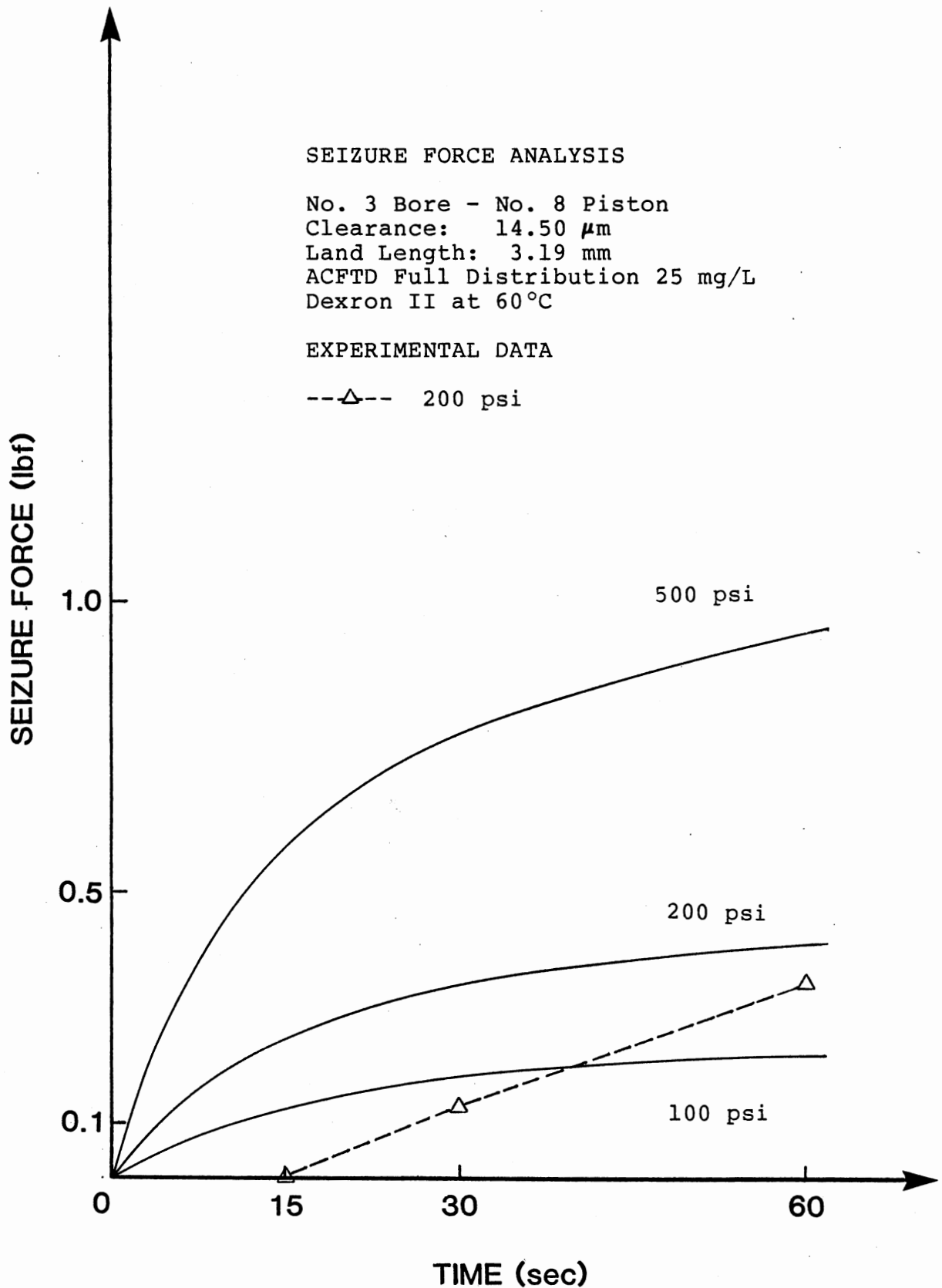












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